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(54) Title : METHOD FOR PREPARING AQUEOUS SUSPENSIONS OF MINERAL MATERIALS USING AMINES IN COMBINATION WITH VINYL CARBOXYLIC POLYMERS

(54) Titre : PROCEDE DE PREPARATION DE SUSPENSIONS AQUEUSES DE MATERIES MINERALES AU MOYEN D'AMINES EN COMBINAISON AVEC DES POLYMERES VINYL-CARBOXYLIQUES

(57) Abstract : The invention relates to the preparation of an aqueous suspension of mineral material by means of dispersion and/or grinding in the presence of at least one amine and one vinyl carboxylic polymer, in which the amine makes it possible to reduce the amount of polymer. The invention also relates to the use of the suspension obtained.

(57) Abrégé : L'invention concerne la préparation d'une suspension aqueuse de matière minérale par dispersion et/ou broyage en présence d'au moins une amine et d'un polymère vinyl- carboxylique, l'amine permettant de réduire la quantité dudit polymère ainsi que l'utilisation de la suspension obtenue.

METHOD FOR PREPARING AQUEOUS SUSPENSIONS USING MINERAL AMINES IN COMBINATION WITH VINYL-CARBOXYLIC POLYMER

5 The present invention relates to agents used to disperse or to assist in the grinding of minerals in humid conditions.

It allows the expert to minimize the amount of vinyl-carboxylic polymers, commonly used in these operations, without altering the stability and the dry extract of aqueous suspensions of mineral matter thus manufactured. This invention is based on the 10 implementation of amines in combination with the said vinyl-carboxylic polymers. Surprisingly and advantageously, we manage to reduce the amount of polymer vinyl carboxylic implemented, while maintaining the above properties to a level at least equivalent to that obtained without the addition of amines under the conditions specified by the present invention .

15

The mineral industry is a major consumer of chemicals. These are used in various steps of conversion / modification / preparation to which mineral substances are subjected. Thus, in the case of natural or synthetic calcium carbonate, the person skilled in the art performs many operations referred to as "grinding" (reduction of particle size) in a dry 20 or more frequently a moist medium, or "dispersion" (suspension of particles in a liquid).

These two operations are rendered easier by the use of grinding aid agents and dispersants respectively. The role of grinding agents is to minimize the yield point of the suspension during the grinding operation so as to increase the productivity of the grind 25 mill. In this way the mechanical action of attrition and fragmentation of the particles is facilitated. As to the dispersants, they help maintain the viscosity of a suspension within acceptable ranges as the mineral substances are introduced. This allows an increase in the solids content while retaining a viscosity level that is low enough to handle the suspension and store it without the risk of sedimentation.

30

The prior art is particularly rich with regard to such additives. For many years, we know that the homopolymers of acrylic acid are effective agents to assist in the dispersion and wet grinding of calcium carbonate. For reference, reference may be made to documents FR 2539137 A1, FR 2683536 A1, FR 2683537 A1, FR 2683538 A1, FR 2683539 A1

and FR 2802830 A1, FR 2818165 A1, which illustrate many variations of these homopolymers, according to their molecular weight and their neutralization.

For the same type of application, it is also interesting to copolymerize acrylic acid with

5 another carboxylic monomer such as methacrylic acid or maleic acid (see on this EP 0850 685 A1 and FR 2903618 A1) and / or with other ethylenically unsaturated monomer without carboxylic function such as an ester (meth)acrylic: the latter variant is described in the documents cited in the preceding paragraph.

10 It means, in terms of legislation and environmental requirements, to reduce the amount of polymer used is a priority for the art, provided it can accommodate a level of performance equivalent to that obtained so far. Of these performances, it especially emphasizes the stability of aqueous suspensions made, as determined by Brookfield TM viscosity measurements at different times, and the final solids content expressed in % by

15 dry weight of mineral matter relative to the total weight of said suspensions.

In this regard, the document FR 2894846 A1 teaches the implementation of fluorinated compounds with polyacrylates of the prior art, thereby reducing their dose in processes of dispersion and grinding of mineral matter. However, fluorinated compounds remain

20 scarce and expensive products, which in turn could have a negative impact on the environment.

We also know that reducing the polydispersity index of acrylic polymers gives them the properties of dispersion and grinding aid improved. To do this, one approach is to

25 isolate, for a given polymer, the chains of a certain molecular weight by separation techniques, static or dynamic, in the presence of solvents, as described in EP 0499267 A1. Another way is based on the implementation of the "controlled" radical polymerization (CRP). This term refers to synthesis techniques based on the use of specific chain transfer agents such as xanthate or trithiocarbonate (see EP 1529065 A1

30 and EP 1 377 615A1).

