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(54) Title: STABLE, ONE-COMPONENT, CURABLE EPOXY/POLYAMIDE RESIN DISPERSIONS

(57) Abstract

Stable, one-component, curable epoxy resin and polyamide resin dispersions and methods for their preparation, wherein the polyamide resin is a polymerized fatty acid polyamide resin; the curable compositions, used as laminating agents, adhesives, potting and casting resins, show improved shelf life.

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STABLE, ONE-COMPONENT, CURABLE EPOXY/POLYAMIDE RESIN DISPERSIONS

BACKGROUND OF THE INVENTION

Curable compositions containing epoxy and
polyamide resins are known in the art. For example,
European Patent Application Publication No. 0 157 478
describes adhesive compositions prepared by mixing solid
particles of polyamide resins with solid particles of
epoxy resins. If desired, the composition also contains a
polymeric binder. Prior to application as an adhesive,
the polyamide and epoxy composition is preferably
dispersed in a non-solvent.

Hastings et al., U.S. Patent No. 3,945,964, describes stable aqueous emulsions of epoxy resins

15 containing, as emulsifying agents, ethylene oxide propylene oxide block polymers of specified formulae.

Curing agents described as useful with the epoxy resin emulsion include polyamides.

Aelony et al., U.S. Patent No. 2,899,397,

describes mixed aqueous emulsions of polyamide and epoxy resins prepared by mixing a solution of epoxy resinous material with a solution of polymeric polyamides, combining the two solutions in the presence of an aqueous medium containing a water soluble organic carboxylic acid and agitating the combined solutions to produce an emulsion.

One problem with many of the prior art epoxy/polyamide resin compositions, however, is the rapid reactivity of the mixed resins, producing in a relatively

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short amount of time an infusible, insoluble composition.

Where such compositions are intended for use as laminating agents, adhesives, potting and casting resins, and the like, this brief reaction time requires that the resin mixture be prepared at point of use and in relatively small quantities. Attempts have been made to lengthen the shelf life of these compositions, however, such attempts have met with little success. In addition, relatively large amounts of volatile organic solvents used in these processes (i.e. toluene, isopropanol, methylethyl ketone) are flammable and environmentally undesirable.

New and/or better curable epoxy and polyamide resin compositions, particularly compositions having a longer and more stable shelf life, are needed. The present invention is directed to these important ends.

SUMMARY OF THE INVENTION

The present invention relates to a stable, one-component, curable system comprising, in combination:

- (a) a stable, non-solvated, aqueous dispersion 20 of an epoxy resin having unreacted epoxy groups; and
 - (b) a stable, non-solvated aqueous dispersion of a polyamide resin having excess acid or amine groups.

The invention is also directed to a method for the preparation of a stable, one-component, curable system which comprises:

- (a) preparing a stable, non-solvated, aqueous dispersion of epoxy resin having unreacted epoxy groups;
- (b) preparing a stable, non-solvated, aqueous dispersion of polyamide resin having excess acid or amine30 groups; and
 - (c) blending said epoxy resin dispersion with said polyamide resin dispersion at atmosphere between about 0°C and 90°C.

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DETAILED DESCRIPTION OF THE INVENTION

The present invention is practiced by first preparing a stable, non-solvated, aqueous dispersion of an epoxy resin having unreacted epoxy groups, and a stable, 5 non-solvated aqueous dispersion of a polyamide resin having excess acid or amine groups. The term "polyamide resin dispersion" as used collectively herein is meant to include those dispersions of solid polyamide resin particles in water having average volume particle size of less than about 1 micron, referred to herein as 10 "microdispersions," and those dispersions having average volume particle size of between about 1 and 20 microns, referred to herein as "regular dispersions." "Epoxy resin dispersions" as used herein refers to dispersions of epoxy 15 in water, including liquid/liquid and solid/liquid dispersions, wherein the epoxy phase may comprise liquid droplets or solid particles. "Non-solvated" as used herein means that the epoxy and polyamide resin dispersions of the present invention contain no organic 20 solvents in amounts sufficient to dissolve the respective resins. The term "stable", as used in connection with the separate polyamide and epoxy resin dispersions, refers to the stability of the separate dispersions, which when cooled to ambient temperatures, that is, room temperature, 25 will not separate within 24 hours. The term "aqueous", as used in connection with the separate polyamide and epoxy resin dispersions, denotes a water-based dispersion.

There exist numerous types of polyamide resins having excess acid or amine groups which may be employed to form the aqueous polyamide resin dispersions used in the present invention. Polyamide resins are a well-known class of resins and include, for example, nylon-type polyamide resins and polymerized fatty acid polyamide resins. Preferably, the polyamide resins have an acid number of less than about 50 and an amine number of less than about 50. More preferably, the polyamide resins are polymerized fatty acid polyamide resins which have a

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cumulative acid and amine number between about 3 and 40, most preferred between about 5 and 20. The polymerized fatty acid polyamide resins and other polyamide resins suitable for use in the present invention can be obtained commercially or can be prepared by generally well known methods.

The term "polymerized fatty acid" as used in this specification is intended to be generic in nature and refers to polymerized acids obtained from fatty acids.

10 The term "fatty acids" refers to saturated, ethylenically unsaturated and acetylenically unsaturated, naturally occurring and synthetic monobasic aliphatic carboxylic acids which contain from about 8 to about 24 carbon atoms.

For purposes of facilitating the explanation of
this invention, specific references will be made to
polymerized fatty acid polyamide resins which are obtained
from unsaturated C₁₈ fatty acids. It should be
appreciated, however, that the compositions and methods of
this invention can likewise be practiced using other
polymerized fatty acid polyamides, and of course other
types of polyamides.

The preferred starting acids for the preparation of the polymerized fatty acids useful in the invention are oleic and linoleic acids because of their ready

25 availability and relative ease of polymerization.

