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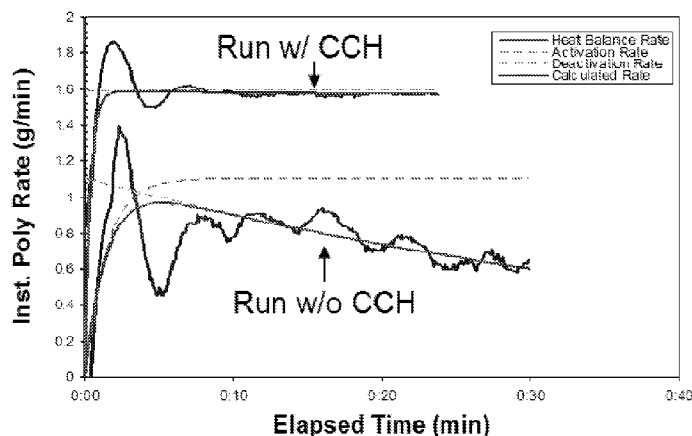


FIGURE 1

(57) Abstract: Processes for producing impact copolymers are provided. Ethylene and at least one copolymer can be polymerized in the presence of one or more catalysts, polypropylene particles, and one or more halocarbon compounds to produce an impact copolymer that includes the polypropylene particles and an ethylene copolymer.

**POLYMERIZATION ACTIVATORS FOR SUPPORTED
ZIEGLER-NATTA CATALYSTS**

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PRIORITY CLAIM

- 5 [0001] This application claims priority to and the benefit of US Provisional Application No. 61/761,375, filed February 6, 2013 and EP 13161995.9 filed April 2, 2013.

FIELD

- [0002] Embodiments provided herein generally relate to processes for making impact copolymers. More particularly, embodiments provided herein relate to processes for making
10 impact copolymers using two or more polymerization stages.

BACKGROUND

- [0003] Impact copolymers (ICP's) are commonly used in a variety of applications where strength and impact resistance are desired, such as molded and extruded automobile parts, household appliances, luggage, and furniture. Propylene based ICP's are typically an intimate
15 mixture of a continuous phase of a crystalline polypropylene polymer and a dispersed rubbery phase of a secondary polymer, *e.g.*, an ethylene copolymer. While these so-called ICP products have been produced by melt compounding the individual polymer components, multi-reactor technology makes it possible to produce them directly. This is accomplished by polymerizing propylene in a first reactor and transferring the polypropylene polymer from the
20 first reactor into a second reactor where the secondary copolymer is produced in the presence of the polypropylene polymer.

- [0004] A variety of polymerization processes can be used to prepare the crystalline polypropylene polymer and the secondary polymer, such as gas phase, slurry, liquid, and/or solution polymerization. It is also quite common to make the constituent polymers in two
25 different polymerization processes, for example, slurry phase for the polymerization of the polypropylene polymer and gas phase for the polymerization of the ethylene copolymer. The composition, composition distribution, amount, molecular weight, and/or molecular weight distribution of the secondary polymer primarily determines the engineering properties of the ICP. Accordingly, control over the secondary polymer is desirable in order to control the
30 properties of the ICP produced via the two stage polymerization process.

- [0005] One problem encountered in a two stage or two step polymerization process that uses gas phase polymerization for the secondary ethylene copolymer is that the catalyst, *e.g.*, titanium catalyst, tends to degrade in activity and/or selectivity toward the polymerization of the secondary polymer. As such, the amount of the secondary polymer made in the second

polymerization stage is typically less than desired. Additionally, degradation of the catalyst's selectivity toward a particular copolymer causes the secondary copolymer to have a range of molecular weights, varying composition, and/or other varying properties that cannot be controlled.

- 5 [0006] There is a need, therefore, for improved polymerization processes for making ICP's having improved catalyst activity and/or selectivity toward the polymerization of the secondary polymer.

SUMMARY

- 10 [0007] Processes for producing impact copolymers are provided. In at least one specific embodiment, the process can include polymerizing ethylene and at least one comonomer in the presence of one or more catalysts, polypropylene particles, and one or more halocarbon compounds to produce an impact copolymer that includes the polypropylene particles and an ethylene copolymer.

- 15 [0008] In at least one specific embodiment, the process for making an impact copolymer can include contacting polypropylene particles having a weight average particle size along the longest cross-sectional length thereof of from 0.05 mm to 5 mm and a pore volume of 5% to 80%, one or more halocarbon compounds, ethylene, and at least one comonomer with one another under conditions sufficient to polymerize the ethylene and the at least one comonomer to produce an impact copolymer comprising the polypropylene particles and an
20 ethylene copolymer.

- [0009] In at least one specific embodiment, the process for making an impact copolymer can include combining propylene with a Ziegler-Natta catalyst or a single site catalyst in a polymerization reactor at conditions sufficient to produce polypropylene particles having a weight average particle size along the longest cross-sectional length thereof of 0.05 mm to 5
25 and a pore volume of 5% to 80%. The polypropylene particles can be combined with a halocarbon compound to produce halocarbon-containing polypropylene particles having at least a portion of the halocarbon compound within the pores of the polypropylene particles. Ethylene and at least one comonomer can be combined with the halocarbon-containing polypropylene particles and the catalyst. At least a portion of the ethylene and at least a
30 portion of the comonomer can be located within the pores of the polypropylene particles. The ethylene and the comonomer can be polymerized within the pores of the polypropylene particles to produce an impact copolymer.

BRIEF DESCRIPTION OF THE DRAWINGS

[0010] Figure 1 is a graphical representation of the catalyst activity during gas phase polymerization of an ethylene-propylene copolymer with the addition of chlorocyclohexane (CCH) versus a comparative case without the addition of chlorocyclohexane.

5 [0011] Figure 2 is a graphical representation of the effect chlorocyclohexane (CCH) had on the ethylene-propylene copolymer content of an impact copolymer over a range of homopolymer melt flow rates in gas phase polymerization.

[0012] Figure 3 is a graphical representation of the effect chlorocyclohexane (CCH) had on the ethylene-copolymer content of an impact copolymer over a range of ethylene mole
10 fractions in a gas phase polymerization reactor.

[0013] Figure 4 is a graphical representation of the effect chlorocyclohexane (CCH) had on the ethylene-copolymer content over a range of homopolymer melt flow rates versus comparative ethylene-copolymers made in the absence of chlorocyclohexane.

[0014] Figure 5 is a graphical representation of the effect halocarbon compounds had on
15 the composition of ethylene-propylene copolymer over a range of ethylene concentrations during gas phase polymerization.

DETAILED DESCRIPTION

[0015] The in-situ polymerization of the impact copolymer can employ any appropriate polymerization catalyst or combination of catalysts capable of polymerizing the monomer
20 component(s) of the polypropylene component and the ethylene copolymer component. For example, the catalyst can be or include one or more Ziegler-Natta and/or one or more single-site, *e.g.*, metallocene, polymerization catalysts. The catalyst(s) can be supported, *e.g.*, for use in heterogeneous catalysis processes, or unsupported, *e.g.*, for use in homogeneous catalysis processes. Preferably, the polypropylene polymer and the ethylene copolymer can
25 be made with a common supported Ziegler-Natta or single-site catalyst.

[0016] It has been surprisingly and unexpectedly discovered that mixing, blending, combining, or otherwise contacting the catalyst and monomer mixture with one or more halocarbon compounds during polymerization increases the catalyst activity and/or produces an impact copolymer having a more uniform copolymer component, *e.g.*, more uniform
30 molecular weight and/or composition, as compared to a copolymer made under the same conditions, but in the absence of the halocarbon compound. Without wishing to be bound by theory, it is believed that the presence of the halocarbon compound(s) during polymerization of the impact copolymer can selectively reactivate catalyst that has become deactivated or at

least less active than its original state. For example, if the catalyst is or includes a Ziegler-Natta catalyst, contacting the catalyst with the halocarbon compound can reverse the reduction that can occur in the transition metal component during polymerization. The reversal in the reduction of the transition metal component can be such that a larger fraction of the reactivated transition metal atoms are of the same chemical identity, which can result in the polymerization of the ethylene copolymer having a more uniform or similar composition and/or molecular weight. It is believed that the halocarbon compound also reacts with excess tri alkyl aluminum that may be present in the vicinity of the catalyst to attenuate the reactivity of the trialkyl aluminum toward the reduction of the Ziegler-Natta catalyst. The halocarbon is believed to slow the reduction of the Ziegler-Natta catalyst and reactivate the Ziegler-Natta catalyst by oxidation caused by the transfer of a halogen to the catalyst.

[0017] Suitable halocarbon compounds can include, but are not limited to, one or more compounds containing a plurality of halogen atoms bonded to a single carbon, one or more activated halogen compounds, one or more acyl halide compounds, one or more allylic halogen compound, one or more benzylic halogen compound, elemental halogens including mixed halogens or any easily reduced source of halogen where the surplus of halogen (typically chlorine) is bound to a single atom or moiety. Exemplary structures of the last kind are ferric chloride, phosphorus pentachloride and trichloro toluene, or any mixture thereof. As used herein, the term "activated halogen compound" refers to the ability of the halogen compound to easily oxidize a reduced early transition metal to a higher oxidation state on simple admixture. Suitable halogen atoms include fluorine, chlorine, bromine, and iodine.

[0018] Suitable compounds containing a plurality of halogen atoms on a single carbon can be represented by the general formula: $CX_1X_2R_1R_2$, where X_1 and X_2 , are each independently selected from fluorine, chlorine, bromine, and iodine, and where R_1 and R_2 are independently selected from fluorine, chlorine, bromine, iodine, hydrogen, oxygen, nitrogen, and a hydrocarbyl group. Illustrative hydrocarbyl groups can include, but are not limited to, alkyl groups, aryl groups, and alkoxy groups. The alkyl groups and/or alkoxy groups can include from 1 to 12 carbon atoms, or from 1 to 10 carbon atoms, or from 1 to 8 carbon atoms, or from 1 to 6 carbon atoms, or from 1 to 4 carbon atoms (preferably the alkyl group or the alkyl of the alkoxy group is one or more of methyl, ethyl, propyl, butyl, pentyl, hexyl, heptyl, octyl, nonyl, decyl, undecyl or dodecyl). The aryl groups can include from 6 to 12 carbon atoms, or from 6 to 10 carbon atoms, or from 6 to 8 carbon atoms. Illustrative

halocarbon compounds containing a plurality of halogen atoms bonded to a single carbon can include, but are not limited to, carbon tetrachloride, chloroform, trichloro toluene, ferric chloride, carbonyl chloride, or any mixture thereof.

[0019] Suitable acyl halide compounds can be represented by the general formula
5 $R\{(CO)X\}_n$, where R is a chemical fragment of valence n (preferably R is a hydrocarbyl group and n is 1, 2, 3, 4, 5 or 6) and X is a halogen, preferably Cl. Preferred R groups may be selected from the group consisting of: substituted alkyls, unsubstituted alkyls, (preferably the alkyls are C1 to C20 alkyls) substituted aromatics (such as substituted phenyl or benzyl groups), and unsubstituted aromatics (such as phenyl or benzyl). Illustrative acyl halide
10 compounds can include, but are not limited to, benzoyl chloride, acetyl chloride, or any mixture thereof.

[0020] The impact copolymer includes one or more polypropylene polymers and one or more ethylene copolymers. The polypropylene polymer and the ethylene copolymer can be made using any one or more polymerization processes capable of polymerizing their
15 respective monomer components. As used herein, the terms "ethylene copolymer," "elastomeric polymer," "ethylene rubber," "elastomer," and "rubber" are used interchangeably and refer to the ethylene copolymer or "secondary copolymer" component of the impact copolymer.

[0021] Illustrative polymerization processes can include, but are not limited to, gas-phase, solution, slurry, high-pressure, or combinations thereof. In at least one example, the
20 polypropylene polymer can be produced via a solution or slurry polymerization process and the ethylene copolymer can be produced via a gas-phase polymerization process. More preferably, the impact copolymer can be made using slurry polymerization to produce the polypropylene polymer followed by gas-phase polymerization of ethylene and one or more
25 comonomers in the presence of the polypropylene polymer particles to produce the ethylene copolymer to form the impact copolymer.

[0022] The impact copolymer can have an ethylene copolymer content from a low of 5 wt%, 8 wt%, 10 wt%, 15 wt%, 25 wt%, 35 wt%, or 45 wt% to a high of 55 wt%, 65 wt%, 75 wt%, or 85 wt%, based on the combined weight of the polypropylene polymer and the
30 ethylene copolymer. Said another way, the amount of the ethylene copolymer can be such that the impact copolymer contains from 5 wt% to 85 wt% of the ethylene copolymer, based on the combined weight of the polypropylene polymer and the ethylene copolymer. For example, the impact polymer can have an ethylene copolymer content of 5 wt% to 80 wt%, 5

wt% to 60 wt%, 5 wt% to 50 wt%, 5 wt% to 40 wt%, 6 wt% to 35 wt%, 7 wt% to 30 wt%, or 8 wt% to 30 wt%, based on the combined weight of the polypropylene polymer and the ethylene copolymer. In another example, the impact copolymer can have an ethylene copolymer content of at least 5 wt%, at least 10 wt%, at least 15 wt%, at least 20 wt%, at least 25 wt%, at least 30 wt%, at least 40 wt%, or at least 45 wt% to a high of 50 wt%, 60 wt%, 70 wt%, 80 wt%, or 85 wt%.

[0023] The one or more halocarbon compounds can be present during polymerization of the monomer mixture in an amount from a low of 5 mg, 10 mg, 50 mg, 75 mg, 100 mg, 125 mg, 150 mg, 175 mg, or 200 mg to a high of 500 mg, 550 mg, 600 mg, 650 mg, 700 mg, 750 mg, 800 mg, 900 mg, 1,000 mg, 2,500 mg, or 5,000 mg per mole of ethylene present during polymerization. For example, the amount of the halocarbon can be from 90 mg to 750 mg, 175 mg to 625 mg, 230 mg to 575 mg, 200 mg to 300 mg, 225 mg to 275 mg, 450 mg to 550 mg, 475 mg to 525 mg, or 100 mg to 700 mg per mole of ethylene present during polymerization.

[0024] The halocarbon compound could potentially adversely affect downstream equipment. As such, the halocarbon compound can be selected such that the halocarbon compound can be removed relatively easily from the impact copolymer. For example, the halocarbon compound can include one or more halocarbon compounds capable of being disengaged from the impact copolymer product via standard separation processes, e.g., flash separation.

[0025] The halocarbon compound can have a boiling point at atmospheric pressure from a low of -80°C, -60°C, or -20°C to a high of 300°C, 200°C, or 150°C. For example, the halocarbon compound can have a boiling point at atmospheric pressure of -75°C to 300°C, -50°C to 250°C, -25°C to 150°C, -10°C to 100°C or 0°C to 50°C.

[0026] The halocarbon compound can have a reactivity at a temperature of less than 200°C toward a molar excess of a scavenging agent at atmospheric pressure such that no less than 99.5% or no less than 99% or no less than 98% or no less than 97% or no less than 90% or no less than 80% or no less than 50% is reacted in 10 minutes in the presence of the polymeric product. Suitable scavenging agents can include, but are not limited to, water, metal oxides, metal hydroxides, metal carbonates, and other metal salts of weak acids such as stearate, organic compounds which react with halocarbons. Exemplary scavenging agents include calcium oxide and phenol derivatives.

[0027] In one or more embodiments, the catalyst activity during polymerization of the ethylene copolymer can be such that the instantaneous polymerization rate in grams per minute of the ethylene copolymer decreases by less than 50%, less than 45%, less than 40%, less than 35%, less than 30%, less than 25%, less than 20%, less than 15%, less than 10%, less than 8%, less than 7%, less than 6%, less than 5%, less than 4%, less than 3%, less than 2%, or less than 1% over a time period of at least 10 minutes after the instantaneous polymerization rate reaches a maximum after start of the polymerization compared to the same catalyst and polymerization system in the absence of the halocarbon.