By reducing the polydispersity index of acrylic polymers produced, it increases their ability to disperse or to facilitate the grinding of mineral matter in water. This is

described in the documents "Dispersion of calcite by poly (sodium acrylate) Prepared by Reversible Addition-Fragmentation chain Transfer (RAFT) polymerization" (Polymer (2005), 46 (19), pp. 8565-8572) and "Synthesis and Characterization of Poly (acrylic acid) Produced by RAFT Polymerization. Application as a Very Efficient 5 Dispersant of CaCO₃, Kaolin, and TiO₂" (Macromolecules (2003), 36 (9), pp. 3066-3077).

However, recent solutions based on separation techniques or CRP, are sometimes difficult to implement: they require special facilities which do not necessarily have any 10 industrial unit. Finally, French Patent Application FR 2 940 141 relates to the neutralization of polyacrylates by lithium hydroxide, which can reduce the amount of polymer to disperse and / or facilitate the grinding in water of calcium carbonate. However, lithium hydroxide, which is also the subject of the patent application WO 2010/063757, remains an extremely expensive compound, which does pose serious 15 environmental problems (see the provisions on the recycling of this compound).

To propose a simple solution to improve the performance of the prior art polyacrylates as dispersants and grinding aid of mineral matter in an aqueous medium, as mentioned, making it possible to decrease the amount to a level equivalent performance, 20 satisfactorily, is so far an unsolved problem.

Continuing his research in this area, the Applicant has succeeded in developing a method for producing an aqueous suspension of mineral matter by dispersion and / or grinding in the presence of at least one amine and at least one vinyl-carboxylic polymer, 25 as an agent to reduce the amount of the said polymer, the latter being completely neutralized by an agent other than the amine.

So totally unexpected, the combination of the amine and vinyl-carboxylic polymer allows to disperse and / or facilitate the grinding in an aqueous medium of a mineral, 30 more effective than the acrylic polymer used without the amine. We prove that for a level of performance at least equivalent (in terms of dry extract and Brookfield™ viscosity measured at 10 rounds / minute, for a given particle size) we are able, according to the invention, to reduce the amount of vinyl-carboxylic polymer used.

An example of amine implementation according to the invention is the AMP (2-amino-2-methyl-1-propanol, CAS # 124-68-5). Furthermore, according to a preferred embodiment of the invention, the amines have implemented the specific formula (I) which will be explained below. We then show that they are more efficient than the AMP

5 to improve the effectiveness of the dispersant according to the parameters mentioned above. It also indicates that the amines of formula (I) are already known, such as agents to develop the colour strength of a painting (see WO 2009 / 087 330 A1).

In the prior art, the AMP has been implemented with an acrylic polymer to disperse a

10 mineral matter. Reference may be made to US 4370171 A1 which teaches a combination of some alkanolamines with acrylic polymers to disperse calcium carbonate. According to Example 1 of this document, we can see that the combination claimed is in fact to premix non-neutralized acrylic dispersant with an alkanolamine: in this sense, the dispersant acid is neutralized by the alkanolamine. This is not the case of

15 our invention wherein the acrylic polymer is completely neutralized by an agent different from the amine.

Moreover, nothing in US 4370171 A1 suggests that the alkanolamines described would reduce the amount of acrylic polymer, without affecting the performance of the

20 dispersant system. In addition, the mass ratio alkanolamine:dispersant is between 0.5:1 and 1.5:1 in this document: this does not describe or suggest the preferred ratio of our invention which is between 0.05:1 and 0.35 to 1. Finally, according to another preferred embodiment of our invention not disclosed or suggested in the prior art, the compounds of formula (I) lead to the performance of particular interest, in terms of solids content

25 and rheology of aqueous suspensions made.

Also, a first object of the present invention is the method of preparing an aqueous suspension of mineral matter comprising the steps:

- a) Make available at least one mineral matter,
- 30 b) Preparing an aqueous suspension comprising at least the mineral from step a),
- c) grinding the mineral matter from the aqueous suspension of step b),

d) and possibly to select and / or concentrate the aqueous suspension of step c) before dispersing the concentrate obtained
characterized in that we add at least one amine and one vinyl-carboxylic polymer completely neutralized by a neutralizing agent of a different amine between steps a) and
5 b) and / or c) or during step c) or after step c) during or after the dispersion of the concentrate obtained.

"Preparing an aqueous suspension comprising at least the mineral matter" means in this patent application "to form an aqueous suspension" by the addition of the mineral in
10 water stirred with or without the addition of dispersants until obtain a dry extract expressed as a percentage by dry weight of mineral matter relative to the total weight of the suspension, between 10% and 82%.

"Select" means in this patent application "to remove coarse particles having a particle size above 45 microns" by any means known in the art, including the implementation of
15 sieve or pickers.

