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DESCRIPTION

Description

[0001] The present invention relates to a plate heat exchanger for treatment of a liquid feed, a heat exchanging plate for a plate heat exchanger for treatment of a liquid feed, and a method of manufacturing a plate heat exchanger for treatment of a liquid feed.

Background of the invention

[0002] Equipment for desalination of seawater, where one or several plate packages of heat exchanger plates form the main components in the process, has been manufactured since many years. The applicant company has since several years produced a fresh water generator where the evaporation, separation and condensation take place in the plate package. The details may be found in the international application WO 2006 / 104443 A1 assigned to Alfa Laval Corporate AB. It is disclosing a plate heat exchanger for desalination having first- and second type plate interspaces formed in alternating order in the heat exchanger. The first type plate interspaces form evaporation sections, separation sections and condensation sections, whereas the second type plate interspaces form heating sections, separation sections and cooling sections. A heat exchange plate according to the preamble of claim 1 is disclosed in WO 2006/104443 A1.

[0003] The evaporation section is used for evaporating a liquid feed, such as sea water, the separation section is used for separating evaporated feed from non-evaporated feed and the condensation section is used for condensing the evaporated feed. The heating section is heating the evaporation section and the cooling section is cooling the condensation section. The advantage of the above-mentioned heat exchanger is that it does not need any container since the whole treatment of the seawater is performed in the plate package. The above plate heat exchanger has centrally located ports for heating fluid, cooling fluid and fresh water and the ports for brine and feed are symmetrically arranged about a central axis of the heat exchanger plate. In this way only one plate type is needed. The first type interspaces and second type interspaces are formed by using two different gaskets and arranging the heat exchange plates face to face by turning every second plate 180 degrees about the centre axis. In this way the corrugations in the opposing plates in the evaporation sections and condensation sections will form a cross-shaped pattern in which opposing ridges in each plate interspace abut. The valleys in each plate interspace form ridges in the neighbouring plate interspaces which will abut the ridges of an opposing plate in the respective neighbouring plate interspaces.

[0004] The separation section, however, typically extends between all plate interspaces, i.e.

also between the heating sections and cooling sections in the second type plate interspaces. In the separation section no heat exchange takes place between the plates. This is different from the condensation section and the evaporation section. In the separation section the plates are designed such that the main corrugated pattern of two adjacent plates will fall into each other and not abut, except on occasional contact points. In this way a meandering flow path is achieved in which the flow constantly is caused to change direction and in which way the droplets of non-evaporated feed will be trapped by impacting on the plate and then released from the evaporation section while evaporated feed can pass through to the condensation section.

[0005] Using only one plate type, the separation section has been achieved in the prior art heat exchanger by having a ridge on the left side horizontally level with a valley on the right side and vice versa. In the above-mentioned prior art heat exchanger, the central part of the heat exchanger is used for ports for heating fluid, cooling water, fresh water etc. Also, the separation section has a non-corrugated central zone between the left and right side of the separation area and designing the pattern so that a ridge on the left side is horizontally level with a valley on the right side, and vice versa, is not a problem. In the above-mentioned prior art heat exchanger, the non-corrugated central zone is partly used for the outlet port for fresh water which extend into the central part of the separation section.

[0006] The centrally located ports and the ports adjacent the edges of the heat exchanger plate implies that up to six gasket elements will be required along the width of the heat exchanger plate. The gaskets occupy space on the heat exchanger plate which cannot be used for the process. The width of the gasket will be about the same for a large heat exchanger as for a small heat exchanger. For a large heat exchanger, the space occupied by the gaskets may be negligible, however, for a small heat exchanger it may be significant.

[0007] There is an increased need for smaller fresh water generators which may be used on board smaller vessels. When reducing the size of the fresh water generator as discussed above, the gaskets will still take up essentially the same amount of space. This will make the smaller fresh water generators less area efficient compared to the large fresh water generators. This is especially problematic for the condenser which needs a large heat exchanging area to operate properly.

[0008] One solution to the above problem is to omit the centrally located ports, in particular in the condenser, and have all of the ports arranged at the edges of the heat exchanging plate. One example of such design for the condenser is presented in the European patent application EP19171723.0. The ports may then still be symmetrical placed about the centre axis to allow the individual plates to be turned over, i.e. turned 180 degrees about the centre axis, while keeping the ports at the same relative position. By keeping the ports and the gasket grooves symmetric about the centre axis, only one plate type is needed.

[0009] However, the above implies that the central parts of the heat exchanging plate will be used for heat exchange in the evaporation section and in the condensation section. Thus, it will

not be efficient to have a central non-corrugated area in the separator for the change between the ridges and valleys takes place.

[0010] Further, changing between ridges and valleys along the central axis will result in an open non-corrugated channel along the central axis. Even without using a central non-corrugated area an open non-corrugated channel will be established due to the corrugations having flanks between tops and bottoms. The open channel along the straight central axis will allow a large number of droplets to pass directly to the condenser without impacting on the plate. This will affect the separation negatively.

[0011] It is therefore an object of the present invention to find a more efficient solution for the change between ridges and valleys at the central part of the heat exchanger.

[0012] Omitting the centrally located ports will also remove any central contact location between opposing plates in the separation section. This may result in a reduced structural stability in the central region of the separation section.

[0013] It is a further object of the present invention to improve the structural stability of the separation section when there are no centrally located ports.

[0014] If the corrugated pattern of the opposing plates falling into each other in the separation section extends all the way to the gasket groove, the plate interspace will also lack any contact point along the gasket groove. This will lead to a less robust gasket groove and may lead to that the gasket will be mispositioned in the gasket groove, which in turn may lead to leakage.

[0015] In the prior art, the press depth of the corrugation has been slightly increased adjacent the gasket groove in order to improve the support of the gasket in the gasket groove. However, still no contact between plates between the gasket groove and the separation section have been provided.

[0016] It is thus a yet further object of the present invention to improve the design of the gasket groove and increase the structural stability at the gasket and gasket groove at the edge of the plate.

[0017] Further prior art includes CN203820488UU disclosing a heat exchange plate which is sequentially divided from top to bottom into a condensation zone, an evaporation zone and a heating zone.

[0018] CN206262115UU describes an evaporating-separating-condensing three-in-sea water collecting plate. The gas-liquid separation zone separation structure using a flap. The flap is provided with reinforcing ribs.

[0019] GB1211065A describes a plate heat exchanger in which two plates are assembled in superimposed relation. One of the plates being turned 180° in its own plane relative to the

other, and a passage is obtained between the plates.

[0020] KR101345733B1 describes a heat exchanger plate with barriers.

[0021] US8646517B2 describes a heat exchanger plate heat exchanger plate for a plate heat exchanger, which plate has a number of ports, a distribution region, a heat transfer region, a first adiabatic region, a second adiabatic region and an edge area that extends outside the ports and the regions.

Summary of the invention

[0022] The above objects are realised in a first aspect by plate heat exchanger for treatment of a liquid feed, the heat exchanger comprising a plate package having a plurality of successively arranged heat exchanger plates, each heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part,

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa,

a first edge part between the first vertical edge and the first part, and

a second edge part between the second vertical edge and the second part, , the ridges and valleys in the first edge part and second edge part extending at an oblique angle relative to the central vertical axis

whereby adjacent heat exchanging plates are arranged such that ridges fall into valleys of opposing plates in the first and second parts and opposing ridges of opposing plates contact each other in the first edge part and second edge part.

