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APPLICATION FOR A STANDARD PATENT 602969

1/We Amoco Corporation

200 East Randolph Drive, Chicago, Illinois, UNITED STATES OF AMERICA.

hereby apply for the grant of a standard patent for an invention entitled:

MANNICH DISPERSANT VI-IMPROVER BLENDED WITH PHENOLIC COMPOUND FOR IMPROVED STORAGE STABILITY

which is described in the accompanying complete specification.

Details of basic application

Number of basic application: 031,355

Convention country in which

basic application was filed: UNITED STATES OF AMERICA

Date of basic application : 30 March 1987

Address for Service:

PHILLIPS ORMONDE & FITZPATRICK Patent and Trade Mark Attorneys 367 Collins Street Melbourne 3000 AUSTRALIA

Dated: 21 March 1988

PHILLIPS ORMONDE & FITZPATRICK Attorneys for: Amoco Corporation

By:

Our Ref : 88290 POF Code: 1482/1482



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ADDITION ACCEPTED AND AMENDMENTS PERMITS

STAMP TO YALUE OF 180: ATTACHED

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DECLARATION FOR A PATENT APPLICATION

INSTRUCTIONS Insert "Convention" if applicable Insert FULL name(s)
of applicant(s)

In support of the (a) Convention

application made by

AMOCO CORPORATION

Insert "of addition" if applicable Insert TITLE of invention

(hereinafter called "applicant(s) for a patent (c) invention entitled (d)

for an

MANNICH DISPERSANT VI-IMPROVER BLENDED WITH PHENOLIC COMPOUND FOR IMPROVED STORAGE STABILITY

Insert FULL name(s)
AND address(cs) of
declarant(s)
(See headnote*)

Inte t FULL name(s)
AND address(es) of
actual inventor(s)

) Recite how appli-cant(s) derive(s) title from actual inventor(s) (See headnote**)

Insert country, filing date, and hasic applicant(a) for the/or EACH basic application

I/We (c) Ralph Charles Medhurst, General Manager, Patents and Licensing Department, of 416 Illinois Street, Park Forest, Illinois 60466 United States of America

do solemnly and sincerely declare as follows:

1. I am/We are the applicant(s).

(or, in the case of an application by a body corporate)

- 1. I am/We are authorized to make this declaration on behalf of the applicant(s).
- 2. I-am/We are the actual inventor(s) of the invention. (or, where the applicant(s) is/are not the actual inventor(s))

(f) Yoon Soo Song: 664 Chippewa Drive, Naperville, Illinois 60540, United States of America and Robert Joseph Basalay: 1117 Catalpa Lane, Naperville, Illinois 60540, United States of America

ig/are the actual inventor(s) of the invention and the facts upon which the applicant(g) is/are entitled to make the application are as follows:

(g)

The applicant is the assignee of the said inventors.

(Note: Paragraphs 3 and 4 apply only to Convention applications)

The basic application(s) for patent or similar protection on which the application is based is/are identified by country, filing date, and basic applicant(s) as follows:

UNITED STATES OF AMERICA 30 March, 1987 Yoon Soo Song and Robert Joseph Basalay

4. The basic application(3) referred to in paragraph 3 hereof was/were the first application(3) made in a Convention country in respect of the invention the subject of the application.

> Declared at (k) Chicago, Illinois U.S.A.

GENERAL MALVH CHARLES MEDHURST, MANAGER, PATENTS AND LICENSING

DEPARTMENT

To: The Commissioner of Patents

) Insert PLACE of signing

Insert DATE of signing

n) Signature(s) of declarant(s)

lote: No legalization or ther witness required

18/7/78

PHILLIPS ORMONDE & FITZPATRICK Patent and Trade Mark Attorneys 367 Collins Street Melbourne, Australia

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- (74) Attorney or Agent PHILLIPS ORMONDE & FITZPATRICK, 367 Collins Street, MELBOURNE VIC 3000
- (57) Claim
- 1. An improved dispersant and viscosity index improving Mannich composition suitable for use as lubricant additive having reduced susceptibility to viscosity increase during storage, consisting essentially of physical blend prepared by admixing (a) Mannich condensation product obcained from the Mannich reaction of an oxidized polymer, an amine and a formaldehyde yielding reagent and (b) from 0.1 to 20 wt% of a phenolic compound having the formula represented by:

wherein R is any hydrocarbyl or hydroxy-, chloro-, bromo-substituted hydrocarbyl group which results oil soluble phenol or salt thereof and y is an integer from 1-5, said R group having a molecular weight of 15 to 100,000, and said improved composition being essentially free of other lubricant additive compositions.

