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# PURIFICATION OF VWF FOR INCREASED REMOVAL OF NON-LIPID ENVELOPED VIRUSES

#### **CROSS-REFERENCE TO RELATED APPLICATIONS**

**[0001]** This application claims the priority benefit under 35 U.S.C. § 119(e) of U.S. Provisional Application No. 61/235,570, filed August 20, 2009, the disclosure of which is incorporated herein by reference in its entirety.

## FIELD OF THE INVENTION

[0002] Generally, the invention relates to methods of purifying VWF for increased removal of non-lipid enveloped viruses.

## **BACKGROUND OF THE INVENTION**

[0003] Von Willebrand factor (VWF) is a glycoprotein circulating in plasma as a series of multimers ranging in size from about 500 to 20,000 kD. Multimeric forms of VWF are composed of 250 kD polypeptide subunits linked together by disulfide bonds. VWF mediates initial platelet adhesion to the sub-endothelium of the damaged vessel wall. Only the larger multimers exhibit hemostatic activity. It is assumed that endothelial cells secrete large polymeric forms of VWF and those forms of VWF which have a low molecular weight (low molecular weight VWF) arise from proteolytic cleavage. The multimers having large molecular masses are stored in the Weibel-Pallade bodies of endothelial cells and liberated upon stimulation.

**[0004]** VWF is synthesized by endothelial cells and megakaryocytes as prepro-VWF that consists to a large extent of repeated domains. Upon cleavage of the signal peptide, pro-VWF dimerizes through disulfide linkages at its C-terminal region. The dimers serve as protomers for multimerization, which is governed by disulfide linkages between the free end termini. The assembly to multimers is followed by the proteolytic removal of the propeptide sequence (Leyte et al., Biochem. J. 274 (1991), 257-261).

**[0005**] The primary translation product predicted from the cloned cDNA of VWF is a 2813-residue precursor polypeptide (prepro-VWF). The prepro-VWF consists of a 22 amino acid signal peptide and a 741 amino acid propeptide, with the mature VWF comprising 2050 amino acids (Ruggeri Z.A., and Ware, J., FASEB J., 308-316 (1993)).

[0006] Defects in VWF are causal to Von Willebrand disease (VWD), which is characterized by a more or less pronounced bleeding phenotype. VWD type 3 is the most severe form in which VWF is completely missing, and VWD type 1 relates to a quantitative loss of VWF and its phenotype can be very mild. VWD type 2 relates to qualitative defects of VWF and can be as severe as VWD type 3. VWD type 2 has many sub forms, some being associated with the loss or the decrease of high molecular weight multimers. Von Willebrand syndrome type 2a (VWS-2A) is characterized by a loss of both intermediate and large multimers. VWS-2B is characterized by a loss of highest-molecular-weight multimers. Other diseases and disorders related to VWF are known in the art.

[0007] The removal or inactivation of non-lipid enveloped viruses from therapeutic protein solutions has traditionally been accomplished by treatment with physical methods like high temperature (e.g., dry heat, vapor heat, pasteurization), irradiation with high energy rays (e.g., ultraviolet (UV) rays or beta radiation), low pH, nanofiltration or by chromatographic procedures, in particular affinity chromatography. However, these procedures are often ineffective when purifying a high molecular weight protein such as VWF which does not pass through a nanofilter and/or loses its potency or molecular integrity upon treatment with heat or radiation.

[0008] Current regulatory guidelines ask manufacturers to address the issue of reduction and/or inactivation of both lipid enveloped and non-lipid enveloped viruses for recombinant pharmaceutical products. The ICH "Guideline on Viral Safety Evaluations of Biotechnology Products" (Federal Register, 1998, 63(185): 51074- 51084) gives manufacturers flexibility how to address viral issues taking into account the type of product, the production process and the risk of potentially contaminating viruses. These guidelines point out that the risk of viral contamination is a feature common to all biotechnology products derived from cell lines. Such contamination could have serious clinical consequences and can arise from the contamination of the source cell lines themselves (cell substrates) or from adventitious introduction of virus during production.

**[0009]** Whereas the inactivation of lipid-enveloped viruses can be performed very effectively by a solvent/detergent (S/D) treatment approach, the inactivation or removal of non-lipid-enveloped model viruses (NLEV's) can be challenging due to their small size and physical stability.

[0010] Thus there exists a need in the art to develop methods to efficiently inactivate or remove non-lipid enveloped viruses during the purification of VWF.

#### **SUMMARY OF THE INVENTION**

**[0011]** The present invention provides an efficient method for purifying VWF for increased removal of non-lipid enveloped viruses. The present invention provides a novel method of purifying VWF for increased removal of NLEV's by performing the product loading step and the wash step of the purification process at a high pH.

[0012] One method known in the art for purifying polypeptides from NLEV's involves the use of nanofiltration. The principle behind efficient separation of protein and virus using nanofiltration exploits the size difference between the polypeptide and the virus; efficient separation requires the polypeptide to have an effective size smaller that the virus, which allows the polypeptide to pass through the pores of the nanofilter while the virus is retained. If the polypeptide and virus are of a comparable size relative to each other, however, separation is problematic because either the polypeptide and virus both pass through the nanofilter pores or neither do. The methods disclosed herein overcome this problem by using a cation exchange resin rather than nanofiltration and loading and/or washing the resin at a sufficiently high pH to separate the polypeptide from the virus.

[0013] Without being bound by theory, the methods disclosed herein are useful for improved removal of NLEV from polypeptide solutions wherein the polypeptide is of a certain size and/or conformation. A polypeptide of a sufficiently large size is likely to have localized charge characteristics at or above the isoelectric point of the polypeptide, *i.e.*, regions of the polypeptide can maintain localized positive or negative charges, thereby allowing the polypeptide to adsorb to the column resin while the virus flows through. This uneven charge distribution over the length of a polypeptide allows the polypeptide to remain attached to the resin despite loading and/or washing of the resin at a high pH.

[0014] The invention provides a method for removing a non-lipid enveloped virus from a protein-containing solution comprising loading a protein in the solution onto a cation

exchange resin, and washing the resin with a buffer at a pH higher than the isoelectric point of the protein to elute the virus. In one aspect, the protein is loaded onto the resin in a buffer at a pH higher than that of the isoelectric point of the protein to elute the virus. In another aspect, the protein is loaded onto the resin in a buffer that is not the buffer used in the wash step, and the resin is subsequently washed with the buffer that is at a pH higher than an isoelectric point of the protein.

**[0015]** In one embodiment, a method for removing a non-lipid enveloped virus from a protein-containing solution is provided comprising applying the solution to a cation exchange resin at a pH higher than the isoelectric point of the protein, and washing the cation exchange resin with a first wash buffer to form an eluate, said first wash buffer having a pH that is equal to or lower than the solution applied to the cation exchange resin.

In one aspect, the pH of the solution is about 1 pH unit above the isoelectric point of the protein. In other aspects, the pH of the solution is about 1.1, or about 1.2, or about 1.3, or about 1.4, or about 1.5, or about 1.6, or about 1.7, or about 1.8, or about 1.9, or about 2.0, or about 2.1, or about 2.2, or about 2.3, or about 2.4, or about 2.5, or about 2.6, or about 2.7, or about 2.8, or about 2.9, or about 3.0, or about 3.1, or about 3.2, or about 3.3, or about 3.4, or about 3.5, or about 3.6, or about 3.7, or about 3.8, or about 3.9, or about 4.0, or about 4.1, or about 4.2, or about 4.3, or about 4.4, or about 4.5, or about 4.6, or about 4.7, or about 4.8, or about 4.9, or about 5.0, or about 5.1, or about 5.2, or about 5.3, or about 5.4, or about 5.5, or about 5.6, or about 5.7, or about 5.8, or about 5.9, or about 6.0or more pH units or more above the isoelectric point of the protein. In these embodiments, the pH is greater than about 7. In a related aspect, the pH of the protein-containing solution is about 7.0. In other aspects, the pH of the protein-containing solution is about 7.1, or about 7.2, or about 7.3, or about 7.4, or about 7.5, or about 7.6, or about 7.7, or about 7.8, or about 7.9, or about 8.0, or about 8.1, or about 8.2, or about 8.3, or about 8.4, or about 8.5, or about 8.6, or about 8.7, or about 8.8, or about 8.9, or about 9.0, or about 9.1, or about 9.2, or about 9.3, or about 9.4, or about 9.5, or about 9.6, or about 9.7, or about 9.8, or about 9.9, or about 10.0, or about 10.1, or about 10.2, or about 10.3, or about 10.4, or about 10.5, or about 10.6, or about 10.7, or about 10.8, or about 10.9, or about 11.0, or about 11.1, or about 11.2, or about 11.3, or about 11.4, or about 11.5, or about 11.6, or about 11.7, or about 11.8, or about 11.9, or about 12.0, or about 12.1, or about 12.2, or about 12.3, or about 12.4, or about 12.5, or about 12.6, or about 12.7, or about 12.8, or about 12.9, or about 13.0 or higher.

In another embodiment, a method is provided for removing a non-lipid enveloped [0017] virus from a protein-containing solution comprising applying the solution to a cation exchange resin, washing the cation exchange resin with a first wash buffer at a pH higher than the pH of the solution applied to the cation exchange resin, and washing the cation exchange resin with a second wash buffer to form an eluate, said first eluant having a pH that is equal to or lower than the first wash buffer. In one aspect, the pH of the first wash buffer is about 1 pH unit above the pH of the solution applied to the cation exchange resin. In other aspects, the pH of the first wash buffer is about 0.1, or about 0.2, or about 0.3, or about 0.4, or about 0.5, or about 0.6, or about 0.7, or about 0.8, or about 0.9, or about 1.1, or about 1.2, or about 1.3, or about 1.4, or about 1.5, or about 1.6, or about 1.7, or about 1.8, or about 1.9, or about 2.0, or about 2.1, or about 2.2, or about 2.3, or about 2.4, or about 2.5, or about 2.6, or about 2.7, or about 2.8, or about 2.9, or about 3.0, or about 3.1, or about 3.2, or about 3.3, or about 3.4, or about 3.5, or about 3.6, or about 3.7, or about 3.8, or about 3.9, or about 4.0, or about 4.1, or about 4.2, or about 4.3, or about 4.4, or about 4.5, or about 4.6, or about 4.7, or about 4.8, or about 4.9, or about 5.0, or about 5.1, or about 5.2, or about 5.3, or about 5.4, or about 5.5, or about 5.6, or about 5.7, or about 5.8, or about 5.9, or about 6.0, or about 6.1, or about 6.2, or about 6.3, or about 6.4, or about 6.5, or about 6.6, or about 6.7, or about 6.8. or about 6.9, or about 7.0, or about 7.1, or about 7.2, or about 7.3, or about 7.4, or about 7.5, or about 7.6, or about 7.7, or about 7.8, or about 7.9, or about 8 or about 8.1, or about 8.2, or about 8.3, or about 8.4, or about 8.5, or about 8.6, or about 8.7, or about 8.8, or about 8.9, or about 9, or about 9.1, or about 9.2, or about 9.3, or about 9.4, or about 9.5, or about 9.6, or about 9.7, or about 9.8, or about 9.9, or about 10 or more pH units or more above the isoelectric point of the protein. In these embodiments, the pH of the first wash buffer is greater than about 7. In other aspects, the pH of the first wash buffer is about 7.1, or about 7.2, or about 7.3, or about 7.4, or about 7.5, or about 7.6, or about 7.7, or about 7.8, or about 7.9, or about 8.0, or about 8.1, or about 8.2, or about 8.3, or about 8.4, or about 8.5, or about 8.6, or about 8.7, or about 8.8, or about 8.9, or about 9.0, or about 9.1, or about 9.2, or about 9.3, or about 9.4, or about 9.5, or about 9.6, or about 9.7, or about 9.8, or about 9.9, or about 10.0, or about 10.1, or about 10.2, or about 10.3, or about 10.4, or about 10.5, or about 10.6, or about 10.7, or about 10.8, or about 10.9, or about 11.0 or higher.