[0023] The evaporation section is located in the lower part of the plate package, the

condensation section is located in the upper part of the plate package and the separation section is located in between the evaporation section and the condensation section. The heat exchanging plates at the evaporation section and condensation section are corrugated with a corrugation of ridges and valleys. Using a single plate type for the complete plate package, every second plate is turned 180 degrees about the centre axis when forming the plate package. In other words, front surfaces of each plate face front surfaces of adjacent plates and rear surfaces of each plate face rear surfaces of adjacent plates. Thereby, alternating first type and second type plate interspaces are formed. The evaporation section and the condensation section may be located in the same type interspace; however, they may also be located in different type interspaces, i.e. in neighbouring plate interspaces. In this way the evaporation section and the condensation section are formed on opposite sides of the plate.

[0024] The corrugations in the evaporation section and condensation section should be made such that when every second plate is turned about the centre axis, a cross corrugated pattern is formed in the plate interspaces in which opposing ridges contact each other at contact points. The cross-corrugated pattern improves the heat transfer between the plate interspaces at the evaporation section and condensation section.

[0025] In the separation section, no heat exchange between the plate interspaces takes place. Instead, in the first and second parts of the separation section, constituting the major part or the separation section, the heat exchanging plates are corrugated with a corrugation of ridges and valleys in such a way they permit catching of a liquid, i.e. liquid droplets, flowing from the evaporation section to the condensation section. In order to do that the ridges and valleys should extend in the transversal direction of the plate, i.e. transversally with respect to the vertical edges and the central axis. Further, the ridges of each plate should fall into valleys of opposing plates, and conversely, the valleys of each plate should receive ridges of opposing plates, without thereby contacting the opposite plate. Thereby a meandering flow path is established in the plate interspaces between the plates of the plate package in the first- and second parts of the separation section. In other words, a ridge thus is facing a valley of the opposing plate, and vice versa. No contact is thereby established between the plates in the first- and second parts.

[0026] The edge parts are located adjacent the gasket groove at the edge of the plate. The ridges and valleys extend in an oblique angle in the first edge part and second edge part. In this way a cross-corrugated pattern will be achieved adjacent the gasket groove. This will improve the design and the structural stability of the gasket groove since the contact point established thereby will absorb pressure loads which otherwise would have affected the gasket. Further, having contact points adjacent the gasket groove will keep the gasket in place in the groove and substantially prevent the gasket from being mispositioned. The risk of leakage is thereby reduced.

[0027] According to a further embodiment of the first aspect, wherein the ridges and valleys in the central part extend at an oblique angle relative to the central vertical axis such that opposing ridges of opposing plates contact each other in the central part.

[0028] In order for a ridge to be able to fall into an opposing valley when every second plate is turned by 180 degrees, a ridge between the first edge and the central axis must in the horizontal (transversal) direction correspond to a valley between the central axis and the second edge. This corresponds to a vertical shift between the respective ridges and valleys in the first part relative to the second part by half the distance between the centre of adjacent ridges. In this way, when every second plate is turned by 180 degrees, ridges will face valleys and vice versa, in the first- and second parts.

[0029] There will thus be a transition at the central axis, where ridges and valleys meet. When using centrally located ports, the transition will be made at the port, however, when omitting the centrally located ports, another solution must be found. Preferably, the central part extending symmetrically on both sides of the central axis between the first part and the second part in order to minimize the central part and to have the contact points along the centre axis. The central part thus forms the transition between the first part and the second part in the transversal direction.

[0030] In order to increase the structural stability of the separation section, the opposing plates at the central part form a cross-corrugated pattern, i.e. the ridges and valleys in the central part extending at an oblique angle relative to the central vertical axis such that opposing ridges contact at contact points. The valleys in each plate interspace will contact the respective neighbouring plate in the neighbouring plate interspace, as a valley will form a ridge on the opposite side of the plate. In this way, the plates in the separation section which do not contact in the first- and second parts have additional support at the central axis.

[0031] According to a further embodiment of the first aspect, the plate package defining first plate interspaces and second plate interspaces arranged in alternating order, each plate interspace being enclosed by a gasket extending along the first and second vertical edges of each plate.

[0032] Alternating first- and second plate interspaces are preferably realized by using a single plate and turning every second plate by 180 degrees about the central axis such that plate front surfaces face each other and plate rear surfaces face each other in the plate package. The plates in the package are mutually sealed by gaskets, preferably made by rubber.

[0033] According to a further embodiment of the first aspect, the separation section is provided in both the first and second plate interspaces.

[0034] As no heat transfer is taking place in the separation section, both the first- and second plate interspaces may be used for separation.

[0035] According to a further embodiment of the first aspect, the heat exchanging plate is provided with apertures at the first and second passages for communication between the plate interspaces.

[0036] Apertures should be provided between the plate interspaced for allowing the vaporized feed to flow between the plate interspaces. Preferably, both the lower part and the upper part of the separation section of each plate is provided with one or more apertures each.

[0037] According to a further embodiment of the first aspect, the ridges and valleys in the first and second parts define a first press depth, whereas the ridges and valleys in the central part and/or in the first and second edge parts define a second press depth, the first press depth being larger than the second press depth.

[0038] The press depth of the plate is defined as the distance between an imaginary central plane of each plate and the tops of the ridges and bottom of the valleys, respectively. The removal of liquids in the separation section may be improved by increasing the press depth of the ridges and valleys in the separation section compared to the ridges and valleys in the evaporation section and condensation section. In this way the flow path from the evaporation section to the condensation section will be increased and there will be an increased change of direction of the flow path when passing the deeper corrugations which will cause more droplets to impact the plate and be separated from the vapor flow. The press depth in the central part and/or in the first and second edge parts should be the same as in the evaporation section and condensation section as the opposing ridges contact at contact points and if some ridges and valleys would define a larger press depth, they would be over compressed at the contact points.

[0039] The press depth can be increased in the first and second parts of the separation section as the ridges fall into the valleys. There are also no contact points in the first and second parts of the separation section. Using the larger press depth in the first and second parts of the separation section requires a height adjustment of the press depth in the central part and/or in the first and second edge parts such that the press depth corresponds to the press depth of the evaporation second and condensation section.

[0040] According to a further embodiment of the first aspect, the liquid feed is sea water.

[0041] Using sea water as the liquid feed, the condensate output will be fresh water having a lower salinity than the feed and the concentrate output will be brine having a higher salinity than the feed.

[0042] According to a further embodiment of the first aspect, the width of the central part is smaller than the width of each of the first and second parts.

[0043] The central part defines a cross corrugated patent it is not used for separating liquid and vapour and only improves the structural stability of the plate package. Therefore, it should be as small as possible.

[0044] According to a further embodiment of the first aspect, the edge parts defines an area less than 20% of the area of each of the first and second parts, preferably less than 10%, more

preferably less than 5%.

[0045] The above values allow for good structural stability of the plate package while maintaining most of the effective separation area.

[0046] According to a further embodiment of the first aspect, the width of the edge part is substantially equal to the distance between the centre of adjacent ridges in the first and second parts.

