



(12)

Oversættelse af
europæisk patentskriftPatent- og
Varemærkestyrelsen

(51) Int.Cl.: **F 16 J 15/08 (2006.01)** **B 01 D 53/04 (2006.01)** **B 01 D 53/26 (2006.01)**
B 01 J 20/28 (2006.01) **B 01 J 20/32 (2006.01)** **F 16 J 15/10 (2006.01)**
F 16 J 15/3236 (2016.01)

(45) Oversættelsen bekendtgjort den: **2024-02-12**

(80) Dato for Den Europæiske Patentmyndigheds
bekendtgørelse om meddelelse af patentet: **2023-11-15**

(86) Europæisk ansøgning nr.: **20199982.8**

(86) Europæisk indleveringsdag: **2016-06-14**

(87) Den europæiske ansøgnings publiceringsdag: **2021-03-03**

(30) Prioritet: **2015-08-31 US 201562212128 P** **2015-11-06 BE 201505727**

(62) Stamansøgningsnr: **16757135.5**

(84) Designerede stater: **AL AT BE BG CH CY CZ DE DK EE ES FI FR GB GR HR HU IE IS IT LI LT LU LV MC MK MT NL NO PL PT RO RS SE SI SK SM TR**

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(54) Benævnelse: **Adsorptionsindretning til komprimeret gas.**

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DK/EP 3785787 T3

DESCRIPTION

[0001] The present invention relates to an adsorption device for compressed gas, for example compressed air.

[0002] More specifically, the invention concerns an adsorption device for compressed gas, whereby this adsorption device comprises a vessel in which an adsorbent, for example a drying agent, or a 'desiccant', is placed. The vessel concerned is provided with an inlet for supplying a compressed gas to be treated, and an outlet for discharging treated gas.

[0003] The adsorbent concerned is generally realised in the form of a regeneratable adsorbent, or in other words an adsorbent that can be regenerated after reaching a certain degree of saturation. For simplicity, the following primarily refers to an adsorbent in the form of a drying agent, but the invention also extends to other adsorbents. For example, with a drying device it is indeed the case that as the adsorbent, that is constructed in the form of a drying agent, extracts moisture from the gas to be dried, this drying agent will become increasingly saturated with adsorbed moisture. Hence, it is usual, after using the drying agent for a certain time to dry compressed gas, to regenerate this drying agent, for example by exposing it to a regeneration gas flow that extracts the moisture from the drying agent. Such a regeneration gas flow can consist of a fraction of the dried gas and/or hot gas for example whose relative humidity is sufficiently low to be able to realise the regeneration of the drying agent.

[0004] In some embodiments of drying devices for compressed gas, use is made of two or more vessels of drying agent. With two vessels this principle of drying device is also referred to as a twin tower dryer. In such a type of drying device a compressed gas, for example originating from a compressor, can be passed through the first of the aforementioned vessels for example, where it will be dried by the drying agent in the vessel concerned, after having passed through an after cooler and a condensate separator (which may or may not form part of the after cooler concerned). This vessel consequently acts as a drying vessel.

[0005] At the same time, a regeneration gas flow can be guided through a second aforementioned vessel in order to regenerate the drying agent in that second vessel by extracting the moisture from this drying agent. This can be done by making use of a gas that has already been dried, for example, that is tapped off downstream from the drying vessel for example and/or by supplying a gas flow that has been heated, for example by recovering the heat generated in the compressor during the compression. In this last case it is called a "heat of compression" or HOC dryer. Other known regeneration principles can of course also be used.

[0006] When the drying agent in the drying vessel has reached a certain degree of saturation, the gas flows through the first and the second vessel can be changed over, such that the drying agent in the first vessel will now be regenerated by a regeneration gas flow while the second vessel will take on the role of drying vessel. In this way the two or more vessels will

alternately operate as a drying pressure vessel and a regenerating pressure vessel, such that continuity in the drying process can be realised. Examples of such drying devices with a number of vessels are described for example in US 2003/023.941, US 4.783.432, US 6.375.722, EP 1.776.171 and WO 2006/050.582.

[0007] The drying agent that is used in such adsorption devices with a number of vessels often consists of grains of silica gel, activated alumina or a molecular sieve material, or a combination thereof. As is known activated alumina is produced by thermal dehydration or activation of aluminium hydroxide Al(OH)_3 , while molecular sieves consist of synthetic zeolites (crystalline aluminosilicates).

[0008] A limitation of such a type of drying device that comprises a drying agent in a granular form, consists of the gas speeds through the vessels having to be limited in order to counteract grains moving against one another or even fluidisation. Indeed, due to the grains being set in motion friction will occur between them, which in turn leads to dust formation and a reduced drying capacity. Other causes of such dust formation are for example pressure variations and/or thermal shocks. Moreover, the pressure drop across a twin tower dryer is relatively high and the desiccant grains have a rather high thermal mass.