Mixtures of these two acids are found in tall oil fatty acids making commercial tall oil fatty acids a convenient source of the starting materials. The fatty acids can be polymerized using various well known catalytic and

30 noncatalytic polymerization methods. A typical composition of the polymerized fatty acids based on the C₁₈ tall oil fatty acids which are used as the starting materials for the polyamide resins employed in the present invention is as follows:

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monobasic acids (monomer) 0-15% by wt. C18

dibasic acids (dimer) 60-95% by wt. C_{36}

trimer acid (or higher) C₅₄ or polybasic acids 0.2-35% by wt.

In the preparation of the polymerized fatty acid polyamide resins used in the present invention, it is preferable that the starting polymerized fatty acid contain as high a percentage of the dimer acid (the C36 dibasic acid) as possible in order to obtain the optimum 10 physical properties in the final product.

In addition to the polymerized fatty acids, a wide variety of dicarboxylic acids can be used in the preparation of the polymerized fatty acid polyamide resins employed in the present invention, including aliphatic, 15 cycloaliphatic and aromatic dicarboxylic acids. Representative of such acids, which may contain from 2 to 22 carbon atoms, are oxalic, glutaric, malonic, adipic, succinic, suberic, sebacic, azelaic, pimelic, terephthalic, isophthalic, phthalic, naphthalene 20 dicarboxylic acids and 1,4- or 1,3-cyclohexane dicarboxylic acids. Preferred dicarboxylic acids employed in the invention are straight chain aliphatic diacids having at least about 6 carbon atoms and more preferably about 6 to about 22 carbon atoms, such as azelaic, 25 sebacic, and dodecanedioic dicarboxylic acids. It should be understood that use of the corresponding acid anhydrides, esters, and acid chlorides of these acids is included in the term dicarboxylic acid. Methods of preparing these preferred acids are well known, and many

Linear, branched, or cyclic polyamines are also used in the preparation of the polymerized fatty acid polyamide resins of the present invention and may be one or more of the well known aliphatic, cycloaliphatic or 35 aromatic diamines having from about 2 to about 60 carbon atoms. Preferred are the alkylene diamines. Illustrative of the preferred diamines are ethylene diamine, 1,3-

30 are readily available commercially.

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diaminopropane, 1,4-diaminobutane, terephthalyl diamine, known as p-xylene diamine, 1,6-hexamethylene diamine, methyl-1,5-pentamethylene diamine, methyl-1,9-nonane diamine, piperazine, 1-(aminoethyl)piperazine, 1,4-5 (bisaminoethyl)piperazine, 1,3-di-(1-piperidyl)propane, dimer diamine (diamine made from dimer acid), dipiperazine, 4,4' methylenebis(cyclohexylamine), 2,2-bis-(4-cyclohexylamine) propane, polyglycol diamines, isophorone diamine, isophthalyl diamine, known as m-xylene 10 diamine, cyclohexanebis(methylamines), 1,4-bis-[2'aminoethyl) benzene, 4,4'methylenebis (cyclohexylamine) and piperazine. These diamine compounds are all prepared by well known methods and many are commercially available. Preferred particularly are the straight chain aliphatic 15 diamines of about 2 to about 20 carbons atoms, especially ethylene diamine and hexamethylene diamine, and cycloaliphatic diamines, especially 4,4'methylenebis(cyclohexylamine) and piperazine. Monoamines may also be added to control molecular weight and 20 functionality. Mixtures of polyamines, including triamines, can be used to obtain a good balance of properties.

Polyetherdiamines provide products with better flow properties. The most preferred polyetherdiamines include diamines made from propylene oxide polymers having molecular weights of from about 100 to about 8,000, diamines made from ethylene oxide polymers having molecular weights of from about 100 to 8,000, and diamines made from ethylene oxide/propylene oxide polymers having molecular weights of from about 100 to about 8,000. Other suitable polyetherdiamines include triamines made from propylene oxide polymers or ethylene oxide polymers and having molecular weights from about 100 to about 8,000.

In the method of the present invention, it is

desirable to use as the polymerized fatty acid polyamide a

material which is the result of a relatively complete

amidation reaction between the starting polymerized fatty

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acid and the diamine. The degree of completion of the amidation process can be determined by evaluating the acid number and the amine number of the final polymer. The term acid number refers to the number of milligrams of potassium hydroxide required to neutralize the free acid in one gram of the polymer. The term amine number refers to the number of milligrams of potassium hydroxide equivalent to the free or excess amine groups present in the final polymer. The polymerized fatty acid polyamide resins having amine numbers of, for example, up to about 50, and acid numbers of, for example, up to about 50, are especially useful in the present invention.

As those skilled in the art would recognize, the number of free acid groups and free amine groups present in the polymerized fatty acid polyamide resin are directly related to the relative amount of the polymeric fatty acids, dicarboxylic acids and the diamines involved in the polymerization reaction and the degree of completion of the reaction. Thus, in preparing the low acid and amine number polyamides, approximate stoichiometric amounts of the polymerized fatty acids plus the dicarboxylic acids and the diamines based on the total number of available acid and amine groups should be used to prepare the polyamide resins for this invention and the reaction conditions should be selected to ensure substantial completion of the amidation reaction. The reaction conditions required for the amidation reaction are well known in the art with the reaction being generally conducted at temperatures from about 100°C to about 300°C for about 1 to about 8 hours.

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In preparing the stable, non-solvated, aqueous dispersion of the polyamide resins, a number of techniques can be employed. Preferably, the resultant polyamide resin dispersion, prepared by whatever technique, has a high resin content. As used herein, the term high resin content denotes a resin content of at least about 20% by weight.