"Focus" means in this patent application "to increase the content of dry mineral matter from the aqueous suspension obtained in step c)" so that the concentrate obtained in the
20 context of this patent application is recognized by the art as the result of concentration means known in the prior art, such as mechanical concentration, for example by the implementation of centrifuge or filter press or press-tube or combinations thereof, or as thermal concentration, such as evaporation or a combination of mechanical and thermal concentration. The concentrate thus obtained is also known by the synonyms of "cake"
25 or "filter cake".

This process is characterized in that the weight ratio amine:v vinyl-carboxylic polymer is between 0.05:1 and 0.35 to 1, preferably between 0.10:1 and 0.30:1.

30 In a first variant this method is characterized in that the amine is selected from dimethylamine, monoethanolamine, diethanolamine, triethanolamine, N-methylethanolamine, 2-amino-2-methyl-1-propanol, triisopropanolamine,

2,3,4,6,7,8,9,10-octahydropyrimido[1,2-a]azepine (DBU; CAS No. 6674-22-2), the 2,2-diazabicyclo [2.2.2] octane (DABCO; CAS No. 280-57-9).

In a second preferred variant, the process is also characterized in that the amine has the
5 formula (I):



with R_1 , R_2 , R_3 identical or different, chosen from:

- a linear or branched alkyl or oxyalkyl radical having from 1 to 12 carbon atoms,
- 10 - a cycloalkyl radical having from 3 to 12 carbon atoms,
- a linear hydroxyl alkyl having from 1 to 6 carbon atoms,

provided that:

- at the most one group R_2 or R_3 is hydrogen,
- at least one of R_1 , R_2 , R_3 groups contains an OH group,
- 15 - at least one of R_1 , R_2 , R_3 includes at least one branch in position α to the nitrogen atom.

In this variant, this process is characterized in that in formula (I), R_1 is hydrogen, R_2 and R_3 are identical or different, chosen from:

- 20 - a linear or branched alkyl or oxyalkyl radical or branched radical having from 1 to 12 carbon atoms,
- a cycloalkyl radical having from 3 to 12 carbon atoms,
- a linear hydroxyl alkyl radical having from 1 to 6 carbon atoms,

provided that:

- 25 - at the most one group of R_2 or R_3 contains an OH group,
- at least one of R_2 or R_3 group includes at least one branch in position α to the nitrogen atom.

In this variant, this process is also characterized in that in formula (I), each alkyl or
30 cycloalkyl or oxyalkyl radical contains from 3 to 10, preferably from 3 to 8 carbon atoms.

In this variant, this process is also characterized in that, in formula (I), one or more radicals carrying the OH group has 2 or 3, preferably 2 carbon atoms.

In this variant, this process is also characterized in that in formula (I), R₁ is hydrogen, R₂ and R₃ are identical or different, chosen from:

- a linear or branched alkyl or oxyalkyl radical or having from 3 to 8 carbon atoms,
- 5 - a cycloalkyl radical having from 6 to 10 carbon atoms,
- a linear hydroxyl alkyl radical having from 2 to 3, preferably 2 carbon atoms,

provided that:

- at least one of R₂ or R₃ group contains an OH group,
- at least one of R₂ or R₃ group includes at least one branch in position α to the nitrogen atom.

In this variant, this process is also characterized in that the amine is selected from:

- N-(1-methylpropyl)-N-(2-hydroxyethylamine)
- N-(1,3-dimethylbutyl)-N-(2-hydroxyethylamine)
- 15 - N-(1-ethyl-3-methylpentyl)-N-(2-hydroxyethylamine)
- N-(3,3', 5-trimethylcyclohexyl)-N-(2-hydroxyethylamine)
- N-(4-hydroxycyclohexyl)-N-(2-hydroxyethylamine).

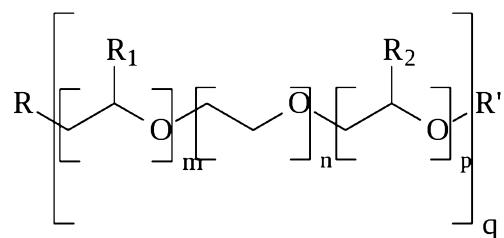
Other amines can also be implemented. This will include heavy polyamines such as piperazine substituted or unsubstituted, amino ethyl piperazine substituted or unsubstituted, amino ethyl ethanol amine, polyether amines, primary amines with polyethylene and / or polypropylene glycol, ethylene amines such as the 2 - (diethylamino) ethyl amine, 2 - (diisopropylamino) ethyl amine, or the pentamethyldiethylenetriamine or also N-(2-aminoethyl) ethanol amine, propylene amines such as N3-amine (3 - (2-aminoethylamino) propylamine, 1,3 - diaminopropane, morpholines substituted such as N-ethylmorpholine, N-methylmorpholine. It may also include products marketed under the brand Alpamine TM by the Arkema Group, particularly the Alpamine TM N72 .

