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(54) Title: DIRECT COMPRESSIBLE DEXTROSE

(57) Abstract: This invention relates to a direct compressible dextrose composition, a process for preparing such a direct compressible dextrose composition by compression and subsequent granulation, and processes for preparing pharmaceutical formulations or food formulations in tablet form using the direct compressible dextrose composition. The invention further concerns pharmaceutical or food formulations, which comprise the directly compressible dextrose composition, and the use of the direct compressible dextrose composition for the preparation of pharmaceutical and food formulations.

Direct compressible dextrose

This invention relates to a direct compressible dextrose composition, a process for preparing such a direct compressible dextrose composition by compression and 5 subsequent granulation, and processes for preparing pharmaceutical formulations or food formulations in tablet form using the direct compressible dextrose composition. The invention further concerns pharmaceutical or food formulations, which comprise the direct compressible dextrose composition, and the use of the direct compressible dextrose composition for the preparation of pharmaceutical and food formulations.

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Compressed tablets represent the most popular pharmaceutical dosage form with about one-half of all prescriptions dispensed for compressed tablets. There are currently three basic methods of commercially preparing compressed tablets. These are direct compression, dry granulation followed by compression, and wet 15 granulation followed by drying and compression.

The direct compression method involves directly compacting a blend of active ingredient(s) and one or several inert materials, referred to as excipients, by means 20 of a tablet press. This method offers the advantage of only a few production steps but also has many technological limitations. For example, direct compression is only employable if a sufficiently homogeneous mix can be obtained by simple mixing, the flow property of the mix is satisfactory, and the ingredients of the mix allow for direct compression.

25 In cases where direct compression cannot be used due to the nature of the used active substances or other ingredients, which is often the case, a method called granulation is used. Granulation is a process in which primary powder particles are made to form larger entities called granules. The granulation allows to prevent segregation of the constituents of the powder mix, to improve the flow properties of 30 the powder mix, and to improve the compaction characteristics of the powder mix.

Granulation methods can be divided in two basic types, namely wet methods, which use a liquid in the process, and dry methods in which no liquid is used. Wet

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5 granulation is most often used and involves many steps, including: agglomerating of dry primary powder particles of active ingredients and excipients in the presence of a granulating fluid upon agitation using low-shear or high-shear mixers or fluidized beds, wet sieving to remove larger lumps, drying the granulation, and milling or sieving the dried granulation to achieve a granulation having the desired granule size distribution. The obtained granulation may subsequently be tabletted, capsulated or filled in sachets.

10 In dry granulation methods, the primary powder particles are aggregated under high pressure. In pharmacy, two methods are commonly used for dry granulation. Either a large tablet (known as a 'slug') is produced in a heavy-duty tablet press (a process known as 'slugging') or the powder is compacted between two rollers to produce so-called 'flakes' (a process known as 'roller compaction'). In both cases the 15 intermediate products are broken using a suitable milling technique to produce a granular material, which is usually sieved to separate the desired size fraction. The dry granulation method is particular useful for active ingredients that do not compress well after wet granulation, or those that are moisture sensitive or thermo labile.

20 For dry granulation two different apparatus are necessary: first, an apparatus for compacting the dry powders into compacts ('compactor'), and secondly an apparatus for crushing these compacts into granules ('granulator'). In commercially available roller compactors the process of roller compaction and granulation, i.e. the crushing 25 of the compacts into granules, are usually combined in a single compactor/granulator, commonly known as 'roller compactor'.

30 The compressed tablets produced by the above methods are usually composed of food ingredients (in the case of food-related compressed tablets) or one or more active ingredients (in the case of pharmaceutical compressed tablets) and several inert materials, referred to as excipients. The numerous tabletting excipients which are currently used for preparing tablets are generally classified according to their function, such as (i) diluents (also called bulking agents and fillers), e.g. lactose or sorbitol, which provide a quantity of material that can accurately be formed into a

5 compressed tablet, (ii) binders, e.g. methyl cellulose, which hold the ingredients together in the compressed tablet, (iii) lubricants, e.g. magnesium stearate or polyethylene glycol, which improve the release of the compressed tablet from the die and punches of the tablet press, and (iv) disintegrants, e.g. starch or cellulose, which help facilitate the break-up of the tablet when placed in a fluid environment, and (v) other substances, such as emulsifiers and surfactants.

10 As mentioned above, when direct compression methods are used, the choice of excipients is highly critical. In particular, the active ingredients and the excipients need to be 'direct compressible', i.e. needs to have good flow properties and the compaction characteristics required to produce strong tablets. Excipients that are suited for direct compression are well-known in the art and include, for example, various sugars, such as lactose and sucrose, and sugar alcohols, such as sorbitol and mannitol.

15 Dextrose (D-glucose) in powder form is one of the sugars which have been used as a diluent in tablets formed by direct compression methods. Three crystalline forms of dextrose are commonly described. These are (i) α dextrose monohydrate, which is traditionally produced by slow crystallisation, and by cooling supersaturated syrups 20 with a high glucose content originating from the hydrolysis of starch, (ii) anhydrous α dextrose, which is generally produced by dissolving crystals of α dextrose monohydrate in water at 60°C to 65°C, for example, in autoclaves under a high vacuum and under carefully controlled conditions, and (iii) anhydrous β dextrose, which is typically produced by a crystallization process at a high temperature.

25 The above-mentioned single crystal forms of dextrose, however, do not show sufficient compressibility. It is generally accepted that the preparation of a dextrose in powder form having sufficient compressibility properties and suitable to prepare tablets with desirable properties, requires the mixing of α dextrose monohydrate with 30 additives, such as maltose, maltodextrins or other polysaccharides with a higher degree of polymerisation (DP), or the production of mixed compositions of anhydrous α and β forms of dextrose, for example, by atomisation of a glucose syrup with a high dry matter content.

5 US 2005/020284 A1 discloses a pharmaceutical composition in the form of a chewable tablet for the suppression of gastric reflux comprising an alginic acid or salt thereof, a water-soluble carbonate radical precursor, a calcium salt, a first bulk sweetener, and a binding agent. In the process to render the calcium salt suitable for tabletting the calcium carbonate is granulated with a bulk sweetener which can be dextrose. The amount of bulk sweetener, however, is lower than 50% by weight.

10 US-A-4,072,535 teaches a free-flowing binder-disintegrant powder material consisting essentially of a precompacted-starch powder. According to this document, a dry granulation process may be utilized in preparing a direct compressible starch composition.

15 US 4,327,077 discloses that dextrose monohydrate can be used as a direct compaction vehicle in compressed chewable antacid tablets. In these antacid tablets the dextrose monohydrate acts as a binder for combined particles of recrystallized fatty material, such as chocolate, and an antacid. According to US 4,327,077, the used dextrose in the monohydrate form may be one of several mentioned, commercially available direct compressible dextrose preparations. These dextrose 20 preparations, however, are known to contain 5% to 6% of maltose, maltotriose and maltodextrins with a higher DP, and are generally obtained by atomisation of a glucose syrup with a dextrose equivalent (DE) in the range of 93% to 99%.

