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(54) Title: HYDROPHOBICALLY MODIFIED SACCHARIDE SURFACTANTS

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(57) Abstract: The invention relates to the use as surfactant, for the preparation of dispersions of multiphase systems that comprise a continuous aqueous phase containing a high concentration of electrolytes, of hydrophobically modified saccharides of general formula (I) and (II) $[A]_n(-M)_s$ (I) $[B]_m(-M)_{s'}$ (II) wherein $[A]_n$ represents a fructan-type saccharide $[B]_m$ represents a starch-type saccharide $(-M)$ represents a hydrophobic moiety that substitutes a hydrogen atom of a hydroxyl group of the fructosyl and/or glucosyl units of the fructan-type and starch-type saccharides, which is selected from the group consisting of an alkylcarbonyl radical of formula $R-NH-CO-$ and an alkylcarbonyl radical of formula $R-CO-$, wherein R represents a linear or branched, saturated or unsaturated alkyl group with from 4 to 32 carbon atoms, and s and s', which can have the same value or not, represent the number of said hydrophobic moieties that substitute the fructosyl or glucosyl unit, expressed as average degree of substitution (av. DS) which ranges from 0.01 to 0.5. The invention also relates to a method for the preparation and/or stabilisation of dispersions of multiphase systems that comprise a continuous aqueous phase containing a high concentration of electrolytes, by using as surfactant one or more hydrophobically modified saccharides of general formula (I) and/or (II) defined above. Also dispersions of multiphase systems are disclosed that comprise a continuous aqueous phase containing a high concentration of electrolytes and that comprise as surfactant one or more hydrophobically modified saccharides of general formula (I) and/or (II) defined above.

HYDROPHOBICALLY MODIFIED SACCHARIDE SURFACTANTS

Field of the invention

5 The present invention relates to the use as surfactant of hydrophobically modified saccharides for the preparation of dispersions of multiphase systems composed of one or more liquids, solids and/or gases dispersed in a continuous aqueous phase containing an electrolyte, to said dispersions, as well as to a method for preparing and stabilising dispersions.

Background and prior art

10 Industry is often confronted with the technical problem of making dispersions from a mixture of two or more phases which are non-miscible or only partly miscible with each other. The term dispersion refers to a composition that consists of a continuous phase that contains dispersed in
15 it small particles of one or more other phases forming one or more discontinuous phases. The dispersions which are most frequently encountered and, accordingly, which are of high interest to industry, are composed of a continuous aqueous phase and one or more discontinuous non-aqueous phases.

The term dispersion refers hereinafter to compositions that consist of a
20 continuous aqueous phase that contains dispersed in it small particles of one or more other phases forming one or more discontinuous phases (also named dispersed phases). Depending on the nature of the other phase(s) involved, the particles can be droplets (in case of a liquid phase), solid particles (in case of a solid phase) or gas bubbles (in case of a gaseous phase). Dispersions are
25 commonly prepared from a mixture or a pre-mix of the composing phases by thoroughly mixing the phases, for example by means of a high speed mixer or a homogeniser in case of liquid phases, or through grinding by means of a bead mill or a colloid mill in case of the presence of a solid phase. However, due to the non-miscibility or partial miscibility of the composing phases, the obtained
30 dispersions are commonly unstable.

In systems with a discontinuous liquid non-aqueous phase, the instability is characterised by the coalescence of the droplets of the dispersed liquid phase. In systems with a discontinuous solid phase, the instability is characterised by the flocculation, typically with formation of aggregates or clumps, of the
35 dispersed solid phase. In systems with a discontinuous gaseous phase, commonly named foams, the instability is characterised by fusing of the gas bubbles, resulting in the collapse of the foam.

As a result of said coalescence, flocculation or collapse of, respectively, the droplets, the solid particles or the gas bubbles, the dispersion may separate to a more or lesser extent into separate phases, and may ultimately separate completely into separate phases, which is thermodynamically the most favourable system.

It is already known for a long time that the addition of certain compounds to a mixture of non-miscible or partly miscible phases enables or facilitates the formation of dispersions and/or improves the stability of said dispersions against coalescence, flocculation and/or collapse, hereinafter termed in short stability. As a result of said improved stability, the coalescence, flocculation and/or collapse of the discontinuous phase or phases is inhibited, delayed or reduced to a more or lesser extent, compared to those of dispersions prepared in the absence of said compounds.

Typically said compounds are molecules that consist of a hydrophilic moiety that interacts with the aqueous continuous phase, and a hydrophobic moiety that interacts with the non-aqueous phase. They usually reduce the interfacial tension between liquid phases, solid/liquid phases and/or gas/liquid phases and, accordingly, they are said to present tensio-active properties. Said reduction facilitates the dispersion in the continuous aqueous phase of a liquid or of aggregates of liquid or solid particles into single particles, improves the wettability of a solid phase by a liquid phase, and enables the formation of a foam. As a result thereof the stability of the dispersions is improved and the tendency of the dispersions to separate into separate phases is reduced.

The compounds which enable or facilitate the formation of a dispersion and/or improve the stability of a dispersion against coalescence, flocculation and/or collapse are commonly referred to as surfactants, tensio-active agents or surface active agents. After the discovery of the effect of the tensio-active agents on dispersions, it has become common practice to add a surfactant to one or more of the phases or to a mixture of the phases of a composition to enable or facilitate the preparation of a dispersion from said phases and/or to improve the stability of the dispersion.

There exist various kinds of dispersions, which are in fact multiphase systems, such as biphasic systems and triphasic systems in which two or more phases appear as a discontinuous phase in the form of very small liquid, solid or gaseous particles, dispersed in a continuous aqueous phase. Biphasic systems include systems composed of a gas phase (gas bubbles) / continuous aqueous phase; a liquid phase (droplets)/continuous aqueous phase; or a solid phase

(solid particles)/ continuous aqueous phase. Triphase systems include systems composed of a gas phase/ liquid phase/continuous aqueous phase; a gas phase/ solid phase/ continuous aqueous phase; or a solid phase/ liquid phase/ continuous aqueous phase.

5 The dispersions of multiphase systems are conventionally classified, in function of the nature of the composing phases, in four groups, as follows:

(i) suspensions: systems consisting of a discontinuous solid phase which is composed of one or more solid compounds in a finely divided form, dispersed in a continuous aqueous phase;

10 (ii) emulsions: systems consisting of a discontinuous liquid phase in a finely divided form, which is composed of one or more miscible, partly miscible or non-miscible liquids, dispersed in a continuous aqueous phase;

(iii) foams: in biphasic systems: consisting of a discontinuous gas phase composed of bubbles of a gas or mixture of gases, dispersed in a continuous aqueous phase, and, in triphase systems: consisting of a discontinuous gas phase composed of bubbles of a gas or mixture of gases, dispersed in a said suspension or in a said emulsion;

15 (iv) suspoemulsions: triphase systems consisting of a discontinuous solid phase composed of finely divided particles of one or more solids and a discontinuous liquid phase composed of one or more miscible, partly miscible or non-miscible liquids, dispersed in a continuous aqueous phase.

20 Furthermore, still other variations of multiphase systems exist, for example a system consisting of a gas phase, a solid phase and two liquid phases.

25 All said multiphase systems are embraced herein by the term dispersion.

Surface active agents are usually classified, based on their action on the phases of a dispersion as *i.a.* detergent, emulsifier, emulsion stabiliser, wetting agent, suspension stabiliser, foaming agent, or foam stabiliser.

30 The action and effect of the surfactant largely depend of its chemical structure and/or the nature of the components of the dispersion. Accordingly, for the preparation of a dispersion, the kind of surfactant is commonly selected in function of the components of the multiphase system involved. Said selection is often made by the skilled person on the basis of screening experiments that are carried out routinely.

35 The earliest surfactants, typically used as detergents, were alkali soaps of naturally occurring fatty acids, commonly termed soaps, such as sodium palmitate. These compounds have been mostly replaced now by more effective synthetic surfactants. Typical classes of synthetic surface-active agents

that are used in industry now include anionic, cationic, amphoteric and non-ionic surfactants.

Anionic surfactants include, apart from said soaps, for example alkylbenzenesulfonates (ABS). ABS-type surfactants, being poorly
5 biodegradable, are nowadays mostly substituted for the better biodegradable linear alkylsulfonates (LAS).

Cationic surfactants typically include tetra-alkyl ammonium salts, such as dodecyl trimethyl ammonium chloride.

Amphoteric surfactants commonly include zwitterionic type compounds,
10 such as 3-[N,N-dimethyl N-dodecyl ammonio] 1-propane sulphonate.

Non-ionic surfactants mostly belong to the class of alkoxylated compounds, typically ethoxylated compounds, such as dodecyl hexa-oxyethylene glycol monoether.

The above surfactants perform satisfactorily in many multiphase systems
15 enabling the preparation of dispersions of industrially acceptable stability against coalescence, flocculation and/or collapse.

The presence of an electrolyte in the aqueous phase of a dispersion usually destabilises the dispersion, in spite of the presence of a surfactant, and provokes a considerable up to a complete coalescence of the discontinuous liquid
20 phase(s), flocculation of the solid phase(s), and/or collapse of the foam. Usually the higher the concentration of the electrolyte (up to a ceiling level) in the aqueous phase of a dispersion, and the higher the temperature, the more pronounced the destabilisation of the dispersion.

