### WORLD INTELLECTUAL PROPERTY ORGANIZATION International Bureau



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT) (51) International Patent Classification 4: (11) International Publication Number: WO 86/ 02393 A1 D21C 3/02 (43) International Publication Date: 24 April 1986 (24.04.86) (21) International Application Number: PCT/SE85/00321 (74) Agent: ILLUM, Leif-Otto; Svenska Cellulosa Aktiebolaget SCA, Kungsgatan 33, S-111 56 Stockholm (SE). (22) International Filing Date: 29 August 1985 (29.08.85) (81) Designated States: AT, AU, BR, DE, FI, JP, NO, US. (31) Priority Application Number: 8405061-6 (32) Priority Date: 10 October 1984 (10.10.84) Published With international search report. (33) Priority Country: (71) Applicant (for all designated States except US): SVENS-KA TRÄFORSKNINGSINSTITUTET [SE/SE]; Drottning Kristinas väg 37 F, 53-69, S-114 28 Stockholm (SE). (72) Inventors; and (75) Inventors/Applicants (for US only): TEDER, Ants [SE/ SE]; Sportvägen 13 A, S-183 40 Täby (SE). OLM, Leelo [SE/SE]; Sjövägen 7, S-133 00 Saltsjöbaden (SE). WIKÉN, Jan-Erik [SE/SE]; Kometvägen 23, VII, S-183 33 Täby (SE).

(54) Title: PROCESS OF MAKING CELLULOSE PULP

## (57) Abstract

A process of manufacturing cellulose pulp from wood by division with sulphite cooking liquor containing additions of sulphide and in the presence of a quinonoide or hydroquinonoide compound. According to the invention, the mole ratio between sulphide and sulphite shall amount to 0,01-0,2, preferably 0,05-0,15, suitably 0,08-0,12.

## FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

			-			
ΑT	Austria	GA	Gabon	MR	Mauritania	
AU	Australia	GB	United Kingdom	MW	Malawi	
BB	Barbados	HU	Hungary	NL	Netherlands .	
BE	Belgium	П	Italy	NO	Norway	
BG	Bulgaria	JP	Japan	RO	Romania	
BR	Brazil	KP	Democratic People's Republic	SD	Sudan	
CF	Central African Republic		of Korea	SE	Sweden	
CG	Congo	KR	Republic of Korea	SN	Senegal	
CH	Switzerland	LI	Liechtenstein	SU	Soviet Union	
CM	Cameroon	LK	Sri Lanka	TD	Chad	
DE	Germany, Federal Republic of	LU	Luxembourg	TG	Togo	
DK	Denmark	MC	Monaco	US	United States of America	
FI	Finland	MG	Madagascar			
ED	Financ	MI.	Mali			

# Frocess of making cellulose pulp

This invention relates to the making of cellulose pulp by processing wood or similar cellulose-containing starting material with alkalic sulphite cooking liquid containing small amounts of sulphide in the presence of anthraquinone or similar quinonoide substances. According to the invention, the cooking liquid consists of sodium sulphite, anthraquinone and small amounts of sulphide. The cooking liquid, in addition, may include sodium hydroxide and sodium carbonate. The process is charachterized in that the mole ratio between sulphide and sulphite is in the range 0,01 - 0,2.

The present invention can be used in existing pulp mills (in sulphite pulp mills on sodium basis as well as in sulphate pulp mills). The amount of evil smelling compounds formed, however, is substantially smaller than at conventional sulphate digestion. The sulphate pulp mill, however, must be provided with (known) equipment for converting sulphide to sulphite. The invention renders it possible to manufacture pulp with good strength, similar to that of sulphate pulp, from different types of wood and in different yield ranges. The pulp, besides, is easy to bleach.

During the last decade, the sulphite process has become attractive again, due to the fact, that the recovery problems have been solved, and that it is now possible to manufacture pulps similar to sulphate.

