

**(12) STANDARD PATENT
(19) AUSTRALIAN PATENT OFFICE**

(11) Application No. AU 2005339365 B2

(54) Title
Process and related plant for producing steel strips with solution of continuity

(51) International Patent Classification(s)
B21B 1/46 (2006.01)

(21) Application No: **2005339365** (22) Date of Filing: **2005.12.22**

(87) WIPO No: **WO07/072515**

(43) Publication Date: **2007.06.28**
(44) Accepted Journal Date: **2011.12.01**

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(56) Related Art
WO 2004/026497
US 6092586

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
28 June 2007 (28.06.2007)

PCT

(10) International Publication Number
WO 2007/072515 A1

(51) International Patent Classification:
B21B 1/46 (2006.01)

CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KN, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, LY, MA, MD, MG, MK, MN, MW, MX, MZ, NA, NG, NI, NO, NZ, OM, PG, PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SM, SY, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM, ZW.

(21) International Application Number:
PCT/IT2005/000754

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HU, IE, IS, IT, LT, LU, LV, MC, NL, PL, PT, RO, SE, SI, SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

(22) International Filing Date:
22 December 2005 (22.12.2005)

Published:

- with international search report
- with amended claims and statement

(25) Filing Language:
English

(26) Publication Language:
English

(71) Applicant and

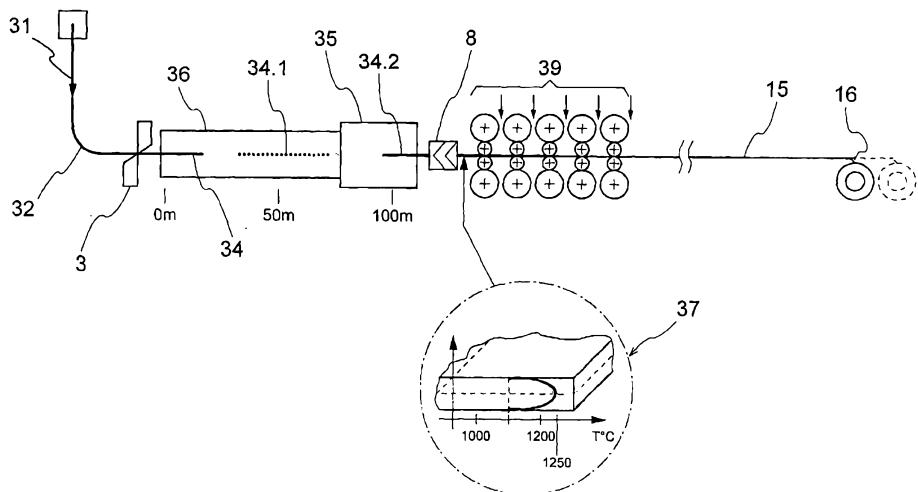
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For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

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(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN,

(54) Title: PROCESS AND RELATED PLANT FOR PRODUCING STEEL STRIPS WITH SOLUTION OF CONTINUITY



(57) **Abstract:** A process for the manufacturing of steel strips with solution of continuity is described, comprising a continuous casting step for thin slabs with a high "mass flow", a shearing step and subsequent heating in furnace, followed by a multiple stand rolling step, wherein the average temperature of the product at the inlet of the rolling is higher than the surface temperature, which is equal to at least 1100°C, lower than that measured in the inner central area by about 100°C. A plant is also described for the accomplishment of such process, wherein at the inlet of a furnace (25; 35), possibly of the induction type, combined with a temperature maintaining tunnel (36) a shear (3) is provided for, cutting into pieces (24; 34) a slab (22; 32) coming from continuous casting (21; 31), wherein the distance between the outlet of said continuous casting and the inlet into the finishing rolling mill (29; 39) is not greater than 100 m.

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"PROCESS AND RELATED PLANT FOR PRODUCING STEEL STRIPS WITH
SOLUTION OF CONTINUITY"

The present invention relates to a process and related plant for the manufacturing of steel strips.

