

EUROPEAN PATENT SPECIFICATION

- ④ Date of publication of patent specification: **23.01.85** ⑤ Int. Cl.⁴: **C 08 L 75/06, C 08 L 67/06 // C08L75/02**
⑥ Application number: **80303639.1**
⑦ Date of filing: **15.10.80**

⑧ **Solutions of resins in a monomer, containing polyamine reactable with isocyanates, moulding compositions and cured product thereof.**

⑨ Priority: **29.10.79 US 89128**

⑩ Date of publication of application:
13.05.81 Bulletin 81/19

⑪ Publication of the grant of the patent:
23.01.85 Bulletin 85/04

⑫ Designated Contracting States:
AT BE CH DE FR GB IT LI LU NL SE

⑬ References cited:
DE-A-2 337 706
DE-A-2 707 230
DE-A-2 715 294
US-A-4 107 101

⑭ Proprietor: **ICI AMERICAS INC**
Concord Pike & New Murphy Road
Wilmington Delaware 19897 (US)

⑮ Inventor: **Magrans, Juan Jose, Jr.**
2602 Bel Air Drive
Wilmington Delaware 19808 (US)

⑯ Representative: **Jones, Martin et al**
Imperial Chemical Industries PLC Legal
Department: Patents Po Box 6
Welwyn Garden City Herts, AL7 1HD (GB)

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European patent convention).

Description

This invention is directed to blends of polyamines, ethylenically unsaturated monomers and certain ethylenically unsaturated resins such as vinyl-terminated polyester urethane resins, ethylenically
 5 unsaturated polyester resins, and ethylenically unsaturated polyisocyanurate resins, which can be thickened by the addition of polyisocyanates to form polyurea moulding compositions which are tack-free within a few minutes. It is also directed to the gelled or thickened unsaturated monomer solutions of these resins which are obtained by the homogeneous intermixing of polyamines and polyisocyanates. It is further directed to a process for the formation of gelled solutions wherein a
 10 relatively large molar excess of aromatic polyisocyanate is added to an ethylenically unsaturated monomer solution containing polyamines and one or more of the ethylenically unsaturated polyester, polyisocyanurate or polyester urethane resins. When fully cured by addition reaction between the ethylenically unsaturated components the resulting compositions are surprisingly high in flexural and tensile strength. The moulding compositions made from the resins of this invention when mixed with
 15 glass and other fillers, pigments, peroxides, mould release agents and so forth can be converted into tractable, tack-free, handleable gels which can be cut into preforms and shaped by either injection or compression moulding techniques.

Prior art

20 Moulding compositions employing ethylenically unsaturated polyester resin blends having unreacted carboxyl groups and vinyl monomers have been thickened by the addition of inorganic materials such as calcium or magnesium oxide. Gelation takes place rather slowly with the employment of these oxides and in some instances requires as much as two or three days to obtain a handleable or non-sticky sheet moulding product. If not moulded within a short period of time thereafter they must be
 25 discarded since the gelation and cross-linking continues to a point where the composition is no longer tractable.

In recent years the automobile industry has been striving to reduce weight in newly manufactured vehicles as a means of reducing fuel consumption. A most attractive way to reduce weight is to substitute metal with lightweight plastic components. However plastics are inherently weak and must
 30 be highly reinforced to meet the tensile strength requirements of certain components such as wheels, brackets, structural panels and bumpers. In order to meet these requirements resins must be reinforced with materials such as glass fibre filaments in high concentrations mostly exceeding 50% by weight. Compositions having large amounts of filler, while producing very strong completely cured resins, are difficult to mould in articles having uniformly distributed reinforcing materials. In producing moulded
 35 articles having intricate shapes, wherein a preform containing fibre reinforcement is squeezed between male/female sections of a mould and the flowout exceeds 30%, it is difficult to obtain a uniformly reinforced article. Usually resin flows away from the fibre filler leaving the article more highly filled in the region of the original preform and scantily filled or resin rich at the mould extremities or locations of maximum flow.

40 More recently however polyurethane resins systems have been used to thicken ethylenically unsaturated monomers and monomer solutions of polyester where there are insufficient reaction sites present within the system which can undergo a thickening reaction with the alkaline oxides. Such systems are described in U.S. 3,047,530; 3,290,208; 3,455,857; 3,464,935; 3,644,569; 3,700,752; 3,859,381; 3,868,431; 3,886,229; 3,893,956; 3,962,370; 3,994,764; 3,997,490; 4,062,826;
 45 4,086,203; and 4,128,600. The thickener systems described in these patents include both linear and branch polyurethane copolymers and have been used to thicken monomer solutions of ethylenically unsaturated polyester resins.

Of particular interest are patents directed to thickener systems employing both urethane and urea linkages as described in U.S. 4,073,828 and 4,129,641. Such systems employ an —NCO terminated
 50 polyester free of ethylenic unsaturation having a molecular range of 500—3,000 as a polyisocyanate source for reaction with a polyamine. The present system differs in that a relatively high molecular weight polyamine is reacted with a relatively low molecular weight polyisocyanate to form a composition having only polyurea linkages in the gel resin polymer chain. Because the rate of reaction between amines and isocyanates is extremely fast, unsaturated monomer can be readily thickened or
 55 gelled by 5—50% by weight of polyurea precursors. In addition to monomer may be incorporated 5—95% by weight of a prepolymerized resin which may or may not contain ethylenic unsaturation. For example ethylenically unsaturated polyesters, ethylenically unsaturated polyisocyanurates and polyethylenically unsaturated polyester urethane resins are particularly compatible and can be converted within minutes to a handleable tack-free gel which can be stored under normal conditions for
 60 long periods of time before they are formed by injection and compression moulding techniques.

In the practice of the invention essentially three steps are taken:

The first involves formation of an ethylenically unsaturated monomer solution having dissolved therein 1.5—30% by weight based on the total weight of said solution of a polyamine free of ethylenic
 65 unsaturation. This solution also contains 30—70% by weight of a soluble polymeric resin which contains ethylenic unsaturation.

In the second step the monomer solution is gelled or thickened by the addition thereto of an organic polyisocyanate free of ethylenic unsaturation.

In the third step the gelled material is moulded and fully cured by the polymerization of the monomer and/or copolymerization of the monomer and unsaturated resin.