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One dispersion technique found by the inventors to be useful in preparing "regular dispersions" of the polymerized fatty acid polyamide resin is as follows. polyamide resin is first liquified by heating the 5 polyamide resin to a temperature above its melting point, and more preferably to a temperature of at least about 5°C above its melting point, but below the decomposition temperature of the polyamide resin. The liquification process is preferably conducted in a closed vessel under a 10 protective blanket of inert gas such as nitrogen. melting temperature of the polyamide resin will vary considerably depending upon the particular starting reactants employed to prepare the polyamide resin. Typically, however, the polymerized fatty acid polyamide resins will melt in the temperature range from somewhat below the boiling point of water to somewhat above the boiling point of water. If the temperature to which the molten polyamide resin will be heated for liquification is above the boiling point of water, the process equipment 20 used must be capable of being operated at elevated pressures and temperatures. In a separate vessel, water is heated to a temperature which is preferably at least as high as the melting point of the polyamide resin which is to be dispersed, and more preferably at least about 5°C 25 higher than the melting point of the polyamide resin. Under these conditions, the water may be required to be heated and maintained under pressure in order to have sufficient temperature to be higher than the melting point of the polyamide resin. In an alternative method, the 30 water can be heated to a temperature somewhat below the temperature of the polyamide resin and the polyamide resin heated to a temperature significantly above its melting point so that the resulting blend of water and polyamide resin will have a temperature above the melting point of 35 the polyamide resin.

A surfactant, or combination of surfactants, is added to either the molten polyamide resin, or to the

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water, or to both the polyamide resin and the water, in a predetermined amount. The surfactant or combination of surfactants which are used in this dispersion technique are ones which will promote the emulsification of the

5 molten polyamide resin and the water and which will also act to stabilize the final dispersion of the polyamide resin in the water. A wide variety of different types of surfactants can be successfully employed in this technique. The surfactants which should be selected are those which are capable of acting as water-in-oil emulsifying agents for the polyamide resin-water mixture. The surfactants should also act as oil-in-water emulsifying agents upon inversion of the emulsion. The surfactants include well known anionic, polar and nonpolar nonionic, and cationic surfactants.

The cationic surfactants which have been found to be especially useful in this polyamide resin dispersion technique are the alkyl ammonium salts such as: 1-hexadecyltrimethyl ammonium bromide or chloride; alkyl pyridinium salts such as 1-hexadecylpyridinium bromide and cetylpyridinium chloride; alkyl imidazolinium salts such as 1-hexadecylimidazolinium bromide; and the salts of tallow diamines, such as Jet Amine DT, tallow ammonium chloride salts, such as Jet Quat DT-50, ethoxylated tallow amines, such as Jet Amine DT-5, and the salts of tallow triamines, such as Jetco TRT (manufactured by Jetco Chemicals, Corsicana, Texas).

Among the anionic surfactants which have been found to be especially useful are the sodium and potassium salts of fatty acids, the sodium and potassium salts of dimer acid or polymerized fatty acids, phosphate esters of fatty acids, and the sodium and potassium salts of rosin.

Among the nonionic surfactants which have been found to be especially useful are nonylphenol polyethoxyethanol, commercially available under the name Tergitol NP-40TM from Union Carbide Corporation, Danbury, CT, and polyethoxylated castor oil, commercially available

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under the name GAF EmulphorsTM from GAF Corporation, Wayne, N.J.

while not all surfactants are suitable for use in the dispersion of polyamide resins according to this technique, it has been found that a wide range of surfactants are suitable. It is relatively simple to screen suitable surfactants for such use. It was found, for example, that the preferred surfactants are those which exhibit outstanding ability to cause the emulsification of the liquified polymerized resin in the water. These surfactants are typically also highly effective in imparting a long term stability to the final dispersion.

either to the molten polyamide resin or to the water to be used in the dispersion process. The surfactant, however, is preferably added to the water because of the relative ease of addition. The relative amount of the surfactant added is based on the amount of the polyamide resin which is to be present in the final dispersion, and on the particular surfactant used. It has been found, however, that optimum results are generally obtained when the surfactant is used in an amount from about 0.2% to about 10% by weight, and preferably from about 0.2% to about 2% percent by weight, based on the weight of the polyamide resin.

In carrying out this polyamide resin dispersion technique, the liquified polyamide resin, the heated water and the surfactant are blended together in a predetermined ratio while maintaining the temperature of the individual components and the mixture above the melting point of the polyamide resin. In this regard, it is important that the equipment utilized in the initial blending step likewise be heated to appropriate temperatures to prevent the premature deposition of liquified polyamides on the equipment and a cooling of the blend of materials. The molten polyamide resin, the water and the surfactant are

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blended in ratios such that the resulting mixture of materials will contain from about 20% to about 60%, and preferably about 25% to about 40% by weight of the polyamide resin. The mixture is subjected to comminuting 5 forces sufficient to form a finely divided emulsion in which the droplets of the molten polyamide resin have a volume average size distribution of 20 microns or less in diameter and more preferably 5 microns or less in diameter. Particle size distribution can be determined by 10 a number of methods, such as sedimentation or laser light scattering techniques. The particular type of apparatus used for applying the comminuting force to the blend of the polyamide resin, water, and surfactant to some extent is a matter of choice and can include apparatus which 15 operates on the basis of shear, impact, or a combination of these process steps. The equipment includes commercially available apparatus such as homogenizers, submicron dispersers, emulsifiers, colloid mills, ultrasonic sound mixers and the like. In general it is preferable for process purposes to run the blend through 20 the comminuting equipment for one pass, in that this facilitates the manufacturing process. It should be appreciated, however, that the blend may be sent through the comminuting equipment for a number of passes in order 25 to obtain the smaller size droplets. In general, the smaller the size of the liquid droplets, the more stable will be the resulting dispersions.

The final step in the foregoing polymerized fatty acid polyamide resin dispersion technique concerns cooling down the emulsion to a temperature below the melting point of the polymerized resin so as to cause the finely divided droplets in the emulsion to solidify into finely divided dispersed particles. The cooling is preferably conducted in a relatively rapid fashion so as to prevent coagulation of the particles during that portion of the solidification wherein the droplets become semi-solid and highly adhesive. Cooling of the emulsions

prepared at super atmospheric pressures can be rapidly performed by pumping the emulsion through a heat exchanger or the like. Alternatively, or in addition to using a heat exchanger, the cooling can be caused by evaporation of water from a rapid reduction in the pressure.