[0028] The polymerization of propylene and, if present, any other monomer(s) to produce the polypropylene polymer can form polypropylene particles having a weight average particle size along the longest cross-sectional length thereof from a low of 0.01 mm, 0.05 mm, 0.1 mm, 0.3 mm, or 0.5 mm to a high of 2 mm, 3 mm, 4 mm, 5 mm, or 6 mm. For example, the polypropylene particles can have a weight average particle size along the longest cross-sectional length thereof of from 0.05 mm to 5 mm, 0.1 mm to 4 mm, 1 mm to 4.5 mm, 1.5 mm to 3 mm, 2 mm to 4 mm, or 0.2 mm to 3.5 mm.

[0029] The polypropylene particles can also have one or more pores at least partially formed therein and/or therethrough. The polypropylene particles can have a pore volume of less than 80%, less than 75%, less than 70%, less than 60%, less than 50%, or less than 40%. For example, the polypropylene particles can have a pore volume from a low of 5%, 10%, 15%, or 20% to a high of 55%, 65%, 75%, 80%, 85%, or 90%. Preferably, the polypropylene particles have a pore volume of less than 80%.

[0030] The pores formed in and/or through the polypropylene particles can have an average volume from a low of 10^{-9} mm³, 10^{-8} mm³, 10^{-7} mm³, or 10^{-5} mm³, to a high of 10 mm³, 10^{-2} mm³, about 10^{-1} mm³, 1 mm³, or 10 mm³. For example, the polypropylene particles can have pores having an average volume of 10^{-9} mm³ to 10 mm³, 10^{-7} mm³ to 10^{-2} mm³, or 10^{-5} mm³ to 10^{-4} mm³.

[0031] The pores formed in and/or through the polypropylene particles can have a cross-sectional length or in the case of spherical pores a diameter from a low of 10^{-6} mm, 10^{-5} mm, 10^{-4} mm, or 10^{-3} mm to a high of 10^{-3} mm, 10^{-2} mm, about 10^{-1} mm, 1 mm, or 10 mm.

[0032] Without wishing to be bound by theory, it is believed that the catalyst resides, occupies or at least partially resides or occupies within the pores or along the inner walls of the pores that are at least partially formed in or through the polypropylene particles. Accordingly, it is believed that the polymerization of the ethylene and the at least one

comonomer, or at least a majority of the polymerization of the ethylene and the at least one comonomer, occurs within the pores of the polypropylene particles as opposed to outside or external the polypropylene particles. Thus, the resulting impact copolymer can be in the form of polymer particles having a continuous phase composed of the polypropylene particles with
5 a disperse, discontinuous, or occluded phase made up of the ethylene copolymer. Said another way, the ethylene copolymer component can at least partially occupy one or more of the pores that were present in the polypropylene polymer particles prior to polymerization of the ethylene and the comonomer therein. Accordingly, it is believed that halocarbon compounds capable of flowing into the pores of the polypropylene particles can have a
10 greater influence on the catalyst activity and/or the polymerization of the ethylene and the one or more monomers to produce the copolymer component as compared to those that are not capable of flowing into the pores of the polypropylene particles.

[0033] The halocarbon compound, when in the polymerization reactor, can be a gas, a liquid, or both a gas and a liquid, *i.e.*, a first portion of the halocarbon compound can be in
15 the gas phase and a second portion of the halocarbon compound can be in the liquid phase, within the reactor. Halocarbon compounds in the gas and/or liquid phase can more readily flow into the pores of the polypropylene particles and, thus, more efficiently come into contact with the catalyst.

[0034] In one or more embodiments, one or more inert solvents can also be introduced to
20 the polymerization process that can further increase or enhance the concentration of the halocarbon compound and/or the ethylene and/or the at least one other comonomer within the pores of the polypropylene particles. The inert solvent can be mixed, blended, combined, or otherwise contacted with the halocarbon compound and introduced to the polymerization process as a mixture. The inert solvent and the halocarbon compound can be introduced to
25 the polymerization process independent one another. The inert solvent and/or the halocarbon compound can be combined with the polypropylene particles prior to, during, and/or after the addition of the ethylene and the at least one comonomer. The inert solvent and/or the halocarbon compound can be combined with the propylene and present during the polymerization of the propylene to produce the polypropylene particles.

30 [0035] Without wishing to be bound by theory, it is believed that the presence of the inert solvent and/or the halocarbon compound creates, induces, promotes, forms, or otherwise causes an increased presence or concentration of the ethylene and/or the comonomer within the pores of the polypropylene particles. For example, the ethylene and/or the comonomer

can be miscible with, dissolvable in, mixable with, or otherwise combinable with the inert solvent and/or the halocarbon compound, and the ethylene and/or comonomer combined with the inert solvent and/or the halocarbon compound can be present within the pores of the polypropylene particles in an greater amount when the inert solvent and/or halocarbon compound is present compared to when the inert solvent and/or halocarbon compound is/are not. The inert solvent and/or the halocarbon compound can be said to act as a miscibility agent or miscibility compound that can increase the concentration of the ethylene and/or comonomer(s) within the pores of the polypropylene particles.

[0036] Suitable inert solvents can contain from 2 carbon atoms to 20 carbon atoms. For example, the inert solvent can have 3, 4, 5, 6, 7, 8, 9, 10, 11, 12, 13, 14 or 15, carbon atoms. The inert solvent can include alkanes, cycloalkanes, aromatics, cycloalkenes, or any combination thereof. Illustrative alkanes can include, but are not limited to, pentane, hexane, heptane, octane, nonane, decane, isomers thereof, *e.g.*, neopentane, and/or any mixture thereof. Illustrative cycloalkanes can include, but are not limited to, cyclopentane, cyclohexane, cycloheptane, cyclooctane, cyclononane, cyclodecane, or any mixture thereof. Illustrative aromatics can include, but are not limited to, toluene, xylene, naphthalene, or any mixture thereof. Illustrative cycloalkenes can include, but are not limited to, cyclohexane, cyclopentane, methyl cyclohexane, or any mixture thereof. Suitable inert solvents can also include materials containing silicon, boron, and/or aluminum which have the same or similar solubility and boiling characteristics as the afore mentioned carbon containing compounds. Suitable inert solvents that include silicon, boron, and/or aluminum can include, but are not limited to, tetramethyl silane, triethyl borane, or any mixture thereof.

[0037] In one or more embodiments, the miscibility or dissolvability of the one or more comonomers in the inert solvent can be greater than the miscibility or dissolvability of ethylene in the inert solvent. In such a scenario, it is believed that the increased concentration of the comonomer, *e.g.*, propylene, can further increase the molecular weight and/or concentration of the ethylene copolymer in the impact copolymer due to the increased molecular weight of the comonomer relative to ethylene. The inert solvent can be capable of dissolving about 10^{-2} g ethylene per gram inert solvent to 10 g ethylene per gram inert solvent at a pressure from 3 psi to 300 psi absolute and a temperature from 20°C to 130°C. The inert solvent can be capable of dissolving 10^{-2} g propylene per gram inert solvent to 20 g propylene per gram inert solvent at a pressure from 3 psi to 300 psi absolute and a temperature from 20°C to 130°C.

[0038] The amount of the inert solvent combined with the polypropylene particles can be from a low of 0.1, 0.2, 0.3, 0.4, 0.5, 0.6, 0.7, or 0.8 to a high of 1.2, 1.3, 1.4, 1.5, 1.6, 1.7, 1.8, 1.9, or 2 times the pore volume of the polypropylene particles. In at least one embodiment, the inert solvent can be present in an amount of less than 1.5 times, less than 1.4 times, less than 1.3 times, less than 1.2 times, less than 1.1 times, less than 1 times, less than 0.9 times, less than 0.8 times, less than 0.7 times, or less than 0.6 times the pore volume of the polypropylene particles. In at least one other embodiment the inert solvent can be combined with the polypropylene particles in an amount greater than 0.5 times, or greater than 0.65 times, or greater than 0.75 times to less than 1.4 times, less than 1.25 times, or less than 1.15 times the pore volume of the polypropylene particles.

Polypropylene Polymers

[0039] As used herein, "polypropylene polymer" can include homopolymers of propylene derived units and/or copolymers of propylene derived units comprising within the range from 0.1 wt% to 1 wt%, 3 wt%, or 5 wt% of a copolymer of ethylene or C4 to C12 α -olefin derived units, ethylene derived units in a particular embodiment. As such, the polypropylene polymer can be selected from polypropylene homopolymer, polypropylene copolymers, blends thereof, or any combination thereof. The homopolymer can be atactic polypropylene, isotactic polypropylene, highly isotactic polypropylene, syndiotactic polypropylene, and blends thereof. The polypropylene copolymer can be a polypropylene homopolymer (HPP), a random copolymer (RCP), a statistical copolymer, a block copolymer, and blends thereof.

[0040] The polypropylene polymer can have a propylene content of at least 85 wt%, preferably at least 90 wt%, preferably at least 95 wt%, preferably at least 97 wt%, or preferably 100 wt%. For example, the polypropylene polymer can have a propylene content from 85 wt% to 99 wt%, 88 wt% to 98 wt%, 87 wt% to 96 wt%, 91 wt% to 98 wt%, or 86 wt% to 99 wt%. In at least one embodiment, the polypropylene polymer can be a homopolymer.

[0041] The polypropylene polymer can have a weight average molecular weight (Mw) from a low of 25 kg/mol, 50 kg/mol, 100 kg/mol, 200 kg/mol, or 500 kg/mol to a high of 700 kg/mol, 900 kg/mol, 1,200 kg/mol, 1,600 kg/mol, or 2,000 kg/mol. For example, the polypropylene polymer can have a Mw from 30 kg/mol to 2,000 kg/mol, 50 kg/mol to 1,000 kg/mol, or 90 kg/mol to 500 kg/mol.

[0042] The polypropylene polymer can have ratio of the weight average molecular weight (Mw) to number average molecular weight (Mn) or (Mw/Mn) from a low of 1, 1.5, or

2 to a high of 20, 30, or 40. For example, the polypropylene polymer can have an Mw/Mn of 1.4 to 20, or 1.6 to 10, or 1.8 to 3.5, or 1.8 to 2.5.

[0043] The polypropylene polymer can have a branching index (g') from a low of 0.2, 0.5, or 1 to a high of 1.3, 1.5, 1.7, or 2. For example, the polypropylene polymer can have a
5 branching index of 0.2 to 2.0, or 0.5 to 1.5, or 0.7 to 1.3, or 0.9 to 1.1.

[0044] The polypropylene polymer can have a melt flow rate (MFR) from a low of 1 dg/min, 15 dg/min, 30 dg/min, or 45 dg/min to a high of 75 dg/min, 100 dg/min, 200 dg/min, or 300 dg/min. For example, the polypropylene polymer can have an MFR of 1 dg/min to 300 dg/min, 5 dg/min to 150 dg/min, or 10 dg/min to 100 dg/min, or 20 dg/min to 60 dg/min.

10 [0045] The polypropylene polymer can have a melting point (T_m , peak second melt) of at least 100°C, or at least 110°C, or at least 120°C, or at least 130°C, or at least 140°C, or at least 150°C, or at least 160°C, or at least 165°C. For example, the polypropylene polymer can have a melting point from at least 100°C to 175°C, or 170°C to 165°C, or 160°C to 145°C.

15 [0046] The polypropylene polymer can have a crystallization temperature (T_c , peak) of at least 70°C, or at least 90°C, or at least 110°C, or at least 130°C. For example, the polypropylene polymer can have a crystallization temperature from at least 70°C to 75°C, or 80°C to 90°C, or 110°C to 130°C, or 120°C to 150°C.

[0047] The polypropylene polymer can have a heat of fusion (H_f) from a low of 40 J/g,
20 45 J/g, 55 J/g, or 65 J/g to a high of 90 J/g, 110 J/g, 140 J/g, or 170 J/g. For example, the polypropylene polymer can have a heat of fusion from 40 J/g to 160 J/g, or 50 J/g to 140 J/g, or 60 J/g to 120 J/g, or 80 J/g to 100 J/g.

[0048] The polypropylene polymer can have a crystallinity from a low of 5%, 12%, 22%, 33%, or 44% to a high of 60%, 68%, 78%, or 83%. For example, the polypropylene polymer
25 can have a crystallinity of 5% to 80%, 10% to 75%, 20% to 70%, 30% to 65%, or 40% to 60%.

[0049] The polypropylene polymer can have a heat deflection temperature (HDT) from a low of 45°C, 50°C, 55°C, or 65°C to a high of 100°C, 115°C, 130°C, or 140°C, as measured according to ASTM D 648 (0.45 MPa). For example, the polypropylene polymer can have a
30 heat deflection temperature from 45°C to 140°C, 60°C to 135°C, or 75°C to 125°C, as measured according to ASTM D 648 (0.45 MPa).

[0050] The polypropylene polymer can have a Gardner impact strength at 23°C from a low of 30 KJ/m², 60 KJ/m², 100 KJ/m², or 150 KJ/m² to a high of 500 KJ/m², 700 KJ/m²,

900 KJ/m², 1,100 KJ/m², or 1,350 KJ/m², as measured according to ASTM D 5420 (GC). For example, the polypropylene polymer can have a Gardner impact strength at 23°C of 30 KJ/m² to 1,300 KJ/m², 40 KJ/m² to 800 KJ/m², or 50 KJ/m² to 600 KJ/m², as measured according to ASTM D 5420 (GC).

5 [0051] The polypropylene polymer can have a 1% secant flexural modulus from a low of 300 MPa, 500 MPa, 800 MPa, or 1,000 MPa to a high of 1,700 MPa, 2,100 MPa, 2,600 MPa, or 3,100 MPa, as measured according to ASTM D 790 (A, 1.3 mm/min). For example, the polypropylene polymer can have a flexural modulus from 300 MPa to 3,000 MPa, 600 MPa to 2,500 MPa, 800 MPa to 2,000 MPa, or 1,000 MPa to 1,500 MPa, as measured according to
10 ASTM D 790 (A, 1.3 mm/min).

[0052] The polypropylene polymer can have some level of isotacticity or syndiotacticity. In one embodiment the polypropylene polymer is isotactic polypropylene. In another embodiment the polypropylene polymer is highly isotactic polypropylene. In still another embodiment the polypropylene polymer is a polypropylene homopolymer having at least
15 85% or at least 90% isotactic pentads. In yet another embodiment the polypropylene polymer is a polypropylene homopolymer having at least 85% or at least 90%) syndiotactic pentads. As used herein, "isotactic" is defined as having at least 10% isotactic pentads according to analysis by ¹³C NMR. As used herein, "highly isotactic" is defined as having at least 60% isotactic pentads according to analysis by ¹³C NMR.

20 [0053] The polypropylene polymer can have a propylene meso diads of 90% or more, 92% or more, 94% or more, 95% or more, 96% or more, 97% or more, or 98% or more. The isotacticity of the polypropylene polymer can be measured by ¹³C NMR. For example, suitable techniques for measuring the isotacticity of the polypropylene polymer can be as discussed and described in US: 4,950,720. Expressed another way, the isotacticity of the
25 polypropylene polymer, as measured by ¹³C NMR, and expressed as pentad content, is greater than 93% or 95%, or 97% in certain embodiments.

