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[54] **APPARATUS FOR SPINNING AND PROCESSING COLLAGEN FIBER**

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[51] **Int. Cl.**[6] **B05C 3/12**; B05C 3/00; B05C 19/02; B28B 5/00

[52] **U.S. Cl.** ..... **118/420**; 118/428; 118/67; 118/68; 264/131; 264/178 R; 264/183; 425/71

[58] **Field of Search** ..... 118/641, 58, 67, 118/68, 420, 428; 425/67, 68, 71, 104; 264/178 R, 181, 183, 189, 131, 186, 210.8

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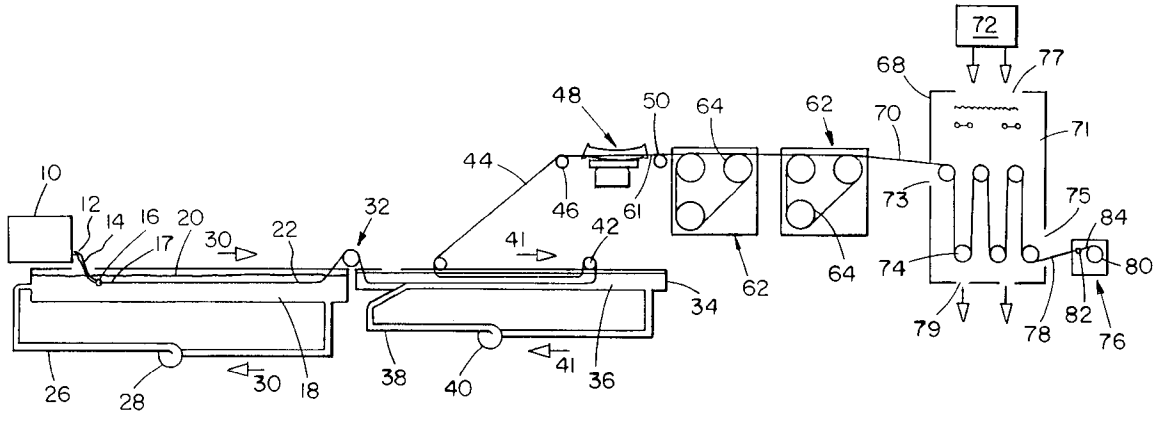
[57] **ABSTRACT**

An apparatus for forming a collagen fiber having microparticulates coated on the surface of the fiber and the method for forming the fiber are disclosed.

10 Claims, 2 Drawing Sheets



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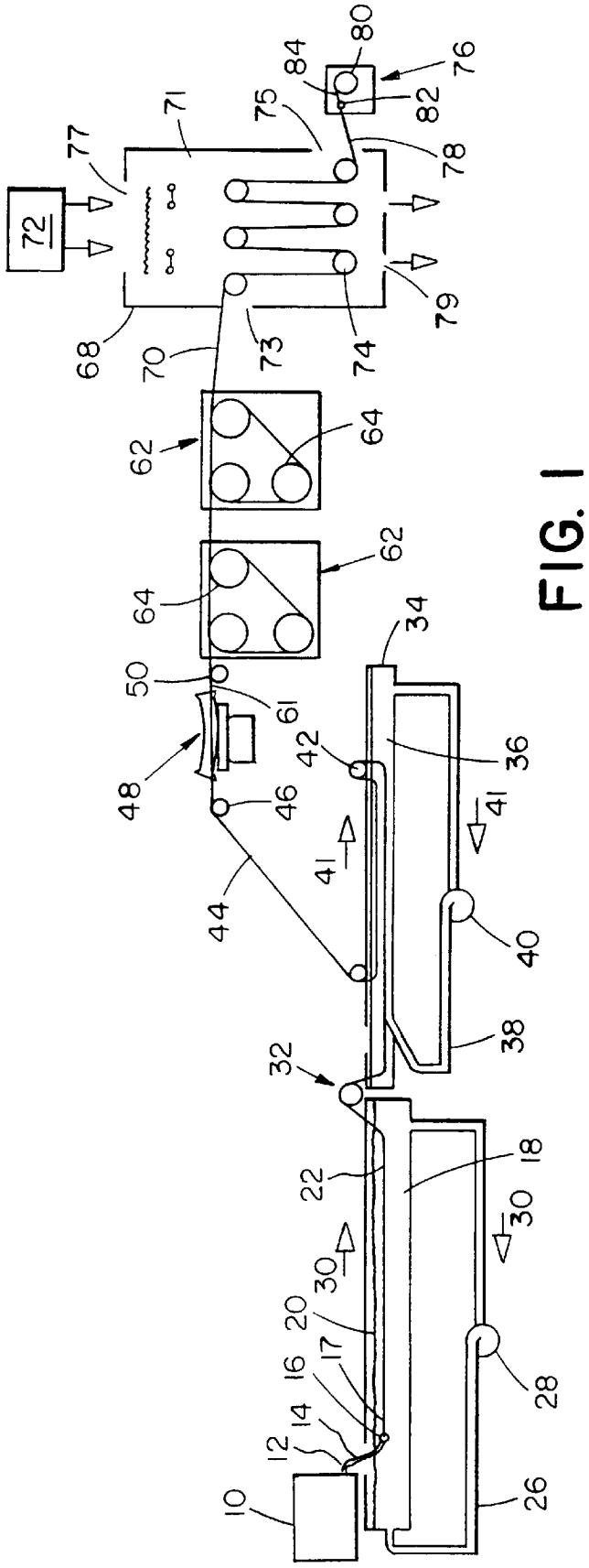
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FIG. 1