The foregoing polymerized fatty acid polyamide resin dispersion technique is set forth in greater detail in U.S.S.N. 464,572, filed January 16, 1990, which is a continuation of U.S.S.N. 151,773, filed February 3, 1988, the disclosures of which are incorporated herein by reference, in their entirety. This technique will provide stable, non-solvated, aqueous polyamide resin dispersions suitable for use in the subject epoxy resin and polyamide resin composition.

Other polyamide resin dispersion techniques that 15 will lead to stable non-solvated aqueous polyamide resin dispersions for use in the subject epoxy resin and polyamide resin composition, are described, for example, in U.S.S.N. 664,276, filed March 4, 1991, which is a continuation of U.S.S.N. 537,318, filed June 13, 1990, the disclosures of which are also incorporated herein by reference, in their entirety. As disclosed therein, aqueous polyamide dispersions having improved stability against phase separation and gelation are achieved by the addition to such dispersions of a water soluble, amphoteric chemical moiety, such as an amino acid, anionic or cationic salts of amino acid, or mixtures thereof, which exhibit dipolar character in aqueous media. addition to methods for preparing the polyamide resin 30 dispersions as described in the present application, other embodiments utilizing the polymerized fatty acid polyamide resins, neutralizing agents and surfactants (as described in the present application) are disclosed in the U.S.S.N. 664,276 application. In one method described 35 therein, a solid polymerized fatty acid polyamide resin is mixed with water, a neutralizing agent, and an amount of surfactant which will promote emulsification of the

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polyamide resin in water. The mixture is heated to a temperature at least as high as the resin softening point to form a water-in-oil emulsion which is inverted by adding thereto an effective amount of inversion water in 5 which has been dissolved a dispersion stabilizing amount of glycine. The resulting emulsion of polyamide resin in water is then cooled below the resin's melting point, causing emulsified droplets of the polyamide resin to solidify as finely divided particles which are dispersed 10 uniformly through the aqueous phase.

Polyamide resin "microdispersions" and methods for the manufacture thereof are discussed in U.S.S.N. 674,846, filed March 25, 1991, the disclosure of which is incorporated herein by reference, in its 15 entirety. The polyamide "microdispersions" disclosed therein also have improved stability against phase separation and gelation. Additionally, they are capable of forming clear, continuous films at ambient or near ambient temperatures.

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The microdispersions are produced by first forming a water-in-oil emulsion by mixing together at a first temperature the polyamide resin, water, at least one surfactant, at least one co-surfactant, and a neutralizing acid or base, wherein the water and surfactant are present 25 in amounts effective to form the water-in-oil emulsion, the co-surfactant is present in an amount effect to form the aqueous microdispersion, the neutralizing acid or base is present in an amount effective to neutralize residual acid or base in the polyamide resin, and the first 30 temperature is effective to liquify the polyamide resin and to maintain an oil phase of a water and oil emulsion as a liquid.

The aqueous microdispersions are then formed by mixing together at a second temperature the water-in-oil 35 emulsion and a second amount of water effective to form an oil-in-water emulsion. The oil-in-water emulsion is then cooled to a third temperature effective to form the

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aqueous microdispersions. At least one water soluble, dipolar, chemical moiety is added to either the oil—in—water emulsion at the second temperature or to the aqueous microdispersion, in an amount effective to stabilize the aqueous microdispersion. The chemical moiety, for example, is an amino acid, anionic and cationic salts derived therefrom, or mixtures thereof. Surfactants utilized in processes disclosed therein include well known anionic, polar and non-polar, non-ionic, amphoteric, and cationic surfactants. The co-surfactants employed are preferably alcohols having up to 10 carbon atoms. Additional embodiments of methods for the preparation of the microdispersions, as well as more detailed discussions of materials used therein, are found in the application, which application is incorporated herein by reference.

The present invention also contemplates the use of other polyamide resin dispersion techniques known to those skilled in the art that will lead to a stable, non-solvated, aqueous polyamide resin dispersion suitable for use in the subject epoxy resin and polyamide resin compositions.

To prepare the compositions and practice the methods of the invention, stable, non-solvated, aqueous dispersions of epoxy resin having unreacted epoxy groups 25 must also be prepared. There exists numerous types of epoxy resins having unreacted epoxy groups, that is, oxirane group containing compounds, which may be employed to form the aqueous epoxy resin dispersions used in the present invention. The phrase "epoxy resin having 30 unreacted epoxy groups" is used herein to collectively refer to oxirane group containing compounds, and polymers and mixtures of these compounds with other materials. Such epoxy resins are well known in the art and can be obtained commercially or can be prepared by generally well 35 known methods. Such epoxy resins include, but are not limited to, the diglycidyl ethers of bisphenol A (commonly referred to as DGEBA), brominated resins, epoxyphenol

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novolac and epoxy cresol novolac resins, and cycloaliphatic resins. These and other examples of epoxy resins suitable for use in the present invention are described, for example, in Lee and Neville, Handbook of Epoxy Resins, McGraw-Hill, Inc. (New York, 1967), the disclosures of which are incorporated herein by reference, in their entirety.

The preferred epoxy resins are those of the diglycidyl ethers of bisphenol A, (DGEBA) and those of the polyglycidyl ethers of novolac resins, which are typically derived from phenol-formaldehyde or cresol-formaldehyde. EPON 828TM is a liquid DGEBA resin (Shell Chemical Co., Houston, TX.) having an epoxy equivalent weight of 185 to 192 and a viscosity in centipoises at 25°C of 10,000-15 16,000. DEN 438 and 439 are epoxyphenol novolac resins having an epoxy equivalent weight of 170 to 210 and a viscosity in centipoises at 80°C of 1,000-30,000, commercially available from Dow Chemical Company, Midland, MI.

