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DESCRIPTION

FIELD OF THE INVENTION

[0001] This invention relates to a trunk piston marine engine lubricating composition for a medium-speed four-stroke compression-ignited (diesel) marine engine and lubrication of such an engine.

BACKGROUND OF THE INVENTION

[0002] Marine trunk piston engines generally use Heavy Fuel Oil ('HFO') for offshore running. Heavy Fuel Oil is the heaviest fraction of petroleum distillate and comprises a complex mixture of molecules including up to 15% of asphaltenes, defined as the fraction of petroleum distillate that is insoluble in an excess of aliphatic hydrocarbon (e.g. heptane) but that is soluble in aromatic solvents (e.g. toluene). Asphaltenes can enter the engine lubricant as contaminants either via the cylinder or the fuel pumps and injectors, and asphaltene precipitation can then occur, manifested in 'black paint' or 'black sludge' in the engine. The presence of such carbonaceous deposits on a piston surface can act as an insulating layer that can result in the formation of cracks that then propagate through the piston. If a crack travels through the piston, hot combustion gases can enter the crankcase, possibly resulting in a crankcase explosion.

[0003] It is therefore highly desirable that trunk piston engine oils ('TPEO's) prevent or inhibit asphaltene precipitation. TPEO's using Group 1 basestocks may have the ability to solubilise asphaltenes. However, TPEO's using high saturate basestocks (e.g. Group II or III) require a booster to achieve similar performance levels in this respect.

[0004] WO 2010/115594 ("594") and WO 2010/115595 ("595") describe the use, in trunk piston marine engine lubricating oil compositions that contain 50 mass % or more of a Group II basestock, of respective minor amounts of a calcium salicylate detergent and of a polyalkenyl-substituted carboxylic and anhydride. The data in "594" and "595" show that the combination gives rise to improved asphaltene dispersancy.

[0005] US 2011/0319304 A1 ('304) describes the use of ester basestock in a high saturates basestock TPEO to improve asphaltene dispersancy.

[0006] A problem in the art is to improve still further the asphaltene dispersancy performance of TPEO's that employ high saturate basestocks.

SUMMARY OF THE INVENTION

[0007] The invention meets the above problem by employing an anhydride and an ester in a TPEO: a synergistic effect is observed as demonstrated in the data herein.

[0008] A first aspect of the invention is a trunk piston marine engine lubricating oil composition for improving asphaltene handling in use thereof in operation of the engine when fuelled by a heavy fuel oil, which composition comprises or is made by admixing

(A) 50 mass % or more of the composition of an oil of lubricating viscosity which is either:

- an oil-soluble ester basestock (A1); or
- comprises greater than 0.1 to less than 90 mass %, preferably greater than 1 to less than 80 mass%, of an oil-soluble ester basestock (A1) and, as 50 mass % or more of the remainder of the oil of lubricating viscosity, a basestock containing greater than or equal to 90% saturates and less than or equal to 0.03 % sulphur or a mixture thereof (A2);

(B) an oil-soluble overbased metal hydrocarbyl-substituted hydroxybenzoate detergent, in a minor amount; and

(B) an oil-soluble polyalkenyl-substituted carboxylic acid anhydride, in a minor amount of from greater than 0.1 to less than 10 mass % of the composition preferably greater than 1 to less than 8 mass%, the, or at least one, polyalkenyl group being derived from polyalkene having a number average molecular weight of from 200 to 3000.

[0009] A second aspect of the invention is a method of operating a trunk piston medium-speed compression-ignited marine engine comprising

1. (i) fuelling the engine with a heavy fuel oil; and
2. (ii) lubricating the crankcase of the engine with a composition according to the first aspect of the invention.

[0010] A third aspect of the invention is a method of dispersing asphaltenes in a trunk piston marine lubricating oil composition during its lubrication of surfaces of the combustion chamber of a medium-speed compression-ignited marine engine and operation of the engine, which method comprises:

1. (i) providing a composition according to the first aspect of the invention;
2. (ii) providing the composition in the combustion chamber;
3. (iii) providing heavy fuel oil in the combustion chamber; and
4. (iv) combusting the heavy fuel oil in the combustion chamber.

[0011] A fourth aspect of the invention is the use of detergent (B) in combination with component (C) as defined in and in the amounts stated in the first aspect of the invention in a trunk piston marine lubricating oil composition for a medium-speed compression-ignited marine engine, which composition comprises an oil of lubricating viscosity (A) in a major amount as defined in the first aspect of the invention, to provide comparable or improved asphaltene handling during operation of the engine, fuelled by a heavy fuel oil, and its lubrication by the composition, in comparison with that of a comparable oil where the basestock is a Group I basestock.

[0012] In this specification, the following words and expressions, if and when used, have the meanings ascribed below:

"active ingredients" or "(a.i.)" refers to additive material that is not diluent or solvent;

"comprising" or any cognate word specifies the presence of stated features, steps, or integers or components, but does not preclude the presence or addition of one or more other features, steps, integers, components or groups thereof; the expressions "consists of" or "consists essentially of" or cognates may be embraced within "comprises" or cognates, wherein "consists essentially of" permits inclusion of substances not materially affecting the characteristics of the composition to which it applies;

"major amount" means 50 mass % or more, preferably 60 mass % or more, more preferably 70 mass % or more, even more preferably 80 mass % or more, of a composition;

"minor amount" means less than 50 mass %, preferably less than 40 mass %, more preferably less than 30 mass %, and even more preferably less than 20 mass %, of a composition;

"TBN" means total base number as measured by ASTM D2896.

[0013] Furthermore in this specification, if and when used:

"calcium content" is as measured by ASTM 4951;

"phosphorus content" is as measured by ASTM D5185;

"sulphated ash content" is as measured by ASTM D874;

"sulphur content" is as measured by ASTM D2622;

"KV100" means kinematic viscosity at 100°C as measured by ASTM D445.