However, industry often has to prepare dispersions of multiphase
25 systems, typically biphasic and triphasic systems, that comprise a continuous aqueous phase containing a high concentration of one or more electrolytes. In these particular multiphase systems most known surfactants fail to provide dispersions of industrially acceptable stability.

As a result thereof, industry is often confronted with the technical
30 problem of providing dispersions of multiphase systems comprising a continuous aqueous phase containing one or more electrolytes, which present an industrially acceptable stability against coalescence, flocculation and/or collapse, particularly when the electrolyte is present at a high concentration and/or the dispersion is at a temperature above room temperature.

35

Aim of the invention.

The present invention aims to provide a solution to one or more of said technical problems as well as to other ones.

Description of the invention

In the search for improved and/or alternative surfactants, the inventors have unexpectedly found that the use as surfactants of a particular class of hydrophobically modified saccharides enables to solve one or more of the said technical problems.

Accordingly, in one aspect the present invention relates to a method of use as surfactant of hydrophobically modified saccharides for the preparation of stable dispersions or dispersions of improved stability from multiphase systems that comprise a continuous aqueous phase containing a high concentration of one or more electrolytes.

In an other aspect, the present invention relates to a method for the preparation of stable dispersions or dispersions of improved stability from multiphase systems comprising a continuous aqueous phase containing a high concentration of one or more electrolytes, by using a hydrophobically modified saccharide as surfactant.

In still a further aspect, the present invention relates to stable dispersions or dispersions of improved stability of multiphase systems that comprise a continuous aqueous phase containing a high concentration of one or more electrolytes, and a hydrophobically modified saccharide as surfactant.

By dispersion is meant hereinafter all multiphase systems composed of at least two phases of which one phase is a continuous aqueous phase, and the other phase or phases are discontinuous phases which are in the form of very small liquid, solid and/or gaseous particles that are dispersed in the said continuous aqueous phase. Said discontinuous phases are also named dispersed phase(s). The term dispersion preferably refers to biphasic systems and triphasic systems and includes suspensions, emulsions, foams and suspoemulsions.

By stable dispersion is meant herein a dispersion of industrially acceptable stability, which means that within a set time period and temperature range which are suitable for the intended industrial application, (i) in case of an emulsion: the discontinuous liquid phase(s) present an industrially acceptable stability against coalescence, (ii) in case of a suspension: the solid particles of the discontinuous phase(s) present an industrially acceptable stability against flocculation, (iii) in case of a foam: the gas bubbles present an industrially acceptable stability against collapse, and (iv) in case of a suspoemulsion: any of the discontinuous phases present an industrially acceptable stability against coalescence and/or flocculation.

By dispersion with improved stability is meant herein a dispersion that presents an improved stability against coalescence, flocculation and/or collapse, compared to dispersions known in the art.

A phenomenon often encountered with dispersions, typically in emulsions, suspensions and suspoemulsions, is that the dispersed particles of the discontinuous phase(s), being droplets and/or solid particles, upon standing, converge without coalescing or flocculating at either the upper or lower side of the continuous aqueous phase. This phenomenon is due to the difference in density between the continuous aqueous phase and the dispersed phase(s), and may even make appear a part of the continuous aqueous phase about free of dispersed particles. In case of an emulsion, this phenomenon is commonly named creaming. It is emphasised that said phenomenon is not regarded as instability and that a dispersion presenting creaming is considered herein as still a stable dispersion.

By electrolyte is meant herein a salt which dissolved in water or in contact with water or an aqueous medium will provide ionic conductivity as a result of its partial or complete dissociation into cations and anions.

The class of hydrophobically modified saccharides in accordance with the present invention consists of substituted polymeric saccharides corresponding to general formula (I) or (II)



wherein

$[A]_n$ represents a fructan-type saccharide with $[A]$ representing a fructosyl unit or a terminal glucosyl unit and n representing the number of fructosyl and glucosyl units in said saccharide molecule, n being named degree of polymerisation (DP),

$[B]_m$ represents a starch-type saccharide with $[B]$ representing a glucosyl unit and m representing the number of glucosyl units in said saccharide molecule, m being named degree of polymerisation (DP),

$(-M)$ represents a hydrophobic moiety that substitutes a hydrogen atom of a hydroxyl group of said fructosyl or glucosyl units, said moiety being selected from the group consisting of an alkylcarbamoyl radical of formula $R-NH-CO-$ and an alkylcarbonyl radical of formula $R-CO-$, wherein R represents a linear or branched, saturated or unsaturated alkyl group with 4 to 32 carbon atoms, and s and s' , which can have the same value or not, represent the number of hydrophobic moieties that substitute the fructosyl or glucosyl unit, expressed as (number) average degree of substitution (av. DS).

The substituted polymeric saccharides of formula (I) and (II) according to the present invention are derived by appropriate substitution from homodisperse or polydisperse, linear or branched fructan-type saccharides which are selected from the group consisting of inulin, oligofructose, fructo-
5 oligosaccharide, partially hydrolysed inulin, levan, and partially hydrolysed levan, or starch-type saccharides which are selected from the group consisting of modified starches and starch hydrolysates, namely by the substitution of the hydrogen atom of one or more of the hydroxyl groups of the fructosyl and/or glucosyl units by an hydrophobic moiety (-M), defined above.

10 Inulin is a fructan composed of molecules mainly consisting of fructosyl units that are bound to one another by β (2-1) fructosyl - fructosyl bounds, and possibly having a terminal glucosyl unit. It is synthesised by various plants as a reserve carbohydrate, by certain bacteria, and can also be synthetically obtained through an enzymatic process from sugars containing fructose units, such as
15 sucrose. Very suitable in accordance with the present invention is polydisperse, linear inulin or slightly branched inulin (typically inulin having a branching that is below 20 %, preferably below 10 %) from plant origin with a degree of polymerisation (DP) ranging from 3 to about 100.

Very suitable inulin is chicory inulin that has a DP ranging from 3 to about
20 70 and an av. DP of ≥ 10 . Even more suitable is chicory inulin that has been treated to remove most monomeric and dimeric saccharide side products, and that optionally also has been treated to remove inulin molecules with a lower DP, typically a DP from 3 to about 9.

Said grades of chicory inulin can be obtained from roots of chicory by
25 conventional extraction, purification and fractionation techniques, as for example disclosed in US 4,285,735, in EP 0 670 850 and in EP 0 769 026. They are commercially available for example from ORAFTI, Belgium as RAFTILINE® ST (standard grade chicory inulin with av. DP of 10-13), RAFTILINE® LS (standard grade chicory inulin with an av. DP of 10-13, and with in total less
30 than 0.5 wt% (on dry substance) of monomeric and dimeric saccharides) and RAFTILINE® HP (high performance grade chicory inulin, with an av. DP of about 23 which contains only minor amounts of monomeric saccharides, dimeric saccharides and inulin molecules with a DP from 3 to about 9).

Further suitable saccharides of the fructan-type include partially
35 hydrolysed inulin and inulin molecules with a DP ranging from 3 to about 9, namely oligofructose and fructo-oligosaccharide (*i.e.* oligofructose molecules with an additional terminal glucosyl unit). Said saccharides are known in the art. Typically suitable products are obtained by partial, enzymatic hydrolysis of

chicory inulin, for example as disclosed in EP 0 917 588. They are commercially available, for example as RAFTILOSE® P95 from ORAFTI, Belgium.

Further suitable saccharides of the fructan-type are levans and partially hydrolysed levans, molecules mainly consisting of fructosyl units that are bound to each other by β (2-6) fructosyl - fructosyl bounds and may have a terminal glucosyl unit. Levans and partially hydrolysed levans are known in the art.

Modified starches and starch hydrolysates are polymeric saccharides of the starch-type, consisting of D-glucosyl units which are linked to one another. In starch the glucosyl units are typically linked by α -1,4-glucosyl-glucosyl bounds, forming linear molecules, named amylose, or by α -1,4- and α -1,6 glucosyl-glucosyl bounds, forming branched molecules, named amylopectin. Starch occurs in various plants as a reserve carbohydrate and is manufactured at industrial scale from plant sources by conventional techniques.

The linkages between the glucosyl units in starch-type molecules are sensitive to disruption. This phenomenon is industrially exploited to prepare modified starches and starch hydrolysates from starch through thermal treatment commonly in the presence of a catalyst, through acidic hydrolysis, enzymatic hydrolysis, or shearing, or through combinations of such treatments. Depending on the source of the starch and the reaction conditions, a wide variety of modified starches and starch hydrolysates can be prepared at industrial scale by conventional methods. Modified starches (commonly named dextrans) and starch hydrolysates are known in the art.