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COMPLETE SPECIFICATION (ORIGINAL)

Class

Int. Class

This document contains the

amendments made under Section 49 and is correct for

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Application Number: Lodged:

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Related Art:

APPLICANT'S REFERENCE: 27,018

Name(s) of Applicant(s):

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Address(es) of Applicant(s):

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Complete Specification for the invention entitled:

MANNICH DISPERSANT VI-IMPROVER BLENDED WITH PHENOLIC COMPOUND FOR IMPROVED STORAGE STABILITY

Our Ref : 88290 POF Code: 1482/1482

The following statement is a full description of this invention, including the best method of performing it known to applicant(s):

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MANNICH DISPERSANT VI-IMPROVER BLENDED WITH PHENOLIC COMPOUND FOR IMPROVED STORAGE STABILITY

This invention relates to an oil soluble Mannich condensation product prepared from an oxidized olefin polymer, an amine, and an aldehyde. More particularly, it relates to a Mannich condensation product admixed or blended with an phenolic compound for improved storage stability measured in terms of greater resistance to viscosity increase upon storage in the presence of air.

The operation of diesel and spark ignition internal combustion engines is typically accompanied by lubricant deterioration, which results in the formation of sludge, lacquer, and resinous deposits on interior engine surfaces. These lubricant deterioration products reduce engine efficiency and accelerate engine wear. In order to prevent or reduce the formation of these deposits, a wide variety of chemical additives have been developed for incorporation into lubricating oils. These additives, which are commonly referred to as detergents or dispersants, have the ability to keep deposit-forming materials suspended in the oil so that the engine remains in a clean and efficient operating condition for extended periods of time.

A further characteristic of lubricating oils is their tendency to become thin at elevated temperatures while becoming thick at low temperatures. In the case of a 25 crankcase lubricating oil, it is desirable that the oil not become so thick in a cold engine that starting is difficult. On the other hand, the oil must remain sufficiently viscous in a hot engine so that an oil film is maintained between the moving parts. As a consequence, it 30 is frequently necessary to incorporate additives into lubricating oils which serve to improve the viscositytemperature relationship. Additives which have the ability to reduce the variation with temperature of the 35 viscosity of a lubricating oil are commonly referred to as viscosity index improvers.

Commonly assigned U.S. Patent Nos. 3,864,268 (1975) and 3,872,019 of Culbertson, et al.; U.S. Patent Nos. 4,011,380 (1977), 4,131,553 (1978), and 4,170,562 (1979) of West; and U.S. Patent No. 4,444,956 (1984) of Schaffhausen, et al. (all of which are incorporated by reference herein) disclose preparation of lubricant additives which exhibit both dispersant and viscosity index improving properties. These additives are obtained from 0 Mannich condensation of an oxidized, high molecular weight, amorphous ethylene-propylene copolymer with a formaldehyde-yielding reactant, and a primary or secondary amine or polyamine.

While these products are excellent commercial lubricant additives, it has been observed that the commercial
product, generally comprising about 5 to 15 wt. percent
additive and about 85-95% neutral base oil, has a tendency
to gradually increase in viscosity upon storage, an effect
which we find becomes more pronounced as the total amount
of polymer in the product, versus the amount of diluent
oil, increases.

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Viscosity increase on storage can be particularly troublesome in the case of Mannich dispersant/VI improvers having greater shear stability. One method for improving 25 shear stability in Mannich products obtained from a given molecular weight polymer is to subject the polymer to greater oxidation such that the polymer, prior to the Mannich condensation, is degraded to a lower molecular weight and viscosity, and is thus more shear stable in terms of a Bosch Shear Stability index measurement. While deeper 30 oxidation can enhance the final shear stability of the Mannich product, it has the disadvantage of reducing the thickening power of the polymeric Mannich additive material. Therefore, to compensate for the loss in thickening 35 power it is necessary to use more polymer in the oxidation step in order that the final product has a higher concentration of polymer. Unfortunately, higher polymer levels

in the final product can render the product more susceptible to viscosity increase on storage in the presence of oxygen. Although the mechanism for such viscosity increase is not well understood, it is believed, without limitation, that the polymeric Mannich condensation product possibly undergoes cross-linking reactions tending to increase the molecular weight of the polymeric additive, and hence its viscosity.

Based on the foregoing, there is a clear need for improved polymeric Mannich VI-improver/dispersant compositions which are less susceptible to viscosity increase on storage.

