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(54) Titre : MACROMOLECULE AMPHIPHILE ET SON UTILISATION
(54) Title: AMPHIPHILIC MACROMOLECULE AND USES THEREOF

(57) Abrégé/Abstract:
The present invention provides an amphiphilic macromolecule and the use thereof. The amphiphilic macromolecules have repeating structural units: structural units to adjust molecular weight and molecular weight distribution and charging property effects, high stereo-hindrance structural units, and amphiphilic structural units, which are suitable for fields such as oil field well drilling, well cementation, fracturing, oil gathering and transfer, sewage treatment, sludge treatment and papermaking, etc., and can be used as an oil-displacing agent for enhanced oil production, a heavy oil viscosity reducer, a fracturing fluid, a clay stabilizing agent, a sewage treatment agent, a papermaking retention and drainage aid or a reinforcing agent, etc.

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Abstract

The present invention provides an amphiphilic macromolecule and the use thereof. The amphiphilic macromolecules have repeating structural units: structural units to adjust molecular weight and molecular weight distribution and charging property effects, high stereo-hindrance structural units, and amphiphilic structural units, which are suitable for fields such as oil field well drilling, well cementation, fracturing, oil gathering and transfer, sewage treatment, sludge treatment and papermaking, etc., and can be used as an oil-displacing agent for enhanced oil production, a heavy oil viscosity reducer, a fracturing fluid, a clay stabilizing agent, a sewage treatment agent, a papermaking retention and drainage aid or a reinforcing agent, etc.

Amphiphilic macromolecule and uses thereof

Technical Field

This invention relates to an amphiphilic macromolecule and uses thereof, and this amphiphilic macromolecule is applicable to oilfield drilling, well cementing, fracturing, crude oil gathering and transporting, sewage treating, sludge treating and papermaking, and it can be used as intensified oil producing agent and oil displacing agent, heavy oil viscosity reducer, fracturing fluid, clay stabilizer, sewage treating agent, retention aid and drainage aid and strengthening agent for papermaking.

Background of Invention

The solution viscosity and viscosity stability of the polymer used for tertiary oil recovery are important indicators to determine its using effect. Reservoir temperature, mineralization degree of formation water and injection water affect the viscosifying capacity of the polymer solution directly. For partially hydrolyzed polyacrylamide, although it has obvious viscosifying action in fresh water, the hydrodynamic radius of polymer macromolecules decreases with the increase of reservoir temperature, mineralization degree of formation water and injection water, in the meantime, the increase of the adsorption amount of this polymer on the surface of rocks also decrease the valid concentration of the solution, resulting a decline of the solution viscosity. Amphiphilic macromolecule is an important class of water-soluble polymer; by introducing a small amount of hydrophobic group on the hydrophilic macromolecular chains, an intramolecular or intermolecular hydrophobic interaction is generated, rendering the macromolecules to form a steric network structure, and thus has a remarkable viscosifying effect. By increasing the hydrophobic group content on the macromolecule chain or increasing the molecular weight, the impacts of high temperature and high salinity can be resisted to some extent; however, it may also result in deterioration of dissolving capacity of polymer, substantial increase of dissolving time, easy shear degradation of macromolecular chain and easy adsorption on the rock and other problems. Furthermore, with the increase of formation

temperature and water mineralization degree, these problems are particularly serious.

Heavy oil resource has become one of the important natural resources for strategic replacement, but it's difficult to exploit. The main reason is that the heavy oil is high in viscosity, high in gum, asphaltenes contents or wax content, not easily flow in formation, wellbore and pipeline. Additionally, because of the great oil-water mobility ratio, it will also cause fast water breakthrough, high water content, and easy formation sand production and other serious problems negatively affecting the oil production.

Nowadays, to keep the viscosifying properties and viscosity stability of the polymer solution, and to improve its ability for heavy oil emulsification, dispersion and viscosity-reduction have great significance on the enhance of crude oil recovery and the maximizing of tapping of the potential underground residual crude oil.

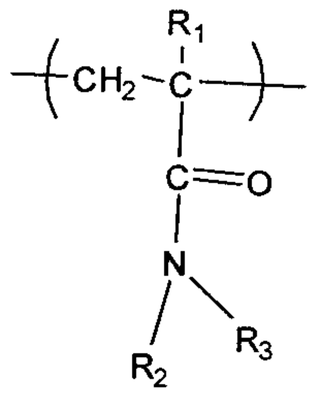
Brief Description of the Invention

In the following context of this invention, unless otherwise defined, the same variable group, and molecular and structural formula have the same definitions.

The instant invention relates to an amphiphilic macromolecule. This amphiphilic macromolecule has repeating units as described below: a structural unit A for adjusting molecular weight, molecular weight distribution and charge characteristics, a highly sterically hindered structural unit B and an amphiphilic structural unit C.

In an embodiment, the structural unit A for adjusting molecular weight, molecular weight distribution and charge characteristics comprises (meth)acrylamide monomer unit A_1 and/or (meth)acrylic monomer unit A_2. Preferably, the structural unit A includes (meth)acrylamide monomer unit A_1 and / or (meth)acrylic monomer unit A_2 simultaneously. In the art, the molecular weight of the amphiphilic macromolecule may be selected as needed, preferably, this molecular weight may be selected between 1000000-20000000.

Preferably, the (meth)acrylamide monomer unit A_1 has a structure of formula (1):



formula (1)

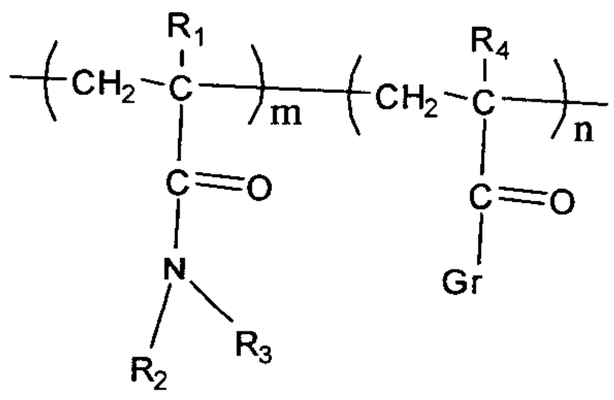
In formula (1), R_1 is H or a methyl group; R_2 and R_3 are independently selected from the group consisting of H and a C_1-C_3 alkyl group; R_2 and R_3 are preferably H.

Preferably, the (meth)acrylic monomer unit A_2 is (meth)acrylic acid and/or (meth)acrylate. Preferably the (meth)acrylate is sodium methacrylate.

Preferably, based on 100 mol% of the entire amphiphilic macromolecule repeating units, the molar percentage of (meth)acrylamide monomer unit A_1 is 70-99mol%; preferably 70-90mol%, more preferably 70-78mol%.

Preferably, the molar percentage of (meth)acrylic acid monomer unit A_2 in the whole amphiphilic polymer repeat unit is 1-30mol%; preferably 1-28mol%, and more preferably 20-28mol%.

In another embodiment, the structural unit A for the regulation of molecular weight, molecular weight distribution and charge characteristics has a structure of formula (2):



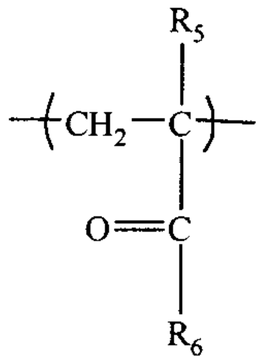
formula (2)

wherein, R_1 is H or a methyl group; R_2 and R_3 are independently selected from the group consisting of H and a C_1-C_3 alkyl group; R_2 and R_3 are preferably H; R_4 is selected from H or a methyl group; Gr is -OH or $-O^-Na^+$; m and n represent the molar percentages of the structural units in the entire amphiphilic macromolecule repeating unit, and m is 70-99mol%, preferably 70-90mol%, more preferably 70-78 mol%; n is 1-30mol%, preferably 1-28mol%, more preferably 20-28mol%.

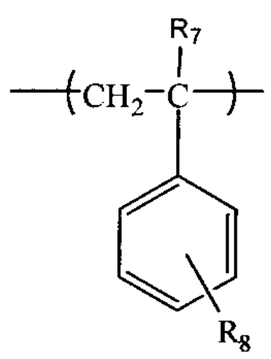
In another embodiment, in formula (2), R_1-R_3 are preferably H, and Gr is

preferably -O^-Na^+.

In another embodiment, the highly sterically hindered structural unit B contains at least a structure G, wherein the structure G is a cyclic hydrocarbon structure formed on the basis of two adjacent carbon atoms in the main chain, or is selected from a structure of formula (3), and the highly sterically hindered structural unit B optionally contains a structure of formula (4):

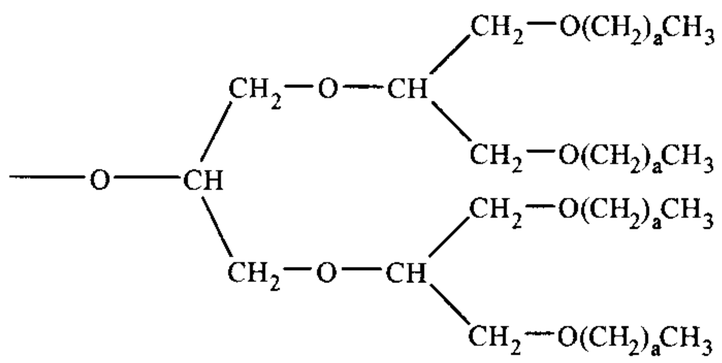


formula (3)

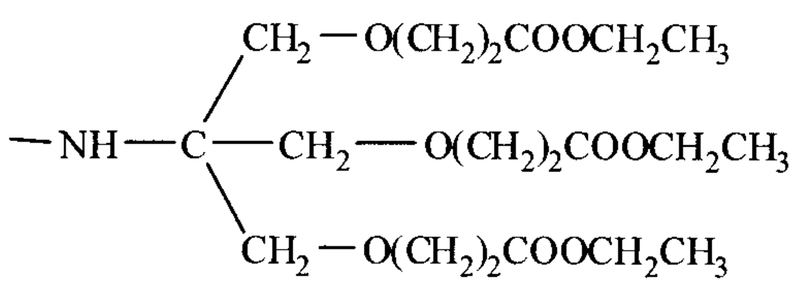


formula (4)

In formula (3), R_5 is H or a methyl group; preferably H; R_6 is a radical selected from the group consisting of the structures of formulas (5) and (6).



formula (5)



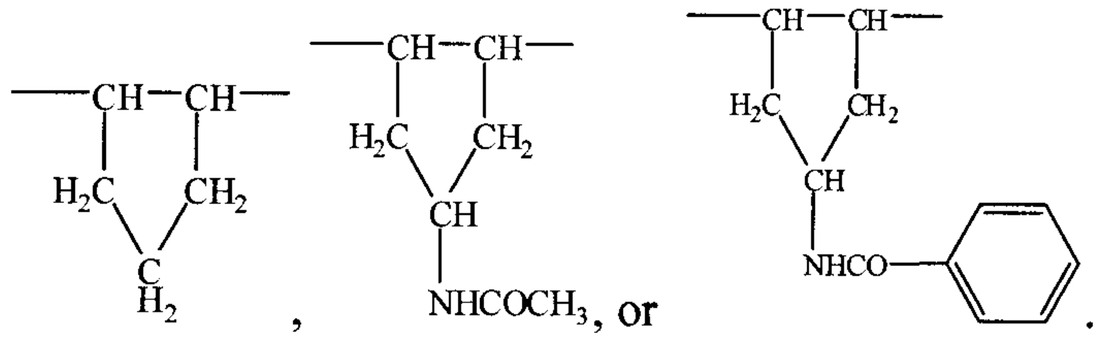
formula (6)

In formula (5), a is an integer from 1 to 11; preferably 1-7;

In formula (4), R_7 is H; R_8 is selected from H, -SO_3H and salts thereof, -$(CH_2)_2CH_3Cl$, -$CH_2N^+(CH_3)_2(CH_2)_\xi CH_3Cl^-$ or -$CH_2N^+(CH_3)_2(CH_2)_2N^+(CH_3)_2(CH_2)_\sigma$ CH_32Cl^-; ξ and σ are respectively integers from 1 to 15, preferably 1-11.

Preferably, the highly sterically hindered structural unit B comprises a structure G and a structure of formula (4).

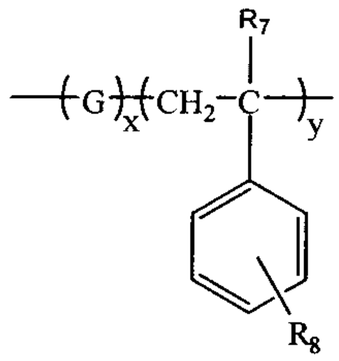
In another embodiment, the cyclic hydrocarbon structure formed on the basis of two adjacent carbon atoms in the main chain is selected from the group consisting of:



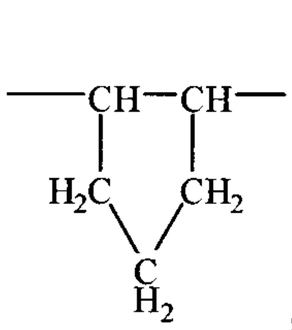
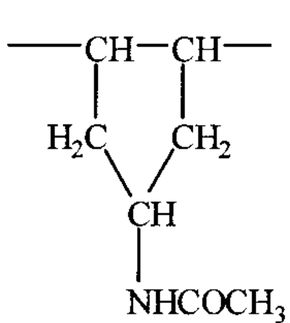
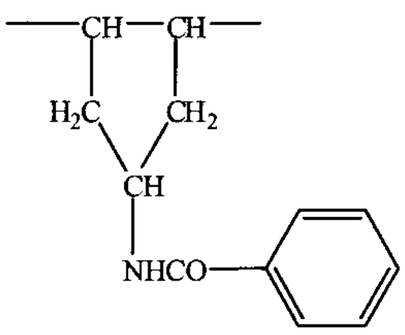
Preferably, the molar percentage of structure G of the highly sterically hindered structural unit B in the entire amphiphilic macromolecule repeating units is 0.02-2mol%; preferably 0.02-1.0mol%, more preferably 0.1-0.5 mol%.

Preferably, the molar percentage of the structure of formula (4) of the highly sterically hindered structural unit B in the entire amphiphilic macromolecule repeating units is 0.05-5mol%; preferably 0.1-2.5mol%, more preferably 0.1-1.5mol%.

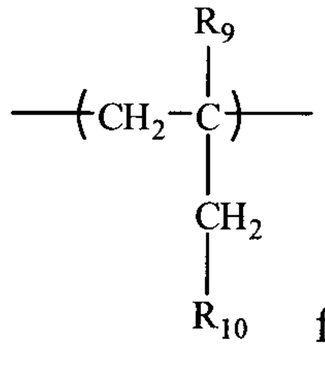
In another embodiment, the highly sterically hindered structural unit B has a structure of formula (7):



formula (7)

In formula (7), the definition on G is as described above, preferably the structure of formula (3),  ,  or  ; the definitions on R_7 and R_8 are as described in formula (4); x and y represent the molar percentages of the structure units in the entire amphiphilic macromolecule repeating units, and x is 0.02-2mol%, preferably 0.02-1.0mol%, more preferably 0.1-0.5mol%; y is 0.05-5 mol%, preferably 0.1-2.5mol%, and more preferably 0.1-1.5mol%.

In another embodiment, the amphiphilic structural unit C has a structure of formula (8):



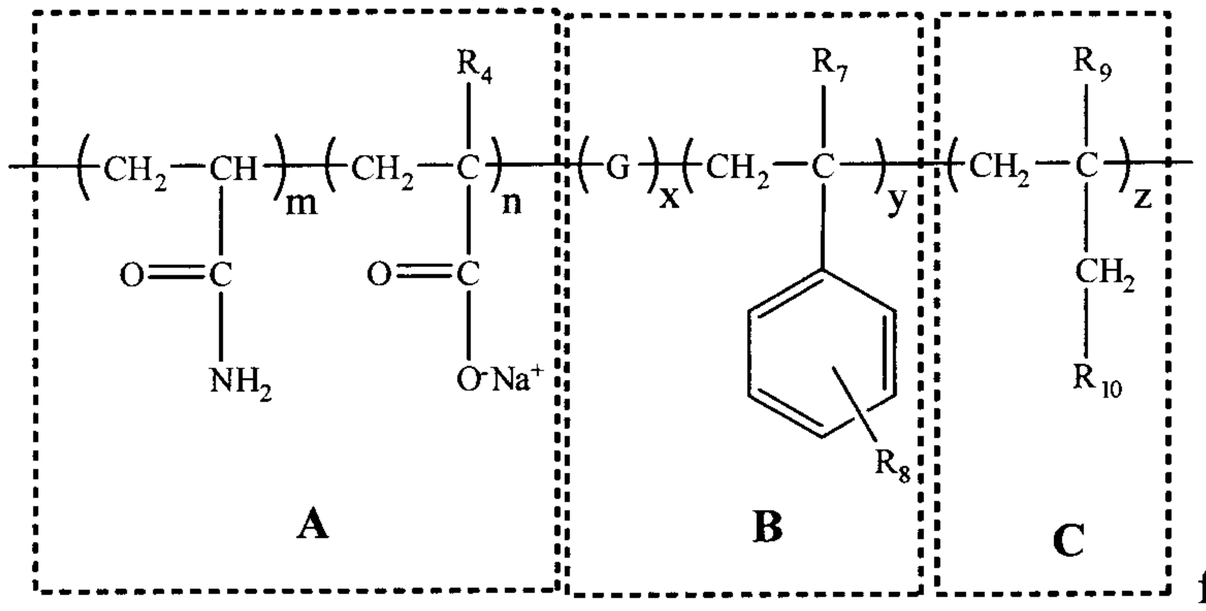
formula (8)

In formula (8), R_9 is H or a methyl group; R_{10} is $-N^+(CH_3)_2(CH_2)_rCH_3X^-$, $-N^+((CH_2)_sCH_3)_3X^-$ or $-N^+(CH_3)((CH_2)_tCH_3)_2X^-$; r is an integer from 3 to 21; s is an integer from 2 to 9; t is an integer from 3 to 15; X^- is Cl^-or Br^-. Preferably, r is from 3

to 17, s is from 2 to 5, t is from 3 to 11.

Preferably, the molar percentage of amphiphilic structural unit C in the entire amphiphilic macromolecule repeating units is 0.05-10mol%; preferably 0.1-5.0mol%, more preferably 0.5-1.5mol%.