The molecular weight of the polymers used is not critical, provided it is not too high in which case, the polymer acts as a thickener in the community. It may be approximately 300 000 g/mol the maximum value of this molecular weight. In addition, the expert knows how to regulate and adjust the molecular weight; it may particularly be made reference to documents cited at the beginning of the application for different acrylic polymers used to facilitate the grinding or dispersing in water a mineral matter.

This process is also characterized in that the vinyl-carboxylic polymer is completely neutralized by at least one neutralizing agent selected from the hydroxides and / or oxides of calcium, magnesium, or from sodium, potassium, lithium hydroxides and mixtures thereof.

5 This process is further characterized in that said vinyl-carboxylic polymer is a homopolymer of acrylic acid or a copolymer of acrylic acid with another monomer.

This process is also characterized in that, for the copolymer of acrylic acid with another monomer, such another monomer is selected from methacrylic acid, maleic anhydride, 10 2-acrylamido-2-methyl propane sulfonic acid, phosphoric esters of (meth) acrylates of alkylene glycol and non-ionic monomers of formula (II):



15 where m, n, p and q are integers and m, n, p are less than 150, q is greater than 0 and at least one integer among m, n and p is not zero, R is a radical with a function polymerizable unsaturated, R₁ and R₂ are identical or different and represent hydrogen atoms or alkyl groups, R' represents hydrogen or a hydrocarbon radical having 1 to 40 carbon atoms, or an ionic group or ionizable.

20

This process is further characterized in that said aqueous suspension after dispersion and / or grinding, has a solids content expressed as a percentage by dry weight of mineral matter relative to its total weight, between 10% and 82%, preferably between 50 % and 81%, most preferably between 65% and 78%.

25

This process is also characterized in that said aqueous slurry has a content by dry weight of acrylic polymer, compared to the total dry weight of mineral matter, between 0.01% and 5.00%, preferably between 0.01% and 2.00% and most preferably between 0.05% and 1.00%.

30

This process is further characterized in that the mineral matter is selected from calcium carbonate, synthetic or precipitated, talc, kaolin, and mixtures thereof, preferably from

natural, synthetic or precipitated calcium carbonate and mixtures thereof, and is preferably a natural calcium carbonate.

This natural calcium carbonate is preferably selected from limestone, marble, calcite,
5 chalk, dolomite and mixtures thereof.

The following examples will illustrate the invention without limiting its scope.

EXAMPLES

All particle size distributions and diameters indicated are determined with a Sedigraph 5100 TM, marketed by Micromeritics TM.

- 5 In all tests, ppm of dry products is indicated by the dry weight of mineral matter used.

Example 1

This example describes the grinding of calcium carbonate (calcite from Orgon, France)

- 10 in water, for implementation during the grinding stage of a homopolymer of acrylic acid, alone or in combination with certain amines.

The grinding is performed on a laboratory device, Dyno Mill type, KDL TM type, the volume of the grinding chamber being 1.4 liters, and the grinding body is made up of 2500 grams of corundum balls with a diameter between 0.6 and 1 mm.

- 15 In practice, we first introduced the acrylic polymer, then the amine, and then we proceed with the grinding operation.

In addition, the grinding is carried out using techniques well known to those skilled in the art, and in particular described in FR 2539137 A1, FR 2683536 A1, FR 2683537 A1, FR 2683538 A1, FR 2683539 A1 and FR 2802830 A1 and FR 2818165 A1.

20

Test No. 1-a

This test illustrates the prior art and implements 3500 ppm of a homopolymer of acrylic acid, in which 70 mol% of carboxylic sites are neutralized by the sodium ion and 30% calcium ion, and molecular weight as determined by GPC equal to 5500 g/mol.

25

Test No. 1-b

This test illustrates the prior art and implements 3500 ppm of a homopolymer of acrylic acid, in which all carboxylic sites are neutralized by an amine which is 2-amino-2-methyl-1-propanol, and with a molecular weight as determined by GPC equal to 5500

g/mol. This test illustrates the prior art so as described in US 4370171 A1 already discussed earlier, when the dispersant is first neutralized with an alkanolamine.

Test No. 2

5 This test illustrates the invention and implements 3300 ppm of a homopolymer of acrylic acid, in which 70 mol% of carboxylic sites are neutralized by the sodium ion and 30% by the calcium ion, and with a molecular weight as determined by GPC equal to 15 5500 g/mol, in combination with 800 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine).

10

Test No. 3

This test illustrates the invention and implements 3150 ppm of a homopolymer of acrylic acid, in which 70 mol% of carboxylic sites are neutralized by the sodium ion and 30% by the calcium ion, and with a molecular weight as determined by GPC equal to 15 5500 g/mol, in combination with 800 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine).