Starch hydrolysates conventionally refer to polydisperse mixtures composed of D-glucose, oligomeric (DP 2 to 10) and/or polymeric (DP>10) molecules composed of D-glucosyl chains. D-glucose (dextrose) presents strong reducing power and said oligomeric and polymeric molecules also present reducing power resulting from the presence of reducing sugar units (which are essentially terminal glucosyl units). Accordingly, starting from a given starch, the more the hydrolysis has proceeded, the more molecules (monomeric D-glucose, oligomeric and polymeric molecules) will be present in the hydrolysate, and thus the higher will be the reducing power of the hydrolysate. The reducing power has become the feature of choice of industry to differentiate the various starch hydrolysates. It is expressed in dextrose equivalent (D.E.) which formally corresponds to the grams of D-glucose (dextrose) per 100 grams of dry substance. D-glucose having per definition a D.E. of 100, the D.E. indicates the amount of D-glucose and reducing sugar units (expressed as dextrose) in a given product on dry product basis. The D.E.

is in fact a measurement of the extent of the hydrolysis of the starch and also a relative indication of the average molecular weight of the starch-type saccharide molecules in the hydrolysate. Starch hydrolysates may range from a product essentially composed of glucose, over products with a D.E. greater
5 than 20 (commonly named glucose syrups), to products with a D.E. of 20 or less (commonly named maltodextrins). Starch hydrolysates are typically defined by their D.E. value. Often industry additionally defines starch hydrolysates by the source of the starch and/or their method of manufacture.

10 Starch hydrolysates that are very suitable saccharides for the preparation of hydrophobically modified saccharides of formula II above, have a D.E. ranging from 2 to 47. They may be obtained by conventional processes from various starch sources, such as for example starch from corn, potato, tapioca, rice, sorghum and wheat.

15 Starch hydrolysates are commercially available. For example, in the brochure from Roquette company " GLUCIDEX® Brochure 8/ 09.98 ", maltodextrins and glucose syrups are described in detail and various grades are offered for sale.

20 In a preferred embodiment of the invention, the above defined fructan-type saccharides and starch-type saccharides are substituted by two or more alkylcarbamoyl moieties of formula $R-NH-CO-$ in which the R group can be the same or different.

25 In another preferred embodiment of the invention, the above defined fructan-type saccharides and starch-type saccharides are substituted by two or more alkylcarbonyl moieties of formula $R-CO-$ in which the R group can be the same or different.

30 In still another preferred embodiment of the invention, the above defined fructan-type saccharides and starch-type saccharides are substituted by two or more hydrophobic moieties defined above, which are of a different nature. Accordingly, the saccharide may be substituted by one or more alkylcarbamoyl moieties and by one or more alkylcarbonyl moieties.

35 In said alkylcarbamoyl and alkylcarbonyl moieties, the alkyl group (R) is a linear or branched radical of 4 to 32 carbon atoms. Preferably, it is a linear radical with 6 to 20 carbon atoms, more preferably with 6 to 18 carbon atoms, most preferably with 8 to 12 carbon atoms. Said alkyl radical can be a saturated alkyl radical as well as an unsaturated alkyl radical, typically an unsaturated alkyl radical with one or two double or triple carbon-carbon bounds.

In a preferred embodiment said alkyl group (R-) is a linear, saturated or mono-unsaturated alkyl radical with 6 to 18 carbon atoms.

Highly preferred hydrophobic moieties include the ones shown in Table 1 below.

The fructosyl and glucosyl units of said polymeric saccharide molecules of the fructan-type and starch-type have two, three or four hydroxyl groups of which the hydrogen atom can be substituted by a said hydrophobic moiety, depending respectively whether the unit is at a branching point of the saccharide chain, is a unit of a linear part of the chain or is a terminal unit of the chain. The number of hydrophobic moieties per unit, indicated by the indexes s and s' in formula (I), respectively formula (II) above, is commonly expressed as the average degree of substitution (av. DS), corresponding to the average number of hydrophobic moieties per unit of the substituted saccharide molecule. The av. DS of hydrophobically substituted saccharides of formula (I) and (II) which are suitable in accordance with the present invention ranges from 0.01 to 0.5, preferably from 0.02 to 0.4, more preferably from 0.05 to 0.35, most preferably from 0.1 to 0.3.

The hydrophobically modified saccharides of formula (I) and (II) are known in the art and can be prepared by conventional methods. Hydrophobically modified saccharides of formula (I) and (II) wherein the hydrophobic moiety is an alkylcarbamoyl radical ($R-NH-CO-$) can be prepared for example by reaction of the appropriate fructan-type saccharide or starch-type saccharide with an alkyl isocyanate of formula $R-N=C=O$ (R having the meanings given above) in an inert solvent as described *e.g.* in WO 99/64549 and WO 01/44303. Hydrophobically modified saccharides of formula (I) and (II) wherein the hydrophobic moiety is an alkylcarbonyl radical ($R-CO-$) can be prepared by conventional esterification reactions, as for example disclosed in EP 0 792 888 and EP 0 703 243, typically by reaction of the appropriate fructan-type saccharide or starch-type saccharide with an anhydride of formula $R-CO-O-CO-R$ or an acid chloride of formula $R-CO-Cl$ (R having the meanings given above) in an appropriate solvent. Also Japanese patent application JP 3-197409 discloses fatty acid esters of fructo-oligosaccharides of the inulin-type as well as of the levan-type.

Many of the hydrophobically modified saccharides of formula (I) and (II) are disclosed to present tensio-active properties and to be useful as surfactant for the preparation of dispersions containing a continuous aqueous phase that is free of electrolytes or that contains only low concentrations of an electrolyte.

However, the prior art is absolutely silent about the particular and unexpected tensio-active properties of the hydrophobically modified saccharides of formula (I) and (II) above which enable to use these

hydrophobically modified saccharides as surfactants for the manufacture of dispersions that are stable or present improved stability from multiphase systems that comprise a continuous aqueous phase containing a high concentration of one or more electrolytes. Said electrolytes typically include
5 metal salts, ammonium salts, amine salts, quaternary ammonium salts, salts of organic bases and mixtures thereof, which partially or completely dissociate in an aqueous medium forming cations and anions, or zwitterions. The cations include metal ions from monovalent, bivalent, trivalent and tetravalent metals, and ions involving a nitrogen atom. Typical metal cations include ions of
10 lithium, sodium, potassium, magnesium, calcium, barium, chromium, manganese, iron, cobalt, nickel, copper, zinc and aluminium. Typical cations involving a nitrogen atom include ammonium ions, ions from salts of primary, secondary and tertiary amines such as for example monoalkyl amines, dialkyl amines, trialkyl amines and benzyl dialkyl amines, quaternary ammonium ions,
15 and ions formed from organic nitrogen bases such as for example morpholine, piperazine and heterocyclic compounds such as *e.g.* pyridine.

Said anions include hydroxyl anions and anions derived from inorganic acids as well as from organic acids, such as, for example, hydrogen halides including hydrofluoric acid, hydrochloric acid, hydrobromic acid and
20 hydroiodic acid, sulphuric acid, phosphoric acid, carbonic acid, formic acid, acetic acid and lactic acid.

By concentration of one or more electrolytes is meant herein the total concentration of the one or more electrolytes in the continuous aqueous phase of the dispersion. By high concentration is meant a total concentration of the
25 one or more electrolytes in the continuous aqueous phase which is higher, typically significantly higher, than the total concentration of the electrolyte(s) in the continuous aqueous phase of dispersions disclosed in the prior art. In accordance with the present invention, said total concentration in the continuous aqueous phase ranges from the lower limit of 0.1 to 1 mole per litre, depending on the nature of the electrolyte(s), including the valency of the ions
30 involved, and the temperature to which the dispersion is subjected, up to the higher limit of the range being the limit of the solubility of the electrolyte(s) in water at 25°C.

Typically, said high concentration ranges from about 0.5 mole to about 5
35 moles per litre, more typically from about 1 mole to about 5 moles per litre, even from about 2 moles to about 5 moles electrolyte(s) per litre continuous aqueous phase. The high concentration typically ranges for salts of monovalent cations from 0.1 mole, most typically from 0.5 mole, to about 5 mole per litre

aqueous phase, for salts of bivalent cations from 0.1 mole, most typically from 0.5 mole, to about 3 moles per litre aqueous phase, and for salts of trivalent cations from 0.1 to about 1 mole per litre aqueous phase.

5 In the dispersions according to the subject invention, the ratio non-aqueous phase(s) / aqueous phase may range from about 90 : 10 to about 1 : 99. Preferably said ratio ranges from about 65 : 35 to about 20 : 80. A typical ratio is 50 : 50. In case of non-aqueous liquid phase(s) or gas phases said ratio is expressed as volume : volume ratio; in case of non-aqueous solid phase(s), the ratio is expressed as weight : volume ratio.

10 Since the hydrophobically modified saccharides of formula (I) and (II) are more or less sensitive to hydrolysis, the pH of the aqueous phase of the multiphase system is preferably kept between 4 and 10, more preferably between 5 and 9, most preferably between 6 and 8.

15 The efficiency of the hydrophobically modified saccharides of formula (I) and (II) acting as surfactants in the preparation of dispersions from multiphase systems in accordance with the present invention depends from various factors. Said factors include the kind of the multiphase system, the kind and nature of the composing phases, the structure of the surfactant including the type and the degree of polymerisation of the saccharide, the nature of the hydrophobic moiety or moieties, the nature of the alkyl group of said hydrophobic moiety or moieties and the average degree of substitution DS. The efficiency furthermore depends on the nature of the electrolyte(s), the concentration of the respective electrolytes, the total concentration of the electrolyte(s) in the aqueous phase, the method of manufacture of the dispersion, the pH of the aqueous phase and the temperature at which the dispersion is stored. Usually the higher the total concentration of electrolyte(s) in the aqueous phase, the higher the amount of hydrophobically modified saccharide that is required for the preparation of a stable dispersion.