Ethylene Copolymer

[0054] As used herein, "ethylene copolymer" is a material that can stretch and recover such that it exhibits an Ultimate Tensile Strength of greater than 2.0 MPa, an Ultimate
30 Elongation of at least 200%, and Tension Set of less than 20% at 100% deformation, as determined by ASTM D412. Non-limiting examples of ethylene copolymers include, but are not limited to, EPM (ethylene-propylene rubber), and EPDM rubber (ethylene-propylene-diene rubber) as well as copolymers of ethylene with an alpha olefin or a mixture of alpha

olefins. An "alpha olefin," alternatively referred to as "alkene," is a linear, branched, or cyclic compound of carbon and hydrogen having at least one double bond. For purposes of this specification and the claims appended thereto, when a polymer or copolymer is referred to as comprising an olefin, including, but not limited to, ethylene, propylene, and butene, the olefin present in such polymer or copolymer is the polymerized form of the olefin. For example, when a copolymer is said to have an "ethylene" content of 35 wt% to 55 wt%, it is understood that the mer unit in the copolymer is derived from ethylene in the polymerization reaction and said derived units are present at 35 wt% to 55 wt%, based upon the weight of the copolymer. A "polymer" has two or more of the same or different mer units. A "homopolymer" is a polymer having mer units that are the same. A "copolymer" is a polymer having two or more mer units that are different from each other. A "terpolymer" is a polymer having three mer units that are different from each other. "Different" as used to refer to mer units indicates that the mer units differ from each other by at least one atom or are different isomerically. Accordingly, the definition of copolymer, as used herein, includes terpolymers and the like. An ethylene polymer is a polymer comprising at least 50 mol% of ethylene; propylene polymer is a polymer having at least 50 mol% of propylene; a butene polymer is a polymer comprising at least 50 mol% butene; and so on.

[0055] An "alpha-olefin" is an olefin having a double bond at the alpha (or 1-) position. A "linear alpha-olefin" or "LAO" is an olefin with a double bond at the alpha position and a linear hydrocarbon chain. For the purposes of this disclosure, the term " α -olefin" includes C₂-C₂₀ olefins. Non-limiting examples of α -olefins include ethylene, propylene, 1-butene, 1-pentene, 1-hexene, 1-heptene, 1-octene, 1-nonene, 1-decene, 1-undecene, 1-dodecene, 1-tridecene, 1-tetradecene, 1-pentadecene, 1-hexadecene, 1-heptadecene, 1-octadecene, 1-nonadecene, 1-eicosene, 1-heneicosene, 1-docosene, 1-tricosene, 1-tetracosene, 1-pentacosene, 1-hexacosene, 1-heptacosene, 1-octacosene, 1-nonacosene, 1-triacontene, 4-methyl-1-pentene, 3-methyl-1-pentene, 5-methyl-1-nonene, 3,5,5-trimethyl-1-hexene, vinylcyclohexane, and vinylnorbornene.

[0056] The ethylene copolymer can have an ethylene content from a low of 20 wt%, 35 wt%, 40 wt%, or 45 wt% to a high of 65 wt%, 70 wt%, 80 wt%, or 85 wt%, based on the combined weight of the ethylene monomer and the one or more comonomers, *e.g.*, propylene, polymerized to produce the ethylene copolymer. For example, the ethylene copolymer can have an ethylene content of 25 wt% to 80 wt%, 30 wt% to 75 wt%, 35 wt% to 70 wt%, or 40 wt% to 65 wt%, based on the combined weight of the ethylene monomer and the one or more

comonomers, *e.g.*, propylene, polymerized to produce the ethylene copolymer. As such, the comonomer content, *e.g.*, propylene, in the ethylene copolymer can be from a low of 15 wt%, 20 wt%, 25 wt%, or 20 wt% to a high of 50 wt%, 60 wt%, 70 wt%, or 80 wt%. In at least one specific embodiment, the comonomer content, *e.g.*, propylene, in the ethylene copolymer
5 can be at least 15 wt%, at least 20 wt%, at least 25 wt%, at least 30 wt%, or at least 35 wt%, based on the combined weight of the ethylene monomer and the comonomer(s) polymerized to produce the ethylene copolymer.

[0057] The ethylene copolymer can have a comonomer, *e.g.*, propylene, content from a low of 15 wt%, 20 wt%, or 25 wt% to a high of 50 wt%, 77 wt%, or 80 wt%, based on the
10 combined weight of the ethylene monomer and the propylene monomer polymerized to produce the ethylene copolymer. For example, the ethylene copolymer can have a comonomer, *e.g.*, propylene, content from 25 wt% to 80 wt%, 10 wt% to 75 wt%, 35 wt% to 70 wt%, or at least 40 wt% to 80 wt%, based on the combined weight of the ethylene monomer and the propylene monomer polymerized to produce the ethylene copolymer.

15 [0058] The ethylene copolymer can have a non-conjugated diene or termonomer content of 15 wt% or less, 12 wt% or less, 9 wt% or less, 6 wt% or less, 3 wt% or less, or 1 wt% or less. For example, the ethylene copolymer can have a non-conjugated diene content of 2 wt% to 14 wt%, 6 wt% to 13 wt%, 4 wt% to 8 wt%, or 1 wt% to 11 wt%. Particularly preferred ethylene copolymers can contain no diene. If one or more dienes are present (*e.g.*,
20 an ethylene-propylene-diene terpolymer), preferably the diene is a norbornene-derived diene such as ethylidene norbornene (ENB) or vinylidene norbornene (VNB). Diene content can be measured according to ASTM D 6047. In at least one example the ethylene copolymer can be free from any diene.

[0059] The ethylene copolymer can have a density of 0.87 g/cm³ or less, 0.865 g/cm³ or less, 0.86 g/cm³ or less, or 0.855 g/cm³ or less. For example, the ethylene copolymer can
25 have a density of 0.84 g/cm³ to 0.85 g/cm³, 0.86 g/cm³ to 0.87 g/cm³, 0.88 g/cm³ to 0.89 g/cm³, or 0.90 g/cm³ to 0.92 g/cm³.

[0060] The ethylene copolymer can have a heat of fusion (H_f), if detected, of less than 20 J/g, less than 15 J/g, less than 10 J/g, less than 5 J/g, or less than 3 J/g. In at least one
30 example the ethylene copolymer can have a heat of fusion that is indiscernible.

[0061] The ethylene copolymer can have an ethylene or propylene crystallinity, if measurable, of less than 10 wt%, less than 7.5 wt%, less than 5 wt%, less than 2.5 wt%, or less than 1 wt%. In at least one example, the ethylene copolymer can have an ethylene or

propylene crystallinity that is undetectable. In a preferred embodiment, the ethylene copolymer has a crystallinity, as determined by DSC, of less than 20 %, preferably less than 10%, preferably less than 5%, preferably less than 1%.

[0062] The ethylene copolymer can have a melting point (T_m , peak first melt), if
5 detected, of 60°C or less, 50°C or less, 40°C or less, or 35°C or less. The ethylene copolymer can have a glass transition temperature (T_g) of -30°C or less, -40°C or less, -50°C or less, or -60°C or less.

[0063] The ethylene copolymer can have a weight average molecular weight (M_w) from
10 a low of 50 kg/mol, 75 kg/mol, 150 kg/mol, or 300 kg/mol to a high of 600 kg/mol, 900 kg/mol, 1,300 kg/mol, 2,000 kg/mol, 2,500 kg/mol, or 3,000 kg/mol. For example, the ethylene copolymer can have a M_w of 50 kg/mol to 3,000 kg/mol, 100 kg/mol to 2,000 kg/mol, or 200 kg/mol to 1,000 kg/mol.

[0064] The ethylene copolymer can have a ratio of weight average molecular weight
15 (M_w) to number average molecular weight (M_n) or (M_w/M_n) from a low of 1, 1.5, or 2 to a high of 20, 30, or 40. For example, the ethylene copolymer can have an M_w/M_n of 1.4 to 20, or 1.6 to 10, or 1.8 to 3.5, or 1.8 to 2.5.

[0065] The ethylene copolymer can have a Mooney viscosity, $ML(1+4)$ at 125°C, from a
low of 10, 13, 17, or 23 to a high of 80, 87, 93, or 100. For example, the ethylene copolymer can have a Mooney viscosity, $ML(1+4)$ at 125°C, of 10 to 100, 15 to 90, or 20 to 85).

20 [0066] As discussed and described above and elsewhere herein, the particular process of making the polypropylene polymer and the ethylene copolymer is not critical, as it can be made by slurry, solution, gas-phase, high-pressure, or any other suitable processes, or combinations of processes, through the use of catalyst systems appropriate for the polymerization of polyolefins, such as Ziegler-Natta-type catalysts, metallocene-type
25 catalysts, other appropriate catalyst systems or combinations thereof. In a preferred embodiment, the propylene polymers are made by the catalysts, activators, and processes discussed and described in US 5,741,563; 6,342,566; 6,384,142; and WO 03/040201 and WO 97/19991. Such catalysts are well known in the art, and are described in, for example, "Ziegler Catalysts," Gerhard Fink, Rolf Mülhaupt, and Hans H. Brintzinger, eds., Springer-
30 Verlag 1995; Resconi *et al.*, "Selectivity in Propene Polymerization with Metallocene Catalysts," 100 CHEM. REV. 1253-1345 (2000); and "I, II Metallocene-Based Polyolefins" (Wiley & Sons 2000).

Impact Copolymer

[0067] The impact copolymer (ICP) can include the polypropylene polymer and the ethylene copolymer. In at least one example, the impact copolymer can include a HPP (homopolypropylene) or RCP (random copolymer) polypropylene polymer component and
5 an ethylene-propylene copolymer. The morphology can be such that the matrix phase is primarily the polypropylene polymer and the dispersed phase can be primarily the ethylene copolymer phase.

[0068] The impact copolymer can have a total propylene content of at least 75 wt%, at least 80 wt%, at least 85 wt%, at least 90 wt%, or at least 95 wt%, based on the combined
10 weight of the polypropylene polymer and the ethylene copolymer. The impact copolymer can have a total propylene content of at least 75 wt%, at least 80 wt%, at least 85 wt%, at least 90 wt%, or at least 95 wt%, based on the total weight of the impact copolymer. For example, if the impact copolymer includes the polypropylene polymer, the ethylene copolymer, and a second polypropylene polymer, with no other components being present,
15 the impact copolymer can have a total propylene content of at least 75 wt%, at least 80 wt%, at least 85 wt%, at least 90 wt%, or at least 95 wt%, based on the combined weight of the polypropylene polymer, the ethylene copolymer, and the second polypropylene polymer or said another way the total weight of the impact copolymer.

[0069] The impact copolymer can have a total comonomer content from a low of 1 wt%,
20 5 wt%, 9 wt%, or 12 wt% to a high of 18 wt%, 23 wt%, 28 wt%, or 35 wt%, based on the total weight of the impact copolymer. For example, the impact copolymer can have a total comonomer content of 1 wt% to 35 wt%, 2 wt% to 30 wt%, 3 wt% to 25 wt%, or 5 wt% to 20 wt%, based on the total weight of the impact copolymer.

[0070] The impact copolymer can have an ethylene copolymer content from a low of 5
25 wt%, 8 wt%, 10 wt%, or 15 wt% to a high of 25 wt%, 30 wt%, 38 wt%, or 42 wt%. For example, the impact polymer can have an ethylene copolymer content of 5 wt% to 40 wt%, 6 wt% to 35 wt%, 7 wt% to 30 wt%, or 8 wt% to 30 wt%.

[0071] The impact copolymer can have a propylene content of the ethylene copolymer component from a low of 25 wt%, 37 wt%, or 46 wt% to a high of 73 wt%, 77 wt%, or 80
30 wt%, based on the based on a weight of the ethylene copolymer. For example, the impact copolymer can have a propylene content of the ethylene copolymer component from 25 wt% to 80 wt%, 10 wt% to 75 wt%, 35 wt% to 70 wt%, or at least 40 wt% to 80 wt%, based on the weight of the ethylene copolymer.

[0072] The impact copolymer can have ratio of the intrinsic viscosity (IV, ASTM D 1601 -135°C in decalin) of the ethylene copolymer component to the intrinsic viscosity of the polypropylene component from a low of 0.5, 1.5, 3, or 4 to a high of 6, 9, 12, or 15. For example, the impact copolymer component can have a ratio of the intrinsic viscosity of 0.5 to 15, 0.75 to 12, or 1 to 7.

[0073] The impact copolymer can have a propylene meso diads content in the polypropylene component 90% or more, 92% or more, 94% or more, or 96% or more.

[0074] The impact copolymer can have a weight average molecular weight (Mw) from a low of 20 kg/mol, 50 kg/mol, 75 kg/mol, 150 kg/mol, or 300 kg/mol to a high of 600 kg/mol, 900 kg/mol, 1,300 kg/mol, or 2,000 kg/mol. For example, the ethylene copolymer can have a Mw of 50 kg/mol to 3,000 kg/mol, 100 kg/mol to 2,000 kg/mol, or 200 kg/mol to 1,000 kg/mol.

[0075] The impact copolymer can have a melt flow rate (MFR) from a low of 1 dg/min, 15 dg/min, 30 dg/min, or 45 dg/min to a high of 75 dg/min, 100 dg/min, 200 dg/min, or 300 dg/min. For example, the impact copolymer can have an MFR of 1 dg/min to 300 dg/min, 5 dg/min to 150 dg/min, or 10 dg/min to 100 dg/min, or 20 dg/min to 60 dg/min.

[0076] The impact copolymer can have a melting point (T_m, peak second melt) of at least 100°C, or at least 110°C, or at least 120°C, or at least 130°C, or at least 140°C, or at least 150°C, or at least 160°C, or at least 165°C. For example, the impact copolymer can have a melting point from at least 100°C to 175°C, 105°C to 165°C, 105°C to 145°C, or 100°C to 155°C.

[0077] The impact copolymer can have a heat of fusion (H_f, DSC second heat) from a high of 60 J/g, 75 J/g, 85 J/g, or 95 J/g to a low of 20 J/g, 30 J/g, 40J/g, or about 50J/g. In at least one embodiment the impact copolymer can have a heat of fusion of 60 J/g or more, 70 J/g or more, 80 J/g or more, 90 J/g or more, 95 J/g or more, or 100 J/g or more.

[0078] The impact copolymer can have glass transition temperature (T_g) of the ethylene copolymer component of -20°C or less, -30°C or less, -40°C or less, or -50°C or less.

[0079] The impact copolymer can have a 1% secant flexural modulus from a low of 300 MPa, 600 MPa, 800 MPa, 1,100 MPa, or 1,200 MPa to a high of 1,500 MPa, 1,800 MPa, 2,100 MPa, 2,600 MPa, or 3,000 MPa, as measured according to ASTM D 790 (A, 1.3 mm/min). For example, the impact copolymer can have a flexural modulus from 300 MPa to 3,000 MPa, 500 MPa to 2,500 MPa, 700 MPa to 2,000 MPa, or 900 MPa to 1,500 MPa, as measured according to ASTM D 790 (A, 1.3 mm/min).

[0080] The impact copolymer can have a notched Izod impact strength at 23°C of 2.5 KJ/m² or more, 5 KJ/m² or more, 7.5 KJ/m² or more, 10 KJ/m² or more, 15 KJ/m² or more, 20 KJ/m² or more, 25 KJ/m² or more, or 50 KJ/m² or more, as measured according to ASTM D 256 (Method A). For example, the impact copolymer can have a notched Izod impact strength at 23°C from a low of 3 KJ/m², 6 KJ/m², 12 KJ/m² or 18 KJ/m² to a high of 30 KJ/m², 35 KJ/m², 45 KJ/m², 55 KJ/m², or 65 KJ/m², as measured according to ASTM D 256 (Method A).

[0081] The impact copolymer can have a Gardner impact strength at -30°C from a low of 2 KJ/m², 3 KJ/m², 6 KJ/m², 12 KJ/m², or 20 KJ/m² to a high of 55 KJ/m², 65 KJ/m², 75 KJ/m², 85 KJ/m², 95 KJ/m², or 105 KJ/m², as measured according to ASTM D 5420 (GC). For example, the impact copolymer can have a Gardner impact strength at -30°C of 2 KJ/m² to 100 KJ/m², 3 KJ/m² to 80 KJ/m², or 4 KJ/m² to 60 KJ/m², as measured according to ASTM D 5420 (GC).