[0014] Also, it will be understood that various components used, essential as well as optimal and customary, may react under conditions of formulation, storage or use and that the invention also provides the product obtainable or obtained as a result of any such reaction.

[0015] Further, it is understood that any upper and lower quantity, range and ratio limits set forth herein may be independently combined.

DETAILED DESCRIPTION OF THE INVENTION

[0016] The features of the invention will now be discussed in more detail below.

OIL OF LUBRICATING VISCOSITY (A)

ESTER BASESTOCKS (A1)

[0017] These are organic ester basestocks that include but are not limited to monoesters, diesters and polyolesters, and also polymer esters. They are generally considered to be Group V basestocks and are typically derived from animal or vegetable sources. Naturally-occurring organic esters can be found in animal fats or in vegetable oils. Organic esters can be synthesised by reacting organic acids with alcohols.

[0018] Monoesters may be prepared by reacting monohydric alcohols with monobasic fatty acids to create a molecule with a single ester linkage and linear or branched alkyl groups.

[0019] Diesters may be prepared by reacting monohydric alcohols (e.g., butyl alcohol, hexyl alcohol, dodecyl alcohol, 2-ethylhexyl alcohol, ethylene glycol, diethylene glycol monoether, propylene glycol) with dibasic acids (e.g., phthalic acid, succinic acid, alkyl succinic acids and alkenyl succinic acids, maleic acid, azelaic acid, suberic acid, sebacic acid, fumaric acid, adipic acid, linoleic acid dimer, malonic acid, alkylmalonic acids, alkenyl malonic acids) to create a molecule which may be linear, branched or aromatic with two ester groups. Specific examples of such esters includes dibutyl adipate, di(2-ethylhexyl) sebacate, di-n-hexyl fumarate, dioctyl sebacate, diisooctyl azelate, diisodecyl azelate, dioctyl phthalate, didecyl phthalate, dieicosyl sebacate, the 2-ethylhexyl diester of linoleic acid dimer, and the complex ester formed by reacting one mole of sebacic acid with two moles of tetraethylene glycol and two moles of 2-ethylhexanoic acid.

[0020] Polyol esters may be prepared by esterifying one or more polyols such as neopentyl glycol, trimethylolpropane, pentaerythritol, dipentaerythritol and tripentaerythritol with one or more organic acids such as C₅ to C₁₂ monocarboxylic acids. See, for example, US-A-6,462,001. Examples of polyol esters include trimethylolpropane (TMP) esters.

[0021] Tricarboxylic acid esters are also preferred. The tricarboxylic acid ester is preferably a benzene tricarboxylic acid. A preferred benzene tricarboxylic acid ester is 1,2,4-benzenetricarboxylic acid having alkyl chain lengths ranging from 5 to 10, preferably from 7 to 9. A preferred 1,2,4-benzenetricarboxylic acid is trioctyl trimellitate.

[0022] Examples of ester basestocks for use in the present invention are those having a kinematic viscosity of 2 to 10 mm²s⁻¹ at 100°C or those having a kinematic viscosity of greater than 10 to 100 mm²s⁻¹ at 100°C. A specific example of suitable polyol ester is Priolube (Registered Trade Mark) 3970, which is an ester of a neopentyl polyol, suitably TMP, with at least one aliphatic, saturated monocarboxylic acid and having 6 to 12 carbon atoms and a kinematic viscosity of 4.4 mm²s⁻¹ at 100°C.

[0023] The ester basestock may be present in an amount in the range of 2 to 85, preferably 5 to 50, more preferably 8 to 40 mass %.

BASESTOCKS (A2)

[0024] These may range in viscosity from light distillate mineral oil to heavy lubricating oil. Generally, the viscosity of the oil ranges from 2 to 40 mm²s⁻¹, as measured at 100°C.

[0025] Natural oils include animal oils and vegetable oils (e.g., castor oil, lard oil); liquid petroleum oils and hydrorefined, solvent-

treated or acid-treated mineral oils of the paraffinic, naphthenic and mixed paraffinic-naphthenic types. Oils of lubricating viscosity derived from coal or shale also serve as useful base oils.

[0026] Synthetic lubricating oils include hydrocarbon oils and halo-substituted hydrocarbon oils such as polymerized and interpolymers of olefins (e.g., polybutylenes, polypropylenes, propylene-isobutylene copolymers, chlorinated polybutylenes, poly(1-hexenes), poly(1-octenes), poly(1-decenes)); alkybenzenes (e.g., dodecylbenzenes, tetradecylbenzenes, dinonylbenzenes, di(2-ethylhexyl)benzenes); polyphenyls (e.g., biphenyls, terphenyls, alkylated polyphenols); and alkylated diphenyl ethers and alkylated diphenyl sulphides and derivative, analogues and homologues thereof.

[0027] Unrefined, refined and re-refined oils can be used in lubricants of the present invention. Unrefined oils are those obtained directly from a natural or synthetic source without further purification treatment. For example, a shale oil obtained directly from retorting operations; and petroleum oil obtained directly from distillation are unrefined oils. Refined oils are similar to unrefined oils except that the oil is further treated in one or more purification steps to improve one or more properties. Many such purification techniques, such as distillation, solvent extraction, acid or base extraction, filtration and percolation, are known to those skilled in the art. Re-refined oils are obtained by processes similar to those used to provide refined oils but begin with oil that has already been used in service. Such re-refined oils are also known as reclaimed or reprocessed oils and are often subjected to additional processing using techniques for removing spent additives and oil breakdown products.

[0028] The American Petroleum Institute (API) publication "Engine Oil Licensing and Certification System", Industry Services Department, Fourteenth Edition, December 1996, Addendum 1, December 1998 categorizes base stocks as follows:

Group I base stocks contain less than 90 percent saturates and/or greater than 0.03 percent sulphur and have a viscosity index greater than or equal to 80 and less than 120 using the test methods specified in Table E-1.