[0009] Alternative drying devices are known for compressed gas, whereby the drying agent is placed in a rotating drum, while a drying zone and regeneration zone extend in the vessel. During the operation of such a drying device, the drying drum will be made to rotate by drive means provided to this end, such that the drying agent in this drying drum will alternately be taken through the drying zone and the regeneration zone. The compressed gas to be dried will be guided through the drying zone, while the regeneration gas flow is guided through the regeneration zone, in order to realise simultaneous drying of compressed gas in the drying zone and regeneration of the drying agent in the regeneration zone.

[0010] Examples of such drying devices that are provided with a rotating drying drum are described for example in WO 00/033.943, WO 00/074.819, WO 01/078.872, WO 01/087.463, WO 02/038.251, WO 2007/079533, WO 2005/070.518, WO 2006/012.711, GB 1.226.348, GB 1.349.732, GB 1.426.292, US 3.490.201, US 5.385.603 and US 8.349.054. Examples of adsorbing cartridges comprising a series of adsorbing structures stacked in series is known from US2008/282888, US 2014/305309 A1 and US 2015/040765 A1.

[0011] The drying agent or desiccant that is used in the known drying devices for drying compressed gas consists of silica gel, molecular sieves, activated alumina or a combination thereof, for example. As is known, the drying agent can be affixed on a support such as a corrugated structure of glass fibres or ceramic fibres that are rolled up for example to form a honeycomb structure in the vessel, for example as described in US 5.683.532.

[0012] In practice it turns out that with the known drying devices for drying compressed gas, under certain conditions such as in the event of insufficient regeneration of the drying agent and oversaturation thereof, the drying agent goes through a complex breakdown process that

in some cases can ultimately result in the failure of the drying device, for example in the case of silica gel as a drying agent in a rotor, because the binder function of the silica gel decreases, which leads to a loss of structural strength of the supporting glass fibre matrix, and also because the adsorbing function of the silica gel decreases as a result of hydrolysis and breakdown of the silica gel structure.

[0013] Thus the adsorption behaviour and adsorption capacity of a silica gel rotor, in severe conditions of high moisture and high temperature will substantially change during the useful life of the rotor.

[0014] The purpose of the present invention is to provide an adsorption device for compressed gas that provides a solution for one or more of the disadvantages attached to the conventional, already known, adsorption devices that make use of an adsorbent.

[0015] To this end the invention concerns an adsorption device for compressed gas, whereby this adsorption device is provided with a vessel with an inlet for the supply of a compressed gas to be treated, and an outlet for treated gas and whereby an adsorption element is affixed in the aforementioned vessel, whereby this adsorption element extends along the flow direction of the compressed gas to be treated between the aforementioned inlet and the aforementioned outlet, and, according to the invention, consists of a monolithic supporting structure that is at least partially provided with a coating that comprises an adsorbent.

[0016] An advantage of such an adsorption device according to the invention is that there is no risk of movement or fluidisation, as no loose grains of adsorbent are used. As a result dust formation is prevented, while a relatively high flow rate of the compressed gas to be treated through the adsorption device is possible.

[0017] Moreover, such an adsorption device according to the invention enables the vessel to be placed vertically, sloping or even horizontally, which is not possible with conventional drying devices that make use of a granular drying agent for example, as the horizontal use of such known drying devices can lead to a rearrangement of the grains and the formation of internal leakage paths and consequently a reduced dryer performance.

[0018] According to a preferred characteristic of the invention, the aforementioned monolithic supporting structure comprises one or more of the following materials: ceramic material, metal foil, a fibre structure and a polymer. Particularly good results are obtained with the use of a ceramic structure that contains cordierite.

[0019] Preferably the aforementioned adsorbent contains one or more of the following materials: a zeolite, silica gel, activated alumina, activated carbon, metal organic frameworks, carbon molecular sieve (CMS), an impregnated adsorbent and a hybrid adsorbent. In particular a hydrophilic zeolite support is preferable. Good results are obtained by making use of faujasite or zeolite type X, in which the silicon/aluminium ratio is between 2 and 3.

[0020] According to the invention, the adsorption device comprises a number of adsorption elements placed in series in the aforementioned vessel along the flow direction of the gas.

[0021] The present invention also relates to an adsorption element for an adsorption device for compressed gas, whereby this adsorption element comprises a monolithic supporting structure that is at least partially provided with a coating that contains an adsorbent.

[0022] In addition the invention also concerns a cartridge that comprises a stack of adsorption elements that are provided with a monolithic supporting structure that is at least partially provided with a coating that contains an adsorbent.