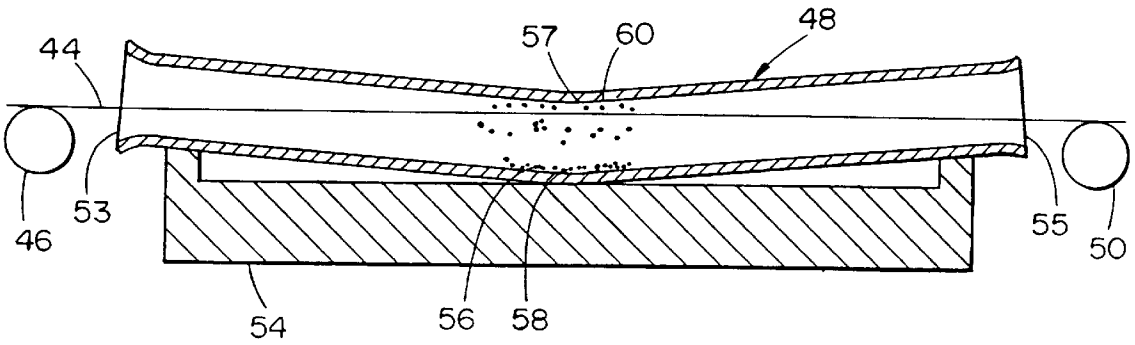

FIG. 2

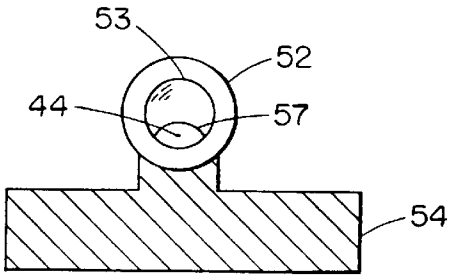

FIG. 3

APPARATUS FOR SPINNING AND PROCESSING COLLAGEN FIBER

This application is a divisional application of pending application Ser. No. 08/333,414 filed on Nov. 2, 1994.

BACKGROUND OF THE INVENTION

The use of synthetic materials, such as polyester fiber (Dacron™) or polytetrafluoroethylene (PTFE) (Teflon™), as implants designed to replace diseased or damaged body parts has been extensive. These materials have however, enjoyed limited success. This has been due to the poor biocompatibility of many of these materials which among other problems, frequently initiate persistent inflammatory reactions. Additionally, the failure of the body to integrate these materials, because they do not break down and do not lend themselves to remodeling by tissue cells that may come into contact with them, causes further problems.

Efforts to use animal or human materials have also been unsatisfactory when these materials are crosslinked by formaldehyde or glutaraldehyde, for example. The process of generalized aldehydic crosslinking renders biomaterials sufficiently unrecognizable to tissue cells so that normal remodeling and integration are not promoted. Similarly, other types of chemical processing of animal or human biomaterials, such as extraction with detergents, or hypertonic buffers or hypotonic buffers can alter them to the degree that they are ineffective in promoting angiogenesis and in stimulating repair and remodeling processes needed for the conversion of an implant into a functional substitute for the tissue or organ being replaced.

A third approach has been that of reconstituting issue and organ equivalents from structural matrix components, such as collagen, for example, that have been extracted and purified and combined with specialized cells. The process depends upon interactions between the cells and matrix proteins that the cells condense and organize. While tissue-like constructs have been fabricated and been shown to somewhat resemble their natural counterparts, they do not readily develop the matrix complexity characteristic of the actual tissues they are meant to imitate.

Therefore, a need exists for an improved apparatus and method for spinning and processing collagen fibers which will enrich them with the other constituents of the extracellular matrix.

SUMMARY OF THE INVENTION

The invention relates to a method for forming a collagen fiber having microparticulates coated to the surface of the fiber. The method includes directing a liquid collagen solution into a coagulation bath to form a continuous collagen gel fiber. The continuous collagen gel fiber is removed from the coagulation bath and directed into dehydrating bath, whereby the collagen gel fiber is partly dehydrated undergoing further polymerization. The partially dehydrated collagen fiber is removed from the dehydrating bath. Microparticulates are coated to the surface of the fiber, and the fiber is stretched. The microparticulate-coated fiber is then further dried.