[0018] In an embodiment, the protein in the solution is a polypeptide having a molecular mass of at least about 150 kilodaltons. In various aspects, the protein in the solution is a polypeptide having a molecular mass of at least about 175 kilodaltons, or about 180

kilodaltons, or about 190 kilodaltons, or about 200 kilodaltons, or about 210 kilodaltons, or about 220 kilodaltons, or about 230 kilodaltons, or about 240 kilodaltons, or about 250 kilodaltons, or about 260 kilodaltons, or about 270 kilodaltons, or about 280 kilodaltons, or about 290 kilodaltons, or about 300 kilodaltons, or about 310 kilodaltons, or about 320 kilodaltons, or about 330 kilodaltons, or about 340 kilodaltons, or about 350 kilodaltons, or about 360 kilodaltons, or about 370 kilodaltons, or about 380 kilodaltons, or about 390 kilodaltons, or about 400 kilodaltons, or about 410 kilodaltons, or about 420 kilodaltons, or about 430 kilodaltons, or about 440 kilodaltons, or about 450 kilodaltons, or about 460 kilodaltons, or about 470 kilodaltons, or about 480 kilodaltons, or about 490 kilodaltons, or about 500 kilodaltons or more. As described herein, polypeptides also comprise multimeric structures and such multimeric structures, in various aspects, have a molecular mass of at least about 500 kilodaltons. In related aspects, the multimeric structures have a molecular mass of at least about 510, or about 520, or about 530, or about 540, or about 550, or about 560, or about 570, or about 580, or about 590, or about 600, or about 610, or about 620, or about 630, or about 640, or about 650, or about 660, or about 670, or about 680, or about 690, or about 700, or about 710, or about 720, or about 730, or about 740, or about 750, or about 760, or about 770, or about 780, or about 790, or about 800, or about 810, or about 820, or about 830, or about 840, or about 850, or about 860, or about 870, or about 880, or about 890, or about 900, or about 910, or about 920, or about 930, or about 940, or about 950, or about 960, or about 970, or about 980, or about 990 kilodaltons, or about 1 megadalton, or about 1.1 megadaltons, or about 1.2 megadaltons, or about 1.3 megadaltons, or about 1.4 megadaltons, or about 1.5 megadaltons, or about 1.6 megadaltons, or about 1.7 megadaltons, or about 1.8 megadaltons, or about 1.9 megadaltons, or about 2.0 megadaltons, or about 2.1 megadaltons, or about 2.2 megadaltons, or about 2.3 megadaltons, or about 2.4 megadaltons, or about 2.5 megadaltons, or about 2.6 megadaltons, or about 2.7 megadaltons, or about 2.8 megadaltons, or about 2.9 megadaltons, or about 3.0 megadaltons, or about 3.1 megadaltons, or about 3.2 megadaltons, or about 3.3 megadaltons, or about 3.4 megadaltons, or about 3.5 megadaltons, or about 3.6 megadaltons, or about 3.7 megadaltons, or about 3.8 megadaltons, or about 3.9 megadaltons, or about 4.0 megadaltons, or about 4.1 megadaltons, or about 4.2 megadaltons, or about 4.3 megadaltons, or about 4.4 megadaltons, or about 4.5 megadaltons, or about 4.6 megadaltons, or about 4.7 megadaltons, or about 4.8 megadaltons, or about 4.9 megadaltons, or about 5.0 megadaltons or more.

[0019] In some embodiments, the cation exchange resin has a negatively charged group selected from the group consisting of carboxymethyl (CM), sulphoalkyl (SP, SE), sulphate and methylsulfonate (S) as well as any other negatively charged ligand.

**[0020]** In a further embodiment, the protein is a blood coagulation protein. In various aspects, the blood coagulation protein is selected from the group consisting of Factor VIII, von Willebrand factor, FI (Fibrinogen), FV (Proaccelerin), FXI (plasma-thromboplastin antecedent), and FXIII (fibrin stabilizing factor).

[0021] In an embodiment, a method for removing a non-lipid enveloped virus from a von Willebrand (VWF)-containing solution is provided comprising applying the solution to a cation exchange resin at a pH higher than the isoelectric point of the protein and washing the cation exchange resin with a first wash buffer to form an eluate, said first wash buffer having a pH that is equal to or lower than the solution applied to the cation exchange resin.

[0022] In another embodiment, a method for removing a non-lipid enveloped virus from a VWF-containing solution is provided comprising applying the solution to a cation exchange resin, washing the cation exchange resin with a first wash buffer at a pH higher than the pH of the solution applied to the cation exchange resin and washing the cation exchange resin with a second wash buffer to form an eluate, said first eluant having a pH that is equal to or lower than the first wash buffer.

[0023] In a further embodiment, a method for removing a non-lipid enveloped virus from a VWF-containing solution comprising applying the solution to a cation exchange resin at a pH higher than the isoelectric point of the protein and washing the cation exchange resin with a first wash buffer at a pH higher than the isoelectric point of the protein applied to the cation exchange resin; and washing the cation exchange resin with a second wash buffer to form an eluate, said first eluant having a pH that is equal to or lower than the first wash buffer.

[0023a] Definitions of the specific embodiments of the invention as claimed herein follow.

**[0023b]** According to a first embodiment of the invention, there is provided a method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the protein-containing solution to a cation exchange resin at a pH of at least 1.6 units above the isoelectric point of a protein in the protein-containing solution; and

washing the cation exchange resin with a wash buffer to form an eluate, said wash buffer having a pH that is lower than the pH of the protein-containing solution applied to the cation exchange resin but having a pH higher than the isoelectric point of the protein, wherein the protein in the protein-containing solution has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

**[0023c]** According to a second embodiment of the invention, there is provided a method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the protein-containing solution to a cation exchange resin;

washing the cation exchange resin with a first wash buffer having a pH higher than the pH of the protein-containing solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein; and

washing the cation exchange resin with a second wash buffer to form an eluate, said eluate having a pH that is equal to or lower than the first wash buffer, wherein the protein in the protein-containing solution has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

**[0023d]** According to a third embodiment of the invention, there is provided a method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the solution to a cation exchange resin at a pH higher than the isoelectric point of the protein in the protein-containing solution; and

washing the cation exchange resin with a first wash buffer at a pH higher than the isoelectric point of the protein in the protein-containing solution applied to the cation exchange resin; and

washing the cation exchange resin with a second wash buffer to form an eluate, said eluate having a pH that is equal to or lower than the pH of the first wash buffer, wherein the protein in the protein-containing solution has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

**[0023e]** According to a fourth embodiment of the invention, there is provided a method for removing a non-lipid enveloped virus from a von Willebrand Factor (VWF)-containing solution comprising:

applying the VWF-containing solution to a cation exchange resin at a pH of at least 1.6 units above the isoelectric point of VWF; and

washing the cation exchange resin with a first wash buffer to form an eluate, said wash buffer having a pH that is equal to or lower than the pH of the VWF-containing solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein, and whereby the non-lipid enveloped virus is removed from the VWF-containing solution.

[0023f] According to a fifth embodiment of the invention, there is provided a method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the protein-containing solution to a cation exchange resin, wherein the pH of the protein-containing solution is at least 2.0 pH units or more above the isoelectric point of a protein in the protein-containing solution; and

washing the cation exchange resin with a wash buffer to form an eluate, said wash buffer having a pH that is equal to or lower than the pH of the solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein, wherein the protein has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

# **BRIEF DESCRIPTION OF THE FIGURES**

[0024] Figure 1 shows the result of an SDS-PAGE separation followed by silver staining (A) and Western Blot (B) analysis for residual rFVIII.

[0025] Figure 2 shows the stained gel of the UNO S runs with MMV and REO virus spiked samples.

# [TEXT CONTINUES ON PAGE 8]

[0026] Figure 3 shows the stained gel of the UNO S runs with MMV and REO virus spiked samples.

**[0027]** Figure 4 shows the results of subjecting the purified preparations of rVWF obtained by the process variants to proteolytic digestion by V8 protease in the native state and separating the resulting peptides by RP-HPLC.

**[0028]** Figure 5 shows the results of subjecting the purified preparations of rVWF obtained by the process variants to trypsin in the denatured state and separating the resulting peptides by RP-HPLC.

#### **DETAILED DESCRIPTION OF THE INVENTION**

[0029] The present invention relates to a method for purifying VWF with increased removal of non-lipid enveloped viruses. The methods of the invention are applicable in column (*i.e.*, chromatography) as well as batch (*i.e.*, without column hardware) mode.

**[0030]** The method of the present invention utilizes a purification method on a cation exchange resin for the increased removal of non-lipid enveloped viruses. Previous methods of purification of VWF using cation exchange chromatography were performed at a neutral pH. These methods allowed for the manufacture of purified VWF of good yield and purity, but surprisingly the process had no capacity to remove non-lipid enveloped viruses.

#### **Definition of terms**

[0031] Unless otherwise defined, all technical and scientific terms used herein have the same meaning as commonly understood by one of ordinary skill in the art to which this invention belongs. The following references provide one of skill with a general definition of many of the terms used in this invention: Singleton, et al., DICTIONARY OF MICROBIOLOGY AND MOLECULAR BIOLOGY (2d ed. 1994); THE CAMBRIDGE DICTIONARY OF SCIENCE AND TECHNOLOGY (Walker ed., 1988); THE GLOSSARY OF GENETICS, 5TH ED., R. Rieger, et al. (eds.), Springer Verlag (1991); and Hale and Marham, THE HARPER COLLINS DICTIONARY OF BIOLOGY (1991).

[0032] Each publication, patent application, patent, and other reference cited herein is incorporated by reference in its entirety to the extent that it is not inconsistent with the present disclosure.

[0033] It is noted here that, as used in this specification and the appended claims, the singular forms "a," "an," and "the" include plural reference unless the context clearly dictates otherwise.

[0034] As used herein, the following terms have the meanings ascribed to them unless specified otherwise.

[0035] As used herein the terms "express," "expressing" and "expression" mean allowing or causing the information in a gene or DNA sequence to become manifest, for example, producing a protein by activating the cellular functions involved in transcription and translation of a corresponding gene or DNA sequence. A DNA sequence is expressed in or by a cell to form an "expression product" such as a protein. The expression product itself, e.g. the resulting protein, may also be said to be "expressed." An expression product can be characterized as intracellular, extracellular or secreted. The term "intracellular" means inside a cell. The term "extracellular" means outside a cell, e.g., certain types of transmembrane proteins. A substance is "secreted" by a cell if it appears in significant measure outside the cell, from somewhere on or inside the cell.

**[0036]** As used herein a "polypeptide" refers to a polymer composed of amino acid residues, structural variants, related naturally-occurring structural variants, and synthetic non-naturally occurring analogs thereof linked via peptide bonds. Synthetic polypeptides can be prepared, for example, using an automated polypeptide synthesizer. The term "protein" typically refers to large polypeptides. The term "peptide" typically refers to short polypeptides. The term "polypeptide" also includes polymeric structures. Therefore, a "polypeptide" may be a monomer, dimer, trimer, or larger multimeric structure. These multimeric structures can be up to 5 megadaltons or larger.

[0037] As used herein, the "isoelectric point" is the pH value at which the net electric charge of a polypeptide in an aqueous solution is zero.

[0038] As used herein a "fragment" of a polypeptide is meant to refer to any portion of a polypeptide or protein smaller than the full-length polypeptide or protein expression product.