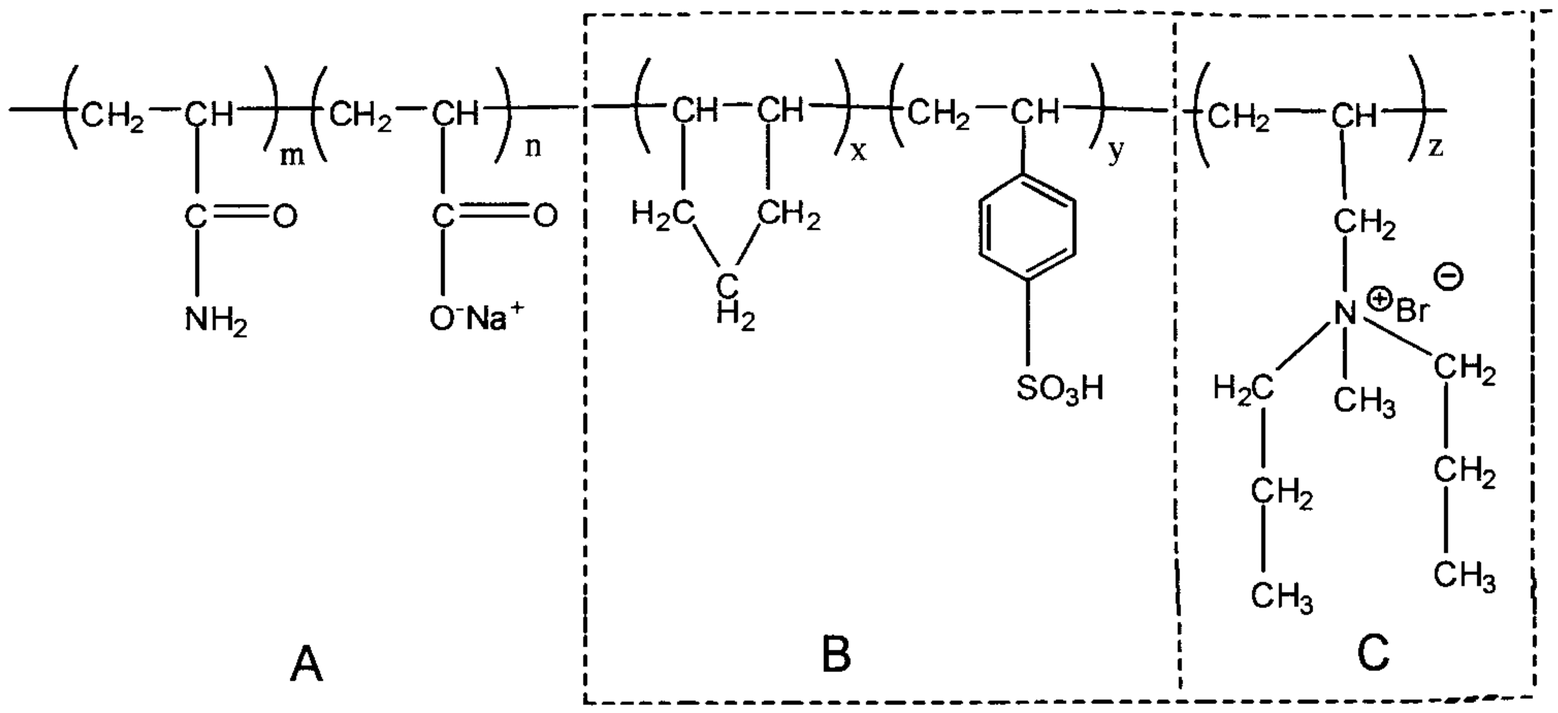
In another embodiment, the amphiphilic macromolecule has a structure of formula (9):



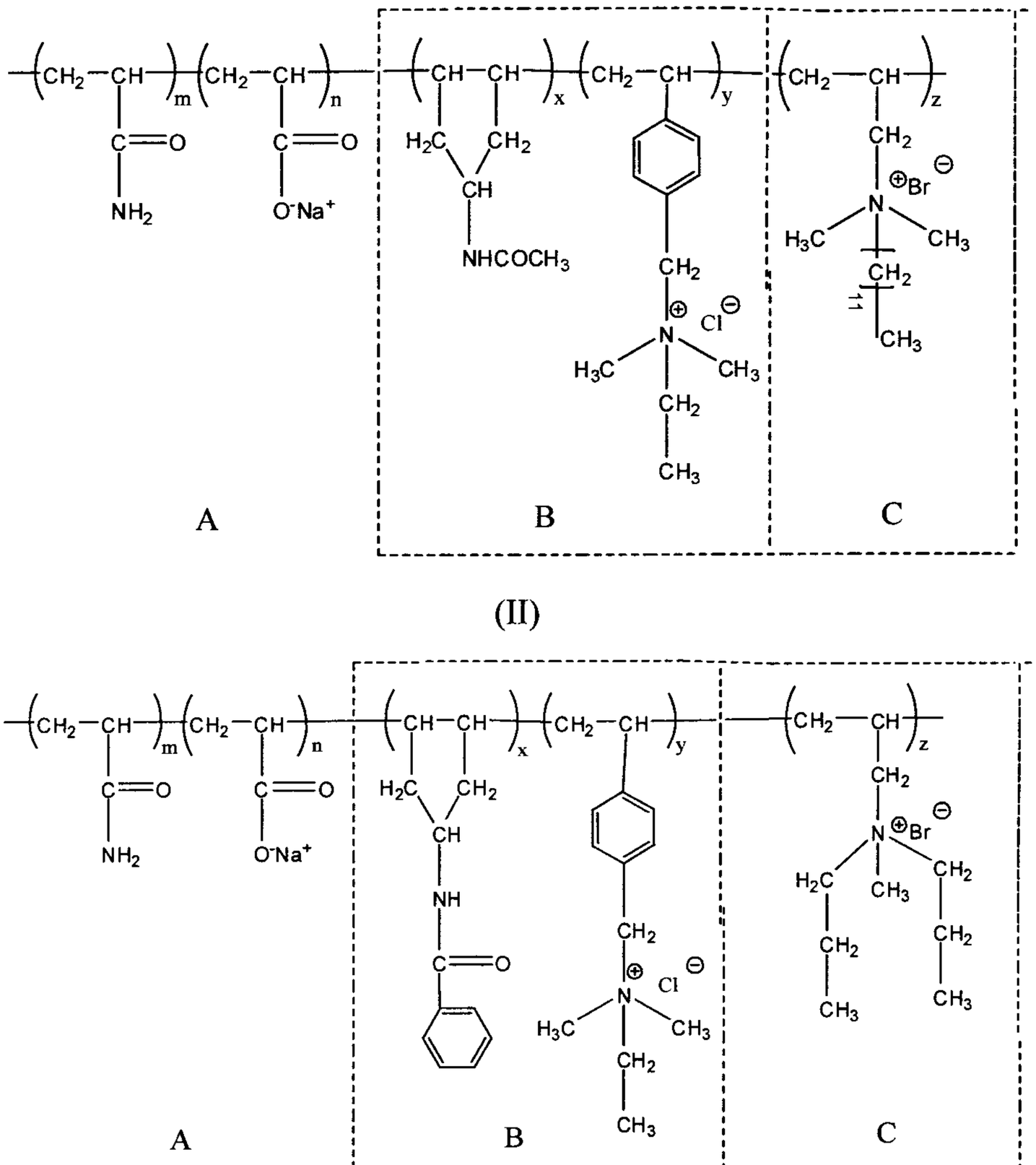
formula (9)

In formula (9), the definitions on R_4, m and n are as described in formula (2); the definitions on R_7, R_8, G, x and y are as described in formula (7); the definitions on R_9, and R_{10} are as described in formula (8); z represents the molar percentage of this structural unit in the entire amphiphilic macromolecule repeat units, and z is 0.05-10 mol%, preferably 0.1-5.0mol%, more preferably 0.5-1.5mol%.

Specifically, this present invention provides a high molecular compound having a structure of formulas (I)-(X):

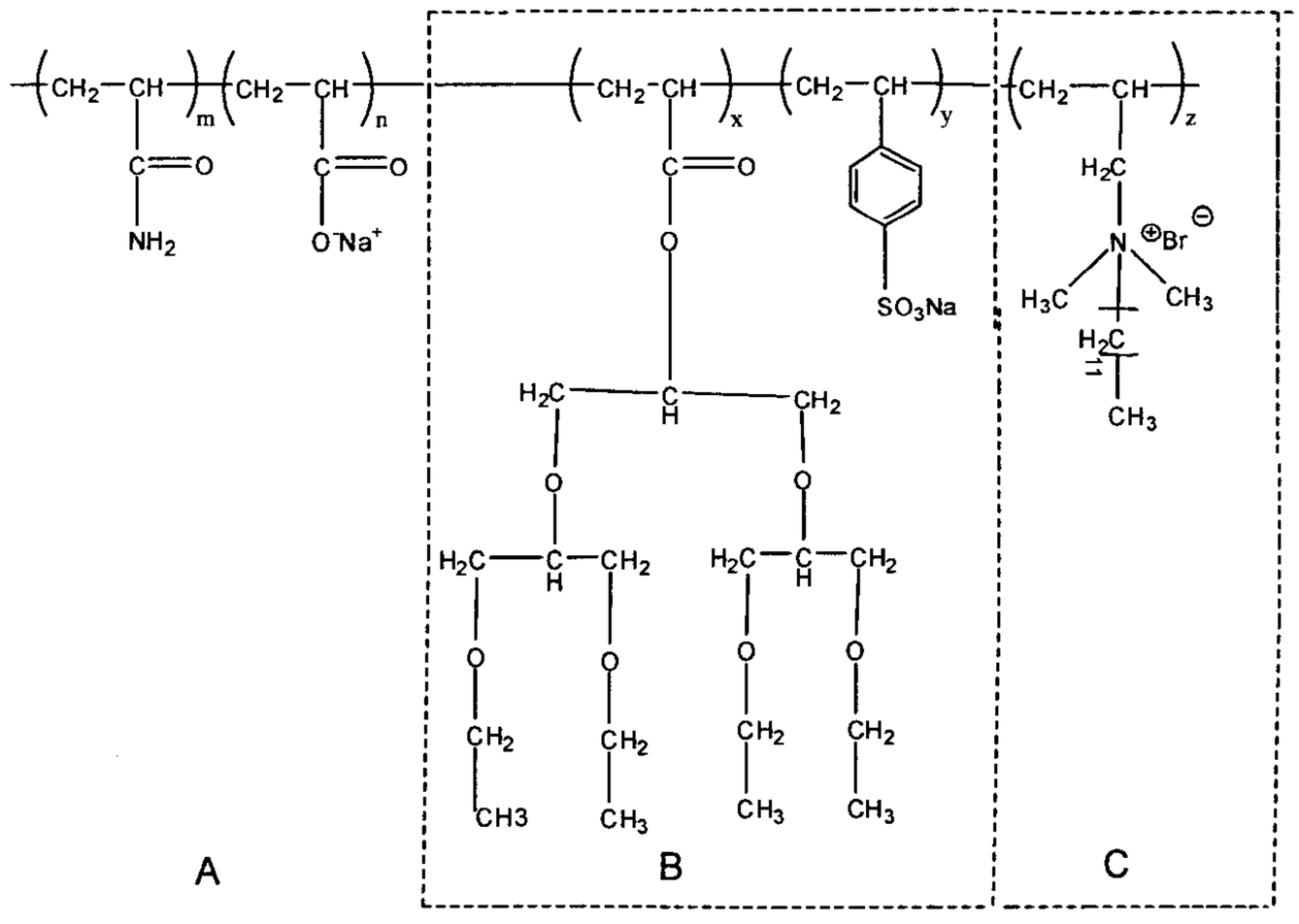


(I)

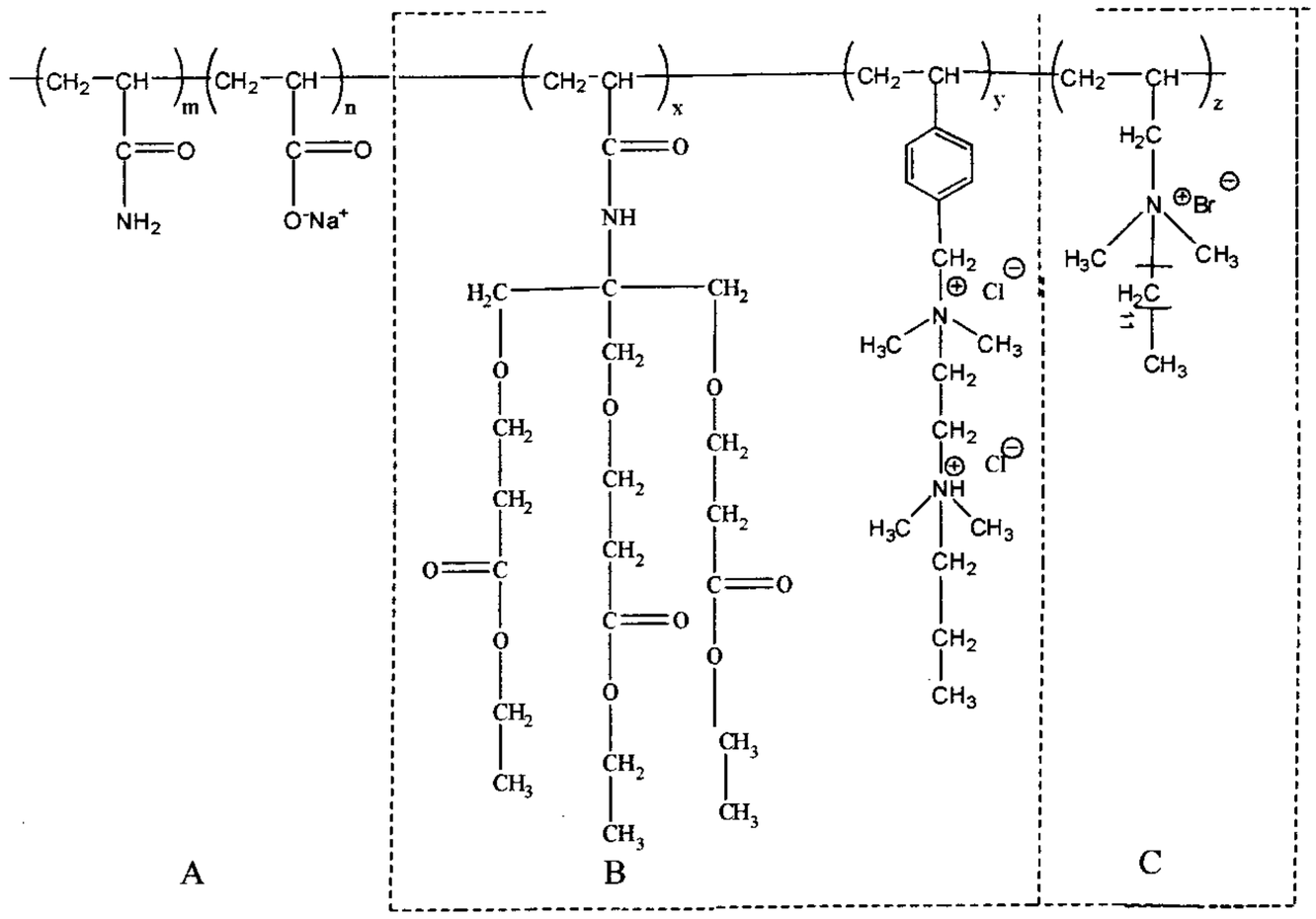


(II)

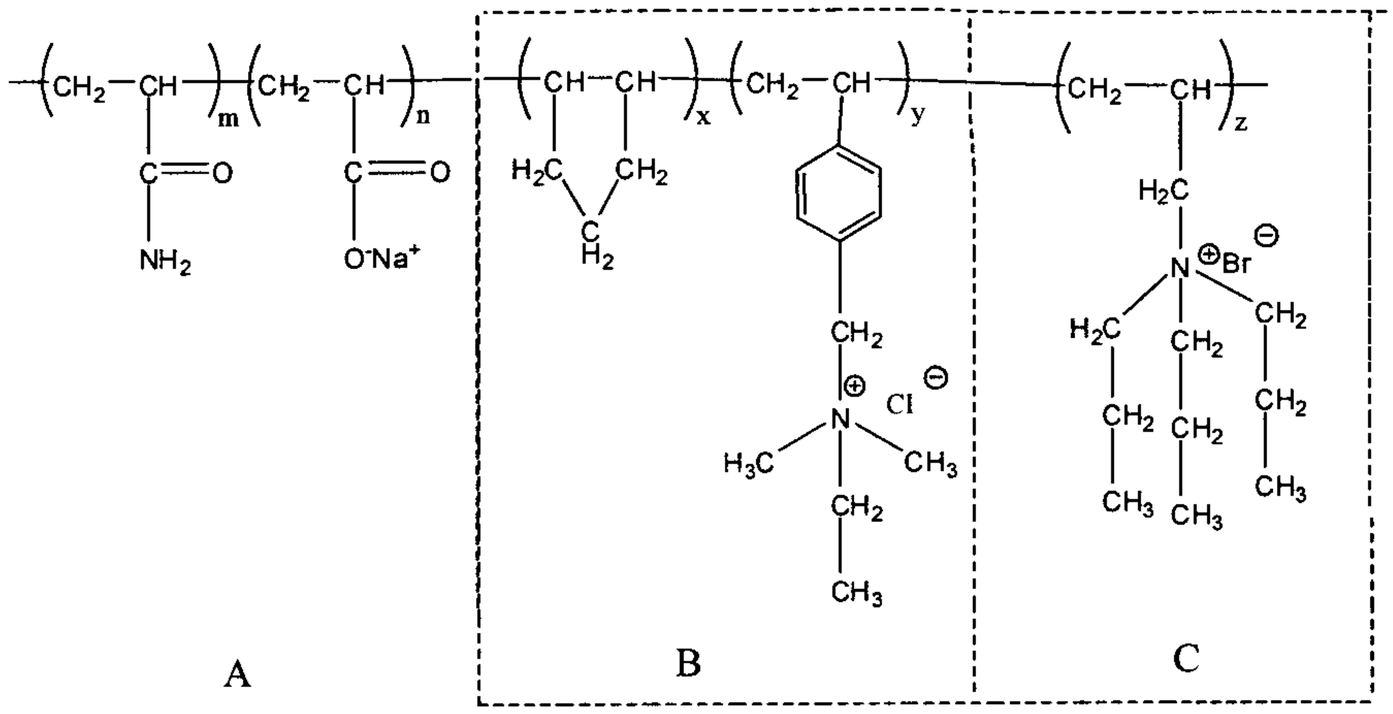
(III)



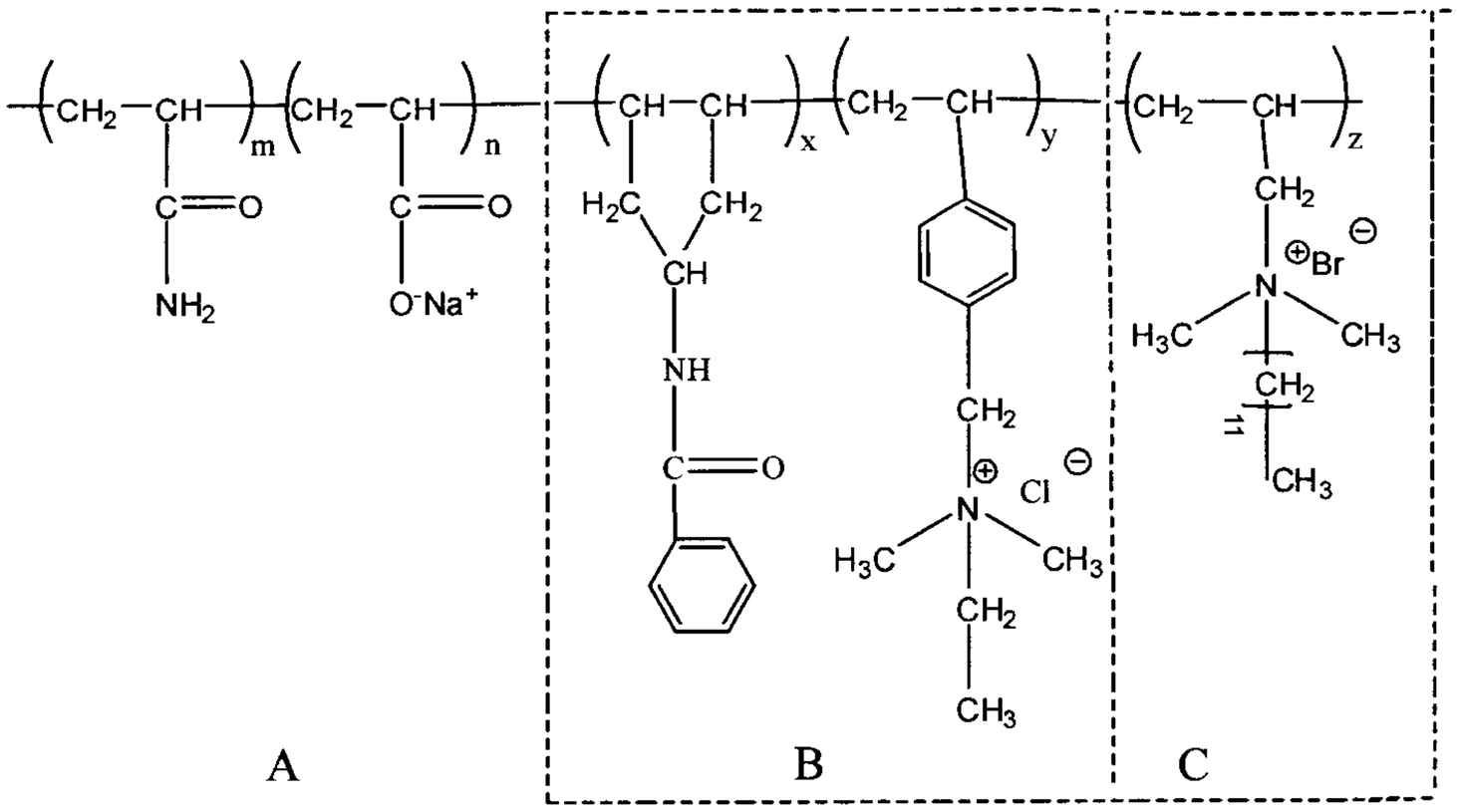
(IV)