[0047] In this way, the ridges and valleys can form a 45-degree angle relative to the central axis. In this way, opposing plates form contact points at the central axis.

[0048] The above objects are realised in a second aspect by a heat exchanger plate for a plate heat exchanger for treatment of a liquid feed, heat exchanger plate defining each heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part,

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa,

a first edge part between the first vertical edge and the first part, and

a second edge part between the second vertical edge and the second part, the ridges and valleys in the first edge part and second edge part extending at an oblique angle relative to the central vertical axis.

[0049] The above heat exchanger plate according to the second aspect is preferably used in a plate heat exchanger according to the first aspect.

[0050] The above objects are realised in a third aspect by a method of manufacturing a plate

heat exchanger for treatment of a liquid feed, the method comprising providing a plurality of heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part,

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa,

a first edge part between the first vertical edge and the first part, and

a second edge part between the second vertical edge and the second part, the ridges and valleys in the first edge part and second edge part extending at an oblique angle relative to the central vertical axis, and

arranging the heat exchanger plates successively in a plate package forming the heat exchanger, whereby every second plate is turned about the central axis such that ridges fall into valleys of opposing plates in the first and second parts and opposing ridges of opposing plates contact each other in the first and second edge part.

[0051] The above method according to the third aspect is preferably used together with heat exchanger plates according to the second aspect to manufacture a plate heat exchanger according to the first aspect.

[0052] The evaporation section is located in the lower part of the plate package, the condensation section is located in the upper part of the plate package and the separation section is located in between the evaporation section and the condensation section.

[0053] The above objects are realised in a fourth aspect by a plate heat exchanger for treatment of a liquid feed, the heat exchanger comprising a plate package having a plurality of successively arranged heat exchanger plates, each heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an

evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis, the ridges and valleys in the central part extending at an oblique angle relative to the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part, and

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa,

whereby adjacent heat exchanging plates are arranged such that ridges fall into valleys of opposing plates in the first and second parts and opposing ridges of opposing plates contact each other in the central part.

[0054] The above objects are realised in a fifth aspect by heat exchanger plate for a plate heat exchanger for treatment of a liquid feed, heat exchanger plate defining each heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis, the ridges and valleys in the central part extending at an oblique angle relative to the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part, and

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa.

[0055] The above objects are realised in a sixth aspect by a method of manufacturing a plate heat exchanger for treatment of a liquid feed, the method comprising providing a plurality of heat exchanger plate defining a first vertical edge, an opposite second vertical edge extending parallel to the first vertical edge and a central vertical axis extending substantially centrally between and in parallel with the first vertical edge and the second vertical edge, each heat exchanger plate further defining an evaporation section for vaporizing the feed, a condensation section for condensing the vaporized feed, and a separation section for separating vaporized feed and non-vaporized feed, the separation section being located between the evaporation section and the condensation section along the direction of the central vertical axis and forms alternating ridges and valleys, the separation section defines:

a central part extending on both sides of the central vertical axis, the ridges and valleys in the central part extending at an oblique angle relative to the central vertical axis,

a first part extending between the first vertical edge and the central part, the ridges and valleys in the first part extending horizontally and connect with respective ridges and valleys in the central part, and

a second part extending between the second vertical edge and the central part, the ridges and valleys in the second part extending horizontally and connect with respective ridges and valleys in the central part, the ridges in the first part being horizontally level with the valleys in the second part and vice versa, and

arranging the heat exchanger plates successively in a plate package forming the heat exchanger, whereby every second plate is turned about the central axis such that ridges fall into valleys of opposing plates in the first and second parts and opposing ridges of opposing plates contact each other in the central part.

Brief description of the drawings

[0056]

Fig. 1 discloses a side view of a plate heat exchanger

Fig. 2 discloses a front view of a prior art heat exchanging plate

Fig. 3 discloses how the horizontally oriented ridges and valleys fall into each other

Fig. 4 discloses a front view of a heat exchanging plate

Fig. 5 discloses view of the rear side of a heat exchanger plate

Fig. 6 discloses the separation section of a heat exchange plate

Fig. 7 discloses two opposite plates of which one has been turned 180 degrees

Detailed description of the drawings

[0057] Fig. 1 discloses a side view of a plate heat exchanger 10 of the invention. In the following description an application with respect to desalination of seawater is described, i.e. the feed is sea water. However, it is to be noted that the invention is not limited to the feed being sea water but may also refer to any other treatment, for instance distillation of a liquid. The plate heat exchanger comprises a large number of compression moulded heat exchanger plates 12, which are provided in parallel to each other and successively in such a way that they form a plate package 14. The plate package 14 is provided between a frame plate 16 and a pressure plate 18.

[0058] Between the heat exchanger plates 12, first plate interspaces 20 and second plate interspaces 22 are formed. The first plate interspaces 20 and the second plate interspaces 22 are provided in an alternating order in the plate package 14 in such a way that substantially each first plate interspace 20 is neighbouring two second plate interspaces 22, and substantially each second plate interspace 22 is neighbouring two first plate interspaces 20. Different sections in the plate package 14 are delimited from each other by means of gaskets (not shown) in each plate interspace whereby the first plate interspace 20 includes a first type gasket (not shown) and the second plate interspace 22 includes a second type gasket (not shown). The plate package 14, i.e. the heat exchanger plates 12 and the gaskets (not shown) provided therebetween, is kept together by means of schematically indicated tightening bolts 24 in a manner known per se.

[0059] The plate package 14 is connected to a cooling water inlet conduit 26, a cooling water outlet conduit 28 and a fresh water outlet conduit 30. The cooling water is typically sea water and thus the cooling water outlet conduit 28 is connected to a sea water inlet conduit 32 in order to recover the heat absorbed by the cooling water. The plate package 12 is further connected to a heating fluid inlet conduit 34 and a heating fluid outlet conduit 36. The heating fluid is used for vaporizing the feed, i.e. the sea water which is entering the plate package 14 through the sea water inlet conduit 32. The heating fluid may be heated water, such as jacket water from a ship's engine. The condensed fresh water is leaving the plate package 14 through the fresh water outlet conduit 30.

[0060] Fig. 2 discloses a front view of a prior art heat exchanging plate 12 having an evaporation section 40, a separation section 44 and a condensation section 42. The plate 12 also defines centrally located ports 46 48 50 52 54 along the centre axis C, The ports 46 48 constituting cooling fluid outlet and inlet ports, the port 50 constituting a fresh water outlet port and the ports 52 54 constituting heating fluid inlet and outlet ports. The separation section defines transversally oriented ridges 56 and valleys 58. The plate also defines a gasket 38 in a gasket groove.

[0061] Fig. 3 discloses how the horizontally oriented ridges 56 and valleys 58 fall into each

other in two adjacent plates 12 12'. It is also illustrated how the press depth of the ridges and valleys is increased in the separation section. The ridges 56 and valleys 58 define a press depth such that the lowest part of the upper plate 12 is lower than the highest part of the adjacent plate 12'. In this way the flow path from the evaporation section to the condensation section will be increased and the changes of direction of the flow over the corrugations will be increased, which will improve the separation of liquids from the vaporized feed, however, the press depth of the ridges 56 and valleys 58 must be reduced in locations where the ridges 56 and valleys 58 should contact the neighbouring plate..

