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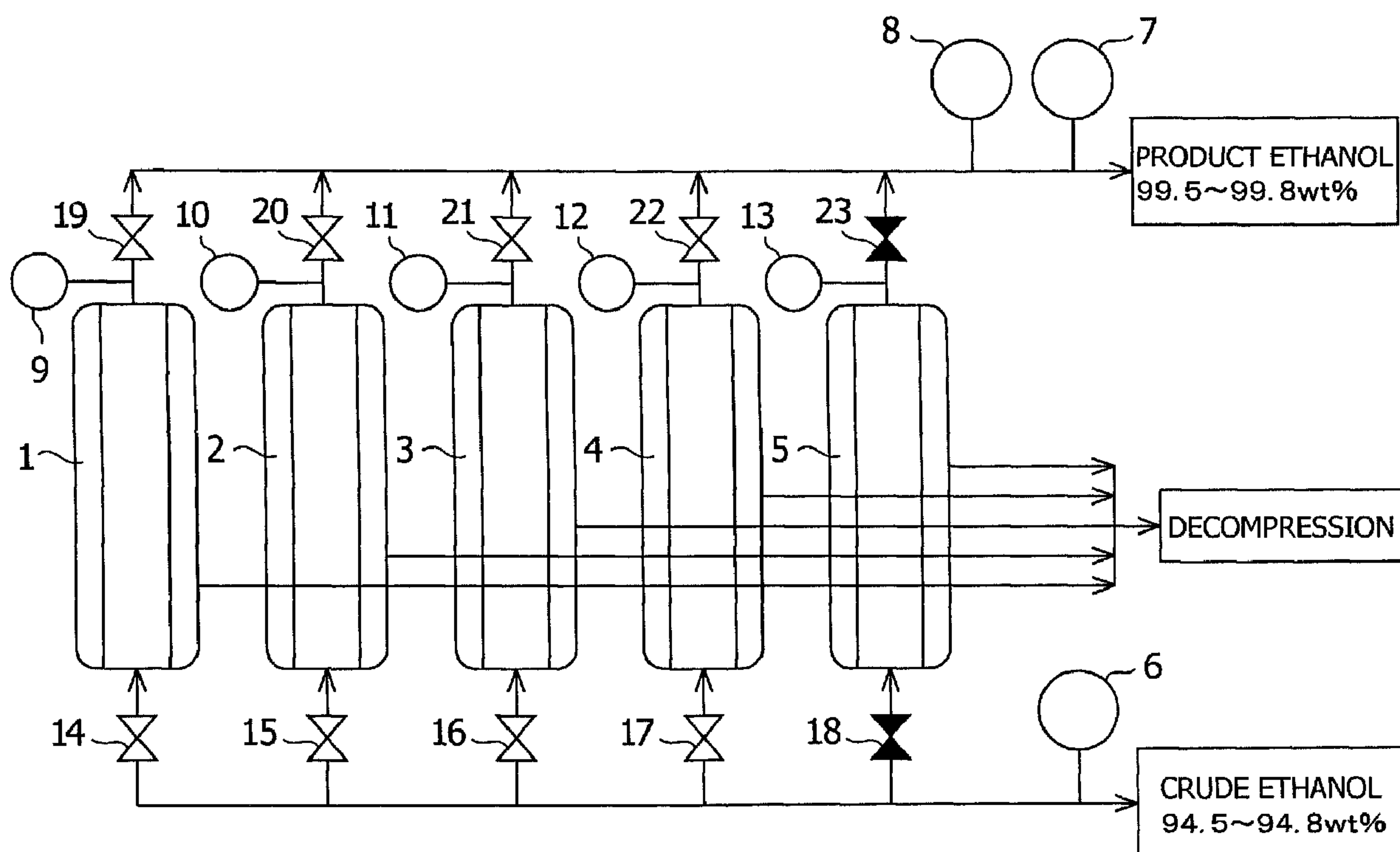
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(54) Title: DEHYDRATING SYSTEM



(57) Abrégé/Abstract:

A dehydrating system is designed to maintain the availability of a plant having the dehydrating system using a water separation membrane by allowing a water separation membrane unit to be replaced while the plant is in operation. The dehydrating system comprises at least two water separation membrane units in use arranged parallel to the direction of flow of a fluid to be processed, is configured so that at least one spare water separation membrane unit can be installed parallel to the direction of flow of the fluid to be processed with respect to the at least two water separation membrane units, having monitoring devices for the product fluid to be taken out, and maintains the properties of the product fluid by operating the spare water separation membrane unit depending on the properties of the product fluid monitored by the monitoring devices.