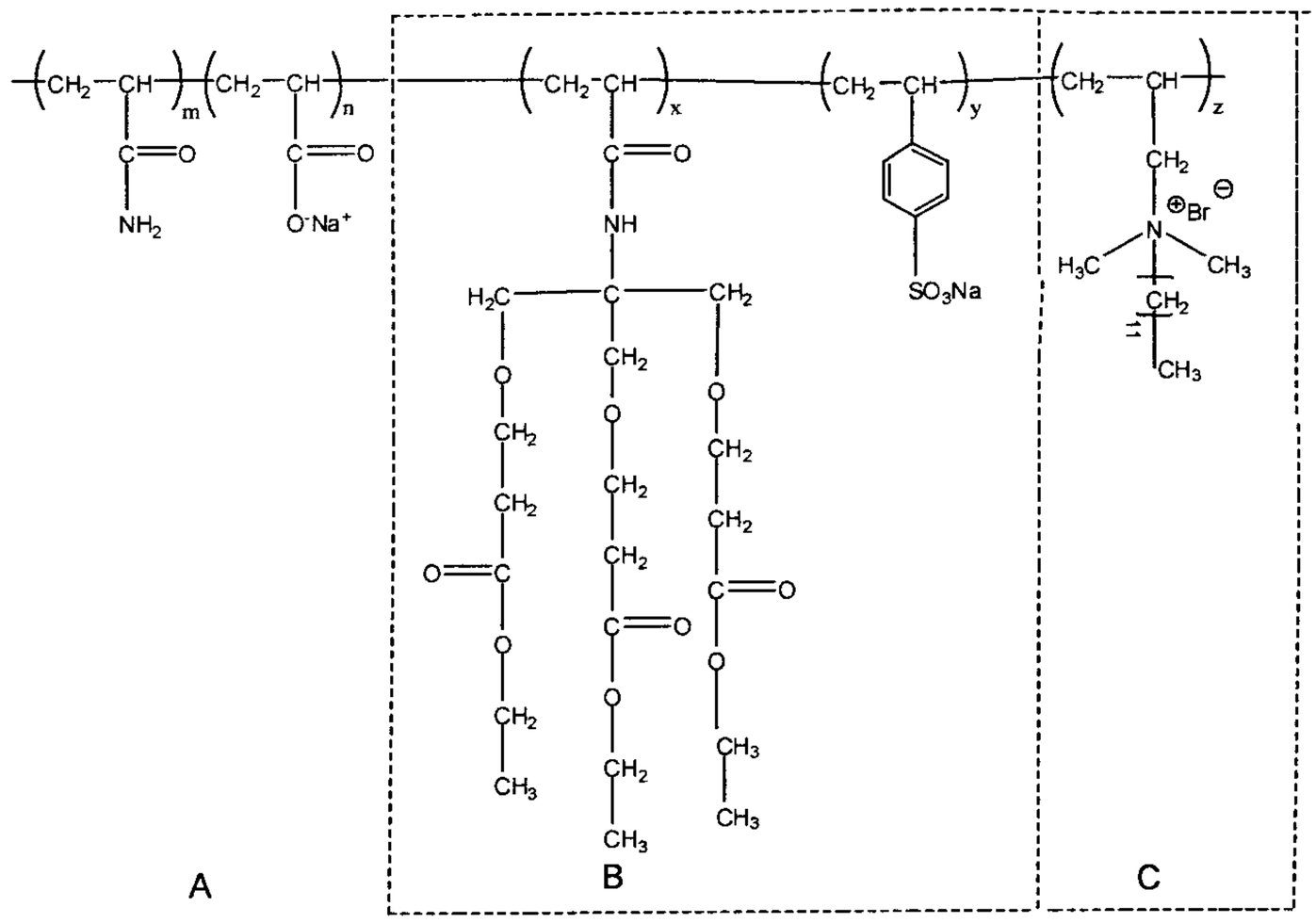
(V)



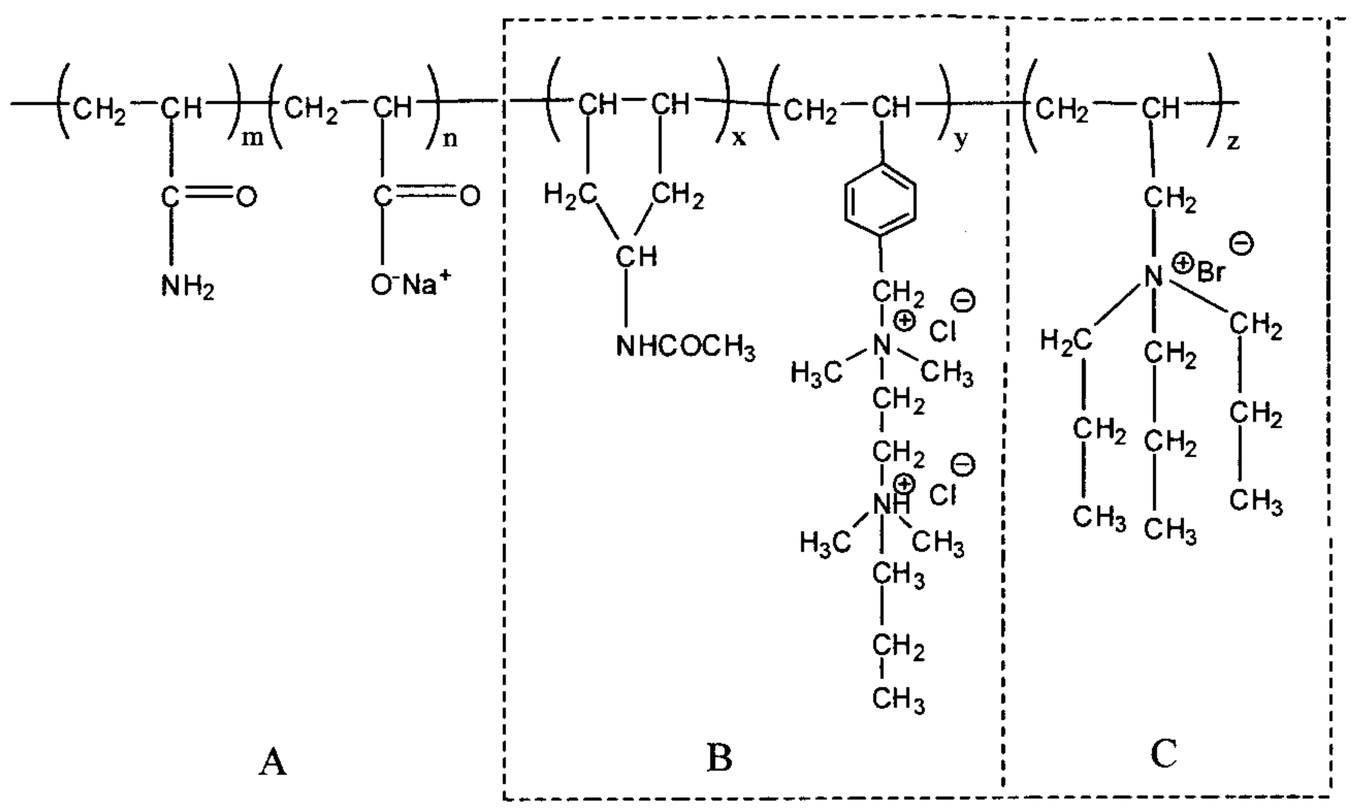
(VI)



(VII)

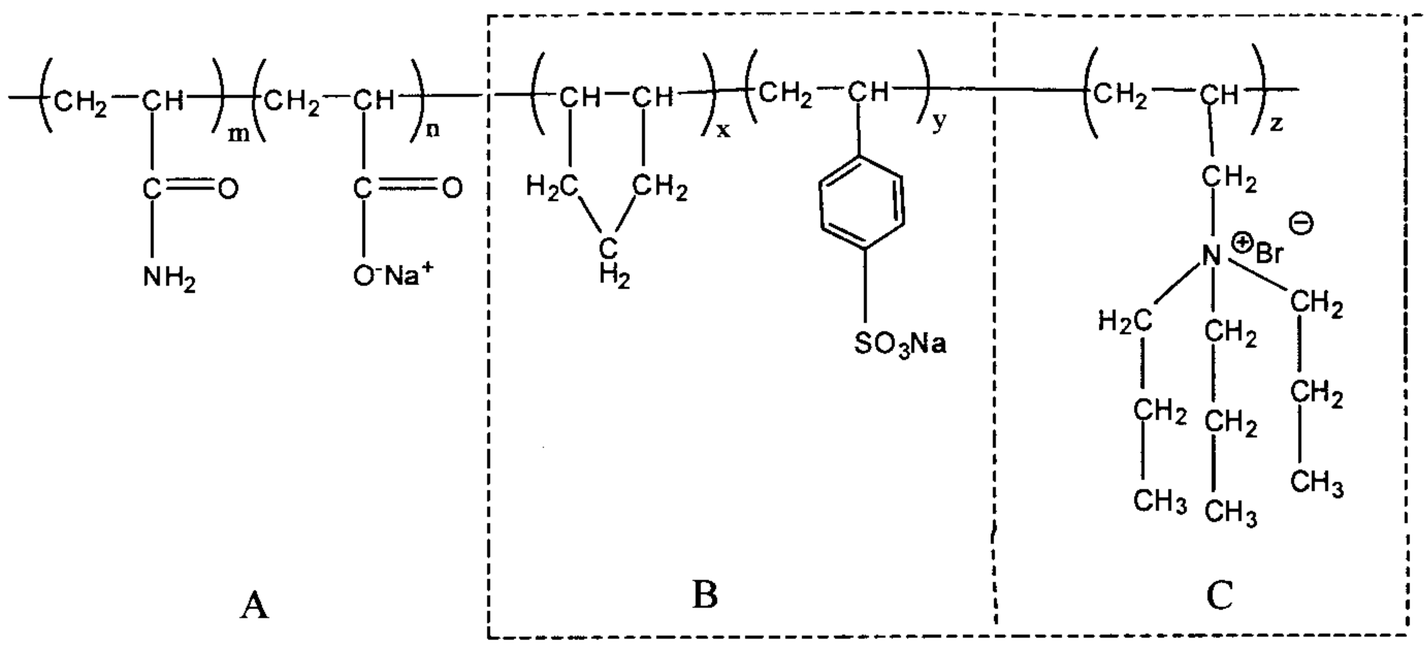


(VIII)



or

(IX)



(X)

The molecular weight of the amphiphilic macromolecule described above is between 1000000 and 20000000; preferably between 3000000 and 13000000.

The measurement of the molecular weight M is as follows: The intrinsic viscosity $[\eta]$ is measured by Ubbelohde viscometer as known in the art, then the obtained intrinsic viscosity $[\eta]$ value is used in the following equation to obtain the desired molecular weight M:

$$M = 802[\eta]^{1.25}$$

The amphiphilic macromolecule according to this present invention can be prepared by known methods in the art, for example, by polymerizing the structural unit for adjusting molecular weight, molecular weight distribution and charge characteristics, the highly sterically hindered structural unit and the amphiphilic structural unit in the presence of an initiator. The polymerization process can be any type well known in the art, such as, suspension polymerization, emulsion polymerization, solution polymerization, precipitation polymerization, etc.

A typical preparation method is as follows: the above monomers are each dispersed or dissolved in an aqueous system under stirring, the monomer mixture is polymerized by the aid of an initiator under nitrogen atmosphere to form the amphiphilic macromolecule. The so far existing relevant technologies for preparing an amphiphilic macromolecule can all be used to prepare the amphiphilic macromolecule of this invention.

All the monomers for preparing the amphiphilic macromolecule can be commercially available, or can be prepared on the basis of prior art technology directly, and some monomers' synthesis are described in details in specific examples.

Description of Figures

Figure 1 depicts the relationship of viscosity vs. concentration of the amphiphilic macromolecules obtained from examples 1-5 of the invention in saline having a degree of mineralization of 1×10^4 mg/L at a temperature of 60□.

Figure 2 depicts the relationship of viscosity vs. temperature of the amphiphilic

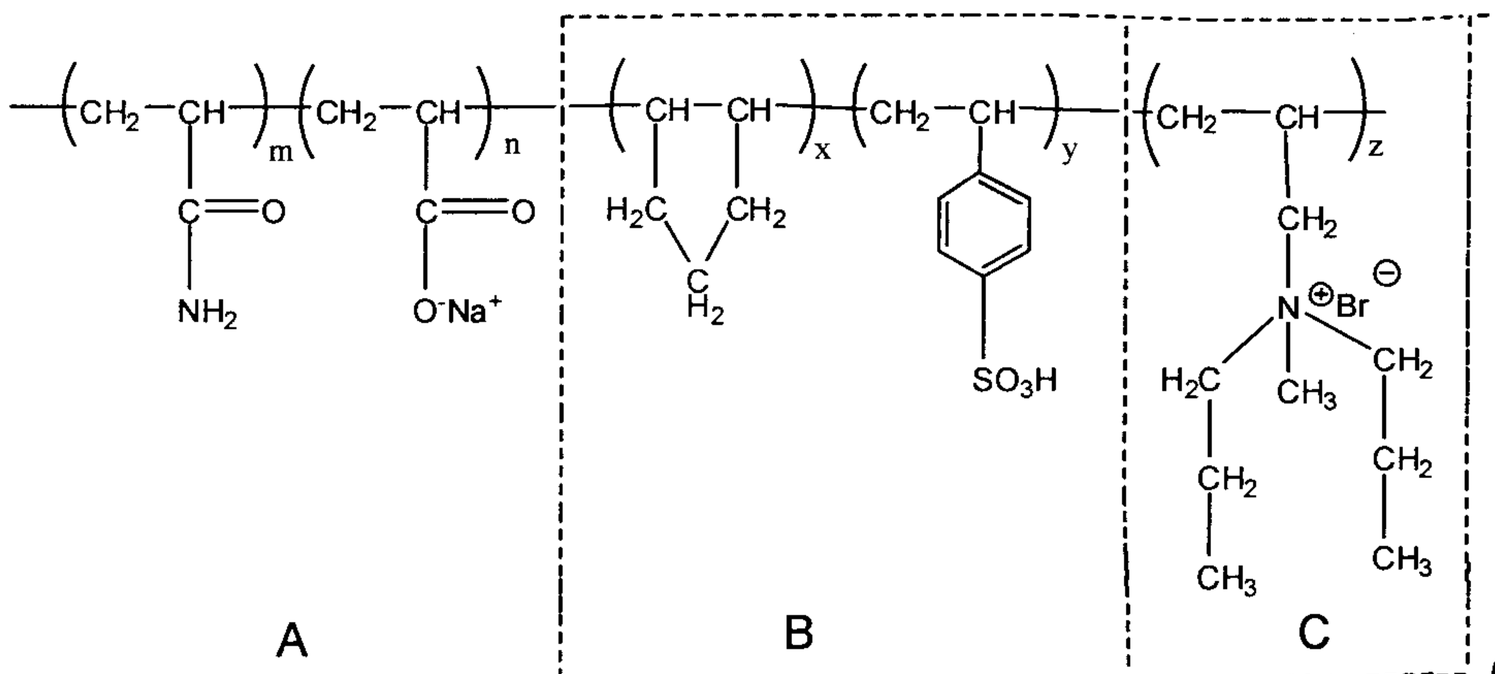
macromolecules obtained from the examples 1-5 of the invention in saline having a degree of mineralization of 1×10^4 mg/L at the concentration of 1750mg/L.

Detailed Description of the Invention

The present invention is further illustrated below by combining specific examples; however, this invention is not limited to the following examples.

Example 1

This example synthesized the amphiphilic macromolecule of formula (I):



(I)

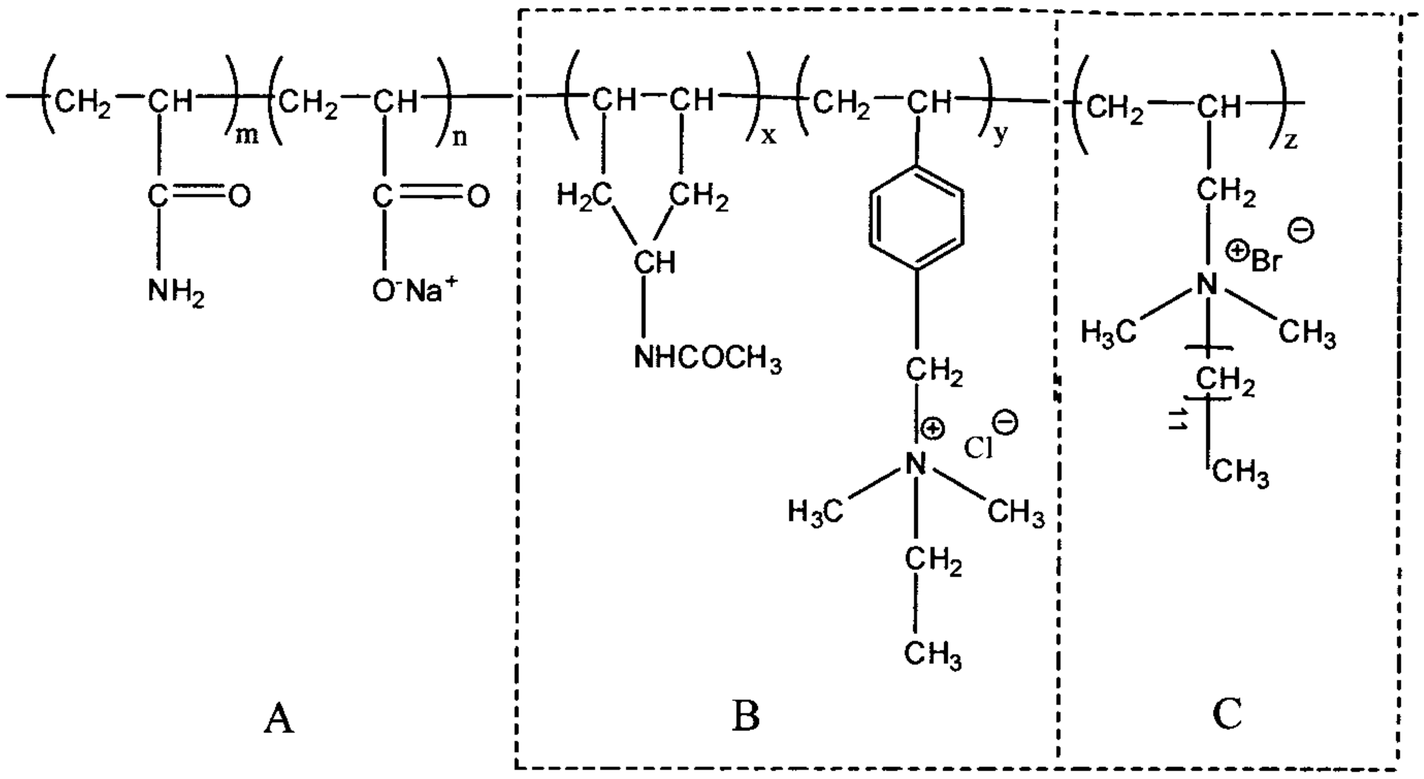
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 78%, 20%, 0.25%, 0.5%, 1.25% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 18□; after 5 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight

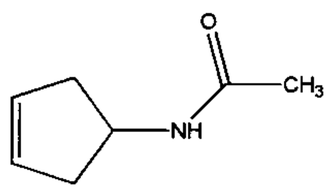
of the amphiphilic macromolecule was 970×10^4.