Previously, two new digestion processes have been developed, viz. neutral sulphite - AQ and, respectively, alkalic sulphite - AQ, for the manufacture of high-yield pulps and pulps for bleaching. The division into neutral

and alkalic sulphite is based mostly on the different digestion chemicals being charged, viz.  $Na_2SO_3$  and  $\mathrm{Na_2^{CO}_3}$  in neutral sulphite, and  $\mathrm{Na_2^{SO}_3}$  and  $\mathrm{NaOH}$  in alkalic sulphite. The pH-intervals (cold pH) for these digestion types, however, overlap. Neutral sulphite digestion normally is carried out at cold pH < 12,5, and alkalic sulphite digestion in the pH-range 10 - 13,5. The greatest advantages of the sulphite - AQ process over the sulphate process are the substantially higher yield -  $\sim 10\%$  for high-yield pulps and  $\sim 7\%$  for fully bleached pulps - and the smaller amounts of evil smelling substances formed. The disadvantages are that, irrespective of the anthraquinone addition, the deliginification proceeds slower, the digesting time at maximum digestion temperature is longer, and a higher digestion chemical addition, compared with the sulphate process, is required for digestion to a certain kappa number. The slightly lower strength does not seem restrictory for the process.

The process according to the present invention shows all the advantages of a sulphite - AQ process. The amount of evil smelling substances assumedly is slightly higher, but still is on a much lower level compared with the amount of evil smelling substances formed at the sulphate process.

The sulphite-sulphide process heretofore has interested a few researchers. Peckham and van Druven investigated 1961 the sulphite process with Na-basis for the entire pH-range. The investigation also included two sulphite-sulphide processes. The results showed that the solving-out of lignin as well as the viscosity and strength of the pulp depended strongly on the composition of the cooking liquid (sulphite-sulphide-alkali). Similar results

were obtained at a later date by Hinrichs in Sv. Papperstidning 73 (1973), No 5:122 and 76 (1973), No 5:182. He was the only researcher who had studied in greater detail the SS-process (for high-yield pulps, kappa number 50). According to Hinrichs, the optimum liquid composition for obtaining the highest possible polymerization degree was 28% Na<sub>2</sub>SO<sub>3</sub> and 12% Na<sub>2</sub>S (all calculated in NaOH on wood) and with MaOH and the Na<sub>2</sub>CO<sub>3</sub>-charge 0%. Hinrichs made his eperiments at high liquid:wood ratios (6:1) and at very high total chemical charges (~10 mol Na/kg wood).

A. Teder and F.Johansson have published in STFI-Kontakt, No 5,1978, that AQ accelerates the solving-out of lignin during an SS-digestion. The pulp was also at this investigation treated with an SS-cooking liquid where the sulphide-sulphite ratio was on a substantially higher level compared with the process described according to the invention.

The present invention relates to a process for the manufacture of chemical pulp where together with anthraquinone small amounts of sodium sulphide are added to the sulphite cooking liquor. Owing to the sulphide addition, the solving-out of lignin increases, and the digesting time at maximum digestion temperature, and therewith also the steam consumption, can be reduced. Furthermore, also the demand on chemicals decreases. An addition of sodium sulphide corresponding to a mole ratio between sulphide and sulphite of the magnitude 0,01-0,2 is sufficient. The necessary sulphide amount can be obtained easily, for example by directing a small amount of green liquor past the apparatus where sodium sulphide is converted to sodium sulphite solution. The amount of evil smelling substances formed at the digestion with the aforesaid cooking liquor is substantially smaller than at conventional sulphate digestion.

The process according to the invention offers advantages over alkalic sulphite with or without anthraquinone in respect of delignification, and over the sulphate digestion in the entire kappa number range in respect of yield, but is especially advantageous at kappa numbers exceeding 40-50. The pulps manufactured with high kappa numbers, however, advantageously can be delignified to lower kappa numbers in an additional delignification step of the type digestion with pure alkali, oxygen gas in alkali, etc.