[0023] With the intention of better showing the characteristics of the present invention, a few preferred embodiments of an adsorption device according to the invention are described hereinafter by way of an example, without any limiting nature, with reference to the accompanying drawings, wherein:

figure 1 schematically shows an adsorption device;

figure 2 shows a cartridge of adsorption elements according to the invention;

figure 3 shows the part indicated by F3 in figure 2 on a larger scale;

figure 4 shows a variant of an adsorption device according to figure 1;

figure 5 shows a variant of figure 3 in the mounted state of the stack of adsorption elements in a vessel; and

figure 6 shows a detail of the top edge of a stack of adsorption elements in the mounted state in a vessel.

[0024] Figure 1 schematically shows a possible embodiment of an adsorption device 1, which in this case forms a drying device and which comprises two vessels 2A and 2B that are each provided with an inlet 3A and 3B respectively for the supply of a compressed gas to be treated (in this case dried) and an outlet 4A and 4B respectively for the discharge of treated (in this case dried) compressed gas.

[0025] The respective outlets 4A and 4B are connected to a pressure pipe 5 of a compressor 6 via outlet pipes 5A and 5B, in this example an air compressor. Each of the outlet pipes 5A and 5B can be shut off by means of an outlet valve 7A and 7B respectively provided to this end.

[0026] Between the outlet valve 7A and 7B respectively on the one hand and the outlet 4A and 4B respectively, a connection is provided on each outlet pipe 5A and 5B to a discharge pipe 8A and 8B respectively that can be closed off by means of a discharge valve 9A and 9B respectively, and which in this case, but not necessarily, is connected to a common outlet 10.

[0027] The aforementioned inlets 3A and 3B are connected together by means of a connecting pipe 11 in which a first set of two shutoff valves 12A and 12B are placed in series. The valves 12A and 12B concerned are bypassed by a bypass pipe 13 in which a second set of two shutoff valves 14A and 14B are placed in series.

[0028] The connecting pipe 11 and the bypass pipe 13 are connected together by means of a cooling pipe 15, in which a heat exchanger 16 and a condensate separator 17 are affixed. One end of the cooling pipe 15 connects to the connecting pipe 11 between the first set of shutoff valves 12A and 12B, while the other end of the cooling pipe 15 is connected to the bypass pipe 13, between the second set of shutoff valves 14A and 14B.

[0029] In this example each of the outlet valves 7A and 7B, the discharge valves 9A and 9B and the shutoff valves 12A, 12B, 14A, 14B are constructed in the form of a controllable shutoff valve that is connected to a control unit 18, either via control cables provided to this end, which for clarity are not included in the drawing, or wirelessly.

[0030] An adsorption element 19A and 19B respectively is affixed in each of the aforementioned vessels 2A and 2B, in this case in the form of drying elements, more specifically in the flow path of the gas to be dried, or in other words according to the flow direction of the compressed gas to be treated between the aforementioned inlet 3A and 3B respectively on the one hand, and the aforementioned outlet 4A and 4B respectively on the other hand.

[0031] With regard to the first vessel 2A, an inlet side 20A of the adsorption element 19A will extend opposite the aforementioned inlet 3A, while an outlet side 21A of the adsorption element 19A extends opposite the outlet 4A.

[0032] Analogously the adsorption element 19B in the second vessel 2B has an inlet side 20B and an outlet side 21B that extend opposite the inlet 3B and the outlet 4B respectively.

[0033] The adsorption elements 19A and 19B comprise a monolithic supporting structure that preferably, but not necessarily, consists of a ceramic structure that contains cordierite, for example Celcor[®] by Corning. Alternatively, according to the invention, other materials can also be used for the manufacture of the supporting structure concerned, such as:

- other ceramic materials such as mullite, γ - or α -alumina or silicon carbide (SiC);
- metal foil; or
- a fibre structure, for example based on glass fibre, ceramic fibre or other fibres, or a mixture of different types of fibres; or
- a polymer.

[0034] It goes without saying that the aforementioned list is not exhaustive and the use of

other materials is not excluded.

[0035] It is not excluded either that the monolithic supporting structure is made of a combination of two or more of the aforementioned and/or other materials.

[0036] The material of the supporting structure preferably contains between 31 and 186 cells per cm² (200 and 1200 cells per square inch), and more preferably between 54,3 and 89,8 cells per cm² (350 and 450 cells per square inch).

[0037] The wall thickness of the supporting structure is preferably between 0,05 and 0,28 mm (2 and 11 milli-inch), and more preferably between 0,05 and 0,23 (3 and 9 milli-inch), and even more preferably between 0,13 and 0,19 mm (5 and 7,5 milli-inch). In a most preferred embodiment, the wall thickness is between 0,18 and 0,18 (6 and 7 milli-inch), preferably approximately 0,16mm (6,5 milli-inch).