**[0039]** As used herein an "analog" refers to any of two or more polypeptides substantially similar in structure and having the same biological activity, but can have varying degrees of activity, to either the entire molecule, or to a fragment thereof. Analogs differ in the composition of their amino acid sequences based on one or more mutations involving substitution of one or more amino acids for other amino acids. Substitutions can be

conservative or non-conservative based on the physico-chemical or functional relatedness of the amino acid that is being replaced and the amino acid replacing it.

[0040] As used herein a "variant" refers to a polypeptide, protein or analog thereof that is modified to comprise additional chemical moieties not normally a part of the molecule. Such moieties may modulate the molecule's solubility, absorption, biological half-life, etc. The moieties may alternatively decrease the toxicity of the molecule and eliminate or attenuate any undesirable side effect of the molecule, etc. Moieties capable of mediating such effects are disclosed in Remington's Pharmaceutical Sciences (1980). Procedure for coupling such moieties to a molecule are well known in the art. For example, the variant may be a blood clotting factor having a chemical modification which confers a longer half-life in vivo to the protein. In various aspects, polypeptides are modified by glycosylation, pegylation, and/or polysialylation.

#### **Recombinant VWF**

[0041] The polynucleotide and amino acid sequences of prepro-VWF are set out in SEQ ID NO:1 and SEQ ID NO:2, respectively, and are available at GenBank Accession Nos. NM\_000552 and NP\_000543, respectively. The amino acid sequence corresponding to the mature VWF protein is set out in SEQ ID NO: 3 (corresponding to amino acids 764-2813 of the full length prepro-VWF amino acid sequence).

[0042] One form of useful rVWF has at least the property of *in vivo*-stabilizing, e.g. binding, of at least one Factor VIII (FVIII) molecule and having optionally a glycosylation pattern which is pharmacologically acceptable. Specific examples thereof include VWF without A2 domain thus resistant to proteolysis (Lankhof et al., Thromb. Haemost. 77: 1008-1013, 1997), and the VWF fragment from Val 449 to Asn 730 including the glycoprotein lb-binding domain and binding sites for collagen and heparin (Pietu et al., Biochem. Biophys. Res. Commun. 164: 1339-1347, 1989). The determination of the ability of a VWF to stabilize at least one FVIII molecule can be carried out in VWF-deficient mammals according to methods known in the state in the art.

[0043] The rVWF of the present invention may be produced by any method known in the art. One specific example is disclosed in WO86/06096 published on Oct. 23, 1986 and U.S. Patent Application No. 07/559,509, filed on Jul. 23, 1990, which is incorporated herein by reference with respect to the methods of producing recombinant VWF. Thus, methods are known in the art for (i) the production of recombinant DNA by genetic engineering, e.g. via

reverse transcription of RNA and/or amplification of DNA, (ii) introducing recombinant DNA into procaryotic or eucaryotic cells by transfection, e.g. via electroporation or microinjection, (iii) cultivating said transformed cells, e.g. in a continuous or batchwise manner, (iv) expressing VWF, e.g. constitutively or upon induction, and (v) isolating said VWF, e.g. from the culture medium or by harvesting the transformed cells, in order to (vi) obtain purified rVWF, e.g. via anion exchange chromatography or affinity chromatography. A recombinant VWF may be made in transformed host cells using recombinant DNA techniques well known in the art. For instance, sequences coding for the polypeptide could be excised from DNA using suitable restriction enzymes.

[0044] Alternatively, the DNA molecule could be synthesized using chemical synthesis techniques, such as the phosphoramidate method. Also, a combination of these techniques could be used.

**[0045**] The invention also provides vectors encoding polypeptides of the invention in an appropriate host. The vector comprises the polynucleotide that encodes the polypeptide operatively linked to appropriate expression control sequences. Methods of effecting this operative linking, either before or after the polynucleotide is inserted into the vector, are well known. Expression control sequences include promoters, activators, enhancers, operators, ribosomal binding sites, start signals, stop signals, cap signals, polyadenylation signals, and other signals involved with the control of transcription or translation. The resulting vector having the polynucleotide therein is used to transform an appropriate host. This transformation may be performed using methods well known in the art.

**[0046]** Any of a large number of available and well-known host cells may be used in the practice of this invention. The selection of a particular host is dependent upon a number of factors recognized by the art, including, for example, compatibility with the chosen expression vector, toxicity of the peptides encoded by the DNA molecule, rate of transformation, ease of recovery of the peptides, expression characteristics, bio-safety and costs. A balance of these factors must be struck with the understanding that not all host cells are equally effective for the expression of a particular DNA sequence. Within these general guidelines, useful microbial host cells include bacteria, yeast and other fungi, insects, plants, mammalian (including human) cells in culture, or other hosts known in the art.

[0047] Next, the transformed host is cultured and purified. Host cells may be cultured under conventional fermentation conditions so that the desired compounds are expressed.

Such fermentation conditions are well known in the art. Finally, the polypeptides are purified from culture by methods well known in the art.

[0048] Depending on the host cell utilized to express a compound of the invention, carbohydrate (oligosaccharide) groups may conveniently be attached to sites that are known to be glycosylation sites in proteins. Generally, O-linked oligosaccharides are attached to serine (Ser) or threonine (Thr) residues while N-linked oligosaccharides are attached to asparagine (Asn) residues when they are part of the sequence Asn-X-Ser/Thr, where X can be any amino acid except proline. X is preferably one of the 19 naturally occurring amino acids not counting proline. The structures of N-linked and O-linked oligosaccharides and the sugar residues found in each type are different. One type of sugar that is commonly found on both is N-acetylneuraminic acid (referred to as sialic acid). Sialic acid is usually the terminal residue of both N-linked and O-linked oligosaccharides and, by virtue of its negative charge, may confer acidic properties to the glycosylated compound. Such site(s) may be incorporated in the linker of the compounds of this invention and are preferably glycosylated by a cell during recombinant production of the polypeptide compounds (e.g., in mammalian cells such as CHO, BHK, COS). However, such sites may further be glycosylated by synthetic or semi-synthetic procedures known in the art.

[0049] Alternatively, the compounds may be made by synthetic methods. For example, solid phase synthesis techniques may be used. Suitable techniques are well known in the art, and include those described in Merrifield (1973), Chem. Polypeptides, pp. 335-61 (Katsoyannis and Panayotis eds.); Merrifield (1963), J. Am. Chem. Soc. 85: 2149; Davis et al. (1985), Biochem. Intl. 10: 394-414; Stewart and Young (1969), Solid Phase Peptide Synthesis; U.S. Pat. No. 3,941,763; Finn et al. (1976), The Proteins (3rd ed.) 2: 105-253; and Erickson et al. (1976), The Proteins (3rd ed.) 2: 257-527. Solid phase synthesis is the preferred technique of making individual peptides since it is the most cost-effective method of making small peptides.

#### Fragments, variants and analogs of VWF

[0050] Methods for preparing polypeptide fragments, variants or analogs are well-known in the art.

[0051] Fragments of a polypeptide are prepared using, without limitation, enzymatic cleavage (e.g., trypsin, chymotrypsin) and also using recombinant means to generate a polypeptide fragments having a specific amino acid sequence. Polypeptide fragments may be

generated comprising a region of the protein having a particular activity, such as a multimerization domain or any other identifiable VWF domain known in the art.

[0052] Variants of a polypeptide are contemplated to include human and non-human forms of VWF (e.g., murine VWF). Also contemplated by the methods herein are chimeric polypeptides comprising, e.g., a mouse/human fusion polypeptide.

**[0053**] Methods of making polypeptide analogs are also well-known. Amino acid sequence analogs of a polypeptide can be substitutional, insertional, addition or deletion analogs. Deletion analogs, including fragments of a polypeptide, lack one or more residues of the native protein which are not essential for function or immunogenic activity. Insertional analogs involve the addition of, e.g., amino acid(s) at a non-terminal point in the polypeptide. This analog may include insertion of an immunoreactive epitope or simply a single residue. Addition analogs, including fragments of a polypeptide, include the addition of one or more amino acids at either of both termini of a protein and include, for example, fusion proteins.

[0054] Substitutional analogs typically exchange one amino acid of the wild-type for another at one or more sites within the protein, and may be designed to modulate one or more properties of the polypeptide without the loss of other functions or properties. In one aspect, substitutions are conservative substitutions. By "conservative amino acid substitution" is meant substitution of an amino acid with an amino acid having a side chain of a similar chemical character. Similar amino acids for making conservative substitutions include those having an acidic side chain (glutamic acid, aspartic acid); a basic side chain (arginine, lysine, histidine); a polar amide side chain (glutamine, asparagine); a hydrophobic, aliphatic side chain (leucine, isoleucine, valine, alanine, glycine); an aromatic side chain (phenylalanine, tryptophan, tyrosine); a small side chain (glycine, alanine, serine, threonine, methionine); or an aliphatic hydroxyl side chain (serine, threonine).

[0055] Analogs may be substantially homologous or substantially identical to the recombinant VWF from which they are derived. Preferred analogs are those which retain at least some of the biological activity of the wild-type polypeptide, *e.g.* blood clotting activity.

**[0056]** Polypeptide variants contemplated include polypeptides chemically modified by such techniques as ubiquitination, glycosylation, including polysialation, conjugation to therapeutic or diagnostic agents, labeling, covalent polymer attachment such as pegylation (derivatization with polyethylene glycol), introduction of non-hydrolyzable bonds, and insertion or substitution by chemical synthesis of amino acids such as ornithine, which do not

normally occur in human proteins. Variants retain the same or essentially the same binding properties of non-modified molecules of the invention. Such chemical modification may include direct or indirect (e.g., via a linker) attachment of an agent to the VWF polypeptide. In the case of indirect attachment, it is contemplated that the linker may be hydrolyzable or non-hydrolyzable.

[0057] Preparing pegylated polypeptide analogs will generally comprise the steps of (a) reacting the polypeptide with polyethylene glycol (such as a reactive ester or aldehyde derivative of PEG) under conditions whereby the binding construct polypeptide becomes attached to one or more PEG groups, and (b) obtaining the reaction product(s). In general, the optimal reaction conditions for the acylation reactions will be determined based on known parameters and the desired result. For example, the larger the ratio of PEG: protein, the greater the percentage of poly-pegylated product. In some embodiments, the binding construct will have a single PEG moiety at the N-terminus. Polyethylene glycol (PEG) may be attached to the blood clotting factor to provide a longer half-life in vivo. The PEG group may be of any convenient molecular weight and may be linear or branched. The average molecular weight of the PEG ranges from about 2 kiloDalton ("kD") to about 100 kDa, from about 5 kDa to about 50 kDa, or from about 5 kDa to about 10 kDa. The PEG groups are attached to the blood clotting factor via acylation or reductive alkylation through a natural or engineered reactive group on the PEG moiety (e.g., an aldehyde, amino, thiol, or ester group) to a reactive group on the blood clotting factor (e.g., an aldehyde, amino, or ester group) or by any other technique known in the art.

[0058] Methods for preparing polysialylated polypeptide are described in United States Patent Publication 20060160948, Fernandes et Gregoriadis; Biochim. Biophys. Acta 1341: 26-34, 1997, and Saenko et al., Haemophilia 12:42-51, 2006. Briefly, a solution of colominic acid containing 0.1 M NaIO<sub>4</sub> is stirred in the dark at room temperature to oxidize the CA. The activated CA solution is dialyzed against, e.g., 0.05 M sodium phosphate buffer, pH 7.2 in the dark and this solution was added to a rVWF solution and incubated for 18 h at room temperature in the dark under gentle shaking. Free reagents can then be separated from the rVWF-polysialic acid conjugate by ultrafiltration/diafiltration. Conjugation of rVWF with polysialic acid may also be achieved using glutaraldehyde as cross-linking reagent (Migneault et al., Biotechniques 37: 790-796, 2004).