25 In accordance with the present invention also mixture of two or more surfactants of formula (I) and/or formula (II) may be used.

30 In addition to the hydrophobically modified saccharides according to the present invention, also conventional surfactants may be used to facilitate the formation of the dispersion and/or to improve its stability.

35 Furthermore, in cases where creaming occurs in emulsions or the comparable phenomenon in suspensions prepared in accordance with the present invention, conventional thickeners can be added to the dispersion to reduce the difference in density between the phases. As a result thereof the

dispersed liquid and/or solid phases remain better and/or longer homogeneously dispersed in the continuous aqueous phase.

It is to be noted that the hydrophobically modified saccharides of formula (I) and (II) above or a mixture thereof also perform well as surfactants for the preparation of stable dispersions, or dispersions with improved stability, comprising an aqueous phase which is free of electrolytes or contains only low concentrations of electrolytes.

For the preparation of a dispersion in accordance with the present invention, usually an amount is used of surfactant or mixture of surfactants of formula (I) and/or formula (II) above, that ranges from about 0.10 to about 20 %, preferably from about 0.15 to about 15 %, more preferably from about 0.20 to about 15 %, typically from about 0.50 to about 10 %. In case of emulsions, the % is expressed as % weight/volume (%w/v) on dispersed phase(s), in case of suspensions as % weight/weight (% w/w) on dispersed phase(s), and in case of foams as % weight/volume (%w/v) on the aqueous phase.

Preferred multiphase systems in accordance with the present invention include the biphasic systems: oil phase/aqueous phase (*i.e.* emulsions), solid phase/ aqueous phase (*i.e.* suspensions), and gas phase/aqueous phase (*i.e.* foams), and the triphasic systems: solid phase/oil phase/aqueous phase (*i.e.* suspoemulsions), gas phase/oil phase/aqueous phase, and solid phase/gas phase/aqueous phase.

The present invention is illustrated by the examples given below. The dispersions were prepared and evaluated according to the following methods.

Example 1.

Several emulsions were prepared according to four different methods.

In a first step of these methods the oil phase was added dropwise to the aqueous phase containing the surfactant (hydrophobically modified saccharide of formula (I) or (II) in demineralised water), while the mixture was stirred by means of a high speed homogeniser (for example CAT* X620, * trade name of Ingenieurbüro CAT, M. Zipperer GmbH, Staufen, Germany).

The dispersions were prepared on a 50 ml scale.

The particular conditions of the addition of the oil phase to the aqueous phase and of the homogenising applied in each method are indicated below.

Method A (Four step process): The oil was added during the first step. In the four step mixing procedure, the mixing speed was stepwise increased as

follows: 2 minutes at 9,500 rpm, followed by 1 minute at 13,500 rpm, followed by 45 seconds at 20,500 rpm and finally 1 minute at 24,000 rpm. Mixing was carried out by means of a high speed homogeniser.

5 Method B (One-step process): The oil was added during the first minute of the mixing process while stirring the mixture at 9,500 rpm, and this speed was maintained for 5 minutes in total. Mixing was carried out by means of a high speed homogeniser.

10 Method C (Two-step process): The oil was added during the first minute of the mixing process with stirring at 9,500 rpm, and this speed was maintained for 5 minutes in total. Mixing was carried out with a high speed homogeniser. Then, the obtained mixture was treated at 700 bar for 1 minute in a high pressure homogenizer (Microfluidizer®, trade name of Microfluidics Corp., USA).

15 Method D (Two-step process): The oil was added during the first minute of the mixing process while stirring at 9,500 rpm and this speed was maintained for 5 minutes in total. Mixing was carried out with a high speed homogeniser. Then the mixture obtained was subjected to a treatment at 700 bar for 30
20 seconds in a high pressure homogenizer (Microfluidizer®, trade name of Microfluidics Corp., USA).

Evaluation of the stability of the emulsions.

25 The emulsions obtained were divided in two parts, one of which was stored at room temperature (RT) and the other one at 50°C.

The stability of the emulsions was evaluated macroscopically by visual inspection for oil droplets and oil separation.

Specific emulsions evaluated.

30 The nature of the hydrophobically modified saccharides of formula (I) and (II) used as surfactant in Example 1 is indicated in Table 1 below.

The particulars of the emulsions tested and the results obtained in Example 1 are shown in Table 2 below.

Table 1: Hydrophobically modified saccharides of formula (I) and (II)

SURFACTANT						
Product n°	Lab ref.	Formula (I) or (II)	Type	Hydrophobic Moiety		av. DS
				M	R-	
1	MP 79	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.02
2	AM 150	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.08
3	AM 149	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.09
4	AM 154	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.2
5	AM 238	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.07
6	AM 219	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.09
7	AM 259	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
8	MP 28	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
9	MP 73	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
10	MP 66b	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.12
11	AM 220b	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.15
12	AM 82	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.21
13	MP 20	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.3
14	MP 32	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₅ -	0.21
15	MP 78	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.023
16	AM 22	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.054
17	MP 80	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.11
18	AM 244	(I)	b	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.3
19	MP 36	(I)	a	R-CO	CH ₃ (CH ₂) ₁₀ -	0.12
20	MP 41	(I)	a	R-CO	CH ₃ (CH ₂) ₁₄ -	0.1
21	MP 40	(I)	a	R-CO	CH ₃ (CH ₂) ₇ CH=C H-(CH ₂) ₇ -	0.05
22	MP 42	(I)	a	R-CO	CH ₃ (CH ₂) ₁₆ -	0.11
23	AM 141	(II)	d	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.05
24	AM 117	(II)	e	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
25	PC 17	(II)	c	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
26	PC 16	(II)	d	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.18
27	MP 98	(II)	d	R-CO	CH ₃ (CH ₂) ₁₀ -	0.1
28	AM 70	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.11
29	MP 31	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₅ -	0.12
30	MP 92B	(I)	f	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.19
31	MP 102	(I)	f	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.13

Formula [A]_n(-M)_s (I) [B]_m(-M)_{s'} (II)

- 5 a = inulin, av. DP : 23 (RAFTILINE® HP, ORAFTI, Belgium)
 b = inulin, DP mainly between 2 and 8, av. DP : about 4.5 (RAFTILOSE® P95, ORAFTI, Belgium)
 c = maltodextrin, DE 2 (Roquette, France)
 d = maltodextrin, DE 28 (Roquette, France)
 10 e = maltodextrin, DE 47 (Roquette, France)
 f = inulin, av. DP : 13 (RAFTILINE® ST, ORAFTI, Belgium)

Table 2 : Emulsions: Particulars and Stability

Surfactant		Ratio composing phases oil phase/ aqueous phase		Disper- sion	Salt		Stability (in months)	
Prod. n° (*)	%w/v on disper sed liquid phase	Ratio (v/v) (**)	Kind of oil	Method of prep.	Kind	Molar ity in aqueous phase	at Room Temp	at 50°C
1	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 4	> 4
2	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
2	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 5	> 5
3	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
3	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1,5		> 2.5
3	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	2		2,5
4	8	50:50	85% Isoparaffinic oil ¹ + 15% Squalane oil ²	D	NaCl	1	> 2	> 2
4	8	50:50	85% Isoparaffinic oil ¹ + 15% Squalane oil ²	D	MgSO ₄	1	1,5	1.5
5	2	50:50	Isoparaffinic oil ¹	B	NaCl	1	> 14	> 1
6	2	50:50	Isohexadecane oil ³	A	NaCl	1	> 14	> 1
7	2	50:50	Oilmix ⁴	A	NaCl	1	> 12	> 1.3
7	2	50:50	Isoparaffinic oil ¹	A	CaCl ₂	1	> 12	> 4
7	2	50:50	Isoparaffinic oil ¹		CaCl ₂	2	> 12	4
8	0.25	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 7	> 7
8	1.6	50:50	Isoparaffinic oil ¹ + 0.4% Sorbitan monolaurate ⁵	A	NaCl	1	> 7	> 7
8	0.8	50:50	Isoparaffinic oil ¹ + 0.2% Sorbitan ⁵ monolaurate	A	NaCl	1	> 7	> 7
8	0.4	50:50	Isoparaffinic oil ¹ + 0.1% Sorbitan ⁵ monolaurate	A	NaCl	1	> 7	> 7
8	2	50:50	Isoparaffinic oil ¹	A	MgCl ₂	5	> 2	> 0.7
9	2	50:50	Isoparaffinic oil ¹	A	Ca- lactaat	1	> 3	> 3
9	2	50:50	Isoparaffinic oil ¹	A	Na- lactaat	1	> 3	> 3
9	2	50:50	Isoparaffinic oil ¹	A	Ammon ium sulfate	1	> 3	> 3
10	2	50:50	Cyclomethicone oil ⁶	A	NaCl	1	> 6	> 6
10	2	50:50	Isoparaffinic oil ¹	A	MgCl ₂	1	> 3	> 3