5

Polymer-in-monomer solutions

Polyester resins

The hereinafter described unsaturated monomers may be used in combination with from 30—70% by weight of ethylenically unsaturated resins. Such resins may include unsaturated polyester resins made by reacting carboxylic acids or their anhydrides with polyhydric alcohols. These materials usually have molecular weights ranging from 400—4,000 and often 1,000—3,000. Unsaturated polyesters can be prepared by a procedure wherein at least one of the reactive components contains alpha, beta-ethylenic unsaturation. These resins are primarily linear but may contain branch chains by the addition of polyols or polycarboxylic acids having more than two functional groups. Usually they contain a plurality of ethylenically unsaturated linkages distributed along the backbone of their polymer chains. The use of alpha, beta-ethylenically unsaturated polycarboxylic acid provides a convenient method of introducing ethylenic unsaturation into the polyester resin. It is preferred to employ dicarboxylic acids such as maleic, fumaric, citraconic, gamma-dimethylcitraconic, mezaconic, itaconic, alpha methylitaconic, gamma-methylitaconic and tetraconic as well as mixtures thereof but minor amounts of alpha, beta-ethylenically unsaturated polycarboxylic acids containing three or more carboxylic groups such as aconitic and alike together with the dicarboxylic acids are also useful.

Whenever available the anhydrides of any of the aforementioned alpha, beta-ethylenically unsaturated polycarboxylic acid may be substituted for the acid. In addition suitable saturated acids, or their anhydrides when available, may also be incorporated along with the unsaturated polycarboxylic acids and include for example phthalic acid or anhydride, isophthalic acid, terephthalic acid, tetrabromophthalic acid, tetrachlorophthalic acid, adipic acid, sebacic acid, glutaric acid or pimelic acid or their mixtures. Of particular interest may be mentioned a mixture of isophthalic or orthophthalic acid and fumaric or maleic acids.

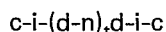
Any of a large number of ethylenically unsaturated or saturated polyhydric alcohols may be employed with any of the above suitable mixtures. Dihydric alcohols and especially saturated aliphatic diols are preferred as coreactants in the preparation of polyester resins. Among the dihydric alcohols which may be employed are saturated aliphatic diols such as ethylene glycol, propylene glycol, butylene glycol, diethylene glycol, dipropylene glycol, triethylene glycol, tetraethylene glycol, butylene diol, pentane diol, hexane diol, neopentyl glycol, bisphenol A and alkoxylated derivatives thereof such as oxypropylated bisphenol A and mixtures thereof. Polyols having more than two hydroxy groups which may be employed in minor amounts to form branch chains can be selected from saturated aliphatic polyols such as glycerol, trimethylolethane, trimethylolpropane, pentaerythritol, arabitol, xylitol, dulcitol, donnitol, sorbitol, mannitol and alike as well mixtures thereof. In addition aliphatic aromatic diols and polyols may be employed as well as halogenated and alkoxylated derivatives thereof. In most instances the condensation products contain unreacted carboxylic acid or hydroxyl groups at the end of the chain branches. In the present invention the active hydrogens remaining on the hydroxyl or carboxyl group may be removed by neutralization but such precautions are not considered necessary to prevent cross linking to the thickener chain because the reaction of the amine with the isocyanate takes place more readily. A preferred polyester resin is a condensation product of a polyalkoxylated bisphenol A compound, an unsaturated dicarboxylic acid and an aromatic dicarboxylic acid.

Preparation A

A polyester resin is prepared by condensing equal molar quantities in a resin kettle of isophthalic acid, propylene glycol, dipropylene glycol, and maleic anhydride until an acid number of not less than 25 is obtained and thereafter dissolving of the resin in styrene to form a 60% resin in styrene solution.

Polyesterurethane resins

Other ethylenically unsaturated resins may be added along with or in place of polyester resin such as vinyl ester urethane resins such as those disclosed in U.S. Patent 3,876,726; 3,297,745; 3,371,056; 3,509,234; 3,641,199; 3,642,943; and 3,677,920. These polyurethanes have the general formula:



wherein d is a radical derived from an organic polyol, n is a radical derived from an unsaturated aliphatic dicarboxylic acid or an anhydride thereof, i is a radical derived from a polyisocyanate, c is a carbamyl-linked radical derived from a hydroxy-terminated ester of acrylic or methacrylic acid, and t is an integer of 1—5; and must be substantially free of unreacted isocyanate groups so as to preclude the formation of urea cross-links with the polyurea thickener chain. A preferred vinyl ester urethane resin is one in which the organic polyol is a polyoxyalkylene bisphenol A having 2—60 mols of ethylene oxide or

propylene oxide per mol, n is derived from maleic acid or maleic anhydride and i is a radical derived from toluene diisocyanate or a polyisocyanate having 2.4 to 3 isocyanate groups per mol.

Preparation B—Polyester urethane resin

5 Into a two litre reaction flask equipped with a stirrer, thermometer, nitrogen inlet tube and distillation head there is added 4 mols of oxypropylated bisphenol A containing an average of 2.2 mols of propylene oxide per mol of bisphenol A and 2 mols of maleic anhydride. The resulting reaction mixture is heated to between 210°—215°C. 1 mol of the diester which results is further reacted in the presence of 1.44 grams of hydroquinone, by heating to 80°C with 2 mols of hydroxypropylmethacrylate and 2 mols of toluene diisocyanate and mixing for a period of 1 hour. The reaction mixture is permitted to rise to a temperature of 135°C and held at that point for 1/2 hour. The resultant light colored solid has a melting point of 97°C, an acid number of 7.6, a saponification number of 201, a hydroxyl number of 22, and no residual unreacted isocyanate. The resulting resin is ground to a white finely divided powder and dissolved in styrene to form a 50% solids containing solution.