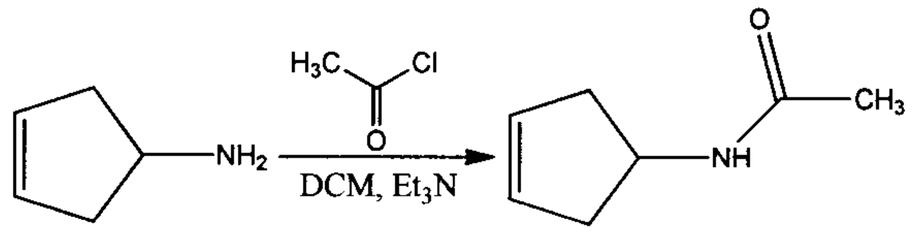
Example 2

This example synthesized the amphiphilic macromolecule of formula (II):



(II)

The synthesis route of the monomer  was as follows:



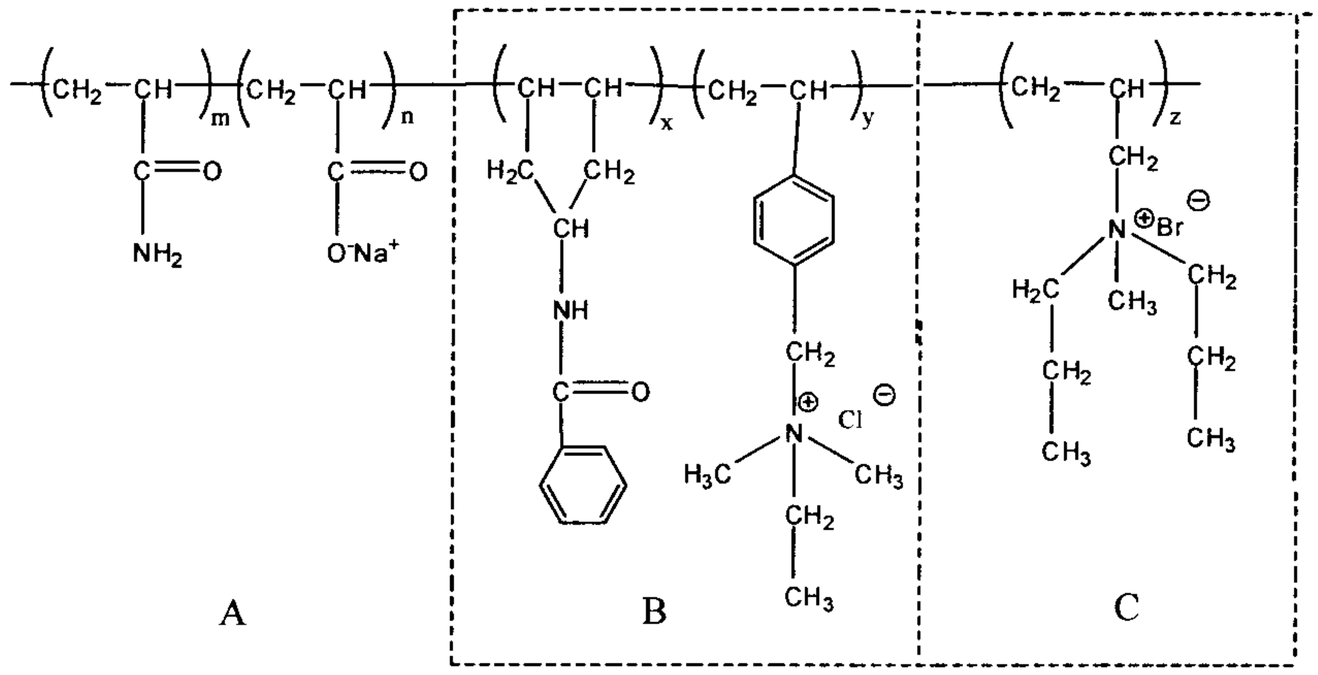
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 75%, 23%, 0.25%, 0.25%, 1.5% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 40 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 22□; after 5 hours, the reaction was ended with a complete conversion. After the drying of the obtained

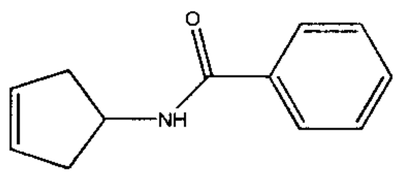
product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 1030×10^4.

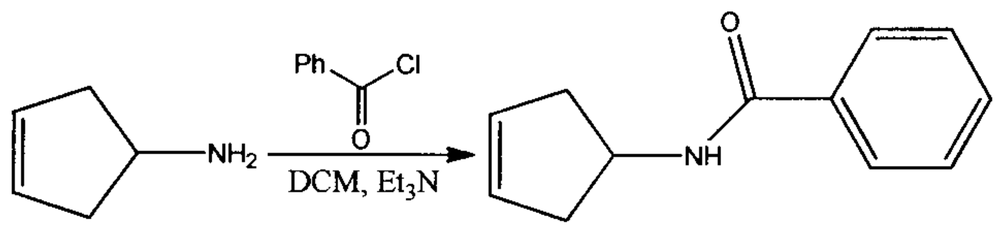
Example 3

This example synthesized the amphiphilic macromolecule of formula (III):



(III)

The synthesis route of the monomer  was as follows:



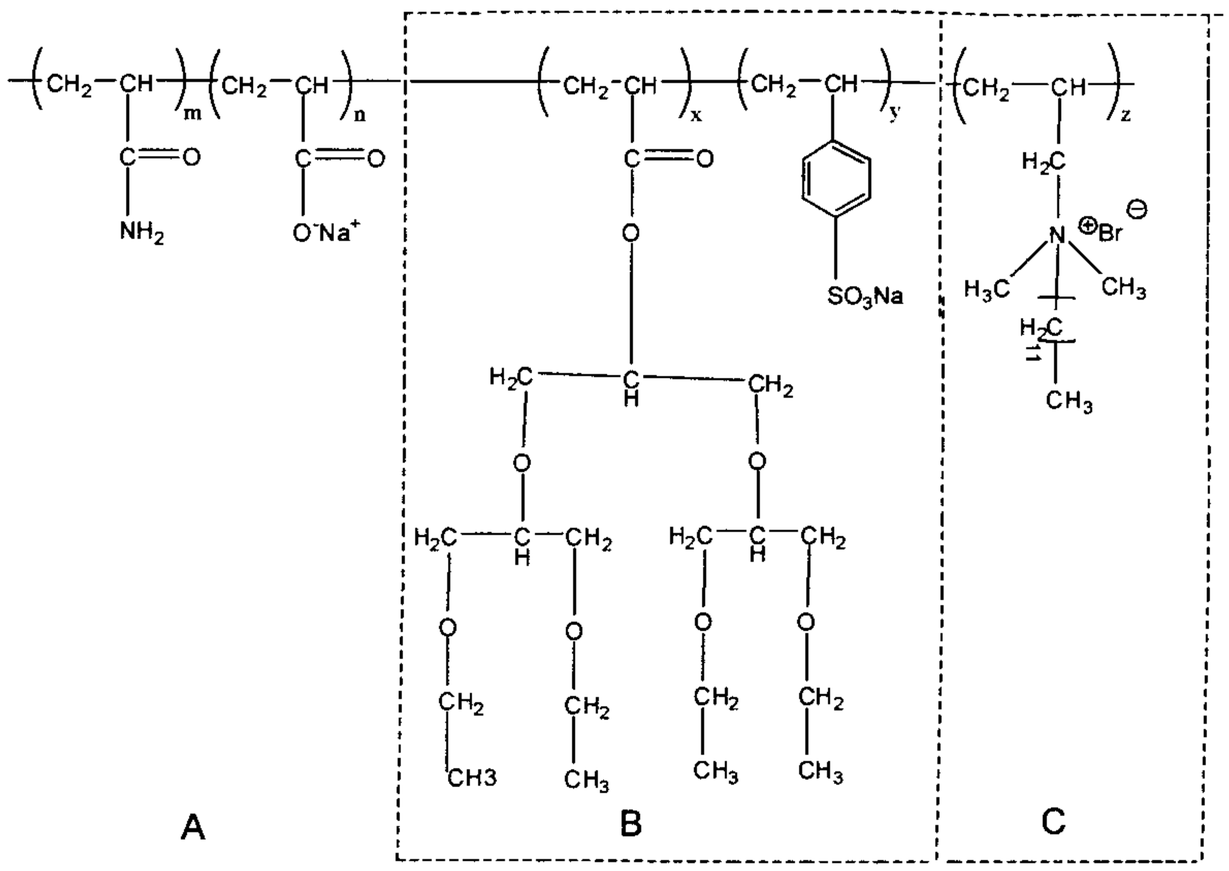
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 73%, 26%, 0.1%, 0.1%, 0.8% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 9, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 25□; after 6 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic

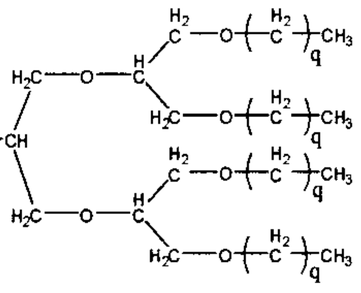
macromolecule was 620×10^4.

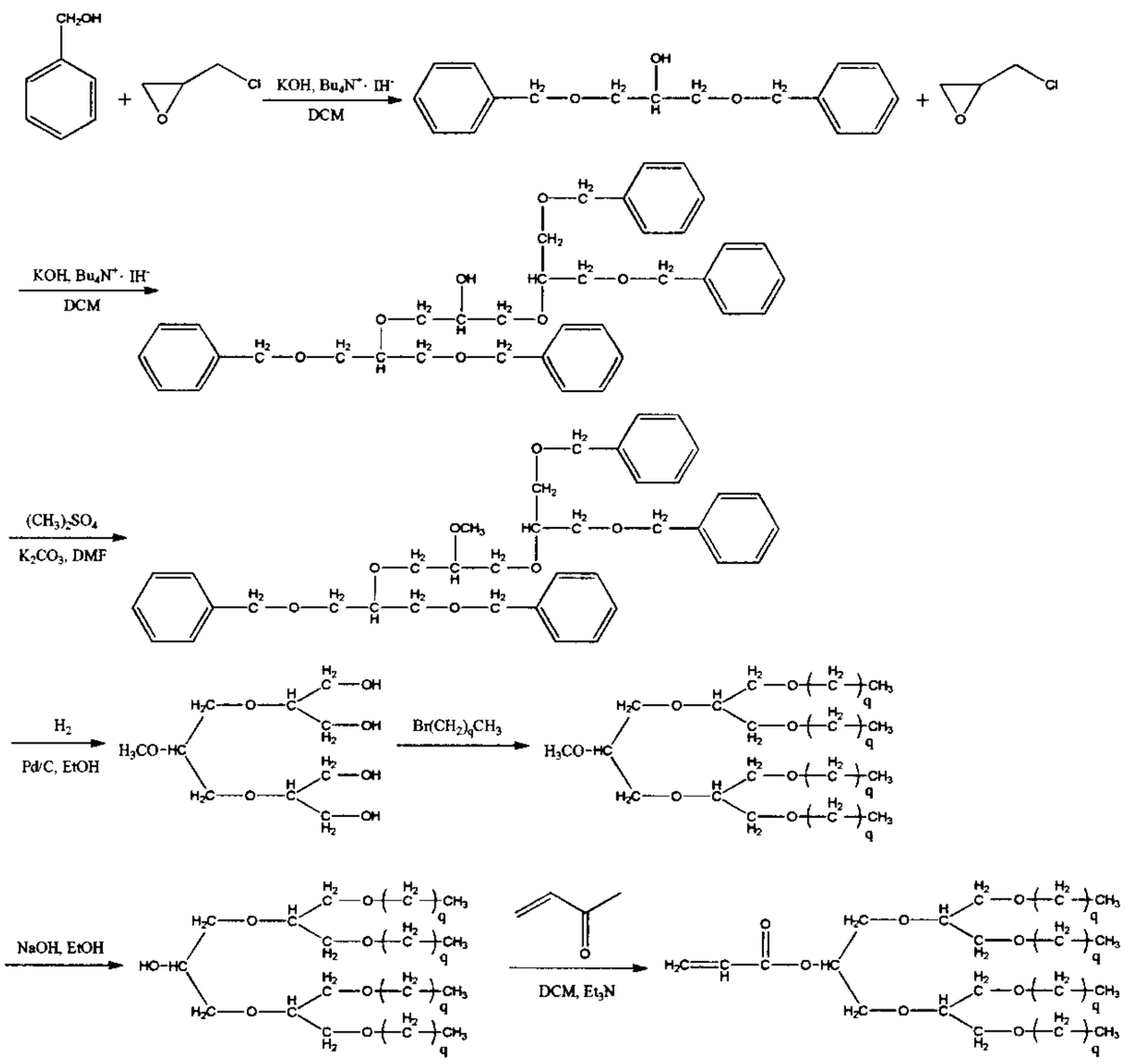
Example 4

This example synthesized the amphiphilic macromolecule of formula (IV):



(IV)

The synthesis route of the monomer  was as follows:

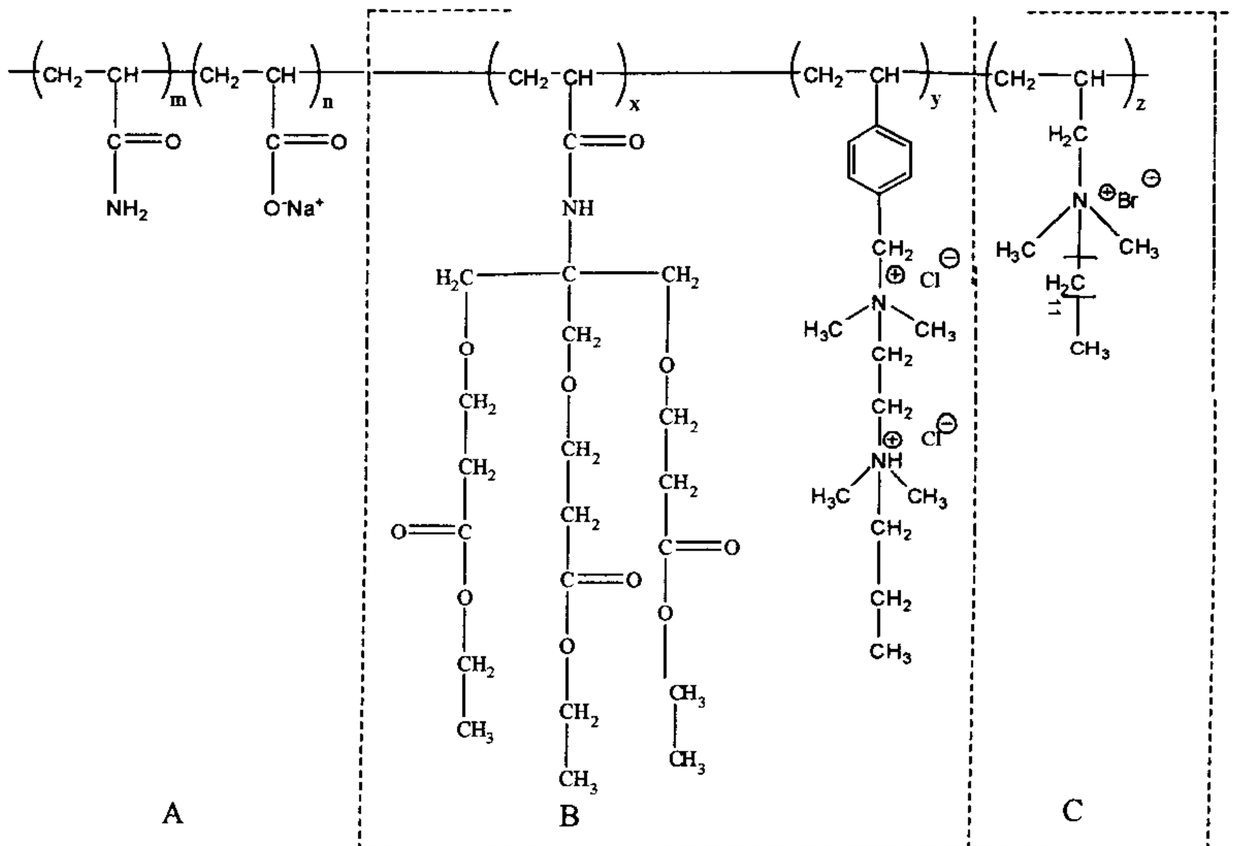


The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 75%, 23%, 0.1%, 0.4%, 1.5% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 9, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 25□; after 6 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 390×10^4.