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West U.S. Patent No. 4,170,562 discloses that the Mannich condensation reaction of oxidized olefinic polymers with an amine and formaldehyde can be carried out in the presence of 0.01 to 25.0 wt. percent of an oil soluble phenol based on the neat polymer to improve the processing and properties of the oxidized oil soluble Mannich reaction product. In particular, West teaches that the inclusion of the phenol as a reactant during the Mannich reaction prevents undesirable resin formation and large increases in viscosity during the Mannich reaction. Although West is directed to preventing resin formation and viscosity increase during the Mannich reaction, it is also the case that the presence of a phenolic compound during the Mannich reaction can improve the storage stability of the finished product, such that the product has less tendency to undergo viscosity increase upon storage.

Unfortunately, despite the efficacy of using phenol compounds, as taught in West, to control viscosity increases and resin formation during the Mannich reaction, and to improve the storage stability of the final product, it is presently more desirable to avoid the addition of the phenol compound during the Mannich reaction. The reason for this is that the viscosity increase observed during the Mannich reaction can be a valuable indicator of

the completeness of the reaction. We have therefore found it useful to measure the viscosity increase produced during the Mannich reaction as a convenient preliminary quality check in combination with other analytical tools, such as infrared analysis. The tendency of the phenolic compounds to suppress the viscosity increase is thus seen as a disadvantage. Also, when phenol present as a Mannich reactant it can impair the reliability of infrared analysis to accurately detect the presence of carbonyl in the final product, thus hampering the use of IR as a quality control tool.

It is therefore desired to obtain the benefits of the phenol treatment of West in terms of storage stability in the product without having to include the phenol compound, as West teaches, directly in the Mannich reaction as an additional reactant.

A general object of the present invention is thus to improve the storage stability of a Mannich condensation product obtained from the reaction of an oxidized olefin polymer with an amine and an aldehyde. More particularly, an object of the invention is to obtain the storage stability benefits of treating the Mannich condensation product with a phenolic compound without need for the phenolic compound to be present as a reactant during the Mannich reaction. Other objects appear hereinafter.

We have now found that the objects of the present invention can be obtained in an improved dispersant and VI-improving Mannich composition having reduced susceptibility to viscosity increase during storage, which composition comprises a physical blend prepared by admixing a phenolic compound with a Mannich condensation product obtained from the Mannich reaction of an oxidized polymer, an amine, and a formaldehyde yielding reagent.

The present invention, which obviates the prior art requirement of including the phenol compound as one of the Mannich reactants, provides an improved Mannich condensa-



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polymer with an amine and an aldehyde.

According to the present invention there is provided improved dispersant and viscosity index an improving Mannich composition suitable for use as lubricant **a** . susceptibility to having reduced consisting essentially increase during storage, admixing physical blend prepared by (a) condensation product obtained from the Mannich reaction of an oxidized polymer, an amine and a formaldehyde yielding reagent and (b) from 0.1 to 20 wt% of a phenolic compound having the formula represented by:

wherein R is any hydrocarbyl or hydroxy-, chloro-, or bromo-substituted hydrocarbyl group which results in an oil soluble phenol or salt thereof and y is an integer from 1-5, said R group having a molecular weight of 15 to 100,000, and said improved composition being essentially free of other lubricant additive compositions.

According to the present invention there is further provided method for reducing a the tendency of dispersant and viscosity index improving Mannich condensation product to increase in viscosity storage, which comprises admixing from 0.1 to 20 wt% of a phenolic compound with a dispersant and viscosity index improving Mannich condensation product obtained from the Mannich reaction of an oxidized olefin polymer, an amine and a formaldehyde yielding reagent wherein the phenolic compound has a formula represented by:

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wherein R is any hydrocarbyl or hydroxy-, chloro-, or bromo-substituted hydrocarbyl group which results in an oil soluble phenol or salt thereof and y is an integer from 1-5, said R group having a molecular weight of 15 to 100,000, said admixture being essentially free of other lubricant additives.

We have now found that the object of the present invention can be obtained in an improved dispersant and VI improving Mannich composition having susceptibility to viscosity increase during storage, which composition comprises physical а blend prepared admixing a phenolic compound with a Mannich condensation product obtained from the Mannich reaction of an oxidized polymer, an amine, and a formaldehyde yielding reagent.

The present invention, which obviates the prior art requirement of including the phenol compound as one of the Mannich reactants, provides an improved Mannich condensa-

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tion product having reduced susceptibility to viscosity increase during storage.