5 In the steel industry it is known the need, being however present in every industrial field, for using manufacturing methods involving lower investment and production costs. It is known as well that in the last years manufacturing methods based on the so-called "thin slab" technologies have had a remarkable development and success in this direction of cost reduction, above all under the energetic aspect. A "thin slab" is commonly known 10 in the field of steel manufacturing as a slab having a thickness of between 45 mm and 110 mm.

Three fundamental types of manufacturing processes and related plants, accomplishing such a technology, can be distinguished, namely a first type which does not provide for solution of continuity between the continuous casting step and the rolling one, 15 a second type wherein said two steps are separated, thereby with a solution of continuity providing for the use of a Steckel rolling mill, and finally a third type, again with solution of continuity, as shown in Fig. 1, as is accomplished, for example, in the so-called CSP plant of the American Company Nucor Steel in Crawfordsville, Indiana (US).

With reference to said Figure 1, wherein the continuous casting machine is 20 schematically represented as 1, a thin slab 2 is produced at the outlet thereof having thickness from 45 to 80 mm and a typical speed of 5m/min. The slab is cut by means of a shear 3 at a typical length of 40 m, anyway depending on its thickness, on its width and on the weight of the desired final strip coil. The thin slab, so cut down into pieces 4, enters a tunnel furnace 5, whose purpose is to homogenize the temperature especially throughout 25 the transverse cross-section, from the external surface to the core, then passes through a descaler 8 before entering the finishing rolling mill 9 comprising, in the example shown, six stands 9.1 – 9.6. After the rolling, from which it comes out on a cooling roller table 15, it goes to the final coiling by means of one or two reels 16 in order to form the desired coil.

It should be noted that the tunnel furnace 5 is characterized, as it is known, by a 30 length of about 200 m and by a typical residence time of the slab inside thereof

comprised between 20 and 40 min at a speed as indicated above. Of course, a continuous casting speed higher than 5 m/min requires a tunnel furnace length even greater than 200 m in order to heat the slab and make its temperature uniform. For example, with a speed of 7 m/min at the outlet of the continuous casting, the tunnel 5 furnace should have a length of about 300 m if maintaining a residence time of the slab in the furnace greater than 40 min is not desired. By further increasing the casting speed, still for the same residence duration in the furnace, this should have an even greater length, hardly feasible both from a technical and an economical point of view.

Still with reference to Figure 1, it shows three slabs 4, 4.1 and 4.2 inside the 10 furnace 5, among which the first one is still connected to the continuous casting before being cut by the shear 3, the second one is free inside the furnace, ready to be rolled and the third one is already drawn by the finishing rolling mill 9 through the descaler 8. The virtual profiles of two additional slabs 4.3 and 4.4 are further represented by a dotted line, which might find a place inside the furnace 5 without having to stop the continuous 15 casting in case of jammings in the rolling mill or of replacement operations of the rolls, if these problems can be solved in a time lower than 20 min.

The transverse temperature profile of the slab, immediately upstream of the first rolling stand, has been represented by the detail marked by reference number 7. The diagram of Fig. 1a further shows that a slab with a average temperature of 1000°C at the 20 inlet of the finishing rolling mill requires a pressure or "flow stress" Kf on the material equal to 100 N/mm², whereas a temperature of 800°C, in the case of low carbon steel, involves a pressure Kf of about 150 N/mm². As it can be noted in detail 7, the temperature profile of the slab at the inlet of the finishing rolling mill is substantially homogeneous, as shown by the slightly convex curve representing it from a minimum of 25 about 990°C at the ends, corresponding to the surface temperature, to a maximum of 1010°C at the center zone, corresponding to the core of the slab, from which comes the previously indicated value of about 1000°C for the average temperature.

