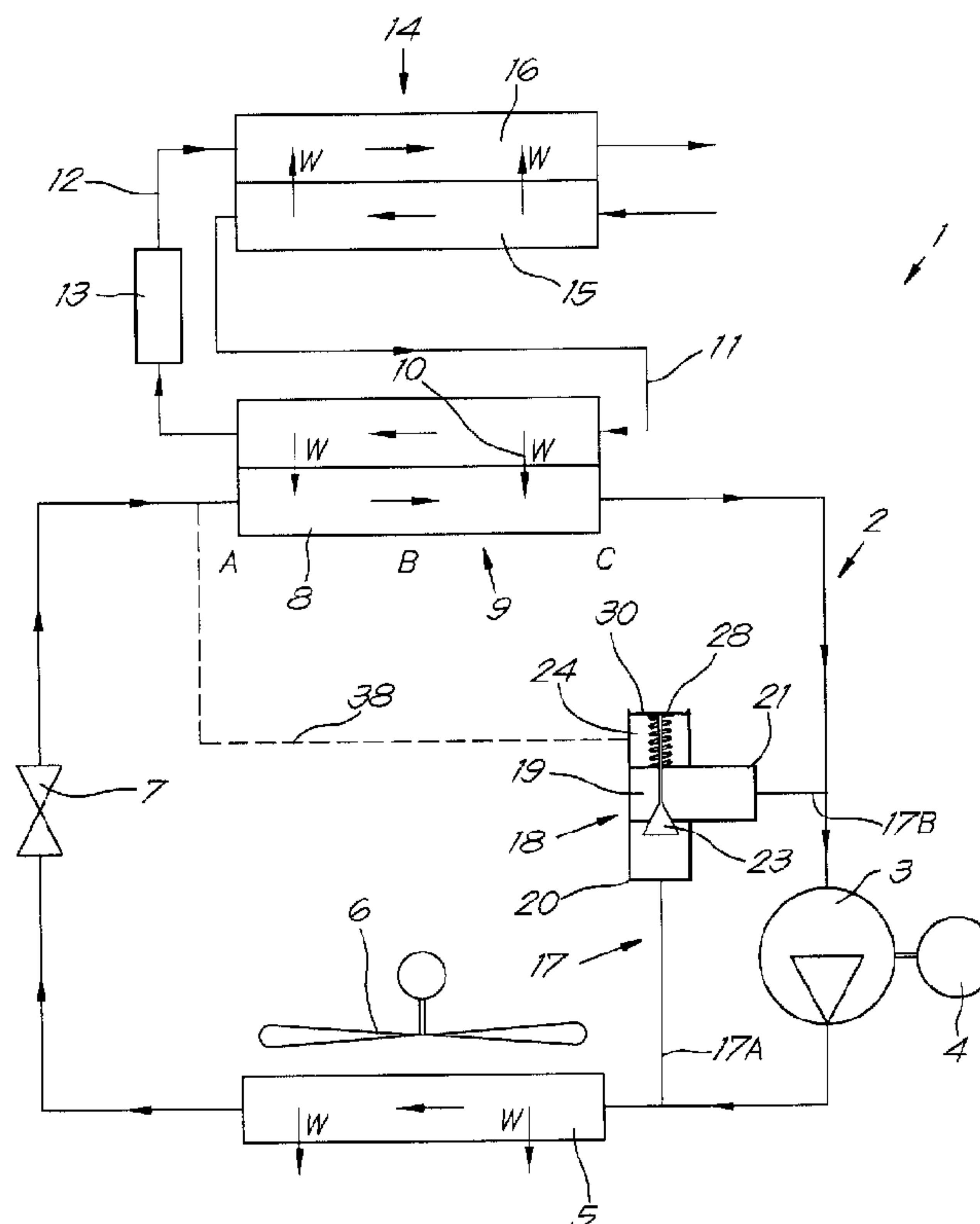




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(54) Titre : DISPOSITIF ET PROCEDE DE SECHAGE A FROID D'UN GAZ
(54) Title: DEVICE AND METHOD FOR COOL DRYING A GAS



