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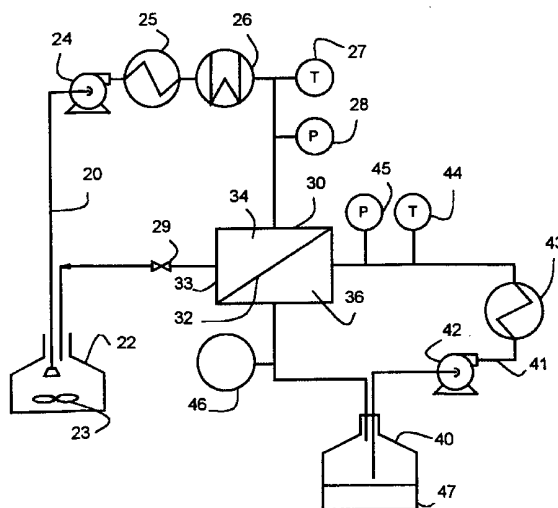
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- (71) Applicant: **COMPACT MEMBRANE SYSTEMS, INC.** [US/US]; 325 Water Street, Wilmington, DE 19804 (US).
- (72) Inventor: **BOWSER, John, J.**; 4 Meadow Wind Circle, Newark, DE 19711 (US).
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(54) Title: OSMOTIC DISTILLATION PROCESS



(57) Abstract: A method of raising the concentration of a liquid mixture utilizing osmotic distillation to transfer a volatile component from the mixture in contact with one side of a nonporous, preferably high free volume, gas permeable membrane (32) to a strip solution in contact with the other side of the membrane. Due to its nonporous nature the gas permeable membrane resists penetration and wetting by oily components that may be present in the feed mixture. Similarly, occlusion of the membrane by solids is resisted. Preferably, an amorphous copolymer of perfluoro-2,2-dimethyl-1,3-dioxole is useful for the gas permeable membrane. Osmotic distillation utilizing such high free volume, nonporous gas permeable membrane can concentrate difficult liquid mixtures such as pulpy fruit juices, and especially, limonene-containing juices, for example, orange juice. The process can be operated at high flux for long durations between membrane cleanings. Additionally, less contamination of the strip solution in a tank (22) into the feed mixture in the tank (40) occurs to provide a high quality concentrate.

OSMOTIC DISTILLATION PROCESS

FIELD OF THE INVENTION

This invention relates to an osmotic distillation process for concentrating a liquid. More specifically, it relates to an osmotic distillation process in which a nonporous
5 membrane of a high free volume polymer composition is utilized to transfer a volatile component from a liquid to be concentrated into a strip solution.

BACKGROUND AND SUMMARY OF THE INVENTION

Osmotic distillation is a type of membrane separation process in which a component of a liquid on one side of a porous or microporous membrane is transported through the
10 membrane to another liquid on the opposite side of the membrane. It differs from other more widely recognized types of membrane separation processes, such as reverse osmosis, ultrafiltration, and pervaporation in that the membrane is not wettable by either of the two liquids, and that the volatile component passes through the membrane in a vapor state. Accordingly, the driving force for transfer of the volatile component is the difference
15 between the vapor pressure of the volatile component over the "sending" liquid and the lower vapor pressure of the component over the "receiving" liquid.

A significant feature of osmotic distillation is that the transfer of the volatile component does not require a substantial system pressure or temperature gradient across the membrane. Therefore, this process advantageously can be carried out at ambient
20 temperatures and pressures. Such low temperature and low pressure process conditions render osmotic distillation ideal for increasing the concentration in an initially dilute liquid phase of a temperature and/or pressure sensitive component. These are materials which have limited stability to elevated temperatures and shear stresses. Such a component is one which would likely be adversely affected or destroyed if concentrated at elevated
25 temperatures or pressures required by other processes. As a result of this important characteristic, osmotic distillation recently has gained much favorable attention in particular for the potential to concentrate liquid foodstuffs, cosmetics (*e.g.*, fragrances), pharmaceutical products and thermally labile biological substances. An excellent survey of osmotic distillation technology is presented in Hogan, Paul A., A New Option: Osmotic

Distillation, *Chemical Engineering Progress*, July, 1998, pp. 49-61, which is incorporated herein by reference in its entirety.

The concentration of beverages such as fruit and juices and alcoholic beverages is a primary application for osmotic distillation. Perhaps the most notable reasons for concentrating beverages are that the concentrates do not contain large amounts of solvent and they are stable much longer than in the dilute state. The concentrates thus can be shipped less expensively for long distances and remain fresh far longer than if diluted.

Some fruit juices, especially those of citrus fruit have oils or other components that reduce the surface tension of the juice, *e.g.*, surfactants. These oils and other surface tension reducing components are collectively referred to herein as "oils" or "oily components". For example, orange juice contains a substantial amount of dissolved limonene oils. The presence of dissolved oils in a primarily aqueous juice solution can be problematic for osmotic distillation because the oily components tend to wet the membrane surface, fill the pores and reduce or altogether block desired transmission of the volatile component, thereby preventing further concentration of the starting material. Oils may also eventually penetrate the membrane and allow the fluids on either side of the membrane to mix, which is undesirable.

Fruit juices as well as other liquids can be pulpy. That is, they contain solids suspended in the liquid. As the juice concentrates, the solid concentration increases. Solids can also block substantial portions of the membrane surface so as to occlude the pores and hinder osmotic distillation to the extent that the rate of transmission of the volatile component is greatly reduced.

It would be desirable to have an osmotic distillation process for concentrating liquids that is resistant to wetting and blocking of the membrane by oily and or solid components in the process liquids. Accordingly, there is now provided according to this invention a process for concentrating a liquid feed mixture comprising the steps of

providing a feed mixture of components present in initial concentration, the mixture comprising a volatile component in which mixture said volatile component is soluble and over which mixture said volatile component has a first vapor pressure, and a strip solution over which the volatile component has a second vapor pressure different from the first vapor pressure;

providing a two sided membrane structure comprising a nonporous membrane on one side and coextensive with a microporous substrate on the second side, the nonporous membrane being of a composition which is permeable to the volatile component and not wettable by either the feed mixture or the strip solution;
5 contacting the feed mixture with the nonporous membrane while contacting the strip solution with the microporous substrate;
maintaining the second vapor pressure below the first vapor pressure, thereby causing the volatile component to permeate the membrane from the feed mixture to the strip solution and thus producing a concentrated liquid mixture comprising
10 components other than the volatile component present at concentration greater than the initial concentration; and
removing the concentrated liquid mixture.