As will be apparent to those skilled in the art, the epoxy resin employed in the present invention can be dispersed to form a non-solvated aqueous epoxy resin dispersion using a number of techniques. Preferably, the resultant epoxy resin dispersion, prepared by whatever technique, has a high resin content as defined above, and more preferably, 40-70% by weight, based on the total weight of the epoxy resin dispersion.

One particularly preferred dispersion technique found by the inventors to be useful in preparing the epoxy resin dispersions used in the invention is as follows. First, the epoxy resin is liquified by heating to at least its melting point, and more preferably to a temperature of at least about 5°C above its melting point, but below the decomposition temperature of the epoxy resin. The heating is preferably carried out with rapid stirring. The melting temperature of the epoxy resin will vary considerably depending upon the particular epoxy resin

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employed. Typically, however, these epoxy resins will melt at temperatures from below ambient to about 100°C. a separate vessel, water is heated to a temperature which is preferably at least as high as the melting point of the 5 epoxy resin which is to be dispersed, and more preferably at least about 5°C higher than the melting point of the epoxy resin. In an alternative method, the water can be heated to a temperature somewhat below the temperature of the epoxy resin and the epoxy resin heated to a 10 temperature significantly above its melting point so that the resulting blend of water and epoxy resin will have a temperature above the melting point of the epoxy resin. The water is generally added to the molten epoxy resin in a drop wise fashion, with rapid stirring.

A surfactant or combination of surfactants is added to either the molten epoxy resin, or to the water, or to both the epoxy resin and the water, in a predetermined amount. The surfactant or combination of surfactants which are used in this epoxy resin dispersion 20 technique are ones which will promote the emulsification of the molten epoxy resin in the water and will also act to stabilize the final dispersion of the epoxy resin in the water. A number of different types of surfactants can be successfully employed in this technique. 25 surfactants which are selected are those which are capable of acting as oil-in-water dispersing agents for the epoxy resin-water mixture. The surfactants include well known anionic, polar and nonpolar nonionics, and cationic surfactants.

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Preferably, the surfactants employed are of the 30 nonionic type, most preferably the nonionic alkylaryl polyether alcohols such as those commercially available under the name Triton $X-207^{TM}$ and Triton $X-405^{TM}$ from Rohm and Haas Company, Philadelphia, PA. Other suitable nonionic surfactants include ethylene oxide propylene oxide block copolymers, such as those disclosed in U.S.

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Patent No. 3,945,964, the disclosures of which are incorporated herein in their entirety.

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While not all surfactants are suitable for use in the dispersion of epoxy resins, as those skilled in the 5 art will recognize, it is a relatively simple procedure to screen suitable surfactants for such use. It was found, for example, that the preferred surfactants are those which exhibit outstanding ability to cause the emulsification of the liquified epoxy resin in the water. These surfactants are also typically highly effective in imparting a long term stability to the final dispersion.

The surfactants as indicated above are added either to the molten epoxy resin or to the water to be used in the dispersion process. The surfactant, however, is preferably added to the water because of the relative ease of addition. The relative amount of the surfactant added is based on the amount of the epoxy resin which is to be present in the final dispersion, and on the particular surfactant used. It has been found, however, 20 that optimum results are obtained when the surfactant is used in an amount from about 1% to about 25% by weight, and preferably 2% to about 10% by weight, based on the weight of the epoxy resin. The epoxy resin dispersions can also contain various additives in addition to the 25 above-noted surfactants, such as protective colloids, viscosity modifiers and the like. Some examples are carboxy methyl cellulose, polyvinyl alcohol, polyethylene oxide and the like. The amount of such additives employed can vary in amounts from about 0.5% to about 10% based on 30 the weight of the epoxy resin.

In carrying out this epoxy resin dispersion technique, the liquified epoxy resin, the heated water, and the surfactant are blended together in a predetermined ratio while maintaining the temperature of the individual 35 components in the mixture above the melting point of the epoxy resin. In this regard, it is important that the equipment utilized in the blending step likewise be heated

to appropriate temperatures to prevent the premature deposition of liquified epoxies on the equipment and a cooling of the blend of materials. The molten epoxy resin, the water and the surfactant are blended in ratios such that the resulting mixture of materials contains epoxy resin in an amount from about 20% to about 60%, and preferably about 40% to about 60% by weight, based on the total weight of the epoxy resin dispersion.

The final step in the foregoing epoxy resin

dispersion technique concerns cooling down the emulsion.

The cooling is preferably conducted in a relatively rapid fashion so as to prevent coagulation of the particles.

Cooling of the emulsions prepared at super-atmospheric pressures can be rapidly performed by pumping the emulsion through a heat exchanger or the like. Alternatively, or in addition to using a heat exchanger, the cooling can be caused by evaporation of water from a rapid reduction in the pressure.

will provide a stable, non-solvated, aqueous epoxy resin dispersion suitable for use in the subject epoxy resin and polyamide resin compositions. The present invention also contemplates the use of other epoxy resin dispersion techniques known to those skilled in the art that will lead to a stable, non-solvated, aqueous epoxy resin dispersion suitable for use in the subject epoxy resin and polyamide resin compositions. Epoxy resin dispersions can also be obtained commercially, such as Epi-Rez W55-5003, Epi-Rez W60-5520, Epi-Rez W60-3515, Epi-Rez 35201, and CMD W50-3519, all available from Rhone-Poulenc Inc., Louisville, Kentucky.

To prepare the stable, one-component, curable system of the invention, the foregoing stable, non-solvated, aqueous dispersion of an epoxy resin having unreacted epoxy groups and the stable, non-solvated, aqueous dispersion of a polyamide resin having excess acid or amine groups are blended together at a temperature

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below the melting point of the epoxy and polyamide resins in the dispersions. Preferably, blending occurs at a temperature of between about 0°C to about 90°C, more preferably between about 10°C to 50°, most preferably at 5 about 20°C or ambient temperatures (that is, room temperature). Blending can be carried out in various fashions using techniques readily apparent to those skilled in the art. Varying ratios of epoxy resin to polyamide resin can be employed, but preferably the 10 initial ratio of epoxy groups of the epoxy resin to the free amine or acid groups of the polyamide resin is greater than about 1:1 and less than about 10:1. more preferred if the ratio of epoxy groups to free amine or acid groups is greater than about 1:1 and less than 15 about 5:1. The most preferred ratio of epoxy groups to free amine or acid groups is greater than about 1.5:1 and less than about 4:1.