[0082] The impact copolymer can have a heat deflection temperature (HDT) from a low of 75°C, 83°C, 87°C, or 92°C to a high of 95°C, 100°C, 105°C, or about 120°C, as measured according to ASTM D 648 (0.45 MPa). For example, the impact copolymer can have a heat deflection temperature of 80°C or more, 85°C or more, 90°C or more, or 95°C or more, as measured according to ASTM D 648 (0.45 MPa).

[0083] In at least one specific embodiment, the impact copolymer can have an MFR from 6 dg/min to 200 dg/min; a 1% Secant Flexural Modulus greater than 820 MPa, and an Izod Impact at 25°C of greater than 26 KJ/m².

[0084] In at least one specific embodiment, the impact copolymer can have an ethylene copolymer concentration of at least 10 wt% to about 35 wt%, based on the combined weight of the polypropylene polymer and the ethylene copolymer, a notched Izod impact strength at 23°C of at least 5 KJ/m² to 75 KJ/m², and a flexural modulus less than 1,200 MPa to 1,900 MPa. In at least one specific embodiment, the impact copolymer can have an ethylene copolymer concentration of at least 15 wt% to 25 wt%, based on the combined weight of the polypropylene polymer and the ethylene copolymer, a notched Izod impact strength at 23°C of at least 15 KJ/m² to 65 KJ/m², and a flexural modulus less than 1,300 MPa to 1,800 MPa.

[0085] In at least one specific embodiment, the impact copolymer can have an ethylene copolymer having a weight average molecular weight of at least 30 kg/mol to 200 kg/mol, a notched Izod impact strength at 23°C of at least 5 KJ/m² to 75 KJ/m², and an MFR at 230°C of from 10 to 75. In at least one specific embodiment, the impact copolymer can have an

ethylene copolymer having a weight average molecular weight of at least 10 kg/mol to 35 kg/mol, a notched Izod impact strength at 23°C of at least 5 KJ/m² to 75 KJ/m², and an MFR at 230°C of from 10 to 75. In at least one specific embodiment, the impact copolymer can have an ethylene copolymer having a weight average molecular weight of at least 45 kg/mol to 150 kg/mol, a notched Izod impact strength at 23°C of at least 15 KJ/m² to 65 KJ/m², and a and an MFR at 230°C of between 10 to 75. In at least one specific embodiment, the impact copolymer can have an ethylene copolymer having a weight average molecular weight of at least 35 kg/mol to 250 kg/mol, a notched Izod impact strength at 23°C of at least 15 KJ/m² to 65 KJ/m², and an MFR at 230°C of from 10 to 75.

10 Additives

[0086] Additives such as antioxidants and stabilizers (including UV stabilizers and other UV absorbers, such as chain-breaking antioxidants), fillers (such as mineral aggregates, fibers, clays, and the like), nucleating agents, slip agents, block, antiblock, pigments, dyes, color masterbatches, waxes, processing aids (including pine or coal tars or resins and asphalts), neutralizers (such as hydro talcite), adjuvants, oils, lubricants, low molecular weight resins, surfactants, acid scavengers, anticorrosion agents, cavitating agents, blowing agents, quenchers, antistatic agents, cure or cross linking agents or systems (such as elemental sulfur, organo-sulfur compounds, and organic peroxides), fire retardants, coupling agents (such as silane), and combinations thereof may also be present in the impact copolymer compositions described herein. Typical additives used in polypropylene and polypropylene blends are described in POLYPROPYLENE HANDBOOK 2ND ED., N. Pasquini, ed. (Hanser Publishers, 2005). The additives may be present in the typically effective amounts well known in the art, preferably at 0.001 to 50 wt% (preferably 0.01 to 20 wt%, preferably 0.1 to 10 wt%, preferably 0.1 to 1 wt%), based upon the weight of the composition. Pigments, dyes, and other colorants may be present from 0.01 to 10 wt% (preferably 0.1 to 6 wt%).

[0087] As used herein, "additives" include, for example, stabilizers, surfactants, antioxidants, anti-ozonants (*e.g.*, thioureas), fillers, colorants, nucleating agents, anti-block agents, UV-blockers/absorbers, coagents (cross-linkers and cross-link enhancers), hydrocarbon resins (*e.g.*, OpperaTM resins), and slip additives and combinations thereof. Primary and secondary antioxidants include, for example, hindered phenols, hindered amines, and phosphates. Slip agents include, for example, oleamide and erucamide. Examples of fillers include carbon black, clay, talc, calcium carbonate, mica, silica, silicate, and

combinations thereof. Other additives include dispersing agents and catalyst deactivators such as calcium stearate, hydrotalcite, and calcium oxide, and/or other acid neutralizers known in the art. In certain embodiments, cross-linkers and cross-link enhancers are absent from the propylene impact copolymers.

5 [0088] The desirable properties of the propylene impact copolymer may be adjusted in part by the balance of properties between the polypropylene matrix and the elastomeric domains. In a particular embodiment, the elastomeric polymer (e.g. the ethylene copolymer) has an intrinsic viscosity, IV^R , and the polypropylene has an intrinsic viscosity, IV^{PP} , wherein the ratio of IV^R/IV^{PP} is within the range from 1.50 or 1.75 or 1.80 to 2.70 or 3.00 or 10 4.00. The term "intrinsic viscosity" is used to indicate the viscosity of a solution of a material, in this case a solution of a polymer, in a given solvent at a given temperature, when the polymer composition is at infinite dilution. According to the ASTM standard test method D 1601-78, its measurement involves a standard capillary viscosity measuring device, in which the viscosity of a series of concentrations of the polymer in the solvent at the given 15 temperature are determined. In the case of the polypropylene polymer, ethylene copolymer, and the impact copolymers discussed and described herein, decalin (decahydronaphthalene) is an illustrative suitable solvent and a typical temperature is 135°C. From the values of the viscosity of solutions of varying concentration, the "value" at infinite dilution can be determined by extrapolation. In the case of the present propylene impact copolymers that are 20 reactor produced *in situ*, the homopolymer portion is initially produced and the intrinsic viscosity of that portion is measured directly. The intrinsic viscosity of the elastomeric portion cannot be measured directly. The intrinsic viscosity of the total propylene impact copolymer product is determined and the intrinsic viscosity of the elastomeric polymer portion ($[\eta]_{\text{elast}}$) is calculated as the quotient of the intrinsic viscosity of the total propylene 25 impact copolymer ($[\eta]_{\text{whole}}$) less the fraction of polypropylene times its intrinsic viscosity ($[\eta]_{\text{PP}}$), all divided by the fraction of the total impact copolymer which is elastomeric polymer. The formula is $[\eta]_{\text{elast}} = [[\eta]_{\text{whole}} - (1-F_c)[\eta]_{\text{PP}}]/F_c$, where F_c is the amount of elastomeric polymer and is stated in terms of a fraction of elastomeric polymer, ethylene/propylene copolymer in a particular embodiment, in the total propylene impact 30 copolymer. This fraction is determined by conventional procedures, including infrared analysis.

[0089] The impact copolymer, described in its various embodiments, can be further characterized by possessing an Instrumented Impact (5 mph at -29°C) of greater than 47 J, a

Tensile at Yield of greater than 21.4 MPa, a Gardner Impact (-29°C) of greater than 34 N-m, or a combination of any two or more of these properties.

Catalysts

[0090] The terms "catalyst" and "catalyst compound" are defined to mean a compound
5 capable of initiating catalysis. In the description herein, the catalyst may be described as a catalyst precursor, a pre-catalyst compound, or a transition metal compound, and these terms are used interchangeably. A catalyst compound may be used by itself to initiate catalysis or may be used in combination with an activator to initiate catalysis. When the catalyst compound is combined with an activator to initiate catalysis, the catalyst compound is often
10 referred to as a pre-catalyst or catalyst precursor. A "catalyst system" is a combination of at least one catalyst compound, an optional activator, an optional co-activator, and an optional support material, where the system can polymerize monomers to polymer. For the purposes of this disclosure, when catalyst systems are described as comprising neutral stable forms of the components, it is well understood by one of ordinary skill in the art, that the ionic form of
15 the component is the form that reacts with the monomers to produce polymers.

[0091] A "scavenger" is a compound that is typically added to facilitate polymerization by scavenging impurities. Some scavengers may also act as activators and may be referred to as co-activators. A co-activator, that is not a scavenger, may also be used in conjunction with an activator in order to form an active catalyst. In some embodiments, a co-activator can be
20 pre-mixed with the catalyst compound to form an alkylated catalyst compound, also referred to as an alkylated compound.

Ziegler-Natta PP Catalysts

[0092] The polypropylene and/or the ethylene copolymer can generally be produced using Ziegler-Natta catalysts. The Ziegler-Natta catalyst can include 1) a solid titanium
25 catalyst component that can include a titanium compound, a magnesium compound, and an internal electron donor; 2) a co-catalyst such as an organoaluminum compound, and 3) external electron donor(s). Ziegler-Natta catalysts, catalyst systems, and preparations thereof can include supported catalyst systems as discussed and described in US 4,990,479 and 5,159,021 and WO 00/44795. Preferably, the Ziegler-Natta catalyst can include solid
30 titanium and/or magnesium. For example, useful Ziegler-Natta catalysts are typically composed of a transition metal compound from groups 4, 5, 6 and/or 7 (preferably group 4) and an organometallic compound of a metal from groups 11, 12 and/or 13 (preferably group 13) of the periodic table. Well-known examples include $\text{TiCl}_3\text{-Et}_2\text{AlCl}$, $\text{AlR}_3\text{-TiCl}_4$, where

Et is an ethyl group and R represents an alkyl group, typically a C1 to C20 alkyl group, such as methyl, ethyl, propyl, butyl, pentyl, hexyl, octyl and the like. These catalysts include mixtures of halides of transition metals, especially titanium, chromium, vanadium, and zirconium, with organic derivatives of nontransition metals, particularly alkyl aluminum compounds. As used herein, the new notation for the Periodic Table Groups is used as described in *Chemical and Engineering News*, 63(5), p. 27 (1985).

[0093] The Ziegler-Natta catalysts can be obtained by: (1) suspending a dialkoxy magnesium compound in an aromatic hydrocarbon that is liquid at ambient temperature; (2) contacting the dialkoxy magnesium-hydrocarbon composition with a titanium halide and with a diester of an aromatic dicarboxylic acid; and (3) contacting the resulting functionalized dialkoxy magnesiumhydrocarbon composition of step (2) with additional titanium halide.

[0094] The Ziegler-Natta catalyst can be combined with one or more co-catalysts. One particularly suitable co-catalyst can include an organoaluminum compound that is halogen free. Suitable halogen free organoaluminum compounds can include, but are not limited to, branched unsubstituted alkylaluminum compounds of the formula AlR_3 , where R denotes an alkyl radical having 1 to 20 carbon atoms (preferably methyl, ethyl, propyl, butyl, pentyl, hexyl, octyl and the like), such as for example, trimethylaluminum, triethylaluminum, triisobutylaluminum and tridiisobutylaluminum. Additional compounds suitable for use as the cocatalyst are readily available and amply disclosed in the prior art including those disclosed in US 4,990,477. The same or different Ziegler-Natta catalyst(s) can be used in both the initial and subsequent polymerization steps. In a preferred embodiment, the solid catalyst is a magnesium supported $TiCl_4$ catalyst and the organoaluminum co-catalyst is triethylaluminum.

[0095] Electron donors can also be used in the formation of ZieglerNatta catalysts and catalyst systems. For example, an internal electron donor can be used in the formation reaction of the catalyst as the transition metal halide reacts with the metal hydride or metal alkyl. Examples of internal electron donors can include, but are not limited to, amines, amides, ethers, esters, aromatic esters, ketones, nitriles, phosphines, stilbenes, arsines, phosphoramides, thioethers, thioesters, aldehydes, alcoholates, salts of organic acids, or any mixture or combination thereof. In conjunction with an internal donor, an external electron donor can also be used in combination with the catalyst. External electron donors often affect the level of stereoregularity in polymerization reactions.

[0096] Another use for an electron donor in the catalyst system can be as an external electron donor and stereoregulator in the polymerization reaction. The same compound can be used in both instances, although typically they are different. Preferred External electron donor materials can include, but are not limited to, organic silicon compounds, *e.g.*,
5 tetraethoxysilane (TEOS) and dicyclopentylmethoxysilane (DCPMS). Internal and external-type electron donors are discussed and described, for example, in US 4,535,068. The use of organic silicon compounds as external electron donors are described, for example, in US 4,218,339; 4,395,360; 4,328,122; 4,473,660; 6,133,385; and 6,127,303. Particularly useful electron donors include external electron donors used as stereoregulators, in
10 combination with ZieglerNatta catalysts.

[0097] A particularly useful Ziegler-Natta catalyst can be a magnesium chloride supported titanium catalyst selected from the group of THC-C type catalyst solid systems available from Toho Titanium Corporation of Japan. Particularly preferred donor systems can include those discussed and described in US 6,087,495. For example, the donor can be or
15 include a blend of propyltriethoxysilane (PTES) and dicyclopentylmethoxysilane (DCPMS), typically a 95/5 mole% blend. Another useful donor is methylcyclohexyl dimethoxysilane (MCMS).

[0098] A particular Ziegler-Natta catalyst may produce better results when paired with a particular group of electron donors. Examples of this paring of catalyst and electron donors
20 are disclosed in US 4,562,173 and 4,547,552.

[0099] Other Ziegler-Natta catalyst compounds are disclosed in European Patent Nos. EP 0103120; EP 1102503; EP 0231102; EP 0703246; US RE 33,683; 4,115,639; 4,077,904; 4,302,565; 4,302,566; 4,482,687; 4,564,605; 4,721,763; 4,879,359; 4,960,741; 5,518,973; 5,525,678; 5,288,933; 5,290,745; 5,093,415; and 6,562,905; and US 2008/0194780.

25 [00100] A mixed catalyst can also be used to produce the linear polyethylene. The mixed catalyst can be a bimetallic catalyst composition or a multi-catalyst composition. As used herein, the terms "bimetallic catalyst composition" and "bimetallic catalyst" include any composition, mixture, or system that includes two or more different catalyst components, each having a different metal group. The terms "multi-catalyst composition" and "multi-
30 catalyst" include any composition, mixture, or system that includes two or more different catalyst components regardless of the metals. Therefore, the terms "bimetallic catalyst composition," "bimetallic catalyst," "multi-catalyst composition," and "multi-catalyst" will be collectively referred to herein as a "mixed catalyst" unless specifically noted otherwise. In

one example, the mixed catalyst includes at least one metallocene catalyst component and at least one non-metallocene component.

Gas Phase Polymerization

[00101] Generally, in a fluidized gas phase process for producing polymers, a gaseous stream containing one or more monomers is continuously cycled through a fluidized bed in the presence of a catalyst under reactive conditions. The gaseous stream is withdrawn from the fluidized bed and recycled back into the reactor. Simultaneously, polymer product is withdrawn from the reactor and fresh monomer is added to replace the polymerized monomer. Illustrative gas phase polymerization processes can be as discussed and described in US 4,543,399; 4,588,790; 5,028,670; 5,317,036; 5,352,749; 5,405,922; 5,436,304; 5,453,471; 5,462,999; 5,616,661; and 5,668,228.

[00102] The reactor pressure in a gas phase process can vary from 69 kPa to 3,450 kPa, 690 kPa to 3,450 kPa, 1,380 kPa to 2,759 kPa, or 1,724 kPa to 2,414 kPa.

[00103] The reactor temperature in the gas phase process can vary from 30°C to 120°C, preferably from 60°C to 115°C, more preferably in the range of from 70°C to 110°C, and most preferably in the range of from 70°C to 95°C. In another embodiment, when high density polyethylene is desired the reactor temperature is typically between 70°C and about 105°C.

[00104] The productivity of the catalyst or catalyst system in a gas phase system is influenced by the partial pressure of the main monomer. The preferred mole percent of the main monomer, ethylene or propylene, preferably ethylene, is from 25 mol% to 90 mol% and the comonomer partial pressure is from 138 kPa to 5,000 kPa, preferably 517 kPa to 2,069 kPa, which are typical conditions in a gas phase polymerization process. Also in some systems the presence of comonomer can increase productivity.