15 Preparation C—Polyester urethane resin

Into a reactor equipped with a stirrer, thermometer and dry air inlet tube were added 0.358 gram mols of a hydroxy-terminated polyester oligomer formed by reacting 4 molar equivalents of oxypropylated (2.2) bisphenol A with 2 molar portions of maleic anhydride, heated to 80°C with 182 grams of styrene and 190 grams (1.22 mols) of 94% hydroxypropyl methacrylate after which the temperature dropped to 45°C. At this point 255 grams (0.717 mols) of Rubinate M, crude polymethylene polyphenyl isocyanate having an average isocyanate functionality of 2.7, were added dropwise causing the temperature to rise to about 79°C. The temperature of the mixture was raised to 90—95°C and held for 5 hours after which point no detectable amount of free NCO groups could be found by infra-red analysis. Additional styrene was added to yield a 50% solid styrene solution. This resin-styrene solution has a viscosity of 380 mPa . s (No. 2 spindle in Brookfield at 30 rpm) at room temperature. The resin styrene solution has an acid number of 2.8, a saponification number of 101 and a hydroxyl number of 5.8.

30 Polyisocyanurate resins

The polymer-in-monomer solution may also include polyisocyanurate resins, such as poly(1,3,5-tri-R substituted s-triazine-2,4,6-trione), wherein the R group may contain ethylenic unsaturation or groups reactive with ethylenically unsaturated materials. R groups may also be linked with epoxy, polyurethane and polyester resins. Such isocyanurates are represented by U.S. Patent 2,952,665; 3,041,313; 3,821,098; 3,850,770; 3,719,638; 3,437,500; 3,947,736; 3,763,269 and 4,218,537. For the purpose of this disclosure polyisocyanurate resins can be considered as cross-linked networks of isocyanurate rings having ethylenically substituted aromatic pendant groups. Aromatic rings may be linked to ethylenically unsaturated groups through carbamyl, ureylene, ether, carbonyl, carboxyl, and combinations thereof. In most instances satisfactory resins are prepared by reacting a polyisocyanate with hydroxyl-terminated ethylenically unsaturated compounds such as ethylenically unsaturated monohydroxy alcohols, monohydroxy ethylenically unsaturated esters, monoamino ethylenically unsaturated esters, monohydroxy ethylenically unsaturated ureas, ethylenically unsaturated monoamines, ethylenically unsaturated hydroxyl amines and polyalkoxylated vinyl alcohols. Monohydroxy compounds are reacted under conditions which favour their reactivity with one isocyanate of each molecule of the polyisocyanate aromatic compound. It is well understood however that some of the polyisocyanate molecules go completely unreacted while others react to form polyurethane.

Preparation D—Polyvinyl isocyanurate resin

50 Into a chemical reactor equipped with agitator, condenser, gas pipe connections, vents, and port holes (which is first flushed with nitrogen and thereafter sparged with 0.944 l/s air and 2.832 l/s nitrogen) is added 2,680 parts of hydroxypropyl methacrylate and agitated at 30 revolutions per minute. Thereafter, 2.5 parts copper acetate catalyst, 12 parts of a 20% solution of t-butyl catechol and 5,743 parts styrene is charged to the reactor. The contents of the reactor are adjusted to 42° ± 2°C and thereafter sparged with 1.416—1.888 l/s nitrogen. Under increased agitation, 50—60 revolutions per minute, 3,063 parts of toluene diisocyanate is added at a rate of 60—70 parts per minute in four 766 part portions. After the first 766 part portion is added, the temperature is permitted to rise to 65°C. After the second portion, the temperature is permitted to rise to 90°C and after the fourth portion, the temperature is permitted to go higher than 93°C. The reaction mix is stirred for one additional hour at 90°C at which time the unreacted isocyanate content should be less than 4.5%. The reaction mix is cooled to 55°C and then mixed with 18 parts N-benzyl trimethyl ammonium hydroxide as a 40% methanol solution.

The exothermic trimerization reaction takes place with additional cooling such that the reaction mixture is not be permitted to go above 60°C. The reaction is continued until the unreacted isocyanate content in ranges between 0.05—0.15% and the viscosity ranges between 425—275 MPa . s. At this

point, 6 parts of methanesulphonic acid is added to inhibit the activity of the trimerization catalyst. The styrene/polyisocyanurate resin solution is stored for later use under conditions which inhibits further polymerization.

The reaction product has a number average molecular weight of about 1160, a weight average
 5 molecular weight of about 2000, and a polydispersity of about 1.9. About 95% of the isocyanurates present have a molecular weight of below about 5200, the remaining isocyanurates having a molecular weight from 5200 to 26,000. This product corresponds to a resin where the number of isocyanurate rings in most of the isocyanurate molecules is less than 10. This product has a ball and ring melting point of about 95°C and a viscosity (in 50% styrene solution) of about 400—600 mPa . s at 25°C, and
 10 a refractive index of about 1.557 ND²⁰. The infra-red spectrum of this product shows absorption bands characteristic of isocyanurates and the essential absence of isocyanate functionality. The hydroxyl number of the product is essentially zero.

Preparation E—Polyvinyl isocyanurate resin

15 This example illustrates the preparation of an allophanate-free resin from a resin containing a large amount of allophanate.

A small reaction vessel is charged with 100 g of a resin prepared according to Preparation D, which by NMR analysis had an allophanate to urethane ratio of 0.45. 0.4 ml of Triton B (40% solution of benzyltrimethylammonium hydroxide in methanol) is added and 0.5 ml of a 10% solution of equal
 20 amounts of t-butylcatechol and the monomethyl ether of hydroquinone. The resulting mixture is heated for 1-1/2 hours at 95°C. The final product is free of all detectable allophanate linkages upon NMR analysis.

Tractable shaped articles capable of being further shaped having from 5—95% by weight ethylenically unsaturated polyisocyanurate resin having 1—3 vinylidene groups per isocyanurate ring or its equivalent in a solution with at least one ethylenically unsaturated monomer which will react with ethylenically unsaturated groups in the isocyanurate resin can be made by thickening a homogeneous
 25 mixture of the polyisocyanurate resin/ethylenically unsaturated monomer solution with polyurethane made in solution therewith by reacting an aromatic polyisocyanate having 2—5 isocyanate groups per mol with a polyol having a molecular weight of about 300—2,000 and wherein the mol ratio of the
 30 total hydroxyl groups to isocyanate groups in the reaction mix is held between 0.66 and 0.95.