In fact, according to the related prior art of this type of technology, it has been so far believed that the product at the outlet of the continuous casting 2, having a 30 temperature profile as shown in the diagram of detail 6, relative to a slab cross-section at the inlet of the furnace 5, i. e. with a surface temperature of about 1100°C and of

about 1250°C at the core (i. e. the apex of the diagram), should undergo a process of complete temperature homogenization. The trend has always been to homogenize such temperature as much as possible, especially throughout the cross-section of the slab, before entering the finishing rolling mill. In fact, it has been always thought that by 5 making the temperature uniform between surface and core of the product, the advantage of a homogeneous fiber elongation could be obtained, in order to show the same strain resistance by substantially having the same temperature. On the basis of such a constant technical prejudice, it has been always tried to have a temperature difference being lower than 20°C between surface and core of the product, as above indicated with 10 reference to detail 7, in order to have a homogeneous fiber elongation, until now considered necessary for the achievement of a good quality of the final product.

On the other hand, as seen above, the temperature uniformity characteristic of the slabs does not allow building plants with the high casting speeds, which would be theoretically possible to achieve (up to values of 12 m/min due to the present 15 technology development), and thereby with very high productivities, due to the inadmissible length the furnace should have.

On the other hand it would be desirable to have furnaces of reduced length between continuous casting and rolling mill in order to obtain space saving and reduction of investments, resulting in a higher average temperature of the product, 20 involving a lower total power of the stands for the same strip thickness, as highlighted in the diagram of Figure 1a already mentioned.

In fact, thus overcoming a widespread prejudice of the prior art, it has been found that with a temperature in the middle of the cross-section of the slab being higher than 100 – 200°C with respect to the surface temperature, maintained at about 1100°C, a 25 lower rolling pressure K_f is required in order to obtain the same final thickness of the strip, because the average rolling temperature is increased, without otherwise worsening the product quality.

It has been also found that such temperature conditions are not prejudicial for the final rolling product quality, when the following conditions are met: the cast product shows a sufficiently high “mass flow” value (i. e. the amount of steel flowing in the 30 time unit at the outlet of the continuous casting), with an outlet speed > 5 m/min after

having undergone a process of liquid core reduction or "soft reduction", in particular according to the teachings of EP 0603330 in the name of the same applicant, in order to guarantee the so-called "central sanity" characteristic of the cast slab and to have a higher temperature at the core, and thereby also a higher average temperature in the rolling step.

5 It is therefore desirable to provide a process for the manufacturing of steel strips with solution of continuity allowing the maximum possible reduction with the minimum separating strength and therefore requiring a reduced total power of the rolling stands with a consequent energy saving for a given strip thickness at the outlet of the rolling mill.

10 It is also desirable to provide a process of the above-mentioned type being able to achieve, with a limited furnace length, very high productivities as a consequence of a high casting speed.

According to a first aspect of the present invention, there is provided a process for the manufacturing of steel strips comprising:

15 continuously casting thin slabs having high "mass flow", which is defined as an amount of steel passing in a time unit at an outlet of the continuous casting, wherein liquid core reduction is performed during continuous casting of the slabs; shearing the slabs directly following the continuous casting where the liquid core reduction has been performed; heating the slabs; rolling the slabs through a finishing rolling mill, which has multiple stands for rolling; wherein said heating is obtained, at least partially, by induction

20 heating with a working frequency sufficiently low to bring the heating to a core of the slab and to substantially maintain a same temperature difference between an inside and an outside of the slab up to entry of the slabs into the finishing rolling mill, whereby the average temperature in any transverse cross-section of the slabs is higher than a surface temperature of the slabs the temperature being equal to or higher than about 1100°C, and at

25 the core of the slabs the temperature is at least 100°C higher than the surface temperature.