There is also provided an osmotic distillation apparatus for concentrating a liquid feed mixture of components present in initial concentration, the mixture comprising a
15 volatile component which is soluble in the feed mixture and over which said volatile component has a first vapor pressure, the apparatus comprising,
a two sided membrane structure comprising a nonporous membrane of a composition permeable to the volatile component, and a microporous substrate adjacent and coextensive with the nonporous membrane,
20 means for contacting the nonporous membrane with the feed mixture,
means for contacting the microporous substrate with a strip solution comprising the volatile component which is present at a second vapor pressure different from the first vapor pressure; and
means for maintaining the second vapor pressure below the first vapor pressure,
25 thereby causing the volatile component to permeate the membrane from the feed mixture to the strip solution,
in which apparatus the composition of the nonporous membrane is not wettable by either the feed mixture or the strip solution.

BRIEF DESCRIPTION OF THE DRAWINGS

30 Fig. 1 is a plot of specific volume versus temperature of a polymer exhibiting excess free volume.

Fig. 2 is a schematic diagram of an apparatus utilized to practice osmotic distillation according to an embodiment of this invention.

Fig. 3 is a plot of conductivity in millisiemens vs. weight of feed tank contents in grams during osmotic distillations to concentrate limonene-containing sucrose solution.

5 Fig. 4 is a plot of transmembrane flux during osmotic distillations to concentrate limonene-containing sucrose solution.

Fig. 5 is a plot of transmembrane water vapor flux and conductivity of the feed stream during osmotic distillation of coffee according to an embodiment of this invention.

DETAILED DESCRIPTION

10 The novel osmotic distillation process basically calls for transferring a volatile component from a first liquid through a nonporous membrane to a second liquid, thereby concentrating the residual components which remain in the first liquid and diluting the second liquid by addition of the transferred volatile component. Often the principal product of this process is the residual-enriched first liquid rather than the diluted second
15 liquid.

The convention has been adopted herein to refer to the first liquid, which is the liquid from which the volatile component is removed, *i.e.*, the concentrating liquid, as the "feed" and further, to refer to the second, or liquid diluted by the volatile component, as the "strip solution". The latter term may be deemed to have been derived from its function of
20 stripping the volatile component from the feed.

The feed is a liquid state mixture comprising at least one volatile component and at least one other component which becomes concentrated by removing some of the volatile component. Solids can be present in the feed mixture, which thus will be a slurry or suspension. The proportion of solids to liquid is not critical provided that the feed mixture
25 remains a freely flowing fluid. When present, the solids are usually uniformly, or at least well dispersed in the feed mixture. Fruit juice with pulp, *i.e.*, pieces of fruit, is a typical example of a solids-containing feed.

The feed mixture can have one or more residual components which are concentrated by operation of the osmotic distillation process. Reference herein to the concentrating
30 component in singular is intended to encompass the plural unless stated otherwise. The concentrating component can be a liquid or a solid. Preferably, if liquid, the concentrating

component should be miscible with the volatile component. Furthermore, the vapor pressure of the concentrating component should be low compared to that of the volatile component to prevent substantial transfer of the former to the strip solution. If the concentrating component is a solid, it can be completely or partially soluble in the volatile component.

In osmotic distillation, the driving force for transfer of the volatile component through the membrane is the gradient of the volatile component vapor pressure between the feed mixture and the strip solution. Therefore the volatile component should provide a high vapor pressure over the concentrating solution so that a large vapor pressure gradient can be obtained. The novel osmotic distillation process is well suited to concentrating initially dilute solutions of low- or non-volatile solutes of moderate to high molecular weight, such as sugars, polysaccharides, carboxylic acid salts, proteins, and the like. The solvent in many industrially important cases is frequently water or an organic solvent, typically a polar organic solvent such as an alcohol, *e.g.*, ethyl alcohol. The actual solvent used will depend on the feed mixture to be treated. Preferably the feed mixture is selected from such compositions as liquid foodstuffs, including soups and fruit, alcoholic, or caffeinated beverages, cosmetics (*e.g.*, fragrances), pharmaceutical products, nutraceuticals, latices and thermally labile biological substances, such as animal body fluids including, blood, urine, cerebrospinal fluid, and the like.

When water is the solvent, the strip solution should be a solution of preferably a high osmotic activity, nonvolatile solute dissolved in the volatile component. That is, the nonvolatile solute should have a low equivalent weight and high solubility in the volatile component. The strip solution should be maintained at a relatively high concentration of the nonvolatile solute so as to depress the vapor pressure of the volatile component at the strip solution side of the membrane. This promotes the rapid transfer of the volatile component to the strip solution.

The vapor pressure of the volatile component in the strip solution will increase as transfer through the membrane progresses. In order to keep the transfer rate high, the volatile component concentration in the strip solution should be kept low. This can be accomplished by restocking the strip solution with virgin, low volatile component concentration strip solution. For economically attractive operation, the strip solution can be reconcentrated by removing excess volatile component and reused. Thus the

nonvolatile solute preferably should be stable at high temperatures which may be used to accelerate reconcentration. The strip solution can also be restocked from brine wells or bodies of water with high salt concentration. It is also desirable for the nonvolatile solvent of the strip solution to be nontoxic, noncorrosive and inexpensive. Preferably the

5 nonvolatile strip solution solute is an alkali hydroxide, a water soluble salt selected from the group consisting of alkali halide salt, and alkaline earth metal halide salt or mixtures thereof. Representative water soluble salts include sodium chloride, calcium chloride, magnesium chloride, monopotassium phosphate, dipotassium orthophosphate, magnesium sulfate, lithium chloride, lithium bromide, lithium iodide, potassium iodide, sodium iodide
10 and mixtures thereof.

In an important aspect, the osmotic distillation process according to this invention utilizes a membrane structure comprising a nonporous gas permeable membrane in contrast to a porous membrane that has heretofore been used in conventional osmotic distillation. This feature renders the novel process exceptionally useful to concentrate liquid mixtures
15 which have oily components and/or suspended solids. Membrane pores can be wetted by oils in the feed mixture, especially as the mixture concentrates. When a porous membrane becomes "wetted out", *i.e.*, saturated with the oily components, the oils can penetrate the membrane to occlude and/or coat the pores. Such occlusion diminishes transfer of the volatile component and such coating can also allow the strip solution and/or the feed
20 mixture to "breakthrough" the membrane and thus contaminate the other. Similarly, solids in the concentrating solution can occlude the pores. It has been discovered that a nonporous membrane can retard or prevent these adverse effects so that the nonporous membrane can be utilized for a much longer time at higher transmission rate between cleanings. Hence it is preferred that the nonporous membrane of the novel osmotic
25 distillation process be of a composition that is not wettable by either the feed or the strip solution. By "non-wettable" is meant that no breakthrough results when the nonporous membrane is subjected to a breakthrough procedure described in Examples 14-16 of U.S. Patent No. 5,876,604, the entire disclosure of which is incorporated herein by reference, using the feed or strip solution at a pressure and duration for which the osmotic distillation
30 process is to be performed. In a broad sense, the duration of the breakthrough test typically falls within the range of 1 day to 1 month and the pressure is usually in the range of about 1-5 pounds/sq. in., "psi", (7-35 KPa). Without undue experimentation, one of

ordinary skill in the art will be able to settle upon a test duration for a particular combination of liquid and membrane compositions.