Ethylenically unsaturated monomers

Ethylenically unsaturated monomers in addition to styrene may be selected from vinyltoluene, divinylbenzene, acrylic acid esters, methacrylic acid esters, such as methylacrylate, ethylacrylate, n-
 35 butylacrylate, 2-ethylhexyl acrylate, methyl methacrylate, pentaerythritol triacrylate, ethylene glycol dimethacrylate, diallylphthalate, diallylmalate, diallylfumarate, triallylcyanurate, vinylacetate, vinylpropionate, divinylether, acrylonitrile and butadiene. In general, by ethylenically unsaturated monomer is meant a monomer containing at least one ethylenically unsaturated group which will react with the ethylenically unsaturated group in a polyester or itself. The proportion of monomer or
 40 monomers in the solution is in the range of 30—70% and preferably in the range of 40—60% by weight.

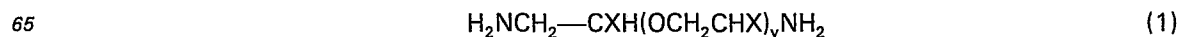
Polyamine polyurea precursors

Aliphatic, cycloaliphatic and aromatic polyamines free of ethylenic unsaturation are preferred
 45 polyurea precursors in that they form individual polyurea chains which are free from cross-linking with the a polymer chain formed by the copolymerization of the ethylenically unsaturated resin and monomers in solution therewith.

Aryl diamines and mixtures thereof such as metaphenylene diamine, parafenylene diamine, naphthalene diamine, benzidine, bis(4-amino-phenyl)methane, 4,4'-diaminodibenzyl, di(para-aminophenyl)ether, 3,3'-diaminodiphenyl sulfone, 4,4'-diaminodiphenyl sulfone and halogenated
 50 derivatives such as those containing halogen on the benzenoid ring such as 3,3'-dichlorobenzidine, bis,4-amino-2-chlorophenyl(propene), bis,4-amino-2-chlorophenyl (sulfone), 4-bromo-1,3-phenylene diamine, to name a few, are operable.

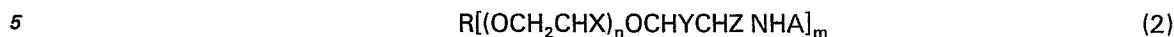
Low molecular weight aliphatic and cycloaliphatic diamines are also suitably employed, such as:
 55 ethylene diamine, propylene diamine, hexamethylene diamine, trimethyl hexamethylene diamine, isophorone diamine, 1-amino-3-amino-3,5,5-trimethyl cyclohexane, hydrogenated di-(aminophenyl)methane, hydrogenated methylene dianiline, diamino menthane, and hydrogenated toluene diamine. The most useful of these are those that are liquids up to 75°C. For those which are solids under these conditions, vinylidene monomer solutions can be employed to form the
 60 homogeneous mix rapidly.

In addition to the amines cited above, preferred results are obtained by using polyoxyalkylene polyamines and cyanoalkylated polyoxyalkylene polyamines having a molecular weight of 190 to 2,000 with a preferred range of 190 to 1,000 which have the general formula:



O 028 470

where X is H or alkyl group having 1—18 carbon atoms and where y is a number from 2 to 16. Triamines prepared according to the procedure outlined in U.S. 3,666,788 may also be used. These materials have the general formula:



where R is the nucleus of an oxyalkylation-susceptible aliphatic polyhydric alcohol containing 2—12 carbon atoms and 2—8 hydroxyl groups, A is hydrogen or a cyano-lower-alkyl radical having one or two carbon atoms between the nitrogen and cyano radical provided at least one A is a cyano-lower-alkyl radical, Z is an alkyl group containing 1—18 carbon atoms, X and Y are hydrogen or Z, n has an average value of 0—50 and m is 2—8, R is saturated and consists of carbon and hydrogen. Where A is cyanomethyl or cyanoethyl it may be further substituted by lower alkyl groups.

Especially preferred are triamines, which have the formula



where z has an average of 1 to 11.

Of particular interest for the practice of the invention are cyanoethylated polyoxypropylene diamines having molecular weights in the range of 230—2,000; and polyoxypropylene triamine and cyanoethylated polyoxypropylene triamine having molecular weights ranging from 400—2,000.

In the practice of the invention a homogeneous mixture containing the unsaturated monomer and ethylenically unsaturated resin is prepared and thereafter mixed with the polyamine. In some instances heat must be applied to aid in dissolving the ingredients to form a homogeneous solution. If the solution is to be stored for any length of time it is advisable to add free radical scavenger inhibitors such as hydroquinone, toluhydroquinone and tert-butyl catechol.

Free-radical initiator catalyst such as a for example peroxide selected from benzoyl peroxide, tert-butyl per benzoate, 1,1-bis(t-butylperoxy)3,3,5-trimethyl-cyclohexane or 2,4-pentanedione peroxide can be added at this point before gelation to insure a homogeneous mixture. Such peroxide catalysts are normally used in combination with a cure accelerator such as cobalt naphthenate or amine such as a dimethylaniline.

In the performance of the moulding step it is preferred that the addition polymerization of the monomer or its copolymerization with the ethylenically unsaturated resin takes place after the gelation or thickening step caused by the formation of polyureas. Normally it is preferred that the addition polymerization takes place within the mold at temperatures of the mould and therefore the a catalyst should be selected such that it is heat activated at this point.

Polyisocyanate polyurea precursors

The polyisocyanates used in the formation of the polyurea thickener system may be bifunctional or trifunctional or of even higher functionality. Polyisocyanates may be aliphatic, cycloaliphatic or aromatic. If desired mixtures of two or more different polyisocyanates may be employed. Examples of polyisocyanates include 4,4'-diphenylmethane di-isocyanate, 2,4- and 2,6-toluene diisocyanate in mixtures thereof, isophorone diisocyanate, tetramethylene diisocyanate, pentamethylene diisocyanate, hexamethylene diisocyanate and 4,4'-dicyclohexylmethane diisocyanate. Particularly useful is polymethylene polyphenyl isocyanate which comprises a mixture having 2—6 isocyanate groups per molecule and which has a functionality averaging between 2.1 and 3 isocyanate groups per mol and most often 2.3—2.7 isocyanate groups per mol and is sometimes referred to in the art as crude MDI.