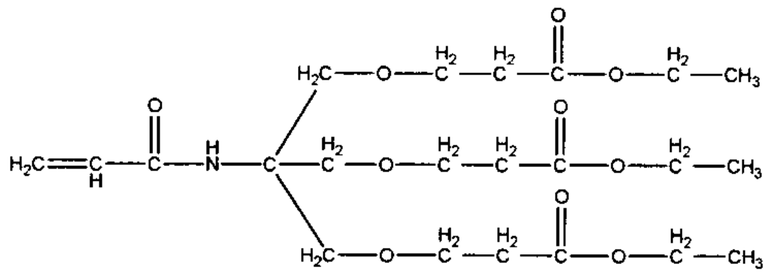
Example 5

This example synthesized the amphiphilic macromolecule of formula (V):

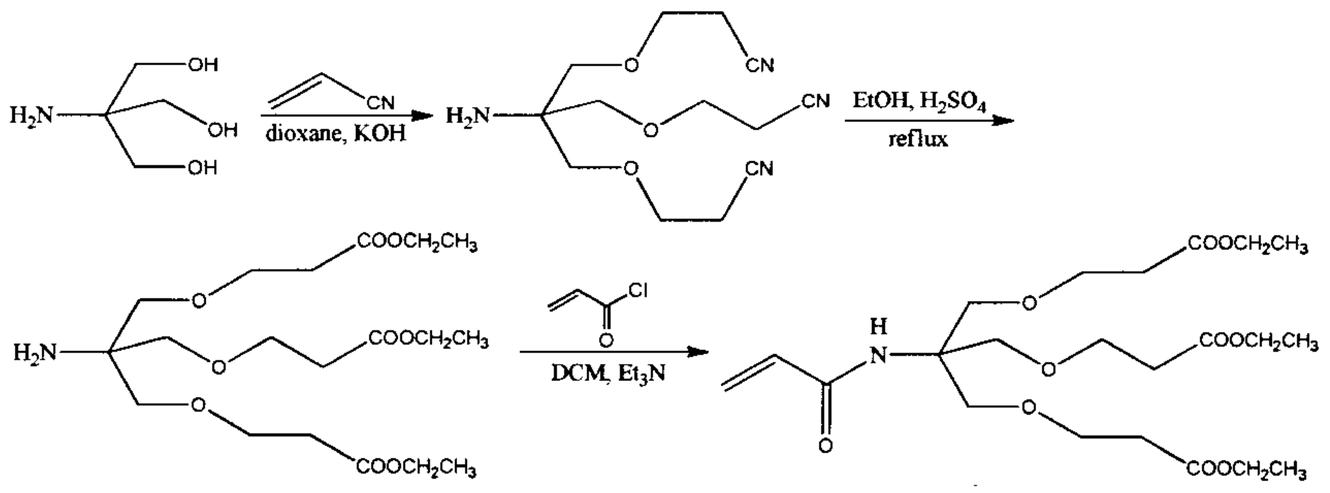


(V)

The synthesis route of the monomer



was as follows:

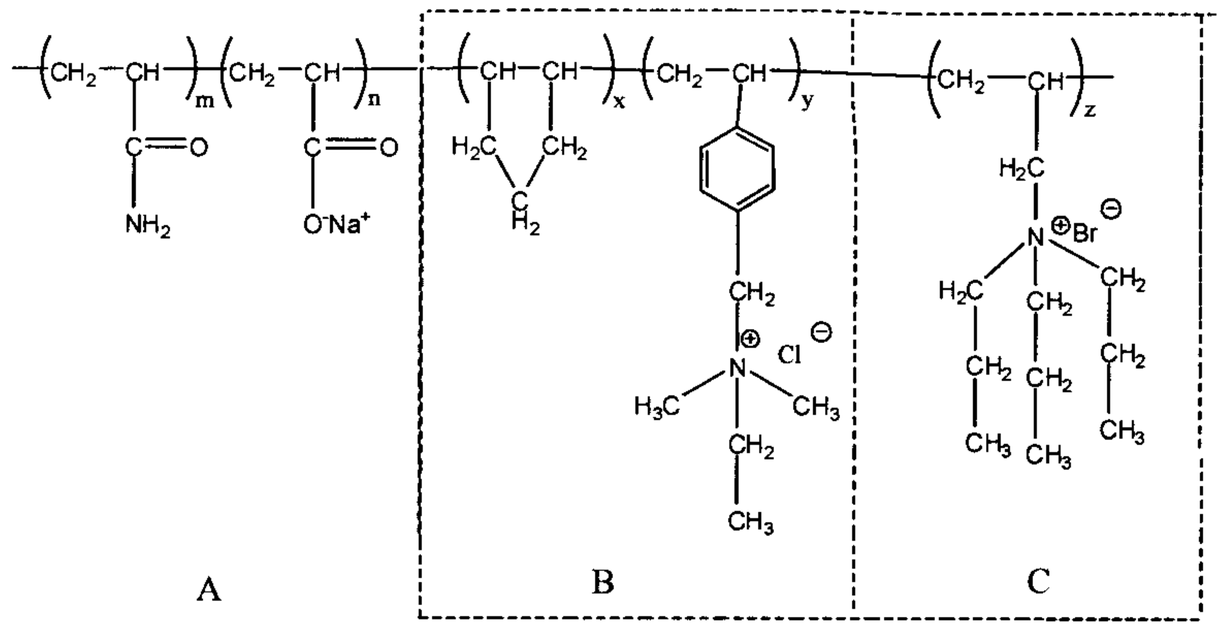


The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 78%, 21%, 0.1%, 0.1%, 0.8% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 25□; after 6 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 390×10^4.

Example 6

This example synthesized the amphiphilic macromolecule of formula (VI):



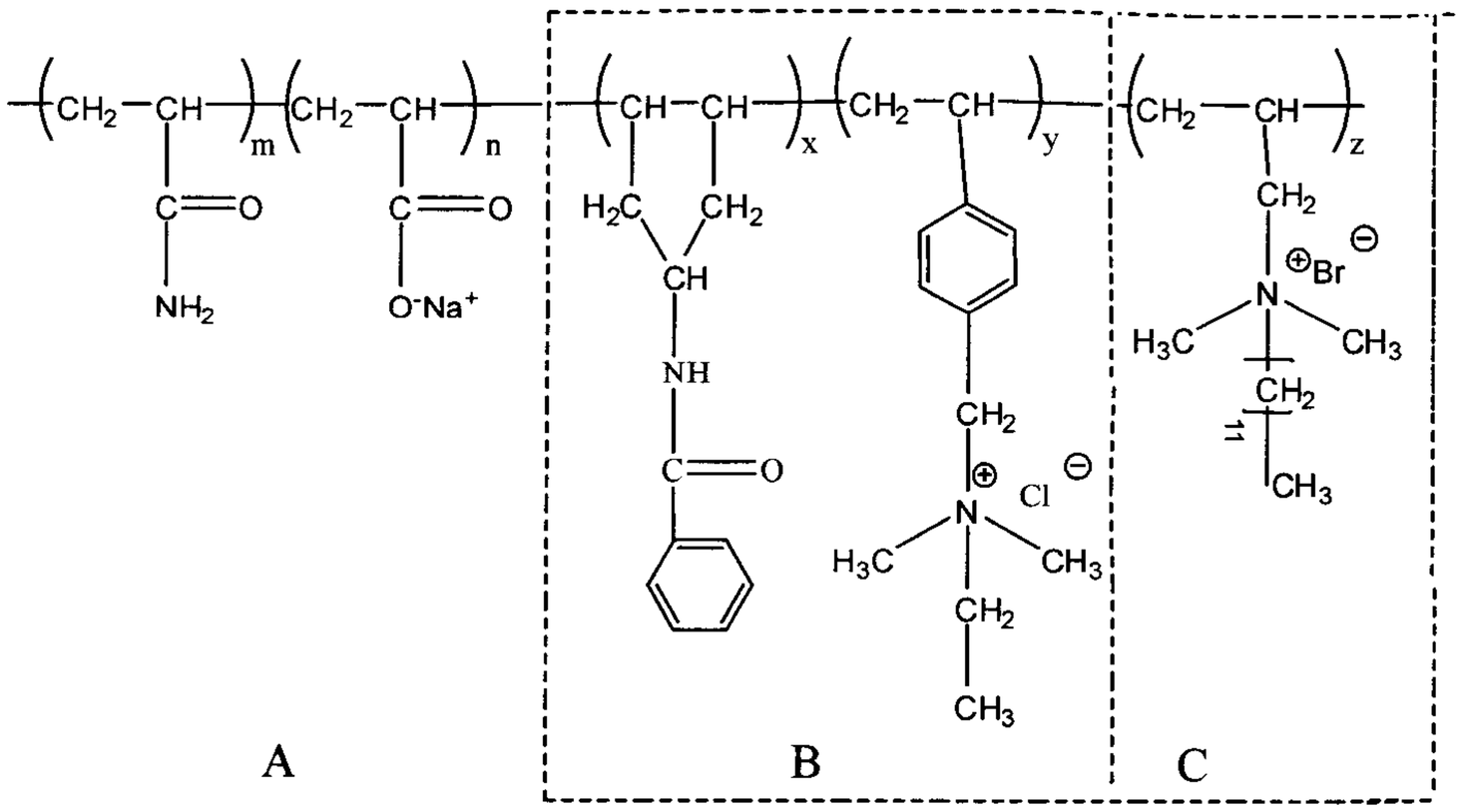
(VI)

The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 73.5%, 25%, 0.5%, 0.5%, 0.5% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 45□; after 3 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 680×10^4.

Example 7

This example synthesized the amphiphilic macromolecule of formula (VII):



(VII)

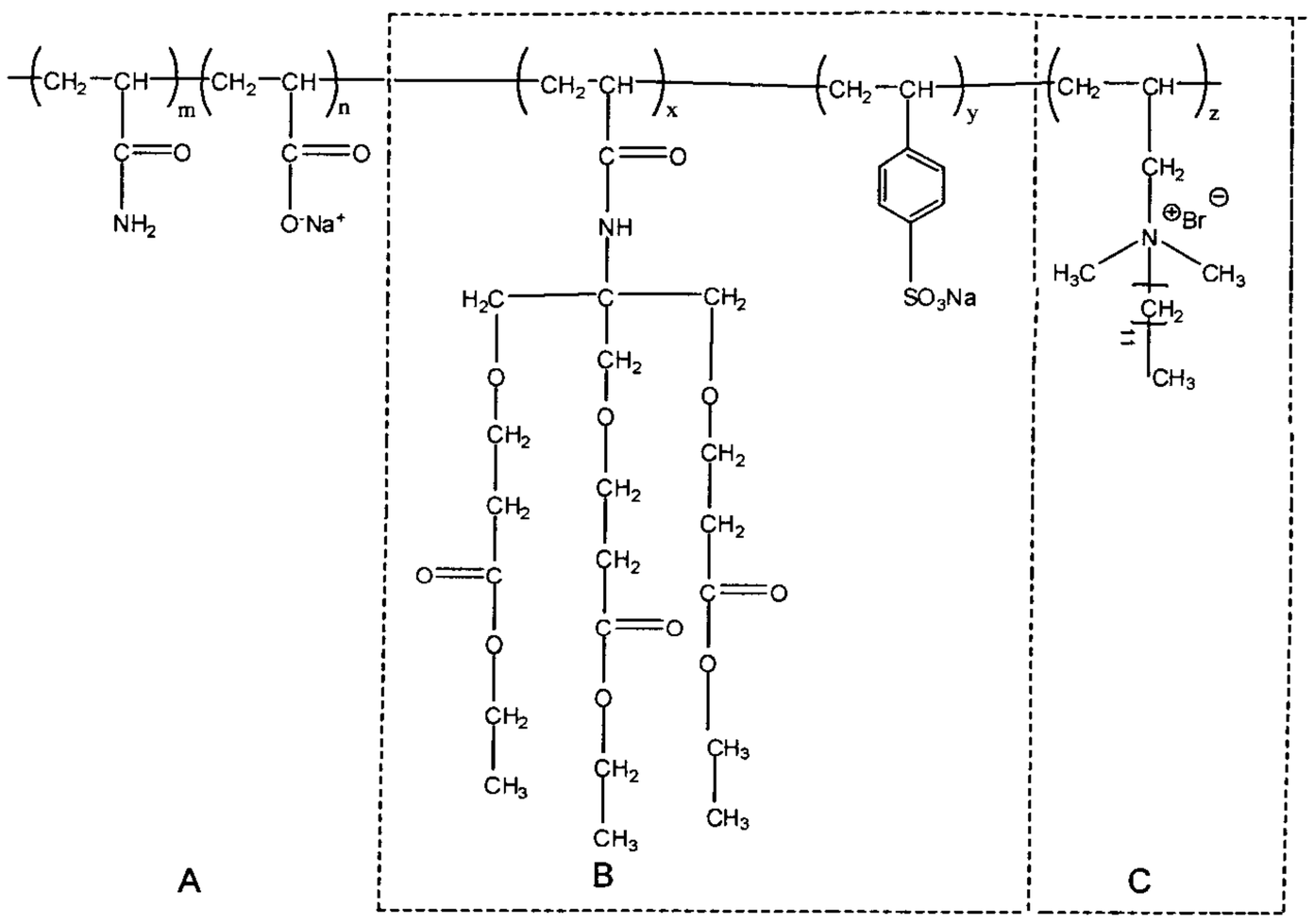
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total

weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 75%, 23%, 0.25%, 0.25%, 1.5% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 9, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 55□; after 3 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 690×10^4.

Example 8

This example synthesized the amphiphilic macromolecule of formula (VIII):



(VIII)

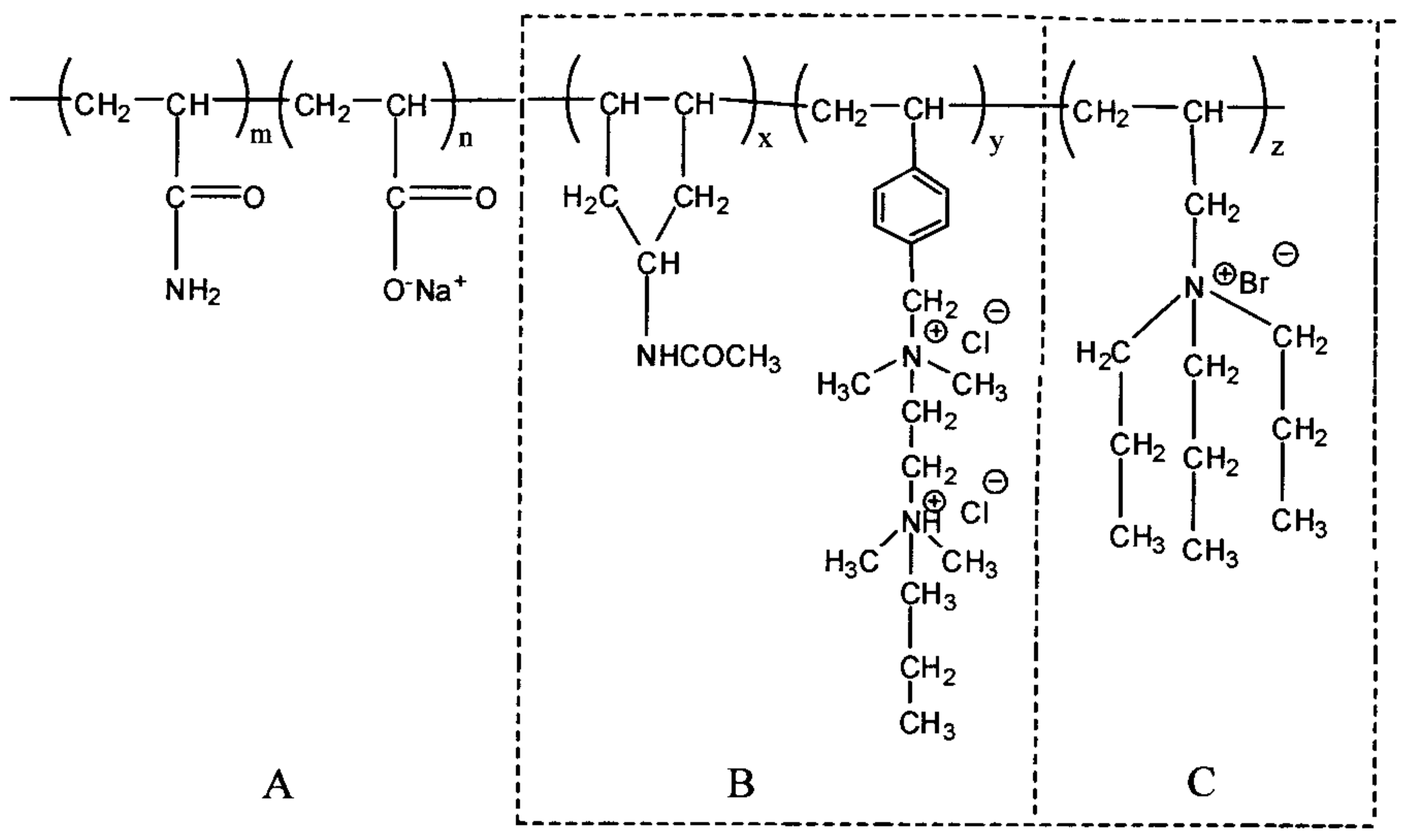
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 70%, 28%, 0.15%, 0.75%,

1.1% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 55□; after 3 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 390×10^4.

Example 9

This example synthesized the amphiphilic macromolecule of formula (IX):



(IX)

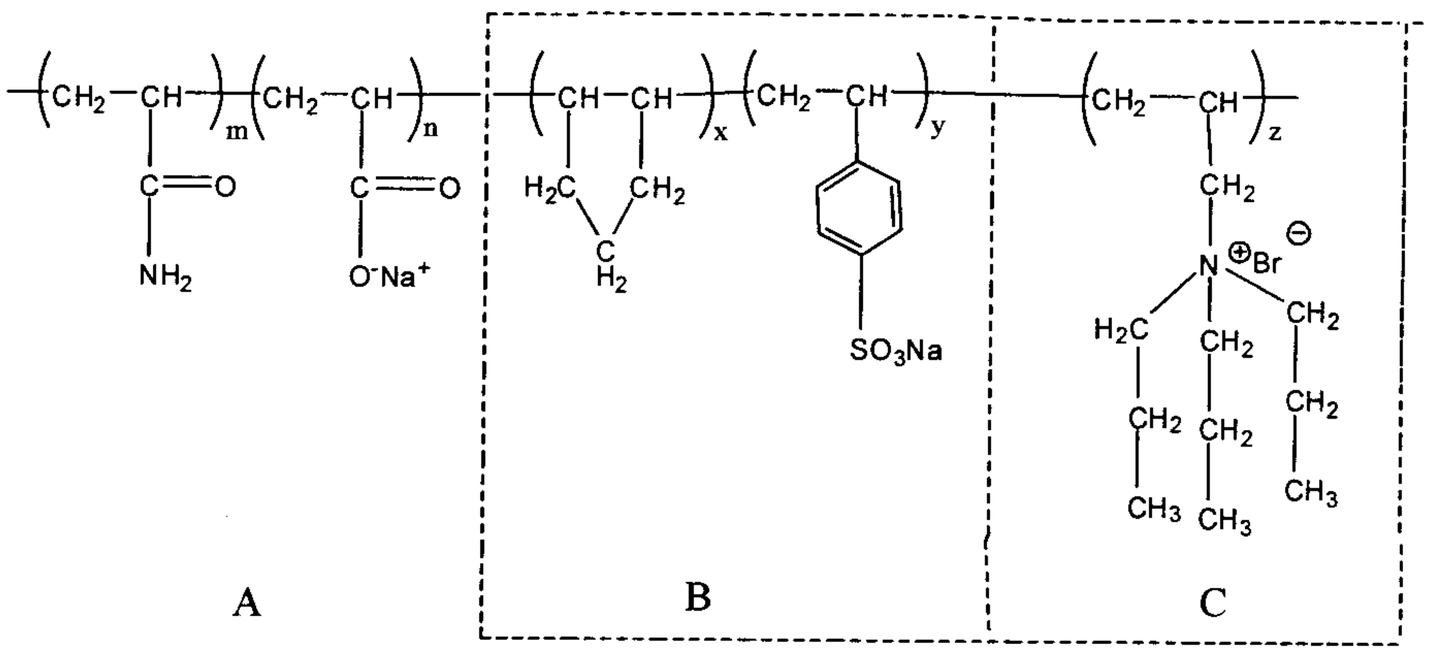
The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 75%, 23.5%, 0.5%, 0.5%, 0.5% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained

therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 50□; after 2.5 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic macromolecule was 430×10^4.