According to a second aspect of the present invention, there is provided a plant for the production of steel strips from thin slabs coming from continuous casting, comprising at least one heating furnace upstream of a multiple stand finishing rolling mill, and a shear for shearing the slab directly following the continuous casting where liquid core reduction

30 has been performed, wherein one of said at least one furnace is an induction furnace the working frequency of which is chosen sufficiently low in order to bring the heating to a core of the slab and to substantially maintain a same temperature difference between an

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inside and an outside of the slabs up to arrival of the slabs at the inlet of the first rolling stand of said finishing rolling mill, whereby the slab average temperature is higher than a surface temperature of the slabs and at the core of the slabs the temperature is at least 100°C higher than said surface temperature, said surface temperature being equal to or 5 higher than 1100°C.

Figure 1 schematically shows a plant for the manufacturing of steel strips from continuous casting, with solution of continuity, according to the prior art, as already described above;

10 Figure 1a is a diagram showing the trend of the rolling pressure required as a function of the average temperature of the material to be rolled;

Figure 2 shows a schematic view of a plant according to a preferred embodiment of the present invention, similar to that of Fig. 1; and

Figure 3 shows a schematical view of a variant of plant according to a preferred embodiment of the present invention, comprising an induction furnace.

15 With reference to Figure 2, an example of plant carrying out the process according to a preferred embodiment of the present invention is schematically shown starting from a thin slab 22 at the outlet of a continuous casting zone schematically represented in its whole as 21 and comprising, as it is known, a mould, as well as possible suitable means to accomplish a

liquid core reduction or “soft reduction”. The thin slab 22 comes out from the continuous casting 21 with the same thickness and speed values already indicated for the slab 2 of the plant of Fig. 1 relating to the prior art, i. e. with a thickness between 45 and 80 mm, e. g. 60 mm, a speed equal to 5 m/min and a width equal to 1600 mm, that 5 is to say with a high “mass flow” as defined above. The temperature profile in the zone upstream of the furnace 25 (here not shown) is still the one shown in detail 6 of Fig. 1, with a surface temperature of about 1100°C and of about 1250°C at the core (diagram apex).

The slab is still cut down in pieces, typically having a length of 40 m, by means of 10 the shear 3, according to the weight of the final coil desired, and enters a traditional tunnel furnace 25 (gas heated), but being of a limited length, having the purpose of maintaining the thin slab 24 in temperature by heating the same. Therefrom it passes, through the descaler 8, into a finishing rolling mill 29 from which comes out, upon its rolling, on a roller table 15 in order to be coiled by means of one or two reels 16, as 15 already seen according to Fig. 1.

Differing from the plant of Fig. 1, the tunnel furnace 25 here shows a length that must be as reduced as possible and anyway not greater than 100 m, so that the residence time of the thin slab inside thereof be as short as possible. This is for the purpose of maintaining a profile with a “triangular” trend at the outlet thereof, as indicated in detail 20 27, being characterized by a surface temperature of about 1100°C, a temperature at the slab core of about 1200°C and a average temperature of about 1150°C. The resulting trend is thereby substantially less homogeneous than the profile shown in detail 7 of Fig. 1, for the same feeding speed.

Inside furnace 25 two slabs 24 and 24.2 are represented of which the first one is 25 still connected to the continuous casting before being cut by shear 3 and the second one is already drawn by the finishing rolling mill 29 through the descaler 8, and thereby is already in the rolling step. The dotted line 24.1, intermediate between the two slabs, instead represents the space available for a further slab, serving as a “lung” in case of jamming of the rolling mill, if the slab thickness at the outlet and the weight of the coil 30 desired allow to have slabs of length < 30 m, given the above-mentioned limits of overall furnace length. Each slab, after the shear 3 cut, is accelerated and transferred to

the central part of the furnace until it reaches the entering speed of the finishing rolling mill, equal to about 15 – 20 m/min, in order to reduce the residence time in the furnace itself as much as possible, which will be able to be even lower than 10 minutes instead of the 20 – 40 min foreseen for a plant according to the prior art shown in Fig. 1.