The thickening reaction is carried out by the intermixing of the polyisocyanate either neat or in solution with solvents with the polymer in monomer solution containing polyamine such that the mol ratio of —NH₂ groups on said polyamine to the —NCO groups on said polyisocyanate is in the range of 0.8—1.2 and preferably about 1. The amine-isocyanate reaction is very fast, quantitative and predictable with no substantial interaction with the resin solution taking place. Once all the amines and isocyanate groups have reacted to form the polyurea there is no further reaction. Consequently, the matured or handleable molding compound remains at the same viscosity indefinitely. Since the maturation reaction is independent of the resin there is no need for the presence of carboxyl or hydroxyl groups. However, polyurea can be used to thicken conventional polyester resins (those having carboxyl or hydroxyl groups) as well as the other ethylenically unsaturated resins having no active hydrogens. In cases where a very fast gelation is desired a low molecular polyamine is employed.

While the polyurethane thickening methods require a select polyol blend to obtain a desired consistency the polyurea systems are less critical in this respect and require no catalysts so that they may be prepared quickly to form homogeneous gels of greater uniformity. This feature offers a particular advantage when it is desired to maintain a uniform dispersion throughout the gel of particulate matter such as fillers, pigments and reinforcing agents. Therefore the physical properties of the fully cured shaped articles of the invention are particularly uniform throughout. Such physical properties include flexural and notched impact strength which are improved by the incorporation of fibrous reinforcing materials which are mixed with the resins prior to gelation. Fibrous material may

include for example glass fibres, acicular rutile, graphite fibres, asbestos fibres or fibres spun from organic polymers for example polyesters. These fibrous materials may be of any suitable form for example in the form of veils, cloth, mat, ribbon, tapes, continuous fibre or as chopped fibre, and may range in length from fibrils up to 1—5 cm.

5 The amount of filler or reinforcing materials to be incorporated depends upon the desired improvement in a particular property of the shaped article. In general from 5—80% of fibrous materials such as fibreglass may be incorporated. To gain a substantial improvement in strength properties usually 60—80% by weight of fibrous material produces the desired result for most applications. In addition to reinforcing material other fillers such as carbon black, clay, iron oxide, lithopone, mica,
10 siliceous materials, titanium dioxide and coloured pigments may be added at some convenient time either prior to or during the gelation step.

Suitable shaping methods include casting and compression moulding. For example a shaped article may be produced by charging the components of the mixture into a suitable mould in which they are first gel polymerized to form what is often referred to as a preform. The mixture may also be
15 compressed during the gel polymerization.

It has been found that the initially shaped gel preform of the invention may be further shaped when the components of the mixture are in a partially gelled stage by first forming a tractable shape of simple profile before the system becomes completely gelled or while the ethylenically unsaturated ingredients polymerizes as previously described; and causing or allowing the thus preshaped gel to
20 retain its shape while completing both polymerization reactions.

The preshaping process of the invention may be effected on any shaped, partially gelled polymerized article of simple profile which may have contain fibrous reinforcement. It also can be adapted to preshaping of a partially gelled polymerized article in the form of sheets or pellets. The preshaping may be carried out by causing a preform of simple profile to form in the contours of a mould
25 for example by mechanical or vacuum means or by combinations thereof. Shaped article of simple profile may be further shaped by pressing between the cooperating parts of a mould or by draping over a vacuum moulding device.

In many instances a preshaped or preformed article may be removed from the mould after the polyamine/diisocyanate reaction has taken place and before the addition polymerization has
30 substantially begun. If the gel polymerized article does not retain its shape the vinyl polymerization may be started while the article is in the preform mould to increase its rigidity and thereafter the article can be removed from the preform mould and inserted quickly into another mould thereby attaining a final shape while both polymerization reactions are going to completion. Furthermore the original liquid monomer solution may be thickened by the resultant effect of the formation of polyurea and the
35 addition reaction such that the thickening takes place as a result of formation of two independent and separate polymer chains.

It may be desirable to react the ethylenically unsaturated ester/monomer partially or almost completely before further shaping and moulding. On the other hand where the mixture comprises a large portion of the polyurea it may not be necessary to complete the reaction between the a monomer
40 and the ethylenically unsaturated resin before moulding. The composition should of course not be gel polymerized or thickened to the point of intractability as to prevent the further shaping. Reaction conditions must be established by experimental trial with catalysts, resin ingredients, fillers, mould release agents and coupling agents well known to the art to gain the desired result.

The invention can be a better understood by the illustrations in the following examples in which
45 all parts are expressed as parts by weight:

Example 1

80 Parts of a 50% solution in styrene of poly(1,3,5-tri-R substituted-triazine-2,4,6-trione) wherein the R group is the mono adduct of hydroxypropylmethacrylate with toluene-diisocyanate (80/20
50 mixture of 2,4- and 2,6-toluenediisocyanate) prepared as shown in Preparation D were mixed with 20 parts of a cyanoethylated polyoxypropylene diamine having a molecular weight of 2000 (available from Jefferson Chemical Company under the trademark Jeffamine CD-2000).

Example 2

90 Parts of a 50% styrene solution of vinylmaleate urethane polymer made according to
55 procedure outlined in Preparation B was intermixed with 10 parts of cyanoethylated polyoxypropylene diamine having a molecular weight of 2,000 as provided by Jefferson Chemical Company under the trademark Jeffamine CD-2000.

Example 3

90 Parts by weight of a 60% solution of isophthalic polyester resin made according to Preparation
60 A in styrene was admixed with 10 parts by weight of Jeffamine CD-2000.

Example 4

95 Parts of a 50% solution of polyisocyanurate resin described in Preparation E and 5 parts of
65 Jeffamine CD-400 were intermixed to form a homogeneous solution.

0 028 470

Example 5

92.5 Parts of a 50% solution of polyisocyanurate resin prepared according to Preparation E was admixed with 7.5 parts of Jeffamine CD-400, 0.35 parts of toluhydroquinone, and 1 part 1,1-bis(tert-butylperoxy)-3,3,5-methylcyclohexane.

5

Example 6

93.5 Parts of a 50% styrene solution containing polyvinylisocyanurate of Preparation D and 6.5 parts of polyoxypropylene diamine was admixed with 0.35 parts toluhydroquinone, 1 part peroxide catalyst and 3 parts zinc stearate.

10

Example 7

91 Parts of 50% solution of polyisocyanurate resin Preparation D and 9 parts Jeffamine CD-400 was admixed with 0.35 parts toluhydroquinone, 1 part peroxide catalyst and 3 parts zinc stearate.