Heretofore, nonporous membranes were not thought suitable for use in osmotic distillation. As mentioned, in osmotic distillation transfer of the volatile component
5 characteristically occurs by permeation of a gas through a membrane. Conventional materials for nonporous membranes generally do not have high gas permeabilities. Therefore, it has been traditionally observed in the art that transmission of a volatile component through a nonporous membrane would be too slow to make osmotic distillation practicable. It has now been found that certain materials can be formed into nonporous
10 membranes which provide acceptable transmission rates for osmotic distillation and thus permit the benefit of reduced wetting derived from utilizing nonporous membranes in osmotic distillation to be achieved.

In an important aspect of this invention, it has been found that high free volume gas permeable membranes can produce flux of a volatile component suitable for commercially
15 viable separation by osmotic distillation even though the membrane is nonporous. Hence, the use of a high free volume, nonporous gas permeable membrane permits a high flux, stable concentration process for concentrating liquid mixtures that had formerly been difficult to concentrate by osmotic distillation.

Free volume is a characteristic of a polymer which can be understood by inspection of a
20 plot of specific volume V versus temperature T as seen in the Fig 1. The term "free volume" refers to the volume of the polymer not actually occupied by the molecules. In Fig. 1, the volume of polymer occupied by the molecules is represented by region 8 below line 7 that defines the volume-temperature relationship of molecules which make up a polymeric article. Line 4 defines the volume-temperature relationship of the article formed
25 of the polymer. Therefore, the region between line 4 and line 7 represents the space between molecules within the physical dimensions of the polymeric article. Further, the region above line 4 represents the volume of space outside the bounds of the article. This uppermost region would include the volume of the pores throughout a porous article of polymer.

30 For many substances, the plot of V vs. T defines a linear relationship 4. However, for certain polymers, a discontinuity 1 in the V - T plot is seen at the glass transition temperature, T_g . That is, below the T_g , where the polymer is glassy, specific volume

increases linearly with increasing temperature along line 4. When the glass transition temperature is reached and exceeded, specific volume continues to increase linearly with temperature along line 2, however, the rate of increase is higher. That is, the slope of the specific volume vs. temperature line 2 above the T_g, is steeper than line 4 below the T_g.

5 At any temperature below the T_g, one can determine the difference between the actual specific volume and the expected specific volume obtained by extrapolating the specific volume vs. temperature line 6 from above the T_g to below the T_g. This difference, shown as region 5 is designated the "excess free volume". Thus glassy polymers at temperatures below the T_g can have a large excess free volume which provides an overall free volume
10 greater than the expected free volume between lines 6 and 7 that is especially high.

High free volume polymers are preferred for use as nonporous membranes for osmotic distillation. By the term "high free volume" is meant that the free volume of the polymer at the temperature of use is at least about 15% and preferably at least about 28%. The temperature of use will be the temperature at which osmotic distillation is performed. It is
15 desirable for the high free volume polymer to have a glass transition temperature above normal room temperature, preferably above about 30°C, and more preferably above about 115°C.

High free volume polymers which are particularly preferred for carrying out osmotic distillation are polytrimethylsilylpropyne, silicone rubber, and certain amorphous
20- copolymers of perfluoro-2,2-dimethyl-1,3-dioxole, the latter being especially favored.

The membrane can be formed from an amorphous copolymer of a certain perfluorinated dioxole monomer, namely perfluoro-2,2-dimethyl-1,3-dioxole ("PDD"). In some preferred embodiments, the copolymer is copolymerized PDD and at least one monomer selected from the group consisting of tetrafluoroethylene ("TFE"),
25 perfluoromethyl vinyl ether, vinylidene fluoride and chlorotrifluoroethylene. In other preferred embodiments, the copolymer is a dipolymer of PDD and a complementary amount of TFE, especially such a polymer containing 50-95 mole % of PDD. Examples of dipolymers are described in further detail in U.S. Patents Nos. 4,754,009 of E. N. Squire, which issued on June 28, 1988; and 4,530,569 of E. N. Squire, which issued on July 23,
30 1985. Perfluorinated dioxole monomers are disclosed in U.S. Patent No. 4,565,855 of B.C. Anderson, D.C. England and P.R. Resnick, which issued January 21, 1986. The disclosures of all of these U.S. patents are hereby incorporated herein by reference.

The amorphous copolymer can be characterized by its glass transition temperature which will depend on the composition of the specific copolymer of the membrane, especially the amount of TFE or other comonomer that may be present. Examples of Tg are shown in FIG. 1 of the aforementioned U.S. Patent No. 4,754,009 of E.N. Squire as ranging from about 260°C for dipolymers with 15% tetrafluoroethylene comonomer down to less than 100°C for the dipolymers containing at least 60 mole % tetrafluoroethylene. It can be readily appreciated that perfluoro-2,2-dimethyl- 1,3-dioxole copolymers according to this invention can be tailored to provide sufficiently high Tg that a membrane of such composition can withstand exposure to steam temperatures. Hence, membranes of this invention can be made steam sterilizable and thereby suitable for various uses requiring sterile materials, especially those involving biological materials.

To achieve optimum osmotic distillation performance, it is desirable to determine that the gas permeable membrane is nonporous. Absence of porosity can be measured by various methods known in the art, including for example, microscopic inspection of the membrane surface. PDD copolymers are particularly advantageous in this regard because they are intrinsically selectively gas permeable. Specifically, nonporous membranes of PDD copolymers exhibit an oxygen/nitrogen gas selectivity of greater than about 1.4. Hence it is possible to measure the difference in flux rates of two gases, for example oxygen and nitrogen, through a PDD copolymer membrane to verify that it is selectively gas permeable, and therefore, intact and nonporous over the membrane surface.

The nonporous membrane can be an unsupported monolithic gas permeable membrane structure. Preferably, a multilayer composite of a nonporous gas permeable layer supported on a porous or microporous substrate layer is utilized in which the nonporous membrane is adjacent and coextensive with the supporting porous substrate. The porous support provides structural integrity for the nonporous membrane. Any porous substrate material which is nonwetable by the strip solution and feed and that offers such support is suitable provided that it also is not degraded by the feed mixture, the volatile component or the strip solution and does not impede the transmission of the volatile component through the nonporous membrane. Additionally, materials that are by themselves wettable by the strip solution or feed can be treated to be made nonwetable. Examples of such materials and methods of rendering them nonwetable to liquids is found in U.S. Patents Nos. 5,116,650 and 5,156,780 the disclosures of which are hereby incorporated herein by

reference. Representative porous substrate materials include polyolefins, such as polyethylene and polypropylene, polytetrafluoroethylene, polysulfone, and polyvinylidene fluoride.