Group II base stocks contain greater than or equal to 90 percent saturates and less than or equal to 0.03 percent sulphur and have a viscosity index greater than or equal to 80 and less than 120 using the test methods specified in Table E-1.

Group III base stocks contain greater than or equal to 90 percent saturates and less than or equal to 0.03 percent sulphur and have a viscosity index greater than or equal to 120 using the test methods specified in Table E-1.

Group IV base stocks are polyalphaolefins (PAO).

Group V base stocks include all other base stocks not included in Group I, II, III, or IV.

[0029] Analytical Methods for Base Stock are tabulated below:

(TABLE E-1)

PROPERTY	TEST METHOD
Saturates	ASTM D 2007
Viscosity Index	ASTM D 2270
Sulphur	ASTM D 2622
	ASTM D 4294
	ASTM D 4927
	ASTM D 3120

[0030] By way of example, the basestocks (A2) embraces Group II, Group III and Group IV basestocks and also basestocks derived from hydrocarbons synthesised by the Fischer-Tropsch process. In the Fischer-Tropsch process, synthesis gas containing carbon monoxide and hydrogen (or 'syngas') is first generated and then converted to hydrocarbons using a Fischer-Tropsch catalyst. These hydrocarbons typically require further processing in order to be useful as a base oil. For example, they may, by methods known in the art, be hydroisomerized; hydrocracked and hydroisomerized; dewaxed; or hydroisomerized and dewaxed. The syngas may, for example, be made from gas such as natural gas or other gaseous hydrocarbons by steam reforming, when the basestock may be referred to as gas-to-liquid ("GTL") base oil; or from gasification of biomass, when the basestock may be referred to as biomass-to-liquid ("BTL" or "BMTL") base oil; or from gasification of coal, when the basestock may be referred to as coal-to-liquid ("CTL") base oil.

[0031] As stated, the basestock (A2), when used in this invention, contains 50 mass % or more of the defined basestock or a

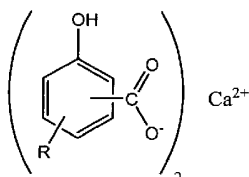
mixture thereof. Preferably, it contains 60, such as 70, 80 or 90, mass % or more of the defined basestock or a mixture thereof. (A2) may comprise substantially all the defined basestock or a mixture thereof.

OVERBASED METAL DETERGENT (B)

[0032] A metal detergent is an additive based on so-called metal "soaps", that is metal salts of acidic organic compounds, sometimes referred to as surfactants. They generally comprise a polar head with a long hydrophobic tail. Overbased metal detergents, which comprise neutralized metal detergents as the outer layer of a metal base (e.g. carbonate) micelle, may be provided by including large amounts of metal base by reacting an excess of a metal base, such as an oxide or hydroxide, with an acidic gas such as carbon dioxide. Examples of detergents include metal salicylates, phenates and salicylates and combinations thereof.

[0033] In the present invention, the overbased metal hydrocarbyl-substituted hydroxybenzoate is preferably a hydrocarbyl-substituted salicylate detergent. The metal may be an alkali metal (e.g. Li, Na, K) or an alkaline earth metal (e.g. Mg, Ca).

[0034] "Hydrocarbyl" means a group or radical that contains carbon and hydrogen atoms and that is bonded to the remainder of the molecule via a carbon atom. It may contain hetero atoms, i.e. atoms other than carbon and hydrogen, provided they do not alter the essentially hydrocarbon nature and characteristics of the group. As examples of hydrocarbyl, there may be mentioned alkyl and alkenyl. A preferred overbased metal hydrocarbyl-substituted hydroxybenzoate is a calcium alkyl-substituted salicylate and has the structure shown:



wherein R is a linear alkyl group. There may be more than one R group attached to the benzene ring. The COO⁻ group can be in the ortho, meta or para position with respect to the hydroxyl group; the ortho position is preferred. The R group can be in the ortho, meta or para position with respect to the hydroxyl group.

[0035] Salicylic acids are typically prepared by the carboxylation, by the Kolbe-Schmitt process, of phenoxides, and in that case will generally be obtained (normally in a diluent) in admixture with uncarboxylated phenol. Salicylic acids may be non-sulphurized or sulphurized, and may be chemically modified and/or contain additional substituents. Processes for sulphurizing an alkyl salicylic acid are well known to those skilled in the art, and are described in, for example, US 2007/0027057.

[0036] The alkyl groups advantageously contain 5 to 100, preferably 9 to 30, especially 14 to 24, carbon atoms.

[0037] The term "overbased" is generally used to describe metal detergents in which the ratio of the number of equivalents of the metal moiety to the number of equivalents of the acid moiety is greater than one. The term 'low-based' is used to describe metal detergents in which the equivalent ratio of metal moiety to acid moiety is greater than 1, and up to about 2.

[0038] By an "overbased calcium salt of surfactants" is meant an overbased detergent in which the metal cations of the oil-insoluble metal salt are essentially calcium cations. Small amounts of other cations may be present in the oil-insoluble metal salt, but typically at least 80, more typically at least 90, for example at least 95, mole % of the cations in the oil-insoluble metal salt, are calcium ions. Cations other than calcium may be derived, for example, from the use in the manufacture of the overbased detergent of a surfactant salt in which the cation is a metal other than calcium. Preferably, the metal salt of the surfactant is also calcium.

[0039] Carbonated overbased metal detergents typically comprise amorphous nanoparticles. Additionally, the art discloses nanoparticulate materials comprising carbonate in the crystalline calcite and vaterite forms.