25 Further, US 2002/0122823 A1 describes a tablet capable of being chewed or disintegrated in the oral cavity, which comprises a pharmaceutically active ingredient, and a matrix comprising direct compressible dextrose monohydrate and sucralose, wherein the table is substantially fat free and the matrix is substantially free of non-saccharide, water soluble polymeric binders. The method of production of the used 'direct compressible dextrose monohydrate', however, is not disclosed. US 30 2002/0122823 A1 only describes that the direct compressible dextrose is a dextrose in the monohydrate form having an average particle size of 100 to 500 μm , wherein this average particle size is said to be required to impart the formulation with adequate flowability and compressibility.

Another dextrose preparation in powder form with high compressibility and high dextrose content and purity, which is suited for the production of tablets by direct compression, is known from US 6,451,122 B1. The dextrose described therein is an anhydrous dextrose characterized by a dextrose content of at least equal to 99%, an anhydrous α crystalline form content of at least equal to 95%, a water content of at most equal to 1%, a compressibility, determined by a test A, of at least equal to 80 N, and a mean diameter in the range of 150 μm to 200 μm . This powdered dextrose is prepared by a rather complicated process comprising subjecting a starting dextrose, i.e. a dextrose powder with a high dextrose content and of essentially the α form, which can be obtained by crystallisation or atomisation, to a dry granulation process using water or glucose syrup as a binder.

In view of the above, there is still a need for a dextrose composition exhibiting excellent flowability, friability and/or compressibility suited for use as an ingredient in pharmaceutical or food formulations that is obtainable in a simple, cost-efficient and reproducible manner.

This need is met by the provision of a direct compressible dextrose composition obtainable by the dry granulation process according to a first aspect of the invention. This process comprises the steps of (a) providing a starting dextrose composition in powder form, (b) compacting the starting dextrose composition by (i) roller compaction using compacting rolls to form flakes or (ii) slugging using a tablet press of single-punch or rotary type to form slugs, (c) crushing the flakes or the slugs obtained in step (b) to form granules, and (d) screening the granules to obtain a direct compressible dextrose composition in the form of granules with a given particle size distribution.

It was surprisingly found that compression of conventional, commercial available dextrose monohydrate by means of roller compaction or slugging followed by granulation leads to a dextrose granulation that is highly suitable for use in, for example, sachets and capsules, and for forming tablets. In particular, the direct compressible dextrose composition of the invention allows to produce tablets with

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higher tablet hardness compared to conventionally used dextrose. This in turn enables the incorporation of more active ingredient(s) while maintaining a certain tablet hardness. It also makes it possible to manufacture smaller and 'nicer' tablet sizes while still providing a particular and sufficient dosage of the active ingredient.

5 Furthermore, the direct compressible dextrose composition allows to prepare tablets having a certain hardness using a lower compression force. In addition, upon compressing the direct compressible dextrose composition into a tablet, no capping is observed. Finally, the friability of tablets produced using the direct compressible dextrose composition of the invention is lower and, thus, more resistant against 10 shipment and abrasion on handling.

The starting dextrose composition used in the context of the present invention comprises at least 50% by weight dextrose, preferably at least 60%, 70% or 80% by weight dextrose, more preferably at least 90% by weight dextrose, and even more 15 preferably 95% to 100% by weight dextrose. Most preferably the starting dextrose composition comprises at least 98%, at least 99%, or at least 99.5% by weight dextrose. The dextrose contained within the starting dextrose composition typically is α dextrose monohydrate, or a mixture of α dextrose monohydrate and anhydrous α dextrose, and/or anhydrous β dextrose provided that the moisture content of the 20 direct compressible dextrose composition is at least 2%, preferably 4%, more preferably 7%, or even between 7 to 12%, or up to 10 to 12%. Preferably, the dextrose is α dextrose monohydrate. According to the European Pharmacopoeia, dextrose monohydrate is containing between 7 to 9.5% water and to the US Pharmacopoeia between 7,5 to 9,5% water.

25 Substances, which may be included in the starting dextrose composition may, for example, comprise conventionally known excipients, such as diluents (bulking agents or fillers), binders, lubricants, disintegrants, and other compounds. For example, a lubricant, such as magnesium stearate and other related stearates, stearic acid, 30 polyethylene glycol, sodium stearyl fumarate, hydrogenated castor or vegetable oil, talc or mixtures thereof in a total amount of 0.01 to 10% by weight, based on the weight of the total composition, may be present. Examples of other excipients are well-known in the art and/or mentioned herein below.

According to the present invention, the additional ingredients, if present, are homogenously blended to provide a homogeneous starting dextrose composition, which is subsequently compacted. Any conventional mixer, such as a ribbon mixer, or 5 a blender, such as a twin shell blender, can be used for blending an ingredient mixture in powder form until a uniform mix is formed.

In a preferred embodiment of the invention, the step (b) of compacting the starting dextrose composition is carried out by roller compaction using at least two 10 compacting rolls to form so-called flakes (a type of compact). The two compacting rolls rotate in opposite directions to draw the starting dextrose composition into the gap between the compacting rolls. The pressure imparted enhances the bonding forces between the solid surfaces of the powder particles of the starting dextrose composition and leads to the formation of the flakes. The roll pressure, roll gap and 15 roll speed can readily be selected by a person skilled in the art to provide the desired characteristics of the flakes, such as strength and friability, and the desired properties of the granules obtained after crushing and screening the flakes, such as particle size distribution and flowability. The roll pressure, the most significant 20 parameter of roller compaction, is preferably in the range of 30 to 150 bar, in particular in the range of 40 to 120 bar, and particularly preferred in the range of 50 to 100 bar. A preferred roll gap is 0.5 to 5 mm, more preferably 0.5 to 3.0 mm and most preferably 1 to 2 mm. Suitable roll speeds to maintain a steady output of 25 material and to obtain flakes and granules, respectively, with the required properties are between 2 and 15 rpm, preferably between 3 and 10 rpm, particularly between 4 and 8 rpm.

The step of compacting the starting dextrose composition by roller compaction can be carried out by means of any commercially available roller compactor, having for 30 instance straight or profilated rollers, vertical, horizontal or diagonal arrangements of the rollers, a roller cooling system, and a feed system with single or multiple-auger operation, optionally designed with a vacuum system. A particularly suited compactor for use within the present invention is roller compactor type WP 120 V Pharma of Alexanderwerk. Other suitable compactors are well-known in the art and may be,

e.g., be obtained from Fitzpatrick Co. (United States), Vector Co. (United States), RIVA S.A. (Argentina), Freund Industrial Co. (United States), Gerteis AG (Germany), and Hutt GmbH (Germany).