[00105] In a preferred embodiment, the reactor can be capable of producing more than 227 kilograms polymer per hour (kg/hr) to 90,900 kg/hr or higher, preferably greater than 455 kg/hr, more preferably greater than 4,540 kg/hr, even more preferably greater than 11,300 kg/hr, still more preferably greater than 15,900 kg/hr, still even more preferably greater than 22,700 kg/hr, and preferably greater than 29,000 kg/hr to greater than 45,500 kg/hr, and most preferably over 45,500 kg/hr.

[00106] The polymerization in a stirred bed can take place in one or two horizontal stirred vessels according to the polymerization mode. The reactors can be subdivided into individually gas-composition-controllable and/or polymerization-temperature-controllable

polymerization compartments. With continuous catalyst injection, essentially at one end of the reactor, and powder removal at the other end, the residence time distribution approaches that of plug flow reactor. Preferably the fluorocarbon, if present, is introduced into the first stirred vessel.

5 [00107] Other gas phase processes contemplated by the processes discussed and described herein can include those described in US 5,627,242; 5,665,818; and 5,677,375; and EP-A-0 794 200; EP-A-0 802 202; and EP-B-634 421.

[00108] In another preferred embodiment the catalyst system is in liquid, suspension, dispersion, and/or slurry form and can be introduced into the gas phase reactor into a resin
10 particle lean zone. Introducing a liquid, suspension, dispersion, and/or slurry catalyst system into a fluidized bed polymerization into a particle lean zone can be as discussed and described in US 5,693,727.

[00109] In some embodiments, the gas phase polymerization can operate in the absence of fluorocarbon. In some embodiments, the gas phase polymerization can be conducted in the
15 presence of a fluorocarbon. Generally speaking the fluorocarbons can be used as polymerization media and/or as condensing agents.

Slurry Phase Polymerization

[00110] A slurry polymerization process generally operates at a pressure range between 103 kPa to 5,068 kPa or even greater and a temperature from 0°C to 120°C. In a slurry
20 polymerization, a suspension of solid, particulate polymer is formed in a liquid polymerization diluent medium to which monomer and comonomers along with catalyst are added. The suspension including diluent is intermittently or continuously removed from the reactor where the volatile components are separated from the polymer and recycled, optionally after a distillation, to the reactor. The liquid diluent employed in the
25 polymerization medium is typically an alkane medium having from 3 to 7 carbon atoms, preferably a branched alkane. The medium employed can be liquid under the conditions of polymerization and relatively inert. When a propane medium is used the process can be operated above the reaction diluent critical temperature and pressure. Preferably, a hexane or an isobutane medium is employed.

30 [00111] In one embodiment, a preferred polymerization technique, referred to as a particle form polymerization or a slurry process, can include maintaining the temperature below the temperature at which the polymer goes into solution. Such technique is well known in the art, and can be as discussed and described in US 3,248,179. The preferred temperature in the

particle form process can be from 20°C to 110°C. Two preferred polymerization processes for the slurry process can include those employing a loop reactor and those utilizing a plurality of stirred reactors in series, parallel, or combinations thereof. Non-limiting examples of slurry processes include continuous loop or stirred tank processes. Also, other
5 examples of slurry processes can be as discussed and described in US 4,613,484.

[00112] In another embodiment, the slurry process can be carried out continuously in a loop reactor. The catalyst, as a slurry in mineral oil and/or paraffinic hydrocarbon or as a dry, free flowing powder, can be injected regularly to the reactor loop, which can be filled with a circulating slurry of growing polymer particles in a diluent containing monomer and
10 comonomer. Hydrogen, optionally, can be added as a molecular weight control. The reactor can be operated at a pressure of 3,620 kPa to 4,309 kPa and at a temperature from 60°C to 115°C depending on the desired polymer melting characteristics. Reaction heat can be removed through the loop wall since much of the reactor is in the form of a double-jacketed pipe. The slurry is allowed to exit the reactor at regular intervals or continuously to a heated
15 low pressure flash vessel, rotary dryer, and a nitrogen purge column in sequence for removal of the diluent and at least a portion of any unreacted monomer and/or comonomers. The resulting hydrocarbon free powder can be compounded for use in various applications.

[00113] The reactor used in the slurry process can produce greater than 907 kg/hr, more preferably greater than 2,268 kg/hr, and most preferably greater than 4,540 kg/hr polymer. In
20 another embodiment the slurry reactor can produce greater than 6,804 kg/hr, preferably greater than 11,340 kg/hr to 45,500 kg/hr. The reactor used in the slurry process can be at a pressure from 2,758 kPa to 5,516 kPa, preferably 3,103 kPa to 4,827 kPa, more preferably from 3,448 kPa to 4,482 kPa, most preferably from 3,620 kPa to 4,309 kPa.

[00114] The concentration of the predominant monomer in the reactor liquid medium in
25 the slurry process can be from 1 wt% to 30 wt%, preferably from 2 wt% to 15 wt%, more preferably from 2.5 wt% to 10 wt%, most preferably from 3 wt% to 20 wt%.

[00115] In one or more embodiments, the slurry and/or gas phase polymerization can be operated in the absence of or essentially free of any scavengers, such as triethylaluminum, trimethylaluminum, tri-isobutylaluminum and tri-n-hexylaluminum and diethyl aluminum
30 chloride, dibutyl zinc and the like. Operation of the slurry and /or gas phase reactors in the absence or essentially free of any scavengers can be as discussed and described in WO 96/08520 and US 5,712,352. In another embodiment the polymerization processes can be run with scavengers. Typical scavengers include trimethyl aluminum, tri-ethyl aluminum, tri-

isobutyl aluminum, tri-n-octyl aluminum, and an excess of alumoxane and/or modified alumoxane.

[00116] In some embodiments, the slurry phase polymerization can operate in the absence of a fluorocarbon. In some embodiments, the slurry phase polymerization can be conducted
5 in the presence of a fluorocarbon. Generally speaking the fluorocarbons can be used as polymerization media.

Solution Phase Polymerization

[00117] As used herein, the phrase "solution phase polymerization" refers to a polymerization system where the polymer produced is soluble in the polymerization medium.
10 Generally this involves polymerization in a continuous reactor in which the polymer formed and the starting monomer and catalyst materials supplied, are agitated to reduce or avoid concentration gradients and in which the monomer acts as a diluent or solvent or in which a hydrocarbon is used as a diluent or solvent. Suitable processes typically operate at temperatures from 0°C to 250°C, preferably from 10°C to 150°C, more preferably from 40°C
15 to 140°, more preferably from 50°C to 120°C and at pressures of 0.1 MPa or more, preferably 2 MPa or more. The upper pressure limit is not critically constrained but typically can be 200 MPa or less, preferably, 120 MPa or less. Temperature control in the reactor can generally be obtained by balancing the heat of polymerization and with reactor cooling by reactor jackets or cooling coils to cool the contents of the reactor, auto refrigeration, pre-chilled feeds,
20 vaporization of liquid medium (diluent, monomers or solvent) or combinations of all three. Adiabatic reactors with pre-chilled feeds can also be used. The purity, type, and amount of solvent can be optimized for the maximum catalyst productivity for a particular type of polymerization. The solvent can be also introduced as a catalyst carrier. The solvent can be introduced as a gas phase or as a liquid phase depending on the pressure and temperature.
25 Advantageously, the solvent can be kept in the liquid phase and introduced as a liquid. Solvent can be introduced in the feed to the polymerization reactors.

[00118] In a preferred embodiment, the polymerization process can be described as a continuous, non-batch process that, in its steady state operation, is exemplified by removal of amounts of polymer made per unit time, being substantially equal to the amount of polymer
30 withdrawn from the reaction vessel per unit time. By "substantially equal" we intend that these amounts, polymer made per unit time, and polymer withdrawn per unit time, are in ratios of one to other, of from 0.9:1; or 0.95:1; or 0.97:1; or 1:1. In such a reactor, there will be a substantially homogeneous monomer distribution.

[00119] Preferably in a continuous process, the mean residence time of the catalyst and polymer in the reactor generally can be from 5 minutes to 8 hours, and preferably from 10 minutes to 6 hours, more preferably from 10 minutes to 1 hour. In some embodiments, comonomer (such as ethylene) can be added to the reaction vessel in an amount to maintain a differential pressure in excess of the combined vapor pressure of the main monomer (such as a propylene) and any optional diene monomers present.

[00120] In another embodiment, the polymerization process can be carried out at a pressure of ethylene of from 68 kPa to 6,800 kPa, most preferably from 272 to 5,440 kPa). The polymerization is generally conducted at a temperature of from 25°C to 250°C, preferably from 75°C to 200°C, and most preferably from 95°C to 200°C.

[00121] The addition of a small amount of hydrocarbon to a typical solution phase process can cause the polymer solution viscosity to drop and or the amount of polymer solute to increase. Addition of a larger amount of solvent in a traditional solution process can cause the separation of the polymer into a separate phase (which can be solid or liquid, depending on the reaction conditions, such as temperature or pressure).

[00122] The processes discussed and described herein can be carried out in continuous stirred tank reactors, batch reactors, or plug flow reactors. One reactor can be used even if sequential polymerizations are being performed, preferably as long as there is separation in time or space of the two reactions. Likewise two or more reactors operating in series or parallel can also be used. These reactors can have or not have internal cooling and the monomer feed may or may not be refrigerated. See the general disclosure of US 5,001,205 for general process conditions. See also, WO 96/33227 and WO 97/22639.

[00123] In another embodiment, a sequential polymerization process is used and the first polymerization is a slurry process to produce homopolymer followed by another slurry reactor for impact copolymer production. Impact copolymers can be produced by first making homopolypropylene in a slurry reactor, and transferring the homopolypropylene to another slurry reactor where copolymers are produced with the presence of homopolypropylene. Fluorocarbon can be introduced into the first reactor, the second reactor or both.

[00124] In another embodiment, the two (or more) polymerizations can occur in the same reactor but in different reaction zones. For example, another preferred embodiment is process to prepare impact copolymers comprising producing a semi-crystalline polymer in a first reaction zone and then transferring the semi-crystalline polymer to a second reaction zone

where a low crystallinity polymer can be produced in the presence of the semi-crystalline polymer.

[00125] In any of the embodiments above the first reactor and second reactor can be reaction zones in the same reactor. Reactors where multiple reaction zones are possible
5 include Spherizone™ type reactors and those described in US 6,413,477.

[00126] In a particular embodiment, the impact copolymer can be produced *in situ* within three reactors, where a first polypropylene is produced in a first reactor, a second polypropylene is produced in a second reactor, and the ethylene copolymer or elastomeric polymer is produced in a third reactor, with each reactor associated in series. In another
10 particular embodiment, the impact copolymer can be produced *in situ* within three reactors, where the first polypropylene is produced in the first reactor with a first catalyst composition and the second polypropylene is produced in the second reactor with a second catalyst composition, where the first and second catalyst compositions differ from one another, and the elastomeric polymer is produced in the third reactor, each reactor associated in series.

[00127] In a particular embodiment, the first and second reactors can be slurry-loop reactors and the third reactor can be a gas phase reactor. The first and second reactors can produce the polypropylenes, homopolymers in a particular embodiment, and the gas phase reactor can produce the ethylene copolymer or elastomeric polymer, thus creating an *in situ* blend of the ethylene copolymer in the polypropylene matrix. The impact copolymer can
20 include from a low of 30 wt%, 35 wt%, or 40 wt% to a high of 60 wt%, 65 wt%, or 70 wt% of the first polypropylene, based on the total weight of the impact copolymer. The impact copolymer can also include from a low of 10 wt%, 15 wt%, or 20 wt% to a high of 30 wt%, 35 wt%, or 40 wt% of the second polypropylene, based on the total weight of the impact copolymer. The impact copolymer can also include from a low of 15 wt%, 20 wt%, or 22
25 wt% to a high of 26 wt%, 30 wt%, or 35 wt% of the ethylene copolymer, based on the total weight of the impact copolymer. These amounts can be achieved, in the case where one or more reactors is used to produce the propylene impact copolymer, by any suitable means known to those skilled in the art including control of the residence time in each stage and/or reactor, the amount and/or particular catalyst composition(s), variation in the reactants in
30 each stage and/or reactor (*i.e.*, propylene, comonomer, hydrogen, etc. concentrations), combinations of these, and/or any other means.

[00128] The catalyst composition can be modified by changing the identity and/or amount of the transition metal component or the electron donors and/or co-catalysts used in

conjunction with the transition metal component. A desirable catalyst composition arrangement can be as discussed and described in WO99/20663A2, where sequential electron donors are used to modify the catalyst composition from one reactor to another, the sequential donors being different compounds or mixtures of compounds. For example, a
5 titanium-magnesium based Ziegler-Natta catalyst can be used in all of the reactors, the same titanium-magnesium composition in a particular embodiment, but the aluminum-alkoxy/alkyl "electron donor" compound used in the first reactor can be different than the aluminum-alkoxy/alkyl compound used in the second reactor. Alternatively, the ratio of a mixture of aluminum-alkoxy/alkyl compounds can be changed in going from the first to the second
10 reactor. In this manner, the isotacticity and/or MFR of the first and second polypropylenes can be tailored.

[00129] In embodiments where one or more reactors are used to produce the impact copolymer(s), one or more chain terminating agent(s) (*e.g.*, hydrogen) can be used to control the MFR (molecular weight) of the polypropylene(s). The chain terminating agents can be
15 used as a means of adjusting the MFR of components of the impact copolymer either alone or in conjunction with other means. In a particular embodiment, the process of producing the impact copolymer can include contacting a catalyst with propylene, a first amount of a chain terminating agent, and optionally one or more comonomers, *e.g.*, ethylene and/or C4 to C12 α -olefins, in a first reactor to form a first polypropylene comprising no more than 5 wt% of
20 ethylene and/or α -olefin derived units, based on the weight of the first polypropylene. The catalyst and the first polypropylene can be contacted with propylene, a second amount of a chain terminating agent, and optionally one or more comonomers, *e.g.*, ethylene and/or C4 to C12 α -olefins in a second reactor to form a second polypropylene comprising no more than 5 wt% of ethylene and/or α -olefin derived units, based on the weight of the second
25 polypropylene. The second amount of chain terminating agent can be greater than the first amount of chain terminating agent. Finally, the catalyst composition, the first polypropylene, and the second polypropylene can be contacted with propylene and ethylene in a third reactor to form an ethylene-propylene copolymer that includes from 35 wt% or 40 wt% or 45 wt% to 60 wt% or 65 wt%, or 70 wt% ethylene-derived units, based on the weight of the impact
30 copolymer.

[00130] The first amount of the chain terminating agent can be added to the one or more reactors and/or one or more stages within the reactor(s) such that the first polypropylene has an MFR₁ from a low of 8 dg/min, 15 dg/min, or 18 dg/min to a high of 33 dg/min, 35 dg/min,

or 40 dg/min. The second amount of chain terminating agent can be added (in certain embodiments) such that the second polypropylene has an MFR_2 from a low of 50 dg/min, 65 dg/min, or 70 dg/min to a high of 100 dg/min, 120 dg/min, or 190 dg/min. Described another way, the second amount of chain terminating agent (in certain embodiments) can be greater than the first amount of chain terminating agent such that the MFR_1 of the first polypropylene is at least 30% less, at least 35% less, at least 40% less, at least 45% less, or at least 50% less than the MFR_2 of the second polypropylene. Stated in yet another way, the chain terminating agent(s) can be added to the reactor(s) such that MFR_2/MFR_1 is from a low of 2, 2.5, or 3 to a high of 4, 4.5, 5, or 6 in certain embodiments, and greater than 1.5, greater than 2.0, greater than 2.5, or greater than 3 in other embodiments. The amount of chain terminating agent can be varied by any suitable means in the reactor(s), and in one embodiment the amount of the first chain terminating agent can be less than 2,000 mol ppm or less than 1,800 mol ppm as measured in the first propylene feed to the reactor, and the amount of the second chain terminating agent can be greater than 2,500 mol ppm or greater than 2,800 mol ppm as measured in the second propylene feed to the reactor.