[0062] Fig. 4 discloses a front view of a heat exchanging plate 12 according to the present invention. Each heat exchanger plate 12 has a first vertical edge 60, an opposite second vertical edge 60' substantially parallel with the first vertical edge 60 and a centre axis C extending in the vertical direction substantially centrally between the vertical edges 60, 60'. The centre axis C extending substantially vertically when the plate package is located in a normal position of use.

[0063] The heat exchanger plate comprises an evaporation section 40 at the bottom for evaporating the feed, i.e. the sea water, a condensation section 42 at the top for condensing the evaporated feed and a separation section 44 located in between the evaporation section 40 and the condensation section 42 for separating evaporated feed and non-evaporated feed. Vaporized feed is allowed to flow from the evaporation section 40 via the separation section 44 to the condensation section 42.

[0064] The evaporation section 40 and the condensation section 42 are corrugated defining valleys and ridges having oblique angles forming a cross corrugated pattern together with the opposing plate in order to increase the heat transfer through the heat exchanger plate 12. A first plate interspace is formed by arranging two plates 12 face-to-face having a gasket 38 of a first type located in-between the heat exchanger plates. The two plates forming the plate interspace are identical, however, one of the heat exchanger plates is turned 180 degrees about the centre axis C. In this way the corrugation of the heat exchanger plates may be arranged such that opposing ridges form a cross shaped pattern and contact each other at contact points in the evaporation section 40 and the condensation section 42 .

[0065] The heat exchanger plate 12 defines one or more apertures 70 located between the evaporation section 40 and the separation section 44 for allowing some vaporized feed from the evaporation section 40 to pass to the opposite plate interspace which includes a parallel separation section. Further, three upper vapor ports 70' are located between the separation section 44 and the condensation section 42 adjacent the first vertical edge 60 for allowing vaporized feed to pass through the heat exchanger plate 12 to the condensation section 42.

[0066] Located adjacent the second edge 60' is a cooling water outlet port 46, a cooling water inlet port 48 and a fresh water outlet port 50. The cooling water inlet port 46 is communicating with the cooling water inlet conduit, the cooling water outlet port 48 is communicating with the cooling water outlet conduit and the fresh water outlet port 50, which collects the condensed

feed from the condensation section 42, is communicating with the fresh water outlet conduit.

[0067] Centrally located adjacent the evaporation section 40 is a heating fluid inlet port 52 and a heating fluid outlet port 54 is provided. The heating fluid inlet port 52 is communicating with the heating fluid inlet conduit and the heating fluid outlet port 54 is communicating with the heating fluid outlet conduit. Additionally, a feed inlet port 72 connected to the sea water inlet conduit for supplying sea water to the evaporation section 40 is centrally located adjacent the bottom and two outlet ports 74 74' for collecting the non-evaporated feed flowing down from the separation section 44 are located on opposite sides of but separated from feed inlet port 72 at the bottom of the plate 12.

[0068] At the upper part of the separation section 44 flow guiding elements 76 may be provided. The flow guiding element 76 directs the vapor flow into the separation section and prevents the flow from taking the direct route through the separation section 44 into the condensation section 42, reducing the risk of carryover of non-evaporated feed.

[0069] Fig. 5 discloses view of the rear side of a heat exchanger plate 12' and a second type gasket 38' of a plate heat exchanger according to the present invention. The heat exchanger plate 12' is thus the same as the heat exchanger plate 12 except that it has been turned 180 degrees about the centre axis 46. It defines a heating section 40' opposite the evaporation section and a cooling section 42' opposite the condensation section. The cooling water inlet port 46 and the cooling water outlet port 48 communicate with the cooling section 42' whereas the heating fluid inlet port 52 and the heating fluid outlet port 54 communicate with the heating section 40'. The cooling section 42' and the heating section 40' are sealed off relative to the other ports, respectively. The cooling section 42' is arranged to cool the opposite condensing section and the heating section 40' is arranged to heat the opposite evaporation section. The rear side forms a second plate interspace.

[0070] The rear side of a heat exchanger plate 12' also includes a separation section 44' between the heating section 40' and the cooling section 42'. Vaporized feed is introduced via the lower vapor aperture 70 from the first plate interspace. The separation section 44' functions identically to the one on the opposite side and separates evaporated feed and non-evaporated feed. The evaporated feed flows up through the upper vapor apertures 70' whereas the non-evaporated feed flows down to the outlets 74 74'.

[0071] Fig. 6 discloses the separation section 44 of a heat exchange plate 12 according to the present invention. The plate 12 comprises parallel ridges 56 and valleys 58. The plate 12 defines a first vertical edge 60 and a second vertical edge 60'. The first vertical edge 60 and a second vertical edge 60' having a gasket for sealing against an opposite plate (not shown). The plate 12 further defines a centre axis in-between the first- and second vertical edges 60 60'. The separation section 44 defines a central part 62 at the centre axis C, a first part 64 between the first vertical edge 60 and the centre part 62 and a second part 66 between the second vertical edge 60' and the centre part 62.

[0072] In the first- and second parts 64 66 the corrugations extend transversally. The ridges 56 in the first part 64 are horizontally level with the respective valleys 58 in the second part 66, and vice versa. In this way, when plates are positioned face-to-face in the plate package, wherein every second plate is turned 180 degrees about the centre axis, the ridges 56 in the first part 64 will fall into valleys 58 in the second part 66 and vice versa. The plate interspaces in the first- and second part 64 66 will thus form a meandering flow path in the vertical direction.

[0073] In the central part 62, the corrugations define an oblique angle relative to the central axis C. Preferably, the angle is about 45 degrees. In this way, when the plates are positioned face-to-face in the plate package, the ridges 56 and valleys 58 of opposing plates will form a cross-corrugated pattern. In this way the ridges 56 and valleys 58 of the first- and second parts 64 66 are interconnected in the central part 62. Opposing ridges 56 of opposing plates will contact at contact points, and valleys 58 will form ridges in the neighbouring plate interspace and also contact opposing ridged in the neighbouring plate interspace, which will improve the structural stability of the plate package in the separation section 42. The width of the central part 62 is significantly smaller than the width of the respective first- and second parts 64 66 as the effective separation takes place in the first- and seconds parts 62.

[0074] The separation section 44 also comprises apertures 70 at the bottom. This is to allow vaporized feed to enter both sides of the plate as both plate interspaces may be used for separation. Vaporized feed may re-enter the plate interspace having the condensation section (not shown here) via apertures 70' at the top of the separation section 44. The condensation section may also in an alternative embodiment be located in the opposite plate interspace relative to the evaporation section.

[0075] Between the first vertical edge 60 and the first part 64, and, between the second vertical edge 60' and the second part 66, respectively, there are located respective edge parts 68 68'. In the edge parts 68 68', the corrugations define an oblique angle relative to the central axis C, similar to the central part 62. Preferably, the angle is about 45 degrees. In this way, when the plates are positioned face-to-face in the plate package, the ridges 56 and valleys 58 of opposing plates will form a cross-corrugated pattern. Opposing ridges 56 of opposing plates will contact at contact points, and valleys 58 will form ridges in the neighbouring plate interspace and also contact opposing ridged in the neighbouring plate interspace, which will improve the structural stability of the plate package at the gasket located at the first and second vertical edges 60 60', respectively. The width of the edge parts 68 68' are similar to the width of the central part 62 as the effective separation takes place in the first- and seconds parts 64 66.