[0059] It is further contemplated that a polypeptide of the invention may be a fusion protein with a second agent which is a polypeptide. In one embodiment, the second agent

which is a polypeptide, without limitation, is an enzyme, a growth factor, an antibody, a cytokine, a chemokine, a cell-surface receptor, the extracellular domain of a cell surface receptor, a cell adhesion molecule, or fragment or active domain of a protein described above. In a related embodiment, the second agent is a blood clotting factor such as Factor VIII, Factor VII, Factor IX. The fusion protein contemplated is made by chemical or recombinant techniques well-known in the art.

**[0060]** It is also contemplated that prepro-VWF and pro-VWF polypeptides may provide a therapeutic benefit in the formulations of the present invention. For example, US Patent No. 7,005,502 describes a pharmaceutical preparation comprising substantial amounts of pro-VWF that induces thrombin generation in the presence of platelets *in vitro*. In addition to recombinant, biologically active fragments, variants, or analogs of the naturally-occuring mature VWF, the present invention contemplates the use of recombinant biologically active fragments, variants, or analogs of the prepro-VWF (set out in SEQ ID NO:2) or pro-VWF polypeptides (amino acid residues 23 to 764 of SEQ ID NO: 2) in the formulations described herein.

[0061] Polynucleotides encoding fragments, variants and analogs may be readily generated by a worker of skill to encode biologically active fragments, variants, or analogs of the naturally-occurring molecule that possess the same or similar biological activity to the naturally-occurring molecule. These polynucleotides can be prepared using PCR techniques, digestion/ligation of DNA encoding molecule, and the like. Thus, one of skill in the art will be able to generate single base changes in the DNA strand to result in an altered codon and a missense mutation, using any method known in the art, including, but not limited to site-specific mutagenesis. As used herein, the phrase "moderately stringent hybridization conditions" means, for example, hybridization at 42°C in 50% formamide and washing at 60°C in 0.1 x SSC, 0.1% SDS. It is understood by those of skill in the art that variation in these conditions occurs based on the length and GC nucleotide base content of the sequences to be hybridized. Formulas standard in the art are appropriate for determining exact hybridization conditions. See Sambrook et al., 9.47-9.51 in Molecular Cloning, Cold Spring Harbor Laboratory Press, Cold Spring Harbor, New York (1989).

## **Methods of Producing VWF**

[0062] Industrially, VWF, in particular human recombinant VWF (rVWF), is synthesized and expressed together with rFVIII in a genetically engineered CHO cell line. The function

of the co-expressed rVWF is to stabilize rFVIII in the cell culture process. rVWF is synthesized in the cell as the pro-form, containing a large pro-peptide attached to the N-terminus. Upon maturation in the endoplasmatic reticulum and Golgi apparatus, the propeptide is cleaved off by the action of the cellular protease furin and is secreted as a homopolymer of identical subunits, consisting of dimers of the expressed protein.

# **Purification of VWF**

**[0063]** Provided herein is a method for removing a non-lipid enveloped virus from a protein-containing solution is provided comprising applying the solution to a cation exchange resin at a pH higher that the isoelectric point of the protein, and washing the cation exchange resin with a first wash buffer to form an eluate, said first wash buffer having a pH that is equal to or lower than the solution applied to the cation exchange resin.

[0064] In one aspect, the pH of the solution is about 1 pH unit above the isoelectric point of the protein. In other aspects, the pH of the solution is about 1.2, or about 1.4, or about 1.6, or about 1.8, or about 2.0, or about 2.2, or about 2.4, or about 2.6, or about 2.8, or about 3.0, or about 3.2, or about 3.4, or about 3.6, or about 3.8, or about 4.0, or about 4.2, or about 4.4, or about 4.6, or about 4.8, or about 5.0, or about 5.5, or about 6.0 pH units or more above the isoelectric point of the protein.

[0065] In these embodiments, the pH is greater than about 7.. In other aspects, the pH is about 7.1, or about 7.2, or about 7.3, or about 7.4, or about 7.5, or about 7.6, or about 7.7, or about 7.8, or about 7.9, or about 8.0, or about 8.1, or about 8.2, or about 8.3, or about 8.4, or about 8.5, or about 8.6, or about 8.7, or about 8.8, or about 8.9, or about 9.0, or about 9.1, or about 9.2, or about 9.3, or about 9.4, or about 9.5, or about 9.6, or about 9.7, or about 9.8, or about 9.9, or about 10.0, or about 10.1, or about 10.2, or about 10.3, or about 10.4, or about 10.5, or about 10.6, or about 10.7, or about 10.8, or about 10.9, or about 11.0, or about 11.1, or about 11.2, or about 11.3, or about 11.4, or about 11.5, or about 11.6, or about 11.7, or about 11.8, or about 11.9, or about 12.0, or about 12.1, or about 12.2, or about 12.3, or about 12.4, or about 12.5, or about 12.6, or about 12.7, or about 12.8, or about 12.9, or about 13.0 or higher.

[0066] In another embodiment, a method is provided for removing a non-lipid enveloped virus from a protein-containing solution comprising applying the solution to a cation exchange resin, washing the cation exchange resin with a first wash buffer at a pH higher than the pH of the solution applied to the cation exchange resin, and washing the cation

exchange resin with a second wash buffer to form an eluate, said second wash buffer having a pH that is equal to or lower than the first wash buffer. In one aspect, the pH of the first wash buffer is about 1 pH unit above the pH of the solution applied to the cation exchange resin. For this stage it is contemplated that the ion exchange media is UNOsphere<sup>TM</sup> S (BioRad Laboratories, Inc., Hercules, CA), but other cation exchange systems may be used in the practice of the methods. These cation exchange systems are known to those of ordinary skill in the art.

[0067] In other aspects, the pH of the first wash buffer is about 1.1, or about 1.2, or about 1.3, or about 1.4, or about 1.5, or about 1.6, or about 1.7, or about 1.8, or about 1.9, or about 2.0, or about 2.1, or about 2.2, or about 2.3, or about 2.4, or about 2.5, or about 2.6, or about 2.7, or about 2.8, or about 2.9, or about 3.0, or about 3.1, or about 3.2, or about 3.3, or about 3.4, or about 3.5, or about 3.6, or about 3.7, or about 3.8, or about 3.9, or about 4.0, or about 4.1, or about 4.2, or about 4.3, or about 4.4, or about 4.5, or about 4.6, or about 4.7, or about 4.8, or about 4.9, or about 5.0, or about 5.1, or about 5.2, or about 5.3, or about 5.4, or about 5.5, or about 5.6, or about 5.7, or about 5.8, or about 5.9, or about 6.0 pH units or more above the isoelectric point of the protein. In these embodiments, the pH of the first wash buffer is greater than about 7. In other aspects, the pH of the first wash buffer is about 7.1, or about 7.2, or about 7.3, or about 7.4, or about 7.5, or about 7.6, or about 7.7, or about 7.8, or about 7.9, or about 8.0, or about 8.1, or about 8.2, or about 8.3, or about 8.4, or about 8.5, or about 8.6, or about 8.7, or about 8.8, or about 8.9, or about 9.0, or about 9.1, or about 9.2, or about 9.3, or about 9.4, or about 9.5, or about 9.6, or about 9.7, or about 9.8, or about 9.9, or about 10.0, or about 10.1, or about 10.2, or about 10.3, or about 10.4, or about 10.5, or about 10.6, or about 10.7, or about 10.8, or about 10.9, or about 11.0, or about 11.1, or about 11.2, or about 11.3, or about 11.4, or about 11.5, or about 11.6, or about 11.7, or about 11.8, or about 11.9, or about 12.0, or about 12.1, or about 12.2, or about 12.3, or about 12.4, or about 12.5, or about 12.6, or about 12.7, or about 12.8, or about 12.9, or about 13.0 or higher.

[0068] The following examples are not intended to be limiting but only exemplary of specific embodiments of the invention.

#### **EXAMPLES**

#### Example 1

[0069] Viruses and cells used in the assays described below are as follows.

[0070] REO-3 (Family Reoviridae; non-enveloped dsRNA virus), Strain Dearing (ATCC VR-824) was obtained from the ATCC. The virus was propagated and titrated on Vero cells obtained from ECACC (84113001). MMV (Family Parvoviridae; non-enveloped ssDNA virus), prototype strain (ATCC VR-1346), was obtained from the American Type Culture Collection, Rockville, Maryland. The virus was propagated and titrated on A9 cells (ATCC CCL-1.4). PPV (Family Parvoviridae; non-enveloped ssDNA virus), strain Tennessee (BRFF #PP951024), was obtained from Biological Research Faculty & Facility, Ijamsville, Maryland. The virus was propagated and titrated on PK-13 cells (ATCC CRL-6489). EMCV (Family Picornaviridae; non-enveloped ssRNA) (ATCC #VR-129B) was obtained from the American Type Culture Collection. The virus was propagated and titrated on Vero cells (European Collection of Cell Cultures, ECACC, #84113001). HadV (Family Adenoviridae; non-enveloped dsDNA), strain Adenoid 75 (ATCC VR-5), was obtained from the American Type Culture Collection. The virus was propagated and titrated on HeLa cells (ATCC CCL-2).

[0071] The steps involved in an exemplary VWF purification process comprise:

- Immune affinity chromatography of cell culture supernatant
  - i. Flow-through fraction
- Anion Exchange (e.g., trimethylaminoethyl anion exchange column)
- Filtration (0.45/0.2 μm)
- Anion Exchange (e.g., Mustang Q (Pall Corporation))
- Virus Inactivation (e.g., using solvent/detergent treatment)
- Filtration (0.8/0.65 μm)
- Cation Exchange (e.g., UNO S column)
- Ultrafiltration/Concentration
- Filtration (0.45/0.2 μm)
- Gel Filtration (Superose 6 prep grade (GE Life Sciences))

[0072] Optimization of UNO S Step. During the UNO S step rVWF is bound to a strong cation exchange resin while some of the impurities pass through. After washing the column with increased conductivity buffers the bound rVWF is released from the column with a salt

step. During the initial virus removal studies, this step showed at least a significant removal rate for the model REO virus. The conditions of the applied parameters and the corresponding results are listed in Table 1, below.

Table 1

Parameter	Standard Value	Changed value	MMV reduction factor (log10)	
Conductivity load/wash	15 mS/cm	25 mS/cm	n.a.	
pH load/wash/elution	6.5	8.0	0.9	
Wash buffer 2	TQA buffer*	TQA buffer with 200mM betains	0.7	
Wash buffer 3	TQA buffer	TQA buffer with 20% ethylen glycol		
Wash buffer 4	TQA buffer	TQA buffer with 10 mM CaCl <sub>2</sub>	0.8	
Wash buffer 5	TQA buffer	TQA buffer U.8 with 10 mM EDTA		
pH load/wash	6.5	9.0	2.0, 2.11, 2.12 and 2.12	
pH load/wash	6.5	9.0	2.12 for REO virus	

\*TQA Buffer: Tris, NaAc, mM NaCl in WFI pH 6.3 - 6.7 at 20 - 25°C

[0073] As can be seen in Table 1 the moderate changes in the process parameters (modification of conductivity, pH 8.0 and additives to wash buffers) did not result in a significant improvement of the MMV removal rates. Increasing the pH further to 9.0 reproducibly resulted in a significant removal rate of more than 2 logs for MMV as well as REO virus. This process change is technically easy to implement and the exposure of rVWF to the high pH environment can be kept relatively short (max. 6 hours). Elution of the bound rVWF is performed under neutral conditions.

**[0074]** The analysis of the virus inactivation capacity of the processes was carried out according to the recommendations of the CPMP guideline 268/95, using the following

formula: 
$$R = \log(\frac{V_1 \times T_1}{V_2 \times T_2})$$

where

R = virus reduction factor

V1 = volume of starting material [ml]

T1 = concentration of virus in starting material [TCID50/ml]

V2 = volume of material after the step [ml]

T2 = concentration of virus after the step [TCID50/ml]

[0075] The volumes and the titers of each spiked sample before and after treatment were used to calculate R. Whenever virus was undetectable, the detection limit was taken as the virus titer for calculation. Calculations were carried out with virus titers (log<sub>10</sub>[TCID50/ml] given to two decimal places, and only final results, i.e. reduction factors (R), were rounded to the first decimal place.