[00131] In certain embodiments of the three reactor process, catalyst components, propylene, chain terminating agent, and any other optional monomers can be fed to a first loop reactor for a first homopolymerization or copolymerization process. The high heat removal capability of the loop reactor can cause or facilitate turbulent mixing of the slurry and the large surface-to-volume ratio of the reactor can enable high specific outputs. Operating conditions are typically in the range of 60°C to 80°C, 500 psi to 700 psi, and an amount of chain terminating agent, hydrogen in a preferred embodiment, of less than 2,000 mol ppm or less than 1,800 mol ppm as measured in the propylene feed to the reactor, and within the range from 1,000 mol ppm, 1,100 mol ppm, or 1,200 mol ppm to 1,800 mol ppm, or 2,000 mol ppm in another embodiment. The polymer produced from the first reactor (along with residual chain terminating agent and monomers) can be transferred to a second loop reactor where the operating conditions can be the same or different with respect to the first loop reactor. Additional monomer, chain terminating agent, and optional comonomer can be added also. In a particular embodiment, at least the amount of the second chain terminating agent will be different, where the amount of chain terminating agent, hydrogen in a preferred embodiment, is greater than 2,500 mol ppm or greater than 2,800 mol ppm as measured in the propylene feed to the second reactor, and within the range of 2,500 mol ppm,

3,000 mol ppm, or 3,400 mol ppm to 3,600 mol ppm, or 4,000 mol ppm in another embodiment.

[00132] Upon exiting the second loop reactor, the polypropylene slurry can be depressurized and flashed at a pressure that allows for recycle of the vaporized monomer(s) by condensation using cooling water or other cooling means, and can be sufficient for gas phase polymerization. The polypropylene and catalyst composition mixture can be transferred to a gas phase reactor. The ethylene copolymer or elastomeric polymer can be produced within this gas phase reactor in certain embodiments. The ethylene copolymer, an ethylene-propylene copolymer in a preferred embodiment, can be produced in a particular embodiment by use of a fluidized bed gas phase reactor operating at a temperature from a low of 50°C, 60°C, or 70°C to a high of 80°C, 90°C, 100°C, 110°C, or 120°C, and pressures from a low of 100 psi, 125 psi, or 150 psi to a high of 200 psi, 250 psi, or 300 psi. Polymer exiting the polymerization section can pass through a low pressure separator, in which the remaining monomer can be separated for recycle. A steam treatment vessel for deactivation of the residual catalyst can present in certain embodiments. A small fluid bed dryer or other drying means can also be present. An example of such a process can include the so called "Spheripol" reactor process.

[00133] The catalyst composition can be any suitable catalyst composition known for polymerizing olefins to produce polyolefins and is desirably a composition that can control the isotacticity of the polymers that are produced. Non-limiting examples of suitable catalysts compositions include Ziegler-Natta catalysts, metallocene catalysts, chromium catalysts, metal-imide/amine coordination catalysts, and combinations of such catalysts each with its desirable co-catalyst and/or electron donor or other modifying agent known in the art. An example of certain desirable catalyst compositions can be as discussed and described in WO99/20663, *e.g.*, a Ziegler-Natta catalyst composition using any one of a combination of aluminum alkyl donor systems. The selection of other conditions for producing the individual impact copolymer components and the whole propylene impact copolymer is reviewed by, for example, G. DiDrusco and R. Rinaldi in "Polypropylene-Process Selection Criteria" in HYDROCARBON PROCESSING 113 (November 1984), and references cited therein.

[00134] In a preferred embodiment, a sequential polymerization process can be used and the first polymerization can be a slurry process to produce homopolymer followed by a gas-phase process for producing the impact copolymer. The slurry process can be a loop reactor

or a CSTR type of reactor. In a loop reactor, the first reaction stage can include one or two tubular loop reactors where bulk polymerization of homopolymers can be carried out in liquid propylene. The catalyst, *e.g.*, a prepolymerized catalyst, and liquid propylene, and hydrogen for controlling molecular weight can be fed into the reactor. The homopolymer in liquid propylene inside the loops can be continuously discharged to a separation unit. Unreacted propylene can be recycled to the reaction medium while the polymer can be transferred to one or two gas phase reactors where ethylene, propylene, and hydrogen can be added to produce the impact copolymers. The granules can be discharged to the monomer flashing and recovery section and sent to a monomer stripping system. After the drying unit, the granular resin can be conveyed to an extrusion system for stabilization, and pelletization.

Examples

[00135] In order to provide a better understanding of the foregoing discussion, the following non-limiting examples are offered. Although the examples may be directed to specific embodiments, they are not to be viewed as limiting the invention in any specific respect. All parts, proportions, and percentages are by weight unless otherwise indicated.

Example I

[00136] A first series of impact copolymers were prepared with and without a halocarbon present during polymerization of the ethylene copolymer. For comparative examples C1-C3 no halocarbon was present during polymerization. For inventive examples Ex. 1-4 a halocarbon was present during polymerization. The halocarbon used in Examples 1-3 was a 10 wt% mixture of chlorocyclohexane in hexane. The halocarbon used in Ex. 4 was a 0.1 wt% mixture of 1,4-dichlorobutane in hexane.

[00137] The impact copolymers were prepared according to the following procedure. In a 2L slurry phase stainless steel reactor 2 mL of a 5 wt% solution of catalyst donor (approximately 5 wt% dicyclopentylmethoxysilane and 95 wt% n-propyltriethoxysilane) in hexane and 2 mL of triethyl aluminum (TEAL) were added at room temperature and atmospheric pressure (0.10 MPa). Thereafter, a charge of 1.82 MPa to 2.51 MPa of hydrogen was introduced into the reactor (range of hydrogen was based on desired set point). A magnesium chloride supported titanium Ziegler-Natta catalyst, which was a THC-C type catalyst solid system from Toho Titanium Corporation of Japan, was used for these experiments.

[00138] For all examples, 250 mL of a 5 wt% solution of magnesium chloride supported titanium Ziegler-Natta catalyst in mineral oil was charged through a catalyst tube with 1,000

mL of propylene into the reactor. A stirrer was used to keep the reaction mixture well mixed at 300-400 rpm, and the reaction was allowed to proceed for 5 minutes at room temperature. The reactor was heated to 70°C and the pressure was allowed to build to a range of 3.48 MPa to 3.67 MPa. The reaction was allowed to proceed for 25 minutes.

5 **[00139]** The reaction mass, *i.e.*, polypropylene homopolymer, unreacted propylene and Ziegler-Natta catalyst, was transferred to a 2 liter stainless steel gas phase reactor and the reactor's stirrer was started to keep the reaction mixture well mixed at 400-450 rpm. The pressure was allowed to build to 1.48 MPa at room temperature and the reactor was heated to 70°C. After reaching temperature, a 0.38 MPa to 0.65 MPa charge of hydrogen was
10 introduced to the reactor through tubing. Thereafter, various amounts of a halocarbon compound dissolved in hexane were charged into the reactor from a catalyst tube using a charge of ethylene through the tubing. The two halocarbon compounds used were a 10 wt% solution of chlorocyclohexane (CCH) in hexane and a 0.1 wt% solution of 1,4-dichlorobutane (1,4-DB) in hexane. The amount of the halocarbon compound present during polymerization
15 of the ethylene-propylene copolymer is shown in Table 1. Ethylene was then charged into the reactor until the pressure reached 1.96 MPa through the same tubing. Ethylene was added throughout the reaction to maintain a pressure of 1.96 MPa. Propylene was added throughout the run as needed through a pump to maintain the desired ethylene mol% gas phase composition. The reaction was allowed to run for 30 minutes and was quenched by lowering
20 the reactor heat, stopping the feeds to the reactor, and de-pressuring the reactor. The end products from these reactions were impact copolymers having a polypropylene polymer component and an ethylene-propylene copolymer.

[00140] Figure 1 depicts a graphical comparison of the catalyst activity during gas phase polymerization of the ethylene-propylene copolymer component without any halocarbon (comparative example C1, C2, C3) and with CCH present (inventive example Ex. 1,2,3). The
25 concentration of the CCH in the polymerization reactor for Ex. 1, 2 and 3 was 50 mg/L. As shown in Figure 1, the presence of chlorocyclohexane provided a surprising and unexpected increase in the catalyst activity. More particularly, Figure 1 depicts the increase in catalyst activity (shown by the instantaneous polymerization rate in grams per minute) with minimal deactivation with the addition of CCH compared to the comparative case without a
30 halocarbon. The calculated instantaneous polymerization rate for Example 1, which remained substantially constant during the monitored time, was 1.6 g/min. In contrast, the calculated instantaneous polymerization rate for the comparative example C1 peaked at 1

g/min at an elapsed time of 5 minutes and steadily declined during the remaining time the polymerization was monitored.

[00141] The data from the CCH (Ex. 1-3) and 1,4-DB (Ex. 4) experimental cases compared to the comparative examples (C1-C3) are shown in Table 1 below. These experiments were designed to test the effect the addition of a halocarbon had on the catalyst activity and the ethylene-propylene rubber content of impact copolymers formed in the presence of the halocarbon. For a gas phase reactor ethylene concentration of 30 mol%, the homopolymer melt flow rate was varied to quantify the effect of the addition of halocarbon on EP rubber content across this range. The gas phase reactor ethylene concentration was also varied from approximately 30 mol% to 55 mol% to quantify the effect of the addition of halocarbon on EP rubber content across this range. The halocarbon concentration shown in Table 2 correspond to approximately 250 mg/mole of ethylene for Examples 1, 2 and 3 and approximately 500 mg/mole of ethylene for example 4.

Table 1: Effect of Halocarbon Addition on the Ethylene-Propylene Copolymer Content						
Example	Halocarbon	Halocarbon Amount (mg)	HPP Melt Flow Rate (dg/min)	Gas Phase Reactor Ethylene Content (mol%)	GPR H ₂ (mol%)	E-P Copolymer Content (wt%)
C1	None	0	70.2	30.0	2.0	21.1
C2	None	0	200.8	29.0	1.7	13.0
C3	None	0	70.9	55.4	3.3	29.0
Ex. 1	CCH	100	72.9	30.0	2.1	25.7
Ex. 2	CCH	100	180.4	30.0	2.5	19.2
Ex. 3	CCH	100	66.0	56.0	1.7	40.8
Ex. 4	1,4-DB	200	72.6	29.0	1.9	22.7

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[00142] As shown in Table 1, at a given homopolymer melt flow rate (HPP MFR) and gas phase reactor ethylene concentration, the ethylene-propylene rubber content for the examples that included the addition of CCH or 1,4-DB significantly exceeded that for the examples in which no halocarbon was present. Figure 2 shows the data for comparative examples C1 and C2 and inventive examples Ex. 1 and Ex. 2 in graphical form. Also, as shown in Table 1, when compared to one another, the CCH examples exhibited a higher ethylene-propylene

20

rubber content than the 1,4-DB case at the same HPP MFR and gas phase reactor ethylene concentration.

[00143] Also shown in Table 1, at an increased concentration of ethylene of approximately 55 mol% in the gas phase reactor, the ethylene-propylene rubber content of the impact copolymer remained higher with the addition of CCH compared to the comparative example without the presence of the halocarbon. Figures 3 shows this data in graphical form.

Example II

[00144] A second series of impact copolymers were prepared with and without the presence of a halocarbon compound during polymerization. For comparative examples C4-10 C7 no halocarbon compound was present during polymerization. For inventive examples Ex. 5-8 a halocarbon compound was present during polymerization and was the same 10 wt% mixture of CCH in hexane as used in Example I above. The impact copolymers of comparative examples C4-C7 and Ex. 5-8 were prepared according to the same procedure used in Example 1.

[00145] The addition of a halocarbon to the gas phase reactor allowed the production of impact copolymers that had a relatively high ethylene propylene rubber content at a relatively high homopolymer melt flow rate compared to the comparative examples without the halocarbon. As shown in Figure 4, upon addition of a halocarbon to the gas phase reactor, an increase in the ethylene content in the ethylene-propylene rubber was observed as compared to the comparative examples that did not include the halocarbon. Table 2 below shows the data for examples that were produced via gas phase polymerization of the ethylene-propylene copolymer component without any halocarbon (comparative example C4-C7) and with chlorocyclohexane present (inventive examples Ex. 5-8). The hydrogen concentration during the polymerization was approximately 5 mol% in the slurry phase reactor during production of the hPP, the hydrogen concentration was approximately 2 mol% gas phase reactor, and the homopolymer melt flow rate was approximately 60-75.

Table 2: The Effect of Cyclochlorohexane (CCH) on EP Rubber Chemical Composition			
Example	Halocarbon	Gas Phase Reactor Ethylene (mol%)	Ethylene Content in the Ethylene Copolymer (wt%)
C4	None	23	48.3
Ex. 5	chlorocyclohexane	23	55.1
C5	None	29	61.7

Ex. 6	chlorocyclohexane	30	85.9
C6	None	35	73.6
Ex. 7	chlorocyclohexane	36	82.0
C7	None	46	83.2
Ex. 8	chlorocyclohexane	48	95.6

[00146] As shown from the data in Table 2, the addition of the halocarbon to the gas phase reactor has the ability to influence the chemical composition of the ethylene-propylene rubber in impact copolymers. More particularly, the addition of the halocarbon can significantly increase the ethylene content of the impact copolymer as compared to when the halocarbon is not present. The data in Table 2 is also graphically depicted in Figure 5.

Experimental Test Methods

[00147] All molecular weights are number average in g/mol unless otherwise noted. Unless otherwise noted, physical and chemical properties described herein are measured using the following test methods.

Dynamic Mechanical Analysis (DMA)

[00148] The glass transition temperature (T_g) is measured using dynamic mechanical analysis. This test provides information the small-strain mechanical response of a sample as a function of temperature over a temperature range that includes the glass transition region and the visco-elastic region prior to melting. Specimens are tested using a commercially available DMA instrument (*e.g.*, TA Instruments DMA 2980 or Rheometrics RSA) equipped with a dual cantilever test fixture. The specimen is cooled to -130°C then heated to 60°C at a heating rate of $2^{\circ}\text{C}/\text{min}$ while subjecting to an oscillatory deformation at 0.1% strain and a frequency of 1 rad/sec. The output of these DMA experiments is the storage modulus (E') and loss modulus (E''). The storage modulus measures the elastic response or the ability of the material to store energy, and the loss modulus measures the viscous response or the ability of the material to dissipate energy. The ratio of E''/E' , called Tan-delta, gives a measure of the damping ability of the material; peaks in Tan-delta are associated with relaxation modes for the material. T_g is defined to be the peak temperature associated with the β -relaxation mode, which typically occurs in a temperature range of -80 to $+20^{\circ}\text{C}$ for polyolefins. In a hetero-phase blend, separate β -relaxation modes for each blend component can cause more than one T_g to be detected for the blend; assignment of the T_g for each

component are preferably based on the T_g observed when the individual components are similarly analyzed by DMA (although slight temperature shifts are possible).

Differential Scanning Calorimetry (DSC)

[00149] Crystallization temperature (T_c) and melting temperature (or melting point, T_m) are measured using Differential Scanning Calorimetry (DSC) on a commercially available instrument (e.g., TA Instruments 2920 DSC). Typically, 6 to 10 mg of molded polymer or plasticized polymer are sealed in an aluminum pan and loaded into the instrument at room temperature. Melting data (first heat) is acquired by heating the sample to at least 30°C above its melting temperature, typically 220°C for polypropylene, at a heating rate of 10°C/min. The sample is held for at least 5 minutes at this temperature to destroy its thermal history. Crystallization data are acquired by cooling the sample from the melt to at least 50°C below the crystallization temperature, typically -50°C for polypropylene, at a cooling rate of 20°C/min. The sample is held at this temperature for at least 5 minutes, and finally heated at 10°C/min to acquire additional melting data (second heat). The endothermic melting transition (first and second heat) and exothermic crystallization transition are analyzed according to standard procedures. The melting temperatures reported are the peak melting temperatures from the second heat unless otherwise specified.