(57) Abrégé/Abstract:

Device for cool drying a gas that consists of a closed cooling circuit (2) with a compressor (3), and which further in the direction of flow (M) of the coolant successively contains a condenser (5), an expansion means (7) followed by an evaporator (8), that constitutes the primary part of a heat exchanger (9) with a secondary part (10) through which the gas to be dried is guided, and whereby there is a bypass pipe (17) in the cooling circuit (2) that can be closed by means of a bypass valve (18) with a valve element (23) and a pressure-sensitive element (30) acting on it that is exposed to a local control pressure in the cooling circuit (2), whereby the control pressure pipe (38) is connected to the closed cooling circuit (2) upstream of the outlet of the evaporator (8).



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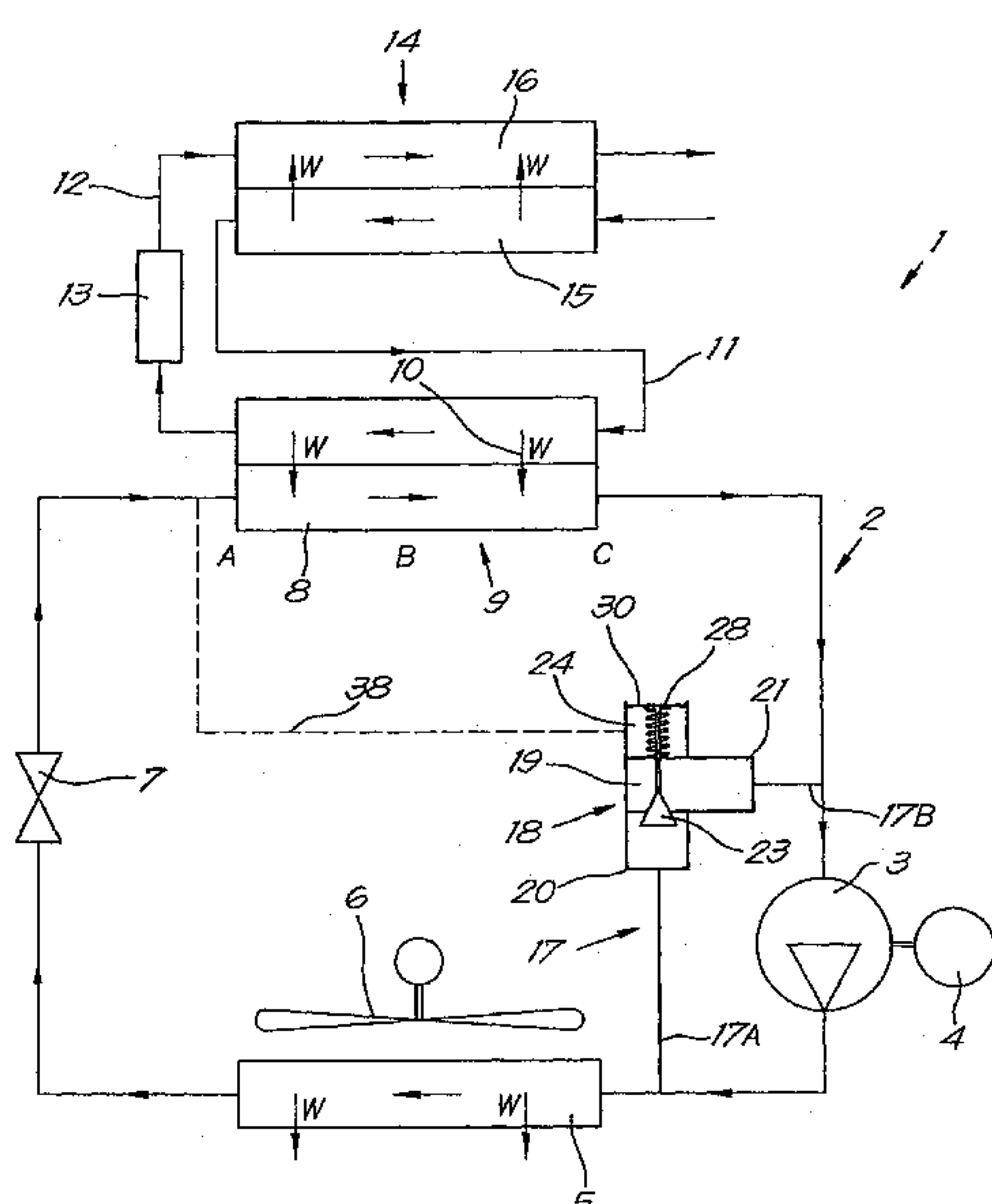