Surfactant		Ratio composing phases oil phase/ aqueous phase		Disper - sion	Salt		Stability (in months)	
Prod. n° (*)	%w/v on disper sed liquid phase	Ratio (v/v) (**)	Kind of oil	Method of prep.	Kind	Molar ity in aqueous phase	at Room Temp	at 50°C
10	2	50:50	Isopropyl myristate oil ⁷	A	NaCl	1	> 4	> 3
10	2	50:50	Isoparaffinic oil ¹	A	NaCl	5	> 5	> 5
10	2	20:80	Isoparaffinic oil ¹	A	MgSO ₄	1	> 2	> 2
10	5	20:80	Isoparaffinic oil ¹	A	MgSO ₄	1	> 2	> 2
10	2	80:20	Isoparaffinic oil ¹	A	MgSO ₄	1	> 2	> 2
10	1.25	80:20	Isoparaffinic oil ¹	A	MgSO ₄	1	> 2	> 2
10	2	50:50	Isoparaffinic oil ¹	A	NH ₄ Cl	1	> 1.5	> 1.5
10	0.5	50:50	Isoparaffinic oil ¹	A	NH ₄ Cl	1	> 1.5	> 1
10	2	50:50	Isoparaffinic oil ¹	A	Et3N. HCl.aq	1	> 1	> 1
10	2	50:50	Isoparaffinic oil ¹	A	Na citrate	0.5	> 1	> 1
10	2	50:50	Isoparaffinic oil ¹	A	Glypho sate ⁸	0.7	> 1.5	> 1.5
11	2	50:50	Isoparaffinic oil ¹	A	NaCl	1.5	> 16	> 2.5
11	2	50:50	Isoparaffinic oil ¹	A	NaCl	2	> 16	2.5
11	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1.5	> 16	2.5
11	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	2	> 16	2.5
12	8	50:50	85 % Isoparaffinic oil ¹ + 15% Squalane oil ²	C	NaCl	1	> 2	> 2
12	8	50:50	85 % Isoparaffinic oil ¹ + 15% Squalane oil ²	C	MgSO ₄	1	> 2	> 2
13	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
13	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 5	> 5
14	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
14	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 5	> 5
15	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
16	2	50:50	High oleic sunflower seed oil ⁹	A	NaCl	1	> 2	> 2
16	2	50:50	High oleic sunflower seed oil ⁹	A	MgSO ₄	1	> 2	> 2
17	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
18	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 14	> 1
20	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 8.5	> 6
21	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 8.5	> 8.5
22	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 8.5	> 8.5

Surfactant		Ratio composing phases oil phase/ aqueous phase		Disper - sion	Salt		Stability (in months)	
Prod. n° (*)	%w/v on disper sed liquid phase	Ratio (v/v) (**)	Kind of oil	Method of prep.	Kind	Molar ity in aqueous phase	at Room Temp	at 50°C
23	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 1.5	> 1.5
24	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 1.5	> 1.5
25	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 4	> 4
26	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 4	> 4
27	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 5	> 5
27	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 5	> 2
30	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 4	> 4
30	2	50:50	Isoparaffinic oil ¹	A	MgSO ₄	1	> 4	> 4
31	2	50:50	Isoparaffinic oil ¹	A	NaCl	1	> 3	> 3

Legend

(*)The product number corresponds to the product number given in Table 1.

(**) volume ratio of the composing phases before homogenising.

Methods A, B, C and D for preparing the dispersions are as defined above.

¹ Isopar M - Exxon Chemicals

² Pripure3759 Squalane (vegetable oil) - Uniqema

³ Arlamol HD - Uniqema

⁴ oilmix = (2/10/4/2) - high oleic sunflower seed oil - FLORASUN 90 (International Flora Technologies Ltd.)/ isohexadecane oil - Arlamol HD (Uniqema)/ glycerol tricaprilate, caprate - Estol 3603 (Uniqema)/ Avocado oil (Alpha pharma)

⁵ Span 20 - Uniqema

⁶ EU 344 cyclomethicone oil - Dow Corning

⁷ Estol 1514 - Uniqema

⁸ Glyphosate was not used as such, but the commercial product Round Up plus® (Monsanto) was used as the aqueous phase.

⁹ FLORASUN 90 - International Flora Technologies Ltd

5

Example 2Comparative tests

The efficiency as surfactant of the hydrophobically modified saccharides of formula (I) and (II) was compared to those of commercial surfactants.

10 The commercial products used in the comparative tests of Example 2 are indicated in Table 3 below.

The same procedures, methods and conditions were used as the ones described in Example 1 above. The data of the tests of Example 2 are shown in Table 4

below and these data are to be compared with the data obtained in Example 1 and presented in Table 2.

5 Table 3 : Commercial products used in the comparative examples of Example 2.

Product reference	Product name (trade name)	Nature	Producer
Ref 1	DUB SE 15P	Saccharose monopalmitate	Stearinerie Dubois, France
Ref 2	DUB SE 16S	Saccharose monostearate	Stearinerie Dubois, France
Ref 3	Pluronic PE 6400	Block copolymer	BASF, Germany
Ref 4	Pluronic PE 6800	Block copolymer	BASF, Germany
Ref 5	Plantacare 1200UP	Lauryl glucoside	Fluka
Ref 6	Pemulen TR1	Polymeric emulsifier	BF Goodrich, Ohio USA
Ref 7	Arlatone Versaflex V-175	Nonionic, polymeric -based emulsifying system ¹	Uniqema, UK

¹ Arlatone Versaflex V-175 is a blend of polysaccharides and esters.

Table 4 : Stability of comparative emulsions

Surfactant		Ratio of phases oil / aqueous phase		Disper - sion	Salt		Stability	
Prod. ref (*)	% w/v on dispersed liquid phase	Ratio (v/v) (**)	Kind of oil	Method of prep.	Kind	Molarity in aqueous phase	at room temp.	at 50°C
Ref 1	2	50/50	Isoparaffinic oil ²	A	NaCl	1	> 5 months	1 day
Ref 2	2	50/50	Isoparaffinic oil ²	A	NaCl	1	> 5 months	1 day
Ref 3	2	50/50	Isoparaffinic oil ²	A	NaCl	1	> 5 months	<5 months
Ref 4	2	50/50	Isoparaffinic oil ²	A	NaCl	1	> 5 months	<5 months
Ref 3 ³	2	50/50	Isoparaffinic oil ²	A	MgSO ₄	1	<5 months	<1 months
Ref 4 ³	2	50/50	Isoparaffinic oil ²	A	MgSO ₄	1	> 5 months	<1 months
Ref 5	2	50/50	Isoparaffinic oil ²	A	NaCl	1	>3 months	>3 months
Ref 5	2	50/50	Isoparaffinic oil ²	A	MgSO ₄	1	>3 months	>3 months
Ref 5	2	50/50	Isoparaffinic oil ²	A	NaCl	5	<8days	<8days
Ref 5	1	50/50	Isoparaffinic oil ²	A	MgSO ₄	2	> 1 day	1 day
Ref 5	2	50/50	Isoparaffinic oil ²	A	MgSO ₄	2	<8days	<8days
Ref 6	4	20/80	Isoparaffinic oil ²	E ⁴	MgSO ₄	1	impossible	impossible
Ref 7	5	20/80	Isoparaffinic oil ²	F ⁵	MgSO ₄	0.5	> 1 week	< 1 week

(*) The product reference corresponds to the one indicated in Table 3.

5 (**) volume ratio of the composing phases before homogenising.
Method A for preparing the dispersions was as defined above

¹ Arlatone V-175 is a blend of polysaccharides and esters.

² IsoparM - Exxon Chemicals

³ Emulsions were very flocculated and had an unsmooth, not bright white look

⁴ preparation of emulsion according to method E: First the surfactant was added to the aqueous phase (containing the salt) under continuous stirring (propeller stirrer) at 850 rpm, then the oil phase was added dropwise while still stirring at 850 rpm during 10 minutes.
Addition of the salt after emulsifying yielded no good result neither (emulsion collapsed)

⁵ preparation of emulsion according to method F (method suggested by Uniqema (ICI, UK) for the preparation of an emulsion with Arlaton Versaflex at lab scale (200 g) according to the cold procedure):

- Put gently bit by bit Arlatone Versaflex in the water phase under stirring (800-1000 rpm)
- Continue to stir for about 10 minutes (800-1000 rpm)
- Add all water-soluble ingredients to the water phase under stirring (800-1000 rpm)
- Add the oil phase to the water phase under stirring (800-1000 rpm)
- Homogenise for 2 minutes at high speed (about 10,000 rpm)
- Stir (800-1000 rpm) until appearance is homogeneous.

Example 3

Suspensions in accordance with the present invention were made and evaluated as follows.

5 2.5 g Carbon Black (Elftex 570, Cabot corporation) was added slowly to 40 ml of a 1.25 % (% in w/v) aqueous surfactant solution (surfactant: product 9 of Table 1) (containing either 0 or 1 Mole of NaCl) while stirring the solution at 8500 rpm by means of a high speed homogeniser. After addition of the powder, the dispersion was stirred for 3 extra minutes at 9500 rpm.

10 Microscopic evaluation of the suspensions made with and without NaCl in the aqueous phase showed that the addition of the surfactant highly reduced flocculation of the particles for at least 5 days at room temperature. In comparative tests, the suspensions made in the absence of the surfactant showed considerable flocculation.