5 As an alternative, the compression may also be carried out by a process called 'slugging' since it is well known that, under appropriate conditions, the slugging end product is largely the same as the one obtained by roller compaction. Slugging involves the compression of the starting dry dextrose composition into larger tablets or 'slugs' by means of a conventional tablet machine or, more usually, a specially 10 designed tablet press, for example a tablet press of single-punch or rotary type, in particular a large heavy-duty rotary press.

15 After compacting, the obtained flakes or slugs are crushed to form granules and subjected to screening to reduce in size. The granulation may occur in a single-stage or a multi-stage granulating process. In other words, the flakes or slugs may be first crushed into smaller particles called granules which are subsequently screened to obtain a direct compressible dextrose composition in the form of granules with a given particle size distribution, wherein the steps of crushing the flakes or slugs and screening the resulting granules can be repeated one or several times. Preferably, 20 the granulation of the flakes or slugs involves crushing and screening the flakes or slugs, followed by recrushing and rescreening the granules one or two times. The crushing may be carried out by using any conventional crusher, such as a pyramid, roller crusher, or, as typically used for crushing the flakes obtained in roller compaction, an oscillating mill. To crush the slugs, a hammer mill is particularly 25 suitable. For screening, a sieve or screen of a certain mesh size may be used. In the case of the flakes, an oscillating mill fitted with a screen is typically employed for crushing and screening. As mentioned above, many of the commercially available roller compactors contain an integrated granulation system for crushing and screening the flakes and, thus, are most conveniently used for the purpose of the 30 present invention.

Depending on the number of steps of crushing and sieving one or more screens having different mesh sizes, wherein the mesh size decreases from the initial or

upper screen to the terminal or lower screen, may be used. A skilled person is readily able to empirically identify appropriate mesh sizes of each of the used screens depending on the particular particle size distribution of the granules required for the intended purpose, such as the preparation of tablets or the use in sachets or capsules. In general, in order to obtain a direct compressible dextrose composition with highly suitable compression properties, a preferred mesh size of the terminal screen, which corresponds to the single screen used in a single-stage granulation process, is 0.1 to 1.8 mm, preferably 0.4 to 1.8 mm. For obtaining granules suited for sachets or capsules filings a terminal screen with a mesh size of 0.4 to 1.8 mm, preferably 0.5 to 1.5 mm, more preferably 0.7 to 1.5 mm, may be used. If the granules are to be compressed into tablets, the terminal screen preferably has a mesh size of 0.1 to 0.8 mm, more preferably 0.2 to 0.7 mm and most preferably 0.4 to 0.6 mm. If more than one screen is used, the initial or first screen preferably has a mesh size of 1.0 to 4.0 mm, preferably 1.0 to 3.0, in particular 2.0 to 3.0 mm.

Preferably, fines that were produced in the compating, crushing and/or screening steps are additionally separated by sieving. The fines may then be recirculated into the roller compactor for re-compression. Typically, particles below 100 µm are sieved out using sieves of a mesh size of 100 µm. This is to say, that, if the process includes the step of separating fines, the lower size limit of the granules is determined by the mesh size of the sieve used for sieving out the fines, and the upper size limit of the granule is determined by the mesh size of the above-mentioned terminal sieve.

The direct compressible dextrose composition obtained by the process according to the first aspect of the invention together with one or more active ingredients and, optionally, one or more additional substances may then be encapsulated to form capsules in a known manner, such as by using a conventional encapsulating machine, or filled into sachets. In particular, the direct compressible dextrose composition of the invention may be formed into tablets by direct compression using a tablet press as further explained below.

In a second aspect, the present invention concerns a direct compression process for preparing a pharmaceutical formulation in tablet form. This process comprises the

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steps of (a) providing a direct compressible dextrose composition by carrying out the process according to the first aspect of the invention, (b) blending the direct compressible dextrose composition with one or more active ingredients to obtain a blend, and (c) compressing the blend into a tablet form.

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For compressing the blend into a tablet form any known tablet presses may be used, such as single-station presses, multi-station rotary presses or eccentric presses. Preferably, a rotary tablet press is used, which continuously rotates as part of a die table from the filling position to a compaction position. The particles are compacted between an upper punch and a lower punch to an ejection position, at which the 10 resulting tablet is pushed from the die cavity by the lower punch.

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The term "active ingredient", as used herein, refers to any chemical compound or composition having a pharmaceutical effect, in particular a therapeutic or 15 prophylactic effect, and, thus, may encompass, e.g. analgesics, decongestants, expectorants, antihistamines, antitussives, antacids, gastric protectants, diuretics, bronchial dilators, sleep-aids, vitamins, laxatives, antibiotics, antispasmolytics, and the like.

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Optionally, the direct compressible dextrose composition is additionally blended with one or more excipients well-known in the art, such as diluents (also called bulking agents or fillers) to provide a quantity of material which can be formed accurately 25 into a compressed tablet, binders to further increase the cohesive properties of the direct compressible dextrose composition, lubricants to further prevent sticking the compressed tablet to the die and punches of the tablet press, disintegrants to facilitate the break-up or disintegration of the compressed tablet after administration, and other compounds, such as preservatives, flavours, antioxidants, surfactants, emulsifiers, and coloring agents. Examples of diluents include lactose, mannitol, sorbitol, microcrystalline cellulose, ethyl cellulose, xylitol, starch, starch derivatives, 30 fructose, calcium carbonate, calcium phosphate, sodium calcium phosphate, and sucrose. Typical binders include hydroxy-propylcellulose, methylcellulose, starch, polyvinylpyrrolidone, hydroxypropylmethylcellulose, gelatin, glycerol, and mixtures thereof. Suitable disintegrants include modified or unmodified starches, clays, cross-

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linked polyvinylpyrrolidone, modified or unmodified celluloses, gums or alginates. Examples for the lubricants include magnesium stearate and other related stearates, stearic acid, sodium stearyl fumarate, hydrogenated castor or vegetable oil, talc, and polyethylene glycol.

5 The active ingredient(s) and the excipient(s) may constitute up to 80% by weight of the blend, preferably up to 50% of the blend. The active ingredient may constitute 1 to 80% by weight, preferably 1 to 50% by weight, and the one or more excipients may constitute 0 to 79% by weight, preferably 0 to 49% by weight of the blend. The 10 appropriate effective amount of the particular active ingredient(s) depends on the desired therapeutic response upon administration and can be readily determined by a person skilled in the art considering the bioavailability of the active ingredient, the dosage scheme, the age, sex and weight of the patient, and other factors, as known in the art. The excipient(s) are usually neither required to be present in such high 15 amounts of up to 79% by weight nor 49% by weight due to the excellent properties of the blend, such as compressibility, flowability and friability, imparted by the used direct compressible dextrose composition of the invention. Thus, the amount of the one or more excipient is preferably 40%, 30%, 20%, more preferably 10% or less and most preferably 0 to 5% by weight of the blend.