In its method aspect, the invention is directed to a method for reducing the tendency of a dispersant VI-improver Mannich condensation product to increase in viscosity during storage, the method comprising admixing a phenolic compound with a Mannich condensation product obtained from the Mannich reaction of an oxidized olefin polymer, an amine, and an a formaldehyde-yielding reactant.

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The invention is further directed to a method for producing an improved Mannich dispersant and VI-improving lubricant additive composition having reduced susceptibility to viscosity increase during storage, the method comprising (a) oxidizing an olefinic polymer, (b) condensing the oxidized olefinic polymer with an amine and a formal-dehyde-yielding reagent under Mannich reaction conditions and (c) admixing the Mannich condensation product obtained in step (b) with a phenolic compound.

The advantages of the invention include the ability to improve the storage stability of Mannich dispersant/VI-improvers by merely physically blending a phenolic compound with the Mannich product, as contrasted with the prior art method of including the phenol as a reactant during the Mannich condensation. Physical blending is preferred because the viscosity increase observed during the Mannich reaction of the oxidized polymer, amine, and aldehyde, when phenol is not present as an additional Mannich reactant, can be used to monitor the completion of the Mannich reaction. Also, IR analysis of the Mannich product is more reliable if the phenol is absent during the Mannich reaction. Finally, greater product flexibility is afforded in that the improved storage stability can be imparted on an "as needed" basis to previously manufactured Mannich product without need for modifying current Mannich manufacturing practices which may

not presently include the addition of phenolic compounds during the Mannich reaction.

Briefly, the Mannich reaction products of the present 5 invention having improved storage stability can be produced by admixing a Mannich condensation product resulting from the Mannich reaction of an oxidized olefinic polymer, an amine, and a formaldehyde-yielding reagent at a temperature of about 250°-400°F product with a phenolic compound at altemperature of about 100-300°F.

The Mannich condensation reaction can be conducted using a nonreactive solvent such as aromatic or aliphatic hydrocarbons, or lubricant oils. Further details of the Mannich condensation reaction are found in Culbertson, et 15 al., U.S. Patent No. 3,872,019, which is expressly incorporated by reference herein.

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The Mannich reaction can be catalyzed by addition of an alkylbenzene sulfonic acid. The oxidized high molecular weight polymer is aminated in the presence of about 20 0.01 to 40.0 wt.% (based on the copolymer) of an oil soluble sulfonic acid. To avoid darkening the reaction mixture, the sulfonic acid is added at the same time as the This catalyst is disclosed in amine or after the amine. West U.S. Patent No. 4,131,553 and is incorporated herein by reference.

The term "olefinic" polymer as used herein and in the claims refers to amorphous addition polymers or copolymers derived from olefinically unsaturated monomers or mixtures thereof. Such olefin monomers include olefins of the general formula R--CH==CH2, in which R is hydrogen, an aliphatic or cycloaliphatic radical of from 1 to about 20 carbon atoms, for example, propene, isobutylene, 1-butene, 1-hexene, 4-methyl-1-pentene, and 1-decene. Other olefinic monomers having a plurality of double bonds can be used, in particular, diolefins containing from about 4 to about 25 carbon atoms, e.g., 1,3-butadiene, 1,4-hexadiene, 1,4-pentadiene, 2-methyl-1,5-hexadiene, 1,7-octadiene,

5-methylene-2-norbornene, norbornadiene, vinyl norbornene, etc.

Suitable ethylene, propylene copolymers comprise about 20 to about 70, preferably from about 35 to about 45, mole percent propylene and have number average molecular weights of at least 20,000, i.e., from about 20,000 to about 200,000 or more.

A particularly suitable ethylene-propylene copolymer 10 is one having the following characteristics:

Number Average Molecular About 60,000
Weight Percent (Molar) Propylene 39-43
Monomer Melt Flow 2.2-3.3 (B)
Mooney Viscosity 65-75 (C)

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- (A) GPC as calibrated against polybutene standards.
- (B) ASTM D-1248 10.1 Kg at 230°C.
- (C) ASTM D-1646 ML 1 + 4 at 125° C.

Methods of preparation of the copolymers are well known. Such methods are described in many U.S. Patents, i.e., U.S. Patent Nos. 2,700,633; 2,725,231; 2,792,288; 2,933,480; 3,000,866; 3,063,973; 3,093,621, and others, which are all incorporated by reference.