5 As previously stated, it should be noted that anyway the distance between the outlet from the continuous casting 21 and the finishing rolling mill 29 will not be greater than about 100 m, with the further consequent advantage of having a more compact plant requiring a reduced space also with high speeds at the outlet of the continuous casting. In such a way the average temperature of the product will be higher
10 than the surface temperature, being higher of at least 100°C at the core with respect to the external surface. From the diagram of Fig. 1a it is clear that a Kf value of about 70 N/mm² corresponds to a average temperature of 1150°C, instead of 100 N/mm² as it happens with the average temperature of 1000°C resulting from the plant of Fig. 1.

15 It should be noted that, by using the above-mentioned higher temperature of the “mass flow”, greater reductions can be achieved, in particular in the first rolling stands, allowing to obtain thinner thicknesses with the same or a lower number of stands with respect to the prior art. In Fig. 2, for example, the rolling mill stands 29 have been represented in a number of five against the six ones of the rolling mill 9 of Fig. 1.

Fig. 3 shows another embodiment of the present invention, wherein the tunnel
20 furnace 25, typically gas heated, is substantially replaced by an induction furnace 35. In the prior art (see for example EP 0415987 in the name of the same applicant) induction furnaces have been used in order to heat a thin slab, previously rolled to a thickness of about 15 mm in a roughing rolling mill, and make it suitable for the subsequent finishing rolling step. As the slab core was anyway hotter than the surface, the working
25 frequency of the furnace was generally chosen sufficiently high so that the depth of penetration of thermal energy, inversely proportional to frequency, were such to mainly heat the surface layer characterized by a lower temperature.

On the contrary, in the preferred embodiment of the present invention shown in Figure 3, the induction furnace 35 is used with a sufficiently low working frequency so that
30 the heating action, being performed in a nearly homogeneous way throughout the whole transverse cross-section of the slab to the core, substantially maintains the same trend as at the inlet thereof until

the end, such trend being shown by the diagram of detail 6 in Fig. 1. Thus, if at the inlet of furnace 35 the slab 34, to be cut by means of shear 3 from slab 32 coming out from the continuous casting 31, has a surface temperature of 1100°C and of 1250°C at the core, at the outlet of said furnace it will be able to have also a surface temperature of 5 1150°C or higher and of about 1250°C at the core, not only maintaining a sensible temperature difference inside-outside, but also increasing the average temperature of the slab under rolling, with all the advantages previously shown with reference to Fig. 1a.

Before entering the induction furnace 35, the thin slab 32 coming from the continuous casting 31 passes anyway, after the shear 3, into a temperature maintaining 10 and possible heating tunnel 36, which has the purpose of limiting the thermal losses.

It should be noted that the induction furnace 35, differently from what is shown in Fig. 3, could also be placed before said tunnel 36, in such a way to increase the slab ... temperature while this is still connected to the continuous casting, for the purpose of limiting its power dimensioning. After the cut by shear 3, the slab cut down piece 34 is 15 accelerated, as already said for slab 24 with reference to Fig. 2, in order to reach the entering speed of the rolling mill 39, equal to about 15 – 20 m/min. The tunnel 36 comprising the roller tables between continuous casting and rolling mill, upstream and/or downstream of the furnace 35, is formed of insulating panels, which might be provided with gas burners and/or resistors in order to further reduce the heat losses. To 20 sum up, given the lower length of an induction furnace with respect to a traditional one, it can be said that also in this case, taken into account tunnel 36, being of a reduced length with respect to furnace 25 of Fig. 2, the total distance between the outlet of the continuous casting and the rolling mill inlet is again not greater than 100 m.

Cooling systems or possibly intermediate heating systems, not shown in the 25 drawing, can be provided for among the stands of the finishing rolling mill 29 or 39, being inserted between one stand and an other according to the rolling speed and to the steel type to be rolled.