# Example 2

[0076] The UNO S eluate was concentrated to approximately 800 µg rVWF antigen/ml by ultrafiltration using 30 kDa cut-off modified cellulose membranes to facilitate the trace analysis of impurities and product variants.

## **Testing of rVWF**

**[0077] Ristocetin Activity**. The Ristocetin Cofactor Activity is determined by a turbidimetric analyzer using a von Willebrand reagent containing stabilized thrombocytes and the antibiotic "ristocetin". The von Willebrand Factor contained in the sample (= Ristocetin Cofactor) causes agglutination of stabilized thrombocytes in the presence of ristocetin. The agglutination reduces the turbidity of the reagent preparation, and the change in optical density is measured by the turbidimetric analyzer. Calibration is performed by the WHO concentrate reference standard #00/514.

**[0078] VWF Antigen**. VWF- samples are tested for their content of vWF-Antigen in an ELISA assay - double sandwich system with two polyclonal antibodies. Measurement of the color reactions on the microtitre plates is performed with a photometer at 490 nm. The concentration of each sample is calculated towards the standard curve with a computer supported ELISAAnalysis Program (curve algorithm : Cubic regression). All readings are corrected against the blank.

[0079] FVIII Binding Activity. FVIII binding of rVWF under static conditions was determined by an ELISA chromogenic assay (ECA) by incubating a constant amount of rFVIII with a diluted VWF-containing sample. The VWF- FVIII- complex formed was then transferred to a microtiter plate coated with a commercially available polyclonal rabbit antihuman VWF antibody. After incubation, unbound FVIII was removed by a subsequent washing step. Bound FVIII was quantified by a commercially available FVIII chromogenic assay (Technochrom FVIII: C reagent kit, Technoclone, Austria). The blank corrected optical densities (in mOD/min at 405 nm) were plotted against the VWF:Ag concentrations in logarithmic scale.

[0080] SDS-PAGE Analysis. Conventional 8% SDS-PAGE analysis under reducing conditions and staining of the gels with Coomassie Blue and Silver Stain can provide insight in the protein composition of rVWF. After transfer of the separated protein bands to a nitrocellulose membrane and immunological staining of the protein with appropriate antibodies against VWF, FVIII and Furin respectively, a comparison of VWF related proteins to total proteins can be made.

- [0081] Multimer Analysis. The multimeric structure of VWF is analyzed by high-density horizontal SDS agarose gel electrophoresis. In brief, samples are diluted to the same concentration in the range of 0.3-1.0 IU/ml VWF:Ag, incubated with Tris-EDTA-SDS buffer and the multimers separated under non-reducing conditions on an agarose gel. VWF multimers were visualized by in-gel immunostaining with a polyclonal rabbit anti human VWF antibody, followed by alkaline phosphatase (ALP) conjugated goat anti-rabbit IgG using the ALP color development kit. Alternatively, agarose gels were blotted onto a blotting membrane and staining was performed by a polyclonal rabbit anti-human VWF antibody followed by horse radish peroxidase conjugated anti-rabbit IgG. For visualization, electrochemi-luminescence was used which increases the sensitivity of detection for VWF by at least two magnitudes. Low (1 % agarose) and high resolution (2.5 % agarose) conditions were used to analyze the size distribution of VWF multimers and the multimeric structure, respectively.
- **[0082] HPLC Analysis**. Recombinant VWF can be cleaved by GluC (V8 protease) under native conditions to give two main fragments (N-terminal and C-terminal homodimer fragment), which are separated on a reverse phase HPLC C4-column. The fragments are detected by by monitoring the UV absorbance at 280 nm.
- **[0083] Peptide Mapping**. The primary structure of rVWF was investigated using a peptide mapping approach. Samples of purified rVWF were reduced with dithiothreitol (DTT) and the free, sulfhydril groups were blocked with 4-vinylpyridin. Sequencing grade trypsin was added to the rVWF and allowed to react for 18 hours. The resulting peptide mixture was separated by reverse phase chromatography. Eluting peptides were detected by on-line UV detection at 214 nm and on-line electrospray ionization mass spectrometry.
- [0084] Test for deamidated rVWF. The analytical method for the detection of iso-aspartate (one reaction product originating from the de-amidation of asparagine) employs tryptic digestion, followed by the Protein Isoaspartyl Methyltransferase (PIMT) enzymatic

reaction using the ISOQUANT IsoAspartate Detection Kit supplied by Promega. PIMT catalyzes the transfer of a methyl group from the substrate S-adenosyl-L methionine (SAM) to IsoAsp at the carboxyl position, generating S-adenosyl homocysteine (SAH). The stoichiometrically released SAH is detected at a wavelength of 260 nm by a RP HPLC method.

[0085] The analytical data for the product obtained by the different processes are summarized in Table 2.

Table 2: Analytical Data for pH 9 and Control Runs

Sample	UNO S #1 (pH 9 run)	UNO S #2 (Control run)	UNO S #3 (Control run pilot scale)
VWF RcoF Activity (U/ml)	36.7	64.8	84.7
VWF Antigen (μg/ml)	715	1090	2010
Specific activity (U/mg)	51.3	59.4	42.1
Collagen binding (U/ml)	63.2	106.7	141.8
Specific collagen binding activity (U/mg)	88.4	97.9	70.5
FVIII binding (%)	51.7	64.6	63.1
CHO protein (µg/ml)	0.09	0.17	n.d.
CHO DNA (pg/ml)	Non detectable	10	n.d.
Furin activity (mU/mi)	< 6.25	< 6.25	<6.25
FVIII Ag (mUlml)	< 125	152	1650
FVIII Activity (mUIml)	71	1452	6222
Deamidation (mol%)	5.1	3.7	5.0
SDS-PAGE	See Figure 1		
Multimer pattern (low resolution)	See Figure 2		
Multimer pattern (high resolution)	See Figure 3		
RP-HPLC	See Figure 4		
Peptide Mapping	See Figure 5		

[0086] As can be seen from Table 2 the biochemical properties of rVWF purified by the different process variants are comparable.

[0087] The major band of the rVWF protein is very similar in all products whereas the extent of impurities is lower in sample #1 (denominated as VWF#07 in figure 1) by both silver staining and western blot analysis for residual rFVIII. The banding pattern for rFVIII

is comparable between all batches which suggests that no degradation due to the pH 9.0 conditions occurred.

[0088] Low and high resolution agarose gel electrophoresis revealed the high similarity of the rVWF preparations. No differences in multimer composition by low resolution multimer analysis could be seen. Figure 2 shows the stained gel of the UNO S runs with MMV and REO virus spiked samples. Also the high resolution multimer analysis revealed the intact multimer pattern suggesting no damage to the rVWF multimers occurred due to the pH 9.0 conditions. Figure 3 shows the stained gel of the UNO S runs with MMV and REO virus spiked samples.

[0089] By the Isoquant assay no enhanced de-amidation could be detected due to the dwell time of rVWF at pH 9.0. Generally the molar percentage of deamidated rVWF is very low. Subjecting the purified preparations of rVWF obtained by the process variants to proteolytic digestion by either V8 protease in the native state (see Figure 4) or trypsin (see Figure 5) in the denatured state and separating the resulting peptides by RP-HPLC resulted in similar chromatograms for all samples.

**[0090]** Minor differences in the peak patterns are due to the presence of different amounts of impurities (mainly residual rVWF propertide as can be seen in Figure 1) in the preparations which was confirmed by mass spectrometry or N-terminal sequence analysis.

#### Example 3

[0091] Purification of rVWF by Cation Exchange chromatography at high pH with MMV spike.

[0092] A UNOsphere S resin packed into a column was activated with 1 CV of 2 M NaCl and equilibrated with 25 CV of an equilibration buffer (pH=9.0). Thereafter, a rVWF containing solution adjusted to a conductivity of 15 mS/cm and a pH of 9.0 and spiked with mouse minute virus (MMV) was loaded onto the column at a linear flow rate of about 10.0 cm/h. The column was then washed with 10 CV of equilibration buffer (pH=9.0) and the product was eluted with 3.5 CV of elution buffer (pH=7.5) at a linear flow rate of 65cm/h. The increased pH during the loading and wash phase significantly reduced the binding of the virus particles to the resin but retained full binding of the product VWF. As a result, most of the loaded virus particles were found in the non-binding (flow through) and wash fraction separated from the product that was recovered in the eluate pool at high yields. The results in

Table 3 show that by applying this procedure a virus removal capacity of 2 logs could be obtained with the non-enveloped model virus mouse minute virus (MMV).

**[0093]** The TCID50 assay was performed as follows. Briefly, serial 1/2 log dilutions of the samples were prepared in the appropriate tissue culture medium and 100  $\mu$ l of each dilution were added to each of 8 wells of a microtiter plate seeded with the indicator cell tine. The cells were then incubated for 7 days at 36°C  $\pm$  2°C before the cytopathic effect was evaluated by visual inspection of the cells under a microscope. Median tissue culture infectious doses (TCID50) were calculated according to the Poisson distribution and expressed as  $\log_{10}[\text{TCID50/ml}]$ .

Virus content Volume Virus titer Reduction (TCID50) **(TCID50)** ml Log<sub>10</sub>/ml  $Log_{10}$  $Log_{10}$ Load 400 5.26 7.86 Eluate pool 89.4 3.8 5.75 2.11

**Table 3: Purification of rVWF on UNOsphere S** 

[0094] The purification was performed using a column with 15 mm diameter and a bed height of 14 cm. Data shown are virus titers of active mouse minute virus.

#### Example 4

[0095] Purification of rVWF by Cation Exchange chromatography at high pH with Reo Type 3 virus spike.

[0096] A UNOsphere S resin packed into a column was activated with 1 CV of 2 M NaCl and equilibrated with 25 CV of an equilibration buffer (pH=9.0). Thereafter, a rVWF containing solution adjusted to a conductivity of 15 mS/cm and a pH of 9.0 and spiked with various non-enveloped viruses was loaded onto the column at a linear flow rate of about 100 cm/h. The column was then washed with 10 CV of equilibration buffer (pH=9.0) and the product was eluted with 3.5 CV of elution buffer (pH=7.5) at a linear flow rate of 65 cm/h. The increased pH during the loading and wash phase significantly reduced the binding of the virus particles to the resin but retained full binding of the product VWF. As a result, most of the loaded virus particles were found in the non-binding (flow through) and wash fraction separated from the product that was recovered in the eluate pool at high yields. The results in Table 4 show that by applying this procedure a virus removal capacity of 2 logs could be obtained with the non-enveloped model virus mouse Reo Virus Type 3 (REO-III).

	Volume	Virus titer (TCID50)	Virus content (TCID50)	Reduction
	ml	Log <sub>10</sub> /ml	Log <sub>10</sub>	$Log_{10}$
Load	897	3.73	6.68	-
Eluate pool	89.3	2.61	4.56	2.12

**Table 4: Purification of rVWF on UNOsphere S** 

[0097] The purification was performed using a column with 15 mm diameter and a bed height of 14 cm. Data shown are virus titers of active mouse Reovirus Type III (REO-III).

#### Example 5

[0098] Purification of rVWF on UNOsphere S according the standard procedure (neutral pH).