[0038] The porosity of the wall of the supporting structure is preferably greater than 5%, and more preferably greater than 10%, and even better greater than 20%.

[0039] The cells formed preferably have a square shape, but can present other shapes such as triangular, sinusoidal, circular, hexagonal and similar.

[0040] The aforementioned monolithic supporting structure is at least partially provided with a coating that contains an adsorbent.

[0041] The adsorbent concerned can contain one or more of the following and/or other materials:

- a zeolite, preferably a hydrophilic zeolite, but a hydrophobic zeolite is also possible - this zeolite can be faujasite zeolite type X for example, for example Zeolium F9 of Tosoh, or a mixture of zeolite type X and A;
- silica gel;
- activated alumina;
- activated carbon;
- metal-organic frameworks;
- carbon molecular sieve (CMS);
- an impregnated adsorbent; and
- a hybrid adsorbent.

[0042] The above list is not exhaustive and other materials are also possible according to the invention.

[0043] The choice of the adsorbent depends on what treatment the gas to be treated must go through, such as drying or the removal of other molecules such as oxygen or carbon dioxide,

for example when using the adsorption device as a nitrogen generator, whereby the compressed gas to be treated is compressed air.

[0044] The distribution of the particle size of the adsorbent is preferably such that D_{50} is less than 10 um and more preferably less than 4 um.

[0045] In addition to the aforementioned adsorbent, the aforementioned coating preferably also contains a binder material, preferably an inorganic binder material such as:

- colloidal silica, for example Ludox-AS 40 of Grace Davison;
- alumina; and/or
- clay.

[0046] Moreover, if need be use can be made of an organic binder material such as:

- methyl cellulose;
- polymers such as acrylic resins, vinyl resins and similar; and/or
- a material from the cellulose group.

[0047] In the example of figure 1 each vessel 2A and 2B contains one single adsorption element 19A and 19B respectively, but according to the invention, as shown in figure 2, two or more adsorption elements 19A or 19B can also be placed in series in a vessel 2A and/or 2B along the flow direction of the gas.

[0048] Figure 2 shows an example of a number of adsorption elements 19A stacked on one another, which in this example are disc shaped and all present a flat top and bottom surface.

[0049] In each case, a seal 22 is provided between two adsorption elements 19A stacked on one another, over the peripheral edge of these adsorption elements 19A, in this case a ring-shaped seal that extends between the interfaces of the stacked adsorption elements 19A with at least one radial lip oriented inwards, and in this case with two V-shaped radial lips 23 oriented inwards.

[0050] Preferably, shrink sleeving 24 is affixed over the peripheral wall of the entire stack of adsorption elements, that is preferably made of an elastic material that is not very permeable to gas, for example polyolefin. The shrink sleeving 24 concerned can also be affixed over just a part of the height of the stack of adsorption elements.

[0051] The set of stacked adsorption elements 19A thus forms a cartridge that is interchangeable or replaceable according to a particular aspect of the invention.

[0052] The operation of an adsorption device 1 according to the invention is very simple and as follows.

[0053] In the first instance, in this example the first vessel 2A will fulfil the role of a drying vessel, while the adsorption element 19B (that is thus a drying element here) will be regenerated in the second vessel 2B.

[0054] The compressor 6 draws in a gas, for example surrounding air, and compresses this gas. The compressed hot gas is then carried through the outlet pipe 5B via the pressure pipe 5 via the open outlet valve 7B to the outlet 4B of the second vessel 2B.

[0055] The hot compressed gas will have a sufficiently low relative humidity to extract moisture from the adsorption element 19B present in the drying agent and will thus regenerate this adsorption element 19B. In other words the desiccant is dried in the second vessel 2B.

[0056] The hot moist gas is then driven via the open shutoff valve 14B to the cooling pipe 15, where it is guided successively through the heat exchanger 16 and the condensate separator 17 to then be carried via the open shutoff valve 12A and the connecting pipe 11 to the inlet 3A of the first vessel 2A.

[0057] The cold compressed gas that is 100% saturated will enter the first vessel 2A via the inlet 3A and be guided through the adsorption element 19A.

[0058] The adsorbent present on the supporting structure will extract moisture from the gas during the flow of the compressed gas through the adsorption element 19A. In this example the adsorbent will consequently fulfil the role of a drying agent or desiccant material.

[0059] The gas that leaves the adsorption element 19A, at the outlet side 21A thereof, will be drier than the gas that entered the vessel 2A via the inlet 3A.

[0060] The dried compressed gas then flows, via the outlet 4A, through the outlet pipe 5A and the open discharge valve 9A to the discharge pipe 8A and to the outlet 10 connected thereto, which can be connected to a consumer of dried compressed gas.