20 After having compressed the blend into the form of a tablet, the obtained tablet may be provided with a coat, in particular, if the active ingredient has an objectionable taste. Techniques for tablet coating, such as sugar coating and film coating, are well-known in the art.

25 The term "tablet form", as used herein, includes any tablet, in particular tablets in any form, shape and of any physical, chemical or sensory property, and tablets for any route of administration, indication and application. The tablets produced according to the invention may be, for example, tablets to be sucked, chewed, 30 dissolved or swallowed. Preferably, the tablet is a chewable tablet. A chewable tablet according to the present invention is a soft tablet where chewing helps to break the tablet particles and release the active ingredient in the mouth before swallowing. A chewable tablet dosage form can be a soft pill, tablet, gum and more recently "chewy

squares". The tablet hardness and friability are highly important properties of a chewable tablet comprising active ingredient(s) and having desirable chewability properties. The direct compressible dextrose is particularly suited to meet these needs.

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In a third aspect, the present invention relates to a direct compression process for preparing a food formulation in tablet form. The process comprises the steps of (a) providing a direct compressible dextrose composition by carrying out the process according to the first aspect of the invention, (b) blending the direct compressible dextrose composition with one or more food ingredients to obtain a blend, and (c) compressing the blend into a tablet form.

The term "food ingredient", as used herein, refers to any chemical compound or composition which is intended for use in food for humans or animals. Preferably, the food ingredient is for human consumption and approved by the Food and Drug Administration (FDA). The food ingredients for use herein comprise, for example, food supplements, confectioner's sugar, sorbitol, mannitol, starch, starch derivatives, hydrogenated starch hydrolysate, isomalt, isomaltulose, polydextrose or other known sweet materials, and other substances, such as flavours, colorants, preservatives, 15 antioxidants, emulsifiers, and the like.

Preferably, the blend comprises at least 20% by weight of the direct compressible dextrose composition, in particular at least 50%, 60%, 70%, 80% or 90% by weight. The one or more food ingredient may be present in the blend in a total amount of 1 25 to 80% by weight, in particular 1 to 50% by weight. Preferably, the lower limit of the total amount of the one or more food ingredient is 5%, 10%, 20% or 30% by weight of the blend. The upper limit is preferably 10%, 20%, 30% or 40% by weight of the blend. The amount of the above-mentioned other substances falling within the definition of a food ingredient in the sense of the present invention, is less than 30 10%, preferably less than 5%, more preferably less than 2% by weight, based on the weight of the blend.

In a fourth aspect of the present invention, there is provided a process for preparing a pharmaceutical formulation in tablet form by dry granulation followed by compression. This process comprises the steps of (a) providing a direct compressible dextrose composition by carrying out the process according to the first aspect of the invention, wherein the starting dextrose composition used in the process according to the first aspect of the invention comprises at least 50% by weight dextrose, 1 to 50% by weight of an active ingredient and 0 to 49% by weight of one or more excipients, and (b) compressing the direct compressible dextrose composition into a tablet form.

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The active ingredient(s) and the excipient(s) comprised within the starting dextrose composition are as defined herein in connection with the process of the second aspect of the invention. The appropriate effective amount for a particular active ingredient depends on several factors, as described hereinbefore, and can be readily determined by a person skilled in the art. Preferably, the amount of the one or more excipient is 40% or less, more preferably 30% or less, yet more preferably 20% or less, even more preferably 10% or less and most preferably 0 to 5% by weight of the total weight of the starting dextrose composition.

20 According to a variation of the process of the fourth aspect of the invention, the direct compressible dextrose composition may be blended with one or more excipients prior to tabletting. Specific examples of optionally used excipients are mentioned herein above. The excipient(s) are preferably added in an amount of less or equal to 40%, 30%, 20%, more preferably less or equal to 10% and most preferably 0 to 5% by weight of the total weight of the blend to be compressed into a tablet form.

25 A fifth aspect of the present invention relates to a direct compressible dextrose composition. The compressible dextrose composition comprises at least 95% by weight dextrose and has a moisture content of at least 2%, preferably at least 7%, and more preferably up to 12% (by weight; water). Thus, the dextrose composition may have a moisture content in the range of preferably 7 to 12%. In contrast to the prior art, the present invention utilizes as the starting material a composition

comprising dextrose monohydrate or mixtures thereof containing a significant portion of dextrose monohydrate (preferably above 50% dextrose monohydrate). In a preferred embodiment, the dextrose is a dextrose monohydrate. Typically, such compressible dextrose composition is obtainable by the dry granulation process 5 according to the first aspect of the invention. The direct compressible dextrose composition of the invention has a favourable dissolution profile and a high flowability, rendering it highly suitable for use in sachets or as capsule fillings. Further, the direct compressible dextrose composition of the invention exhibits an increased bulk density and an improved flow and, thus, provides relatively consistent 10 granulation fill volumes for encapsulation. Moreover, the direct compressible dextrose composition has a high compressibility and, thus, is particularly suited for tabletting.

The direct compressible dextrose composition preferably has a volume mean diameter, reference to ISO 9276 part II, of 100 to 800 μm . For tablet applications, 15 the volume mean diameter is preferably in the range of 150 to 300 μm , more preferably in the range of 200 to 250 μm . Such a particle size is suitable to impart the composition with adequate flowability and compressibility. For sachet or capsule applications, the volume mean diameter is larger, e.g. in the range of 300 to 700 μm . Further, the direct compressible dextrose composition of the invention has preferably 20 a Hausner ratio, an indicator for the flowability which corresponds to the ratio of tapped density to bulk density, of 1.00 to 1.25, typically 1.03 to 1.20, in particular 1.05 to 1.20. The Hausner ratio is determined as described in the example given below.

25 A direct compressible dextrose composition of the invention comprising at least 95%, preferably at least 98%, at least 99%, at least 99.5%, or 100% by weight dextrose and being sieved through a sieve with a mesh size of 500 μm , is characterized by any one of the following parameters: a bulk density of 550 to 750 g/l, preferably 600 to 700 g/l, more preferably 630 to 670 g/l, a tapped density of 700 to 800 g/l, 30 preferably 740 to 780 g/l, a compressibility index of 11 to 17%, preferably 13.0 to 15.5%, and a Hausner ratio of 1.12 to 1.22, preferably 1.14 to 1.20. Further, a tablet prepared from such a direct compressible dextrose composition has a tensile strength at a compression force of 10.0 kN of 0.5 to 2.5 N/mm², preferably 1.0 to 2.0 N/mm²,

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a tensile strength at a compression force of 20.0 kN of 1.5 to 4.0 N/mm², preferably 2.0 to 3.5 N/mm², a tensile strength at a compression force of 30.0 kN of 2.5 to 5.0 N/mm², preferably 3.0 to 4.5 N/mm², and/or a friability of below 1% at compression forces of 20 kN or higher, more preferably a friability of below 1% at compression forces of 10 kN or higher. All these parameters are determined as described in the example as given below.