The shape of the membrane can be in a diverse variety of forms and typically can be in sheet form, such as a perforated sheet; porous woven or nonwoven fabric; microporous polymer film. The sheet can be deployed as a flat sheet, or the sheet can be pleated or rolled into a spiral to increase the surface to volume ratio of the separation unit. The membrane can also be in tube or tube ribbon form. Membrane tubes and tube ribbons are disclosed in U.S. Patent No. 5,565,166 which is incorporated herein by reference.

In a particularly preferred embodiment, the nonporous gas permeable membrane for use in osmotic distillation is applied as a thin layer on a support of a microporous hollow fiber. Such composite hollow fibers beneficially provide a very large surface area per unit of membrane structure volume and thus are able to produce extremely high gas flux in small occupied space. This surface to volume ratio benefit can be exploited further by assembling a plurality of composite hollow fibers in a so-called fiber module. Such module typically includes a bundle of many hollow fibers in substantially parallel alignment. The ends of the fibers are potted in a fixation medium, for example an epoxy resin. The bundle is then sliced through the potted ends and the bundles can be mounted within a casing to form a shell and tube modular unit. Although the nonporous membrane can be formed on the hollow fibers before bundling and assembling the module, it is preferred to form the membrane on the hollow fibers after installing them within a module. U.S. Patent 5,914,154 of Stuart M. Nemser, the disclosure of which is incorporated herein by reference in its entirety, discloses especially effective methods to produce such composite hollow fiber modules.

This invention is now illustrated by examples of certain representative embodiments thereof, wherein all parts, proportions and percentages are by weight unless otherwise indicated. All units of weight and measure not originally obtained in SI units have been converted to SI units.

EXAMPLES

Comparative Example 1 and Examples 1-3

An osmotic distillation apparatus was set up as shown in Fig 2. Calcium chloride strip solution in water was circulated in a brine loop **20** from brine feed tank **22** through a membrane module **30** via a Cole-Parmer Model 7144-05 variable speed, brine feed pump **24**. The brine feed tank was equipped with a magnetic stirrer **23** to maintain a homogeneous solution concentration in the tank. The brine was pumped through a heat exchanger in a VWR model 1140 constant temperature bath **25** maintained at 25°C and an Avecor Affinity™ blood oxygenator (Medtronic, Inc., Minneapolis, Minnesota) **26** to remove excess gases in the strip solution. The latter step was accomplished by passing the strip solution through the side of the oxygenator which normally receives blood while drawing about 25 inches Hg vacuum gauge on the side of the oxygenator which normally receives gas with a Welch Duo-Seal™ model 1400 vacuum pump. Temperature of the circulating strip solution was measured at thermocouple **27** prior to entry into membrane module **30**. Pressure of the circulating strip solution at pressure gauge **28** was controlled by manually throttling valve **29** at return of the solution to the feed tank.

The feed was circulated in a feed loop **41** from supply tank **40** through the membrane module **30** via another Cole-Parmer Model 7144-05 pump **42** and a second heat exchanger in the same VWR model 1140 constant temperature bath **43**. Temperature **44** and pressure **45** were monitored prior to entry into the module. In all examples, brine and feed temperatures entering the module were kept within a narrow range of each other that did not exceed about 2°C and was typically about 0.5°C. Conductance of the feed was continuously measured by a Yellow Springs Instrument Model 32 conductance meter **46**. Hence, a breakthrough of electrically conductive strip solution could be detected by an increase in conductivity of the feed. Mass of the concentrating solution in the supply tank was determine from mass balance calculations based on weight measurements taken using an Acculab® Model V-4800 electronic balance (0.1 g sensitivity) **47** placed under the supply tank. Flow of the feed stream entering the feed tank provided agitation.

The membrane module **30** also was a Avecor Affinity™ blood oxygenator. This unit contained within a cylindrical case **33** multiple, microporous, polypropylene hollow fibers with a total of about 25 square feet of membrane transfer area which are collectively represented by schematic element **32**. Pore size was believed to be about 0.04 µm and the

hollow fibers had a bore diameter of about 230 μm and an outer diameter of about 300 μm .

The apparatus was configured to direct the strip solution through the fiber bores and feed over the outer surface of the fibers to so as to pass these fluids through separate zones **34** and **36** on opposite sides of the membrane while in the module.

5 In operation, solid calcium chloride was added intermittently to the brine feed tank as needed to maintain solid salt present in the tank and thus to keep the concentration of strip solution at or near saturation. Pressure of the strip solution was controlled to at least 0.5 pounds/sq. in., "psi", (3.5 KPa) greater than the feed stream. This was done to assure that any breach of the membrane would cause bulk strip solution to contaminate the feed which
10 then could be detected by conductivity as mentioned earlier.

Osmotic distillation was conducted using four membranes alternately. The stock oxygenator module with uncoated microporous polypropylene hollow fibers was used in Comparative Example 1. In Examples 1-3, an identical type of oxygenator module was used in which the hollow fibers were overlaid with different thicknesses of a nonporous
15 layer of a perfluoro-2, 2-dimethyl-1, 3-dioxole ("PDD")/tetrafluoroethylene copolymer (Teflon® AF 2400, E. I. du Pont de Nemours & Co.) applied to the outside of the fibers according to the method disclosed in U.S. Patent No. 5,914,154, the disclosure of which is incorporated herein by reference. The effective membrane thicknesses on the fibers was 1.3 μm , 2.5 μm and 3.7 μm respectively for Exs. 1-3. Membrane thickness was calculated
20 from gas permeability measurements..

Rates of water vapor transmission from feed to strip solution obtained by osmotic distillation for each of two feeds, distilled water and 10 wt./wt. % sucrose in water are summarized in Table I. Circulation rates were 7.8 cm^3/s and 38 cm^3/s for strip solution and feed stream, respectively. During each procedure no change of feed stream conductivity
25 was detected indicating that bulk strip solution did not break through to contaminate the feed stream.

Table I

		Coating Thickness μm	Water vapor flux $\text{L}/(\text{m}^2 \cdot \text{h})$	Sucrose Sol'n. Water vapor flux $\text{L}/(\text{m}^2 \cdot \text{h})$
Comp.	Ex. 1	0	0.241	0.335
	Ex. 1	1.3	0.144	0.149
	Ex. 2	2.5	0.138	0.129
	Ex. 3	3.7	0.074	0.078

These examples show that osmotic distillation can be carried out according to the present invention with only slight reduction of water vapor flux compared to an uncoated, microporous membrane structure.

5 Example 4 and Comparative Example 2

The osmotic distillation procedure of Example 1 was repeated except that the feed stream consisted of 20 ml r-limonene added to 4 liters of 10 wt./wt.% sucrose solution in water (Ex. 4). For comparison, this procedure was also repeated using the membrane module of Comparative Example 1 (Comp. Ex. 2).