The present invention also relates to an apparatus for forming microparticulate-coated collagen fibers. The apparatus includes means for forming a continuous liquid collagen stream. The apparatus also includes a coagulation bath, wherein a continuous liquid collagen stream can form a continuous collagen gel fiber, and a dehydrating bath, wherein the continuous gel fiber can be partially dehydrated.

Also included are means for applying microparticulates to the surface of the dehydrated fiber and means for stretching the microparticulate-coated fiber. The apparatus further has means for drying the microparticulate-coated fiber.

The present invention further includes an apparatus for applying microparticulates to the surface of a fiber. The apparatus includes a support base and a horizontal tube disposed on the support base. The tube has a first opening and a second opening, wherein the diameter of the tube is sufficient to allow passage of a continuous fiber under tension in a straight line into the first opening and from second opening. The apparatus also includes a microparticulate reservoir within the tube wherein the upper level of the reservoir is lower than the continuous fiber that can be drawn through the tube. The collagen fiber or yarn can be coated with microparticulates by forming a cloud of microparticulates in the tube, wherein the microparticulates can contact the fiber and be applied to the surface of the fiber. In a preferred embodiment, the horizontal tube is an inverted arch, wherein the lower portion of the tube forms the microparticulate reservoir.

The present invention has many advantages. The method and apparatus allows the formation of a uniform collagen fiber with finely coated microparticulates. Further, the method and apparatus allow coating of the collagen fiber without wasting the microparticulates since the excess falls continuously into the reservoir.

DESCRIPTION OF THE DRAWINGS

FIG. **1** is a schematic diagram of an apparatus of the present invention for forming a collagen fiber having microparticulates coated on the surface of the fiber.

FIG. **2** is a cross-sectional view of an apparatus for coating microparticulates on the surface of a fiber.

FIG. **3** is an end view of the apparatus shown in FIG. **2**.

DETAILED DESCRIPTION OF THE INVENTION

The features and other details of the method and apparatus of the invention will now be more particularly described with reference to the accompanying drawings and pointed out in the claims. The same numeral present in different figures represents the same item. It will be understood that the particular embodiments of the invention are shown by way of illustration and not as limitations of the invention. The principal features of this invention can be employed in various embodiments without departing from the scope of the invention. All parts and percentages are by weight unless otherwise specified.

One embodiment of the invention, as shown in FIG. **1** in a schematic view, is an apparatus for forming a collagen fiber having microparticulates coated on the surface of the fiber. The apparatus has collagen reservoir chamber **10** which is for holding a liquid collagen solution. The collagen can be derived from a suitable animal source, such as porcine, bovine, ovine or marine animal extracellular matrix from many tissues such as dermis, tendons, dental and connective tissue as well as others. In one embodiment, a suitable chamber is a stainless steel syringe. Reservoir tube **12** is attached to collagen reservoir chamber **10** for directing collagen solution from collagen reservoir chamber **10** through infusion pump **12** to spinneret **16**. Infusion pump **14** is capable of raising the pressure of the collagen material such that it can be extruded through spinneret nozzle **17** of spinneret **16**. In a preferred embodiment, a positive displace-

ment metering pump is used. Spinneret **16** can be single bore or multiple bore to produce monofilament or multifilament fibers respectively. The spinneret bores can be of various diameters or have tapered profiles to form fibers of different sizes and tensile strengths. Co-component fibers can be produced with other specialized spinnerets as are known in the art. In one embodiment, spinneret nozzle **17** has diameters in the range of between about 100 and 1,000 microns.

Coagulation bath **18** has a coagulation solution **20** that can cause the liquid collagen to form a collagen gel, such as a 0.75% alkaline alginic acid in a boric acid buffer or sugar solutions or polyethylene glycol solution which also has hydrophilic properties. The opening of spinneret is immersed in a flowing coagulation solution **20**. Coagulation bath **18** is suitably sized for allowing extrusion of fiber from spinneret **16** through coagulation solution **20** while having a sufficient residency time for collagen gel fiber **22** to form. Coagulation bath **18** can be heated and instrumented for monitoring the relevant process variables, such as temperature, pH and velocity. Coagulation bath **18** allows collagen gel **22** fiber to be formed in a horizontal trough or in a tube or vertically in a tube. Coagulation bath **18** is configured to allow circulation of coagulation solution **20** through recirculating loop **26** by circulating pump **28**. Coagulation bath flow can be in the same direction **30** of fiber travel. At the end of the coagulation bath **18**, roller **32** is for directing fiber out of the coagulation bath. Roller **32** is motorized and can be activated to wind collagen gel fiber **22** and subsequently tow collagen gel fiber **22** at desired speeds.

Dehydrating bath **34** is adjacent to roller **32** and coagulation bath **18** and is configured to allow fiber **36** to be drawn into dehydrating bath **34** from roller **32**. Dehydrating bath **34** holds dehydrating solution **36**, such as 90% ethanol, which allows further dehydration and annealing of the fiber and promotes polymerization of the collagen to improve fiber strength. An example of another suitable dehydration solution composition is acetone. Dehydrating bath **34** is configured to allow variable circulation of dehydrating solution **36** through recirculating loop **38** by circulating pump **40** which can be adjusted directionally, such as direction **41** or in the opposite direction. Return rollers **42**, which can be near each end of dehydrating bath **34**, allow the fiber path to be lengthened by doubling back to make any number of multiple passes through dehydrating bath **34** to allow further dehydration and promote polymerization of the collagen.