The polymer can be oxidized by contacting the polymer under suitable conditions of temperature and at atmospheric or elevated pressures with an oxidizing agent such as air or free oxygen or any oxygen containing material capable of releasing oxygen under these conditions. If desired, the oxidation can be conducted in the presence of known oxidation catalysts such as platinum or platinum group metals and compounds containing metals such as copper, iron, cobalt, cadmium, manganese vanadium, etc. The oxidation can be carried out by methods described in U.S. Patent Nos. 2,982,728; 3,316,177; 3,153,025;

3,865,499; and 3,544,520, which are all incorporated by reference.

Generally, the oxidation can be carried out over a wide temperature range, depending upon the oxidizing agent used; for example, with an active oxidizing agent, e.g., SO_3 , temperatures in the range of $-40^{\circ}F$ to $400^{\circ}F$ can be used, while with less active oxidizing agents, e.g., air, temperatures in the range of 100°-800°F can be used. polymers are generally dissolved in oil prior to the oxidation. Further, depending upon the rate desired, the 10 oxidation can be conducted at subatmospheric, atmospheric, or super-atmospheric pressures, and in the presence or absence of oxidation catalysts. The conditions of temperature, pressure, oxygen content of the oxidizing agent, the rate of introducing the oxidizing agent, the catalyst employed, if any, etc., are correlated and controlled by those skilled in the art, so as to obtain the desired optimum results.

The following illustrates a preferred method of oxidizing a polymer. To a copolymer of ethylene and propylene (7 parts), having a number average molecular weight of about 60,000 was added a solvent-extracted SAE 5W mineral oil (93 parts) in an open reaction vessel, and the mixture slowly stirred and heated at a temperature of 370°F, under an inert gas atmosphere, until the solution 25 of the rubber-like polymer in the solvent was affected. Maintaining the 370°F temperature, the mixture was rapidly agitated in an atmosphere diluted 1:1 with nitrogen to promote the oxidation of the copolymer. A 50:50 air/nitrogen ratio was used to preclude the possibility of an explosive mixture being formed. Reaction in the 30 described manner was continued for 2.0-4.0 hours. 5-50 oxygen atoms per molecule of the copolymer were introduced under such oxidation conditions.

As indicated in U.S. Patent Nos. 4,011,380 and 4,131,553, sulfonic acid compounds can be advantageously used in the oxidation. Some of the sulfonic acid compounds which can be used have the general formula:

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where R is alkyl, aryl, hydroxy, chloro, or bromo substituted alkyl; n is an integer of 1-5, X is a cation, and M is the valence of the cation. In some cases, the R group can be made by polymerizing C_2 - C_6 olefins to a molecular weight in the range of about 80 to about 1,000 and then attaching said group to a benzene ring by well-known alkylation techniques.

15 R can be any hydrocarbon or substituted hydrocarbon which results in an oil-soluble benzene sulfonic acid. R can be a low molecular weight alkyl with greater than 0 carbon atoms such as nonyl, decyl, dodecyl, and the like with a molecular weight of at least about 120; an intermediate molecular weight hydrocarbyl such as polybutylene or polypropylene polymers with 15 to 1,000 carbon atoms with a molecular weight of at least 200; a high molecular weight hydrocarbyl such as polyolefin having a number average mclecular weight of 100,000; and others. 25 substituted with groups such as chlorine, bromine, or hydroxy groups. Also, the benzene ring of the sulfonic acid may have more than one substituent alkyl or hydroxy or haloalkyl group. X is hydrogen, magnesium, calcium, sodium, amine, etc.

Other suitable oil-soluble benzene sulfonic acids are the oil-soluble petroleum sulfonic acids, commonly referred to as "mahogany acids" of about 350 to 750 molecular weight, aryl sulfonic acids, and alkaryl sulfonic acids. Illustrative of such sulfonic acids are dilauryl benzene sulfonic acid, and lauryl cetyl benzene sulfonic acid. Examples of other suitable sulfonic acids are diparaffin wax-substituted phenol sulfonic acids, cetyl chlo-

robenzene sulfonic acids, cetyl-phenol disulfide sulfonic acids, cetyl-phenol monosulfide sulfonic acids, cetoxy capryl benzene sulfonic acids. Other suitable oil-soluble sulfonic acids are described in the art, such as for example U.S. Patent Nos. 2,616,604; 2,626,207; and 2,767,209, and others. A most important consideration in selecting an R group is that the final substituted compound be oil soluble.

The formaldehyde used in the Mannich reaction can be provided by any common formaldehyde yielding reagent. Examples of formaldehyde yielding reagents are formalin, paraformaldehyde, other linear and cyclic formaldehyde polymers, gaseous formaldehyde, and the like.