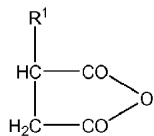
[0040] The basicity of the detergents may be expressed as a total base number (TBN), sometimes referred to as base number (BN). A total base number is the amount of acid needed to neutralize all of the basicity of the overbased material. The TBN may be measured using ASTM standard D2896 or an equivalent procedure. The detergent may have a low TBN (i.e. a TBN of less than 50), a medium TBN (i.e. a TBN of 50 to 150) or a high TBN (i.e. a TBN of greater than 150, such as 150-500). The basicity may also be expressed as basicity index (BI), which is the molar ratio of total base to total soap in the overbased detergent.

POLYALKENYL-SUBSTITUTED CARBOXYLIC ACID ANHYDRIDE (C)

[0041] The anhydride may constitute at least 1 to 7, preferably 2 to 6 mass % of the lubricating oil composition. Preferably it constitutes 3 to 5, even more preferably 4 to 5, mass %.

[0042] The anhydride may be mono or polycarboxylic, preferably dicarboxylic. The polyalkenyl group preferably has from 8 to 400, such as 8 to 100, carbon atoms.

[0043] General formulae of exemplary anhydrides may be depicted as



where R^1 represents a C_8 to C_{100} branched or linear polyalkenyl group.

[0044] The polyalkenyl moiety may have a number average molecular weight of from 200 to 3000, preferably from 350 to 950.

[0045] Suitable hydrocarbons or polymers employed in the formation of the anhydrides used in the present invention to generate the polyalkenyl moieties include homopolymers, interpolymers or lower molecular weight hydrocarbons. One family of such polymers comprise polymers of ethylene and/or at least one C_3 to C_{28} alpha-olefin having the formula $H_2C=CHR^1$ wherein R^1 is straight or branched-chain alkyl radical comprising 1 to 26 carbon atoms and wherein the polymer contains carbon-to-carbon unsaturation, preferably a high degree of terminal ethenylidene unsaturation. Preferably, such polymers comprise interpolymers of ethylene and at least one alpha-olefin of the above formula, wherein R^1 is alkyl of from 1 to 18 carbon atoms, and more preferably is alkyl of from 1 to 8 carbon atoms, and more preferably still of from 1 to 2 carbon atoms. Therefore, useful alpha-olefin monomers and comonomers include, for example, propylene, butene-1, hexene-1, octene-1, 4-methylpentene-1, decene-1, dodecene-1, tridecene-1, tetradecene-1, pentadecene-1, hexadecene-1, heptadecene-1, octadecene-1, nonadecene-1, and mixtures thereof (e.g., mixtures of propylene and butene-1, and the like). Exemplary of such polymers are propylene homopolymers, butene-1 homopolymers, ethylene-propylene copolymers, ethylene-butene-1 copolymers, propylene-butene copolymers and the like, wherein the polymer contains at least some terminal and/or internal unsaturation. Preferred polymers are unsaturated copolymers of ethylene and propylene and ethylene and butene-1. The interpolymers may contain a minor amount, e.g. 0.5 to 5 mole %, of a C_4 to C_{18} nonconjugated diolefin comonomer. However, it is preferred that the polymers comprise only alpha-olefin homopolymers, interpolymers of alpha-olefin comonomers and interpolymers of ethylene and alpha-olefin comonomers. The molar ethylene content of the polymers employed is preferably in the range of 0 to 80 %, and more preferably 0 to 60 %. When propylene and/or butene-1 are employed as comonomer(s) with ethylene, the ethylene content of such copolymers is most preferably between 15 and 50 %, although higher or lower ethylene contents may be present.

[0046] These polymers may be prepared by polymerizing an alpha-olefin monomer, or mixtures of alpha-olefin monomers, or mixtures comprising ethylene and at least one C_3 to C_{28} alpha-olefin monomer, in the presence of a catalyst system comprising at least one metallocene (e.g., a cyclopentadienyl-transition metal compound) and an alumoxane compound. Using this process, a polymer in which 95 % or more of the polymer chains possess terminal ethenylidene-type unsaturation can be provided. The percentage of polymer chains exhibiting terminal ethenylidene unsaturation may be determined by FTIR spectroscopic analysis, titration, or C^{13} NMR. Interpolymers of this latter type may be characterized by the formula $POLY-C(R^1)=CH_2$ wherein R^1 is C_1 to C_{26} alkyl, preferably C_1 to C_{18} alkyl, more preferably C_1 to C_8 alkyl, and most preferably C_1 to C_2 alkyl, (e.g., methyl or ethyl) and wherein POLY represents the polymer chain. The chain length of the R^1 alkyl group will vary depending on the comonomer(s) selected for use in the polymerization. A minor amount of the polymer chains can contain terminal ethenyl, i.e., vinyl, unsaturation, i.e. $POLY-CH=CH_2$, and a portion of the polymers can contain internal monounsaturations, e.g. $POLY-CH=CH(R^1)$, wherein R^1 is as defined above. These terminally unsaturated interpolymers may be prepared by known metallocene chemistry and may also be prepared as described in U.S. Patent Nos. 5,498,809; 5,663,130; 5,705,577; 5,814,715; 6,022,929 and 6,030,930.

[0047] Another useful class of polymers is that of polymers prepared by cationic polymerization of isobutene, styrene, and the like. Common polymers from this class include polyisobutenes obtained by polymerization of a C_4 refinery stream having a butene content of 35 to 75 mass %, and an isobutene content of 30 to 60 mass %, in the presence of a Lewis acid catalyst, such as

aluminum trichloride or boron trifluoride. A preferred source of monomer for making poly-n-butenes is petroleum feedstreams such as Raffinate II. These feedstocks are disclosed in the art such as in U.S. Patent No. 4,952,739. Polyisobutylene is a most preferred backbone because it is readily available by cationic polymerization from butene streams (e.g., using AlCl_3 or BF_3 catalysts). Such polyisobutylenes generally contain residual unsaturation in amounts of one ethylenic double bond per polymer chain, positioned along the chain. A preferred embodiment utilizes polyisobutylene prepared from a pure isobutylene stream or a Raffinate I stream to prepare reactive isobutylene polymers with terminal vinylidene olefins. Preferably, these polymers, referred to as highly reactive polyisobutylene (HR-PIB), have a terminal vinylidene content of at least 65%, e.g., 70%, more preferably at least 80%, most preferably, at least 85%. The preparation of such polymers is described, for example, in U.S. Patent No. 4,152,499. HR-PIB is known and HR-PIB is commercially available under the tradenames Glissopal™ (from BASF) and Ultravis™ (from BP-Amoco).