Partially dehydrated fiber **44** is wound around first applicator roller **46**, through particulate applicator **48** to second applicator roller **50**. Particulate applicator **48** applies a coating of microparticulates to the surface of a fiber as it passes through the applicator. Particulate applicator **48** allows the use of very small powder volumes of high value particulates, such as animal derived matrix (ADMAT), to be coated on the fiber with precision and control and with little loss of particulate matter as waste. Particulate applicator **48** can be operated intermittently as the fiber is passed through the application chamber to allow alternatively coated and uncoated sections of fibers. Particulate applicator **48** can provide a fiber drying effect via the hydration of the contacting dehydrated particulates by drawing liquid from the fiber, thereby aiding fiber polymerization. In a preferred embodiment, particulate applicator **48** has tube **52** curved in an inverted arch.

As shown in a cross-sectional view in FIG. **2** and in an end view in FIG. **3**, lower portion **58** of tube **52**, which is attached to support base **54**, forms particulate reservoir **56**. Tube **52** has a first opening **53** for receiving fiber **44** and second opening **55** at the other end of tube **52** to allow passage of fiber **44** under tension in a straight line to second applicator rollers **50**. Particulate applicator **48** has a pathway which is straight that is achieved by limiting the bend angle at upper portion **60** of the tube **52** such that the apex **57** of the top interior wall of chamber formed within the tube does not project below a height above first opening **53** and second opening **55** of tube **57**.

In base **54**, particle applicator **48** has means for suspending microparticulate particles to produce a particle cloud within tube **52**. The vibrational energy used to produce the cloud can be varied. Tube **52** is sufficiently sized to accommodate the maximum horizontal displacement amplitude of the input vibration, plus the diameter of the fiber. The vibrational frequency can be in the range of between about 1,000 and 3,000 cycles per minute for the size chamber used. The density of the dust cloud can be varied by changing the particulate mass and the frequency of vibration. Tube **52** is attached to a vibration means capable of producing the requisite horizontal and vertical components of vibration. The vibration can excite the particulates into motion to produce a dust cloud of a density dependent upon the amplitude and frequency of the vibration.

Tube **52** is sufficiently sized to allow airborne particulates which do not adhere to the fiber to settle into particulate reservoir pool **56** either directly or by sliding down the entrance or exit ramp floors of particulate applicator **48**. Such particulates can be recycled back into particulate dust cloud within particulate applicator **48**. In one embodiment, tube **52** has a diameter of about 1.8 cm, a length of about 17 cm and a bend angle of about 15°.

Returning to FIG. **1**, stretching roller means **62** is for receiving fiber from particulate applicator **48**, wherein the fiber can undergo a controlled deformation by being stretched between two groups of rollers **64** rotating at slightly different rates of speed. The speed of rotation of rollers **64** can be precisely controlled with digital microprocessors arranged in a closed feedback loop. The fibers are wrapped around each roller **64** several times to prevent fiber slippage relative to the roller surfaces. Roller **64** surfaces can made of a polymer or a hardened metal resistant to corrosion. Roller **64** rotations can be adjusted individually to allow the fiber to be stretched beyond the elastic yield point to produce a longer fiber of reduced diameter. Stretching roller means **62** can operate under semi-dry or dry conditions and also under high moisture content atmosphere.

Drying cabinet **68** has opening **73** for receiving stretched fiber **70** from stretching rollers **62**. Drying cabinet **68** has passage **71** through drying cabinet **68** for receiving warm, dry filtered air or a dry inert gas, such as dry nitrogen gas, from gas source **72** at a suitable temperature and humidity for drying stretched fiber **70**. The air can be passed through air passage opening **77** into passage **71** and exiting from air passage opening **79**. In one embodiment, the temperature of the air is between about 35° C. and 39° C. The humidity is in the range of between 10 and 20 percent relative humidity. Drying cabinet **68** has a series of rollers **74** which allows stretched fiber **70** to remain in drying cabinet **68** while being rolled, thereby increasing the residence time of fiber **70** in drying cabinet **68**. Drying cabinet rollers **74** are adjustable in distance between each other and to compensate for the fiber line speed. Drying cabinet rollers **74** can be driven at a surface roller speed that can be synchronized with that of stretching roller means **62**. Drying cabinet **68** has a door to provide access to the rollers for threading the leader thread.

Take-up winder **76** is for receiving dried fiber **78** from exit **75** of drying cabinet **68**. Take-up winder **76** has spool **80** for

receiving dried fiber on a removable spindle bobbin. Take-up winder **76** has a slip clutch **82** to provide a constant fiber line tension and fiber line speed as the spooled fiber rotates radially around spool **80**. Fiber spool **80** can wind the fiber level or by randomly winding with the take-up winder **76**.