Example 10

This example synthesized the amphiphilic macromolecule of formula (X):



(X)

The synthesis of the amphiphilic macromolecule of this example was as follows:

Firstly, water, accounting for 3/4 of the total weight of the reaction system, was charged into a reactor, then various monomers, totally accounting for 1/4 of the total weight of the reaction system, were charged into the reactor as well, and the molar percentages m, n, x, y, z for each repeating units were 74%, 23%, 0.5%, 1.5%, 1% in succession. The mixture was stirred until complete dissolution, and a pH adjusting agent was then added in to adjust the reaction solution to have a pH value of about 8, then nitrogen gas was introduced in for 30 minutes to remove oxygen contained therein. An initiator was added into the reactor under the protection of nitrogen gas, and nitrogen gas was further continued for 10 minutes, then the reactor was sealed. The reaction was conducted at a temperature of 50□; after 2 hours, the reaction was ended with a complete conversion. After the drying of the obtained product, powdered amphiphilic macromolecule was obtained. The molecular weight of the amphiphilic

macromolecule was 560×10^4.

Measurement Examples

Measurement Example 1

Saline having a mineralization degree of 1×10^4mg/L was used to prepare amphiphilic macromolecule solutions with different concentrations, and the relationship between the concentration, temperature and the viscosity of the solution was determined. The results were shown in Figure 1 and Figure 2.

The figures showed that the amphiphilic macromolecule solutions of examples 1-5 still have favorable viscosifying capacity under the condition of high temperature and high degree of mineralization. The highly sterically hindered unit in the amphiphilic macromolecule reduced the rotational degree of freedom in the main chain and increased the rigidity of the macromolecule chain, which made the macromolecule chain difficult to curl and tend to stretch out, thus enlarging the hydrodynamic radius of the macromolecule; in the meantime, the amphiphilic structural unit associated each other to form the microdomain by intramolecular- or intermolecular- interaction, thus enhancing the viscosifying capacity of the solution remarkably under the conditions of high temperature and high salinity.

Measurement Example 2

Testing method: Under a testing temperature of 25□, 25ml electric dehydration crude oil samples from three types of oilfields were added in a 50ml test tube with a plug, then 25ml aqueous solutions of amphiphilic macromolecule with different concentrations formulated with distilled water were added in. The plug of the test tube was tightened, then the test tube was shaken manually or by using an oscillating box for 80-100 times in horizontal direction, and the shaking amplitude should be greater than 20cm. After sufficient mixing, the plug of the test tube was loosed. Viscosity reduction rate for crude oil was calculated according to the following equation:

$$\text{Viscosity reduction rate}(\%) = \frac{\text{viscosity of crude oil sample - viscosity after mixing}}{\text{viscosity of crude oil sample}} \times 100$$

Table 1 Experimental results of the heavy oil viscosity reduction of the amphiphilic macromolecule obtained from the example 6-example 10. (oil-water ratio 1:1, 25□)

oil-water volume ratio (1:1) / test temperature (25℃)		oil sample 1	viscosity reduction rate (%)	oil sample 2	viscosity reduction rate (%)	oil sample 3	viscosity reduction rate (%)
initial viscosity (mPa·s)		1800	--	6700	--	18000	--
Example 6	400mg/L	850	52.78	2300	65.67	4700	73.89
	600mg/L	550	69.44	1475	77.99	2350	86.94
	800mg/L	340	81.11	975	85.45	1250	93.06
	1000mg/L	280	84.44	750	88.81	950	94.72
	1200mg/L	220	87.78	650	90.30	825	95.42
Example 7	400mg/L	910	49.44	2400	64.18	4450	75.28
	600mg/L	590	67.22	1600	76.12	2100	88.33
	800mg/L	450	75.00	1175	82.46	1050	94.17
	1000mg/L	340	81.11	830	87.61	890	95.06
	1200mg/L	260	85.56	680	89.85	780	95.67
Example 8	400mg/L	820	54.44	2050	69.40	4250	76.39
	600mg/L	470	73.89	1370	79.55	1975	89.03
	800mg/L	315	82.50	850	87.31	1325	92.64
	1000mg/L	230	87.22	675	89.93	930	94.83
	1200mg/L	200	88.89	590	91.19	850	95.28
Example 9	400mg/L	925	48.61	2270	66.12	4700	73.89
	600mg/L	630	65.00	1420	78.81	2550	85.83
	800mg/L	450	75.00	940	85.97	1480	91.78
	1000mg/L	380	78.89	680	89.85	1050	94.17
	1200mg/L	340	81.11	530	92.09	880	95.11
Example	400mg/L	820	54.44	1900	71.64	5100	71.67

10	600mg/L	530	70.56	1250	81.34	2900	83.89
	800mg/L	390	78.33	825	87.69	1890	89.50
	1000mg/L	305	83.06	650	90.30	1400	92.22
	1200mg/L	260	85.56	575	91.42	1175	93.47

Table 1 showed that the amphiphilic macromolecules of examples 6-10 had good effects for viscosity reduction as to all three oil samples. With the increase of the concentration of the amphiphilic macromolecule solution, the viscosity reduction rate increased. And, when the concentration of the amphiphilic macromolecule solution was the same, the viscosity reduction rate increased with the enhancing of the viscosity of the oil sample. It was believed that the amphiphilic macromolecule could reduce the viscosity of the crude oil remarkably via a synergetic effect between the highly sterically hindered structural unit and the amphiphilic structural unit, which could emulsify and disperse the crude oil effectively.

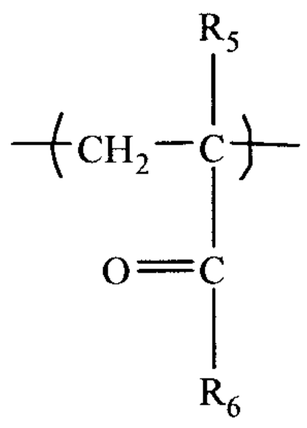
Industrial Application

The amphiphilic macromolecule of this invention can be used in oilfield drilling, well cementing, fracturing, crude oil gathering and transporting, sewage treating, sludge treating and papermaking, and it can be used as intensified oil producing agent and oil displacing agent, heavy oil viscosity reducer, fracturing fluid, clay stabilizer, sewage treating agent, retention aid and drainage aid and strengthening agent for papermaking.

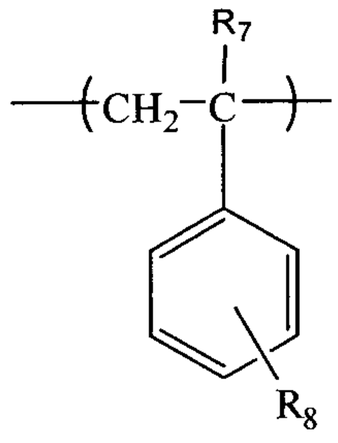
The amphiphilic macromolecule of this invention is especially suitable for crude oil exploitation, for instance, it can be used as an intensified oil displacement polymer and a viscosity reducer for heavy oil. When it is used as an oil displacement agent, it has remarkable viscosifying effect even under the condition of high temperature and high salinity, and can thus enhance the crude oil recovery. When it is used as a viscosity reducer for heavy oil, it can remarkably reduce the viscosity of the heavy oil and decrease the flow resistance thereof in the formation and wellbore by emulsifying and dispersing the heavy oil effectively.

What is claimed is:

1. An amphiphilic macromolecule, characterized in that: as repeating units, it has a structural unit A for adjusting molecular weight, molecular weight distribution and charge characteristics, a highly sterically hindered structural unit B and an amphiphilic structural unit C, the highly sterically hindered structural unit B comprises a structure G and a structure of formula (4), wherein the structure G is a cyclic hydrocarbon structure formed on the basis of two adjacent carbon atoms in the main chain, or is selected from a structure of formula (3):

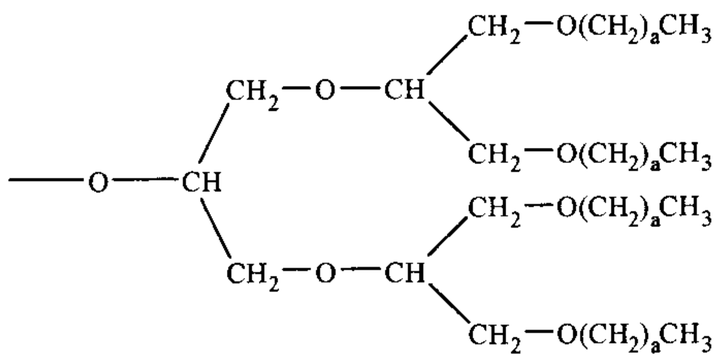


formula (3)

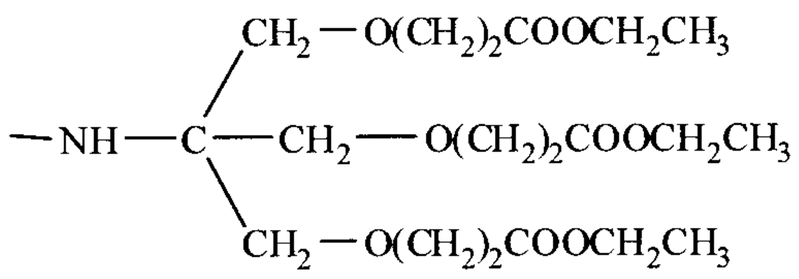


formula (4)

wherein in formula (3), R_5 is H or a methyl group, preferably H; R_6 is a radical selected from the group consisting of the structures of formula (5) and formula (6):



formula (5)

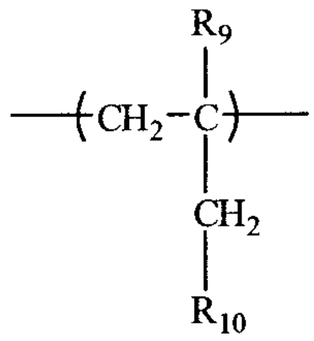


formula (6)

in formula (5), a is an integer from 1 to 11.

in formula (4), R_7 is H; R_8 is selected from the group consisting of H, $-SO_3H$ and salts thereof, $-(CH_2)_2CH_3Cl$, $-CH_2N^+(CH_3)_2(CH_2)_\xi CH_3Cl^-$, and $-CH_2N^+(CH_3)_2(CH_2)_2N^+(CH_3)_2(CH_2)_\sigma CH_32Cl^-$; ξ and σ are respectively integers from 1 to 15; and

the amphiphilic structural unit C has a structure of formula (8):



formula (8),

in formula (8), R_9 is H or a methyl group; R_{10} is $-N^+(CH_3)_2(CH_2)_rCH_3X^-$, $-N^+((CH_2)sCH_3)_3X^-$ or $-N^+(CH_3)((CH_2)_tCH_3)_2X^-$; r is an integer from 3 to 21; s is an integer from 2 to 9; t is an integer from 3 to 15; and X^- is Cl^- or Br^-.

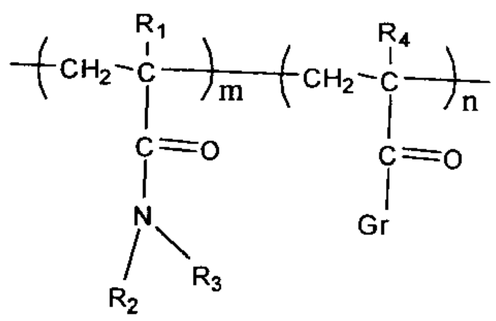
2. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, the structural unit A for adjusting the molecular weight, molecular weight distribution and charge characteristics comprises a (meth)acrylamide monomer unit A_1 and /or a (meth)acrylic monomer unit A_2.

3. The amphiphilic macromolecule as claimed in Claim 2, characterized in that, based on 100 mol% of the entire amphiphilic macromolecule repeating units, the molar percentage of the (meth)acrylamide monomer unit A_1 is 70-99mol%; and the molar percentage of the (meth)acrylic monomer unit A_2 is 1-30mol%.

4. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, based on 100 mol% of the entire amphiphilic macromolecule repeating units, the molar percentage of the structure G is 0.02-2mol%; and the molar percentage of the structure of formula (4) is 0.05-5mol%.

5. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, based on 100 mol% of the entire amphiphilic macromolecule repeating units, the molar percentage of the structure of formula (8) is 0.05-10mol%.

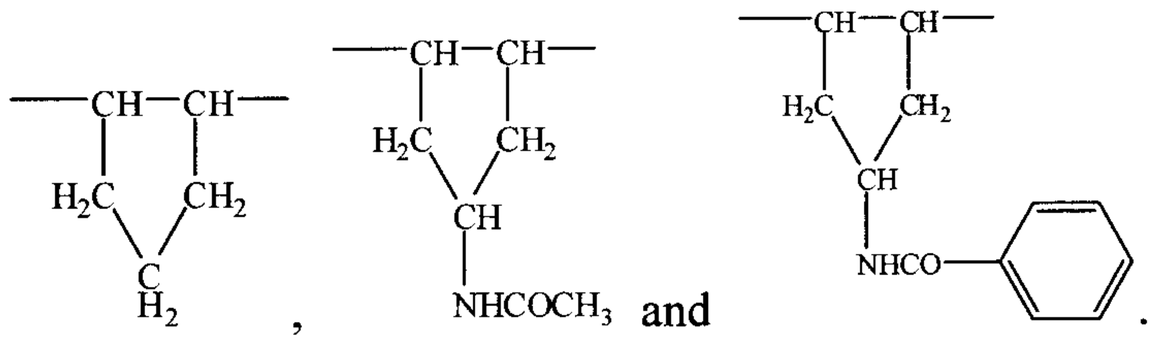
6. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, the structural unit A for adjusting molecular weight, molecular weight distribution and charge characteristics has a structure of formula (2):



formula (2)

wherein in formula (2), R_1 is H or a methyl group; R_2 and R_3 are independently selected from the group consisting of H and a C_1-C_3 alkyl group; R_4 is selected from the group consisting of H and a methyl group; Gr is -OH or $-O^-Na^+$; m and n represent the molar percentages of the structural units in the entire amphiphilic macromolecule, and m is from 70 to 99mol%; n is from 1 to 30mol%.

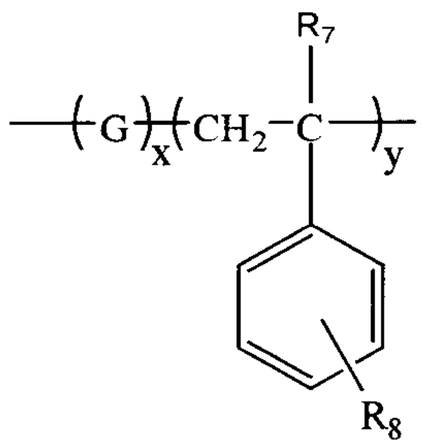
7. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, the cyclic hydrocarbon structure formed on the basis of the two adjacent carbon atoms in the main chain is selected from the group consisting of:



and

.

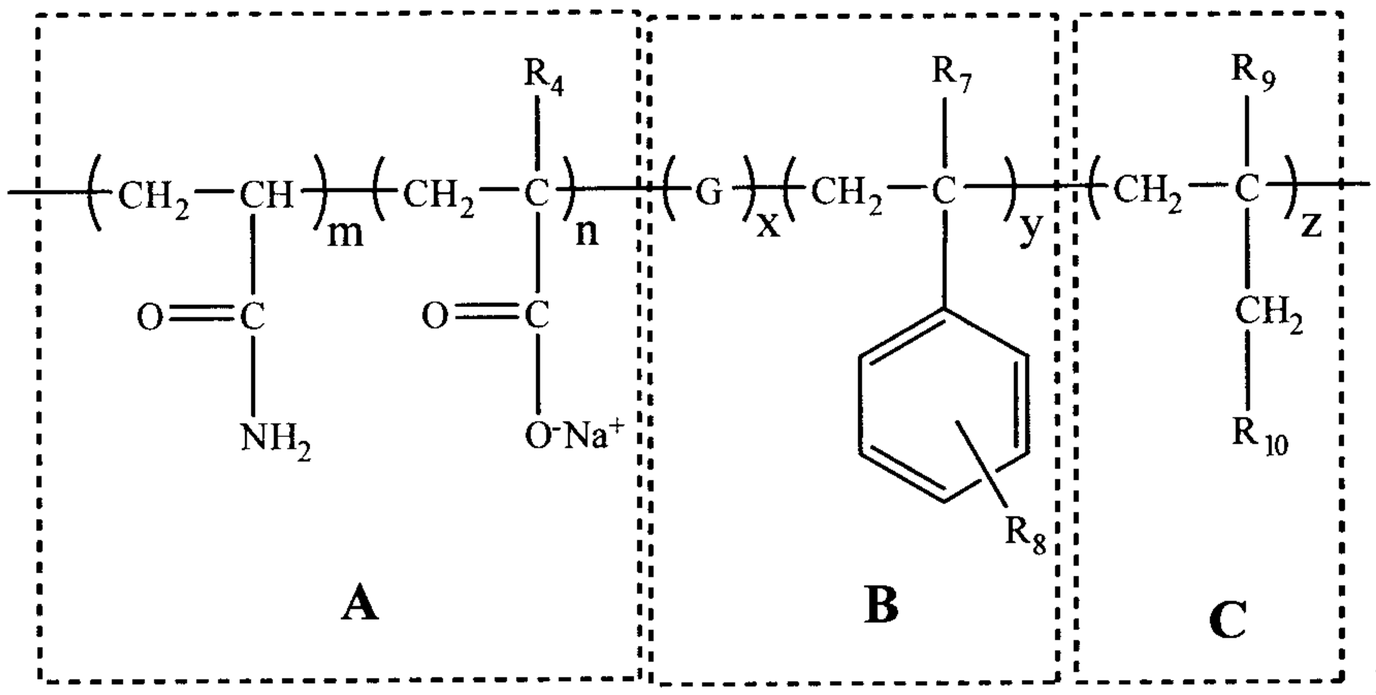
8. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, the highly sterically hindered structural unit B has a structure of formula (7):



formula (7)

wherein in formula (7), the definition on G is as described in Claim 1; the definitions on R_7 and R_8 are as described in formula (4); x and y respectively represent the molar percentages of the structural units in the entire amphiphilic macromolecule, and x is from 0.02 to 2mol%, y is from 0.05 to 5mol%.