For each test No. 1-3, measurements of solids content (SC), the percentage by weight of particles having a diameter less than 2 microns (% <2 microns) and Brookfield TM 20 viscosities at 25 ° C and 10 revolutions / minute at t = 0 (BK10 t0) and at t = 8 days after shaking (BK10 t8) are shown in Table 1.

25

Test No	1-a	1-b	2	3
Prior Art INvention	PA	PA	IN	IN
Dispersant (ppm)	3500	3500	3300	3150
Amine (ppm)	0	0	800	800
SC (%)	78,3	78,3	78,4	78,5
% < 2 µm	59	59	60	59,5
Bk10 t0 (mPa.s)	180	180	200	200
Bk10 t8 (mPa.s)	200	195	180	190

Table 1

These results demonstrate that the addition of one amine reduces the amount of acrylic
5 dispersant used, for values of Brookfield TM viscosities comparable and stable over time.

Example 2

This example describes the grinding of natural calcium carbonate (calcite from Orgon,
France) in water in the presence of a homopolymer of acrylic acid and optionally an
10 amine.

The grinding is carried out under the same conditions as those described in the previous
example, except in Test No. 8, where the amine is introduced into the suspension after
grinding.

15 Test No. 4

This test illustrates the prior art and implements 4500 ppm of a homopolymer of acrylic
acid, completely neutralized by the sodium ion, and with a molecular weight as
determined by GPC equal to 5500 g/mol.

20 Test No. 5

This test illustrates the invention and implements 4500 ppm of a homopolymer of
acrylic acid, completely neutralized by the sodium ion, and with a molecular weight as

determined by GPC equal to 5500 g/mol, in combination with 800 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine).

Test No. 6

5 The test illustrates the invention and implements 4500 ppm of a homopolymer of acrylic acid, completely neutralized by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol in combination with 800 ppm of 2-amino-2-methyl-1-propanol (AMP).

10 Test No. 7

This test illustrates the invention and implements 4000 ppm of a homopolymer of acrylic acid, completely neutralized by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine).

15

Test No. 8

This test illustrates the invention and implements during the grinding step 4500 ppm of a homopolymer of acrylic acid, completely neutralized by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol. 800 ppm of an amine of
20 formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine) were then introduced into the suspension after grinding.

For each test No. 4-8, measurements of solids content (SC), the percentage by weight of particles having a diameter less than 2 microns (% <2 microns) and Brookfield TM
25 viscosities at 25 ° C and 10 revolutions / minute at t = 0 (BK10 t0) and at t = 8 days after shaking (BK10 t8) are shown in Table 2.

Test No	4	5	6	7	8
Prior Art INvention	PA	IN	IN	IN	IN
Dispersant (ppm)	4500	4500	4500	4000	4500
Amine (ppm)	0	800	800	800	800
SC (%)	76,0	76,1	76,2	76,2	76,2
% < 2 µm	88,3	88,4	88,4	88,4	88,4
Bk10 t0 (mPa.s)	1570	770	770	800	790
Bk10 t8 (mPa.s)	2940	1470	2010	1980	1780

Table 2

5 Results by tests No. 5, 6 and 8 compared with those obtained by test No. 4, demonstrate that the addition of one amine reduces the value of the Brookfield TM viscosities for the same dose of acrylic dispersant.

Test No. 7 on the other hand shows that it is possible to reduce the amount of acrylic dispersant by adding one amine, while also reducing the value of the Brookfield TM viscosities.

Finally, the amine of formula (I) implemented in test No. 5 provides better results than the AMP according to Test No. 6. This result is confirmed even for a dose of acrylic dispersant lower in the case of the amine of formula (I), according to tests 7 and 8.

15 Example 3

This example describes the grinding of natural calcium carbonate (calcite from Orgon, France) in water, for implementation during the grinding stage of a homopolymer of acrylic acid, alone or in combination with certain amines.

The grinding is carried out under the same conditions as those described in Example 1.

20

Test No. 9

This test illustrates the prior art and implements 6500 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and

50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol.

Test No. 10

5 This test illustrates the invention and implements 6500 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a weight Molecular as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of 2-amino-2-methyl-1-propanol (AMP).

10 Test No. 11

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a weight Molecular as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of 2-amino-2-methyl-1-propanol (AMP).

15

Test No. 12

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal 20 to 5500 g/mol, in combination with 800 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine).

Test No. 13

This test illustrates the invention and implements 5850 ppm of a homopolymer of 25 acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of 2-aminoethanol (ethanolamine, CAS No. 141-43-5).

Test No. 14

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal 5 to 5500 g/mol, in combination with 800 ppm of 2,2'-iminobis-(diethanolamine, CAS Number 111-42-2).

Test No. 15

This test illustrates the invention and implements 5850 ppm of a homopolymer of 10 acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of 2,2',2"-nitrilotris-(triethanolamine, CAS Number 102-71-6).