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Finally, preferred embodiments of the present invention can also be used in order to carry out processes and related plants with two casting lines supplying the same rolling mill 29 or 39.

The foregoing describes only one embodiment of the invention and modifications 5 can be made without departing from the scope of the invention.

The reference in this specification to any prior publication (or information derived from it), or to any matter which is known, is not, and should not be taken as an acknowledgment or admission or any form of suggestion that that prior publication (or information derived from it) or known matter forms part of the common general 10 knowledge in the field of endeavour to which this specification relates.

Throughout this specification and the claims which follow, unless the context requires otherwise, the word "comprise", and variations such as "comprises" and "comprising", will be understood to imply the inclusion of a stated integer or step or group of integers or steps but not the exclusion of any other integer or step or group of integers or 15 steps.

The reference numerals in the following claims do not in any way limit the scope of the respective claims.

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

1. A process for the manufacturing of steel strips comprising:
continuously casting thin slabs having high "mass flow", which is defined as an
5 amount of steel passing in a time unit at an outlet of the continuous casting, wherein liquid
core reduction is performed during continuous casting of the slabs; shearing the slabs
directly following the continuous casting where the liquid core reduction has been
performed; heating the slabs; rolling the slabs through a finishing rolling mill, which has
multiple stands for rolling; wherein said heating is obtained, at least partially, by induction
10 heating with a working frequency sufficiently low to bring the heating to a core of the slab
and to substantially maintain a same temperature difference between an inside and an
outside of the slab up to entry of the slabs into the finishing rolling mill, whereby the
average temperature in any transverse cross-section of the slabs is higher than a surface
temperature of the slabs the temperature being equal to or higher than about 1100°C, and at
15 the core of the slabs the temperature is at least 100°C higher than the surface temperature.
2. A process according to claim 1, wherein the thin slabs have a thickness of between
45 mm and 80 mm.
3. A process according to claim 1 or 2, wherein at least an intermediate cooling and/or
heating is provided for among the rolling stands.
- 20 4. A plant for the production of steel strips from thin slabs coming from continuous
casting, comprising at least one heating furnace upstream of a multiple stand finishing
rolling mill, and a shear for shearing the slab directly following the continuous casting
where liquid core reduction has been performed, wherein one of said at least one furnace is
an induction furnace the working frequency of which is chosen sufficiently low in order to
25 bring the heating to a core of the slab and to substantially maintain a same temperature
difference between an inside and an outside of the slabs up to arrival of the slabs at the
inlet of the first rolling stand of said finishing rolling mill, whereby the slab average
temperature is higher than a surface temperature of the slabs and at the core of the slabs the
temperature is at least 100°C higher than said surface temperature, said surface temperature
30 being equal to or higher than 1100°C.
5. A plant according to claim 4, further including a descaler between the at least one

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furnace and the rolling mill.

6. A plant according to claim 4 or claim 5, wherein the distance between the outlet of the continuous casting and the inlet to the rolling mill is not greater than 100 m.
7. A plant according to any one of claims 4 to 6, wherein in addition to said induction furnace a second furnace of the tunnel type is provided, heated by gas.
8. A process for the manufacturing of steel strips substantially as hereinbefore described with reference to the drawings and/or Examples.
9. A plant for the production of steel strips substantially as hereinbefore described with reference to the drawings and/or Examples.