[0061] After a certain cycle time, the operation of both vessels 2A and 2B can be changed over and the second vessel 2B can take on the role of a drying vessel, while the desiccant in the first vessel 2A can be regenerated.

[0062] On account of the fact that the adsorption device 1 according to the invention does not make use of a granular desiccant, the vessels 2A and 2B can be placed in any position such as vertical, horizontal or any other position.

[0063] As the adsorbent is attached to a supporting structure there is no risk of fluidisation, such as with a granular desiccant, and consequently dust formation cannot occur, not even at

high gas speeds through the adsorption element.

[0064] When use is made of a number of adsorption elements 19A placed on one another, as shown in figure 2, the gas will flow sequentially through the successive adsorption elements, either as gas to be dried or as a regeneration gas.

[0065] The presence of the aforementioned seals 22 between successive adsorption elements 19A prevents leakages being able to occur between the side wall of the stack of adsorption elements 19A on the one hand, and the inside wall of the vessel 2A on the other hand. For the rest, the same applies to the use of such a stack of a number of adsorption elements 19B in the second vessel 2B, which of course is also possible and can be provided with the said seals 22.

[0066] Figure 4 shows another embodiment of an adsorption device 1, whereby in this case there is only one vessel 25 in which an adsorption element 19 is rotatably affixed. The adsorption element 19 is attached to drive means, for example in the form of an electric motor 26.

[0067] As with known rotary drum dryers a regeneration zone and an adsorption zone (in this case a drying zone) extend in the vessel. The pressure pipe 5, in this case originating from a compressor 6, connects to the inlet of the regeneration zone, as is the case with known HOC dryers. The outlet of the regeneration zone is connected to the inlet of the adsorption zone in a known way via a connecting pipe 27. A heat exchanger 16 and condensate separator 17 are provided in the connecting pipe 27 concerned.

[0068] Finally, the outlet of the regeneration zone is connected to the outlet 10 via a discharge pipe 8.

[0069] The operation of an adsorption device according to figure 4 is analogous to that of known HOC dryers with a rotary drum in which a drying agent is provided. However, on account of the structure of the adsorption element 19, such an improved adsorption device is not susceptible to failure on account of a reduction of strength. After all, the monolithic supporting structure of an adsorption element in an adsorption device of the invention does not lose structural strength, not even under severe conditions of high humidity and high temperature.

[0070] The embodiments of an adsorption device 1 shown in the drawings are both full-flow HOC dryers, however an adsorption device 1 does not necessarily have to operate according to a full-flow principle. Likewise, it is not required either that the heat of compression is employed for the regeneration of the adsorbent, but use can be made of any regeneration gas that originates from the process itself or otherwise, and which is compressed gas or otherwise.

[0071] Figure 5 shows a stack of adsorption elements 19A which is affixed in the vessel 2A and a part of the wall of this vessel 2A can be seen.

[0072] In this example the seal 22 comprises a ring 28, for example but not necessarily of aluminium, another metal or a polymer, whereby the inside diameter of this ring 28 is somewhat larger than the outside diameter of the adsorption elements 19A, which in this example are disc shaped.

[0073] The ring 28 extends over the peripheral edge of the ends of the adsorption elements 19A placed on one another. On its inside periphery the ring 28 concerned is provided with a radial edge 29 oriented inwards, against which the ends concerned of the adsorption elements are affixed.

[0074] In order to obtain a good seal and prevent leakage paths, a sealing layer 30 and 31 respectively is affixed over the entire periphery on either side of the edge 29 concerned, for example in the form of a quantity of adhesive or another sealing element.

[0075] In this example, the ring 28 is provided over its outer periphery with two practically parallel ribs 32 at an axial distance from one another, between which a seal 33 is affixed, in this case in the form of an O-ring. The presence of the ribs 32 is not strictly necessary. For example, only one rib can be provided on which the seal 33 rests, or can be mounted immovably on the ring 28 of the seal, or form an integral part of this.

[0076] When mounting the cartridge consisting of adsorption elements stacked on one another, as shown in figure 5, the seal 33 will press against the inside wall of the vessel 2A. In this way, this construction not only ensures that leaks between the adsorption elements 19A mutually, but also between the cartridge and the wall of the vessel, are prevented.

[0077] Again it is clear that the embodiment concerned is not limited to an application in the vessel 2A, but it can just as well be applied in the vessel 2B of figure 1 and/or in the vessel 25 of figure 4, or in any other type of adsorption device 1.

[0078] Figure 6 shows a detail of a top edge of a top part of a stack of adsorption elements 19A in a mounted state in a vessel 2A. The wall of the vessel 2A is shown in the right of the drawing. The same construction is possible on the bottom edge of a stack of adsorption elements or, when use is made of only one adsorption element in a vessel, on the top and/or bottom side of such a separate adsorption element.