15 Test No. 16

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 800 ppm 2,3,4,6,7,8,9,10-20 octahydropyrimido[1,2-a]azepine (DBU; CAS Number 6674-22-2).

Test No. 17

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of the carboxylic sites are neutralized by the magnesium 25 ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 800 ppm of 2,2-diazabicyclo[2.2.2]octane (DABCO; CAS No. 280-57-9).

Test No. 18

This test illustrates the invention and implements 5850 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with an amine blend consisting of 400 ppm of an amine of formula (I) which is N-(1-methylpropyl)-N-(2-hydroxyethylamine) and 400 ppm of 2-aminoethanol (ethanolamine, CAS No. 141-43-5).

For tests No. 9 to 18, the measurements of solids content (SC), the percentage by weight of particles having a diameter less than 2 microns (% <2 microns) and Brookfield TM viscosities at 25 ° C and 10 rounds / minute at t = 0 (BK10 t0) and at t = 8 days after shaking (BK10 t8) are shown in Table 3.

Test No.	9	10	11	12	13
Prior art Invention	PA	IN	IN	IN	IN
Dispersant (ppm)	6500	6500	5850	5850	5850
Amine (ppm)	0	800	800	800	800
SC (%)	78,4	80	78,4	78,4	78,3
% < 2 µm	88,3	88,4	88,4	88,4	88,3
Bk10 t0 (mPa.s)	4180	1580	1010	870	3790
Bk10 t8 (mPa.s)	5500	1300	1070	840	3170

Test No.	14	15	16	17	18
Prior Art INvention	IN	IN	IN	IN	IN
Dispersant (ppm)	5850	5850	5850	5850	5850
Amine (ppm)	800	800	800	800	800
SC (%)	78,5	78,4	78,4	78,4	78,4
% < 2 µm	88,4	88,4	88,4	88,4	88,3
Bk10 t0 (mPa.s)	1670	2310	2190	1990	2310
Bk10 t8 (mPa.s)	2550	2440	3040	2080	2100

Table 3

Comparison between Tests 9 and 10 made at an equivalent dose of acrylic polymer, we show that the amine enables us to grind at higher solids content, while decreasing the 5 values of Brookfield TM viscosities.

Tests No. 11 to 18, compared with Test No. 9, show that by adding one amine, we manage to reduce the amount of acrylic polymer, while obtaining the same values of dry Brookfield viscosities less high.

The best results are obtained for the amine of formula (I) according to Test No. 12.

10 Finally, we performed a final test No. 19, outside the invention, illustrating the same dose for the polymer and the amine (such as the US 4370171 A1).

It uses 2900 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 2900

15 ppm of N-(1-methylpropyl)-N-(2-hydroxyethylamine).

It failed to grind solids content to 77%, to obtain 88% by weight of particles having a diameter less than 2 microns, as in other tests: the suspension proved here too viscous.

Example 4

20 In the following tests, a coarse calcium carbonate (calcite from Orgon, France) is suspended in water at 20 wt% concentration. This suspension is stirred to prevent sedimentation, and it flows through a grinder type Dyno-Mill TM with a fixed cylinder and rotating impeller, the grinding body consists of 2,900 grams of corundum balls with a diameter between 0.6 mm and 1 mm.

25 At this stage, the particle size distribution is such that 60 wt.% of these have a diameter less than 1 micron.

Calcium carbonate is then concentrated by any means known to those skilled in the art until the concentration required for the application equal to 67.5% by weight of calcium carbonate.

This produces a filter cake that is essential to re-disperse so that it becomes manipulated and this by implementing an acrylic polymer alone or in combination with an amine.

5 This very special process called "crushing at low concentrations without a dispersing agent and then re-concentration" is particularly described in detail in EP 2044159.

These tests of filter cake dispersion are made in the presence of a copolymer of acrylic acid and maleic anhydride, and optionally an amine.

10 Test No. 20

This dispersion test illustrates the prior art, it implements 3500 ppm of a copolymer of acrylic acid and maleic anhydride, consisting of acrylic acid and maleic anhydride in a molar ratio equal to 1,36:1, with a molecular weight of 19,500 g/mol and in which 100% by mole of the acid functions are neutralized by sodium hydroxide.

15

Test No. 21

This test illustrates the invention and implements 3500 ppm of the same copolymer as in Test 1, in combination with 800 ppm of N-(1-methylpropyl)-N-(2-hydroxyethylamine).

20

Test No. 22

This test illustrates the invention and implements 3200 ppm of the same copolymer as in Test 1, in combination with 800 ppm of N-(1-methylpropyl)-N-(2-hydroxyethylamine).