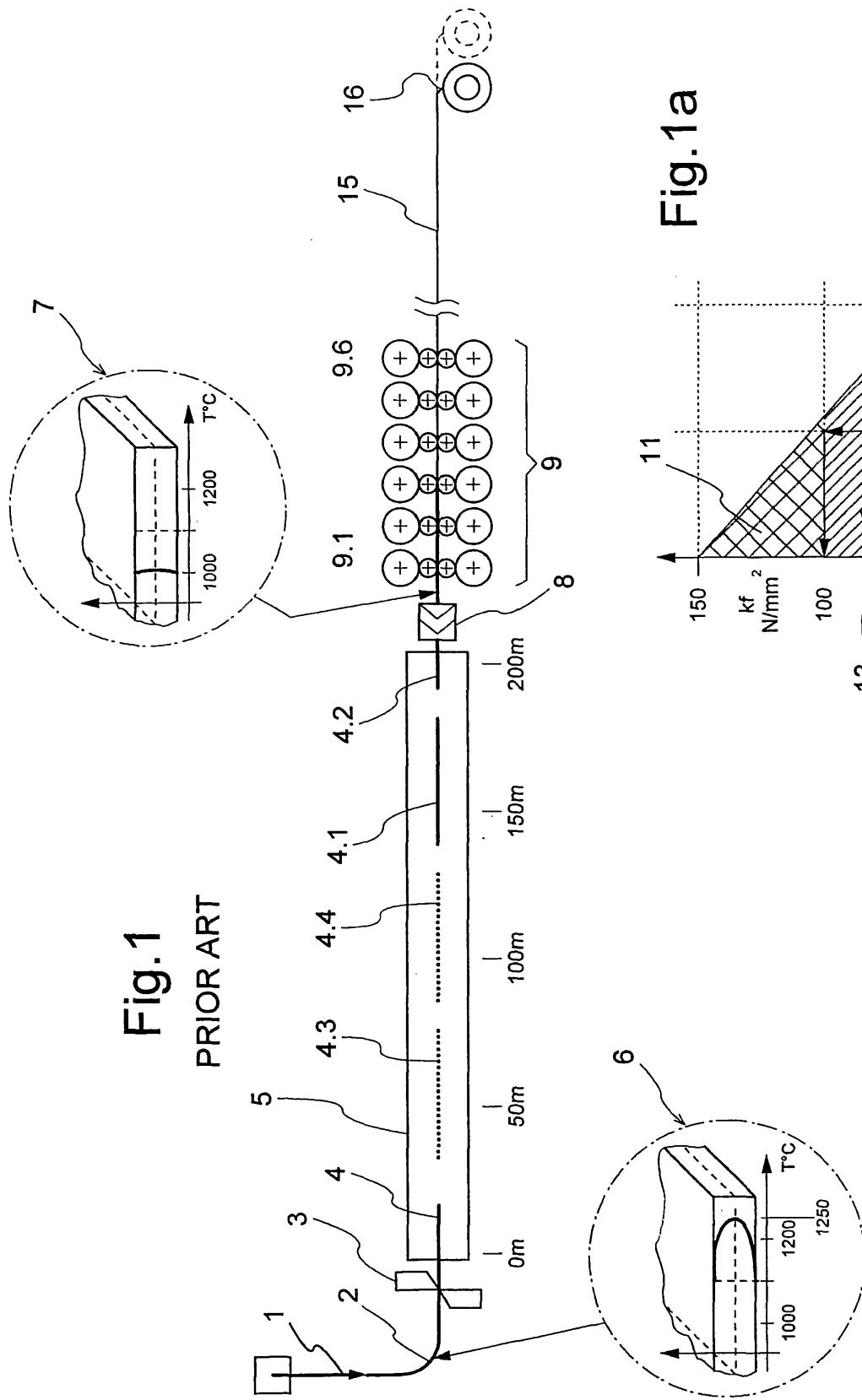


Fig. 1a

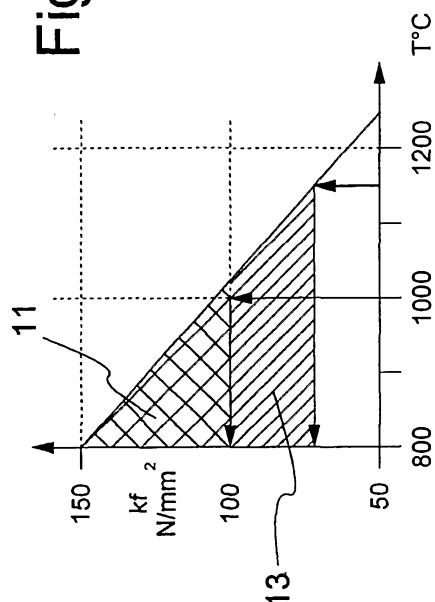