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Example 4

A suspension consisting of polystyrene particles dispersed in aqueous medium was prepared using a surfactant-free method (A. Kotera, *et al.*, Kolloid ZZ. Polym., 227 (1968) 759) by mixing milli-Q water, styrene-monomer (10 % v/v) and potassium persulfate ($K_2S_2O_8$; 0.06 % w/w on total) under nitrogen atmosphere (about 1 bar) at 70°C during 24 hours. In this way negatively charged polystyrene particles with a mean diameter of 210 nm were obtained. The stability of the obtained polystyrene dispersion in the presence of a salt (so-called salt-stability) with and without addition of a surfactant according to the invention was investigated and the critical coagulation concentration (CCC) was determined. The test was carried out by mixing the surfactant-free polystyrene dispersion, diluted with water to a dispersion at 5 % w/w polystyrene, with a given amount of surfactant and electrolyte (NaCl or $CaCl_2$), at room temperature and keeping the samples in a water bath at 25°C for 12 hours. Coagulation of the particles was assessed through visual observation and by optical microscopy. The CCC, being the lowest salt concentration in mole/l at which coagulation was observed, was determined. Table 5 shows the CCC-results for the stabilisation of aqueous dispersions at 5 % w/w polystyrene with various surfactants and salts.

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Table 5: CCC results of aqueous dispersions at 5 % w/w polystyrene

Surfactant	Conc. of surfactant (% w/w on total)	Conc. of surfactant (% w/w on dispersed phase)	CCC (in mole/l)	
			NaCl	CaCl ₂
Without surfactant *	-	-	0.375	0.0075
Product n° 9 of Table 1 above	0.25	5.0	> 5.17	> 4.37
Product n° 9 of Table 1 above	0.01	0.2	nd	> 1.6
Brij [®] 30 (1)*	0.25	5.0	0.32	0.25
Na-dodecylsulfate (2)*	0.25	5.0	nd	0.035
Synperonic PE L64 (3)*	0.25	5.0	nd	0.088
Plantacare 1200UP (4)*	0.25	5.0	nd	0.05
Plantacare 2000 (5)*	0.25	5.0	nd	0.065

Legend:

* : comparative test

nd : not determined

(1) : Brij[®]30 (=fatty alcohol-ethoxylate) (trade name, ICI, UK)

(2) : Sodiumdodecylsulfate (=anionic surface active agent) – 99% pure (Across Organics)

(3) : Synperonic PE L64 (=EO/PO block copolymer) (trade name, ICI, UK)

(4) : Plantacare 1200UP (=laurylglucoside) (trade name, Fluka)

(5) : Plantacare 2000 (=decylglucoside) (trade name, Fluka)

The results of the experiments described in Table 5 regarding a typical, hydrophobically modified saccharide clearly show that, according to the present invention, the hydrophobically modified saccharides are suitable as surfactants for the stabilisation of dispersions that contain a high concentration of an electrolyte. The CCC-value obtained indicates that dispersion stability is guaranteed even at a very low concentration of the hydrophobically modified saccharide.

Example 5

Aqueous poly(methylmethacrylate) (PMMA)-dispersions were made by mixing methyl methacrylate (MMA) (5 % w/w), water (94.7% w/w), potassium persulfate (K₂S₂O₈) (0.025 % w/w) and sodium dodecylsulfate (SDS) (0.286 % w/w). The polymerisation reaction was carried out under nitrogen atmosphere

at about 1 bar at 70°C under stirring during 24 hours. A dispersion of PMMA-particles with a mean diameter of 61.8 nm was obtained. The dispersion obtained was diluted with water to a suspension at 2.5% w/w PMMA-particles, which was used for the determination of the critical coagulation concentration (CCC). By gradual addition of CaCl₂ to the suspension, a CCC value was found for CaCl₂ of 0.0075 mole/l. Addition to the suspension of 0.5 % w/w (20 % w/w on dispersed phase) of an hydrophobically modified saccharide (product 9 of Table 1 above) resulted in a CCC of more than 2.29 mole/l. This illustrates, according to the invention, the dispersion-stabilising effect of the hydrophobically modified saccharides on suspensions containing a high concentration of an electrolyte.

Example 6

The influence of salt on foam stability (a liquid/gas two-phase system) was investigated using a Foamtester R2000 (Sita Messtechnik GmbH, Germany). The apparatus generates in a standardised way foam in a 1500 ml recipient and follows the foam stability as a function of time. In a series of experiments, in accordance with the present invention, a given concentration of a hydrophobically modified saccharide was dissolved in an aqueous 1 mole/l NaCl solution and 300 ml of the solution was put into the Foamtester. The apparatus generated foam by stirring the mixture in contact with air at 2,000 rpm during one minute. Accordingly, the generated foam volume (V₀) was automatically determined and foam stability was followed as a function of time by measurement of the remaining foam volume (expressed as % of V₀). The results are shown in Table 6 below.

Table 6 : Foam stability of a system containing a hydrophobically modified saccharide in an aqueous 1 mole/l NaCl solution

Surfactant	Concentration of surfactant (% w/v)	Generated foam volume V ₀ ** (ml)	% of V ₀ after 80 minutes
SDS *	0.3%	300	50
Product n° 9 of table 1	0.1%	400	75
Product n° 3 of table 1	0.1%	580	90

* : comparative example

** : V₀ = volume of generated foam at time zero (= just after foam generation)

From table 6 it follows that, compared to the use of SDS, the use according to the present invention of hydrophobically modified saccharides generate in the presence of a high concentration of an electrolyte salt, a higher volume of foam and give more stability to the foam.

Examples 7 and 8

Example 7 shows a cosmetic composition according to the present invention, being a highly stable anti-perspirant emulsion containing a high amount of an aluminium salt (as anti-perspirant agent) in the water phase and a high load of an oil phase (as emollient), in the presence of a hydrophobically modified saccharide as surfactant.

Example 8 (comparative) shows a same composition as in example 7, but with a same amount of a commercial surfactant.

To prepare the emulsions of Examples 7 and 8, the composition of which is indicated below, phases A and B were prepared separately at room temperature (RT) by homogeneously mixing of the ingredients. Accordingly, at RT, Phase B was added to phase A in 2 minutes while mixing at 3,000 rpm and the mixture was additionally homogenised by stirring at 15,000 rpm during 3 minutes.

Comparison of the compositions of Examples 7 and 8 showed that the formulation of Example 7 was still stable towards coalescence after storage for 120 hours at 45°C, while the emulsion of Example 8, stored under the same conditions, showed significant oil separation.

Example 7		Example 8*	
Ingredients	%	Ingredients	%
<u>Phase A</u>		<u>Phase A</u>	
Water	22	Water	22
Aluminium Chloro-Hydrate (50 wt%)	50	Aluminium Chloro-Hydrate (50 wt%)	50
Product n° 9-table 1	1	Arlacel 165 (1)	1
<u>Phase B</u>		<u>Phase B</u>	
Caprylic capric Triglyceride	12.5	Caprylic capric Triglyceride	12.5
Isostearyl iso-Stearate	12.5	Isostearyl iso-Stearate	12.5
Phenoxy ethanol		Phenoxy ethanol	
+ Paraben (2)	0.5	+ Paraben (2)	0.5
Fragrance	0.4	Fragrance	0.4

*: comparative example

(1) : Arlacel 165 (trade name, ICI, UK) (=glyceryl stearate and PEG-100 stearate)

(2) : Paraben (trade name, Bufo, Belgium) (= 4-hydroxybenzoic acid)

Examples 9 and 10

- Capillary treatment products often contain high amounts of electrolytes as active materials. The quality of capillary treatment products can be improved by the addition of emollients. Example 9 presents an example of a capillary treatment product in the form of an emulsion, containing a hydrophobically modified saccharide as surfactant in accordance with the present invention, that is enriched by a significant amount of an oil phase. Example 10 (comparative) presents a same emulsion as Example 9 but in which the hydrophobically modified saccharide was replaced by the surfactant sorbitan isostearate.
- The composition of Examples 9 and 10 is indicated below. To prepare the emulsions of Examples 9 and 10, phases A and C were prepared separately at room temperature by homogeneously mixing of the ingredients. The ingredients of phase B were then added to phase A, and then phase C was added under stirring at 3,000 rpm to said mixture of phases A and B, yielding the emulsion of respectively Example 9 and Example 10. After storage for 48 hours at 50°C, the formulation according to Example 10 showed significant oil separation (coalescence), whereas Example 9 showed no oil separation.

Example 9		Example 10*	
Ingredients	%	Ingredients	%
<u>Phase A</u>		<u>Phase A</u>	
Water	47	Water	47
Na ₂ EDTA	0.1	Na ₂ EDTA	0.1
NH ₄ Thioglycolate	17	NH ₄ Thyoglycolate	17
NH ₄ Bicarbonate	4.5	NH ₄ Bicarbonate	4.5
Styrene/vinyl pyrrolidone copolymer	0.3	Styrene/vinyl pyrrolidone copolymer	0.3
Ammonia	0.5	Ammonia	0.5
pH adjustment till pH 8.8		pH adjustment till pH 8.8	
PEG-15 Coco		PEG-15 Coco	
Polyamine	3.6	Polyamine	3.6
Product n°9 (table 1)	0.5 surfactant	—	
<u>Phase B</u>		<u>Phase B</u>	
Polysorbate 20	0.6	Polysorbate 20	0.6
Fragrance	0.4	Fragrance	0.4
<u>Phase C</u>		<u>Phase C</u>	
Isostearyl		Isostearyl	
Isostearate	12.5	Isostearate	12.5
Ethoxy diglycol		Ethoxy diglycol	
Oleate	12.5	Oleate	12.5
Sorbitan isostearate	0.5 surfactant	Sorbitan isostearate	1.0 surfactant

*: comparative

Examples 11 and 12

Using hydrophobically modified saccharides according to the invention, a facial or hand cream containing high amounts of a moisturization agent (typically sodium pyrrolidone carboxylate (Nalidon®, trade name of UCB, Belgium) and presenting excellent stability can be prepared as shown by Examples 11 and 12. The samples are obtained by preparing separately phases A under gently warming up (warm process), B (cold process at RT) and C (cold process at RT). Then Phase B is added to Phase A in 2 minutes while mixing at 3,000 rpm, with additional homogenizing during 5 minutes at 15,000 rpm. Then Phase C is added to the obtained mixture under slow stirring, yielding the emulsions of Examples 11 and 12.