A preferred source material for a source of collagen consists of the skins from near-term, domestic porcine fetuses which are harvested intact, enclosed in their amniotic membranes. Embryonic and fetal tissues are advantageous because they include various molecular factors which are present in normal tissue at different stages of animal development. Other sources for extracellular matrix material are diverse tissues found in organs from porcine, bovine, ovine, marine or other animals.

The collagen fibers or yarn decorated with the informational microparticulates can be used to create strips, sheets, tubes and other shapes using textile machinery by those skilled in the art. The shapes can be in the form of tissues or body parts to be replaced and constitute prostheses.

The extracellular matrix particulates taken from specific tissues have two kinds of informational properties. The first is their molecular diversity and the second is their microarchitecture both preserved in the preparation of the microparticulates. The preferred associations among the different molecules of the extracellular matrix are also preserved in the preparation of the microparticulates.

The extracellular matrix particulates can have cytokines, including growth factors necessary for tissue development. These biomolecular factors are present in normal tissue at different stages of tissue development, such as cell division morphogenesis and differentiation. Among these factors are stimulatory molecules that provide the signals needed for in vivo tissue repair. These cytokines including growth factors, being part of the extracellular matrix microparticulates, can stimulate conversion of an implant into a functional substitute for the tissue being replaced. It is believed that it can do this by mobilizing tissue cell from contiguous like tissues, from the circulation and from stem cell reservoirs; it can promote cell division, morphogenesis and differentiation. Cells can attach to the prostheses which are bioabsorbable and can remodel them into replacement tissues.

Growth factors necessary for cell growth are attached to structural elements of the extracellular matrix. The structural elements include proteins, glycoproteins, proteoglycans and glycosaminoglycans. The growth factors, originally produced and secreted by cells, bind to the extracellular matrix and regulate cell behavior in a number of ways. These factors include, but are not limited to, epidermal growth factor, fibroblast growth factor (basic and acidic), insulin growth factor, nerve growth-factor, mast cell-stimulating factor, platelet-derived growth factor, the family of transforming growth factor-β, platelet-derived growth factor, scatter factor, hepatocyte growth factor and Schwann cell growth factor. Adams et al., "Regulation of Development and Differentiation by the Extracellular Matrix" *Development* Vol. 117, p. 1183–1198 (1993) (hereinafter "Adams et al.") and Kreis et al. editors of the book entitled "Guidebook to the Extracellular Matrix and Adhesion Proteins," Oxford University Press (1993) (hereinafter "Kreis et al.") provide contributions which summarize extracellular matrix components that regulate differentiation and development and describe the regulatory mechanisms involved and that growth factors and extracellular matrix molecules interact in a number of ways to regulate cell behavior. Further, Adams et al. disclose examples of association of growth factors with extracellular matrix proteins and that the extracellular matrix is an important part of the micro-environment and, in collaboration with growth factors, plays a central role in regulating differentiation and development. The teachings of Adams et al. and Kreis et al. are incorporated herein by reference.

The method for forming extracellular matrix particulates for producing graft tissue includes freezing a tissue source having living cells, whereby the living cells are disrupted to form cell remnants. The tissue source is then cryomilled to produce particulates which are thawed and are processed leaving extracellular matrix particulates including cytokines. The term cytokines includes but is not limited to growth factors, interleukins, interferons and colony stimulating factors. The process of washing removes the cell remnants without removing growth and other factors necessary for cell growth, morphogenesis and differentiation. The extracellular matrix is freeze-dried and, if desired, further fragmented.

A method for forming extracellular matrix particulates for producing graft tissue is disclosed in U.S. patent application Ser. No. 07/926,885, filed Aug. 7, 1992, entitled "A Method for Producing Graft Tissue Extracellular Matrix". The teachings of which are herein incorporated by reference. The method for forming extracellular matrix particulates for producing graft tissue includes freezing a connective tissue source having living cells, whereby the living cells are disrupted to form cell remnants. The connective tissue source is processed to remove the cell remnants without removing growth factors necessary for cell growth, differentiation, and morphogenesis to form an extracellular matrix. The extracellular matrix is freeze-dried and fragmented. The extracellular matrix is further processed to remove cytoplasmic and nuclear components without removing the growth factors necessary for cell growth to form extracellular matrix particulates. In one embodiment, the extracellular matrix particulates associated with collagen fibers in a three-dimensional matrix are exposed to cultivated cells under such conditions that the cultivated cells adhere to the extracellular matrix particulates, alone or to the particulates and the collagen fibers thereby producing graft tissue.

In a preferred method for extracting the collagen from tissue, a collagen source includes porcine fetuses. The fetuses are frozen in utero with the uteri maintained in an unbroken condition with the ends tied off by string. Twelve to twenty-four hours before dissection, a uterus is removed from the freezer and placed in a 4° C. cold room. The uterus, which should still be about 90% frozen, is transferred into a large sterile dishpan. As soon as possible, the folded uterus is gently straightened. The exterior surface of the uterus is washed twice for 10 minutes in 1% bleach in Milli-Q™ water and is then washed twice with sterile Milli-Q™ water to sterilize the uterus.