[0048] Polyisobutylene polymers that may be employed are generally based on a hydrocarbon chain of from 400 to 3000. Methods for making polyisobutylene are known. Polyisobutylene can be functionalized by halogenation (e.g. chlorination), the thermal "ene" reaction, or by free radical grafting using a catalyst (e.g. peroxide), as described below.

[0049] To produce (C) the hydrocarbon or polymer backbone may be functionalized with carboxylic anhydride-producing moieties selectively at sites of carbon-to-carbon unsaturation on the polymer or hydrocarbon chains, or randomly along chains using any of the three processes mentioned above or combinations thereof, in any sequence.

[0050] Processes for reacting polymeric hydrocarbons with unsaturated carboxylic, anhydrides and the preparation of derivatives from such compounds are disclosed in U.S. Patent Nos. 3,087,936; 3,172,892; 3,215,707; 3,231,587; 3,272,746; 3,275,554; 3,381,022; 3,442,808; 3,565,804; 3,912,764; 4,110,349; 4,234,435; 5,777,025; 5,891,953; as well as EP 0 382 450 B1; CA-1,335,895 and GB-A-1,440,219. The polymer or hydrocarbon may be functionalized, with carboxylic acid anhydride moieties by reacting the polymer or hydrocarbon under conditions that result in the addition of functional moieties or agents, i.e., acid anhydride, onto the polymer or hydrocarbon chains primarily at sites of carbon-to-carbon unsaturation (also referred to as ethylenic or olefinic unsaturation) using the halogen assisted functionalization (e.g. chlorination) process or the thermal "ene" reaction.

[0051] Selective functionalization can be accomplished by halogenating, e.g., chlorinating or brominating, the unsaturated α -olefin polymer to 1 to 8, preferably 3 to 7, mass % chlorine, or bromine, based on the weight of polymer or hydrocarbon, by passing the chlorine or bromine through the polymer at a temperature of 60 to 250°C, preferably 110 to 160°C, e.g., 120 to 140°C, for 0.5 to 10, preferably 1 to 7 hours. The halogenated polymer or hydrocarbon (hereinafter backbone) is then reacted with sufficient monounsaturated reactant capable of adding the required number of functional moieties to the backbone, e.g., monounsaturated carboxylic reactant, at 100 to 250°C, usually 180°C to 235°C, for 0.5 to 10, e.g., 3 to 8 hours, such that the product obtained will contain the desired number of moles of the monounsaturated carboxylic reactant per mole of the halogenated backbones. Alternatively, the backbone and the monounsaturated carboxylic reactant are mixed and heated while adding chlorine to the hot material.

[0052] While chlorination normally helps increase the reactivity of starting olefin polymers with monounsaturated functionalizing reactant, it is not necessary with some of the polymers or hydrocarbons contemplated for use in the present invention, particularly those preferred polymers or hydrocarbons which possess a high terminal bond content and reactivity. Preferably, therefore, the backbone and the monounsaturated functionality reactant, (carboxylic reactant), are contacted at elevated temperature to cause an initial thermal "ene" reaction to take place. Ene reactions are known.

[0053] The hydrocarbon or polymer backbone can be functionalized by random attachment of functional moieties along the polymer chains by a variety of methods. For example, the polymer, in solution or in solid form, may be grafted with the monounsaturated carboxylic reactant, as described above, in the presence of a free-radical initiator. When performed in solution, the grafting takes place at an elevated temperature in the range of 100 to 260°C, preferably 120 to 240°C. Preferably, free-radical initiated grafting would be accomplished in a mineral lubricating oil solution containing, e.g., 1 to 50, preferably 5 to 30, mass % polymer based on the initial total oil solution.

[0054] The free-radical initiators that may be used are peroxides, hydroperoxides, and azo compounds, preferably those that have a boiling point greater than 100°C and decompose thermally within the grafting temperature range to provide free-radicals. Representative of these free-radical initiators are azobutyronitrile, 2,5-dimethylhex-3-ene-2, 5-bis-tertiary-butyl peroxide and dicumene peroxide. The initiator, when used, is typically in an amount of between 0.005% and 1% by weight based on the weight of the reaction mixture solution. Typically, the aforesaid monounsaturated carboxylic reactant material and free-radical initiator are used in a weight ratio range of from 1.0:1 to 30:1, preferably 3:1 to 6:1. The grafting is preferably carried out in an inert

atmosphere, such as under nitrogen blanketing. The resulting grafted polymer is characterized by having carboxylic acid (or derivative) moieties randomly attached along the polymer chains, it being understood, of course, that some of the polymer chains remain ungrafted. The free radical grafting described above can be used for the other polymers and hydrocarbons used in the present invention.