ABSTRACT OF THE DISCLOSURE

A dehydrating system is designed to maintain the availability of a plant having the dehydrating system using a water separation membrane by allowing a water separation membrane unit to be replaced while the plant is in operation. The dehydrating system comprises at least two water separation membrane units in use arranged parallel to the direction of flow of a fluid to be processed, is configured so that at least one spare water separation membrane unit can be installed parallel to the direction of flow of the fluid to be processed with respect to the at least two water separation membrane units, having monitoring devices for the product fluid to be taken out, and maintains the properties of the product fluid by operating the spare water separation membrane unit depending on the properties of the product fluid monitored by the monitoring devices.

DEHYDRATING SYSTEM

BACKGROUND OF THE INVENTION

Field of the Invention

The present invention relates to a dehydrating system which uses a water separation membrane, and more specifically relates to a dehydrating system designed to appropriately deal with the degradation of the water separation membrane in dehydrating a mixture of water and ethanol or propanol having an azeotropic composition with water, hereinafter referred to as a fluid to be processed.

Description of the Related Art

Ethanol has been attracting attention as an alternative energy source to replace oil and has a market size estimated at 55,000,000 kL in 2010. However, to use ethanol as a fuel, ethanol must be dehydrated to at least 99.5 wt % after distillation and purification of a crude product obtained from a biomass source such as corn.

For dehydration, a dilute aqueous solution of ethanol has traditionally been concentrated nearly to the azeotropic point of the ethanol/water system by distilling the solution in a distillation column and then this was dehydrated.

There is a dehydration technique which adds an entrainer and dehydrates by azeotropic distillation. However, this technique has some disadvantages, such as a huge amount of thermal energy required because of the need for a step which subjects a ternary system to azeotropic distillation and recovers the entrainer.

In addition, there is also a dehydration technique in which multiple molecular sieve vessels are arranged in parallel and switches are made between them on a batch

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basis for dehydration. However, this technique also has the problem of high energy consumption required for the regeneration of molecular sieve vessels.

Thus, the use of an element without the above disadvantages, such as a water separation membrane, has been considered (Japanese Patent Application Laid-Open No. 58-21629).

However, if pervaporation (PV) using a water separation membrane unit comprising a water separation membrane is adopted, the water separation membrane unit typically has a service life of about 2 years and requires annual replacement of all the water separation membranes. The water separation membrane unit has the problem of reduced availability of the plant using the unit because of the inevitable downtime of the plant during the replacement.

The present invention has been made in view of the above circumstances and has as an object providing a dehydrating system designed to maintain the availability of a plant equipped with a dehydrating system using a water separation membrane by allowing water separation membrane units to be replaced while the plant is in operation.

SUMMARY OF THE INVENTION

To achieve the object, the present invention provides a dehydrating system that separates water from a fluid to be processed, wherein the dehydrating system comprises at least two water separation membrane units in use arranged parallel to the direction of flow of the fluid to be processed; the dehydrating system is configured so that at least one spare water separation membrane unit can be installed parallel to the direction of flow of the fluid to be processed with respect to the at least

two water separation membrane units; the dehydrating system comprises a monitoring device for a product fluid to be taken out; and the dehydrating system maintains the properties of the product fluid by operating the at least one spare water separation membrane unit depending on the properties of the product fluid monitored by the monitoring device.

In the dehydrating system according to the present invention, the fluid to be processed is generally an organic aqueous solution. The organic component of which is preferably one organic component selected from the group consisting of alcohols such as ethanol, propanol, isopropanol, and glycol, carboxylic acids such as acetic acid, ethers such as dimethyl ether and diethyl ether, aldehydes such as acetaldehyde, ketones such as acetone and methyl ethyl ketone, and esters such as ethyl acetate.

An embodiment of the dehydrating system according to the present invention comprises a densitometer monitoring the concentration of the organic component of the product fluid to be taken out of the entire dehydrating system as the monitoring device for the product fluid.