The resulting combined epoxy and polyamide resin dispersions of the invention provide a one-component, 20 curable system which exhibits exceptional stability. polyamide and epoxy resin dispersions prepared in accordance with the present invention do not separate or significantly react with one another when allowed to stand at ambient temperatures (that is, at room temperature, about 20°C) for twenty-four hours or more. For purposes of this specification the terms "stable", "stability", and variations thereof, as used in connection with the combined polyamide and epoxy resin dispersions of the invention, refer to the excellent shelf-life of the 30 combined dispersions at ambient temperatures (that is, at room temperatures, about 20°C) in that the combined dispersions will not separate from one another or significantly react with one another within twenty-four hours. It has been found, however, that the dispersions 35 prepared in accordance with this invention typically will be stable over extremely long periods of time with stabilities in excess of six months not being uncommon.

Furthermore, the dispersions of this invention do not require that the starting polyamide and epoxy resin dispersions be solvated.

The combined epoxy and polyamide resins have 5 further advantages such as the elimination of the need for expensive organic solvents, elimination of organic solvent toxicity and associated fire hazards, less impregnation of films into porous surfaces such as paper, more ready handleability, etc. A further advantage of the combined 10 dispersions of this invention is that once formed, they can be freeze-dried resulting in a finely divided powder which can be redispersed with minimal agitation to reform a stable dispersion. The excellent stability of the dispersions of this invention are further shown by the 15 ability of the dispersions to undergo repeated freeze-thaw cycles without causing a breakdown on the dispersion. Of most importance, however, is the excellent stability or shelf life of the combined polyamide and epoxy The combined polyamide and epoxy aqueous dispersions. 20 dispersions of this invention can contain, if desired, in addition to the above-noted materials, various additives. One particularly useful type of additive is stabilizing agents to prevent flocculation of the resin particles. Typical stabilizers include water soluble alkali metal 25 salts of polymeric organic acids. The stabilizers can also include protective colloids such as lignin derivatives, proteins, water soluble cellulose derivatives, starch, alginic acid, and long chain alcohols and lecithin. The amount of stabilizing agent employed 30 can vary in amounts from 0.5% to about 10% based on the weight of the polyamide resin. The dispersions may likewise contain other materials such as viscosity modifiers, plasticizers, dyes, pigments and the like. In this regard, it should be noted that the excellent 35 stability of the resin dispersions of this invention allow substantial loadings of additives without adversely affecting the overall stability of the dispersions.

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Chemical curing accelerators may also be present in the combined dispersions. Examples of such accelerators include bisphenol A, triphenylphosphite, phenolic resins, imidazole compounds, or the like.

A number of inert components may also be incorporated in the composition of the invention, as long as they do not adversely affect the shelf life of the resultant composition, or its ability to be employed in the particular use for which it is intended.

Numerous uses are available for the compositions 10 of the invention. For example, the subject compositions may be used as wet stick adhesives, or may also provide excellent heat seal adhesives. The dispersions may also be used as beater or head box adhesives in the preparation 15 of paper, and as protective or decorative coatings of various sorts. The dispersions may also be employed in the formulation of water-based paints, and may also have applications involving fabrication with glass fiber. dispersions of the present invention may also be of value 20 as structural adhesives for metal, wood, ceramics, glass and other rigid materials. They may also be used as binders for all sorts of particulate matter including cork, cellulosic materials, resinous materials, paper pulp, wood flour, asbestos fiber, textile fibers, clay, 25 sand, plaster of Paris, pigments, leather, numerous waste materials, and the like. The subject dispersions also provide excellent impregnants for paper, textiles, leather and other porous surfaces.

The following Examples are given by way of

further illustration of the present invention, and should

not be construed as limiting the scope of the present

invention as set forth in the appended Claims.

Examination of the examples and resulting data will show

that the curable epoxy/polyamide resin dispersions of the

present invention have significantly improved tensile

properties at ambient temperatures or at 60°C when compared

to either the polyamide resins or polyamide resin

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dispersions. Additionally, the cured epoxy/polyamide resin dispersions are more solvent-resistant than the polyamide resin dispersions.

EXAMPLES

5 Example 1

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A stable, aqueous dispersion of UNI-REZ 2636

(Union Camp Corp., Wayne, N.J.) was prepared as follows.

250 grams of UNI-REZ 2636 were charged to a 2 liter Parr reactor and heated to 160°C with 500 rpm stirring. An

10 aqueous solution containing 5 grams of Jet Amine DT (Jetco Chemicals Inc., Corsicana, TX), 2.5 grams glacial acetic acid and 65 grams of water was added slowly to the molten resin to form an initial water-in-oil emulsion. To invert the emulsion, a solution containing 1 gram of glycine in 680 grams of water was heated to 95°C and added slowly to the initial emulsion. After all of the water was added, the emulsion was cooled to 25°C, thereby forming the dispersion, which was then filtered through a 50 micron polypropylene bag filter.

The resulting material was a white, fluid dispersion at 25% solids. The dispersion had a volume average particle size of 1.0 micron, as determined by light scattering, and showed no signs of separation even after high speed centrifugation.

Test Sample Preparation

Tensile Test Samples:

About 27g of the solid polyamide resin were placed in a Carver Laboratory Press apparatus. The resin was pressed at pressures and temperatures sufficient to obtain a pressed sample of uniform thickness. The pressed sample was stamped using a mallot and die to obtain samples for tensile tests. Tensile samples were tested at 23°C, after 24 hour storage at 23°C and 50% humidity, and at 60°C, after 24 hour storage in 60°C water. The tensile tests were conducted according to standard ASTM method D-

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638. The results of the tensile tests for the polyamide resin are found in Table 1.