15 Example 8

86 Parts of 50% solution in styrene of polyisocyanurate resin of Preparation D and 9.25 parts of Jeffamine CD-400 was admixed with 0.35 parts toluhydroquinone and one part peroxide catalyst and 3 parts zinc stearate.

20 Example 9

82 Parts of Preparation D, 16 parts of Jeffamine CD-2000 a cyanoethylated polyoxy propylene diamine having a molecular weight of 2,000, 0.2 parts of a 10% solution of tert-butylcatechol, 1.5 parts of tert-butylperbenzoate, 0.5 parts 2,4 pentanedione peroxide, 0.5 parts cobalt naphthenate and a 0.4 parts dimethylaniline were mixed together and stored.

25

Example 10

85 Parts of a 50% styrene solution of vinylmaleate urethane resin prepared according to Preparation B 15 parts Jeffamine CD-2000 and one part peroxide catalyst were mixed and stored.

30 Example 11

266 Parts of the 50% styrene solution of Preparation D and 52 parts of Jeffamine CD-2000 were admixed with 0.65 parts of a 10% solution of tert-butylcatechol, 4.88 parts t-butylperbenzoate, 1.63 parts of 2,4 pentanedione peroxide, 1.63 parts cobalt naphthenate and 1.3 parts dimethylaniline.

35 Example 12

270 Parts 50% styrene solution of Preparation D, 30 parts Jeffamine CD-230 cyanoethylated polyoxypropylene diamine having a molecular weight of 230 were admixed with 1.5 parts cobalt naphthenate, 4.5 parts tert-butylperbenzoate, 1.5 parts 2,4 pentanedione peroxide and 1.2 parts dimethylaniline.

40

The resin solutions of Examples 1—12 are stable and can be stored under normal conditions for long periods of time without polymerization.

Examples 13—24

45 Gel times (minutes required to reach three dimensional integrity capable of holding itself together) and viscosity measurements (using a Brookfield Type LVC Viscosimeter, 30 RPM, No. 4 spindle) for the amine styrene resin solutions of Examples 1—10 are measured after the addition thereto of varying amounts of polyisocyanates such as polymethylene polyphenyl isocyanate having a functionality of 2.7 and available as MDI under the trademark Rubinate M from Rubicon Chemical Corp.; a similar polyisocyanate having a functionality averaging 2.3, and toluene diisocyanate referred to as TDI (80/20
50 mixture of 2,4- and 2,6-toluene diisocyanate). Proportions and results of these measurements are tabulated in Table I.

55

60

65

0 028 470

TABLE I
Gel times for polyurea thickened resins

Example No.	Amine solution of Ex. No. (100 parts)	Polyisocyanate	Parts by weight	Gel time (minutes)	
5	13	Ex. 1	Rubinate M	2.57	1
	14	Ex. 2	"	1.30	5
10	15	Ex. 3	"	1.30	1
	16	Ex. 4	"	2.55	Stable at 3,000 mPa
15	17	Ex. 5	"	3.82	Stable at 14,400 mPa
	18	Ex. 6	"	4.33	1
20	19	Ex. 7	"	4.82	30*
	20	Ex. 8	"	4.95	50*
	21	Ex. 9	"	2.10	20*
25	22	Ex. 10	TDI	1.28	—
	23	Ex. 11	Rubinate M	3.42	—
30	24	Ex. 12	MDI 2.3 functionality	7.93	—

* (minutes to 100,000 mPa . s).

Example 25

35 300 Parts of a composition made according to Example 11 was reacted with 6.83 parts of Rubinate M. The solution was then deaired and poured into a glass mould and allowed to gel at ambient temperature. The next day the casting or preform was post cured at 100°C for four hours. Mechanical properties for this casting are listed in Table II.

40 Example 26

300 Parts of a composition made according to Example 12 were reacted with 23.88 parts of MDI of functionality 2.3, then deaired and placed in a mould. The mixture gelled and was permitted to sit for one day at room temperature and thereafter post cured at 100°C four hours. Mechanical properties of this material are listed in Table II.

45 In order to demonstrate the fact that substantially no loss in strength occurs in compositions using a polyurea thickening a component, 300 parts of a vinyl isocyanurate resin preparation containing 1.5 parts cobalt naphthenate, 4.5 parts t-butylperbenzoate, 1.5 parts 2,4-pentanedione peroxide solution with 1.2 parts dimethylaniline were mixed and placed in a mould and fully cured as described in Example 26. The mechanical properties obtained for this material indicated that no substantial loss in strength resulted for the same polyvinyl isocyanurate cured in the presence of a polyurea thickener system of the invention. The mechanical properties for these resins are shown in Table II for purpose of comparison.

55

60

65

0 028 470

TABLE II
Mechanical properties

	Ex. 25	Ex. 26	Comparative Example
5 Flexural modulus, MPa (psi × 10 ⁶)	50332 (0.73)	36542 (0.53)	37232 (0.54)
Flexural yield, MPa (psi)	1070 (15520)	No yield	No yield
10 Flexural strength, MPa (psi)	1145 (16600)	887 (12820)	1227 (17800)
Tensile modulus, MPa (psi × 10 ⁶)	26200 (0.38)	37232 (0.54)	37232 (0.54)
Tensile strength, MPa (psi)	593 (8600)	545 (7900)	621 (9000)
15 Tensile elongation, %	4.95	1.67	1.89
Barcol hardness	24—26	36—41	42—44
20 Charpy impact, unnotched, J/M (ft lb/in)	442 (8.07)	185 (3.37)	187 (3.42)
Heat distortion temperature (°C)	102	118	133

Claims

25 1. A resin blend useful in preparing non-sticky moulding compositions by the reaction therewith of polyisocyanate which comprises:

30 an ethylenically unsaturated monomer, containing dissolved therein 30—70% by weight of a resin selected from vinyl terminated polyester urethane resins, ethylenically unsaturated polyester resins, and ethylenically unsaturated polyisocyanurate resins and 1.5—30% by weight of at least one organic polyamine polyurea precursor free of ethylenic unsaturation, all percentage weights being based on the total weight of the resin blend.

35 2. A composition of claim 1 wherein said ethylenically unsaturated polyester resin is a condensation product of a polyalkoxylated bisphenol A compound, an unsaturated dicarboxylic acid and an aromatic dicarboxylic acid.