Another embodiment of the dehydrating system according to the present invention comprises a densitometer monitoring the concentration of the organic component of the product fluid to be taken out of each of the water separation membrane units as the monitoring device for the product fluid, wherein the densitometer is installed on each of the water separation membrane units.

Yet another embodiment of the dehydrating system according to the present invention comprises a thermometer monitoring the temperature of the product fluid

to be taken out of each of the water separation membrane units as the monitoring device for the product fluid.

The present invention provides a dehydrating system designed to maintain the availability of a plant equipped with a dehydrating system using a water separation membrane by allowing a water separation membrane unit to be replaced while the plant is in operation.

According to another aspect of the present invention, there is provided a dehydrating system that separates water from an organic aqueous solution to be processed, comprising:

at least two water separation membrane units in use to separate said solution from water arranged parallel to the direction of flow of the organic aqueous solution to be processed, each equipped with an inlet valve;

at least one spare water separation membrane unit which is equipped with an inlet valve and is installed parallel to the direction of flow of the organic aqueous solution to be processed with respect to the at least two water separation membrane units;

a monitoring device for monitoring one of a concentration and a temperature of a product fluid to be taken out; and

an inlet flowmeter and an outlet flowmeter for monitoring the flow rate into and out of said water separation membrane units;

wherein the dehydrating system maintains the properties of the product fluid by operating the spare water separation membrane units depending on the concentration or temperature of the product fluid monitored by the monitoring device, and on the flow rate monitored by said outlet flowmeter.

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According to a further aspect of the present invention, there is provided a dehydrating system that separates water from a fluid to be processed, comprising:

at least two water separation membrane units in use arranged parallel to the direction of flow of the fluid to be processed;

at least one spare water separation membrane unit which is installed parallel to the direction of flow of the fluid to be processed with respect to the at least two water separation membrane units;

a monitoring device configured to monitor a concentration of an organic component of a product fluid and a temperature of the product fluid, the product fluid being taken out of each of the water separation membrane units; and

a control unit configured to control an operation of the at least one spare water separation membrane unit depending on the concentration of the organic component and the temperature of the product fluid monitored by the monitoring device to maintain properties of the product fluid.

According to another aspect of the present invention, there is provided a dehydrating method comprising:

providing a plurality of water separation membrane units installed parallel to the direction of flow of a fluid to be processed, the plurality of water separation membrane units comprising at least two operative water separation membrane units and at least one spare water separation membrane unit;

separating water from the fluid through the at least two operative water separation membrane units;

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monitoring one of a concentration of an organic component of a product fluid and a temperature of the product fluid to be taken out of each operative water separation unit; and

operating the at least one spare water separation membrane unit depending on the monitoring to maintain properties of the product fluid.

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a schematic view illustrating an embodiment of the dehydrating system according to the present invention.

Description of Reference Numerals

1 to 5: Water separation membrane units

6: Inlet flowmeter

7: Outlet flowmeter

8: Outlet densitometer

9, 10, 11, 12, and 13: Individual densitometers

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENT

The dehydrating system according to the present invention will be described in detail with reference to an embodiment thereof.

FIG. 1 is an embodiment of the dehydrating system according to the present invention. The dehydrating system according to the embodiment assumes that the fluid to be processed for dehydration is crude ethanol. It is assumed that this crude

ethanol is an aqueous solution having an ethanol concentration of 94.5 wt % to 94.8 wt % (both inclusive). In other words, crude ethanol containing ethanol as the organic component is considered to be the fluid to be processed. The final product fluid, namely, product ethanol (absolute ethanol), has an ethanol concentration of 99.5 wt % to 99.8 wt % (both inclusive).

The dehydrating system according to the embodiment consists mainly of water separation membrane units 1 to 5, an inlet flowmeter 6, an outlet flowmeter 7, outlet densitometer 8, and individual densitometers 9 to 13. The dehydrating system further has inlet valves 14 to 18 and outlet valves 19 to 23 for the water separation membrane units 1 to 5.

The water separation membrane units 1 to 5 are units to separate the crude ethanol into absolute ethanol and water. The water separation membrane as a constituent of the water separation membrane units is preferably a silica or zeolite inorganic water separation membrane having a pore size of 10 angstroms or less. The water separation membrane may also be a carbon membrane.