The polyamide resin dispersion was freeze-dried to remove water, thereby yielding a fine, white powder.

5 Samples for tensile tests were then prepared from the white powder as described above. Results of tensile tests for the polyamide resin dispersion are found in Table 1.

Solvent Double Rub Samples:

films of the resin dispersion were prepared by

drawing down the polyamide resin dispersion on clear glass
plates using a #6 Meyer rod. The films were allowed to
dry and then were heat-cured in a forced air oven at 150°C
for 5 minutes. The films were then allowed to cool to
room temperature. A solvent mixture of hydrocarbons and

alcohols consisting of 2 parts 1-butanol, 1 part 2propanol, and 1 part toluene was prepared. The initial
films were then tested for chemical cross-linking using a
solvent double rub test method as is known to those
skilled in the art. Additional cured films were allowed
to set at room temperature for one week, at which time
final double rub tests were performed. The results of the
solvent double rub test are found in Table 2.

Example 2

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The dispersion prepared in Example 1 was blended with 10% (based on resin solids) Epi-RezTM W55-5003 epoxy resin dispersion (Rhone-Poulenc, Inc., Louisville, KY) at ambient temperature using a simple paddle mixer. The resulting material was a white, fluid dispersion blend. The blend was stable over a period of several months with no signs of creaming or viscosity instability.

Samples of the epoxy polyamide dispersion blend were prepared for tensile testing and solvent double rub testing according to the methods described in Example 1.

Results of those tests are found in Tables 1 and 2,

35 respectively.

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Example 3

A stable, aqueous dispersion of UNI-REZ 2643

(Union Camp Corp.) was prepared as follows. 300 grams of UNI-REZ 2643 and 6 grams of Jet Amine DT (Jetco Chemicals Inc.) were charged to a 1.5 liter glass resin kettle and heated to 170°C. An aqueous solution containing 4 grams of glacial acetic acid in 50 grams of water was added dropwise to the molten resin/surfactant mixture with 570 rpm stirring to form an initial water-in-oil emulsion. To invert the emulsion, an aqueous solution containing 3 grams of glycine dissolved in 650 grams of water was added dropwise with moderate agitation. After all of the water was added, the emulsion was cooled to 25°C with gentle stirring, thereby forming the dispersion, which was then filtered through 50 micron polypropylene bag material.

The resulting material was a white fluid, dispersion at 25% solids. The dispersion was very stable

The resulting material was a white fluid, dispersion at 25% solids. The dispersion was very stable and showed no signs of separation after several weeks on the shelf.

Samples for tensile testing were prepared according to the method described in Example 1 from both the polyamide resin and polyamide resin dispersion.

Results of those tests are found in Table 1.

Example 4

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25 The dispersion prepared in Example 2 was blended with 10% (based on resin solids) Epi-Rez W55-5003 dispersion at ambient temperature using a simple panel mixer. The resulting material was a white, fluid dispersion blend. The resulting blend was stable with no signs of viscosity instability over several weeks at ambient conditions. Samples for tensile testing were prepared according to the method described in Example 1. Results of those tests are found in Table 1.

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Example 5

A high amine number polyamide resin was prepared by reacting 125 equivalents of ethylene diamine (Aldrich Chemical Co.,) with 100 equivalents of Dimer 18 (Union Camp Corp.) The resulting polymer had a ring and ball softening point of 94°C and an amine number of 35. A polyamide resin dispersion was prepared from the polyamide resin according to the methods described in Example 1, using 2% Jet Amine DT (Jetco Chemicals Inc.), based on resin solids. The resulting material was a white, fluid dispersion at 40% solids and showed no signs of separation or gelation. Samples for tensile testing were prepared according to the method described in Example 1 from both the polyamide resin and the resin dispersion. Tensile tests were conducted at 23°C. Results are found in Table 1.

Samples for solvent double rub testing were also prepared from the polyamide resin dispersion according to the method described in Example 1. Results are found in 20 Table 2.

Example 6

The polyamide resin dispersion of Example 5 was blended with 10 percent (based on resin solids) RDX 80204 epoxy dispersion (Rhone-Poulenc, Inc., Louisville, KY).

The resulting epoxy/polyamide dispersion blend was stable and showed no signs of thickening over a 1 month period. Samples were prepared for tensile testing at 23°C and for solvent double rub testing according to methods described in Example 1. Test results are found in Tables 1 and 2, respectively.

Example 7

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The polyamide dispersion of Example 5 was blended with 30 percent (based on resin solids) RDX 80204 epoxy dispersion (Rhone-Poulenc, Inc.). The resulting epoxy/polyamide dispersion blend was stable and showed no

signs of thickening over a one month period. Samples were prepared for solvent double rub testing according to the method described in Example 1. Results are found in Table 2.

5 Example 8

A stable, epoxy resin dispersion was prepared as follows. 200 grams Epon 828 (Shell Chemical Co., Houston, TX), 1 gram Triton X-207 (Rohm and Haas, Philadelphia, PA), and 2.5 grams Triton X-405 were charged to a glass resin kettle. The mixture was heated to 80°C and 200 grams of water were added dropwise with 600 rpm stirring to form an emulsion. The emulsion was allowed to cool to 25°C, thereby forming the dispersion, which was then filtered through 50 micron bag material.

The resulting material was a white, fluid dispersion. This sample showed a slight degree of separation upon standing, but could be redispersed with mild agitation.

Example 9

20 A stable, polyamide resin dispersion of UNI-REZ 2646 was prepared according to the method described in Example 1, using 1% Tryfac 5556 (Henkel Corp., Mauldin, SC), based on resin solids. Samples for tensile testing at 23°C were prepared according to the method described in 25 Example 1 from both the polyamide resin and the resin dispersions. Results are found in Table 1.

Example 10

The polyamide resin dispersion of Example 9 was blended with 10 percent (based on resin solids) of the epoxy resin dispersion prepared in Example 8. The resulting material was a tan colored, fluid dispersion which was stable for several weeks. Samples were prepared for tensile testing at 23°C according to the method described in Example 1. Results are found in Table 1.