Example 11 presents a composition according to the invention of a cream containing a hydrophobically modified saccharide, which shows after storage of 120 hours at 45°C and after 15 minutes of centrifugation at 13,000 rpm, no coalescence. Comparative Example 12 tested under the same conditions showed strong coalescence with eventual formation of an oil layer and an aqueous layer. In Examples 11 and 12 the thickener is sodium magnesium silicate because it is stable towards electrolytes. Conventional thickeners based on polycarboxylic acids and hydrophobically poly-carboxylic acids lose their thickener behaviour under the applied conditions.

Example 11		Example 12 *	
Ingredients	%	Ingredients	%
<u>Phase A (warm process)</u>		<u>Phase A (warm process)</u>	
Water	59	Water	59
Sodium Magnesium silicate	3.0	Sodium Magnesium silicate	3.0
Product n°9-table 1	0.5	Sorbitan isostearate	0.5
Phenoxy ethanol + Paraben **	0.5	Phenoxy ethanol + Paraben **	0.5
<u>Phase B (cold process)</u>		<u>Phase B (cold process)</u>	
Isostearyl Isostearate	12.5	Isostearyl Isostearate	12.5
Caprilic capric triglyceride	12.5	Caprilic capric triglyceride	12.5
Fragrance	0.4	Fragrance	0.4
<u>Phase C</u>		<u>Phase C</u>	
Sodium Pyrrolidone Carboxylate	12	Sodium Pyrrolidone Carboxylate	12

* : comparative

** : Paraben (trade name, Bufo, Belgium) (= 4-hydroxybenzoic acid)

The results of the Examples above clearly show that the hydrophobically modified saccharides of formula (I) and (II) present tensio active properties which make these compounds useful as surfactants for the preparation of
5 dispersions comprising an aqueous phase containing a high concentration of electrolytes, that are stable at room temperature or show improved stability compared to dispersions prepared with known surfactants. The dispersions according to the present invention even present excellent stability at elevated temperatures such as at 50 °C and even at higher temperatures (*e.g.* dispersion
10 with product 5 in Table 2 remains stable for at least 1 month at 65° C).

The dispersions in which hydrophobically modified saccharides of formula (I) and/or (II) are used as surfactants in accordance with the present invention may optionally further comprise one or more conventional
15 surfactants, co-surfactants and/or additives such as for example thickeners and rheology modifiers.

The hydrophobically modified saccharides of formula (I) and/or (II) are suitable as surfactants for the preparation of any kind of dispersions comprising
20 a continuous aqueous phase, typically for the preparation of dispersions in the field of cosmetics and health care, of food preparations, cutting oils, paintings, inks, crop protection, pesticides, insecticides and herbicides.

Since many cosmetic compositions are based on emulsion systems, there is
25 a great interest to formulate electrolyte-active materials into cosmetic emulsions. Examples 7, 9 and 11 indicate hydrophobically modified saccharides of formula (I) and/or (II) are suitable as surfactant for the preparation of such emulsion systems containing a high concentration of an electrolyte in the aqueous phase. Examples of cosmetic compositions of the emulsion type wherein, in accordance
30 with the present invention, hydrophobically modified saccharides are suitable as surfactant are, for example, creams, deodorants, antiperspirants, capillary treatment products, shampoos, health and personal care products containing electrolyte type moisturizing agents, and hair products containing cationic and/or amphoteric active materials.

35 Based on the tensio-active properties of the compounds of formula (I) and (II) defined above, the present invention also provides a method for the preparation of dispersions and/or for stabilising dispersions comprising an aqueous phase containing a high concentration of electrolytes, by including a
40 said compound or mixture of said compounds of formula (I) and/or (II) in the composition of the dispersion. The particular conditions, such as regarding the concentration of said surfactant(s), the ratio non-aqueous phase(s) / continuous

aqueous phase, and others, can be derived from the information provided above.

The dispersions can be prepared by conventional methods and techniques. The dispersions can for example be prepared by bringing together and
5 homogenising the composing phases of the multiphase system, with addition of one or more hydrophobically modified saccharides of general formula (I) and/or (II) defined above to the aqueous phase, to the non-aqueous phase(s) and/or to the composing phases of the multiphase system, so as to bring the non-continuous phase(s) in the form of finely divided particles (droplets, solid
10 particles and/ gas bubbles) dispersed in the continuous aqueous phase. The surfactant(s) of general formula (I) and/or (II) are typically added to the aqueous phase before the composing phases are mixed and homogenised to yield the dispersion.

A considerable advantage of the hydrophobically modified saccharides of
15 formula (I) and/or (II) is that they are very versatile compounds which can be engineered in view of particular dispersions and their application. This versatility results from the several parameters which define the structure of the molecule, namely the saccharide type and its degree of polymerisation, the kind of hydrophobic moiety and the average degree of substitution. Further
20 advantages of the hydrophobically modified saccharides of formula (I) and/or (II) reside in the fact that they are derived from saccharides from renewable resources, and that the products generally present good biodegradability and low toxicity, if any at all, towards humans, mammals, birds and fish.

CLAIMS

1. Use of a surfactant for the preparation of a dispersion of a multiphase system that comprises a continuous aqueous phase, characterised in that said aqueous phase contains one or more electrolytes at a total concentration ranging from the lower limit of 0.1 to 1 mole per litre aqueous phase, depending on the nature of the electrolyte(s) and the temperature of the dispersion, up to the limit of the solubility of the electrolyte(s) in water at 25°C, and that said surfactant is a hydrophobically modified saccharide which is a substituted polymeric saccharide of general formula (I) or (II)



wherein

[A]_n represents a fructan-type saccharide, with [A] representing a fructosyl unit or a terminal glucosyl unit and n representing the degree of polymerisation (DP) being the number of fructosyl and glucosyl units in said fructan-saccharide molecule,

[B]_m represents a starch-type saccharide, with [B] representing a glucosyl unit and m being the number of glucosyl units in said starch-type saccharide molecule, selected from the group consisting of modified starches and of starch hydrolysates with a dextrose equivalent (DE) ranging from 2 to 47,

(-M) represents a hydrophobic moiety that substitutes a hydrogen atom of a hydroxyl group of said fructosyl or glucosyl units, which is selected from the group consisting of an alkylcarbonyl radical of formula R-NH-CO- and an alkylcarbonyl radical of formula R-CO-, wherein R represents a linear or branched, saturated or unsaturated alkyl group with from 4 to 32 carbon atoms, and

s and s', which can have the same value or not, represent the number of said hydrophobic moieties that substitute the fructosyl or glucosyl unit, expressed as the average degree of substitution (av. DS) which ranges from 0.01 to 0.5, and

the total concentration of substituted polymeric saccharide of formula (I) and/or formula (II) ranges from 0.10 to 20 %, being % w/v on dispersed phase(s) in case of emulsions, % w/w on dispersed phase(s) in case of suspensions, and % w/v on aqueous phase in case of foams.

29 α

2. Use according to claim 1, wherein the multiphase system is selected from the group consisting of a biphase system and a triphase system, and the ratio non-aqueous phase(s) / aqueous phase ranges from 90 : 10 to 1 : 99, expressed as volume : volume ratio in case the non-aqueous phase(s) are liquid or gas phases, and as weight : volume ratio in case the non-aqueous phase(s) are solids.