10 Fig. 3 shows a plot of conductivity, Q, in millisiemens vs. weight of feed tank contents, W, in grams for Ex. 4 (data "A") and Comp. Ex. 2 (data "B"). In the case of the nonporous membrane coated fibers, the figure reveals that conductivity increased only slightly then gradually declined as mass of feed in the feed tank declined due to water vapor transferred to the strip solution. This is behavior expected during normal concentration by
15 osmotic distillation of a slightly conductive solution such as sucrose. In contrast, data B in the figure shows conductivity rose rapidly which indicates contamination of the feed stream by the brine. Comp. Ex. 2 was terminated while a substantial amount of feed remained in the supply tank because of the significant amount of mixing of strip solution in the feed stream.

20 Data "C" (Ex. 4) and "D" (Comp. Ex. 2) of Fig 4 show the rate of flow, FX, in $\text{L}/(\text{m}^2 \cdot \text{h})$ across the membranes during osmotic distillation as calculated from weight loss of supply tank inventory. The nearly steady flux of Ex. 4 is probative of water vapor transmission occurring as a result of normal osmotic distillation. In contrast, the large and

erratic flux of Comp. Ex. 2 is indicative of liquid water transport through the membrane that is inconsistent with osmotic distillation.

The comparative example thus shows that the low initial concentration of r-limonene oil present in the feed adversely affected the hydrophobicity of the microporous hollow fiber allowing liquid water to transport through the membrane and cross contaminate the strip solution and feed. However, Example 4 demonstrates that the existence of a nonporous membrane on the microporous polypropylene fibers prevented the r-limonene oil from "wetting out" the membrane so that effective osmotic distillation could be carried out to concentrate the feed. Limonene is a naturally occurring oil in many fruit juices, particularly citrus juices. Hence, these examples indicate that coated membranes can be useful in osmotic distillation processes for concentrating fruit juices containing oily components that wet out porous membranes and render conventional osmotic distillation systems inoperable after a very short time.

Example 5

The apparatus and procedures of Example 2 were repeated with the following differences. Four thousand grams of freshly brewed coffee was circulated through the feed stream circulation loop and supply tank to fill the system. Initial inventory in the supply tank was 3586 grams, implying that the balance of 414 grams was resident in the circulation loop volume. Osmotic distillation was performed until the brewed coffee concentrated to a residue mass of 295 grams in the supply tank.

Fig. 5 is a plot of water vapor flux (data "E") through the membrane calculated from weight loss in the supply tank and conductivity (data "F") of the feed stream as a function of time during osmotic distillation. Water vapor flux rose rapidly to a steady state rate at about 90 minutes then decreased very gradually until about 10 hours of distillation when the transmission rate began to drop precipitously. At the end of the procedure, the level of inventory in the feed tank dropped very close to the feed loop intake. This caused air to be entrained into the feed and is believed to have caused the flux drop seen in the last two recorded points. Because coffee contains electrolytes, conductivity would be expected to rise as the feed became more concentrated. This is seen in Fig. 5 which confirms that osmotic distillation was effectively carried out with the nonporous membrane coated microporous hollow fiber substrate.

Although specific forms of the invention have been selected for illustration in the drawings and the preceding description is drawn in specific terms for the purpose of describing these forms of the invention fully and amply for one of average skill in the pertinent art, it should be understood that various substitutions and modifications which
5 bring about substantially equivalent or superior results and/or performance are deemed to be within the scope and spirit of the following claims.

What is claimed is

1. A process for concentrating a liquid feed mixture comprising the steps of
providing a feed mixture of components present in initial concentration, the mixture
comprising a volatile component in which mixture said volatile component is
soluble and over which mixture said volatile component has a first vapor pressure,
and a strip solution over which the volatile component has a second vapor
pressure different from the first vapor pressure;
providing a two sided membrane structure comprising a nonporous membrane on
one side and coextensive with a microporous substrate on the second side, the
nonporous membrane being of a composition which is permeable to the volatile
component and not wettable by either the feed mixture or the strip solution;
contacting the feed mixture with the nonporous membrane while contacting the strip
solution with the microporous substrate;
maintaining the second vapor pressure below the first vapor pressure, thereby
causing the volatile component to permeate the membrane from the feed mixture
to the strip solution and thus producing a concentrated liquid mixture comprising
components other than the volatile component present at concentration greater
than the initial concentration; and
removing the concentrated liquid mixture.
2. The process of claim 1 in which the nonporous membrane comprises a polymer
composition having a free volume of at least about 15%.
3. The process of claim 1 in which the nonporous membrane is in the form selected
from the group consisting of a flat sheet, a pleated sheet, a spiral rolled sheet, a tube, a tube
ribbon and a hollow fiber.
4. The process of claim 1 in which the microporous substrate is selected from the
group consisting of a perforated sheet; porous woven or nonwoven fabric; microporous
polymer film and microporous, hollow fiber.
5. The process of claim 4 in which the membrane unit is a hollow fiber.

6. The process of claim 2 in which the volatile component is water.
7. The process of claim 2 in which the volatile component is alcohol.
8. The process of claim 2 in which the feed mixture comprises a temperature sensitive substance selected from the group consisting of sugars, polysaccharides, carboxylic salts, proteins, fruit juice, vegetable juice, soup broth, coffee, tea, neutraceuticals, latices, biological substances and mixtures thereof.
9. The process of claim 8 in which the fruit juice is selected from the group consisting of orange juice, grape juice, pineapple juice, apple juice, pear juice, cranberry juice and mixtures thereof.
10. The process of claim 9 in which the food is orange juice.
11. The process of claim 8 in which the food is coffee.
12. The process of claim 8 in which the biological substance is selected from the group consisting of vaccine, peptide hormone, recombinant protein, enzyme, nucleic acid, fermentation product selected from the group consisting of antibiotic, fungicide and oligopeptide, animal body fluid, and mixtures thereof.
13. The process of claim 1 in which the strip solution comprises a component selected from the group consisting of alkali halide salt, alkaline earth metal halide salt, alkali hydroxide, and mixtures thereof.
14. The process of claim 13 in which the water soluble salt is selected from the group consisting of sodium chloride, calcium chloride, magnesium chloride, monopotassium phosphate, dipotassium orthophosphate, magnesium sulfate, lithium chloride, lithium bromide, lithium iodide, potassium iodide, sodium iodide and mixtures thereof.