3. A composition of claim 1 or claim 2 wherein said vinylester urethane resin is a product of the following general formula:

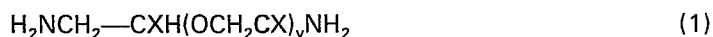


45 wherein d is a radical derived from an organic polyol, n is a radical derived from an unsaturated aliphatic dicarboxylic acid or an anhydride thereof; i is a radical derived from a polyisocyanate; c is a carbamyl-linked radical derived from a hydroxy-terminated ester of acrylic or methacrylic acid; t is an integer equal to from 1 to 5, which is substantially free from unreacted isocyanate groups.

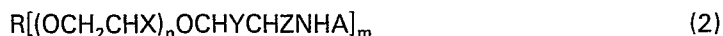
4. A composition of any one of claims 1 to 3 wherein said vinylester urethane resin is a condensation product of polyoxyalkylene bisphenol A having 2—60 mols of ethylene oxide or propylene oxide per mol, n is derived from maleic anhydride or maleic acid, i is a radical derived from 50 toluene diisocyanate or a polyisocyanate having 2.4—3 isocyanate groups per mol.

5. A composition of any one of claims 1 to 4 wherein said polyamine polyurea precursor is selected from aliphatic and cycloaliphatic and aromatic polyamines which are liquids up to 75°C.

6. A composition of any one of claims 1 to 5 wherein said polyamines are selected from polyoxyalkylene polyamines and cyanoalkylated polyoxyalkylene polyamines having a molecular weight 55 of about 190—2,000 of the general formula:



60 wherein X is H or an alkyl group having 1—18 carbons atoms and where y is a number of about 2 to about 16; or



65 where R is the nucleus of an oxyalkylation-susceptible aliphatic polyhydric alcohol containing 2—12 carbon atoms and 2—8 hydroxyl groups, A is hydrogen or a cyano lower alkyl radical having 1 or 2

carbon atoms between the nitrogen and the cyano radical provided at least one A is a cyano-lower-alkyl-radical, Z is an alkyl group containing 1—18 carbon atoms, X and Y are hydrogen or Z, n has an average value of 0—50 and m is 2—8, R is saturated and consists of carbon and hydrogen.

7. A composition of any of claims 1 to 6 further comprising a free-radical initiator catalyst.

8. A composition of any of claims 1 to 7 further comprising an amount of polyisocyanate wherein the mol ratio of the —NH₂ groups on said polyamine to —NCO groups on said polyisocyanate ranges from 0.8—1.2.

9. A handleable tractable composition made by permitting a composition of any one of claims 1 to 8 to thicken to a non-sticky molding by the formation of polyureas.

10. A fully cured intractable composition made by the process of shaping a composition of claim 9 and thereafter copolymerizing said ethylenically unsaturated ingredients in said material by free-radical activation.

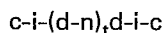
Patentansprüche

1. Harzmischung, die für die Herstellung von nichtklebenden Formmassen durch Umsetzung von Polyisocyanat mit der Harzmischung verwendbar ist, wobei die Harzmischung

ein ethylenisch ungesättigtes Monomer enthält, das darin gelöst 30 bis 70 Gew.-% eines aus Polyester-urethanharzen mit Vinylgruppen als Endgruppen, ethylenisch ungesättigten Polyesterharzen und ethylenisch ungesättigten Polyisocyanuratharzen ausgewählten Harzes und 1,5 bis 30 Gew.-% mindestens eines von ethylenischen Doppelbindungen freien organischen Polyamins als Vorstufe eines Polyharnstoffs enthält, wobei alle Gewichtsprozentwerte auf das Gesamtgewicht der Harzmischung bezogen sind.

2. Masse nach Anspruch 1, bei der das ethylenisch ungesättigte Polyesterharz ein Kondensationsprodukt einer polyalkoxylierten Bisphenol A-Verbindung, einer ungesättigten Dicarbonsäure und einer aromatischen Dicarbonsäure ist.

3. Masse nach Anspruch 1 oder 2, bei der das Vinylesterurethanharz ein Produkt der folgenden allgemeinen Formel ist:

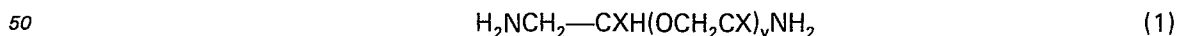


worin d ein von einem organischen Polyol abgeleiteter Rest ist, n ein von einer ungesättigten aliphatischen Dicarbonsäure oder einem Anhydrid davon abgeleiteter Rest ist, i ein von einem Polyisocyanat abgeleiteter Rest ist, c ein von einem Acrylsäure- oder Methacrylsäureester mit einer Hydroxylgruppe als Endgruppe abgeleiteter, an eine Carbamoylgruppierung gebundener Rest ist und t eine ganze Zahl von 1 bis 5 ist, das im wesentlichen frei von unumgesetzten Isocyanatgruppen ist.

4. Masse nach einem der Ansprüche 1 bis 3, bei der das Vinylesterurethanharz ein Kondensationsprodukt von Polyoxyalkylen-Bisphenol A mit 2 bis 60 mol Ethylenoxid oder Propylenoxid pro Mol ist, n von Maleinsäureanhydrid oder Maleinsäure abgeleitet ist und i ein von Toluylendiisocyanat oder einem Polyisocyanat mit 2,4 bis 3 Isocyanatgruppen pro Mol abgeleiteter Rest ist.

5. Masse nach einem der Ansprüche 1 bis 4, bei der die Polyaminvorstufe des Polyharnstoffs aus aliphatischen und cycloaliphatischen und aromatischen Polyaminen, die bis 75°C Flüssigkeiten sind, ausgewählt ist.