[0076] Fig. 7 discloses two opposite plates 38 38' of which one has been turned 180 degrees about the centre axis and positioned face-to-face in the plate package. In the first and second parts 64 66, the corrugations fall into each other without contact, whereas in the central part 62 and in the edge parts 68 68', the corrugations define a cross-corrugated pattern.

Reference numerals

[0077]

- 10. plate heat exchanger
- 12. heat exchanger plates
- 14. plate package
- 16. frame plate
- 18. pressure plate
- 20. first plate interspaces
- 22. second plate interspaces
- 24. tightening bolts
- 26. cooling water inlet conduit
- 28. cooling water outlet conduit
- 30. fresh water outlet conduit
- 32. sea water inlet conduit
- 34. heating fluid inlet conduit
- 36. heating fluid outlet conduit
- 38. gasket
- 40. evaporation section
- 42. condensation section
- 44. separation section
- 46. cooling fluid outlet
- 48. cooling fluid inlet
- 50. fresh water outlet
- 52. heating fluid inlet
- 54. heating fluid outlet

- 56. ridge
- 58. valley
- 60. vertical edges
- 62. central part
- 64. first part
- 66. second part
- 68. edge parts
- 70. apertures
- 72. feed inlet
- 74. brine outlet
- 76. flow guide
- C. centre vertical axis

A (') denotes a similar features in a different embodiment.

REFERENCES CITED IN THE DESCRIPTION

Cited references

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VARMEVEKSLERPLADE OG PLADEVARMEVEKSLER TIL BEHANDLING AF EN FLYDENDE
FØDESTRØM

PATENTKRAV

1. Varmevekslerplade (12) til en pladevarmeveksler (10) til behandling af en flydende fødestrøm, idet
 - 5 varmevekslerpladen (12) definerer en første vertikal kant (60), en modstillet anden vertikal kant (60'), der strækker sig parallelt med den første vertikale kant (60), og en vertikal midterakse (C), der strækker sig i det væsentlige centralt mellem og parallelt med den første vertikale kant (60) og den anden vertikale kant (60'), idet hver varmevekslerplade (12) yderligere definerer et fordampningsafsnit (40) til inddampning af fødestrømmen, et kondensationsafsnit (42) til kondensering af den inddampede fødestrøm og et
 - 10 separeringsafsnit (44) til separering af inddampet fødestrøm og ikke-inddampet fødestrøm, idet separeringsafsnittet (44) er lokaliseret mellem fordampningsafsnittet (40) og kondensationsafsnittet (42) langs den vertikale midterakses (C) retning og danner alternerende toppe (56) og dale (58), hvor separeringsafsnittet (44) definerer:
 - en midterdel (62), der strækker sig på begge sider af den vertikale midterakse (C),
 - 15 en første del (64), der strækker sig mellem den første vertikale kant (60) og midterdelen (62), idet toppene (56) og dalene (58) i den første del (64) strækker sig horisontalt og er forbundet med respektive toppe (56) og dale (58) i midterdelen (62),
 - en anden del (66), der strækker sig mellem den anden vertikale kant (60') og midterdelen (62), idet toppene (56) og dalene (58) i den anden del (66) strækker sig horisontalt og er forbundet med respektive toppe
 - 20 (56) og dale (58) i midterdelen (62), idet toppene (56) i den første del (64) horisontalt står i vater med dalene (58) i den anden del (66) og vice versa, kendetegnet ved, at varmevekslingspladen (12) yderligere definerer
 - en første kantdel (68) mellem den første vertikale kant (60) og den første del (64) og
 - en anden kantdel (68') mellem den anden vertikale kant (60') og den anden del (66), idet toppene (56) og dalene (58) i den første kantdel (68) og den anden kantdel (68') strækker sig i en skrå vinkel i forhold
 - 25 til den vertikale midterakse (C).
 2. Varmevekslerplade (12) ifølge krav 1, hvor toppene (56) og dalene (58) i den første og den anden del (64, 66) definerer en første pressedybde, mens toppene (56) og dalene (58) i midterdelen (62) og/eller i den første og den anden kantdel (68, 68') definerer en anden pressedybde, hvor den første pressedybde er større end den anden pressedybde.
 3. Varmevekslerplade (12) ifølge et hvilket som helst af de foregående krav, hvor kantdelenes bredde
 - 30 er mindre end bredden af hver af den første og den anden del (64, 66).
 4. Varmevekslerplade (12) ifølge et hvilket som helst af de foregående krav, hvor kantdelene (68, 68') definerer et område, der er mindre end 20 % af området for hver af den første og den anden del (64, 66), fortrinsvis mindre end 10 %, mere fortrinsvis mindre end 5 %.
 5. Varmevekslerplade (12) ifølge et hvilket som helst af de foregående krav, hvor kantdelenes (68, 68')
 - 35 bredde i det væsentlige er lig med afstanden mellem midten af nabostillede toppe (56) i den første og den anden del (64, 66).

6. Pladevarmeveksler (10) til behandling af en flydende fødestrøm, hvilken varmeveksler omfatter en pladepakke (14) med en flerhed af successivt anbragte varmevekslerplader (12), idet hver varmevekslerplade (12) er ifølge et hvilket som helst af kravene 1-5,

5 hvor nabostillede varmevekslerplader (12) er anbragt således, at toppe (56) falder ind i dale (58) på modstående plader (12) i den første og den anden del (64, 66), og modstående toppe (56) på modstående plader (12) berører hinanden i den første kantdel (68) og den anden kantdel (68').

7. Pladevarmeveksler (10) ifølge krav 6, hvor toppene (56) og dalene (58) i midterdelen (62) strækker sig i en skrå vinkel i forhold til den vertikale midterakse (C), således at modstående toppe (56) på modstående plader (12) berører hinanden i midterdelen (62).

10 8. Pladevarmeveksler (10) ifølge et hvilket som helst af kravene 6-7, hvor pladepakken (14) definerer første plademellemrum (20) og sekundære plademellemrum (22), anbragt i alternerende rækkefølge, idet hvert plademellemrum (20, 22) er omsluttet af en pakning (38), der strækker sig langs den første og den anden vertikale kant (60, 60') på hver plade (12).

15 9. Pladevarmeveksler (10) ifølge krav 8, hvor separeringsafsnittet (44) er anbragt i både det første og det andet plademellemrum (20, 22).

10. Pladevarmeveksler (10) ifølge krav 9, hvor varmevekslerpladen (12) er forsynet med åbninger (70 70') i den første og den anden passage til kommunikation mellem plademellemrummene (20, 22).