[0079] A V-shaped seal 34 is pushed over the free peripheral edge of the adsorption element 19A, in other words the peripheral edge that is not oriented towards another adsorption element 19A, all such that a first arm 35 of the seal presses against the axial top surface 36 of the adsorption element 19A, while the second arm 37 of this seal 34 presses against the radial outside wall 38 of the adsorption element 19A.

[0080] In this case, the V-shaped seal 34 presents a lobate protuberance 39 on the top, or in other words on the side where the two arms 35 and 38 are connected together.

[0081] According to a preferred characteristic of the invention, pressing means are provided that press a part of the seal 34 radially against the inside wall of the vessel 2A. In this example the pressing means concerned comprise a conical ring 40, that is pressed by means of a spring 41 against the lobate protuberance 39 of the seal 34. To this end the conical surface of the conical ring 40 is oriented towards the seal 34 concerned and presses the spring by its other end against the cover of the vessel 2A, for example. It goes without saying that the part of the seal 34 that is pressed against the inside wall of the vessel 2A does not necessarily have to be lobate, and this part can be constructed in many different ways.

[0082] The largest outside diameter of the conical ring 40 is preferably, but not necessarily, almost as large as the inside diameter of the vessel 2A.

[0083] Alternatively, in the construction as shown by way of an example in figure 6, the seal at the top and bottom of the cartridge, consisting of a stack of adsorption elements 19A, can be obtained in different ways, for example by making use of a glued ring and an O-ring similar to the principle shown in figure 5.

[0084] Although in the above description an adsorption device in the form of a drying device for adsorbing moisture is primarily described, the invention also relates to other types of adsorption devices such as nitrogen generators and similar, whose adsorption element is able to adsorb certain gas molecules such as oxygen, carbon dioxide and/or similar. By removing such gas molecules from compressed air for example, as is known, nitrogen can be generated.

REFERENCES CITED IN THE DESCRIPTION

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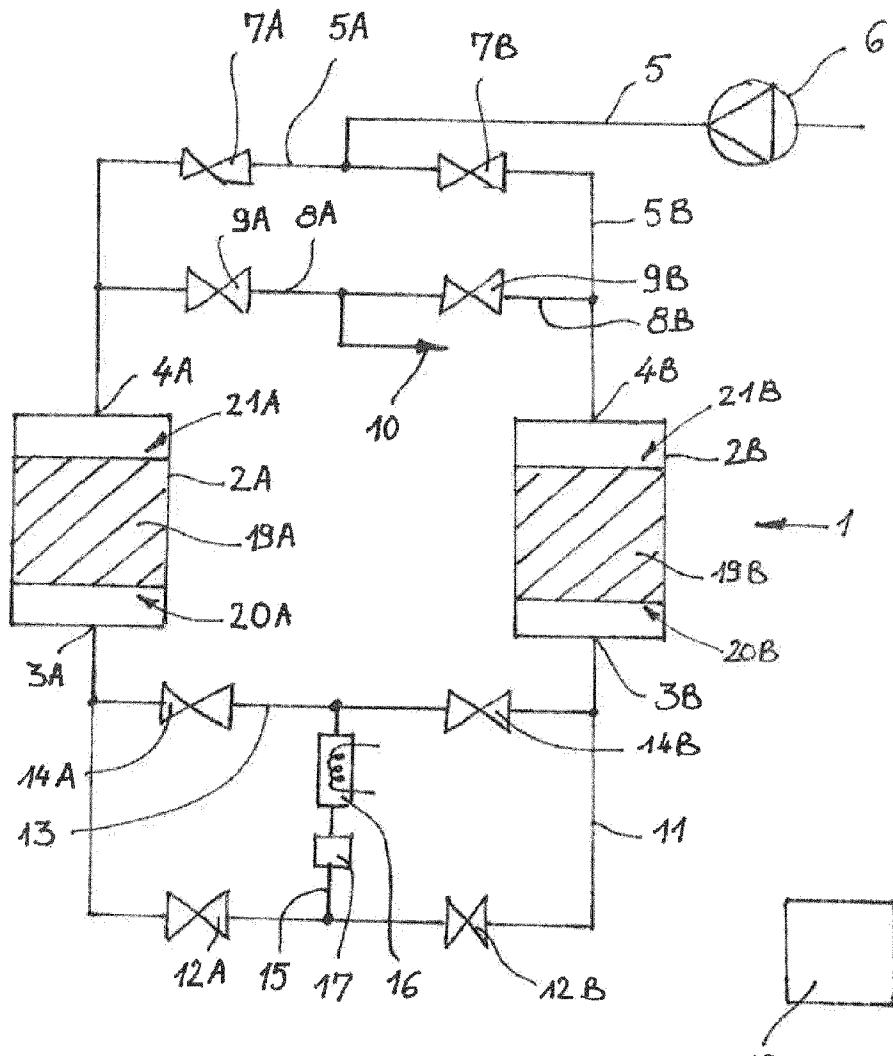
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Patentkrav