Fig.2

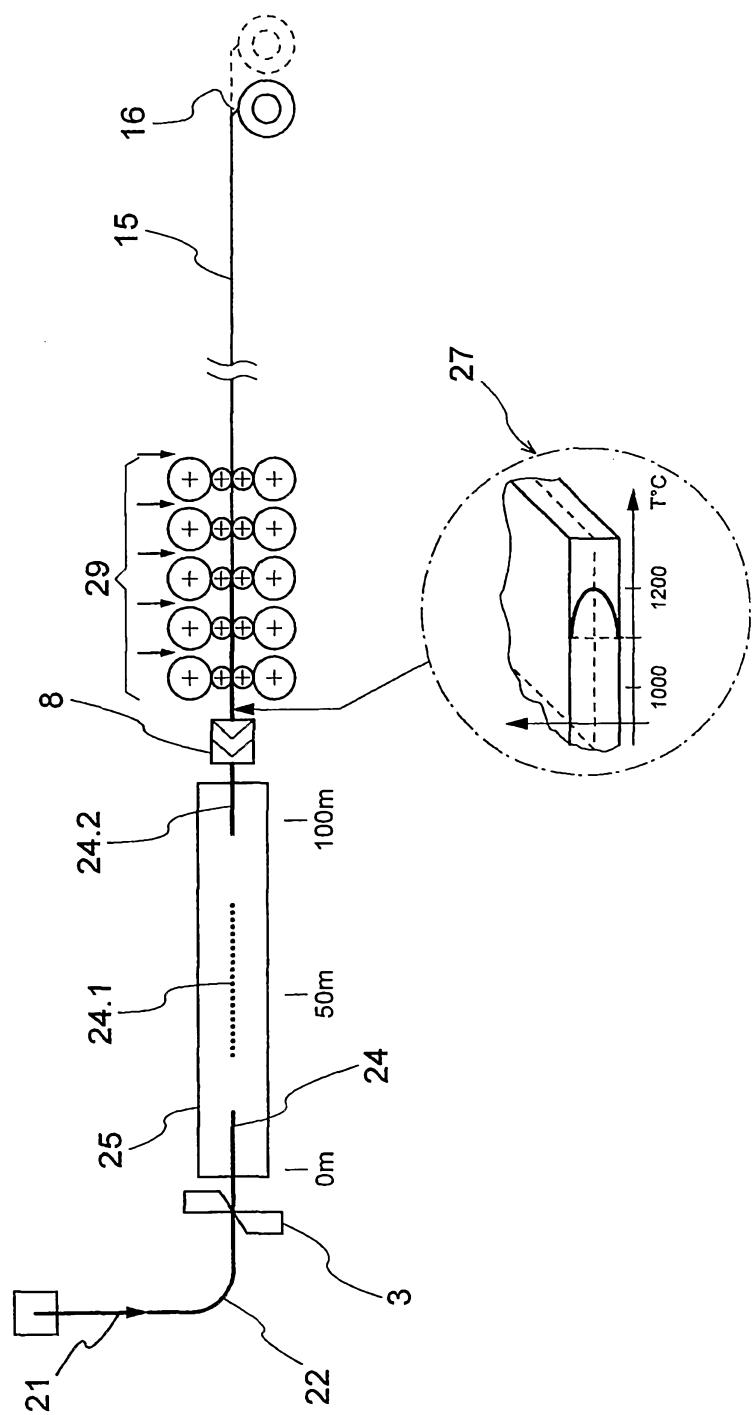


Fig.3