11. Fremgangsmåde til fremstilling af en pladevarmeveksler (10) til behandling af en flydende fødestrøm, hvilken fremgangsmåde omfatter

20 tilvejebringelse af en flerhed af varmevekslerplade (12), der definerer en første vertikal kant (60), en modstillet anden vertikal kant (60'), der strækker sig parallelt med den første vertikale kant (60), og en vertikal midterakse (C), der strækker sig i det væsentlige centralt mellem og parallelt med den første vertikale kant (60) og den anden vertikale kant (60'), idet hver varmevekslerplade (12) yderligere definerer et fordampningsafsnit (40) til inddampning af fødestrømmen, et kondensationsafsnit (42) til kondensering af
25 den inddampede fødestrøm og et separeringsafsnit (44) til separering af inddampet fødestrøm og ikke-inddampet fødestrøm, idet separeringsafsnittet (44) er lokaliseret mellem fordampningsafsnittet (40) og kondensationsafsnittet (42) langs den vertikale midteraksen (C) retning og danner alternerende toppe (56) og dale (58), hvor separeringsafsnittet (44) definerer:

en midterdel (62), der strækker sig på begge sider af den vertikale midterakse (C),

30 en første del (64), der strækker sig mellem den første vertikale kant (60) og midterdelen (62), idet toppene (56) og dalene (58) i den første del (64) strækker sig horisontalt og er forbundet med respektive toppe (56) og dale (58) i midterdelen (62),

en anden del (66), der strækker sig mellem den anden vertikale kant (60') og midterdelen (62), idet toppene (56) og dalene (58) i den anden del (66) strækker sig horisontalt og er forbundet med respektive toppe
35 (56) og dale (58) i midterdelen (62), idet toppene (56) i den første del (64) horisontalt står i vater med dalene (58) i den anden del (66) og vice versa,

en første kantdel (68) mellem den første vertikale kant (60) og den første del (64) og

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en anden kantdel (68') mellem den anden vertikale kant (60') og den anden del (66), idet toppene (56) og dalene (58) i den første kantdel (68) og den anden kantdel (68') strækker sig i en skrå vinkel i forhold til den vertikale midterakse (C), og

5 anbringelse af varmevekslerpladerne (12) successivt i en pladepakke (14), der udgør varmeveksleren (10), hvor hver anden plade (12) er drejet omkring midteraksen (C), således at toppe (56) falder ind i dale (58) på modstående plader (12) i den første og den anden del (64, 66), og modstående toppe (56) på modstående plader (12) berører hinanden i den første og den anden kantdel (68').

12. Anvendelse af pladevarmeveksleren (10) ifølge et hvilket som helst af kravene 6-10, hvor den flydende fødestrøm er havvand.