In addition, the inorganic water separation membrane according to Japanese Patent No. 2808479 is also applicable. This inorganic water separation membrane is an acid-resistant composite separation membrane, obtained by supporting silica gel obtained through hydrolysis of alkoxysilane containing an ethoxy group or a methoxy group within the pores of an inorganic porous body, which can be produced by a production process including the following steps 1 to 11.

The porous substrate described below is generally a ceramic substrate such as alumina, silica, zirconia, or titania, and preferably a cylindrical substrate which has multiple inner tubes having a circular cross section in the longitudinal direction. In

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the following steps 1 to 11, an inorganic water separation membrane is formed to cover the inner wall of each of these inner tubes. This is the meaning of the phrase "supporting silica gel obtained through hydrolysis of alkoxysilane containing an ethoxy group or a methoxy group within the pores of an inorganic porous body."

An organic membrane such as a polyvinyl alcohol membrane, a polyimide membrane, and a polyamide membrane can be used as the water separation membrane in addition to the inorganic water separation membranes. These organic membranes also change over time and are applicable to the present invention.

Step 1: In preparation conditions for multiple silica sols produced by varying the mixing ratio of alkoxysilane, water, and an acid catalyst as the raw materials of silica sol, the mixing ratios of the raw materials of the silica sol to be supported are divided into two types: one for silica sol 1 and the other for silica sol 2.

Step 2: The weight of water relative to the weight of alkoxysilane as one of the raw materials of silica sol 1 is 0.5 to 2.0 (both inclusive), whereas the weight of an acid catalyst as a reaction catalyst relative to the weight of alkoxysilane is 0.01 to 0.1 (both inclusive).

Step 3: The weight of water relative to the weight of alkoxysilane as one of the raw materials of silica sol 2 is 2.0 to 50 (both inclusive), whereas the weight of an acid catalyst as a reaction catalyst relative to the weight of alkoxysilane is 0.01 to 0.5 (both inclusive).

Step 4: While the raw materials of silica sol 1 are kept at the boil, the solutions about 25, 20, and 15 minutes after the start of boiling are defined as 1-A solution, 1-B solution, and 1-C solution, respectively.

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Step 5: The raw materials of silica sol 2 are stirred and mixed at room temperature for 30 to 90 minutes to produce silica sol 2.

Step 6: After the silica sol 1-A solution is supported on the surface of a porous substrate, the porous substrate is burned in an electric furnace set at about 200°C for 5 to 15 minutes (both inclusive), then at about 300°C for 5 to 15 minutes (both inclusive), then about 400°C for 5 to 15 minutes (both inclusive), and finally at about 500°C for 5 to 15 minutes (both inclusive).

Step 7: After the silica sol 1-A solution is further supported on the surface of the porous substrate on which the silica sol 1-A solution has been supported, the operation of step 6 above is repeated two or three times.

Step 8: Next, after the silica sol 1-B solution is further supported on the surface of the porous substrate on which the silica sol 1-A solution has been supported, the same processing as in steps 6 and 7 above is performed.

Step 9: Next, after the silica sol 1-C solution is further supported on the surface of the porous substrate on which the silica sol 1-B solution has been supported, the same processing as in steps 6 and 7 above is performed.

Step 10: Next, after the silica sol 2 solution is further supported on the surface of the porous substrate on which the silica sol 1-A, 1-B, and 1-C solutions have been supported, the porous substrate is burned in an electric furnace set at about 200°C for 5 to 15 minutes (both inclusive), then at about 300°C for 5 to 15 minutes (both inclusive), then at about 400°C for 5 to 15 minutes (both inclusive), and finally at about 500°C for 5 to 15 minutes (both inclusive).

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Step 11: After the silica sol 2 solution is further supported on the surface of the porous substrate on which the silica sol 2 solution has been supported, the operation of step 10 above is repeated two or three times.

A cylindrical porous substrate supporting an inorganic water separation membrane within each of the inner tubes thereof (covering each inner tube with an inorganic water separation membrane) can be obtained through steps 1 to 11 above. In the present invention, such a substrate, for example, is used as a water separation membrane built into each of the water separation membrane units 1 to 5, each of which has such a water separation membrane built into a container which can be decompressed.