The invention hereinafter will be called MSS-AQ process, where MSS means mini-sulphite-sulphide digestion, i.e. sulphite-sulphide digestion with low sulphide charges.

In the following some examples of the invention are described.

## Example 1

300 g pine chips was charged into a 2-litre autoclave. The autoclave was evacuated for 30 minutes whereafter the cooking liquor was sucked in. The liquor:wood ratio was 4,5:1. Pressure impregnation with 0,5 MPa N<sub>2</sub>-pressure was carried out for 30 minutes.

The composition of the cooking liquor for MSS-AQ digestion and reference digestion were as follows:

Cooking liquor	Na <sub>2</sub> SO <sub>3</sub>	Na <sub>2</sub> S	NaOH	AQ
Digestion type	as mole	Na/kg wood		% on wood
MSS-AQ	7,36	0,64	_	0,15
Sulphite -AQ	8,00		-	0,15
Conv.sulphate	-	2,0	3,0	-

1

The digesting time until maximum digestion temperature,  $170^{\circ}$ C, was 100 minutes (from  $70^{\circ}$ C).

After completed digestion, the pulps were washed and refined in an Asplund refiner for 30 seconds at  $20^{\circ}\text{C}$ .

The digestion results are shown in the following Table.

Digestion type	Time at 170 <sup>°</sup> C min	Kappa number	Yield %
MSS-AQ	160	46	55,2
Sulphite-AQ	160	92	66,8
Conv. sulphate	80	45	47,5

Example 2
Digestion type as in Example 1.

The cogking a liquor composition was as follows:

Cooking liquor	Na <sub>2</sub> SO <sub>3</sub> mole Na/kg v	Na <sub>2</sub> S	NaOH	AQ % on wood	
Digestion type	more having .	more having wood		, on wood	
MSS-AQ	5,52	0,48	-	0,15	
Sulphite-AQ	6,00	-	-	0,15	
Conv.sulphate		2,0	3,0	-	

The digestion results were as follows:

Digestion type	Time at min	170°C Kappa number	Yield %
MSS-AQ	90	68	61,8
MSS-AQ	100	57 '	59 <b>,</b> 7
Sulphite-AQ	160	99	71,3
Conv. sulphate	65	66	51,6

# Example 3

Digestion type as in Example 1. No anthraquinone was added.

The cooking liquor composition was as follows:

Cooking liquor Digestion type	Na <sub>2</sub> SO <sub>3</sub> mole Na/kg	Na <sub>2</sub> S ; wood	NaOH	AQ % on wood
MSS-AQ	7,0	1,0	-	0,15
Sulphite-AQ	8,0	-	-	0,15
Conv. sulphate	-	2,2	3,4	-

The digestion result was as follows:

Digestion type	Time at 170 <sup>0</sup> C min	Kappa number	Viscosity dm <sup>3</sup> /kg	Yield %
MSS-AQ	160	42	1590	53,5
Sulphite-AQ	160	84	-	68,5
Conv. sulphate	75	46	1256	51,0

The conventional SS-digestions with high sulphide proportions do not yield the above effect - rapid delignification at low alkalinity.

## Example 4

A comparison between MSS-AQ and so-called conventional SS-AQ.

Digestion type as in Example 1.

The cooking liquor composition was as follows:

Cooking liquor Digestion type	Na <sub>2</sub> SO <sub>3</sub> mole	Na <sub>2</sub> S Na/kg wood	AQ % on wood
MSS-AQ	7,0	1,0	0,15
SS-AQ	4,0	4,0	0,15

The digestion result was as follows:

Digestion time	Time at 170 <sup>0</sup> C	Kappa number	Yield %
	min		
MSS-AQ	160	42	53,5
SS-AQ	160	55 <b>,</b> 2	51,7

The invention is not restricted to the Examples described above, but can be varied within the scope of the invention idea.