The amine reactants used in the preparation of the products of the present invention are primary and secondary aliphatic amines containing up to 10 carbon atoms in the aliphatic groups; diamines of the general formula $NH_2(CH_2)_yNH_2$, wherein y is an integer of 2 to about 12; and polyakyene polyamines of the general formula:

wherein A is a divalent alkylene radical of about 2
to about 12 carbon atoms, and X is an integer from about 1
to about 10. Illustrative of such suitable amines are:
methylamine, dibutylamine, cyclohexylamine, propylamine,
decylamine, ethylenediamine, trimethylenediamine, tetramethylenediamine, hexamethylenediamine, diethylenetriamine, triethylenetetramine, tetraethylenepentamine,
tripropylenetetramine, tetrapropylenepentamine, and other
polyalkylene polyamines in which the alkylene group contains up to about 12 carbon atoms. Cyclic polyamines are
also suitable such as piperazine and aminoethyl piperazine, etc.

As mentioned earlier, infrared spectroscopy can be used to measure the completeness of the reaction used to



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produce the Mannich additive. A measurement of the 1680 cm⁻¹ adsorption of the Mannich additive which is about 0.20 per 0.5 mm cell path length indicates complete reaction and best additive properties, as determined by engine test values.

In greater detail, the Mannich reaction is preferably carried out with an amine, a formaldehyde-yielding reagent, a copolymer oxidized in the presence or absence of sulfonic acid compound, and, if desired, an oil soluble sulfonic catalyst in an amount of about 0.01 to 40.0 wt. percent sulfonic catalyst based on the neat polymer. A wide variety of such sulfonic acid compounds operate to catalyze the reaction. The functional group of the oil soluble sulfonic acid which provides the important catalytic properties is the sulfonic acid group.

The following illustrates a preferred method of conducting the Mannich condensation reaction with an oxidized polymer and sulfonic acid compound catalyst. One hundred parts of the oxidized copolymer in 1350 parts of SAE 5W mineral oil diluent was heated to 360°F under a nitrogen blanket. Three parts of solid paraformaldehyde, 4.7 parts of molten hexamethylenediamine and 6.0 parts of an alkyl benzene sulfonic acid having a molecular weight of about 600 in a 39.0% by weight oil solution, were simultaneously added to the stirred reaction mixture at a temperature of 360°F under a nitrogen blanket. The reaction was continued for 2 hours liberating water until complete. The mixture was stripped with nitrogen at 360°F to remove water and other volatile byproducts. After filtration, the mixture was clear.

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The Mannich reaction is believed to occur between the active acidic protons on carbon atoms, alpha to the carbonyl functions produced during the oxidation. Secondary reactions occur between the active reactants, carbonyl groups, and Mannich nitrogen atoms producing many varied crosslinked and animated compounds. The active acidic

protons react with formaldehyde and the amine. This introduces a detergent dispersant function in the polymer viscosity index improver additive.

The Mannich condensation reaction of the oxidized copolymers can be carried out in the presence of up to about 40 wt. percent, preferably from about 0.10 wt. percent to about 2 wt. percent based on the polymer of an oil soluble sulfonic acid compound. A wide variety of such oil soluble sulfonic acids operate to increase the dispersancy detergent effect of the Mannich sulfonic acid copolymer product and the reaction rate producing the additive.

Preferably the sulfonic acid compound is not added prior to the amine. Sulfonic acid added to the oil-oxidized polymer prior to the amine rapidly decomposes, darkening the oil. The sulfonic acid when added after the amine, reacts with the amine. The acid is neutralized and stabilized preventing decomposition of the acid.

The chemical composition of the final reaction prod-20 uct of the oxidized Mannich condensate of the oxidized polymer, the amine and the formaldehyde yielding reagent cannot be characterized with precise chemical formulas. The oxidation of the polymer produces predominantly carbonyl groups, although a minor amount of aldehyde, acid and perhaps ester may also be present in the polymer chain. In view of the complex nature of the final oxidized reaction product, the precise composition, reaction sites, and final structure of such product cannot be defined by a conventional chemical structure, but rather must be 30 defined purely through method of preparation and product properties. Chemical reactants which are added at different steps in the production beginning with the polymerization of the copolymer and ending with the Mannich condensation reaction, produce useful compounds when added 35 to the reaction at different steps. The reaction sites of the various chemical additives vary with the step in which the various chemical reactants are added. Therefore, a

reactant added during the polymerization will produce unique effects on a chemical and physical properties of the polymer. Reactants which are added during the oxidation of the polymer and during the Mannich condensation reaction will produce different, but unique effects. West, et al. U.S. Patent No. 4,011,380, claims the use of a sulfonic acid salt to promote oxidation of the copolymer. During the oxidation of the copolymer, the sulfonic acid appears to be chemically altered.