[0055] The preferred monounsaturated reactants that are used to functionalize the backbone comprise mono- and dicarboxylic acid material, i.e., acid, or acid derivative material, including (i) monounsaturated C₄ to C₁₀ dicarboxylic acid wherein (a) the carboxyl groups are vicinyl, (i.e., located on adjacent carbon atoms) and (b) at least one, preferably both, of the adjacent carbon atoms are part of the mono unsaturation; (ii) derivatives of (i) such as anhydrides or C₁ to C₅ alcohol derived mono- or diesters of (i); (iii) monounsaturated C₃ to C₁₀ monocarboxylic acid wherein the carbon-carbon double bond is conjugated with the carboxy group, i.e., of the structure -C=C-CO-; and (iv) derivatives of (iii) such as C₁ to C₅ alcohol derived mono- or diesters of (iii). Mixtures of monounsaturated carboxylic materials (i) - (iv) also may be used. Upon reaction with the backbone, the monounsaturation of the monounsaturated carboxylic reactant becomes saturated. Thus, for example, maleic anhydride becomes backbone-substituted succinic anhydride, and acrylic acid becomes backbone-substituted propionic acid. Exemplary of such monounsaturated carboxylic reactants are fumaric acid, itaconic acid, maleic acid, maleic anhydride, chloromaleic acid, chloromaleic anhydride, acrylic acid, methacrylic acid, crotonic acid, cinnamic acid, and lower alkyl (e.g., C₁ to C₄ alkyl) acid esters of the foregoing, e.g., methyl maleate, ethyl fumarate, and methyl fumarate.

[0056] To provide the required functionality, the monounsaturated carboxylic reactant, preferably maleic anhydride, typically will be used in an amount ranging from equimolar amount to 100 mass % excess, preferably 5 to 50 mass % excess, based on the moles of polymer or hydrocarbon. Unreacted excess monounsaturated carboxylic reactant can be removed from the final dispersant product by, for example, stripping, usually under vacuum, if required.

CO-ADDITIVES

[0057] The lubricating oil composition of the invention may comprise further additives, different from and additional to (B) and (C). Such additional additives may, for example include ashless dispersants, other metal detergents, anti-wear agents such as zinc dihydrocarbyl dithiophosphates, anti-oxidants and demulsifiers. In some cases, an ashless dispersant need not be provided.

[0058] It may be desirable, although not essential, to prepare one or more additive packages or concentrates comprising the additives, whereby additives (B) and (C) can be added simultaneously to the base oil to form the lubricating oil composition. Dissolution of the additive package(s) into the lubricating oil may be facilitated by solvents and by mixing accompanied with mild heating, but this is not essential. The additive package(s) will typically be formulated to contain the additive(s) in proper amounts to provide the desired concentration, and/or to carry out the intended function in the final formulation when the additive package(s) is/are combined with a predetermined amount of base oil. Thus, additives (B) and (C), in accordance with the present invention, may be admixed with small amounts of base oil or other compatible solvents together with other desirable additives to form additive packages containing active ingredients in an amount, based on the additive package, of, for example, from 2.5 to 90, preferably from 5 to 75, most preferably from 8 to 60, mass % of additives in the appropriate proportions, the remainder being base oil.

[0059] The final formulation as a trunk piston engine oil may typically contain 30, preferably 10 to 28, more preferably 12 to 24, mass % of the additive package(s), the remainder being base oil. The trunk piston engine oil may have a compositional TBN (using ASTM D2896) of 20 to 60, such as, 30 to 55. For example, it may be 40 to 55 or 35 to 50.

EXAMPLES

[0060] The present invention is illustrated by but in no way limited to the following examples.

COMPONENTS

[0061] The following components were used:

Ester Basestocks (A1)

[0062]

- a polyol ester (PRIOLUBE (Registered Trade Mark) 3970), a trimethylolpropane ester with C8-10 fatty acids, having a viscosity of $4.4 \text{ mm}^2\text{s}^{-1}$ at 100°C , ex Croda Lubricants;
- a polymer ester (KETJENLUBE (Registered Trade Mark) 115), in the form of a copolymer of alpha-olefins and a dicarboxylic acid dibutylester with an average molecular weight of approximately 1400.

Basestocks (A2)

[0063]

- a Group I oil (XOMAPE 600) (for comparison)
- a Group II oil (RLOP 600)
- a Group III oil (YUBASE 8)

[0064] Commercial identifications are in parentheses.

Detergents (B)

[0065]

- calcium alkyl salicylate (BI 8.0)
- calcium alkyl salicylate (BI 3.0)

[0066] Basicity indices are in parentheses.

PIBSA (C)

[0067] a polyisobutene succinic anhydride derived from a polyisobutene having a number average molecular weight of 950

HFO

[0068] a heavy fuel oil (ISO-F-RMK 380)

TRUNK PISTON MARINE ENGINE LUBRICATING OILS (TPEO'S)

[0069] Selections of the above components were blended to give a range of TPEO's. Some are examples of the invention; others are reference examples for comparison purposes. The compositions of the TPEO's tested when each contained an HFO are given (in mass %) in the tables below under the RESULTS heading.

TESTING

Light Scattering

[0070] Test trunk piston marine engine lubricating oils (TPEO's) were evaluated for asphaltene dispersancy using light scattering according to the Focused Beam Reflectance Method ("FBRM"), which predicts asphaltene agglomeration and hence 'black sludge' formation.

[0071] The FBRM test method was disclosed at the 7th International Symposium on Marine Engineering, Tokyo, 24th - 28th October 2005, and was published in "The Benefits of Salicylate Detergents in TPEO Applications with a Variety of Base Stocks" in the Conference Proceedings. Further details were disclosed at the CIMAC Congress, Vienna, 21st-24th May 2007 and published in "Meeting the Challenge of New Base Fluids for the Lubrication of Medium Speed Marine Engines - An Additive Approach" in the Congress Proceedings. In the latter paper it is disclosed that, by using the FBRM method, it is possible to obtain quantitative results for asphaltene dispersancy that predict performance for lubricant systems based on base stocks containing greater than or less than 90% saturates, and greater than or less than 0.03% sulphur. The predictions of relative performance obtained from FBRM were confirmed by engine tests in marine diesel engines.

[0072] The FBRM probe contains fibre optic cables through which laser light travels to reach the probe tip. At the tip, an optic focuses the laser light to a small spot. The optic is rotated so that the focussed beam scans a circular path between the window of the probe and the sample. As particles flow past the window, they intersect the scanning path giving backscattered light from the individual particles.