Under clean-room conditions using sterile, large tissue grip forceps and large scissors, and wearing sterile gloves, mask, hood and gown, the entire length of the uterus on the surface opposite the major blood vessels is opened. Care is taken not to touch or damage the amniotic membranes of the fetus. Instruments that come in contact with the outer surface of the uterus are washed with 70% ethyl alcohol and sterilized with a Bunsen burner. Each fetus is gently lifted from the uterus and the umbilicus is cut at least 2 cm from the fetus. The still mainly frozen fetus is placed into a stainless steel pan.

With sterile gloves, the amniotic membrane is removed and the fetus transferred to a sterile glass dish. With a sterile

scalpel, such as a #11 blade, the skin around each foot is sliced to make a circular incision. A single incision is made through the skin from the first cut, along the inner surface of each limb to the midline of the ventral surface of the trunk. A midline incision is made along the ventral surface of the trunk from the tail to the neck, taking care not to penetrate the underlying muscle tissue. A skin deep circular incision is made around the circumference of the head. The body skin is peeled off. The peeled skin is placed into a sterile container (one liter centrifuge bottle with cap) on ice.

The skins are combined with an equal volume of sterile ice, and the ground tissue is washed twice in 20 liters of ice cold 0.33× phosphate buffered saline (PBS):Mill-Q™ water (1:2) with about 30 minutes allowed for tissue to settle between washes. The tissue is evenly divided into one liter centrifuge bottles as required and each filled with 0.5M acetic acid and 4 mM EDTA. The centrifuge bottles are placed on a roller bottle apparatus for about seven days at a temperature of about 4° C.

On the eighth day after the beginning of the skin preparation, the centrifuge bottles are spun for thirty minutes at 5,000 rpm. The supernatant is aseptically collected in a sterile carboy (20 or 50 liters). The collected supernatant is filtered through four layers of sterile cheese cloth. Sterile sodium chloride is added to bring the solution to about 0.9M. It is stirred over a period of about one hour then placed in a cold room at about 4° C. overnight. The collagen is resuspended. The entire salt precipitated solution and the precipitate is dispensed into sterile one liter centrifuge bottles. The bottles are centrifuged at 5,000 rpm for about thirty minutes using a 6× one liter rotor at about 7,280 gs. The supernatant is removed, and the pellet is kept. To the pellet in each centrifuge bottle, 0.5M acetic acid pH 2.5 plus 4 mM EDTA is added. The pellets are dispersed in the medium and shaken in a gyrator shaker for about sixteen hours at a temperature of about 4° C. The pellets from the bottles are transferred to a six liter flask, by rinsing each bottle with the 0.5M acetic acid, EDTA solution and pouring the mix into the flask. In the six liter flask, the pellets are dispersed with a sterile glass rod. The flask is placed on a shaker for 24 hours at a temperature of about 4° C. The flask is checked for degree of solubilization and resuspension. More 0.5M acetic acid and EDTA solution may be added to bring the volume to five liters.

Sterile sodium chloride is added to the flask to bring the solution to about 0.7M. It is stirred periodically over a period of one hour and then placed in a cold room at a temperature of about 4° C. overnight allowing the salt to precipitate.

The contents are shaken and dispensed into one-liter sterile centrifuge bottles and spun at about 5,000 rpm for 30 minutes at 7,280 gs. A second resuspension is conducted with the step similar to the steps described above for the first resuspension. Instead, of resuspending in six liters, a total volume of two liters is employed in the resuspension process. The flask is shaken in the cold room overnight and its volume adjusted as necessary.

The solution is dialyzed three times for about 20–24 hours against one hundred liters of ice cold 0.05% 0.5M acetic acid in the cold room (4° C.) using 6,000–8,000 MW cutoff, Spectrapore dialysis bags. The dialysis bag is slit with a sterile scalpel blade and the contents transferred into sterile 250 ml centrifuge bottles. The bottles are centrifuged at a temperature of about 4° C. at 10,000 rpm (13,000 g) for one hour. The supernatant is collected and stored in a sterile, sealed bottle.

A 0.5 ml aliquot of the supernatant is removed, combined with equal volume of concentrated hydrogen chloride and the collagen concentration measured using an hydroxyproline assay. The collagen is concentrated to a theoretical concentration of 5 mg/ml using a hollow fiber filter. The concentration can be confirmed with a hydroxyproline assay.

Liquid collagen is extracted from a suitable source, such as described above, and can be mixed with acetic acid and concentrated to five milligrams per milliliter. Liquid collagen can have an additive, such as alginate, or not have additives included. Liquid collagen is centrifuged at about 3,200 rpm and about 1,610 g to reduce gas dissolved in the liquid.