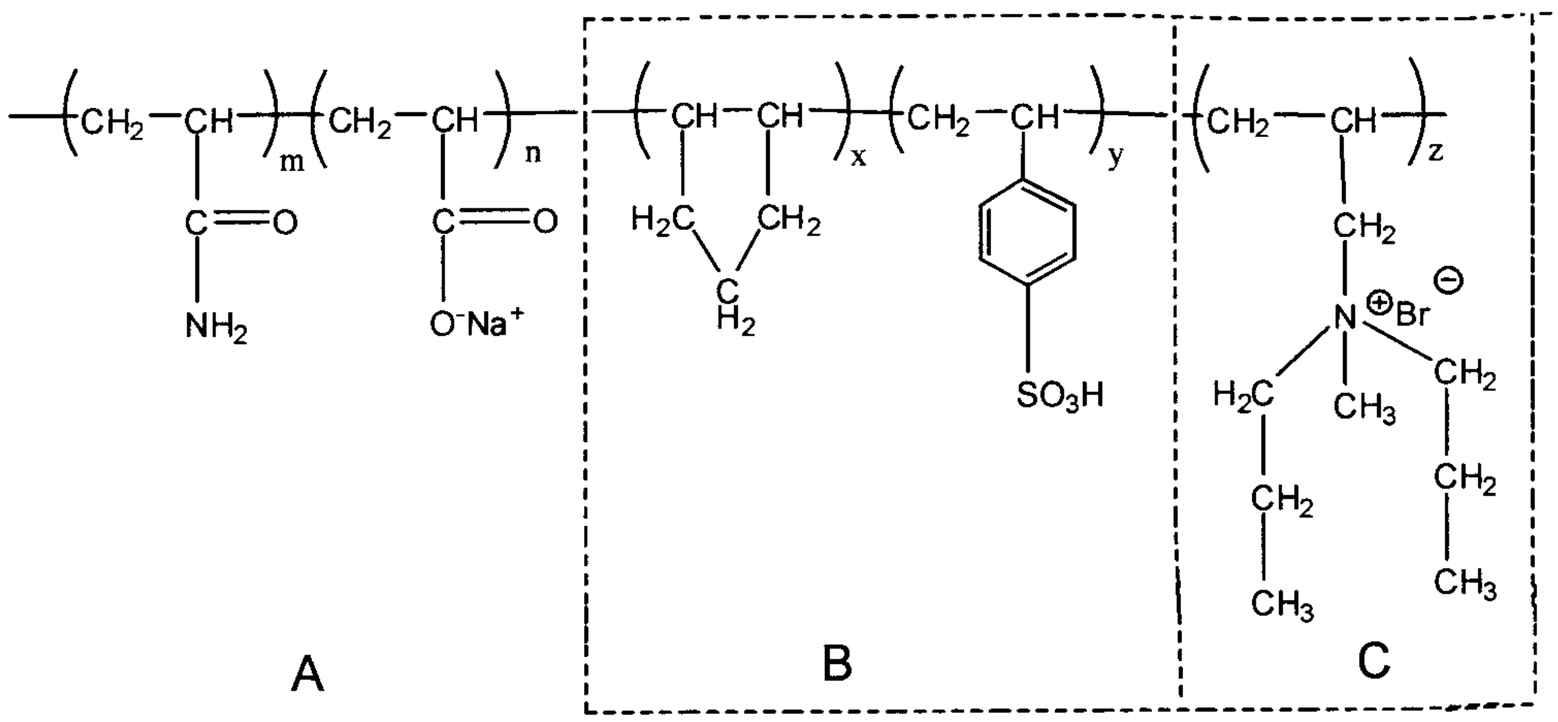
9. The amphiphilic macromolecule as claimed in Claim 1, characterized in that, the amphiphilic macromolecule has a structure of formula (9):



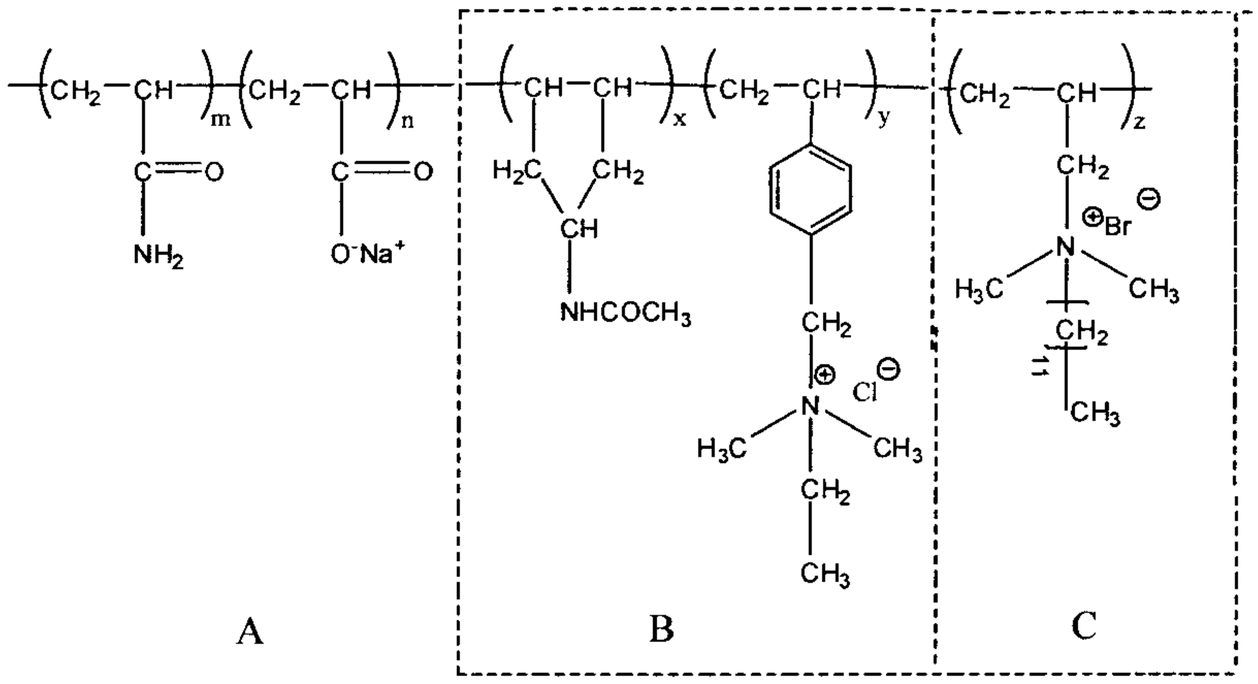
formula (9)

wherein in formula (9), R_4 is selected from the group consisting of H and a methyl group; m and n represent the molar percentages of the structural units in the entire amphiphilic macromolecule, and m is from 70 to 99mol%; n is from 1 to 30mol%; the definitions on G, R_7, R_8, x and y are as described in formula (7); the definitions on R_9 and R_{10} are as described in formula (8); z represents the molar percentage of this structural unit in the entire amphiphilic macromolecule, and z is from 0.05 to 10mol%.

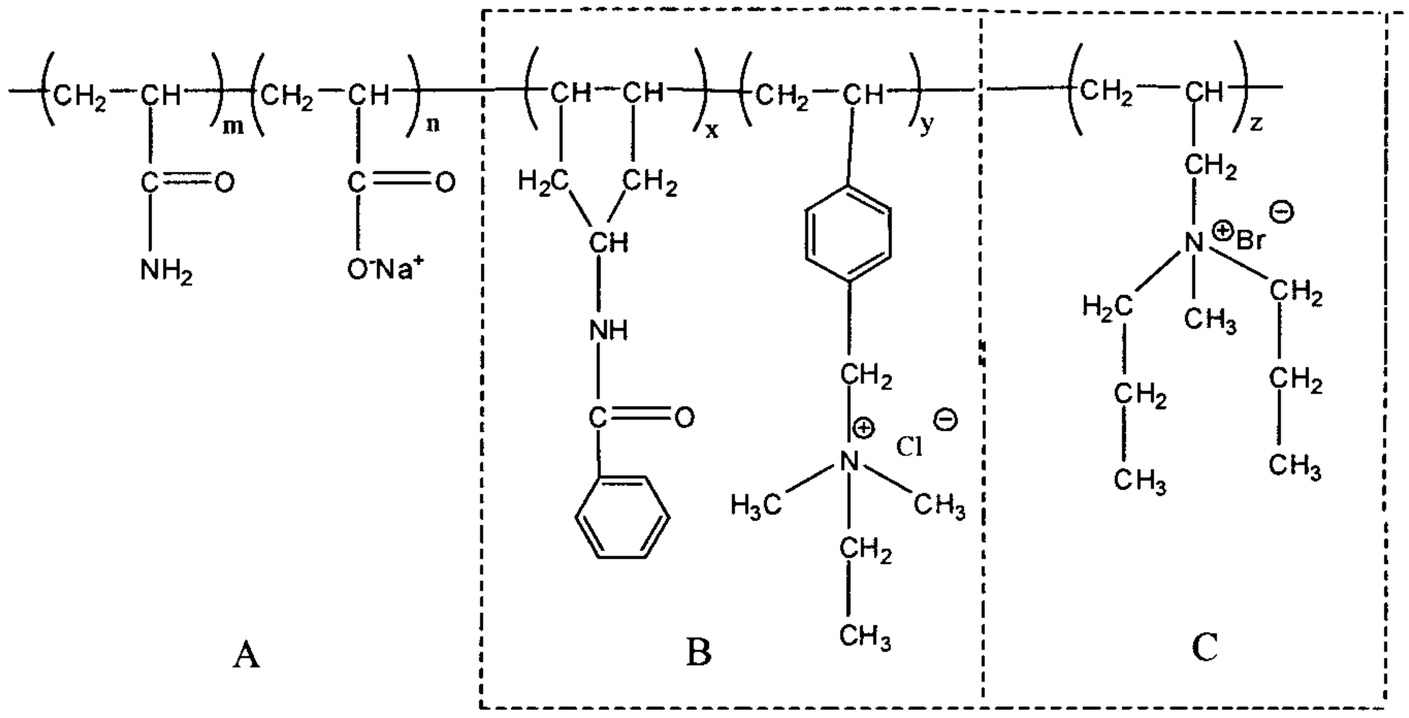
10. The amphiphilic macromolecule as claimed in Claim 1, which is a compound of formulas (I)-(X):



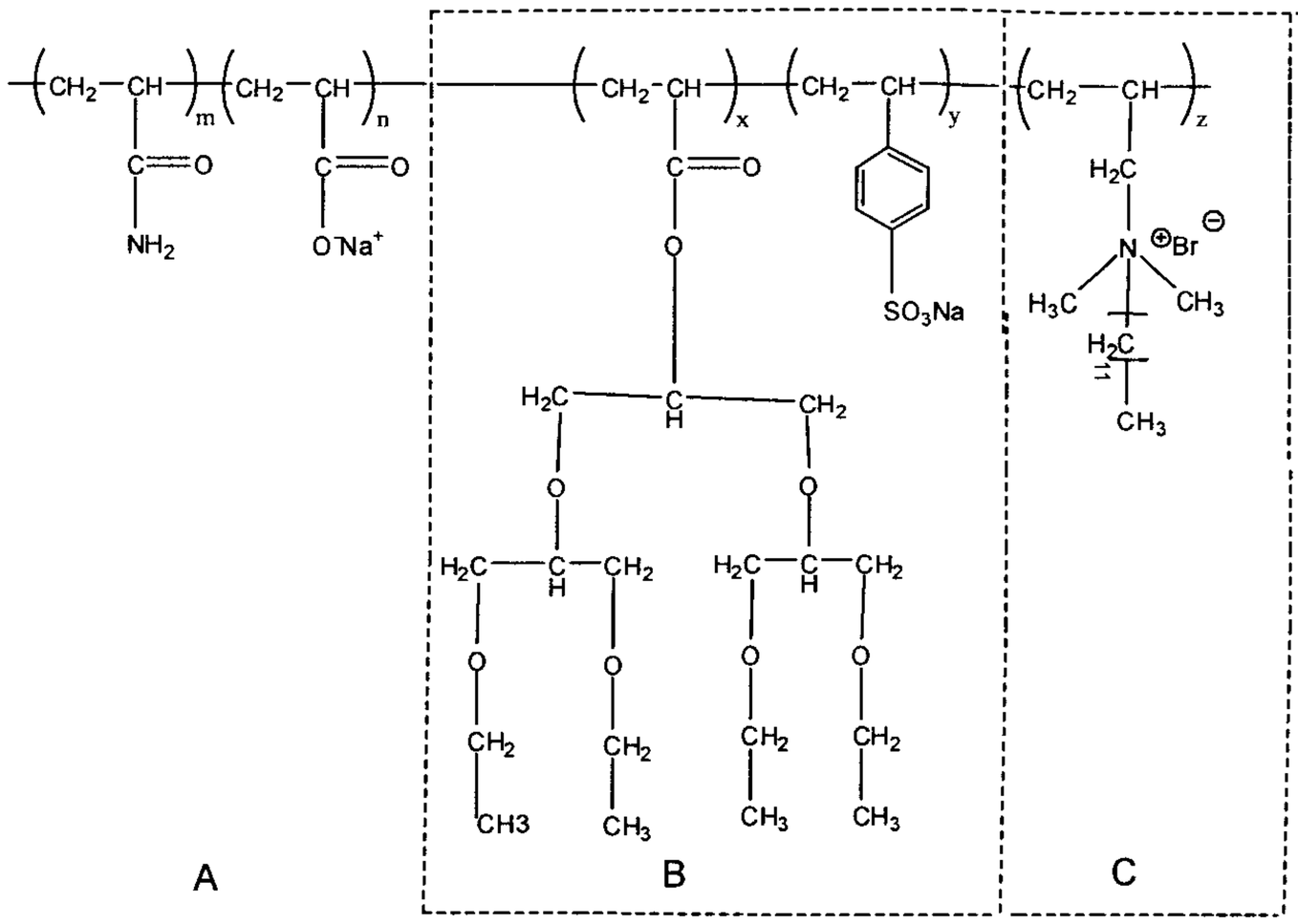
(I)



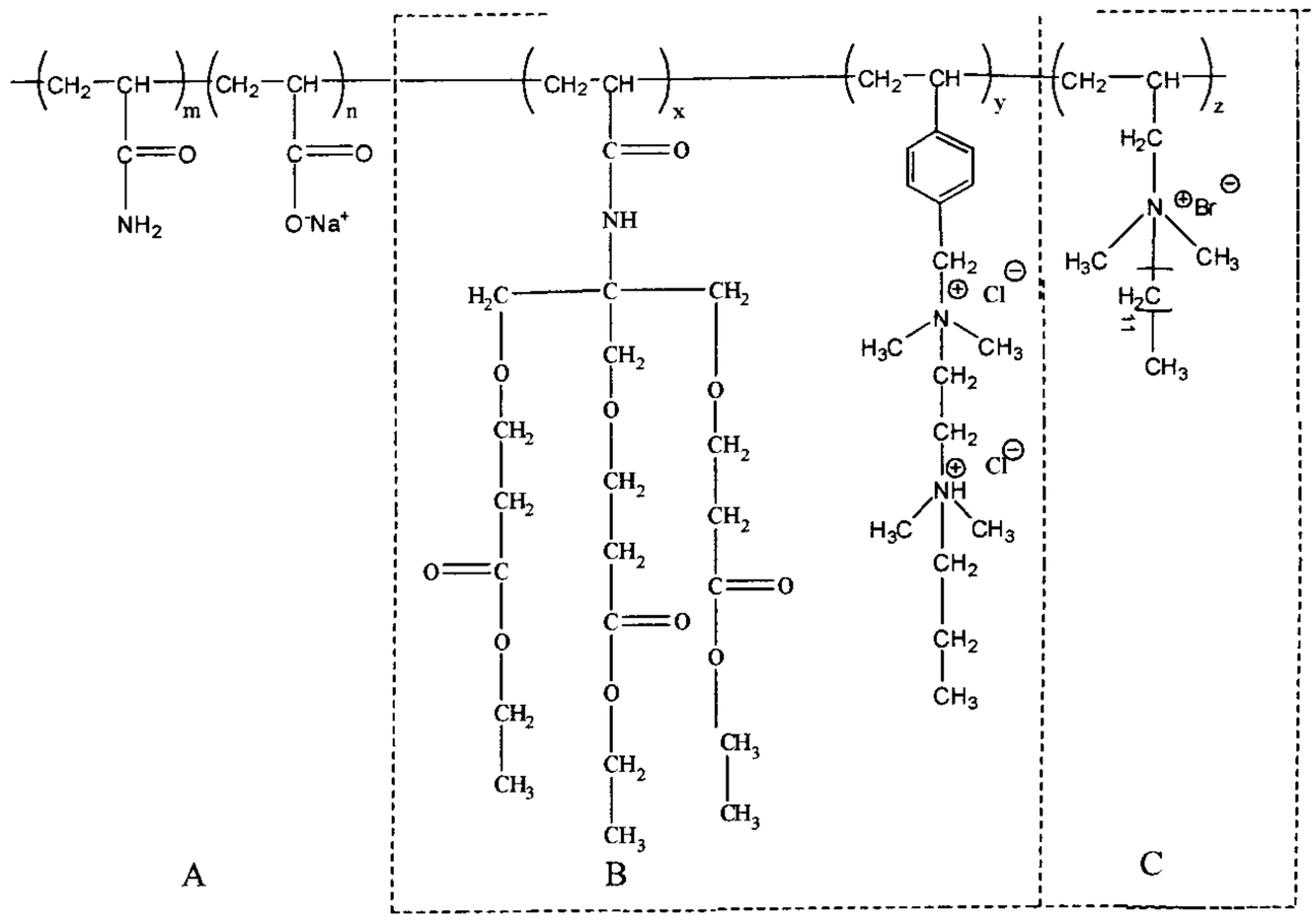
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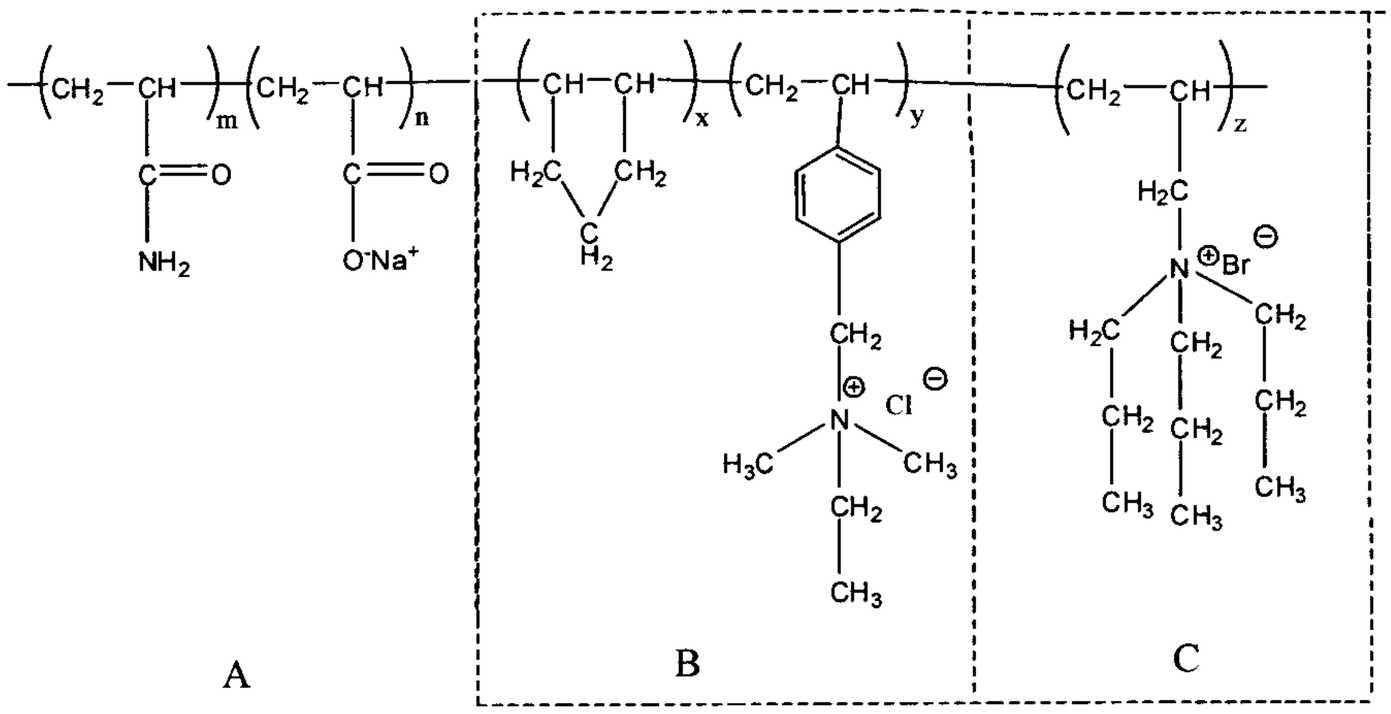
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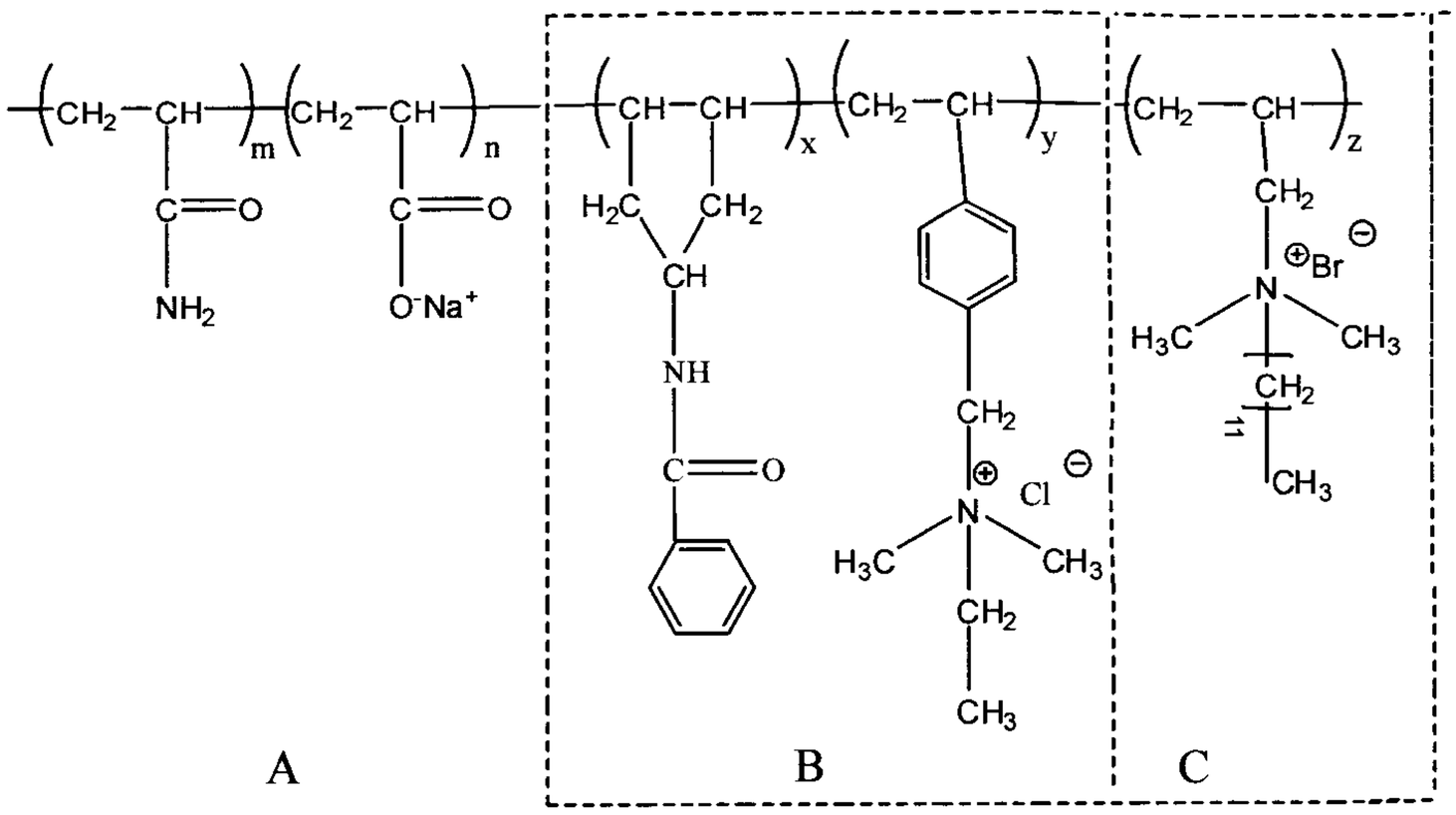
(IV)