A sixth aspect of the present invention concerns to a pharmaceutical formulation comprising the direct compressible dextrose composition according to the fifth aspect of the invention.

The pharmaceutical formulation contains the direct compressible dextrose composition of the invention, one or more active ingredients, and optionally one or more excipients. Preferably, the pharmaceutical formulation is in the form of solid dosage forms, such as capsules, tablets, sachets, pills, lozenges, and the like.

Capsules, which contain the granular direct compressible dextrose composition of the invention, include any capsules known in the art, such as gelatine capsules. Methods for encapsulating the direct compressible dextrose composition of the invention are well-known in the art and include, for example, the encapsulation using a Höfliner and Kary or a Bosel GKF encapsulator. The granular direct compressible dextrose composition of the invention may be filled into the body of the capsule dosage form by tamping or dosing and the capsule may be subsequently sealed using a cap.

The tablets are defined as described hereinbefore in connection with the second aspect of the invention. Preferred tablets are chewable tablets. Preferred values for tensile strength and friability are as described above in connection with the fifth aspect of the invention. The hardness of the resulting tablets is strongly influenced by the compression pressure employed. Thus, where it has been desired to produce a softer tablet, the compression pressure is reduced.

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Sachets represent a further preferable form of the pharmaceutical formulation, which contains a powder of the direct compressible dextrose composition, the active ingredient(s) and, optionally, the one or more additional ingredients.

5 A seventh aspect of the present invention relates to a food formulation, which comprises the direct compressible dextrose composition according to the fifth aspect of the invention.

10 Preferably, the food formulation is a chewable food formulation. A chewable food formulation is a formulation where chewing helps to break up the food formulation and to release single constituents contained herein before swallowing. The food formulation preferably present in the form of tablets, lozenges, lollipops and the like. Preferably, the tablet is a confectionary tablet. Further, the tablet is preferably a 15 chewable tablet as defined herein above. Particularly preferred for use within the present invention is a chewable confectionary tablet. An example thereof is a chocolate based tablet.

20 A last aspect of the present invention concerns the use of a direct compressible dextrose composition according to the fifth aspect of the invention for preparing a pharmaceutical composition or a food formulation, respectively, wherein the pharmaceutical composition and the food formulation are preferably present in a form as defined in connection with the sixth and seventh aspect of the invention.

25 The present invention will now be further described by the following figures and examples.

FIGURES

30 Fig. 1 shows microscopic pictures of pure dextrose before RC (upper picture) and of dextrose after RC (<500 µm) (lower picture).

Fig. 2 is a diagram showing the compression profile of tablets of pure dextrose before RC (●) and RC dextrose (<500 µm) (■).

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Fig. 3 is a diagram showing the friability as a function of compression force of tablets of pure dextrose before RC (●) and RC dextrose (< 500 µm) (■). The horizontal solid line denotes the friability limit according to Ph. Eur. V, USP 29/NF 24.

5

EXAMPLE

In the following example pure dextrose and a blend of dextrose with vitamin C were subjected to roller compaction (RC) followed by granulation, and the resulting RC granules were compared with non roller compacted pure dextrose in terms of particle size distribution, structure, density and flowability. Further, compressed tablets were prepared from these formulations and compared with each other in terms of hardness and friability.

15 The obtained results show that the roller compaction of both pure dextrose and the blend of dextrose with vitamin C results in granules having an improved flowability and a higher compressibility compared to dextrose before RC. Tablets prepared from these granules showed a significantly increased hardness, and an improved and low friability, and no capping was observed.

20

1. Experimental procedures

1.1 Materials

25 a) Raw materials

The following raw materials were used:

- 1) C*PharmDex 02011 (pharma-grade α dextrose monohydrate, available from Cargill)
- 30 2) Fine grade vitamin C (not compressible, available from BASF)

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b) Sample dextrose compositions

The following sample dextrose compositions were provided:

5 1) Pure dextrose (C*PharmDex 02011)
2) 70 wt.% dextrose (C*PharmDex 02011) + 30 wt.% vitamin C

1.2 Preparation of granules and tablets

10 A roller compactor type WP 120 V Pharma of Alexanderwerk was used for roller compacting the sample dextrose compositions. This roller compactor was fitted with a horizontal feed screw system with vacuum station, vertically positioned rollers, and an integrated, two-stage rotor fine granulator unit.

15 The powdered sample dextrose compositions were fed to the vertically positioned compacting rolls by the screw feeder and the vacuum of the horizontal feed system to form flakes of a certain size. These flakes were transferred to a two-stage granulating system consisting of an upper and lower sieve, respectively, to form granules. In order to obtain a desired particle size distribution of the obtained granules, the size of the sieves was adapted as described in the following.

20 An upper sieve having a mesh size of 2.5 mm was used in all experiments and a lower sieve having a mesh size of 1.6 mm and 0.8 mm, respectively, was used to produce granules intended for use in sachets or capsules. To produce granules suited for preparing compressed tablets, a lower sieve having a mesh size of 1.0 mm or 0.8 mm was used. Prior to tabletting these granules, an additional granulation step using a granulator type AR 400 E of Erweka GmbH (Germany) fitted with a sieve of 500 µm was performed to obtain size-reduced granules which are highly suited for the production of tablets.

30 After final granulation of the powdered sample dextrose compositions and prior to determining the granule properties, the amount of fines was decreased as much as

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possible using a sieve of 100 µm, fitted on a 'Fritsch' Vibratory sieve shaker, for 10 minutes at amplitude 2 mm.

The parameters used for compaction and granulation are shown in Table 1 (Dextr. = dextrose; SF-SP = screw feeder speed; CR-SP = compacting roll speed; HPR = hydraulic pressure; FSIZE = flake size; GR-SP = granulating system speed; MS-US = mesh size of upper sieve; MS-LS = mesh size of lower sieve).

Table 1. Roller compaction and granulation conditions

10

	Roller compaction				Granulation		
	SF-SP (rpm)	CR-SP (rpm)	HPR (bar)	FSIZE (mm)	GR-SP (rpm)	MS-US (mm)	MS-LS (mm)
Dextr. (for granules)	50	5	100	2	60	2.5	1.6/0.8*
Dextr. (for tablets)	50	5	50	3	60	2.5	1.0
Dextr. + Vit. C	35	7.5	75	1	60	2.5	0.8

* granules to be used e.g. in sachets or capsules

The obtained granules were then compressed into tablets using a triple punch rotary press type PH 100 – PMA 3 of Korsch GmbH (Germany). The produced tablets were round, flat-faced and had a surface of 1 cm² and a weight of 350 mg.