The liquid collagen is transferred into the reservoir chamber and further degassed by the application of a vacuum for a period of time, such as twenty-minutes, thereby allowing essentially all the gas to be removed from the collagen. The liquid collagen is maintained in collagen reservoir chamber **10** at a temperature in the range of between about 4° C. and 22° C. Liquid collagen is pumped from collagen reservoir chamber **10** by infusion pump **14** through collagen reservoir tube **12** and extruded through spinneret nozzle **17** of spinneret **16**. Various types of fibers can be formed depending upon the spinneret used. The bore holes in spinneret **16** can have various diameters, length to diameter ratios and tapered profiles to form fibers of different sizes and tensile strengths. The formed fibers can have sizes in the range of between 50 and 200 denier. The extruded collagen gel fiber **22** is directed into coagulation solution of coagulation bath **18** at a speed of about two milliliters per minute, for example.

Concurrently, coagulating solution **20** is circulated by circulation pump **28** in a direction parallel with the direction of the extruded collagen gel fiber **22**. The speed of coagulating solution **20** can be the same as the speed of collagen gel fiber **22**. In one embodiment, coagulating solution **20** is heated to a temperature of about 35° C., and the bath is monitored for pH, temperature and velocity. The pH is maintained in a range of between about eight and ten. Continuous collagen gel fiber **22** is formed by polymerization when the acid in the collagen is neutralized upon contact with the alkaline alginic acid/boric acid bath or other suitable neutralizing solution. The ratio of the coagulating bath speed to the infusion rate determines the size fiber for a given spinneret bore. During the residence of collagen fiber gel **22** in coagulation bath **18**, polymerization and dehydration and occur. Fiber residence time is determined by the length of coagulating bath **18** and velocity of coagulation solution **20**, the velocity of the collagen at spinneret **16** and the velocity at which the fiber is withdrawn from the bath. An example of a suitable residence time is about two minutes.

At the end of coagulation bath **18**, collagen gel fiber **22** is removed from coagulation solution **20**. In one embodiment, a leader thread is tied to collagen gel fiber **22** to guide it to dehydrating bath **34**. In the shown embodiment, collagen gel fiber **22** is directed over roller **32** after collagen gel fiber **22** exits from coagulation solution **20**. The leader thread is carried along the downstream fiber process path and motorized rollers are activated to wind the thread which tows the collagen fiber.

Collagen gel fiber **22** is directed from roller **32** into dehydrating solution **36** in dehydrating bath **34** pulled by the leader thread. Dehydrating solution **36** is composed of about ninety percent ethanol and ten percent water. The ethanol further dehydrates and anneals the fiber and promotes the polymerization of the collagen to improve fiber strength. As done with coagulation solution **20**, dehydrating solution **36** is recirculated by circulating pump **40** through recirculation

loop **38** and dehydrating bath **34**. Partially dehydrated fiber **44** can be passed through the dehydrating solution **36** one or more times. The fiber residence time in the dehydrating bath is determined by the speed of the fiber into and out of the bath, the distances between return rollers and the number of passes the fiber makes between return rollers. In one embodiment, the partly dehydrated fiber is in the dehydrating solution **36** for about five to six minutes. The partially dehydrated fiber **44** is directed from the dehydrating bath to particulate applicator **48**. The surface of the partly dehydrated fiber **44** is sufficiently wet to permit adhesion to it of microparticulates, such as ADMAT or other particulate materials that can be applied as the next step of the process to produce a coated fiber.

Fiber **44** is directed through first opening **53** of particulate applicator **48** through horizontal tube **52** and out of second opening **55**. Fiber **44** is positioned within tube **52** so that fiber **44** does not come into contact with any of the sides of tube **52**.

In lower portion **58** of tube **52**, microparticulate reservoir **56** is formed having been loaded with tissue specific microparticulates, for example, from alveolar bone which surrounds teeth. The reservoir can be cooled to protect the biological activity of the particulates. Energy is applied to microparticulate reservoir **56** to cause at least a portion of microparticulates to become airborne. In one embodiment, vibrational energy is directed into microparticulate reservoir. The vibrator operates between about 1,000–3,000 cycles/minutes at an amplitude sufficient to maintain a microparticulate cloud with no displacement of the fiber passing through it. The amount of particulate coating is controlled by the particulate size, total volume of particulates within the applicator chamber, dimensions of the applicator chamber, velocity of a fiber through applicator chamber, the free liquid content of the surface of the fiber, moisture content of the fiber, frequency of the applicator chamber vibration, amplitude of the applicator chamber vibration and static charge of the particles. Tube **52** is vibrated by a mechanical shaking mechanism capable of producing the required horizontal and vertical components of vibration. The vibrational generator excites the particulates into motion to produce a dust cloud.

Particulate applicator **48** can be operated intermittently as the fiber passes through the tube **52** to produce alternatingly coated and uncoated sections of dehydrated fiber **44**. Other selected fiber coatings and other patterns can be applied. Particulates which become airborne and do not adhere to the fiber within tube fall under the gravity and return to lower portion **58** in particulate reservoir **56** either directly or by sliding down tube **52**. In this manner, particulates are recycled back into particulate dust cloud **59** within tube **52**.