1. Adsorptionsindretning til komprimeret gas, hvorved denne adsorptionsanordning (1) er forsynet med en beholder (2A, 2B, 25) med et indløb (3A, 3B) til tilførsel af en komprimeret gas, der skal behandles, og et udløb (4A, 4B) for behandlet gas, og hvorved et adsorptionselement (19A, 19B, 19) er fastgjort i den fornævnte beholder (2A, 2B, 25), hvorved dette adsorptionselement (19A, 19B, 19) strækker sig langs strømningsretningen af den komprimerede gas, der skal behandles, mellem det fornævnte indløb (3A, 3B) og det fornævnte udløb (4A, 4B), **kendeteget ved, at** det fornævnte adsorptionselement (19A, 19B, 19) omfatter en monolitisk støttestruktur, der i det mindste delvis er forsynet med en belægning, der indeholder en adsorbent, **ved, at** et antal adsorptionselementer (19A) er anbragt i serie i den fornævnte beholder (2A, 2B, 25) langs gassens strømningsretning, **ved, at** en tætning (22) er tilvejebragt mellem hvert to adsorptionselementer (19A) placeret på hinanden, **ved, at** den fornævnte tætning (22) er forsynet med mindst én radial læbe (23) vendt indad, som strækker sig mellem adsorptionselementerne (19A).
2. Adsorptionsindretningen ifølge krav 1, **kendeteget ved, at** den fornævnte monolitiske støttestruktur indeholder et eller flere af følgende materialer: keramisk materiale, metalfolie, en fiberstruktur og en polymer.
3. Adsorptionsindretningen ifølge krav 2, **kendeteget ved, at** den fornævnte monolitiske støttestruktur består af en keramisk struktur, der indeholder cordierit.
4. Adsorptionsindretningen ifølge et eller flere af de foregående krav, **kendeteget ved, at** den fornævnte adsorbent indeholder et eller flere af følgende materialer: en zeolit, silicagel, aktiveret aluminiumoxid, aktivt kul, metal-organiske skelet, en imprægneret adsorbent og en hybrid adsorbent.

5. Adsorptionsindretningen ifølge krav 4, **kendetegnet ved, at** den fornævnte adsorbent indeholder en hydrofil zeolit.
6. Adsorptionsindretningen ifølge et eller flere af de foregående krav, 5 **kendetegnet ved, at** den fornævnte coating yderligere indeholder et bindemiddel-materiale ud over den fornævnte adsorbent.
7. Patron bestående af en stak adsorptionselementer (19A, 19B, 19C), hvorved 10 hvert adsorptionselement (19A, 19B, 19C) omfatter en monolitisk støttestruktur, der i det mindste delvist er forsynet med en belægning, der indeholder en adsorbent, **kendetegnet ved, at** en tætning (22) er tilvejebragt mellem hvert to adsorptionselementer (19A) placeret på hinanden og **ved, at** den fornævnte tætning (22) er forsynet med mindst én radial læbe (23) vendt indad, som strækker sig mellem adsorptionselementerne (19A). 15
8. Patronen ifølge krav 7, **kendetegnet ved, at** en krympemuffe (24) er fastgjort over den perifere væg af i det mindste en del af stablen af adsorptionselementer (19A).
9. Patronen ifølge krav 7 eller 8, **kendetegnet ved, at** den fornævnte tætning (22) strækker sig over de respektive perifere kanter af adsorptionselementerne (19A), der er placeret på hinanden. 20
10. Patronen ifølge et hvilket som helst af kravene 7 til 9, **kendetegnet ved, at** den fornævnte monolitiske støttestruktur består af en keramisk struktur, der indeholder cordierit. 25
11. Patronen ifølge et hvilket som helst af kravene 7 til 10, **kendetegnet ved, at** den fornævnte adsorbent indeholder et eller flere af følgende materialer: en zeolit, silicagel, aktiveret aluminiumoxid, aktivt kul og metal-organiske skelet. 30