Crude ethanol is preheated to about 90°C by a heat exchanger (not shown in the figure). The crude ethanol flows through the inner tubes of the water separation membrane because the water separation membrane units 1 to 5 are designed so that the crude ethanol is introduced via the inlet flowmeter 6 and inlet valves 14 to 18 into the units by pumps (not shown in the figure). Water is separated from the crude ethanol by decompressing the water separation membrane. The ethanol from which water has been separated is taken out as product ethanol via the outlet valves 19 to 23 and then the outlet densitometer 8 and the outlet flowmeter 7. The outlet concentrations of the water separation membrane units 9 to 13 are monitored by the individual densitometers 9 to 13.

The dehydrating system according to the present embodiment only uses the water separation membrane units 1 to 4, for example, at the initial operation. The total rates of flow into and out of the water separation membrane units 1 to 4 are monitored by the inlet flowmeter 6 and the outlet flowmeter 7. The outlet

densitometer 8 monitors the ethanol concentration of the product ethanol to check that the concentration is maintained at or above the desired set point. At the same time, the individual densitometers 9 to 12 monitor the outlet concentrations of the water separation membrane units 1 to 4. On the other hand, the water separation membrane unit 5 is a spare water separation membrane unit and is not operated at the initial operation.

Water separation membranes generally degrade as they are used. When the characteristics of any of the water separation membrane units 1 to 4 degrade, the spare water separation membrane unit 5 is operated by a technique as described below.

(1) Of the water separation membrane units 1 to 4, the flow rate of the unit whose characteristics have degraded is reduced. Any characteristics degradation is detected by concentrations measured by the individual densitometers 9 to 12. The outlet densitometer 8 monitors the concentration of the product ethanol to check that the concentration is at or above the desired set point. When the outlet flowmeter 7 shows that only a product ethanol flow rate below the set point can be maintained after the flow rate is reduced, the spare water separation membrane unit 5 is operated to maintain the flow rate of the product ethanol.

Such control can be automatically performed by a control unit (not shown in the figure).

On the other hand, in addition, the outlet valve and inlet valve of the water separation membrane unit that is operating worst are closed to stop the operation of the unit. Then, the water separation membrane unit whose operation has been stopped is replaced with a fresh water separation membrane unit. The replaced

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water separation membrane unit is put on standby as a fresh spare water separation membrane unit. The performance of the dehydrating system can be maintained by following the above procedure without stopping the operation thereof.

(2) The technique described in (1) above also makes it possible to operate the spare water separation membrane unit 5 and stop the operation of the water separation membrane unit of which the characteristics have degraded to conduct the replacement of the units without any control such as reducing the flow rate of the degraded unit.

(3) At the initial operation, it is also possible to appropriately reduce the flow rates of the water separation membrane units 1 to 4 without pushing the flow rates to the limit and control the overall outlet flow rate depending on changes in the characteristics of the water separation membrane units.

It is also possible to begin to operate a spare water separation membrane unit on a yearly basis, for example, and replace any of the other water separation membrane units without installing the separate densitometers 9 to 13. If FIG. 1 is used as an example, the water separation membrane units 1 to 4 were stopped and all replaced once about every 2 years.

It is virtually no problem to begin to operate a fresh spare water separation membrane unit and replace a water separation membrane unit once a year. In this case, the number of units to be replaced is half as many as before. For replacement every 6 months, the number of units to be replaced is the same as before because the number of all units in operation is four. In either case, there is no need to stop the operation of the entire dehydrating system.

In addition, the number of water separation membrane units in use and the number of spare water separation membrane units are not limited to the numbers shown by the embodiment in FIG. 1.

More specifically, if a system comprises at least two water separation membrane units in use arranged parallel to the direction of flow of the fluid to be processed and is configured so that at least one spare water separation membrane unit can be installed parallel to the direction of flow of the fluid to be processed with respect to the at least two water separation membrane units, the system can be configured as the dehydrating system according to the present invention.

In the dehydrating system according to the present invention, a thermometer to monitor the temperature of the product fluid taken out of each of the water separation membrane units 1 to 5 can also be installed at the outlet and inlet (at least the outlet) of each of the water separation membrane units 1 to 5 as a monitoring device for the product fluid with a densitometer or instead of a densitometer.

If a silica membrane is used as the water separation membrane, the dissolution of silica degrades the performance of the water separation membrane. This allows ethanol and water to permeate together through the membrane, increases the latent heat of the fluid, and decreases the outlet temperature. For example, if usually the fluid flows into the unit at 90°C and out of the unit at 40°C, the outlet temperature may be further reduced. In this case, the decrease in temperature is considered to be due to degradation, and the flow rate is reduced and a spare water separation membrane unit is operated as needed.