25

For tests No. 20 to 22, the measurements of solids content (SC) and Brookfield TM viscosities at 25 ° C and 10 revolutions / minute at t = 0 (BK10 t0) and at t = 8 days after shaking (BK10 t8) are shown in Table 4.

Test No.	20	21	22
Prior Art INvention	PA	IN	IN
Dispersant (ppm)	3 500	3 500	3 200
Amine (ppm)	0	800	800
SC (%)	65,3	65,2	65,4
Bk10 t0 (mPa.s)	310	160	200
Bk10 t8 (mPa.s)	600	300	580

Table 4

5 These results demonstrate that the addition of one amine can, at constant dose of acrylic polymer to improve the rheology of the suspension obtained, or decrease the amount of acrylic dispersant while maintaining the Brookfield TM viscosity to a level almost identical.

10 **Example 5**

This example describes the grinding of natural calcium carbonate (calcite from Orgon, France) in water, for implementation during the grinding stage of a homopolymer of acrylic acid, alone or in combination with certain amines. The grinding is carried out under the same conditions as those described in Example 1.

15 Test No. 23

This test illustrates the prior art and implements 12 000 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol.

20 Test No. 24

This test illustrates the invention and implements 10 000 ppm of a homopolymer of acrylic acid, in which 50 mol% of carboxylic sites are neutralized by the magnesium ion and 50% by the sodium ion, and with a molecular weight as determined by GPC equal to 5500 g/mol, in combination with 500 ppm of 2 [(methylpropyl)amino]ethan-1-ol

25 (CAS No. 35265-04-4).

For tests 23 and 24, measurements of solids content (SC), the percentage by weight of particles having a diameter less than 1 micron (% <1 micron) and Brookfield TM viscosities at 25 ° C and 100 rpm / minute (value after 1 min) at t = 0 (BK100 t0) and at t = 14 days before and after shaking (BK100 t14) are shown in Table 5.

5

Test No.	23	24
Prior Art	PA	
INvention		IN
Dispersant (ppm)	12 000	10 000
Amine (ppm)	0	500
SC (%)	76.0	75.5
% < 1 µm	78	78
Bk100 t0 (mPas)	388	311
Bk100 t14 after shaking (mPas)	351	314
Bk100 t14 before shaking (mPas)	573	668

Table 5

These results demonstrate that the addition of one amine reduces the amount of acrylic dispersant (in this example a 20% reduction of the acrylic dispersant), while maintaining the viscosity Brookfield TM at a level almost identical and stable over time.

15

20

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Claims:

1. A process for preparing an aqueous suspension of mineral matter comprising dispersing and/or grinding an aqueous suspension comprising at least one mineral matter in the presence of (i) at least one amine and (ii) a vinyl-carboxylic polymer completely neutralized by a neutralizing agent selected from the group consisting of calcium hydroxide, calcium oxide, magnesium hydroxide, magnesium oxide, sodium hydroxide, potassium hydroxide, lithium hydroxide, and any mixture thereof, wherein the weight ratio of amine:carboxylic-vinyl polymer is between 0.05:1 and 0.35:1.

2. The process according to claim 1, wherein the weight ratio of amine:carboxylic-vinyl polymer is between 0.10:1 and 0.25:1.

3. The process according to claim 1 or claim 2, wherein the amine is selected from group consisting of dimethylamine, monoethanolamine, diethanolamine, triethanolamine, N-methylethanolamine, 2-amino-2-methyl-1-propanol, triisopropanolamine, 2,3,4,6,7,8,9,10-octahydropyrimido [1,2-a] azepine (DBU, CAS No. 6674-22-2), and 2,2-diazabicyclo[2.2.2]octane (DABCO; CAS No. 280-57-9).

4. The process according to claim 1, wherein the amine has the formula (I):



where R_1 , R_2 , R_3 are identical or different, and are chosen from:

- hydrogen,
- a linear or branched alkyl or oxyalkyl radical having 1 to 12 carbon atoms,
- a cycloalkyl radical having from 3 to 12 carbon atoms, or
- a linear hydroxyl alkyl radical having 1 to 6 carbon atoms,

provided that:

- at most one of R_2 or R_3 groups is hydrogen,
- at least one of R_1 , R_2 , R_3 groups contains an OH group, and
- at least one of R_1 , R_2 , R_3 groups includes at least one branch in position α to the nitrogen atom.

5. The process according to claim 4, wherein in formula (I), R_1 is hydrogen, R_2 and R_3 are identical or different, and are chosen from:

- a linear or branched alkyl or oxyalkyl radical having 1 to 12 carbon atoms,
- a cycloalkyl radical having from 3 to 12 carbon atoms, or
- a linear hydroxyl alkyl radical having 1 to 6 carbon atoms,

provided that:

- at most one of R_2 or R_3 groups contains an OH group, and

- at least one of R₂ or R₃ groups includes at least one branch in position α to the nitrogen atom.