15. The process of claim 2 in which the polymer composition comprises a high free volume polymer selected from the group consisting of polytrimethylsilylpropyne and an amorphous copolymer of perfluoro-2,2- dimethyl-1,3-dioxole.
16. The process of claim 15 in which the high free volume polymer is an amorphous
5 copolymer of perfluoro-2,2- dimethyl-1,3-dioxole.
17. The process of claim 15 in which the amorphous copolymer is a copolymer of perfluoro-2,2-dimethyl-1,3-dioxole and a complementary amount of at least one monomer selected from the group consisting of tetrafluoroethylene, perfluoromethyl vinyl ether, vinylidene fluoride, hexafluoropropylene and chlorotrifluoroethylene.
- 10 18. The process of claim 17 in which the amorphous copolymer is a dipolymer of perfluoro-2,2-dimethyl-1,3-dioxole and tetrafluoroethylene.
19. The process of claim 18 in which the dipolymer comprises 50-95 mole % polymerized perfluoro-2,2-dimethyl-1,3-dioxole.
20. The process of claim 16 in which the membrane has an oxygen/nitrogen
15 selectivity of at least about 1.5.
21. The process of claim 15 in which the polymer composition comprises polytrimethylsilylpropyne.
22. An osmotic distillation apparatus for concentrating a liquid feed mixture of components present in initial concentration, the mixture comprising a volatile component
20 which is soluble in the feed mixture and over which said volatile component has a first vapor pressure, the apparatus comprising,
a two sided membrane structure comprising a nonporous membrane of a composition permeable to the volatile component, and a microporous substrate adjacent and coextensive with the nonporous membrane,

- means for contacting the nonporous membrane with the feed mixture,
means for contacting the microporous substrate with a strip solution comprising the
volatile component which is present at a second vapor pressure different from the
first vapor pressure; and
- 5 means for maintaining the second vapor pressure below the first vapor pressure,
thereby causing the volatile component to permeate the membrane from the feed
mixture to the strip solution,
- in which apparatus the composition of the nonporous membrane is not wettable by either
the feed mixture or the strip solution.
- 10 23. The osmotic distillation apparatus of claim 22 in which the nonporous
membrane comprises a polymer having a free volume of at least 15%.

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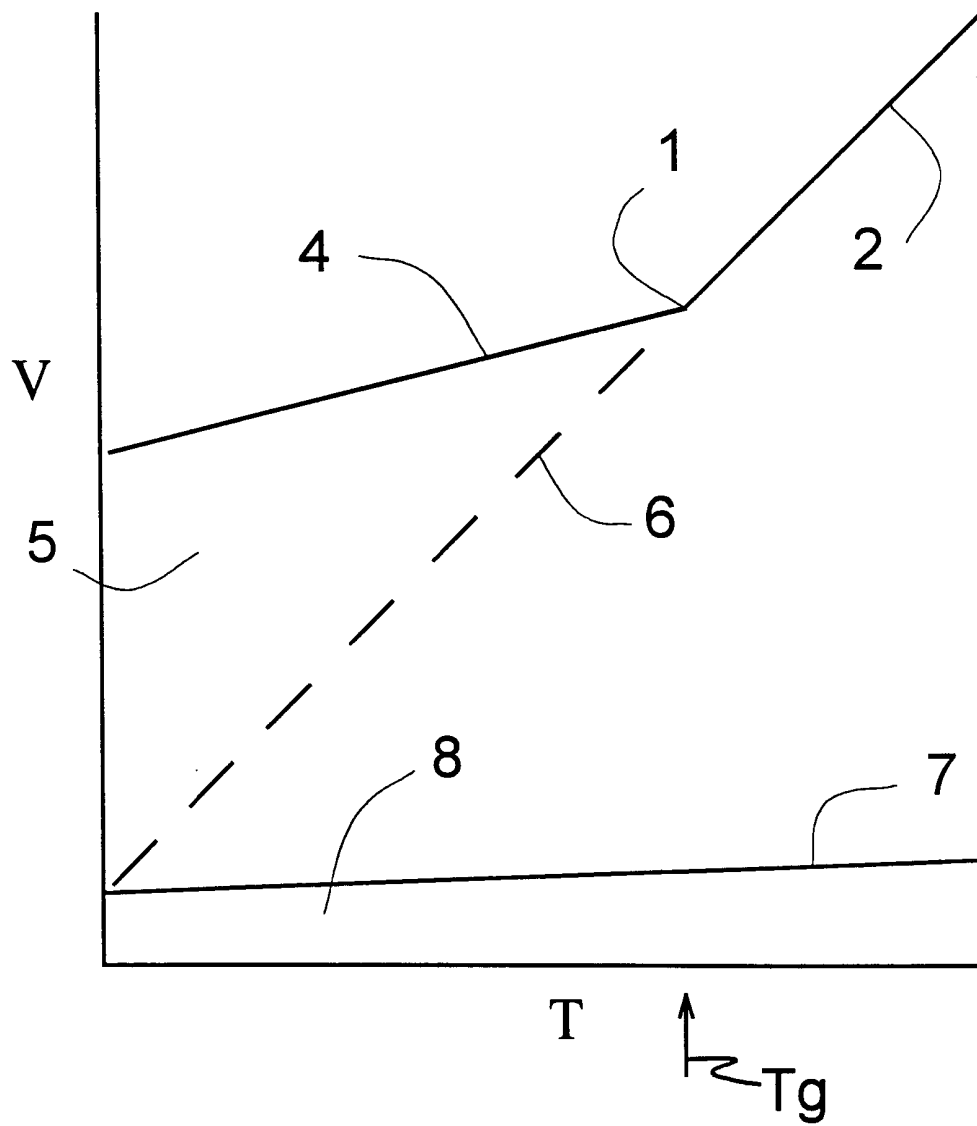