[0073] The scanning laser beam travels much faster than the particles; this means that the particles are effectively stationary. As the focussed beam reaches one edge of the particle, the amount of backscattered light increases; the amount will decrease when the focussed beam reaches the other edge of the particle.

[0074] The instrument measures the time of the increased backscatter. The time period of backscatter from one particle is multiplied by the scan speed and the result is a distance or chord length. A chord length is a straight line between any two points on the edge of a particle. This is represented as a chord length distribution, a graph of numbers of chord lengths (particles) measured as a function of the chord length dimensions in microns. As the measurements are performed in real time, the statistics of a distribution can be calculated and tracked. FBRM typically measures tens of thousands of chords per second, resulting in a robust number-by-chord length distribution. The method gives an absolute measure of the particle size distribution of the asphaltene particles.

[0075] The Focused beam Reflectance Probe (FBRM), model Lasentec D600L, was supplied by Mettler Toledo, Leicester, UK. The instrument was used in a configuration to give a particle size resolution of 1 μm to 1mm. Data from FBRM can be presented in several ways. Studies have suggested that the average counts per second can be used as a quantitative determination of asphaltene dispersancy. This value is a function of both the average size and level of agglomerate. In this application, the average count rate (over the entire size range) was monitored using a measurement time of 1 second per sample.

[0076] The test TPEO's were heated to 60°C and stirred at 400rpm; when the temperature reached 60°C the FBRM probe was inserted into the sample and measurements made for 15 minutes. An aliquot of heavy fuel oil (10% w/w) was introduced into the TPEO under stirring using a four-blade stirrer (at 400 rpm). A value for the average counts per second was taken when the count rate had reached an equilibrium value (typically overnight).

RESULTS

Light Scattering

[0077] The results of the FBRM tests are summarized in the tables below, where lower particle count indicates better performance.

[0078] Reference examples are designated "Ref".

TABLE 1

Each TPEO tested had a BN of 40, contained 1.23 mass% (in terms of calcium) of calcium salicylate of BI 8.0 and 0.24 mass % (in terms of calcium) of calcium salicylate of BI 3.0, and contained the same amount of Zn and of silicone antifoam. The remainder of the finished oil components are given in the table below:

Example	PIBSA (C) (% active matter)	Priolube 3970 (A1) (wt %)	Group II Oil (A2)	Group I Oil	Lasentec Counts
Ref 1	-	-	-	Balance	2,032.43
Ref 2	-	-	Balance	-	5,988.84
Ref 3	-	10.00	Balance	-	9,613.23
Ref 4	-	30.00	Balance	-	732.81
Ref 5	4.80	-	Balance	-	2,205.86
1	4.80	10.00	Balance	-	786.41
2	4.80	30.00	Balance	-	12.82
3	4.80	80.83	-	-	13.89

[0079] Ref 3 and Ref 4 are illustrative of US Patent Application Publication No. 2011/0319304 A1 ('304).

[0080] Ref 4 (use of ester alone) confirms the teaching of '304.

[0081] Ref 5 (use of PIBSA alone) confirms the teaching of '594.

[0082] Examples 1-3 confirm the synergy of PIBSA and ester.

TABLE 2

Each TPEO tested had a BN of 40, contained 0.75 mass % (in terms of calcium) of calcium salicylate of BI 8.0 and 0.68 mass % (in terms of calcium) of calcium salicylate of BI 3.0, and contained the same amount of Zn. The remainder of the finished oil components are given in the table below:

Example	PIBSA (C) (% active matter)	Priolube 3970 (A1) (wt %)	Ketjenlube 115 (A1) (wt%)	Group II (A2)	Group I	Group III (A2)	Lasentec Counts
Ref 6	-	-	-	-	Balance	-	933.83
4	4.80	1.00	-	Balance	-	-	391.79
5	4.80	3.00	-	Balance	-	-	223.56
6	4.80	5.00	-	Balance	-	-	251.08
7	4.80	7.00	-	Balance	-	-	161.13
8	4.80	10.00	-	Balance	-	-	48.38
9	0.80	10.00	-	Balance	-	-	3,499.45
10	1.60	10.00	-	Balance	-	-	1,333.98
11	2.40	10.00	-	Balance	-	-	421.74
12	3.20	10.00	-	Balance	-	-	268.40
13	4.00	10.00	-	Balance	-	-	47.87
14	4.80	10.00	-	-	-	Balance	737.14
15	4.80	-	10	Balance	-	-	110.03

[0083] The results show that varying the treat rate of PIBSA and ester affects performance: in Examples 4-8, the PIBSA treat rate is kept constant and the ester treat rate progressively increased; in Examples 9-13, the ester treat rate is kept constant and the PIBSA treat rate is progressively increased. Example 14 shows the applicability of the invention to a Group III base oil beyond that

of Ref 6 (a Group I oil) and Example 15 shows the applicability of the invention to esters other than Priolube 3970.

TABLE 3

Each TPEO treated had a BN of 30, contained 0.56 mass % (in terms of calcium) of calcium salicylate of BI 8.0 and 0.51 mass % (in terms of calcium) of calcium salicylate of BI 3.0, and contained the same amount of Zn. The remainder of the finished oil components are given in the table below:

Example	PIBSA (C) (% active matter)	Priolube 3970 (A1) (wt %)	Group II (A2)	Group I	Lasentec Counts
Ref 7	-	-	-	Balance	1,755.35
Ref 8	2.40	-	Balance	-	3,638.42
17	2.40	1.00	Balance	-	1,622.23
18	2.40	3.00	Balance	-	1,805.06
19	2.40	5.00	Balance	-	1,626.40
20	2.40	7.00	Balance	-	1,135.09
21	2.40	10.00	Balance	-	899.70

[0084] The results show that the effect of the invention is exhibited in lower BN TPEO's.