[00150] For polymers displaying multiple peaks, the melting temperature is defined to be the peak melting temperature from the melting trace associated with the largest endothermic calorimetric response (as opposed to the peak occurring at the highest temperature). Likewise, the crystallization temperature is defined to be the peak crystallization temperature from the crystallization trace associated with the largest exothermic calorimetric response (as opposed to the peak occurring at the highest temperature).

[00151] Areas under the DSC curve are used to determine the heat of transition (heat of fusion, H_f , upon melting or heat of crystallization, H_c , upon crystallization), which can be used to calculate the degree of crystallinity (also called the percent crystallinity). The percent crystallinity ($X\%$) is calculated using the formula: [area under the curve (in J/g) / H° (in J/g)] * 100, where H° is the ideal heat of fusion for a perfect crystal of the homopolymer of the major monomer component. These values for H° are to be obtained from the *Polymer Handbook, Fourth Edition*, published by John Wiley and Sons, New York 1999, except that a value of 290 J/g is used for H° (polyethylene), a value of 140 J/g is used for H° (polybutene), and a value of 207 J/g is used for H° (polypropylene).

Size-Exclusion Chromatography (SEC)

[00152] Molecular weight (weight-average molecular weight, M_w , number-average molecular weight, M_n , and molecular weight distribution, M_w/M_n or MWD) are determined using a commercial High Temperature Size Exclusion Chromatograph (e.g., from Waters Corporation or Polymer Laboratories) equipped with three in-line detectors: a differential refractive index detector (DRI), a light scattering (LS) detector, and a viscometer.

[00153] The following approach is used for polyolefins. Details not described, including detector calibration, can be found in *Macromolecules* 34, pp. 6812-6820 (2001). Column set: 3 Polymer Laboratories PLgel 10mm Mixed-B columns; Flow rate: 0.5 mL/min; Injection volume: 300 μ L; Solvent: 1,2,4-trichlorobenzene (TCB), containing 6 g of butylated hydroxy toluene dissolved in 4 liters of Aldrich reagent grade TCB.

[00154] The various transfer lines, columns, DRI detector and viscometer are contained in an oven maintained at 135°C. The TCB solvent is filtered through a 0.7 μ m glass pre-filter and subsequently through a 0.1 μ m Teflon filter, then degassed with an online degasser before entering the SEC. Polymer solutions are prepared by placing dry polymer in a glass container, adding the desired amount of TCB, then heating the mixture at 160°C with continuous agitation for 2 hours. All quantities are measured gravimetrically. The TCB densities used to express the polymer concentration in mass/volume units are 1.463 g/mL at room temperature and 1.324 g/mL at 135°C. Injection concentration range from 1.0 to 2.0 mg/mL, with lower concentrations being used for higher molecular weight samples. Prior to running a set of samples, the DRI detector and injector are purged, the flow rate increased to 0.5 mL/min, and the DRI allowed to stabilize for 8-9 hours; the LS laser is turned on 1 hr before running samples.

[00155] The concentration, c , at each point in the chromatogram is calculated from the baseline-subtracted DRI signal, I_{DRI} , using the following equation:

$$c = K_{DRI} I_{DRI} / (dn/dc)$$

where K_{DRI} is a constant determined by calibrating the DRI, and (dn/dc) is the same as described below for the light scattering (LS) analysis. Units on parameters throughout this description are such that concentration is expressed in g/mL, molecular weight is expressed in g/mol, and intrinsic viscosity is expressed in dL/g.

[00156] The LS detector is a Wyatt Technology High Temperature mini-DAWN. The molecular weight, M , at each point in the chromatogram is determined by analyzing the LS

output using the Zimm model for static light scattering (M.B. Huglin, LIGHT SCATTERING FROM POLYMER SOLUTIONS, Academic Press, 1971):

$$\frac{K_o c}{\Delta R(\theta)} = \frac{1}{MP(\theta)} + 2A_2 c$$

where $\Delta R(\theta)$ is the measured excess Rayleigh scattering intensity at scattering angle θ , c is the polymer concentration determined from the DRI analysis, A_2 is the second virial coefficient ($A_2 = 0.0006$ for propylene polymers and 0.001 otherwise), M is molecular weight, $P(\theta)$ is the form factor for a monodisperse random coil, and K_o is the optical constant for the system:

$$K_o = \frac{4\pi^2 n^2 (dn/dc)^2}{\lambda^4 N_A}$$

where N_A is Avogadro's number, and (dn/dc) is the refractive index increment for the system. The refractive index, $n = 1.500$ for TCB at 135°C and $\lambda = 690$ nm. $(dn/dc) = 0.104$ for propylene polymers and 0.1 otherwise.

[00157] A high temperature Viscotek Corporation viscometer, which has four capillaries arranged in a Wheatstone bridge configuration with two pressure transducers, is used to determine specific viscosity. One transducer measures the total pressure drop across the detector, and the other, positioned between the two sides of the bridge, measures a differential pressure. The specific viscosity, η_s , for the solution flowing through the viscometer is calculated from their outputs. The intrinsic viscosity, $[\eta]$, at each point in the chromatogram is calculated from the following equation:

$$\eta_s = c[\eta] + 0.3(c[\eta])^2$$

where c is concentration and was determined from the DRI output.

[00158] The branching index (g') is calculated using the output of the SEC-DRI-LS-VIS method as follows. The average intrinsic viscosity, $[\eta]_{\text{avg}}$, of the sample is calculated by

$$[\eta]_{\text{avg}} = \frac{\sum c_i [\eta]_i}{\sum c_i}$$

where the summations are over the chromatographic slices, i , between the integration limits. The branching index g' is defined as:

$$g' = \frac{[\eta]_{\text{avg}}}{kM_v^\alpha}$$

where, $\alpha = 0.695$ for ethylene, propylene, and butene polymers; and $k = 0.000579$ for ethylene polymers, $k = 0.000262$ for propylene polymers, and $k = 0.000181$ for butene polymers. M_v is the viscosity-average molecular weight based on molecular weights
 5 determined by LS analysis.

¹³C-NMR Spectroscopy on Polyolefins

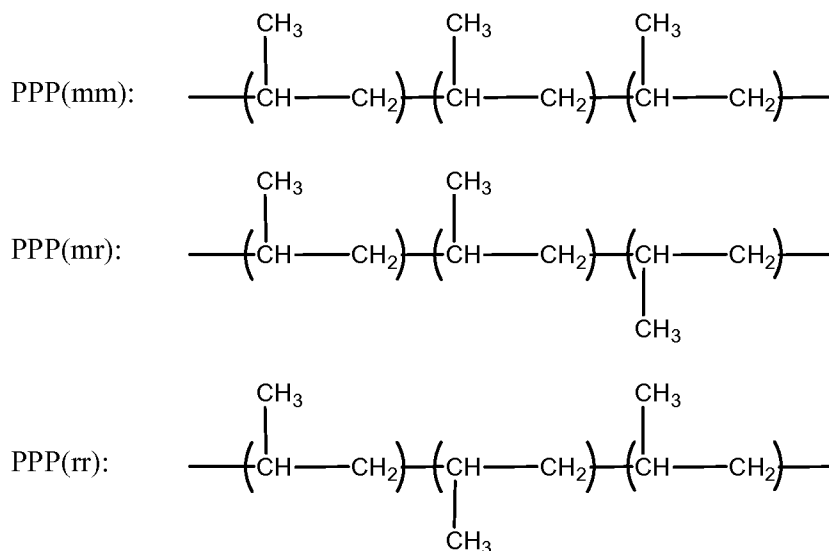
[00159] Polypropylene microstructure is determined by ¹³C-NMR spectroscopy, including the concentration of isotactic and syndiotactic diads ([m] and [r]), triads ([mm] and [rr]), and pentads ([mmmm] and [rrrr]). The designation "m" or "r" describes the stereochemistry of
 10 pairs of contiguous propylene groups, "m" referring to meso and "r" to racemic. Samples are dissolved in d₂-1,1,2,2-tetrachloroethane, and spectra recorded at 125°C using a 100 MHz (or higher) NMR spectrometer. Polymer resonance peaks are referenced to mmmm = 21.8 ppm. Calculations involved in the characterization of polymers by NMR are described by F. A. Bovey in POLYMER CONFORMATION AND CONFIGURATION (Academic Press, New York 1969)
 15 and J. Randall in POLYMER SEQUENCE DETERMINATION, ¹³C-NMR METHOD (Academic Press, New York, 1977).

[00160] The "propylene tacticity index", expressed herein as [m/r], is calculated as defined in H.N. Cheng, *Macromolecules*, 17, p. 1950 (1984). When [m/r] is 0 to less than 1.0, the polymer is generally described as syndiotactic, when [m/r] is 1.0 the polymer is atactic, and
 20 when [m/r] is greater than 1.0 the polymer is generally described as isotactic.

[00161] The "mm triad tacticity index" of a polymer is a measure of the relative isotacticity of a sequence of three adjacent propylene units connected in a head-to-tail configuration. More specifically, the mm triad tacticity index (also referred to as the "mm Fraction") of a polypropylene homopolymer or copolymer is expressed as the ratio of the
 25 number of units of meso tacticity to all of the propylene triads in the copolymer:

$$\text{mm Fraction} = \frac{\text{PPP}(\text{mm})}{\text{PPP}(\text{mm}) + \text{PPP}(\text{mr}) + \text{PPP}(\text{rr})}$$

where PPP(mm), PPP(mr) and PPP(rr) denote peak areas derived from the methyl groups of the second units in the possible triad configurations for three head-to-tail propylene units, shown below in Fischer projection diagrams:



[00162] The calculation of the mm Fraction of a propylene polymer is described in US 5,504,172 (homopolymer: column 25, line 49 to column 27, line 26; copolymer: column 28, line 38 to column 29, line 67). For further information on how the mm triad tacticity can be determined from a ^{13}C -NMR spectrum, see 1) J. A. Ewen, CATALYTIC POLYMERIZATION OF OLEFINS: PROCEEDINGS OF THE INTERNATIONAL SYMPOSIUM ON FUTURE ASPECTS OF OLEFIN POLYMERIZATION, T. Keii and K. Soga, Eds. (Elsevier, 1986), pp. 271-292; and 2) US 2004/054086 (claims [0043] to [0054]).

[00163] Ethylene content in ethylene copolymers is determined by ASTM D 5017-96, except that the minimum signal-to-noise should be 10,000:1. Propylene content in propylene copolymers is determined by following the approach of Method 1 in Di Martino and Kelchermans, *J. Appl. Polym. Sci.* **56**, p. 1781 (1995), and using peak assignments from Zhang, *Polymer* **45**, p. 2651 (2004) for higher olefin comonomers.

[00164] Procedures for measuring the total pore volume of a porous support are well known in the art. Details of one of these procedures is discussed in Volume 1, *Experimental Methods in Catalytic Research* (Academic Press, 1968) (specifically see pages 67-96). This preferred procedure involves the use of a classical BET apparatus for nitrogen absorption. Another method well known in the art is described in Innes, *Total Porosity and Particle Density of Fluid Catalysts By Liquid Titration*, Vol. 28, No. 3, *Analytical Chemistry* 332-334 (March, 1956). Another well known method is described in ASTM D4284. For purposes of this invention and the claims thereto, in the event of conflict between the three, Volume 1, *Experimental Methods in Catalytic Research* (Academic Press, 1968) (specifically see pages 67-96) shall be used. The weight average particle size is measured by determining the weight

of material collected on a series of U.S. Standard sieves and determining the weight average particle size in micrometers based on the sieve series used.

CLAIMS:

1. A process for making an impact copolymer, comprising: polymerizing ethylene and at least one comonomer in the presence of one or more catalysts, polypropylene particles, and one or more halocarbon compounds to produce an impact copolymer comprising the polypropylene particles and an ethylene copolymer.
2. The process according to claim 1, wherein the one or more halocarbon compounds is present in an amount from 50 mg to 1,000 mg per mole of ethylene.
3. The process according to claim 1, wherein the polypropylene particles have a weight average particle size along the longest cross-sectional length thereof of 0.05 mm to 5 mm, and wherein the halocarbon compound is present in an amount from 50 mg to 1,000 mg per mole of ethylene.
4. The process according to claim 1, wherein the polypropylene particles have a pore volume from 5% to 80%, and wherein the halocarbon compound is present in an amount from 50 mg to 1,000 mg per mole of ethylene.
5. The process according to claim 1, wherein the polypropylene particles have a weight average particle size along the longest cross-sectional length thereof of 0.05 mm to 5 mm and a pore volume of 5% to 80%, and wherein the halocarbon compound is present in an amount from 50 mg to 1,000 mg per mole of ethylene.
6. The process according to any one of claims 1 to 5, wherein the one or more halocarbon compounds comprises a plurality of halogen atoms bonded to a single carbon atom.
7. The process according to any one of claims 1 to 6, wherein the one or more halocarbon compounds comprises an activated halogen.
8. The process according to any one of claims 1 to 7, wherein the one or more halocarbon compounds comprises an acyl halide.
9. The process according to any one of claims 1 to 8, wherein the one or more halocarbon compounds is selected from the group consisting of: one or more compounds containing a plurality of halogen atoms bonded to a single carbon, one or more activated halogen compounds, one or more acyl halide compounds, one or more allylic halogen compounds, one or more benzylic halogen compounds, elemental halogens, and any mixture thereof.
10. The process according to any one of claims 1 to 9, wherein the one or more halocarbon compounds comprises carbon tetrachloride, chloroform, trichloro toluene, ferric chloride, carbonyl chloride, trichloro toluene, benzoyl chloride, acetyl chloride, or any mixture thereof.

11. The process according to any one of claims 1 to 10, wherein the ethylene and at least one comonomer is polymerized in the presence of the one or more catalysts, the polypropylene particles, the one or more halocarbon compounds, and one or more inert solvents to produce the impact copolymer.
12. The process according to claim 11, wherein a miscibility of propylene in the inert solvent is greater than a miscibility of ethylene in the inert solvent.
13. The process according to claim 11, wherein the inert solvent comprises hexane, cyclohexane, toluene, or any mixture thereof.
14. The process according to any one of claims 1 to 13, wherein the ethylene copolymer has an ethylene content of from 20 wt% to 85 wt%, and wherein an amount of the ethylene copolymer in the impact copolymer is from 5 wt% to 85 wt%, based on the combined weight of the polypropylene particles and the ethylene copolymer.
15. The process according to any one of claims 1 to 14, wherein the impact copolymer comprises at least 15 wt% to 45 wt% of the ethylene copolymer, based on the combined weight of the polypropylene particles and the ethylene copolymer.
16. The process according to any one of claims 1 to 15, wherein the ethylene and the at least one comonomer are polymerized within a gas-phase reactor.
17. The process according to any one of claims 1 to 16, wherein the catalyst comprises a metallocene catalyst.
18. The process according to any one of claims 1 to 17, wherein the catalyst comprises a Ziegler-Natta catalyst.
19. The process according to claim 18, wherein the Ziegler-Natta catalyst comprises a solid catalyst component, a co-catalyst, and an external electron donor, and wherein the solid catalyst component comprises a titanium compound, a magnesium compound, and an internal electron donor.
20. A process for making an impact copolymer, comprising: contacting polypropylene particles having a weight average particle size along the longest cross-sectional length thereof of from 0.05 mm to 5 mm and a pore volume of 5% to 80%, one or more halocarbon compounds, ethylene, and at least one comonomer with one another under conditions sufficient to polymerize the ethylene and the at least one copolymer to produce an impact copolymer comprising the polypropylene particles and an ethylene copolymer.
21. The process according to claim 20, wherein the one or more halocarbon compounds is present in an amount from 50 mg to 1,000 mg per mole of ethylene.