Coated fiber **61** is directed from second applicator roller **50** of particulate **48** applicator to stretching roller means **62**. Coated fiber is stretched by force developed between two groups of stretching rollers **64** rotating at slightly different rates of speed. The speeds of rotation of the roller groups **64** can be controlled with digital microprocessors arranged in a closed feedback loop. Stretching roller **64** speeds are controlled so that the ratio may be adjusted such that the fiber is stretched beyond the elastic yield point to produce a longer coated fiber of reduced diameter. Coated fiber **61** is wrapped three or four times around each set of stretching roller **64** to prevent slippage. Stretching rollers **64** can be arranged in series to stretch coated fiber **61** at each roller.

Stretched fiber **70** is directed from stretching roller means **62** to drying cabinet **68**. Stretched fiber **70** is directed through opening **73** to drying cabinet **68** as drying cabinet **68** is flushed with warm dry filtered air at a temperature in the range of between about 35° C. and 39° C. Stretched fiber **70** is directed around drying cabinet rollers **74** contained in the drying cabinet **68** as air is blown over stretched fiber **70**. Stretched fiber **70** maintains a minimum residence time to allow stretched fiber **70** to become dried. Drying cabinet rollers **74** are synchronized with the last group of stretching roller means **62** so that stretched fiber **70** does not stretch to a point of breaking.

Dried fiber **78** is directed through exit **75** of drying cabinet to take-up winder **76**. Take-up winder **76** spools dried fiber **78** on a removable spindle bobbin. Take-up winder **76** incorporates the change of speed of dried fiber **78** as it is taken up on take-up winder **76** to provide a constant fiber line tension as the spool. fiber package builds up radially. The fiber is wound either in order or randomly with the take-up mechanism.

Equivalents

Those skilled in the art will recognize, or be able to ascertain using no more than routine experimentation, many equivalents to specific embodiments of the invention described specifically herein. Such equivalents are intended to be encompassed in the scope of the following claims.

What is claimed is:

1. An apparatus for forming microparticulate-coated collagen fibers, comprising:

a) means for forming a continuous liquid collagen stream;

b) a coagulation bath, wherein a continuous liquid collagen stream can be formed into a continuous collagen gel fiber;

c) a dehydrating bath, wherein said continuous collagen gel fiber can be partially dehydrated and further polymerized; and

d) means for coating microparticulates on the surface of the partly dehydrated fiber, said means including

a support base;

a horizontal tube disposed on and rigidly attached to said support base, said tube having a first opening and a second opening, wherein the diameter of said tube is sufficient to allow passage of a continuous fiber under tension in a straight line into the first opening and from second opening, said horizontal tube being an inverted arch, wherein the lower portion of said horizontal tube forms the microparticulate reservoir;

a microparticulate reservoir within said tube, wherein the upper level of the reservoir is lower than the passage for said continuous fiber; and

means for shaking said support base and said tube as one unit to suspend said microparticulates in said tube, wherein the microparticulates can contact the fiber and be coated on the surface of the fiber.

2. The apparatus of claim **1** wherein the apparatus further includes means for stretching said microparticulate-coated fiber.

3. The apparatus of claim **2** wherein the apparatus further includes means for drying said microparticulate-coated fiber.

4. The method of claim **3** wherein means for forming a continuous liquid collagen stream includes collagen extract from fetal, young or adult pigs.

5. The method of claim **4** wherein the coagulation bath includes a solution of alkaline alginic acid/boric acid.

6. The method of claim **5** wherein the dehydrating includes a solution of ninety percent ethanol.

7. The method of claim **6** wherein said microparticulates include an animal derived matrix.

8. An apparatus for applying microparticulates to the surface of a fiber, said apparatus comprising

a) means for forming a continuous liquid collagen stream;

b) a coagulation bath, wherein a continuous liquid collagen stream can be formed into a continuous collagen gel fiber;

c) a dehydrating bath, wherein said continuous collagen gel fiber can be partially dehydrated and further polymerized; and

d) means for coating microparticulates on the surface of the partly dehydrated fiber, said means including

a support base;

a horizontal tube disposed on said support base, said horizontal tube having a first opening and a second opening, wherein the diameter of said horizontal tube is sufficient to allow passage of a continuous fiber under tension in a straight line into the first opening and from second opening, said horizontal tube being an inverted arch, wherein the lower portion of said horizontal tube forms the microparticulate reservoir;

a microparticulate reservoir within said tube, wherein the upper level of the reservoir is lower than the passage for said continuous fiber; and

means for suspending said microparticulates in said tube, wherein the microparticulates can contact the fiber and be coated on the surface of the fiber.

9. The apparatus of claim 8 wherein said means for suspending said microparticulates includes a vibrational generator.

10. The apparatus of claim 9 wherein said vibrational generator operates at a frequency in the range of between about 1,000 and 3,000 cycles per minute and an amplitude of about one millimeter or less.

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