FIG. 1

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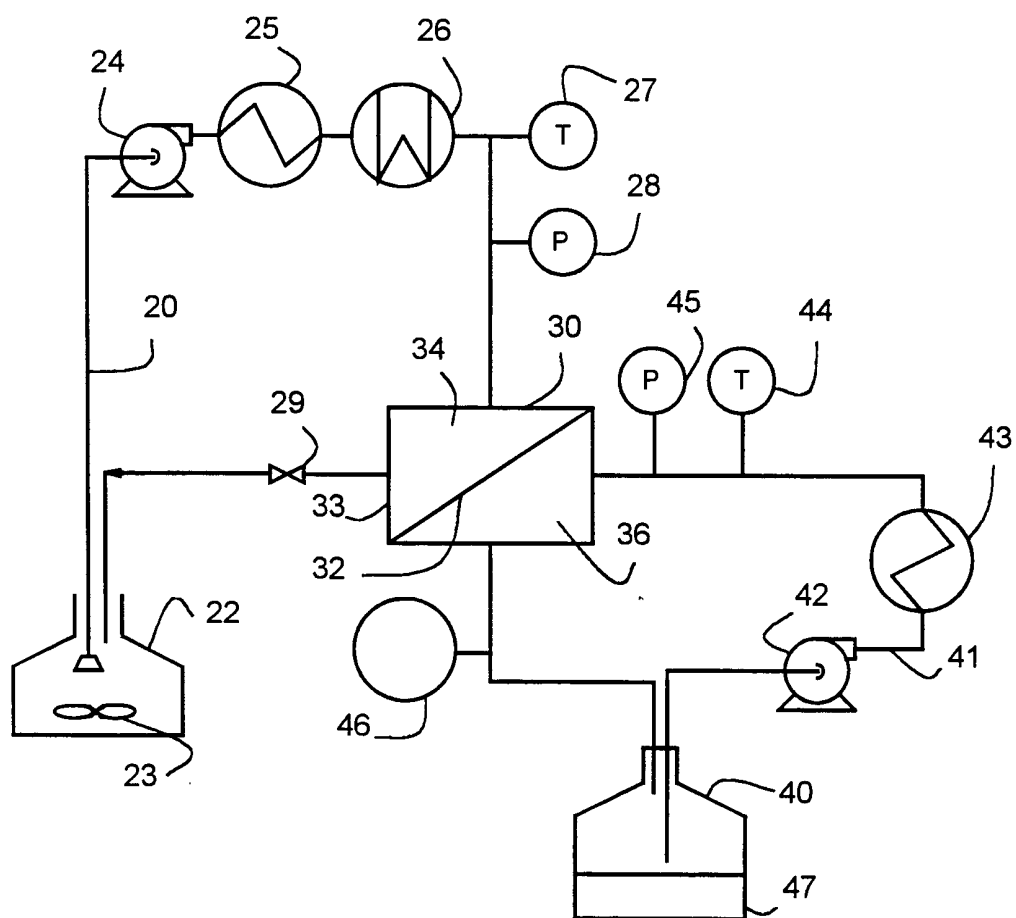
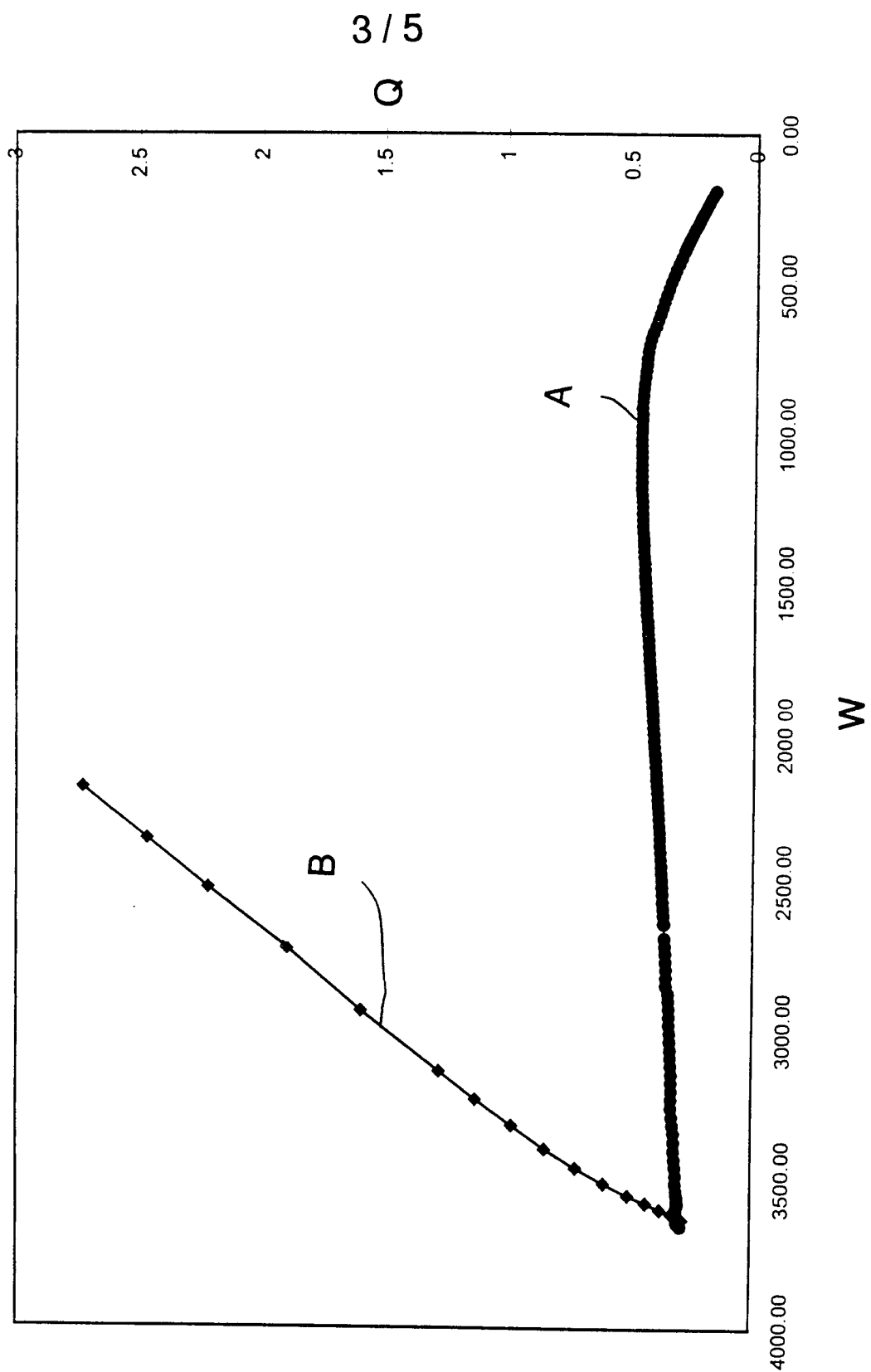