DRAWINGS

Drawing

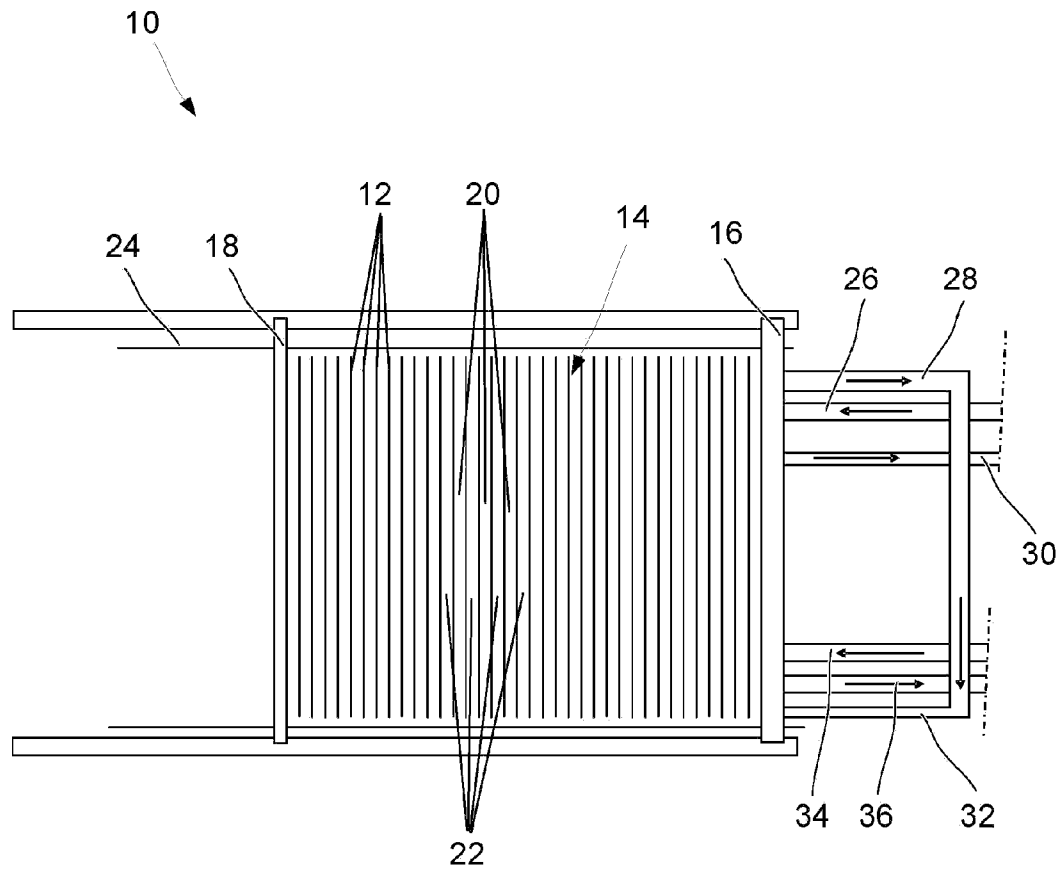
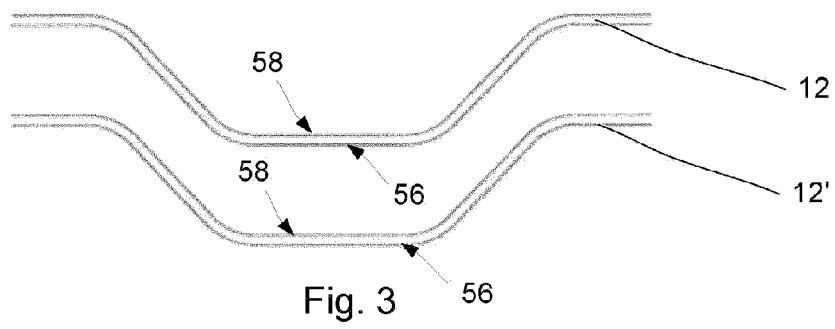
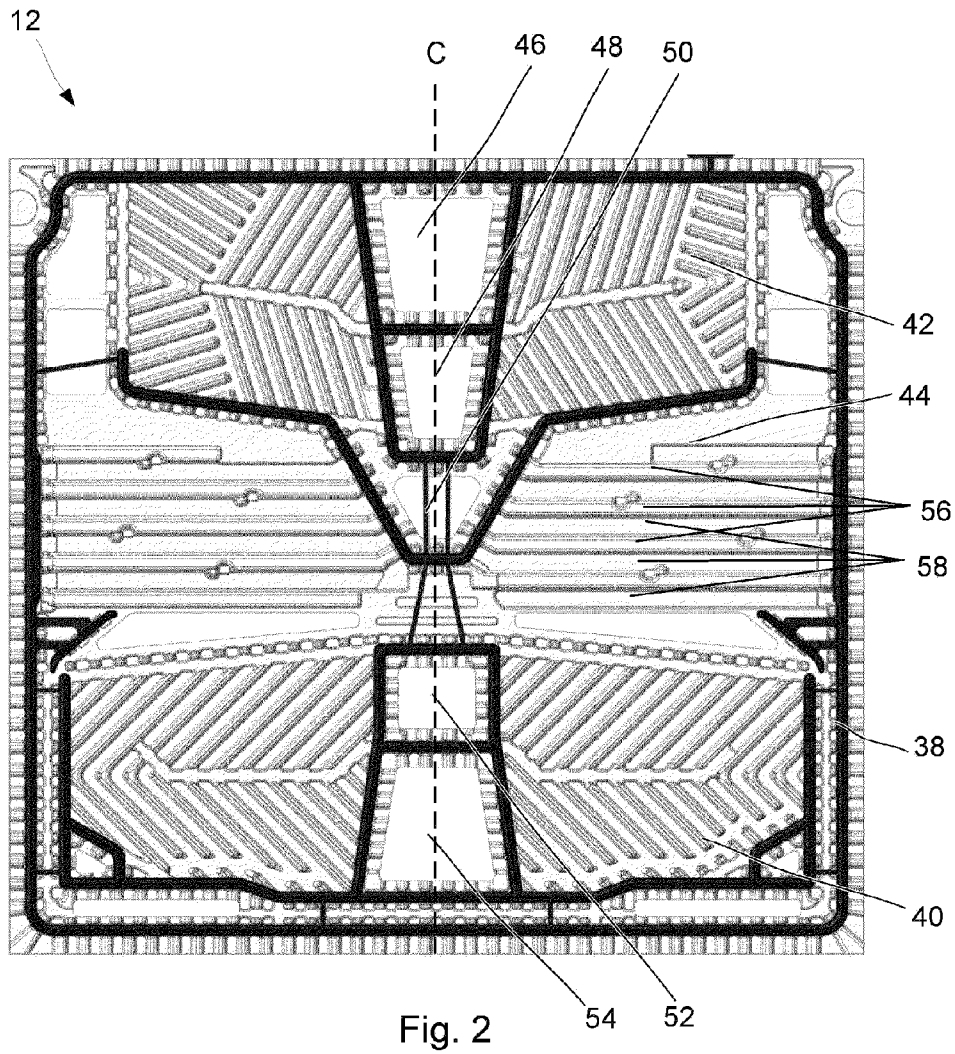
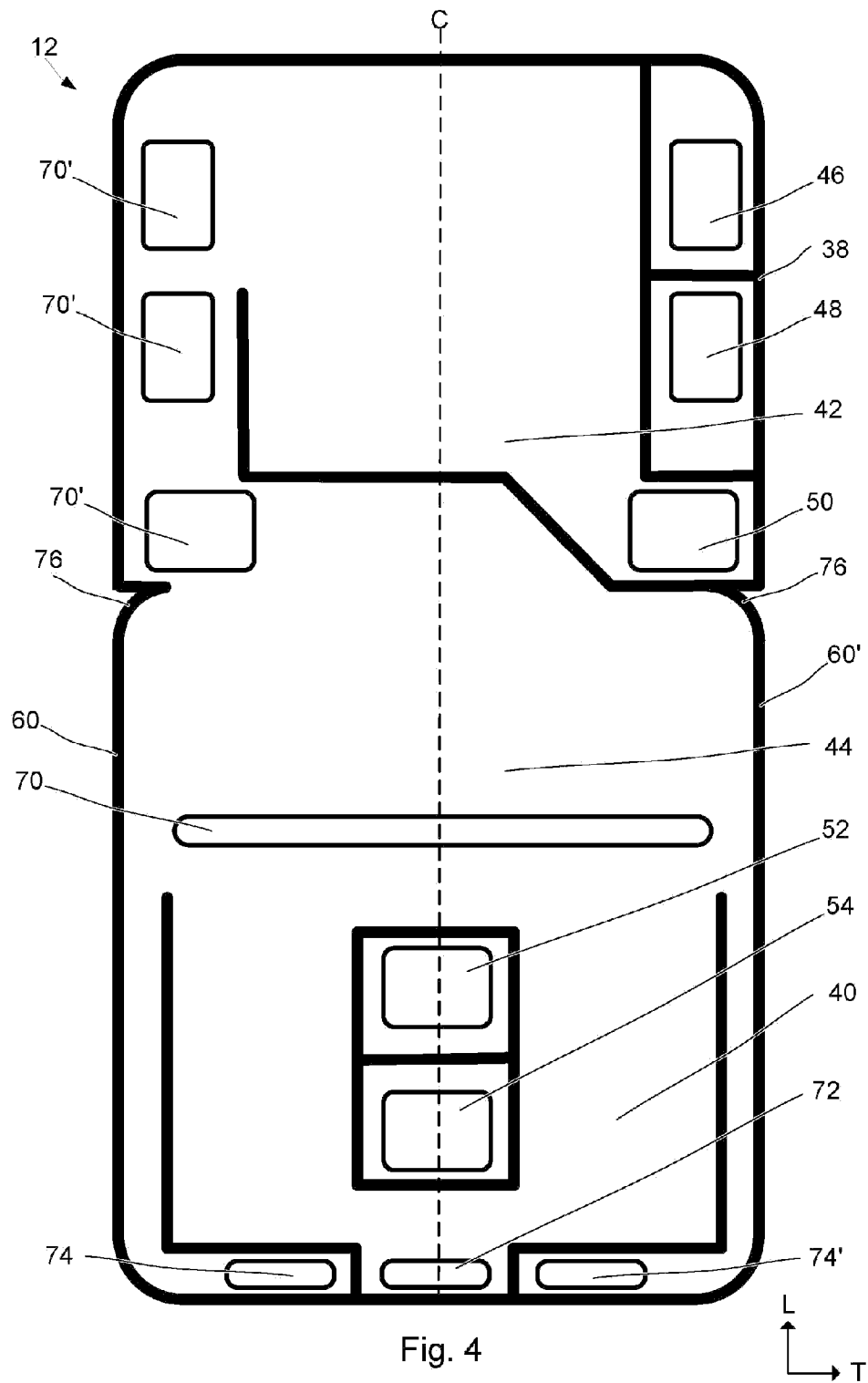
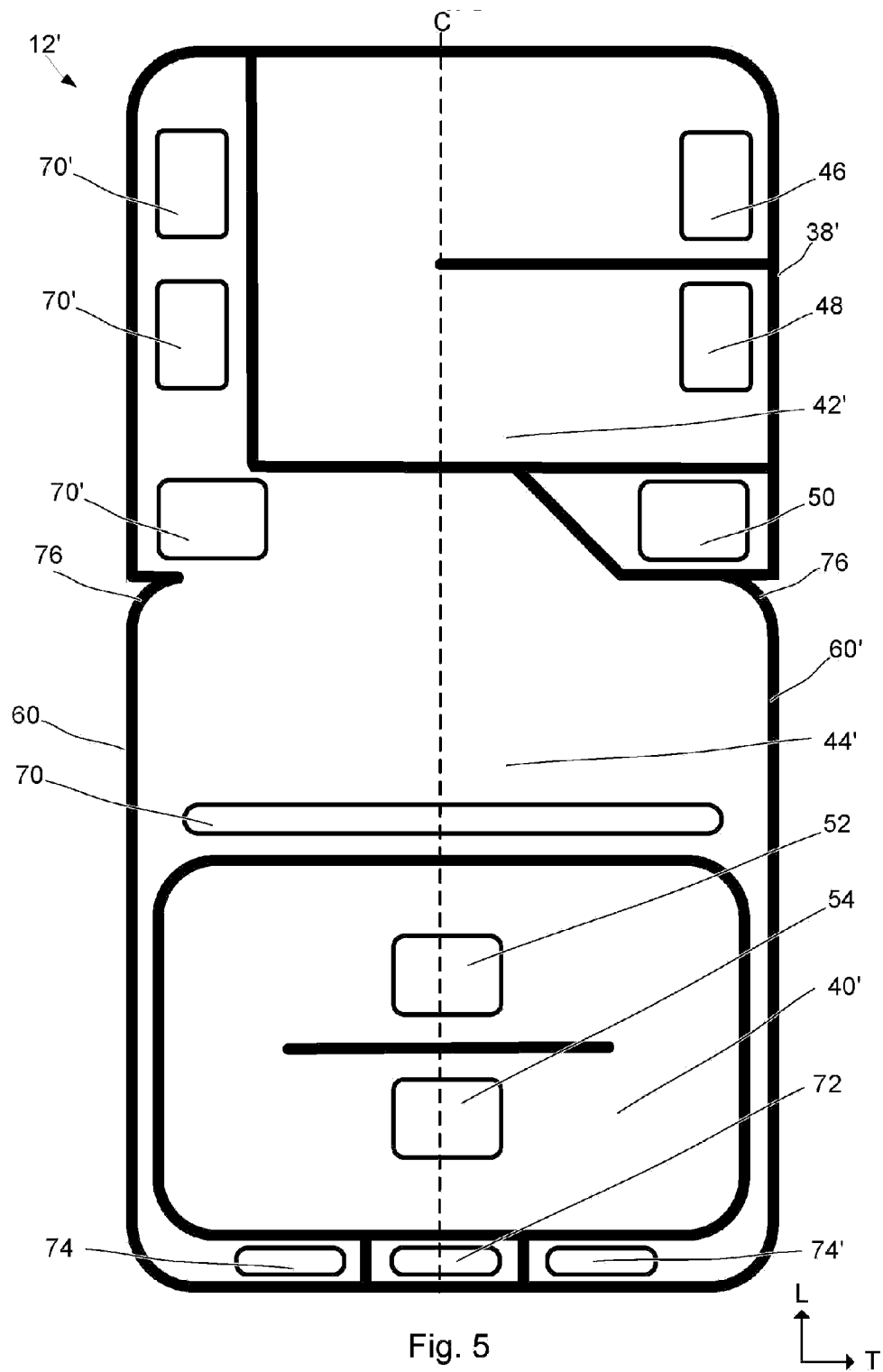