In addition, the pores of a water separation membrane may be clogged with iron rust, adhesive material, or solid material. This increases the outlet temperature.

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If usually the fluid flows out of the unit at 40°C, the outlet temperature may not be reduced to the temperature. In this case, the increase in temperature is considered to be due to degradation, and the flow rate is reduced and a spare water separation membrane unit is operated as needed.

In the embodiment in FIG. 1, a fluid to be processed containing ethanol as the organic component is to be dehydrated. In the dehydrating system according to the present invention, however, the fluid to be processed is not limited to such a fluid if the fluid is an organic aqueous solution. More specifically, the organic component of the organic aqueous solution may be preferably one organic component selected from the group consisting of alcohols such as ethanol, propanol, isopropanol, and glycol, carboxylic acids such as acetic acid, ethers such as dimethyl ether and diethyl ether, aldehydes such as acetaldehyde, ketones such as acetone and methyl ethyl ketone, and esters such as ethyl acetate.

What is claimed is:

1. A dehydrating system that separates water from an organic aqueous solution to be processed, comprising:

at least two water separation membrane units in use to separate said solution from water arranged parallel to the direction of flow of the organic aqueous solution to be processed, each equipped with an inlet valve;

at least one spare water separation membrane unit which is equipped with an inlet valve and is installed parallel to the direction of flow of the organic aqueous solution to be processed with respect to the at least two water separation membrane units;

a monitoring device for monitoring one of a concentration and a temperature of a product fluid to be taken out; and

an inlet flowmeter and an outlet flowmeter for monitoring the flow rate into and out of said water separation membrane units;

wherein the dehydrating system maintains the properties of the product fluid by operating the spare water separation membrane units depending on the concentration or temperature of the product fluid monitored by the monitoring device, and on the flow rate monitored by said outlet flowmeter.

2. The dehydrating system according to claim 1, wherein each of said at least two water separation membrane units is equipped with an outlet valve.

3. The dehydrating system according to claim 1 or 2 further comprising a densitometer monitoring the concentration of the organic component of the product

fluid to be taken out of the entire dehydrating system as the monitoring device for the product fluid.

4. The dehydrating system according to claim 1 or 2 further comprising a densitometer monitoring the concentration of the organic component of the product fluid to be taken out of each of the water separation membrane units as the monitoring device for the product fluid, wherein the densitometer is installed at each of the water separation membrane units.

5. The dehydrating system according to any one of claims 1 to 4 further comprising a thermometer monitoring the temperature of the product fluid to be taken out of each of the water separation membrane units as the monitoring device for the product fluid.

6. The dehydrating system according to any one of claims 1 to 5 wherein the organic component of the organic aqueous solution is water-soluble.

7. The dehydrating system of claim 6 wherein the organic component is selected from the group consisting of alcohols, carboxylic acids, ethers, aldehydes, ketones and esters.

8. The dehydrating system of claim 7 wherein the alcohol is selected from the group consisting of ethanol, propanol, isopropanol, and glycol.

9. The dehydrating system of claim 7 wherein the carboxylic acid is acetic acid.

10. The dehydrating system of claim 7 wherein the ether is selected from the group consisting of dimethyl ether and diethyl ether.
11. The dehydrating system of claim 7 wherein the aldehyde is acetaldehyde.
12. The dehydrating system of claim 7 wherein is selected from the group consisting of acetone and methyl ethyl ketone.
13. The dehydrating system of claim 7 wherein the ester is selected from the group consisting of ethyl acetate.
14. A dehydrating system that separates water from a fluid to be processed, comprising:
 - at least two water separation membrane units in use arranged parallel to the direction of flow of the fluid to be processed;
 - at least one spare water separation membrane unit which is installed parallel to the direction of flow of the fluid to be processed with respect to the at least two water separation membrane units;
 - a monitoring device configured to monitor a concentration of an organic component of a product fluid and a temperature of the product fluid, the product fluid being taken out of each of the water separation membrane units; and
 - a control unit configured to control an operation of the at least one spare water separation membrane unit depending on the concentration of the organic component and the temperature of the product fluid monitored by the monitoring device to maintain properties of the product fluid.