[0099] A UNOsphere S resin packed into a column was activated with 1 CV of 2 M NaCl and equilibrated with 25 CV of an equilibration buffer (pH=6.5). Thereafter, a rVWF containing solution adjusted to a conductivity of 15 mS/cm and a pH of 6.5 and spiked with various non-enveloped viruses was loaded onto the column at a linear flow rate of about 100 cm/h. The column was then washed with 10 CV of equilibration buffer (pH=6.5) and the product was eluted with 3.5 CV of elution buffer (pH=7.5) at a linear flow rate of 65 cm/h. The virus titer of the various viruses tested were evaluated in the different chromatographic fractions (load, column flow through, wash, eluate, post eluate) and the reduction factors were calculated. The results in Table 5 show that by applying the standard purification procedure for VWF on UNOsphere S the removal capacity for non-enveloped viruses was insufficient for the different model viruses tested to claim a robust chromatographic step for removal of non-lipid enveloped viruses.

<u>Table 5: VWF purification according to the standard procedure and the corresponding</u> reduction capacities for non-enveloped viruses.

	Reduction	Comment
	$Log_{10}$	Virus Characteristics
PPV (porcine Parvovirus)	<1	small, DNA virus
hAdV (human Adenovirus)	1.8	large, DNAvirus
EMCV (Enzephalo Myocarditis	<1	small, RNA
Virus)		
Reo Virus Type III	1.8	large, RNA
MMV (mouse Minute Virus)	<1	small, DNA

[0100] The reduction rate is calculated as the total virus load in the load fraction divided by the total virus load in the eluate fraction expressed in logarithmic values.

[0101] The term "comprise" and variants of the term such as "comprises" or "comprising" are used herein to denote the inclusion of a stated integer or stated integers but not to exclude any other integer or any other integers, unless in the context or usage an exclusive interpretation of the term is required.

[0102] Any reference to publications cited in this specification is not an admission that the disclosures constitute common general knowledge in Australia.

#### **CLAIMS:**

1. A method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the protein-containing solution to a cation exchange resin at a pH of at least 1.6 units above the isoelectric point of a protein in the protein-containing solution; and

washing the cation exchange resin with a wash buffer to form an eluate, said wash buffer having a pH that is lower than the pH of the protein-containing solution applied to the cation exchange resin but having a pH higher than the isoelectric point of the protein, wherein the protein in the protein-containing solution has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

- 2. The method of claim 1 wherein the protein-containing solution applied to the cation exchange resin is at least 1.8 pH units above the isoelectric point of the protein in the proteincontaining solution.
- A method for removing a non-lipid enveloped virus from a protein-containing 3. solution comprising:

applying the protein-containing solution to a cation exchange resin;

washing the cation exchange resin with a first wash buffer having a pH higher than the pH of the protein-containing solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein; and

washing the cation exchange resin with a second wash buffer to form an eluate, said eluate having a pH that is equal to or lower than the first wash buffer, wherein the protein in the proteincontaining solution has a molecular mass of at least about 150 kilodaltons, and whereby the nonlipid enveloped virus is removed from the protein-containing solution.

- 4. The method of claim 3 wherein the pH of the first wash buffer is at least 1 pH unit above the isoelectric point of the protein in the protein-containing solution applied to the cation exchange resin.
- A method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the solution to a cation exchange resin at a pH higher than the isoelectric point of the protein in the protein-containing solution; and

washing the cation exchange resin with a first wash buffer at a pH higher than the isoelectric point of the protein in the protein-containing solution applied to the cation exchange resin; and

washing the cation exchange resin with a second wash buffer to form an eluate, said eluate having a pH that is equal to or lower than the pH of the first wash buffer, wherein the protein in the protein-containing solution has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

- 6. The method of claim 5 wherein the protein-containing solution applied to the cation exchange resin is at least 1 pH unit above the isoelectric point of the protein in the proteincontaining solution.
- 7. The method of claim 5 wherein the pH of the first wash buffer is at least 1 pH unit above the pH of the protein-containing solution applied to the cation exchange resin.
- 8. The method of any one of claims 2, 4, 6 and 7 wherein the pH of the proteincontaining solution applied to the cation exchange resin is greater than pH 7.0.
- 9. The method of any one of claims 1-8, wherein the cation exchange resin has a negatively charged group selected from the group consisting of carboxymethyl (CM), sulphoalkyl (SP, SE), sulfated esters of cellulose, heparin and methylsulfonate (S).
- 10. The method of any one of claims 1-9, wherein the protein in the protein-containing solution is a blood coagulation protein.
- 11. The method of claim 10, wherein the blood coagulation protein is selected from the group consisting of Factor VIII and von Willebrand factor.
- 12. A method for removing a non-lipid enveloped virus from a von Willebrand Factor (VWF)-containing solution comprising:

applying the VWF-containing solution to a cation exchange resin at a pH of at least 1.6 units above the isoelectric point of VWF; and

washing the cation exchange resin with a first wash buffer to form an eluate, said wash buffer having a pH that is equal to or lower than the pH of the VWF-containing solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein, and whereby the non-lipid enveloped virus is removed from the VWF-containing solution.

- 13. The method of claim 3, wherein the protein is von Willebrand Factor (VWF).
- 14. The method of claim 5, wherein the protein is von Willebrand Factor (VWF).
- 15. The method of claim 1, wherein the protein-containing solution applied to the cation exchange resin is at least 2 pH units above the isoelectric point of the protein in the protein-containing solution.
- 16. A method for removing a non-lipid enveloped virus from a protein-containing solution comprising:

applying the protein-containing solution to a cation exchange resin, wherein the pH of the protein-containing solution is at least 2.0 pH units or more above the isoelectric point of a protein in the protein-containing solution; and

washing the cation exchange resin with a wash buffer to form an eluate, said wash buffer having a pH that is equal to or lower than the pH of the solution applied to the cation exchange resin and having a pH higher than the isoelectric point of the protein, wherein the protein has a molecular mass of at least about 150 kilodaltons, and whereby the non-lipid enveloped virus is removed from the protein-containing solution.

17. The method of claim 16, wherein the pH of the protein containing-containing solution and the pH of the wash buffer is about 9.0.

Date: 30 January 2015



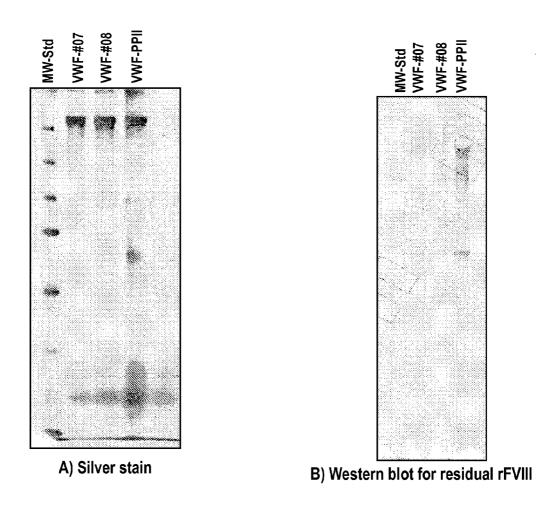
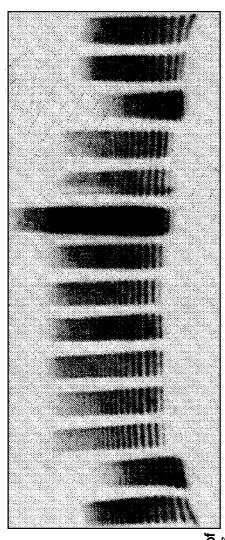


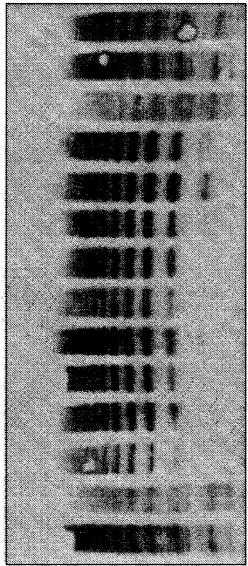
FIG. 1

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- 🕰 normal human plasma
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- ORVWSEC07004A Pool
- ₩F\_VR\_UnoSO3 Eluate
- **♥ VWF\_VR\_UnoSO2 Eluate**
- **≈** VWF\_VR\_UnoSO2 Load
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- ⇔ cryoprecipitate
- 🕰 normal human plasma

Number of



normal human plasma

normal human plasma

cryoprecipitate

VWF\_VR\_UnoSO4 Eluate

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ORVWSEC07004A Pool

VWF\_VR\_UnoSO3 Eluate

VWF\_VR\_UnoSO3 Load

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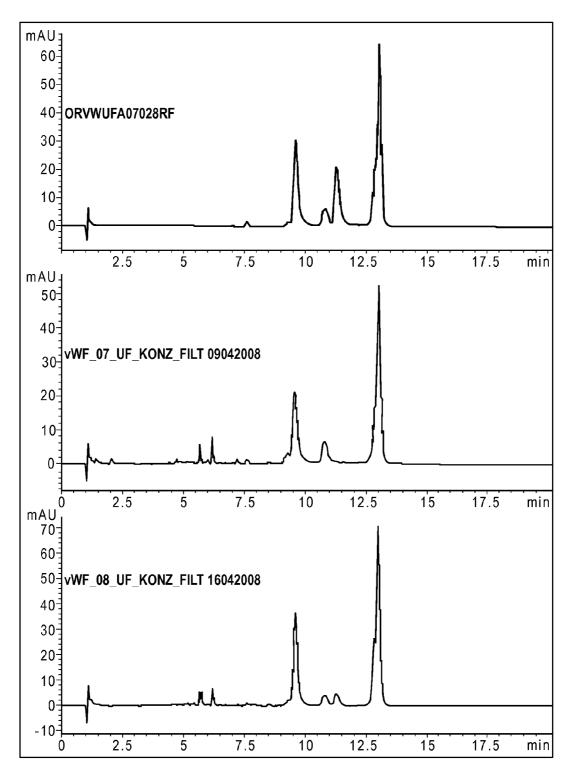


FIG. 4

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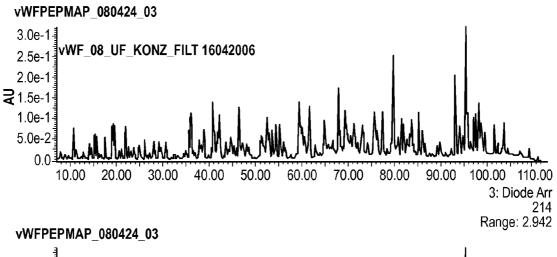
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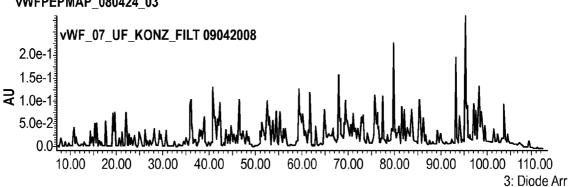
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FIG. 5

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Page 9

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Gin Thr Leu Leu Lys Ser His Arg Val Asn Cys Asp Arg Gly Leu 1910 1915 1920 Arg Pro Ser Cys Pro Asn Ser Gin Ser Pro Val Lys Val Giu Giu 1925 1930 1935 Thr Cys Gly Cys Arg Trp Thr Cys Pro Cys Val Cys Thr Gly Ser 1940 1945 1950 Ser Thr Arg His IIe Val Thr Phe Asp Gly Gln Asn Phe Lys Leu 1960 Thr Gly Ser Cys Ser Tyr Val Leu Phe Gln Asn Lys Glu Gln Asp 1970 1975 1980 1975 Leu Glu Val II e Leu His Asn Gly Ala Cys Ser Pro Gly Ala Arg Gin Gly Cys Met Lys Ser IIe Glu Val Lys His Ser Ala Leu Ser Val Glu Leu His Ser Asp Met Glu Val Thr Val Asn Gly Arg Leu Val Ser Val Pro Tyr Val Gly Gly Asn Met Glu Val Asn Val Tyr Gly Ala II e Met His Glu Val Arg Phe Asn His Leu Gly His II e 2050 2045 Phe Thr Phe Thr Pro Gln Asn Asn Glu Phe Gln Leu Gln Leu Ser Pro Lys Thr Phe Ala Ser Lys Thr Tyr Gly Leu Cys Gly IIe Cys 2075 2085 Asp Gu Asn Gy Ala Asn Asp Phe Met Leu Arg Asp Gy Thr Val 2095 Thr Thr Asp Trp Lys Thr Leu Val Gin Giu Trp Thr Val Gin Arg 2105 2110 Pro Gly Gln Thr Cys Gln Pro IIe Leu Glu Glu Gln Cys Leu Val 2120 2125 2130 Pro Asp Ser Ser His Cys Gin Val Leu Leu Leu Pro Leu Phe Ala 2135 2140 2145 Glu Cys His Lys Val Leu Ala Pro Ala Thr Phe Tyr Ala IIe Cys 2155 Page 13