REFERENCES CITED IN THE DESCRIPTION

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Patentkrav

- 5 1. Smøreoliesammensætning til en trunkstempelskibsmotor til forbedring af asfaltenhåndtering ved anvendelse deraf under motordriften, når den tankes op med en svær brændselsolie, hvilken sammensætning omfatter eller er fremstillet ved tilsætning af
- (A) 50 masseprocent eller mere af sammensætningen af en olie med smøreviskositet, som er enten:
- 10 - et olieopløseligt esterbasismateriale (A1); eller
- omfatter 0,1 til 90 masseprocent af en olieopløselig esterbasismateriale (A1), og som rest af 50 masseprocent eller mere af olien af smøreviskositet, af et basismateriale, som indeholder mere end eller er lig med 90 % mættede dele og mindre end eller lig med 0,03 % svovl eller en blanding deraf (A2);
- 15 (B) et olieopløseligt overbasisk metalhydrocarbyl-substitueret hydroxybenzoatdetergent i en mindre mængde; og;
- (C) en olieopløselig polyalkenyl-substitueret carbonsyreanhydrid i en mindre mængde på mere end 0,1 til mindre end 10 masseprocent af sammensætningen, hvor polyalkenylgruppen eller mindst én polyalkenylgruppe er afledt fra polyalken med en gennemsnitlig molekylvægt i tal fra 200 til 3000.
- 20
2. Smøreolie ifølge krav 1, hvor basismaterialet (A2), hvis det er til stede, i olien med smøreviskositet indeholder mere end 60 masseprocent af et basismateriale, som indeholder mere end eller er lig med 90% mættede dele og mindre end eller lig med 0,03 % svovl eller en blanding deraf.
- 25
3. Smøreolie ifølge krav 1 eller 2, hvor basismaterialet (A2), hvis det er til stede, er et materiale fra Gruppe II, Gruppe III eller Gruppe IV.
- 30
4. Smøreolie ifølge krav 1, 2 eller 3, hvor metaldetergentet (B) er et calciumalkylsalicylat-detergent.
5. Smøreolie ifølge krav 4, hvor metaldetergentet (B) er C₉ til C₃₀ alkyl-substitueret.

6. Smøreolie ifølge krav 4 eller 5, hvor metaldetergentet (B) er C_{20} eller højere alkyl-substitueret.
- 5 7. Smøreolie ifølge et hvilket som helst af kravene 1 til 6, hvor polyalkenyl-substituenten i anhydriden (C) har fra 8 til 400 carbonatomer.
- 10 8. Smøreolie ifølge et hvilket som helst af kravene 1 til 7, hvor polyalkenyl-substituenten i anhydriden (C) har en gennemsnitlig molekylvægt i tal fra 350 til 1000.
- 15 9. Smøreolie ifølge et hvilket som helst af kravene 1 til 8, hvor den polyalkenyl-substituerede carboxylsyreanhydrid (C) er en ravsyreanhydrid.
- 10 10. Smøreolie ifølge et krav 9, hvor ravsyreanhydriden (C) er en polybuten-ravsyreanhydrid.
- 20 11. Smøreolie ifølge et hvilket som helst af kravene 1 til 10, hvor esterbasis-materialet (A1) forefindes i en mængde på 10 til 90 masseprocent.
- 25 12. Smøreolie ifølge et hvilket som helst af kravene 1 til 11, hvor esterbasis-materialet (A1) har en kinematisk viskositet på 2 til 10 mm^2s^{-1} ved 100°C.
- 30 13. Smøreolie ifølge et hvilket som helst af kravene 1 til 12, hvor esterbasis-materialet (A1) er et polyolesterbasismateriale.
- 35 14. Smøreoliesammensætning ifølge et hvilket som helst af kravene 1 til 13, yderligere omfattende et indhold af tung brændselsolie.
15. Fremgangsmåde til drift af en kompressionstændt trunkstempelskibsmotor med middelomdrejningstal, hvilken fremgangsmåde omfatter
(i) optankning af motoren med en tung brændselsolie; og
(ii) smøring af motorens krumbank med en sammensætning som defineret i et hvilket som helst af kravene 1 til 14.
16. Fremgangsmåde til dispergering af asfaltener i en smøreoliesammensætning til et skibstrunkstempel under dens smøring af fladerne af forbræn-

dingskammeret af en kompressionstændt skibsmotor med middelomdrejningstal og drift af motoren, hvilken fremgangsmåde omfatter

(i) det at tilvejebringe en sammensætning som defineret i et hvilket som helst af kravene 1 til 14;

5 (ii) det at forsyne forbrændingskammeret med sammensætningen;

(iii) det at forsyne forbrændingskammeret med tung brændselsolie; og

(iv) det at forbrænde den tunge brændselsolie i forbrændingskammeret.

10 **17.** Fremgangsmåde ifølge krav 16, hvor dispergering af asfaltener måles ved anvendelse af FBRM-fremgangsmåden (Focussed Beam Reflectance Method).

15 **18.** Anvendelse af et detergent (B) i kombination med en komponent (C) som defineret i, og i mængderne angivet i et hvilket som helst af kravene 1 til 14, i en smøreoliesammensætning til et skibstrunkstempel til en kompressions-
tændt trunkstempelskibsmotor med middelomdrejningstal, hvor sammensæt-
ningen omfatter en olie med smøreolieviskositet (A) i en større mængde som
defineret i krav 1, for at tilvejebringe sammenlignelig eller forbedret håndte-
ring af asfalten under driften af motoren forsynet med svær brændselsolie, og
20 smøringen deraf med sammensætningen, i sammenligning med drift af en
sammenlignelig olie, hvor basismaterialet (A2) er et basismateriale af Gruppe I.

25 **19.** Fremgangsmåde ifølge krav 18, hvor asfaltenhåndtering under drift af motoren måles ved anvendelse af FBRM-fremgangsmåden (Focussed Beam Reflectance Method).