6. Masse nach einem der Ansprüche 1 bis 5, bei der die Polyamine aus Polyoxyalkylenpolyaminen und cyanalkylierten Polyoxyalkylenpolyaminen mit einem Molekulargewicht von etwa 190 bis 2000 der allgemeinen Formel:



worin X H oder ein Alkylrest mit 1 bis 18 Kohlenstoffatomen und y eine Zahl von etwa 2 bis etwa 16 ist, oder



worin R das gesättigte, aus Kohlenstoff und Wasserstoff bestehende Grundgerüst eines mehrwertigen aliphatischen Alkohols ist, der 2 bis 12 Kohlenstoffatome und 2 bis 8 Hydroxylgruppen enthält und einer Oxyalkylierung zugänglich ist, A Wasserstoff oder ein niederer Cyanalkylrest mit 1 oder 2 Kohlenstoffatomen zwischen dem Stickstoff und der Cyangruppe ist, wobei vorausgesetzt ist, daß mindestens ein A ein niederer Cyanalkylrest ist, Z ein 1 bis 18 Kohlenstoffatome enthaltender Alkylrest ist, X und Y Wasserstoff oder Z bedeuten, n einen Mittelwert von 0 bis 50 hat und m 2 bis 8 ist, ausgewählt sind.

7. Masse nach einem der Ansprüche 1 bis 6, die ferner einen freie Radikale bildenden Initiator-Katalysator enthält.

0 028 470

8. Masse nach einem der Ansprüche 1 bis 7, die ferner eine Polyisocyanatmenge enthält, wobei das Molverhältnis der Gruppen —NH_2 an dem Polyamin zu den Gruppen —NCO an dem Polyisocyanat in dem Bereich von 0,8:1 bis 1,2:1 liegt.

9. Verarbeitbare bzw. handhabbare, leicht formbare Masse, die hergestellt wird, indem man eine Masse nach einem der Ansprüche 1 bis 8 durch Bildung von Polyharnstoffen dick werden läßt, so daß ein nicht klebender Formling erhalten wird.

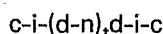
10. Durchgehärtete, schwer bzw. nicht formbare Masse, die durch ein Verfahren hergestellt wird, bei dem eine Masse nach Anspruch 9 geformt wird und bei dem danach die ethylenisch ungesättigten Bestandteile in dem Material durch Aktivierung mittels freier Radikale copolymerisiert werden.

Revendications

1. Mélange de résine utile pour la préparation de compositions à mouler non poisseuses par réaction de celui-ci avec un polyisocyanate, qui comprend un monomère éthyléniquement insaturé contenant, à l'état dissous, 30 à 70% en poids d'une résine choisie parmi les résines de polyester-uréthannes à radicaux vinyliques terminaux, les résines de polyesters éthyléniquement insaturés et les résines de polyisocyanurates éthyléniquement insaturés et 1,5—30% en poids d'au moins une polyamine organique précurseur de polyurée exempte d'insaturation éthylénique, tous les pourcentages pondéraux étant rapportés au poids total du mélange de résine.

2. Composition suivant la revendication 1, dans laquelle la résine de polyester éthyléniquement insaturé est un produit de condensation d'un bisphénol A polyalcoylé, d'un acide dicarboxylique insaturé et d'un acide dicarboxylique aromatique.

3. Composition suivant la revendication 1 ou 2, dans laquelle la résine d'ester-uréthane vinylique est un produit de la formule générale suivante:

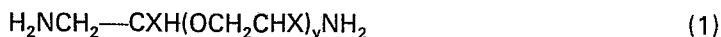


où d représente un radical issu d'un polyol organique, n représente un radical issu d'un acide dicarboxylique aliphatique insaturé ou d'un anhydride de celui-ci; i représente un radical issu d'un polyisocyanate; c représente un radical à liaison carbamyle issu d'un ester d'acide acrylique ou méthacrylique à radical hydroxyle terminal; t représente un nombre entier de 1 à environ 5, qui est sensiblement exempt de radicaux isocyanate qui n'ont pas réagi.

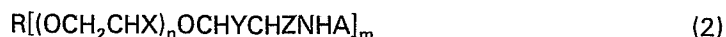
4. Composition suivant l'une quelconque des revendications 1 à 3, dans laquelle la résine d'esteruréthane vinylique est un produit de condensation de polyoxyalcoylène bisphénol A comprenant 2 à 60 moles d'oxyde d'éthylène ou d'oxyde de propylène par mole, n est issu de l'anhydride maléique ou de l'acide maléique, i représente un radical issu du diisocyanatotoluène ou d'un polyisocyanate contenant 2,4—3 radicaux isocyanate par mole.

5. Composition suivant l'une quelconque des revendications 1 à 4, dans laquelle la polyamine précurseur de polyurée est choisie entre les polyamines aliphatiques, cycloaliphatiques et aromatiques qui sont liquides jusqu'à 75°C.

6. Composition suivant l'une quelconque des revendications 1 à 5, dans laquelle les polyamines sont choisies parmi les polyoxyalcoylène-polyamines et les polyoxyalcoylène-polyamines cyanoalcoylées d'un poids moléculaire d'environ 190—2000 de la formule générale:



où X représente H ou un radical alcoyle de 1 à 18 atomes de carbone et y représente un nombre d'environ 2 à environ 16, ou



où R représente le noyau d'un alcool polyhydroxylé aliphatique susceptible d'oxyalcoylation comprenant 2 à 12 atomes de carbone et 2 à 8 radicaux hydroxyle, A représente un atome d'hydrogène ou un radical cyano(alcoyle inférieur) comprenant un ou deux atomes de carbone entre l'azote et le radical cyano, étant entendu qu'au moins un radical A est un radical cyano(alcoyle inférieur), Z représente un radical alcoyle comptant 1 à 18 atomes de carbone, X et Y représentent des atomes d'hydrogène ou Z, n a une valeur moyenne de 0 à 50, m vaut 2 à 8, R est saturé et consiste en carbone et en hydrogène.

7. Composition suivant l'une quelconque des revendications 1 à 6, qui comprend en outre un catalyseur initiateur de radicaux libres.

8. Composition suivant l'une quelconque des revendications 1 à 7, qui comprend en outre une certaine quantité de polyisocyanate, où le rapport molaire des radicaux —NH_2 de la polyamine aux radicaux —NCO du polyisocyanate est situé dans l'intervalle de 0,8—1,2.

9. Composition manipulable traitable obtenue par épaissement d'une composition suivant l'une quelconque des revendications 1 à 8 en un produit à mouler non poisseux par formation de polyurées.

0 028 470

10. Composition non traitable complètement durcie obtenue par un procédé de façonnage d'une composition suivant la revendication 9 et ensuite copolymérisation des constituants éthyléniquement insaturés de la composition par activation radicalaire.

5

10

15

20

25

30

35

40

45

50

55

60

65