Gin Gin Asp Ser Cys His Gin Giu Gin Val Cys Giu Val IIe Ala Ser Tyr Ala His Leu Cys Arg Thr Asn Gly Val Cys Val Asp Trp 2180 2185 Arg Thr Pro Asp Phe Cys Ala Met Ser Cys Pro Pro Ser Leu Val 2195 Tyr Asn His Cys Glu His Gly Cys Pro Arg His Cys Asp Gly Asn 2210 2215 2220 Val Ser Ser Cys Gly Asp His Pro Ser Glu Gly Cys Phe Cys Pro Pro Asp Lys Val Met Leu Glu Gly Ser Cys Val Pro Glu Glu Ala Cys Thr Gin Cys II e Gly Glu Asp Gly Val Gin His Gin Phe Leu Glu Ala Trp Val Pro Asp His Gln Pro Cys Gln Ile Cys Thr Cys Leu Ser Gly Arg Lys Val Asn Cys Thr Thr Gln Pro Cys Pro Thr Ala Lys Ala Pro Thr Cys Gly Leu Cys Glu Val Ala Arg Leu Arg 2300 Gin Asn Ala Asp Gin Cys Cys Pro Giu Tyr Giu Cys Val Cys Asp 2315 2320 2325 Pro Val Ser Cys Asp Leu Pro Pro Val Pro His Cys Glu Arg Gly 2330 2340 Leu Gin Pro Thr Leu Thr Asn Pro Gly Glu Cys Arg Pro Asn Phe 2345 2350 2355 Thr Cys Ala Cys Arg Lys Glu Glu Cys Lys Arg Val Ser Pro Pro 2360 2370 Ser Cys Pro Pro His Arg Leu Pro Thr Leu Arg Lys Thr Gln Cys 2375 2380 2385 2380 Cys Asp Glu Tyr Glu Cys Ala Cys Asn Cys Val Asn Ser Thr Val 2390 2395 2400 Ser Cys Pro Leu Gly Tyr Leu Ala Ser Thr Ala Thr Asn Asp Cys 2410 2415 Page 14

Gly Cys Thr Thr Thr Cys Leu Pro Asp Lys Val Cys Val His 2420 2430 Arg Ser Thr IIe Tyr Pro Val Gly Gln Phe Trp Glu Glu Gly Cys 2435 2440 2445 Asp Val Cys Thr Cys Thr Asp Met Glu Asp Ala Val Met Gly Leu 2450 2460 Arg Val Ala Gin Cys Ser Gin Lys Pro Cys Giu Asp Ser Cys Arg 2470 Ser Gly Phe Thr Tyr Val Leu His Glu Gly Glu Cys Cys Gly Arg 2480 2485 2490 2485 Cys Leu Pro Ser Ala Cys Glu Val Val Thr Gly Ser Pro Arg Gly Asp Ser Gin Ser Ser Trp Lys Ser Val Gly Ser Gin Trp Ala Ser 2510 2515 2520 Pro Glu Asn Pro Cys Leu IIe Asn Glu Cys Val Arg Val Lys Glu Gu Val Phe II e Gin Gin Arg Asn Val Ser Cys Pro Gin Leu Giu Val Pro Val Cys Pro Ser Gly Phe Gln Leu Ser Cys Lys Thr Ser 2555 Ala Cys Cys Pro Ser Cys Arg Cys Glu Arg Met Glu Ala Cys Met 2570 2575 2580 Leu Asn Gly Thr Val IIe Gly Pro Gly Lys Thr Val Met IIe Asp 2585 2590 2595 Val Cys Thr Thr Cys Arg Cys Met Val Gin Val Giy Val IIe Ser 2600 2610 Gly Phe Lys Leu Glu Cys Arg Lys Thr Thr Cys Asn Pro Cys Pro 2615 2620 2625 Leu Gly Tyr Lys Glu Glu Asn Asn Thr Gly Glu Cys Cys Gly Arg 2635 Cys Leu Pro Thr Ala Cys Thr lle Gin Leu Arg Gly Gin lle 2645 2655 2650 Met Thr Leu Lys Arg Asp Glu Thr Leu Gln Asp Gly Cys Asp Thr 2665 Page 15

His Phe 2675 Cys Lys Val Asn Glu Arg Gly Glu Tyr Phe Trp Glu Lys Arg Val Al Thr Gly Cys Pro Pro 2695 Phe Asp Glu His Lys 2700 Cys Leu Ala

Glu Gly Gly Lys IIe Met Lys IIe Pro Gly Thr Cys Cys Asp Thr 2705 2710 2715

Cys Glu Glu Pro Glu Cys Asn Asp IIe Thr Ala Arg Leu Gln Tyr 2720 2730

Val Lys Val Gly Ser Cys Lys Ser Glu Val Glu Val Asp IIe His 2735 2740 2745

Tyr Cys Gln Gly Lys Cys Ala Ser Lys Ala Met Tyr Ser IIe Asp 2750 2760

lle Asn Asp Val Gin Asp Gin Cys Ser Cys Cys Ser Pro Thr Arg 2765 2770 2775

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Arg Lys Cys Ser Lys 2810

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<212> PRT <213> Homo sapiens

<400> 3

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Asn Leu Arg Ala Glu Gly Leu Glu Cys Thr Lys Thr Cys Gln Asn Tyr 20 25 30

Asp Leu Glu Cys Met Ser Met Gly Cys Val Ser Gly Cys Leu Cys Pro 35 40 45

Pro Gly Met Val Arg His Glu Asn Arg Cys Val Ala Leu Glu Arg Cys 50 60

lle Gly Cys Asn Thr Cys Val Cys Arg Asp Arg Lys Trp Asn Cys Thr 85 90 95 Asp His Val Cys Asp Ala Thr Cys Ser Thr IIe Gly Met Ala His Tyr 100 105 110 Leu Thr Phe Asp Gly Leu Lys Tyr Leu Phe Pro Gly Glu Cys Gln Tyr 115 120 125 Val Leu Val Gin Asp Tyr Cys Giy Ser Asn Pro Giy Thr Phe Arg IIe 130 140 Leu Val Gly Asn Lys Gly Cys Ser His Pro Ser Val Lys Cys Lys Lys 145 150 155 160 Arg Val Thr II e Leu Val Glu Gly Glu II e Glu Leu Phe Asp Gly 165 170 175 Glu Val Asn Val Lys Arg Pro Met Lys Asp Glu Thr His Phe Glu Val 180 185 Val Glu Ser Gly Arg Tyr IIe IIe Leu Leu Leu Gly Lys Ala Leu Ser 195 200 205 Val Val Trp Asp Arg His Leu Ser IIe Ser Val Val Leu Lys Gin Thr Tyr G n G u Lys Val Cys G y Leu Cys G y Asn Phe Asp G y II e G n 225 235 240 Asn Asn Asp Leu Thr Ser Ser Asn Leu Gin Val Giu Giu Asp Pro Val Asp Phe Gly Asn Ser Trp Lys Val Ser Ser Gln Cys Ala Asp Thr Arg 260 265 270 Lys Val Pro Leu Asp Ser Ser Pro Ala Thr Cys His Asn Asn IIe Met Lys Gin Thr Met Val Asp Ser Ser Cys Arg IIe Leu Thr Ser Asp Val 290 295 300 Phe Gin Asp Cys Asn Lys Leu Val Asp Pro Giu Pro Tyr Leu Asp Val 305 310 315 320 Cys IIe Tyr Asp Thr Cys Ser Cys Glu Ser IIe Gly Asp Cys Ala Cys Phe Cys Asp Thr II e Ala Ala Tyr Ala His Val Cys Ala Gin His Gly 340 345 350

Val Thr Trp Arg Thr Ala Thr Leu Cys Pro Gin Ser Cys Glu 360 Gu Arg Asn Leu Arg Glu Asn Gly Tyr Glu Cys Glu Trp Arg Tyr Asn Ser Cys Ala Pro Ala Cys Gln Val Thr Cys Gln His Pro Glu Pro Leu 385 390 400 Ala Cys Pro Val Gin Cys Val Giu Giy Cys His Ala His Cys Pro Pro 405 410 415 Gly Lys II e Leu Asp Glu Leu Leu Gln Thr Cys Val Asp Pro Glu Asp Cys Pro Val Cys Glu Val Ala Gly Arg Arg Phe Ala Ser Gly Lys Lys 445 Thr Leu Asn Pro Ser Asp Pro Glu His Cys Gln IIe Cys His Cys 450 460 Asp Val Val Asn Leu Thr Cys Glu Ala Cys Gln Glu Pro Gly Gly Leu 465 470 480 Val Val Pro Pro Thr Asp Ala Pro Val Ser Pro Thr Thr Leu Tyr Val Glu Asp II e Ser Glu Pro Pro Leu His Asp Phe Tyr Cys Ser Arg Leu 500 510 Leu Asp Leu Val Phe Leu Leu Asp Gly Ser Ser Arg Leu Ser Glu Ala 515 Gu Phe Gu Val Leu Lys Ala Phe Val Val Asp Met Met Gu Arg Leu 530 Arg II e Ser Gin Lys Trp Val Arg Val Ala Val Val Giu Tyr His Asp Gly Ser His Ala Tyr IIe Gly Leu Lys Asp Arg Lys Arg Pro Ser Glu 565 570 575 Leu Arg Arg IIe Ala Ser Gln Val Lys Tyr Ala Gly Ser Gln Val Ala 580 585 590 Ser Thr Ser Glu Val Leu Lys Tyr Thr Leu Phe Gln Ile Phe Ser Lys lle Asp Arg Pro Glu Ala Ser Arg IIe Thr Leu Leu Leu Met Ala Ser

Gin Giu Pro Gin Arg Met Ser Arg Asn Phe Val Arg Tyr Val Gin Gly Leu Lys Lys Lys Val IIe Val IIe Pro Val Gly IIe Gly Pro His Ala Asn Leu Lys Gin Ile Arg Leu Ile Giu Lys Gin Ala Pro Giu Asn Lys Ala Phe Val Leu Ser Ser Val Asp Glu Leu Glu Gln Gln Arg Asp Glu II e Val Ser Tyr Leu Cys Asp Leu Ala Pro Glu Ala Pro Pro Pro 690 700 Thr Leu Pro Pro Asp Met Ala Gin Val Thr Val Giy Pro Giy Leu Leu 705 710 715 Gly Val Ser Thr Leu Gly Pro Lys Arg Asn Ser Met Val Leu Asp Val 725 730 735 Ala Phe Val Leu Glu Gly Ser Asp Lys IIe Gly Glu Ala Asp Phe Asn 740 745 Arg Ser Lys Glu Phe Met Glu Glu Val IIe Gln Arg Met Asp Val Gly 765 Gln Asp Ser IIe His Val Thr Val Leu Gln Tyr Ser Tyr Met Val Thr 770 780 Val Glu Tyr Pro Phe Ser Glu Ala Gln Ser Lys Gly Asp IIe Leu Gln 785 795 800 Arg Val Arg Glu II e Arg Tyr Gln Gly Gly Asn Arg Thr Asn Thr Gly 805 810 815 Leu Ala Leu Arg Tyr Leu Ser Asp His Ser Phe Leu Val Ser Gin Gly Asp Arg Glu Gln Ala Pro Asn Leu Val Tyr Met Val Thr Gly Asn Pro Ala Ser Asp Glu II e Lys Arg Leu Pro Gly Asp II e Gln Val Val Pro 850 855 860 lle Gly Val Gly Pro Asn Ala Asn Val Gln Glu Leu Glu Arg lle Gly Trp Pro Asn Ala Pro IIe Leu IIe Gin Asp Phe Giu Thr Leu Pro Arg 890