22. The process according to claim 21, wherein the one or more halocarbon compounds is selected from the group consisting of: one or more compounds containing a plurality of halogen atoms bonded to a single carbon, one or more activated halogen compounds, one or more acyl halide compounds, one or more allylic halogen compounds, one or more benzylic halogen compounds, elemental halogens, and any mixture thereof.

23. A process for making an impact copolymer, comprising: combining ethylene and at least one comonomer with a Ziegler-Natta catalyst or a single site catalyst in a polymerization reactor at conditions sufficient to produce polypropylene particles having a weight average particle size along the longest cross-sectional length thereof of 0.05 mm to 5 and a pore volume of 5% to 80%; combining the polypropylene particles with a halocarbon compound to produce halocarbon-containing polypropylene particles having at least a portion of the halocarbon compound within the pores of the polypropylene particles; combining ethylene and at least one comonomer with the halocarbon-containing polypropylene particles and the catalyst, wherein at least a portion of the ethylene and at least a portion of the comonomer are located within the pores of the polypropylene particles, and wherein the halocarbon compound is present in an amount from 50 mg to 1,000 mg per mole of ethylene; and polymerizing the ethylene and the comonomer within the pores of the polypropylene particles to produce an impact copolymer.

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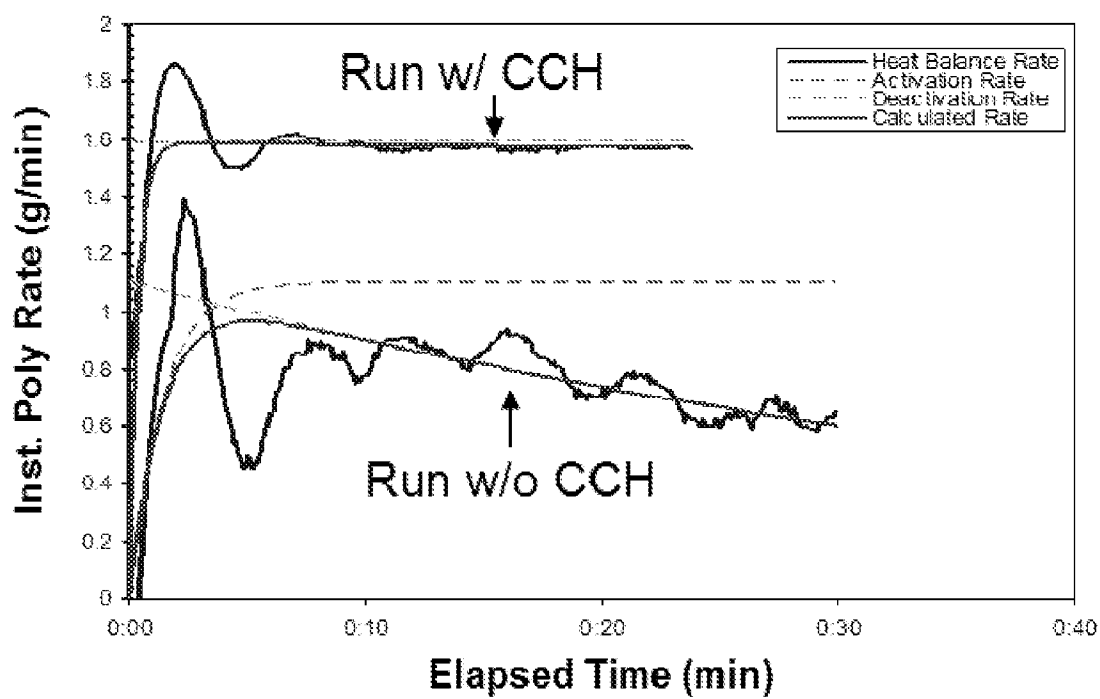


FIGURE 1

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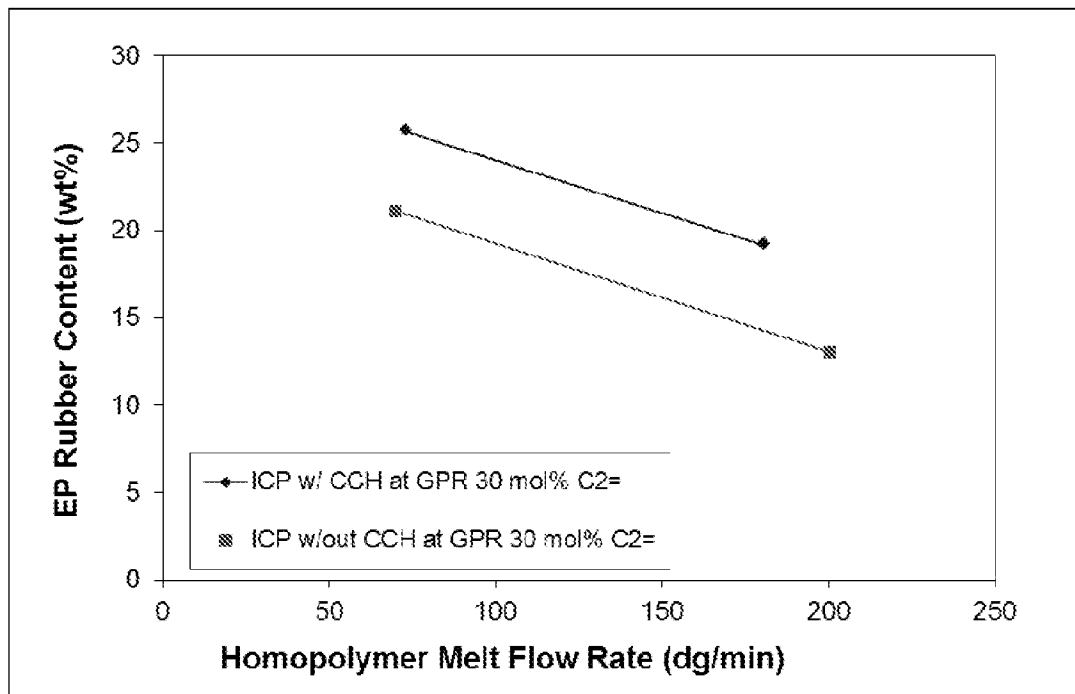


FIGURE 2

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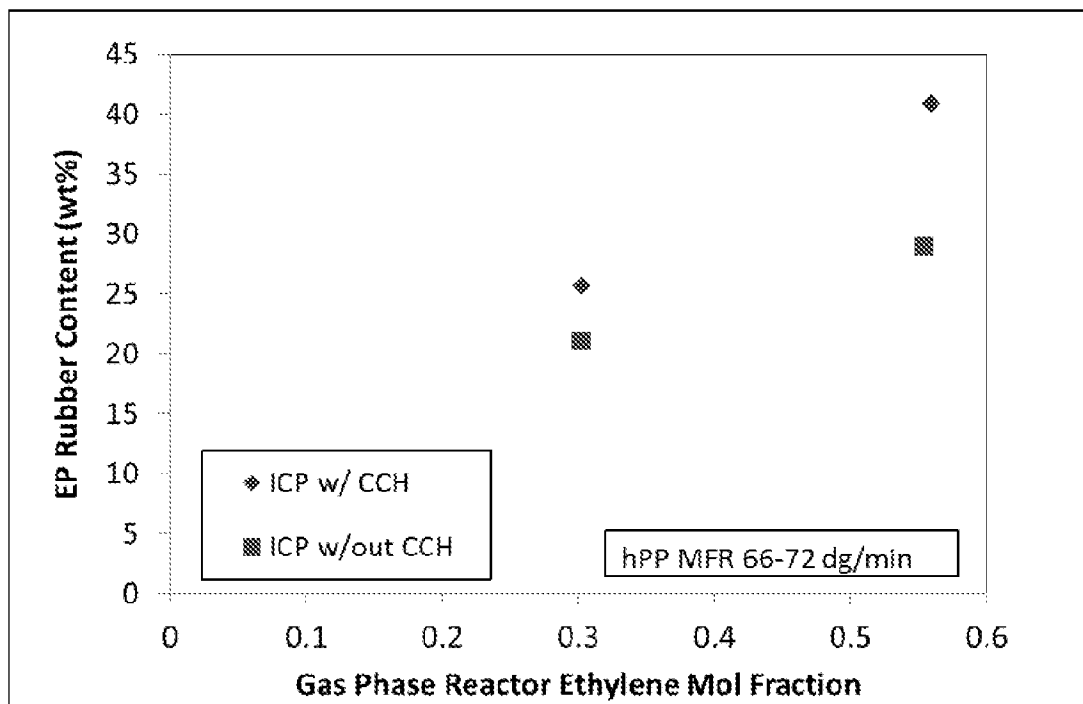


FIGURE 3

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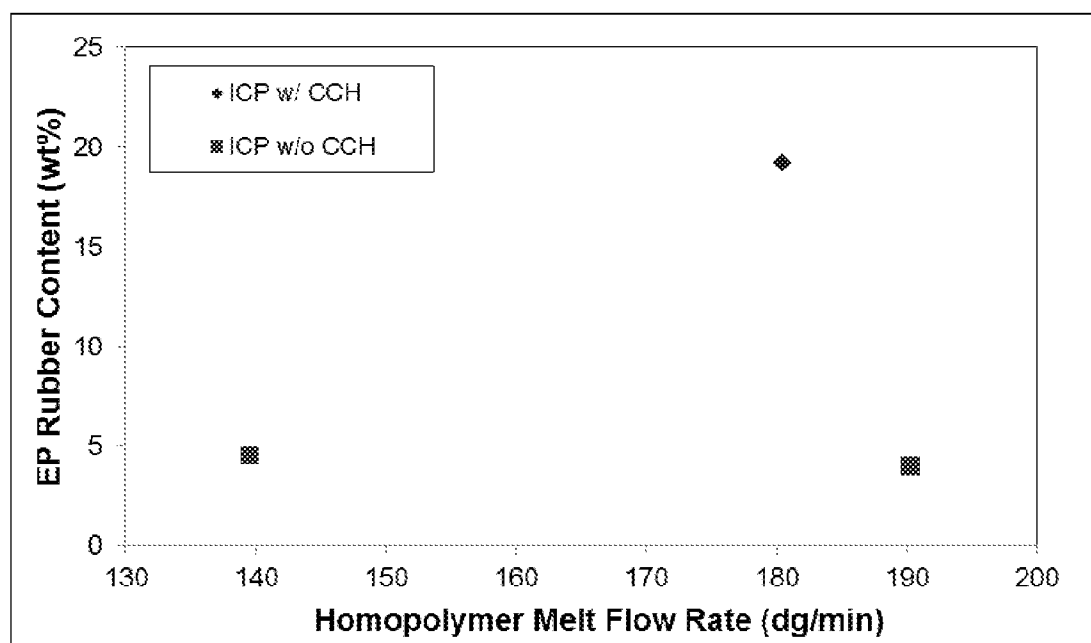


FIGURE 4

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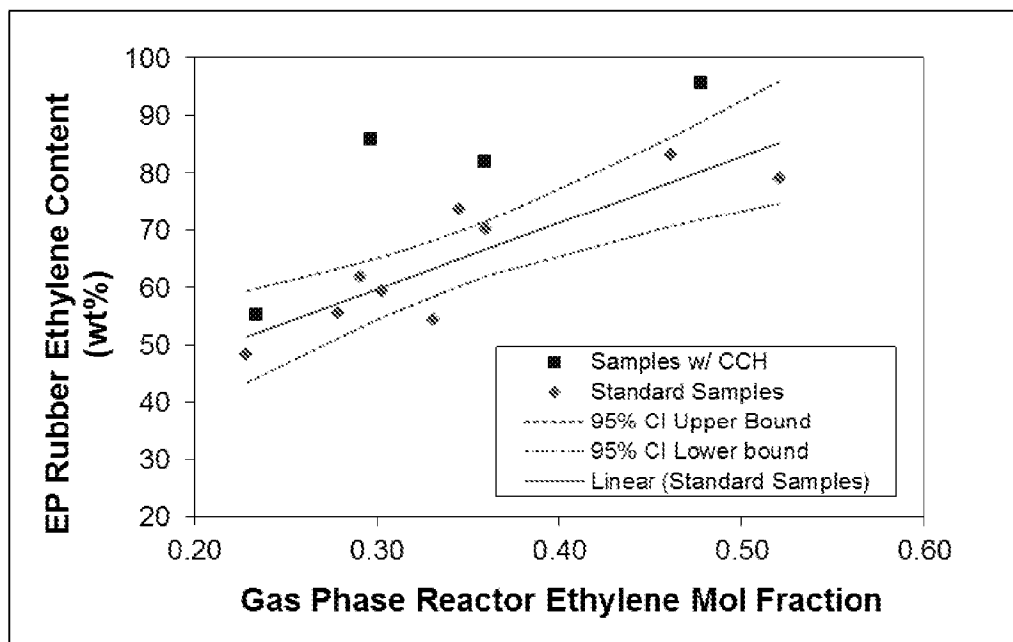


FIGURE 5

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US2014/011474**A. CLASSIFICATION OF SUBJECT MATTER****C08F 210/02(2006.01)i, C08F 210/06(2006.01)i, C08F 210/16(2006.01)i, C08F 8/18(2006.01)i**

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

C08F 210/02; C08F 4/64; C08F 2/00; C08F 4/42; C08F 4/72; C08F 297/08; C08F 2/01; C08L 23/16; C08F 210/06; C08F 210/16; C08F 8/18

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Korean utility models and applications for utility models

Japanese utility models and applications for utility models

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

eKOMPASS(KIPO internal) & Keywords: impact copolymer, catalyst, ethylene, propylene, halocarbon

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 2007-0225455 A1 (JIANG, PEIJUN et al.) 27 September 2007 See abstract; paragraphs [0035], [0042], [0045]-[0048], [0063], [0064], [0085], [0096], [0109], [0111], [0112], [0194]; claims 1-4, 12.	1-6, 20-22
A		23
A	US 2009-0209706 A1 (SHEARD, WILLIAM G. et al.) 20 August 2009 See abstract; paragraphs [0022], [0027], [0088], [0093]; claims 1, 2, 9.	1-6, 20-23
A	US 2010-0144990 A1 (YUKAWA, KIYOSHI et al.) 10 June 2010 See abstract; paragraphs [0029], [0030], [0081], [0024], [0130], [0131]; claims 1, 6, 9.	1-6, 20-23
A	US 5922813 A (COSTA, JEAN-LOUIS et al.) 13 July 1999 See abstract; column 7, lines 9-44; column 10, lines 25-50; column 12, lines 6-9; claims 1, 3.	1-6, 20-23
A	EP 0029651 A1 (MITSUBISHI CHEMICAL INDUSTRIES LIMITED) 3 June 1981 See abstract; page 6, lines 17-24; page 20, lines 14-24; claims 1, 3.	1-6, 20-23



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier application or patent but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

09 May 2014 (09.05.2014)

Date of mailing of the international search report

09 May 2014 (09.05.2014)

Name and mailing address of the ISA/KR

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INTERNATIONAL SEARCH REPORTInternational application No.
PCT/US2014/011474**Box No. II Observations where certain claims were found unsearchable (Continuation of item 2 of first sheet)**

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☒ Claims Nos.: 12,13,19
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
Claims 12, 13 and 19 are unclear because they refer to multiple dependent claims 11 and 18 respectively which do not comply with PCT Rule 6.4(a).
3. ☒ Claims Nos.: 7-11,14-18
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box No. III Observations where unity of invention is lacking (Continuation of item 3 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fees, this Authority did not invite payment of any additional fees.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest and, where applicable, the payment of a protest fee.
- ☐ The additional search fees were accompanied by the applicant's protest but the applicable protest fee was not paid within the time limit specified in the invitation.
- ☐ No protest accompanied the payment of additional search fees.

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