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	2,09	Break Strain	213 114 769	147 151 594		
ļ		Break Stress psi	116 85 901	186 215 1867		
TABLE 1 TENSILE DATA	23°C	Break Strain	444 270 751	160 142 502	23 376 258 54	120 65 358
		Break Stress psi	301 268 1271	324 328 2370	386 264 958 1752	577 433 1112
		Sample Example 1	Polyamide Resin Polyamide Dispersion Example 2	Example 3 Polyamide Resin Polyamide Dispersion Example 4	Example 5 Polyamide Resin Polyamide Dispersion Example 6 Example 7	Example 9 Polyamide Resin Polyamide Dispersion Example 10

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TABLE 2 SOLVENT DOUBLE RUB^(I) DATA

	Sample	<u>Initial</u>	One Week
5	Example 1 Dispersion Example 2	15 13	15 100
	Example 5 Dispersion Example 6 Example 7	14 32 >100	14 >100 >100

⁽¹⁾ Number of Cycles

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What is claimed is:

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- 1. A stable, curable epoxy resin and polyamide resin composition comprising, in combination:
- (a) a stable, non-solvated, aqueous 5 dispersion of an epoxy resin having unreacted epoxy groups; and
 - (b) a stable, non-solvated, aqueous dispersion of a polyamide resin having excess acid or amine groups.
- 2. A composition according to Claim 1 wherein said polyamide resin has a low acid and a low amine number.
- 3. A composition according to Claim 1 wherein said polyamide resin is a polymerized fatty acid polyamide 15 resin.
 - 4. A composition according to Claim 1 wherein said epoxy resin dispersion and said polyamide resin dispersion each have a high resin content.
- 5. A method for preparing a stable, curable 20 epoxy resin and polyamide resin composition comprising:
 - (a) preparing a stable, non-solvated, aqueous dispersion of epoxy resin having unreacted epoxy groups;
- (b) preparing a stable, non-solvated, 25 aqueous dispersion of polyamide resin with excess acid or amine groups; and
 - (c) blending said epoxy resin dispersion with said polyamide resin dispersion at a temperature between about 0°C and 90°C.
- 30 6. A method according to Claim 5 wherein said polyamide resin has a low acid and a low amine number.

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7. A method according to Claim 5 wherein said polyamide resin is a polymerized fatty acid polyamide resin.

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- 8. A method according to Claim 5 wherein said 5 epoxy resin dispersion and said polyamide resin dispersion each have a high resin content.
 - 9. A method according to Claim 5 wherein said epoxy resin and polyamide resin dispersions are blended at room temperature.

INTERNATIONAL SEARCH REPORT

International application No. PCT/US92/03558

A. CLASSIFICATION OF SUBJECT MATTER IPC(5) :C08L 63/00 US CL :523/414				
	to International Patent Classification (IPC) or to bo LDS SEARCHED	th national classification and IPC		
	documentation searched (classification system follow	ved by classification symbols)		
U.S. :	523/414			
Documenta	tion searched other than minimum documentation to t	he extent that such documents are included	d in the fields searched	
	data base consulted during the international search (see Extra Sheet.	name of data base and, where practicable	e, search terms used)	
C. DOC	CUMENTS CONSIDERED TO BE RELEVANT			
Category*	Citation of document, with indication, where	appropriate, of the relevant passages	Relevant to claim No.	
x	US, A, 2,811,495 (WITTCOFF ET AL.) 29 Octo	ober 1957 (See the entire document).	1-9	
х	US,A, 3,956,208 (HOKI ET AL.) 11 May 1976 (See the entire document).			
X	JP, A, 62-1448582 (DAINIPPON INK & CREAN	1, 3-5		
X	JP, A, 59-71339 (TOUTOU KIKI KK) 23 April 1	1, 3-5		
X	JP, A, 63-10643 (TOTO LTD) 18 January 1988,	Abstract	1, 3-5	
Further documents are listed in the continuation of Box C. See patent family annex.				
* Special categories of cited documents: "A" later document published after the international filing date or prior date and not in conflict with the application but cited to understand on the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to understand the conflict with the application but cited to underst			tion but cited to understand the	
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special reason (as specified) "Y" document of particular relevance; the claimed invention cannol considered to involve an inventive step when the documen combined with one or more other such documents, such combina being obvious to a person skilled in the art			step when the document is documents, such combination	
P° document published prior to the international filing date but later than '&' document member of the same patent family the priority date claimed				
Date of the actual completion of the international search Date of mailing of the international search report			rch report	
13 JULY 1992 1 4 SEP 1992				
Name and mailing address of the ISA/ Commissioner of Patents and Trademarks Box PCT RANDY GUŁAKOWSKI			Sonla	
•	D.C. 20231 NOT APPLICABLE	Telephone No. (703) 308-2351		

INTERNATIONAL SEARCH REPORT

International application No. PCT/US92/03558

B. FIELDS SEARCHED

Electronic data bases consulted (Name of data base and where practicable terms used):

APS Text Search (US and Japan)

L1	63 S FATTY ACID POLYAMID#
L2	22 S L1 AND EPOXY
L3	6 S L2 AND DISPERSION
L4	0 S L2 AND AQUEOUS DISPERSION#
L5	5 S L2 AND AQUEOUS DISPERSION#
L6	5 S (POLYAMIDE# AND EPOXY AND DISPERSION#) /AB
L7	8 S (FATTY ACID POLYAMIDE#) /AB
L8	1 S L7 AND EPOXY /AB
L9	0 S L8 AND DISPERSION
L10	18 S FATTY ACID EPOXY
L11	4 S L10 AND EPOXY
L12	0 S L11 AND DISPERSION#
L13	28 S POLYAMIDE# AND EPOXY AND DISPERSION
L14	3 S POLYAMIDE# AND EPOXY AND AQUEOUS DISPERSION