DRAWINGS



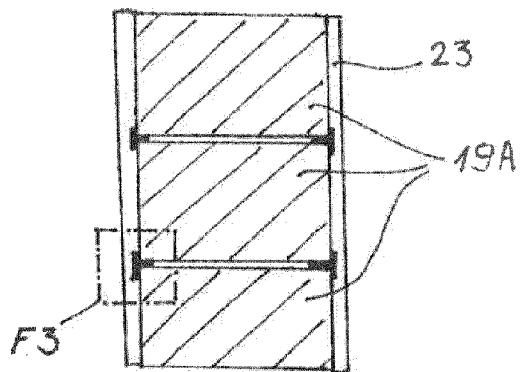


Fig. 2

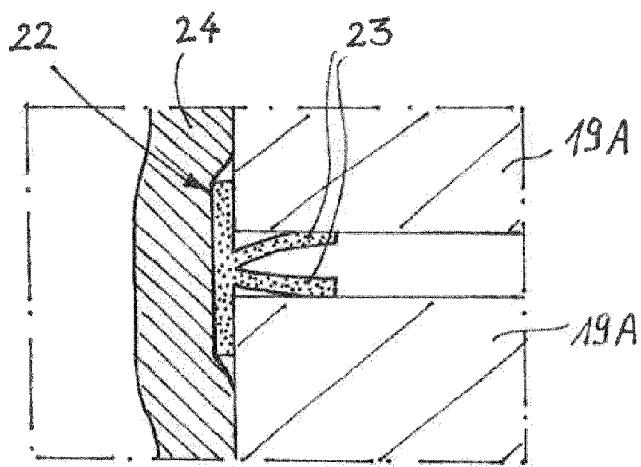


Fig. 3

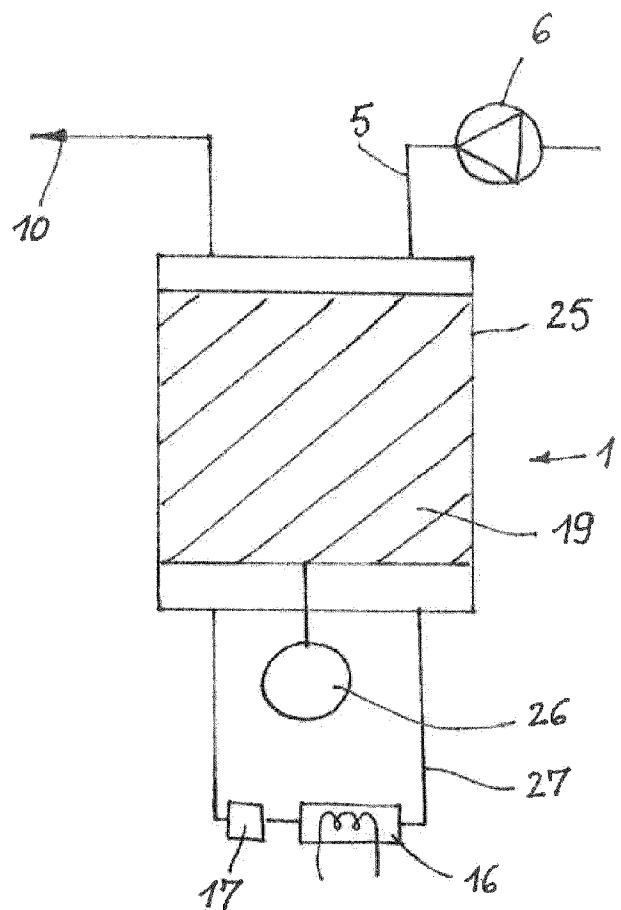


Fig. 4

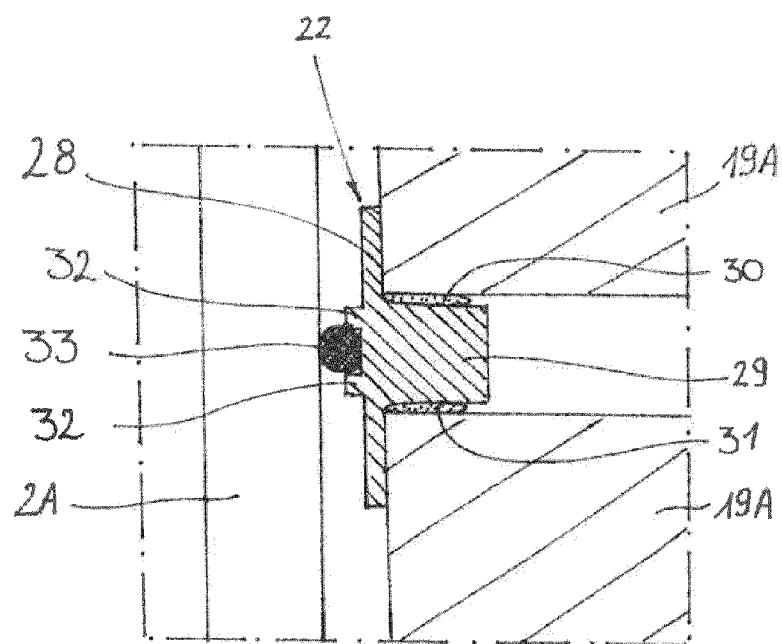


Fig. 5