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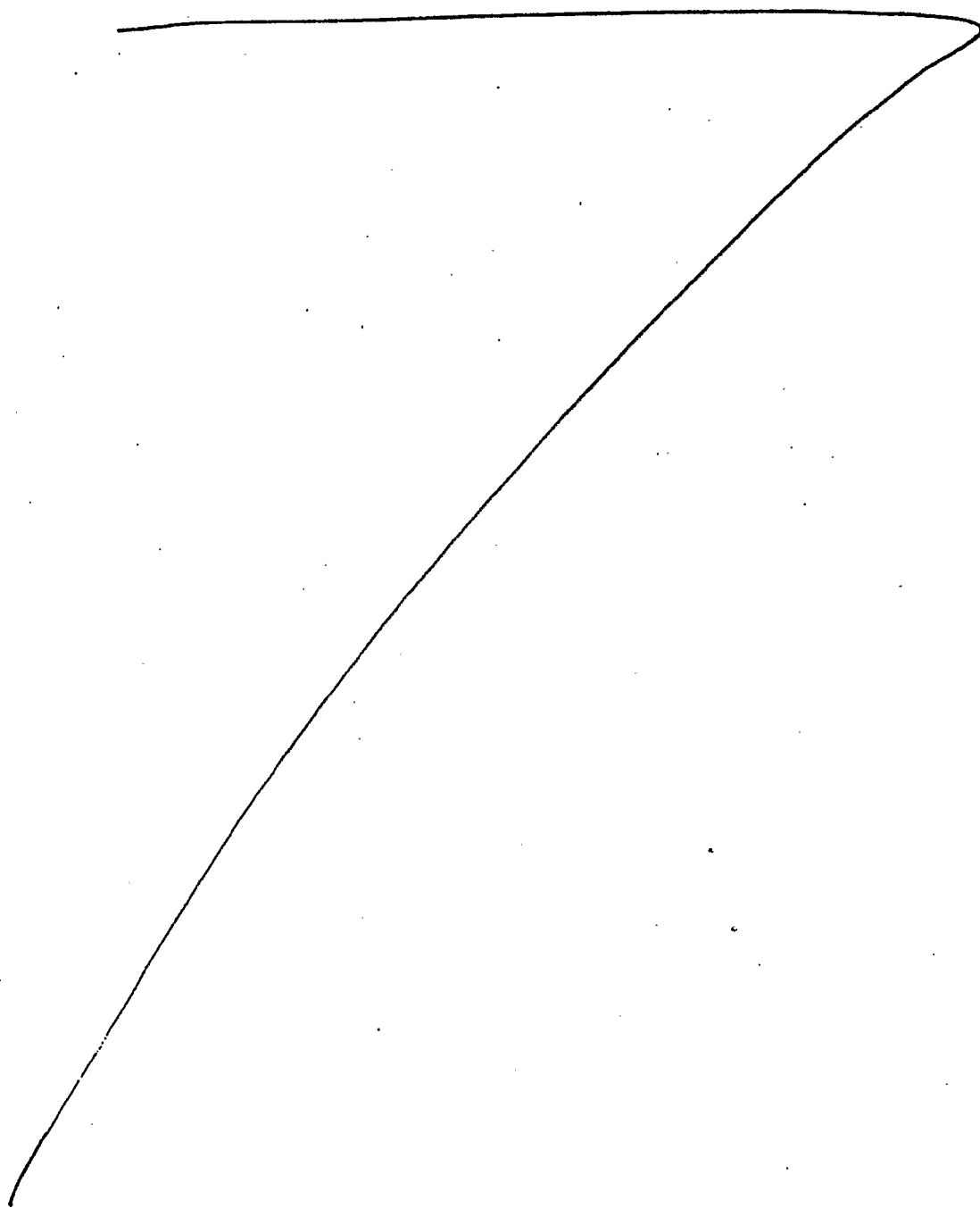
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3. Use according to claim 1, wherein the multiphase system is a biphasic system consisting of an oil phase/aqueous phase and the volume ratio non-aqueous phase(s) / aqueous phase ranges from 65 : 35 to 20 : 80.

5 4. Use according to any one of claims 1 to 3, wherein the substituted polymeric saccharide is of formula (I) defined in claim 1 and the fructan-type saccharide is selected from the group consisting of inulin, oligofructose, fructo-oligosaccharide, partially hydrolysed inulin, levan^{and} partially hydrolysed levan.

10 5. Use according to claim 4, wherein the fructan-type saccharide is selected from the group consisting of polydisperse inulin from plant origin and oligofructose, fructo-oligosaccharide and partially hydrolysed inulin with a degree of polymerisation (DP) ranging from 3 to 9.

15 6. Use according to any one of claims 1 to 3, wherein the substituted polymeric saccharide is of formula (II) defined in claim 1 and the starch-type saccharide is a starch hydrolysate with a dextrose equivalent (DE) ranging from 2 to 47.

20 7. Use according to any one of claims 1 to 6, wherein the hydrophobic moieties (-M) of the substituted polymeric saccharide of formula (I) or (II) as defined in claim 1 are all of the same nature, being alkylcarbamoyl radicals of formula R-NH-CO- wherein the alkyl radicals R can be the same or different and R has the meanings defined in claim 1.

25 8. Use according to any one of claims 1 to 6, wherein the hydrophobic moieties (-M) of the substituted polymeric saccharide of formula (I) or (II) as defined in claim 1 are all of the same nature, being alkylcarbonyl radicals of formula R-CO- wherein the alkyl radicals R can be the same or different and R has the meanings defined in claim 1.

30 9. Use according to claim 1, wherein the hydrophobic moieties (-M) of the substituted polymeric saccharide of formula (I) or (II) as defined in claim 1 are of a different nature being an alkylcarbamoyl radical of formula R-NH-CO- or an alkylcarbonyl radical of formula R-CO- , R having the meanings defined in claim 1 and wherein the alkyl radicals R are the same or are different.

10. Use according to claim 1 wherein the surfactant is composed of a mixture of two or more substituted polymeric saccharides of formula (I) and/or formula (II) as defined in any of the claims 7 to 9.

35 11. Use according to any one of claims 1 to 10 wherein the surfactant or mixture of surfactants is selected from the group consisting of compounds 1 to 31 indicated in the following table

Product n°	Formula (I) or (II)	Type	Hydrophobic Moiety		av. DS
			M	R-	
1	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.02
2	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.08
3	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.09
4	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.2
5	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.07
6	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.09
7	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
8	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
9	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
10	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.12
11	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.15
12	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.21
13	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.3
14	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₅ -	0.21
15	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.023
16	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.054
17	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₇ -	0.11
18	(I)	b	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.3
19	(I)	a	R-CO	CH ₃ (CH ₂) ₁₀ -	0.12
20	(I)	a	R-CO	CH ₃ (CH ₂) ₁₄ -	0.1
21	(I)	a	R-CO	CH ₃ (CH ₂) ₇ CH=C H-(CH ₂) ₇ -	0.05
22	(I)	a	R-CO	CH ₃ (CH ₂) ₁₆ -	0.11
23	(II)	d	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.05
24	(II)	e	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
25	(II)	c	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.1
26	(II)	d	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.18
27	(II)	d	R-CO	CH ₃ (CH ₂) ₁₀ -	0.1
28	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₇ -	0.11
29	(I)	a	R-NH-CO	CH ₃ (CH ₂) ₁₅ -	0.12
30	(I)	f	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.19
31	(I)	f	R-NH-CO	CH ₃ (CH ₂) ₁₁ -	0.13

Formula [A] n (-M) s (I) [B] m (-M) s' (II)

a = inulin, av. DP : 23

b = inulin, DP mainly between 2 and 8, av. DP : about 4.5

c = maltodextrin, DE 2

d = maltodextrin, DE 28

e = maltodextrin, DE 47

f = inulin, av. DP : 13

12. Use according to any one of claims 1 to 11, wherein the aqueous phase contains one or more electrolytes in a total concentration ranging from 0.5 moles/l to 5 moles/l.

13. Use according to claim 12, wherein the aqueous phase contains one or more electrolytes selected from the group consisting of metal salts, ammonium salts, amine salts, quaternary ammonium salts and salts of organic bases.

14. Use according to claim 13, wherein the salts are derived from hydrogen halides, sulphuric acid, phosphoric acid, carbonic acid and/or lactic acid and/or are salts providing hydroxide anions when dissociating.

2002362697 29 Jul 2008

15. Use according to any of claims 1 to 14 wherein the dispersion additionally comprises one or more conventional surfactants, co-surfactants, thickeners, rheology modifiers and/or conventional additives.
16. Method for the preparation of a dispersion and/ or for the stabilisation of a dispersion of a multiphase system that comprises a continuous aqueous phase containing one or more electrolytes at a total concentration ranging from the lower limit of 0.1 to 1 mole per litre, depending on the nature of the electrolyte(s) and the temperature of the dispersion, up to the limit of the solubility of the electrolyte(s) in water at 25°C, comprising bringing together and homogenising the composing phases of the multiphase system with addition of one or more hydrophobically modified saccharides of general formula (I) and/or (II) defined in claim 1 to the aqueous phase, or to the non-aqueous phase(s) or to the composing phases, whereby the total concentration of substituted polymeric saccharide or mixture of two or more substituted polymeric saccharides of formula (I) and/or formula (II) defined in claim 1 ranges from 0.1 to 20 %, being % w/v on dispersed phase(s) in case of emulsions, % w/w on dispersed phase(s) in case of suspensions, and % w/v on aqueous phase in case of foams, and optionally with addition of one or more conventional surfactants, co-surfactants and/or additives.
17. Dispersion of a multiphase system that comprises a continuous aqueous phase, characterised in that said aqueous phase contains one or more electrolytes at a total concentration ranging from the lower limit of 0.1 to 1 mole per litre aqueous phase, depending on the nature of the electrolyte(s) and the temperature of the dispersion, up to the limit of the solubility of the electrolyte(s) in water at 25°C, and that said dispersion comprises as surfactant one or more hydrophobically modified saccharides of general formula (I) or (II) defined in claim 1, whereby the total concentration of substituted polymeric saccharide or mixture of two or more substituted polymeric saccharides of formula (I) and/or formula (II) defined in claim 1 ranges from 0.1 to 20 %, being % w/v on dispersed phase(s) in case of

2002362697 29 Jul 2008

emulsions, % w/w on dispersed phase(s) in case of suspensions, and % w/v on aqueous phase in case of foams, and optionally further comprises one or more conventional surfactants, co-surfactants and/or additives.

18. Dispersion according to claim 17, wherein the multiphase system is a biphasic system and said biphasic system is an emulsion, a suspension or a foam.