- Glu Ala Pro Asp Leu Val Leu Gln Arg Cys Cys Ser Gly Glu Gly Leu 900 905 910
- Gin II e Pro Thr Leu Ser Pro Ala Pro Asp Cys Ser Gin Pro Leu Asp 915 920 925
- Val II e Leu Leu Leu Asp Gly Ser Ser Ser Phe Pro Ala Ser Tyr Phe 930 940
- Asp Glu Met Lys Ser Phe Ala Lys Ala Phe IIe Ser Lys Ala Asn IIe 945 950 955 960
- Gly Pro Arg Leu Thr Gln Val Ser Val Leu Gln Tyr Gly Ser IIe Thr 965 970 975
- Thr II e Asp Val Pro Trp Asn Val Val Pro Glu Lys Ala His Leu Leu 980 985 990
- Ser Leu Val Asp Val Met Gin Arg Giu Giy Giy Pro Ser Gin Ile Giy 995 1000 1005
- Asp Ala Leu Gly Phe Ala Val Arg Tyr Leu Thr Ser Glu Met His 1010 1020
- Gly Ala Arg Pro Gly Ala Ser Lys Ala Val Val IIe Leu Val Thr 1025 1030 1035
- Asp Val Ser Val Asp Ser Val Asp Ala Ala Ala Asp Ala Ala Arg 1040 1045 1050
- Ser Asn Arg Val Thr Val Phe Pro IIe Gly IIe Gly Asp Arg Tyr 1055 1060 1065
- Asp Ala Ala Gin Leu Arg IIe Leu Ala Giy Pro Ala Giy Asp Ser 1070 1075 1080
- Asn Val Val Lys Leu Gin Arg IIe Giu Asp Leu Pro Thr Met Val 1085 1090 1095
- Thr Leu Gly Asn Ser Phe Leu His Lys Leu Cys Ser Gly Phe Val 1100 1105 1110
- Arg II e Cys Met Asp Glu Asp Gly Asn Glu Lys Arg Pro Gly Asp 1115 1120 1125
- Val Trp Thr Leu Pro Asp Gln Cys His Thr Val Thr Cys Gln Pro 1130 1140
- Asp Gly Gln Thr Leu Leu Lys Ser His Arg Val Asn Cys Asp Arg 1145 1150 1155

GГу	Leu 1160	Ar g	Pr o	Ser	Cys	Pr o 1165	Asn	Ser	GI n	Ser	Pr o 1170	Val	Lys	Val
Glu	Gl u 1175	Thr	Cys	GI y	Cys	Ar g 1180	Trp	Thr	Cys	Pr o	Cys 1185	Val	Cys	Thr
Зy	Ser 1190	Ser	Thr	Ar g	His	lle 1195	Val	Thr	Phe	Asp	Gl y 1200	GIn	Asn	Phe
Lys	Leu 1205	Thr	Glу	Ser	Cys	Ser 1210	Tyr	Val	Leu	Phe	GI n 1215	Asn	Lys	Gш
GIn	Asp 1220	Leu	Glu	Val	Пе	Leu 1225	His	Asn	GI y	Al a	Cys 1230	Ser	Pr o	GI y
Al a	Ar g 1235	Gl n	GI y	Cys	Met	Lys 1240	Ser	lle	Glu	Val	Lys 1245	His	Ser	Al a
Leu	Ser 1250	Val	Gl u	Leu	His	Ser 1255	Asp	Met	Glu	Val	Thr 1260	Val	Asn	GI y
Ar g	Leu 1265	Val	Ser	Val	Pr o	Tyr 1270	Val	Эgy	GI y	Asn	Met 1275	Glu	Val	Asn
Val	Tyr 1280	GI y	Al a	Пе	Met	Hi s 1285	G u	Val	Ar g	Phe	Asn 1290	Hi s	Leu	G y
His	II e 1295	Phe	Thr	Phe	Thr	Pr o 1300	Gi n	Asn	Asn	Gш	Phe 1305	Gin	Leu	G n
Leu	Ser 1310	Pr o	Lys	Thr	Phe	Al a 1315	Ser	Lys	Thr	Tyr	G y 1320	Leu	Cys	G y
lle	Cys 1325	Asp	G u	Asn	Gi y	Al a 1330	Asn	Asp	Phe	Met	Leu 1335	Ar g	Asp	G y
Thr	Val 1340	Thr	Thr	Asp	Tr p	Lys 1345	Thr	Leu	Val	Gп	G u 1350	Tr p	Thr	Val
GIn	Ar g 1355	Pr o	GГу	Gп	Thr	Cys 1360	Gп	Pr o	lle	Leu	G u 1365	Gi u	Gп	Cys
Leu	Val 1370	Pr o	Asp	Ser	Ser	Hi s 1375	Cys	Яп	Val	Leu	Leu 1380	Leu	Pr o	Leu
Phe	Al a 1385	Glu	Cys	His	Lys	Val 1390	Leu	Al a	Pr o	Al a	Thr 1395	Phe	Tyr	Al a
lle	Cys 1400	Gп	Gп	Asp	Ser	Cys 1405	His	Яп	Gш	Gп	Val 1410	Cys	Glu	Val

Ile Ala Ser Tyr Ala His Leu Cys Arg Thr Asn Gly Val Cys Val 1415 1420 1425 Asp Trp Arg Thr Pro Asp Phe Cys Ala Met Ser Cys Pro Pro Ser Leu Val Tyr Asn His Cys Glu His Gly Cys Pro Arg His Cys Asp 1445 1450 1455 Gly Asn Val Ser Ser Cys Gly Asp His Pro Ser Glu Gly Cys Phe 1460 1470 Cys Pro Pro Asp Lys Val Met Leu Glu Gly Ser Cys Val Pro Glu 1475 1480 1485 Gu Ala Cys Thr Gn Cys Ile Gy Gu Asp Gy Val Gn His Gn Phe Leu Glu Ala Trp Val Pro Asp His Gln Pro Cys Gln IIe Cys 1505 1510 Thr Cys Leu Ser Gly Arg Lys Val Asn Cys Thr Thr Gln Pro Cys 1520 1530 Pro Thr Ala Lys Ala Pro Thr Cys Gly Leu Cys Glu Val Ala Arg 1535 1540 Leu Arg Gin Asn Ala Asp Gin Cys Cys Pro Giu Tyr Giu Cys Val 1550 1560 Cys Asp Pro Val Ser Cys Asp Leu Pro Pro Val Pro His Cys Glu Arg Gly Leu Gln Pro Thr Leu Thr Asn Pro Gly Glu Cys Arg Pro 1580 1590 1585 Asn Phe Thr Cys Ala Cys Arg Lys Glu Glu Cys Lys Arg Val Ser 1595 Pro Pro Ser Cys Pro Pro His Arg Leu Pro Thr Leu Arg Lys Thr 1610 1620 Gin Cys Cys Asp Giu Tyr Giu Cys Ala Cys Asn Cys Val Asn Ser 1625 1630 1635 Thr Val Ser Cys Pro Leu Gly Tyr Leu Ala Ser Thr Ala Thr Asn Asp Cys Gly Cys Thr Thr Thr Cys Leu Pro Asp Lys Val Cys 1660

Val	His 1670	Ar g	Ser	Thr	Пе	Tyr 1675	Pr o	Val	G y	Gin	Phe 1680	Tr p	Gi u	Gш
Gl y	Cys 1685	Asp	Val	Cys	Thr	Cys 1690	Thr	Asp	Met	Glu	Asp 1695	Al a	Val	Met
Gi y	Leu 1700	Ar g	Val	Al a	GIn	Cys 1705	Ser	GIn	Lys	Pr o	Cys 1710	Gш	Asp	Ser
Cys	Ar g 1715	Ser	Gшy	Phe	Thr	Tyr 1720	Val	Leu	His	Gш	Gl y 1725	Gш	Cys	Cys
Glу	Ar g 1730	Cys	Leu	Pr o	Ser	Al a 1735	Cys	Gш	Val	Val	Thr 1740	Glу	Ser	Pr o
Ar g	Gl y 1745	Asp	Ser	GIn	Ser	Ser 1750	Tr p	Lys	Ser	Val	Gl y 1755	Ser	GIn	Tr p
Al a	Ser 1760	Pr o	Glu	Asn	Pr o	Cys 1765	Leu	Пе	Asn	Gш	Cys 1770	Val	Ar g	Val
Lys	Gl u 1775	Glu	Val	Phe	Пе	Gl n 1780	Яn	Ar g	Asn	Val	Ser 1785	Cys	Pr o	Яn
Leu	Gl u 1790	Val	Pr o	Val	Cys	Pr o 1795	Ser	GГу	Phe	Яn	Leu 1800	Ser	Cys	Lys
Thr	Ser 1805	Al a	Cys	Cys	Pr o	Ser 1810	Cys	Ar g	Cys	Gш	Ar g 1815	Met	Glu	Al a
Cys	Met 1820	Leu	Asn	Glу	Thr	Val 1825	Пе	GГу	Pr o	Зy	Lys 1830	Thr	Val	Met
lle	Asp 1835	Val	Cys	Thr	Thr	Cys 1840	Ar g	Cys	Met	Val	Gl n 1845	Val	Glу	Val
lle	Ser 1850	Glу	Phe	Lys	Leu	Gl u 1855	Cys	Ar g	Lys	Thr	Thr 1860	Cys	Asn	Pr o
Cys	Pr o 1865	Leu	Glу	Tyr	Lys	Gl u 1870	Glu	Asn	Asn	Thr	Gl y 1875	Glu	Cys	Cys
Gl y	Ar g 1880	Cys	Leu	Pr o	Thr	Al a 1885	Cys	Thr	Пе	Gl n	Leu 1890	Ar g	Gl y	Яy
Gln	II e 1895	Met	Thr	Leu	Lys	Ar g 1900	Asp	Glu	Thr	Leu	Gl n 1905	Asp	GI y	Cys
Asp	Thr 1910	His	Phe	Cys	Lys	Val 1915	Asn	Gi u	Ar g	GI y	G u 1920	Tyr	Phe	Trp

Glu Lys Arg Val Thr Gly Cys Pro Pro Phe Asp Glu His Lys Cys 1925 1930 1935

Leu Ala Glu Gly Gly Lys IIe Met Lys IIe Pro Gly Thr Cys Cys 1940 1950

Asp Thr Cys Glu Glu Pro Glu Cys Asn Asp IIe Thr Ala Arg Leu 1955 1960 1965

Gln Tyr Val Lys Val Gly Ser Cys Lys Ser Glu Val Glu Val Asp 1970 1975 1980

lle His Tyr Cys Gln Gly Lys Cys Ala Ser Lys Ala Met Tyr Ser 1985 1990 1995

lle Asp lle Asn Asp Val Gin Asp Gin Cys Ser Cys Cys Ser Pro 2000 2005 2010

Thr Arg Thr G u Pro Met G n Val Al a Leu His Cys Thr Asn G y 2015 2020 2025

Ser Val Val Tyr His Glu Val Leu Asn Ala Met Glu Cys Lys Cys 2030 2040

Ser Pro Arg Lys Cys Ser Lys 2045 2050