The described reaction products of the present invention are effective dispersant and viscosity index improving additives in lubricant compositions when used in amounts from about 0.1 to 10 percent, based on neat copolvmer.

Suitable lubricating base oils are mineral oils, petroleum oils, synthetic lubricating oils such as those obtained by the polymerization of hydrocarbons, and other well-known synthetic lubricating oils, and lubricating 20 oils of animal or vegetable origin. Concentrates of a suitable oil base containing more than 10 wt. percent, or one or more additives, can be used for blending with the lubricant oils in proportions desired for particular conditions or used to give finished products containing from about 0.1 to about 20% of additives of this invention.

According to the present invention, a Mannich condensation product prepared as described above can be rendered less susceptible to viscosity increase during storage, shipping and handling, by physically blending, i.e., admixing the product with about .1 to about 20 wt.% and preferably about .5 to about 8.0 wt.% (based on copolymer) of a phenolic compound having the general formula:

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where R is alkyl; or hydroxy, chloro or bromo substituted hydrocarbyl; y is an integer from 1 to 5. In some cases the R group can be made by polymerizing C_2 - C_6 olefins to a molecular weight in the range of about 80 to about 100,000, preferably about 80 to 1,000 and then attaching said group to a benzene ring by well known alkylation techniques. R can be a hydrocarbyl group such as methyl ethyl, propyl, isopropyl, butyl, isobutyl, t-butyl, amyl, isoamyl, t-amyl, isomers of hexyl, heptyl, nonyl, decyl, undecyl, dodecyl and other C_{13} - C_{20} isomers and the like, having a molecular weight from about 15 to 1,000.

R can be any hydrocarbon or substituted hydrocarbon which results in an oil soluble phenol or salt thereof. R can be an intermediate molecular weight hydrocarbyl such as a C_{15} - C_{100} of polybutene or polypropylene polymer, a high molecular weight hydrocarbyl such as polyolefin having a number average molecular weight about 15 to 100,000, preferably about 200 to 10,000 and others. R can be substituted with groups such as chlorine, bromine, hydroxy, or other groups.

The manner of admixing the phenol and the Mannich reaction product is not critical. Any conventional mixing or blending procedure which achieves thorough blending is suitable. Preferably, such blending can be carried out at a temperature of about 150°F to about 300°F. At temperatures below 150°F mixing becomes difficult due to the viscosity of the polymeric Mannich product. Temperatures greater than about 300°F can break down the Mannich product. A preferred phenol for use in the present invention is dodecylphenol. Preferably, about .5 to about 8.0 wt. percent (based on copolymer) of the dodecylphenol is mixed with the Mannich product for about 1-3 hours at about 200°F to facilitate mixing.



is dodecylphenol. Dodecylphenol is admixed with the Mannich product in an amount within the range of 0.1 to 20 wt% based on the weight of the polymer. Preferably, about .5 to about 8.0wt. percent (based on copolymer) of the dodecylphenol is mixed with the Mannich product for about 1-3 hours at about 200°F to facilitate mixing.

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EXAMPLE I

Oxidation of the Copolymer

An oxidized copolymer ("Sample I") was obtained as follows: 500 grams of an ethylene propylene copolymer containing about 40 mole% propylene having a molecular weight of about 60,000 was dissolved in 4,500 grams of 100N process oil at 250° to 320°F with stirring under nitrogen in a flask fitted with a stirrer and means to sparge a 50/50 mixture of air and nitrogen through the 10 contents. After 10 grams of an overbased magnesium polypropylbenzene sulfonic acid color inhibitor, having a molecular weight of about 600, was added to the mixture and stirred overnight, 10 grams of polypropylbenzene sulfonic acid oxidation catalyst was added. The oxidative 15 degradation was then begun by heating to 350-400°F and blowing nitrogen and air through the reaction media, each at 1,600 cc/min, and stirring at 325 rpm. After approximately 3-5 hours, the viscosity was reduced from approximately 16,000 cSt at 210°F to about 320 cSt. 20

EXAMPLE II

Oxidation of the Copolymer

An oxidized copolymer (Sample II) was obtained in accordance with the procedures described in Example I above except the copolymer was oxidized to a final viscosity of 270 cSt.