6. The process according to claim 4, wherein in formula (I), each alkyl or cycloalkyl or oxyalkyl radical comprises from 3 to 10 carbon atoms.

5 7. The process according to claim 5, wherein in formula (I), each alkyl or cycloalkyl or oxyalkyl radical comprises from 3 to 8 carbon atoms.

8. The process according to claim 4, wherein in formula (I), one or more radicals containing the OH group have 3 carbon atoms.

10 9. The process according to claim 4, wherein in formula (I), one or more radicals containing the OH group have 2 carbon atoms.

10 10. The process according to claim 4, wherein in formula (I), R₁ is hydrogen, R₂ and R₃ are identical or different, and are chosen from:

- a linear or branched alkyl or oxyalkyl radical having from 3 to 8 carbon atoms,

- a cycloalkyl radical having 6 to 10 carbon atoms, or

15 - a linear hydroxyl alkyl radical having from 2 to 3, preferably 2 carbon atoms, provided that:

- at least one of R₂ or R₃ groups contains an OH group, and

- at least one of R₂ or R₃ groups includes at least one branch in position α to the nitrogen atom.

20 11. The process according to claim 4, wherein the amine is selected from the group consisting of:

- N-(1-methylpropyl)-N-(2-hydroxyethylamine),

- N-(1,3-dimethylbutyl)-N-(2-hydroxyethylamine),

- N-(1-ethyl-3-methylpentyl)-N-(2-hydroxyethylamine),

25 - N-(3,3',5-trimethylcyclohexyl)-N-(2-hydroxyethylamine), and

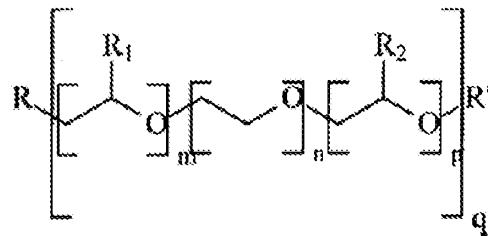
- N-(4-hydroxycyclohexyl)-N-(2-hydroxyethylamine).

12. The process according to any one of claims 1 to 11, wherein the vinyl-carboxylic polymer has carboxylic acid sites that are completely neutralized by (i) sodium ions, (ii) a combination of sodium and calcium ions, or (iii) a combination of magnesium and sodium ions.

30 13. The process according to any one of claims 1 to 11, wherein the vinyl-carboxylic polymer is a homopolymer of acrylic acid or a copolymer of acrylic acid with another monomer.

14. The process according to claim 13, wherein the vinyl-carboxylic polymer is a copolymer of acrylic acid with another monomer selected from methacrylic acid, maleic

anhydride, 2-acrylamido-2-methyl propane sulfonic acid, phosphoric esters of (meth)acrylates of alkylene glycol and non-ionic monomers of formula (II):



5 where m, n, p and q are integers and m, n, p are less than 150, q is greater than 0 and at least one integer m, n and p is not zero, R is a radical with a polymerizable unsaturated function, R₁ and R₂ are identical or different and represent hydrogen atoms or alkyl groups, R' represents hydrogen or a hydrocarbon radical having 1 to 40 carbon atoms, or an ionic group or ionizable.

10 15. The process according to any one of claims 1 to 14, wherein the aqueous suspension of mineral matter has a solids content of between 10% and 82%.

16. The process according to claim 15, wherein the aqueous suspension of mineral matter has a solids content of between 50% and 81%.

15 17. The process according to claim 16, wherein the aqueous suspension of mineral matter has a solids content of between 65% and 78%.

18. The process according to any one of claims 1 to 14, wherein the aqueous suspension of mineral matter has between 0.01% and 5% of vinyl-carboxylic polymer based on dry weight of mineral matter.

19. The process according to claim 18, wherein the aqueous suspension of mineral matter has between 0.01% and 2% of vinyl-carboxylic polymer based on dry weight of mineral matter.

20. The process according to claim 19, wherein the aqueous suspension of mineral matter has between 0.05% and 1% of vinyl-carboxylic polymer based on dry weight of mineral matter.

25 21. The process according to any one of claims 1 to 20, wherein the mineral matter is natural calcium carbonate, precipitated calcium carbonate, talc, kaolin, or any mixture thereof.

22. The process according to claim 21, wherein the mineral matter is natural calcium carbonate.

23. The process according to claim 22, wherein the natural calcium carbonate comprises limestone, marble, calcite, chalk, dolomite, or any mixture thereof.

24. The process according to any one of claims 1 to 23, wherein the aqueous suspension of mineral matter after dispersing and/or grinding is concentrated.

5 25. A filler, paper coating, paint or plastic made from the aqueous suspension of mineral matter obtained from the process of any one of claims 1 to 24.

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