1.3 Methods for evaluating granule and tablet properties

The granules were characterized by their size distribution, microscopic structure, density and flowability. The following measurement methods were employed.

Size distribution. Size distribution was determined according to the European Pharmacopoeia V Test method 2.9.31 using a laser light particle sizer, type Helos KF – Rodos T4.1, of Sympatec GmbH (Germany). The particle size was analysed by laser light diffraction.

25

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Structure. A Zeiss microscope at magnification 10X was used to take microscopic pictures of pure dextrose before and after roller compaction.

5 Bulk density. Bulk density was measured according to the European Pharmacopoeia V Test method 2.9.15 - *Apparent Volume*.

Tapped density. Tapped density was determined according to the European Pharmacopoeia V Test method 2.9.15 - *Apparent volume*, using a Stampfvolumeter, model STAV2003, of JEL AG (Germany).

10 Flowability. Flowability was measured according to the European Pharmacopoeia V Test method 2.9.36 Powder flow – *Compressibility index or Hausner ratio*.

15 The tablets were characterized by their hardness and friability. For each compression force, 20 tablets for hardness and 19 tablets for friability were analyzed and mean values were calculated. The following measuring methods were employed.

20 Hardness. Hardness, i.e. the diametral crushing strength, was determined using a conventional pharmaceutical hardness tester (hardness tester model TBH – WS 50, available from Erweka GmbH (Germany)). In order to compare values across different size tablets, the breaking strength was normalized for the area of the break. The normalized value, expressed as N/mm², is herein referred to as tensile strength (Ts) and calculated as follows:

$$Ts = 2H/\pi TD,$$

25 wherein H is the hardness, T the thickness and D the diameter of the tablet. For each compression force, 20 tablets were analyzed on hardness (H), thickness (T) and diameter (D).

30 Friability. Friability measurements were determined according to the European Pharmacopoeia V Test method 2.9.7 *Friability of uncoated tablets*.

2. Results

2.1 Granule properties

5 a) Particle size distribution

The pure dextrose before RC had a volume mean diameter of 176 μm . In contrast, the dextrose to be used for the production of tablets, which was sieved through a 500 μm sieve (RC dextrose (<500 μm)), exhibited an increased volume mean diameter of 227 μm . The RC dextrose sieved through a 0.8 mm or 1.6 mm sieve as 10 final granulation (RC dextrose (< 1600 μm) and RC dextrose (< 800 μm)), intended for use in sachets or capsules, exhibited volume mean diameters of 602 μm and 402 μm , respectively.

15 The addition of 30 wt.% vitamin C to the pure dextrose, followed by RC and sieving using a sieve of 800 μm (70 wt.% dextrose + 30 wt.% vitamin C (< 800 μm)) leads to a quite similar particle size distribution compared to RC dextrose (< 800 μm). A similar result was obtained for the same RC sample dextrose compositions which, however, had been sieved through a sieve of 0.5 mm as a final granulation instead of 20 a 0.8 mm sieve.

b) Structure

25 As evident from the microscopic pictures shown in Fig. 1, roller compaction leads to a significantly changed structure of the dextrose before (upper microscopic picture) and after (lower microscopic picture) roller compaction and sieving through a sieve of 500 μm in terms of surface, volume, shape and size. The substantially altered structure influences both the properties of the granules obtained after RC and the tablets made thereof.

30 c) Density and flowability

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The bulk density, tapped density, compressibility index and Hausner ratio were determined for RC dextrose, sieved through sieves of 1.6 mm, 0.8 mm and 0.5 mm, and for 30 wt. % vitamin C formulated dextrose sample compositions, sieved through sieves of 0.8 mm and 0.5 mm, respectively. The results are shown in Table 2 below.

5

Table 2. Density and flowability properties of sample dextrose compositions before and after RC

	Bulk density (g/l)	Tapped density (g/l)	Compr. Index (%)	Hausner ratio	Scale of Flowability
PURE DEXTROSE					
After RC (<1.6 mm)	819	853	4	1.04	Excellent
After RC (<800 µm)	709	804	12	1.13	Good
After RC (<500 µm)	650	761	15	1.17	Good
Before RC	553	690	20	1.25	Fair
FORMULATED DEXTROSE					
After RC of 70 wt.% dextr. + 30 wt.% Vit. C (<800 µm)	747	823	9	1.10	Excellent
After RC of 70 wt.% dextr. + 30 wt.% Vit. C (<500 µm)	728	823	12	1.13	Good

10 It was found that the roller compaction of pure dextrose leads to a strong increase of the bulk density and the tapped density. Both the compressibility index and the Hausner ratio are found to be significantly lowered compared to pure dextrose before RC. Low values of compressibility index and Hausner ratio are indicative for a good flowability. In agreement with these findings, the flowability of the RC dextrose was found to be improved compared to the starting dextrose. Further, it was found that the smaller the particle size of the granules, the lower the density and flowability. Similar results were obtained for the dextrose vitamin C formulated granules.

15

2.2 Tablet properties

a) Hardness

5 The compression profile, i.e. the tensile strength as a function of compression force, of tablets made of RC dextrose (<500 µm) was found to be much higher than the compression profile of tablets made of non RC dextrose (Fig. 2).

10 The dextrose tablets, before RC, started to show capping (a tablet defect), which results in a lot of 'incorrect' tablets, at compression forces of 15 kN and higher, and therefore exhibited a decreased tablet hardness. The RC dextrose (<500 µm) did not show this capping and less off-tablets will be produced. The tensile strength of the tablets made of RC dextrose is at least twice that of the tablets made of non RC dextrose. Thus, the RC dextrose powder according to the present invention, is a 15 direct compressible dextrose powder having a higher compressibility than the starting dextrose powder before RC. Similar results were found for tablets made of RC 70 wt.% dextrose + 30 wt.% vitamin C (<500 µm) (results not shown).

b) Friability

20 Fig. 3 shows the results of the friability measurements of tablets prepared of non RC dextrose and RC dextrose. The RC dextrose tablets show good friability values at compression forces of around 15 kN or higher. According to the European Pharmacopoeia V the friability of uncoated 350 mg tablets should be below 1%. At 25 compression forces of around 15 kN or higher, the friability of the tablets is below the 1% limit and, thus, complies with the pharmacopoeia. In contrast, the tablets made of non RC dextrose did not go below the 1% limit. In fact, even at compression forces of around 15 kN and higher, no friability values of the tablets could be measured, since the tablets broke up after the friability test. Thus, the 30 friability of tablets produced using the RC dextrose is lower and, thus, more resistant against shipment and abrasion on handling.