## Claims

- 1. A process at the manufacture of pulp from wood with sulphite cooking liquor containing additions of sulphide in the presence of a quinonoide or hydroquinonoide compound, for example anthraquinone, benzoquinone, naphthoquinone or 1,4 dihydro 9,10 dehydroxyanthracene, c h a r a c t e r i z e d i n that the mole ratio between sulphide and sulphite, calculated as Na<sub>2</sub>S and, respectively, Na<sub>2</sub>SO<sub>3</sub>, amounts to 0,01 0,2, preferably 0,05 0,15, suitably 0,08 0,12.
- 2. A process as defined in claim 1, c h a r a c t e r i z e d i n that the digestion is terminated before the kappa number 50 has been arrived at.
- 3. A process as defined in claim 1 or 2, c h a r a c t e r i z e d i n that the delignification is continued in a subsequent step, for example with alkali, sulphite cooking liquor or alkali and oxygen gas.
- 4. A process as defined in the claims 1 3, c h a r a c t e r i z e d i n that the quinonoide and, respectively, hydroquinonoide compound is added in an amount of 0,01-0,20%, calculated on the wood amount.

# INTERNATIONAL SEARCH REPORT

International Application No PCT/SE85/00321

I. CLASS	SIFICATION OF SUBJECT MATTER (if several class)	ification symbols apply, indicate all) <sup>6</sup>	
According	to International Patent Classification (IPC) or to both Nat	ional Classification and IPC 4	
D 2.	1 C 3/02		
II. FIELD	S SEARCHED		
01		ntation Searched 7	
Classificati		Classification Symbols	
IPC 4	( = == / - <del>-</del>		
US C	l <u>162</u> :72, 83		ļ
	Documentation Searched other	than Minimum Documentation	
	to the Extent that such Documents	are included in the Fields Searched	
	SE, NO, DK, FI classes as	shava	
	JL, NU, DK, FI Classes as	above	
III. DOCL	MENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of Document, 11 with Indication, where app	propriate, of the relevant passages 12	Relevant to Claim No. 12
X	SE, A, 8306139-0 (YHTYNEET 18 May 1984	PAPERITEHTAAT OY)	1-4
X	STFI-Kontakt, No 5, 1978, kinon påskyndar sulfit-sul		1-4
A	US, A, 4 213 821 (NAPHTALI 22 July 1980	N. VANDERHOEK ET AL)	
Α	US, A, 4 363 700 (I. WADA 14 December 1982	ET AL)	
А	TAPPI, Vol. 53, No 8, Augu "High-Yield Pulping Proces Woods, p. 1451-1457		
	-		
* Specia	I categories of cited documents: 19	"T" later document published after th	international filing data
"A" doc	ument defining the general state of the art which is not	or priority date and not in conflic cited to understand the principle	t with the application but
	sidered to be of particular relevance ier document but published on or after the international	invention	· · · · · · · · · · · · · · · · · · ·
filin	g date	"X" document of particular relevance cannot be considered novel or	e; the claimed invention cannot be considered to
whi	ument which may throw doubts on priority claim(s) or the is cited to establish the publication date of another	involve an inventive step	
cita	tion or other special reason (as specified)	"Y" document of particular relevance cannot be considered to involve a	n inventive step when the
othe	ument referring to an oral disclosure, use, exhibition or er means	document is combined with one of ments, such combination being of	
"P" doc	ument published prior to the international filing date but r than the priority date claimed	in the art.	•
		"4" document member of the same pa	reur remny
	IFICATION		
	Actual Completion of the International Search	Date of Mailing of this International Sea	rch Report
198	5-11-06	400F 44. 1	2
Internation	al Searching Authority	1985 -11- 1	<u> </u>
		Signature of Authorized Officer	Fern I
5 W E	dish Patent Office	Marianne Bratsberg	L.