Fig. 2

FIG. 3



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FIG.4

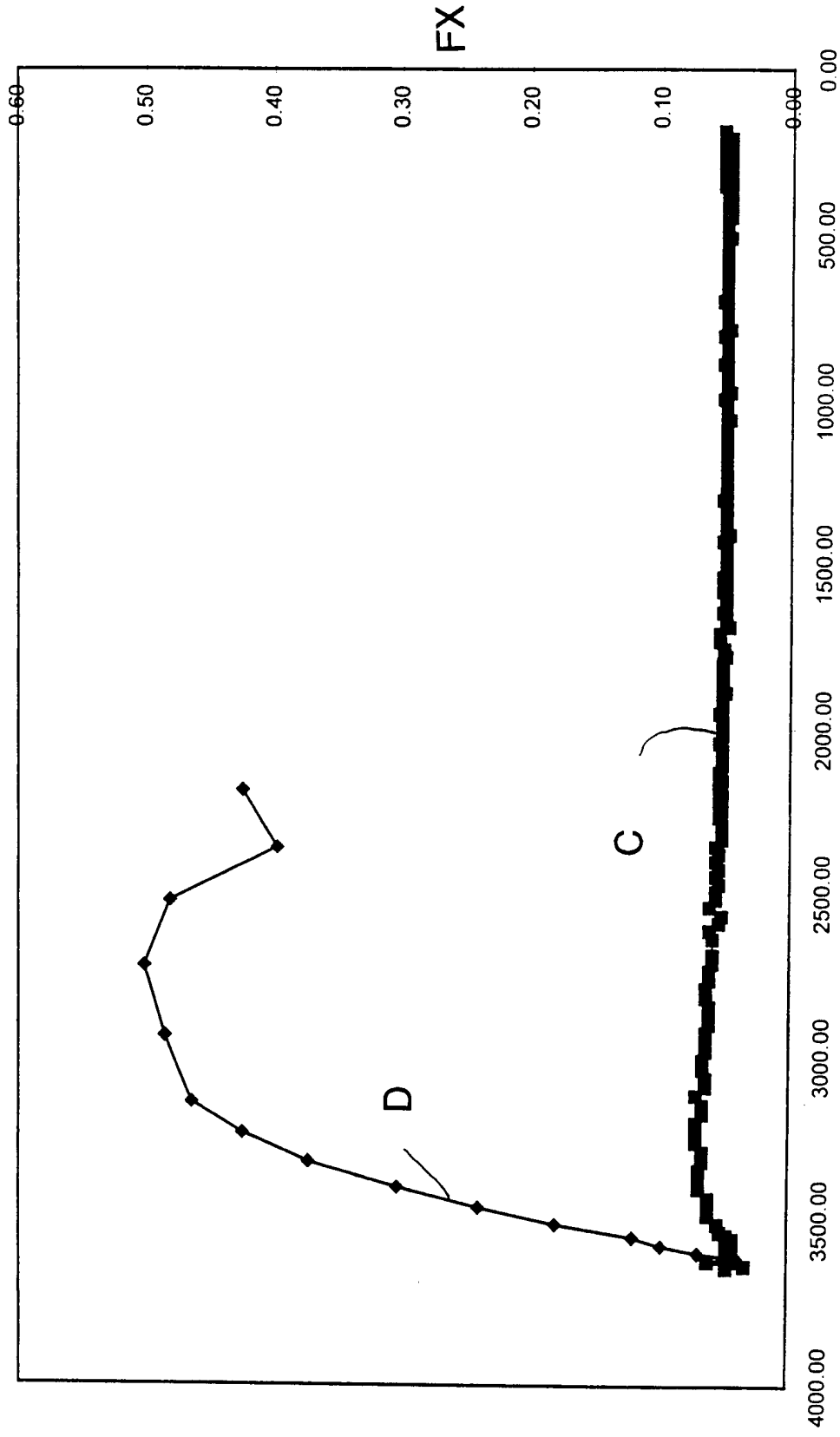
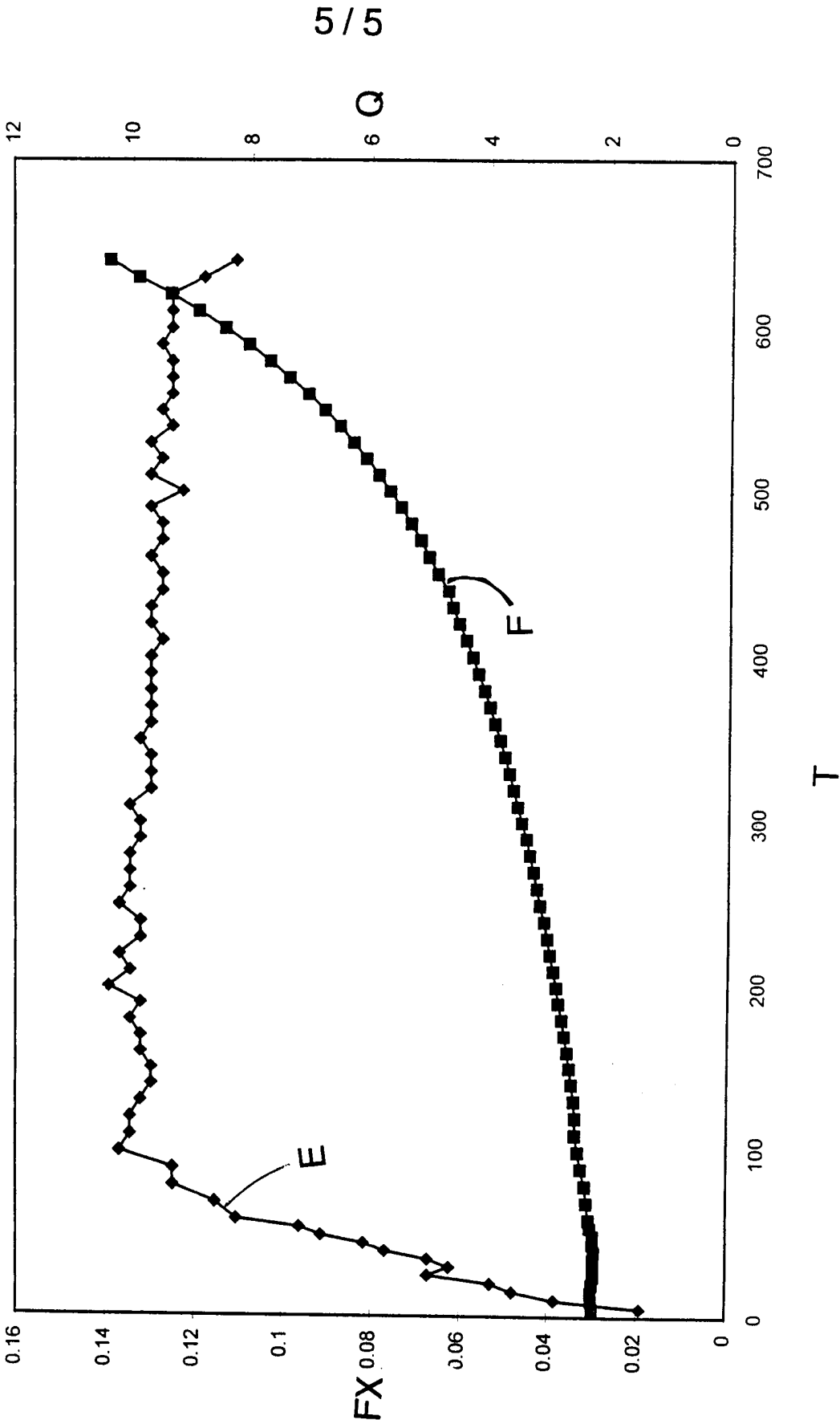


FIG.5



INTERNATIONAL SEARCH REPORT

International application No.
PCT/US00/40493

A. CLASSIFICATION OF SUBJECT MATTER

IPC(7) :B01D 61/36

US CL :210/640, 493.1; 95/45, 50

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 210/640, 493.1; 95/45, 50

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5,876,604 A (Nemser et al.) 02 March 1999, See entire document	1-23



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
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Date of the actual completion of the international search

05 NOVEMBER 2000

Date of mailing of the international search report

12 DEC 2000

Name and mailing address of the ISA/US
Commissioner of Patents and Trademarks
Box PCT
Washington, D.C. 20231

Facsimile No. (703) 305-3230

Authorized officer

ANA FORTUNA

Telephone No. (703) 308-3857