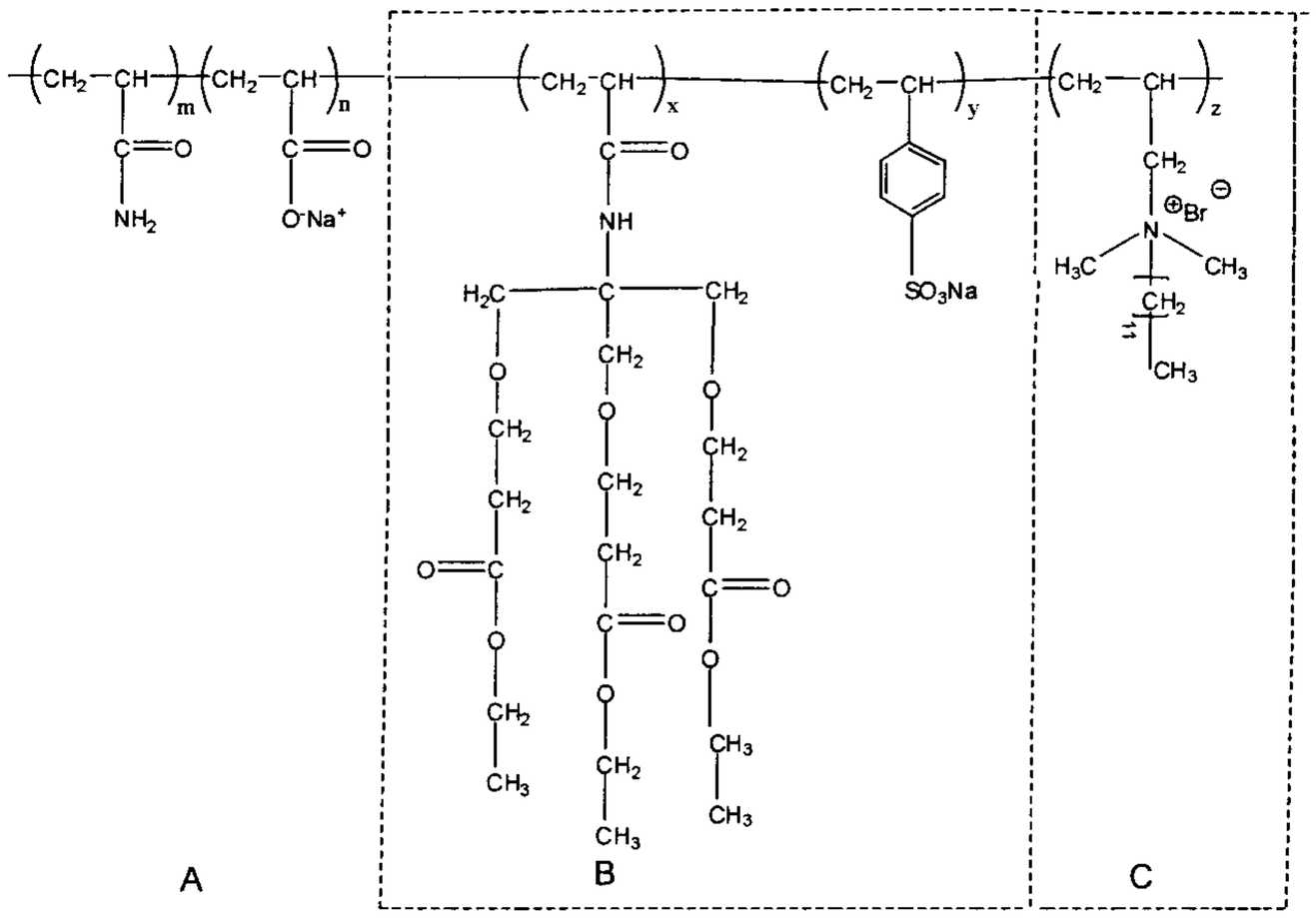
(V)



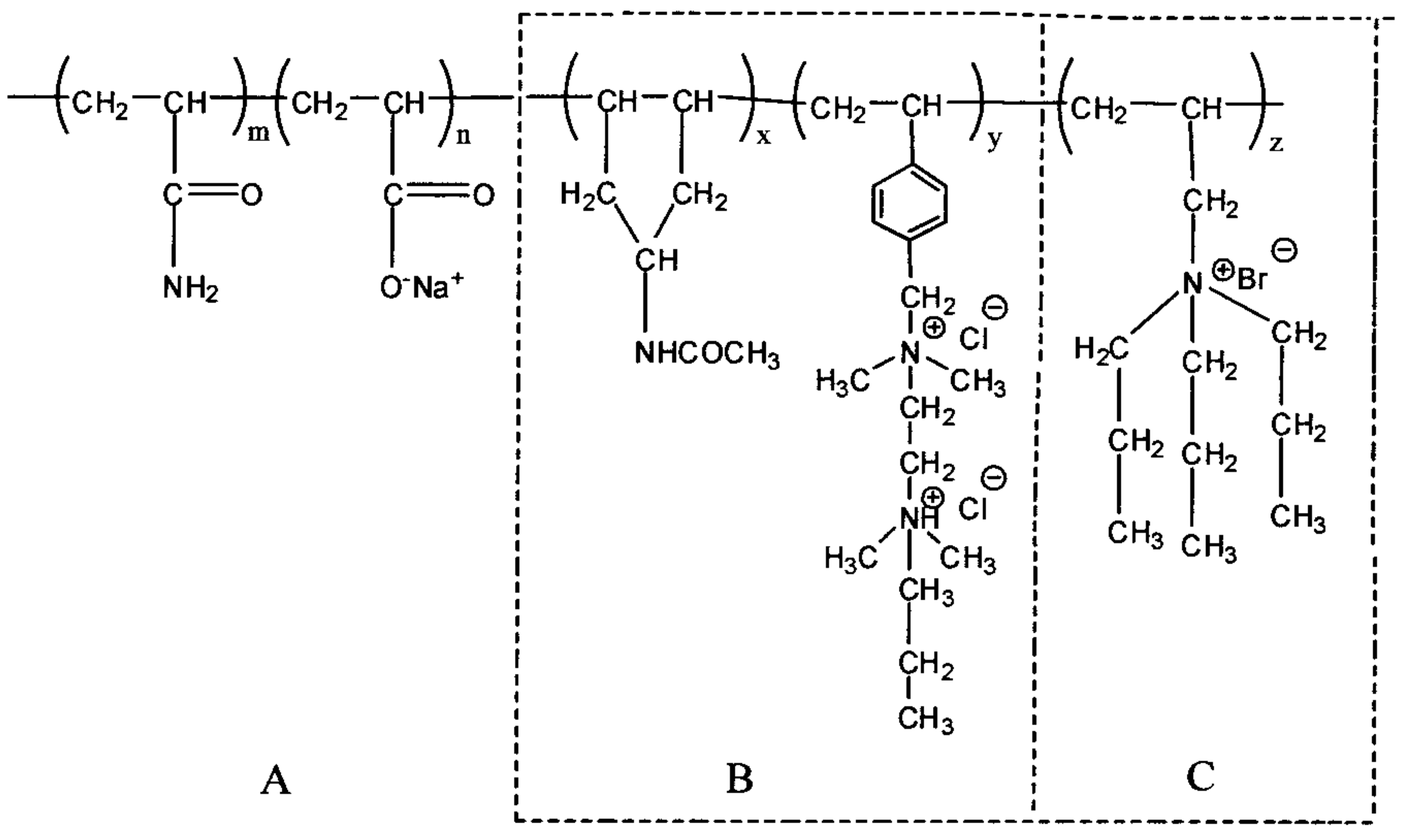
(VI)



(VII)

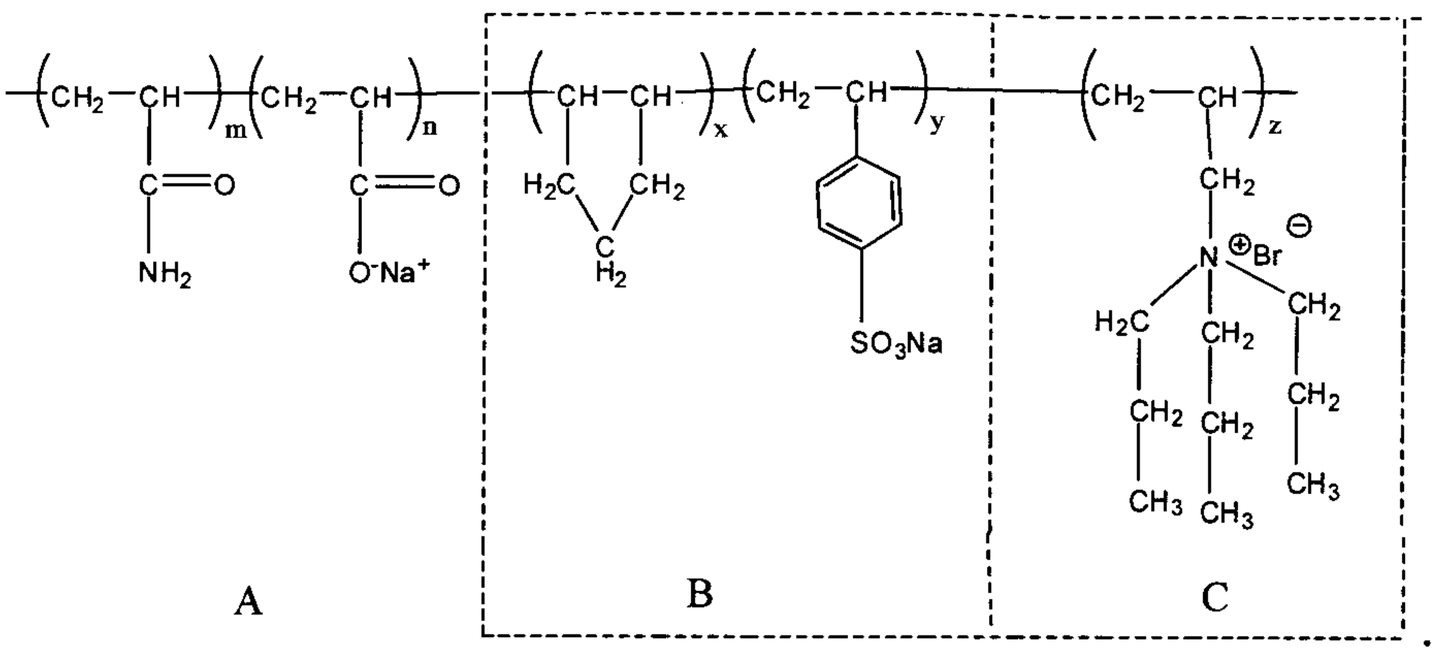


(VIII)



or

(IX)



(X)

11. The amphiphilic macromolecule as claimed in any of claims 1 to 10, characterized in that, it has a molecular weight of between 1000000-20000000.

12. Use of the amphiphilic macromolecule as claimed in any of claims 1 to 10 in oilfield drilling, well cementing, fracturing, crude oil gathering and transporting, sewage treating, sludge treating and papermaking as intensified oil producing agent and oil displacing agent, heavy oil viscosity reducer, fracturing fluid, clay stabilizer, sewage treating agent, retention aid and drainage aid and strengthening agent for papermaking.

Figures

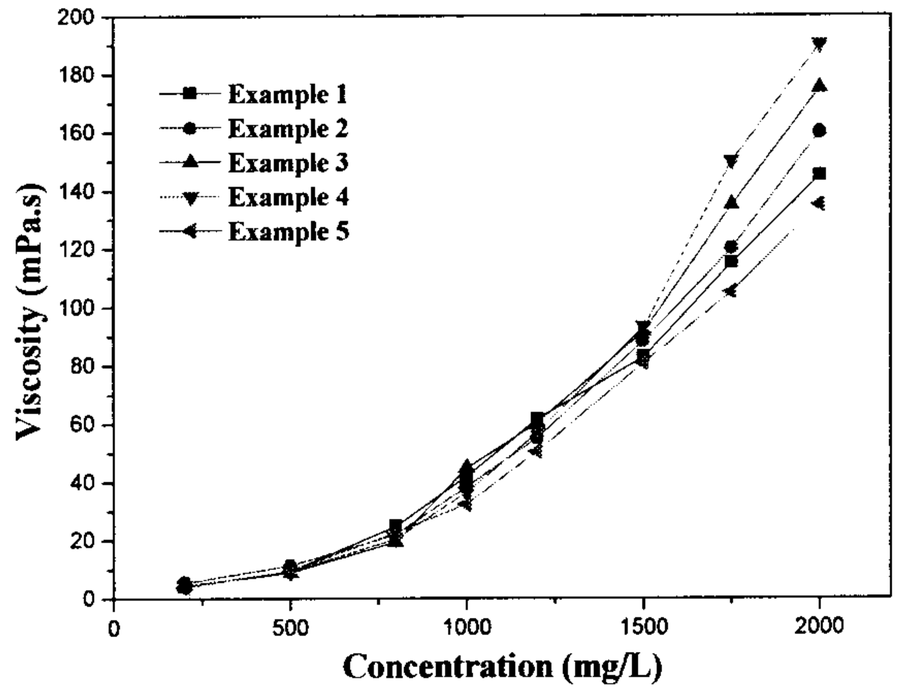


Figure 1: The relationship between the viscosity and concentration

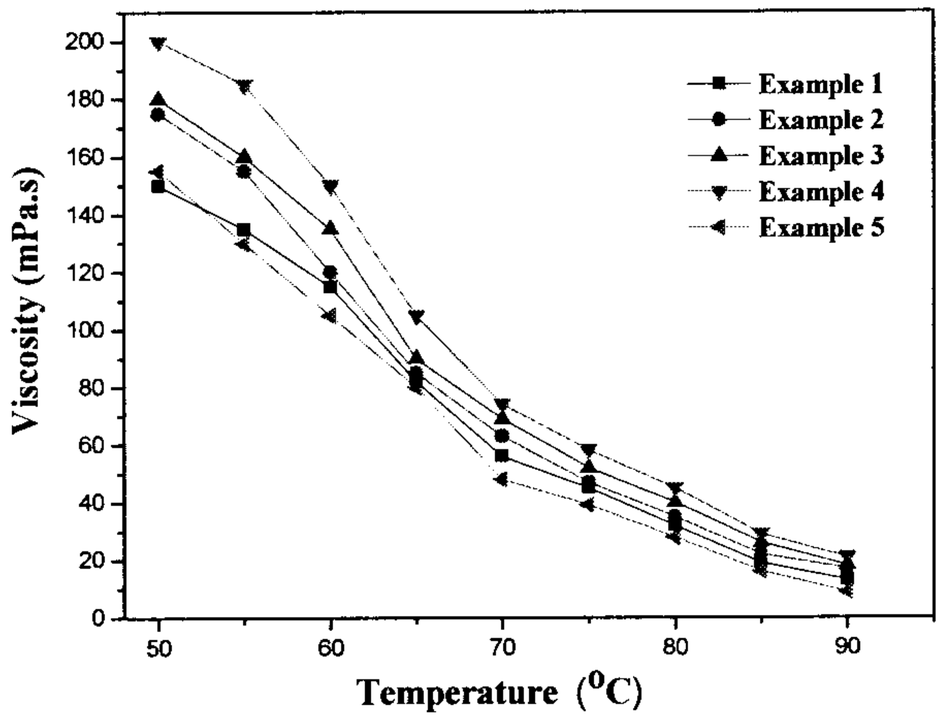


Figure 2: The relationship between the viscosity and temperature