Fig. 1







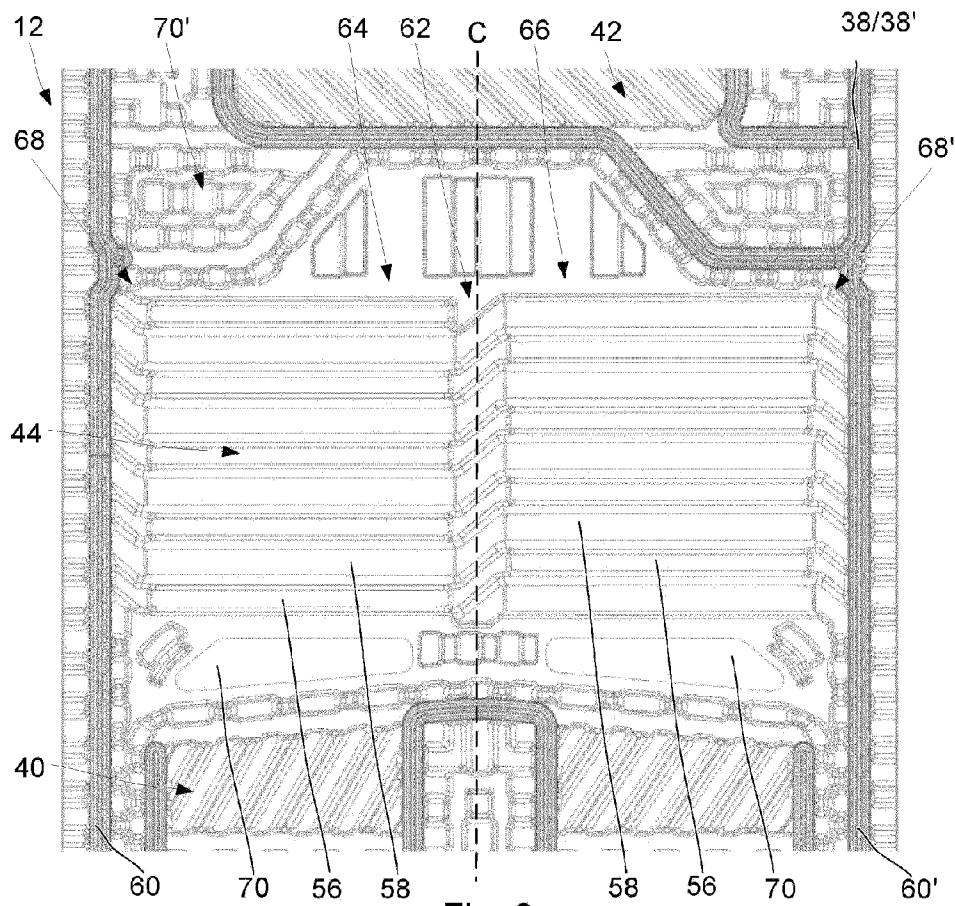


Fig. 6

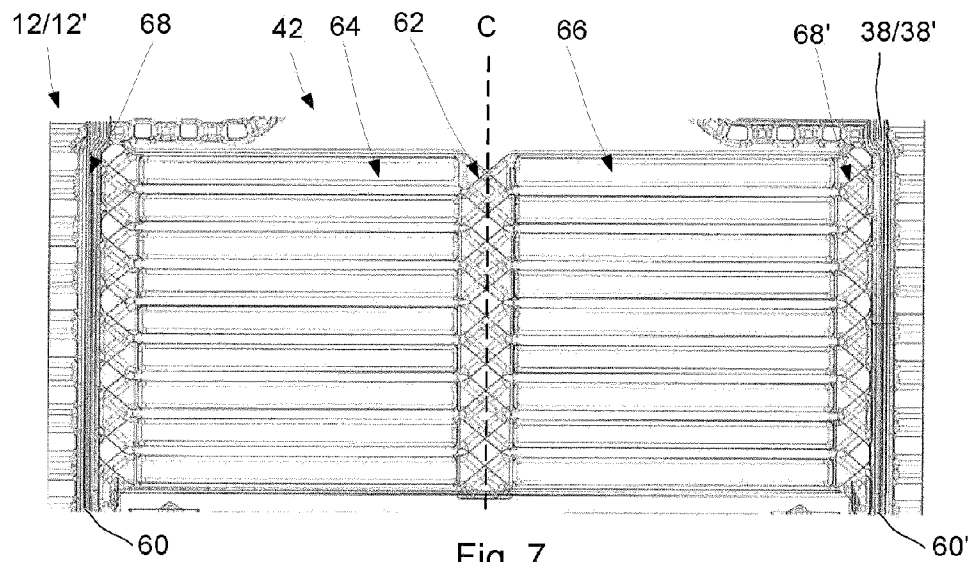


Fig. 7