EXAMPLE III Mannich Reaction

Mannich condensation products from the oxidized

30 polymers (Samples I and II) were prepared by adding slowly to the copolymer with stirring at 360°F, 19 grams of propylbenzene sulfonic acid catalyst, 15 grams of hexamethylene diamine, and 25 grams of a 37% aqueous solution of formaldehyde. After the addition of the reagents, the reaction was stirred one hour at 360°F and then stripped with nitrogen for one hour. The final viscosity of the Mannich product from Sample I had a final viscosity of 450

centistokes and the product from Sample II had a final viscosity of 376 centistokes.

EXAMPLE IV

Addition of Alkylphenol

Samples I and II Mannich products obtained in Example III were individually physically blended with .25 wt % dodecylphenol as follows: 1,000 grams of the Mannich sample was charged into a flask and heated under nitrogen sparge to 200°F. 2.5 grams of dodecylphenol were added when the heated Mannich sample reached 150°F. The mixture was stirred at 200°F for 2 hours.

TABLE I

Effect of Adding Dodecylphenol to Mannich Dispersant/VI Improver in Terms of Reducing Increase in Viscosity During Storage

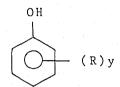
ASTM D-445 was used to measure the difference in kinematic viscosity change (measured at 100°C after one week of storage at 200°F in air) observed for Mannich Samples I and II without dodecylphenol and the same samples with 0.25 wt.% dodecylphenol.

25				M	annich			
	Dodecylphenol (wt.%)				ample	Viscosity Change,		cSt
		0.0			II		+112	
		0.0			I		+117	
30		0.25			II		+64	
		0.25			I		+61	

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The claims defining the invention are as follows:

An improved dispersant and viscosity index improving suitable for use as Mannich composition a having reduced susceptibility viscosity additive to consisting essentially of increase during storage, admixing (a) Mannich physical blend prepared by condensation product obtained from the Mannich reaction of an oxidized polymer, an amine and a formaldehyde yielding reagent and (b) from 0.1 to 20 wt% of a phenolic compound having the formula represented by:



wherein R is any hydrocarbyl or hydroxy-, chloro-, or bromo-substituted hydrocarbyl group which results in an oil soluble phenol or salt thereof and y is an integer from 1-5, said R group having a molecular weight of 15 to 100,000, and said improved composition being essentially free of other lubricant additive compositions.

- 2. The composition of claim 1, wherein R is selected from the group consisting of methyl, ethyl, propyl, isopropyl, butyl, isobutyl, t-butyl, amyl, isoamyl, t-amyl, isomers of hexyl, heptyl, nonyl, decyl, undecyl, dodecyl, and C_{13} C_{20} isomers.
- 3. The composition of claim 2, wherein R is dodecyl.
- 4. The composition of claim 3, wherein the dodecyl-phenol is admixed with the Mannich product in an amount within the range of .1 to 20 wt% based on the weight of the polymer.
- 5. A method for reducing the tendency of a dispersant and viscosity index improving Mannich condensation product to increase in viscosity during storage, which comprises admixing from 0.1 to 20 wt% of a phenolic compound with a dispersant and viscosity index improving Mannich condensation product obtained from the Mannich reaction of an oxidized olefin polymer, an amine and a formaldehyde

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yielding reagent wherein the phenolic compound has a formula represented by: $_{\mathrm{OH}}$

wherein R is any hydrocarbyl or hydroxy-, chloro-, or bromo-substituted hydrocarbyl group which results in an oil soluble phenol or salt thereof and y is an integer from 1-5, said R group having a molecular weight of 15 to 100,000, said admixture being essentially free of other lubricant additives.

- 6. The method of claim 5, wherein the phenolic compound is admixed with the Mannich condensation product in an amount within the range of .1 to 20 wt% based on the weight of the polymer.
- 7. The method of either one of claims 5 or 6, wherein R is selected from the group consisting of methyl, ethyl, propyl, isopropyl, butyl, isobutyl, t-butyl, amyl, isoamyl, t-amyl, isomers of hexyl, heptyl, nonyl, decyl, undecyl, dodecyl, and C_{13} C_{20} isomers.
 - 8. The method of claim 7, wherein R is dodecyl.
 - 9. The method of claim 8, wherein the dodecylphenol is admixed with the Mannich product in an amount within the range of .1 to 20 wt% based on the weight of the polymer.
 - 10 A composition according to claim 1, substantially as hereinbefore described with reference to example IV.
- 11. A method according to claim 5, substantially as 30 hereinbefore described with reference to example IV.

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