15. The dehydrating system according to claim 14, wherein the fluid to be processed is an organic aqueous solution.
16. The dehydrating system according to claim 15 further comprising a densitometer monitoring the concentration of the organic component of the product fluid to be taken out of the entire dehydrating system as the monitoring device for the product fluid.
17. The dehydrating system according to claim 15 further comprising a densitometer monitoring the concentration of the organic component of the product fluid to be taken out of each of the water separation membrane units as the monitoring device for the product fluid, wherein the densitometer is installed at each of the water separation membrane units.
18. The dehydrating system according to claim 14, wherein the control unit is configured to maintain the concentration of an organic component of the product fluid by reducing a product flow rate of the water separation membrane unit whose characteristics have degraded and by operating the at least one spare water separation membrane unit to maintain the product flow rate of the product fluid if the product flow rate below a set point can be maintained after the product flow rate is reduced.
19. The dehydrating system according to any one of claims 15 to 18 wherein the organic component of the organic aqueous solution is water-soluble.

20. The dehydrating system of claim 19 wherein the organic component is selected from the group consisting of alcohols, carboxylic acids, ethers, aldehydes, ketones and esters.
21. The dehydrating system of claim 20 wherein the alcohol is selected from the group consisting of ethanol, propanol, isopropanol, and glycol.
22. The dehydrating system of claim 20 wherein the carboxylic acid is acetic acid.
23. The dehydrating system of claim 20 wherein the ether is selected from the group consisting of dimethyl ether and diethyl ether.
24. The dehydrating system of claim 20 wherein the aldehyde is acetaldehyde.
25. The dehydrating system of claim 20 wherein the ketone is selected from the group consisting of acetone and methyl ethyl ketone.
26. The dehydrating system of claim 20 wherein the ester is selected from the group consisting of ethyl acetate.
27. A dehydrating method comprising:
providing a plurality of water separation membrane units installed parallel to the direction of flow of a fluid to be processed, the plurality of water separation membrane units comprising at least two operative water separation membrane units and at least one spare water separation membrane unit;

separating water from the fluid through the at least two operative water separation membrane units;

monitoring one of a concentration of an organic component of a product fluid and a temperature of the product fluid to be taken out of each operative water separation unit; and

operating the at least one spare water separation membrane unit depending on the monitoring to maintain properties of the product fluid.

28. The method of claim 27 wherein the monitoring further comprises monitoring a concentration of the organic component of the product fluid to be taken out of an entire dehydrating system.

29. The method of claim 27 wherein the monitoring further comprises monitoring a flow rate of the product fluid from an entire dehydrating system.

30. The method of claim 27 wherein the monitoring further comprises monitoring a temperature of the product fluid from an entire dehydrating system.

31. The method of any one of claims 27 to 30 wherein the concentration of the organic component of the product fluid is maintained by reducing the product flow rate of the operative water separation membrane unit whose characteristics have been degraded and operating the at least one spare water separation membrane unit to maintain the product flow rate of the product fluid if the product flow rate can be maintained below a set point after the product flow rate is reduced.

32. The method of claim 31 comprising:
switching off the operative water separation membrane unit whose characteristics have been degraded for replacement, wherein after replacement the switched off water separation membrane unit becomes one of the at least one spare water separation membrane unit.
33. The method of claim 32 wherein the switching off comprises closing an inlet valve associated with the water separation membrane unit.
34. The method of claim 32 or 33 wherein the switching off comprises closing an outlet valve associated with the water separation membrane unit.
35. The method of claim 34 wherein the organic component is water-soluble.
36. The method of any one of claims 27 to 35 wherein the organic component is selected from the group consisting of alcohols, carboxylic acids, ethers, aldehydes, ketones and esters.
37. The method of claim 36 wherein the alcohol is selected from the group consisting of ethanol, propanol, isopropanol, and glycol.
38. The method of claim 36 wherein the carboxylic acid is acetic acid.
39. The method of claim 36 wherein the ether is selected from the group consisting of dimethyl ether and diethyl ether.

40. The method of claim 36 wherein the aldehyde is acetaldehyde.
41. The method of claim 36 wherein the ketone is selected from the group consisting of acetone and methyl ethyl ketone.
42. The method of claim 36 wherein the ester is selected from the group consisting of ethyl acetate.