Claims

5 1. A dry granulation process for preparing a direct compressible dextrose composition, comprising:

providing a starting dextrose composition in powder form, wherein the starting dextrose composition comprises 50 to 100% by weight dextrose;

10 compacting the starting dextrose composition by roller compaction using compacting rolls to form flakes or by slugging using a tablet press of single-punch or rotary type to form slugs;

15 crushing the flakes or the slugs to form granules; and

screening the granules to obtain a direct compressible dextrose composition in the form of granules with a given particle size distribution.

20 2. The dry granulation process of claim 1, wherein the roll pressure is in the range of 30 to 150 bar.

3. The dry granulation process of claim 1 or 2, wherein the roll gap is in the range of 0.5 to 5 mm.

25 4. The dry granulation process of any one of claims 1 to 3, wherein the granules are sieved through one or more sieves, with the terminal sieve having a mesh size of 0.1 to 1.8 mm.

30 5. The dry granulation process of claim 4, wherein the granules are sieved through an initial sieve having a mesh size of 1.0 to 3.0 mm.

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6. A direct compression process for preparing a pharmaceutical formulation in tablet form, comprising:

5 providing a direct compressible dextrose composition by carrying out the process of any one of claims 1 to 5;

10 blending the direct compressible dextrose composition with one or more active ingredients to obtain a blend; and

15 compressing the blend into a tablet form.

7. The direct compression process of claim 6, wherein the direct compressible dextrose composition is additionally blended with one or more excipients.

15 8. The direct compression process of claim 6 or 7, wherein the blend comprises at least 20% by weight of the direct compressible dextrose composition.

20 9. A direct compression process for preparing a food formulation in tablet form, comprising:

25 providing a direct compressible dextrose composition by carrying out the process of any one of claims 1 to 5;

blending the direct compressible dextrose composition with one or more food ingredients to obtain a blend; and

compressing the blend into a tablet form.

30 10. The direct compression process of claim 9, wherein the blend comprises at least 20% by weight of the direct compressible dextrose composition.

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11. A process for preparing a pharmaceutical formulation in tablet form by dry granulation followed by compression, comprising:

5 providing a direct compressible dextrose composition by carrying out the process of any one of claims 1 to 5, wherein the starting dextrose composition comprises at least 20% by weight dextrose, 1 to 80% by weight of an active ingredient and 0 to 79% by weight of one or more excipients;

10 compressing the direct compressible dextrose composition into a tablet form.

12. The process of claim 11, further comprising the step of blending the direct compressible dextrose composition with one or more excipients.

15 13. A direct compressible dextrose composition comprising at least 95% by weight dextrose, a moisture content of at least 2%, preferably at least 7%, more preferably up to 12%.

20 14. A direct compressible dextrose composition according to claim 13 characterized in that it is having a bulk density of 550 to 750 g/L.

15. A direct compressible dextrose composition according to claim 13 or 14 characterized in that it is having a compressibility index of 11 to 17%.

25 16. A pharmaceutical formulation comprising the direct compressible dextrose composition according to anyone of claims 13 to 15.

17. The pharmaceutical formulation of claim 16, wherein the pharmaceutical formulation is a solid dosage form.

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18. A tablet comprising the direct compressible dextrose composition according to anyone of claims 13 to 15 and characterized in that it is having a tensile strength at a compression force of 20.0 kN of 1.5 to 4.0 N/mm².

5 19. A food formulation comprising the direct compressible dextrose composition according to anyone of claims 13 to 15.

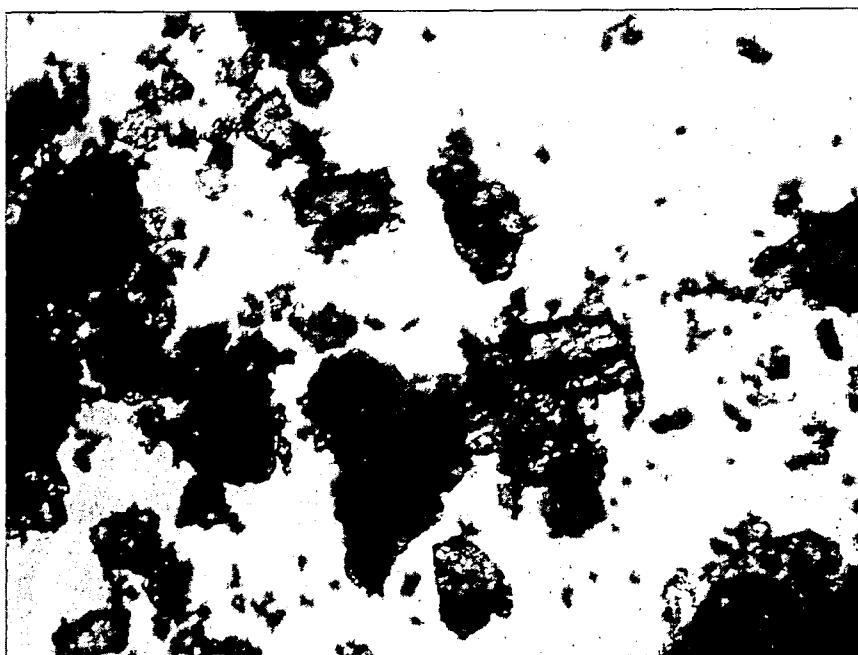
20. The food formulation of claim 19, wherein the food formulation is in the form of tablets, lozenges and lollipops.

10 21. Use of a direct compressible dextrose composition according to anyone of claims 13 to 15 for preparing a pharmaceutical formulation.

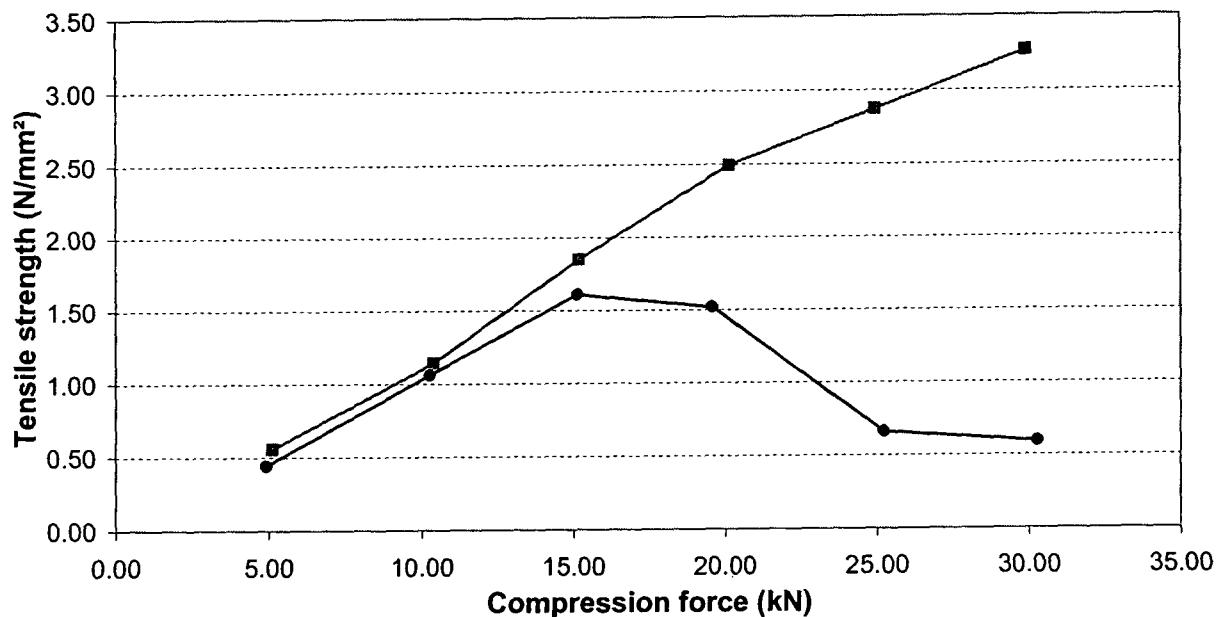
15 22. Use of a directly compressible dextrose composition according to anyone of claims 13 to 15 for preparing a food formulation.

1/3

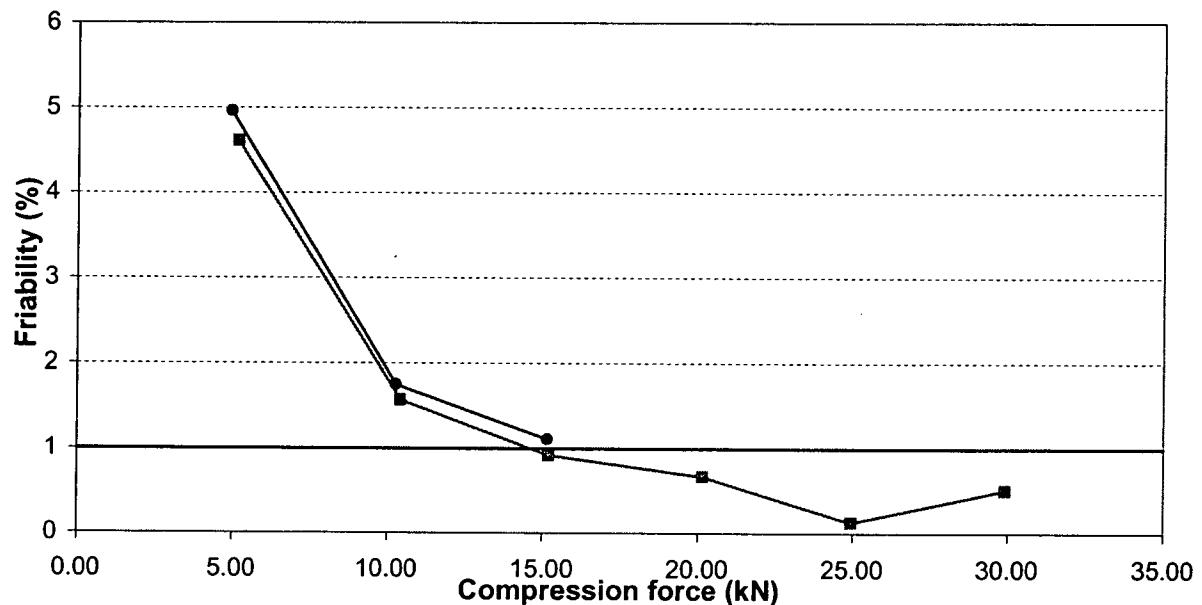
Fig. 1



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Fig. 2

3/3

Fig. 3

INTERNATIONAL SEARCH REPORT

International application No

PCT/EP2008/006283

A. CLASSIFICATION OF SUBJECT MATTER
INV. A23G3/34 A61K9/20 A23G3/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
A23G A23L C13K A61K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, FSTA, EMBASE, BIOSIS

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 2005/202084 A1 (ADUSUMILLI PRASAD [US] ET AL) 15 September 2005 (2005-09-15) paragraph [0048] – paragraph [0059]; claims -----	1-12
A	US 4 072 535 A (SHORT ROLLAND W P ET AL) 7 February 1978 (1978-02-07) column 17 – column 18 -----	1-12
X	US 2003/005923 A1 (MORALY FRANCK [FR] ET AL) 9 January 2003 (2003-01-09) claims examples tables paragraphs [0003], [0024], [0060], [0079] ----- -/-	13-22

Further documents are listed in the continuation of Box C.

See patent family annex.

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- *A* document defining the general state of the art which is not considered to be of particular relevance
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X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

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Date of the actual completion of the international search	Date of mailing of the international search report
19 December 2008	30/12/2008
Name and mailing address of the ISA/ European Patent Office, P.B. 5818 Patentlaan 2 NL – 2280 HV Rijswijk Tel. (+31-70) 340-2040, Fax: (+31-70) 340-3016	Authorized officer Bondar, Daniela

INTERNATIONAL SEARCH REPORT

International application No
PCT/EP2008/006283

C(Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 6 451 122 B1 (MORALY FRANCK [FR] ET AL) 17 September 2002 (2002-09-17) cited in the application claims examples tables page 3, lines 53-64 page 6, lines 51-61 -----	13-22
X	EP 1 108 792 A (ROQUETTE FRERES [FR]) 20 June 2001 (2001-06-20) claims examples paragraphs [0003], [0004] - [0020] -----	13-22

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/EP2008/006283

Patent document cited in search report		Publication date	Patent family member(s)		Publication date
US 2005202084	A1	15-09-2005	NONE		
US 4072535	A	07-02-1978	NONE		
US 2003005923	A1	09-01-2003	NONE		
US 6451122	B1	17-09-2002	AT 262596 T	15-04-2004	
			CA 2296193 A1	24-06-2000	
			DE 69915785 D1	29-04-2004	
			DE 69915785 T2	02-12-2004	
			EP 1013777 A1	28-06-2000	
			ES 2217712 T3	01-11-2004	
			FR 2787811 A1	30-06-2000	
			JP 2000189075 A	11-07-2000	
EP 1108792	A	20-06-2001	AR 026955 A1	05-03-2003	
			AT 264402 T	15-04-2004	
			BR 0005911 A	21-08-2001	
			CA 2328572 A1	17-06-2001	
			DE 60009845 D1	19-05-2004	
			DE 60009845 T2	21-04-2005	
			ES 2218086 T3	16-11-2004	
			FR 2802551 A1	22-06-2001	
			JP 2001224400 A	21-08-2001	
			KR 20010057572 A	04-07-2001	
			MX PA00012442 A	15-10-2004	
			US 2001018092 A1	30-08-2001	