Fig.5

(57) Abstract: Device for cool drying a gas that consists of a closed cooling circuit (2) with a compressor (3), and which further in the direction of flow (M) of the coolant successively contains a condenser (5), an expansion means (7) followed by an evaporator (8), that constitutes the primary part of a heat exchanger (9) with a secondary part (10) through which the gas to be dried is guided, and whereby there is a bypass pipe (17) in the cooling circuit (2) that can be closed by means of a bypass valve (18) with a valve element (23) and a pressure-sensitive element (30) acting on it that is exposed to a local control pressure in the cooling circuit (2), whereby the control pressure pipe (38) is connected to the closed cooling circuit (2) upstream of the outlet of the evaporator (8).

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Device and method for cool drying a gas.

5 The present invention relates to a device and method for cool drying a gas.

Cool drying is applied for example in compressors that supply a hot compressed gas that is often saturated with water.

10

This compressed gas first has to be dried before it can be supplied to a pneumatic network because the moisture in the gas can be harmful to the components and tools in the pneumatic network as moisture can lead to corrosion or the
15 accumulation of water in tools that are not designed for that purpose.

Cool drying is based on the principle that by cooling a gas that is saturated or partly saturated with water, moisture
20 is removed from the gas as the moisture condenses and the condensed water is removed, after which the gas is again heated up whereby it is no longer saturated and is thus dryer.

25 For cool drying, a device is used that primarily consists of a closed cooling circuit that contains a coolant that can be circulated in the circuit by a compressor and which further contains, successively in the direction of flow of the coolant, a condenser connected to an outlet of the
30 compressor; an expansion means followed by an evaporator connected to an inlet of the aforementioned compressor,

whereby the evaporator forms the primary part of a heat exchanger with a secondary part through which the gas to be dried is guided.

5 As a result of the evaporation of the coolant in the evaporator, or thus the primary part of the heat exchanger, as is known, heat is extracted from the gas to be dried flowing through the secondary part, whereby this gas to be dried is cooled and, after evacuation of the condensate
10 formed, is heated up again.

Such a device is designed for a nominal load for drying a normal gas flow.

15 In the unloaded state, in other words when no gas to be dried is flowing through the heat exchanger, the cooling capacity of the cooling circuit is too high, such that freezing can occur in or after the evaporator, which must absolutely be avoided.

20

Moreover the coolant in the cooling circuit is continually pumped around without the cooling capacity of the cooling circuit being usefully employed for drying the gas, such that a lot of energy is lost.

25

A known solution to this is to provide a bypass pipe in the closed cooling circuit with a bypass valve in it, which, on the one hand, is closed when the device is loaded, or in other words when a gas to be dried flows through the heat
30 exchanger and, on the other hand is open when the device is

unloaded and thus no gas to be dried flows through the heat exchanger.

In loaded situations the bypass pipe thus has no effect as
5 it is then closed, and as a result of this the cooling
circuit operates at full capacity as the entire flow of
coolant that is compressed by the compressor is also guided
through the condenser and the expansion means, which
together ensure considerable cooling of the coolant, and as
10 this full flow of cold coolant also flows through the
evaporator in the heat exchanger to cool the gas to be
dried.

In the unloaded state on the other hand the open valve
15 ensures that the compressor is bypassed and that, as a
result of this, at least a part of the coolant compressed
by the compressor does not flow through the condenser and
the expansion means and this part of the coolant is thus
not cooled by expansion such that there is much less
20 cooling in the evaporator and thus there is much less risk
of freezing in or downstream of the evaporator.

Downstream and upstream are considered in the direction of
flow of the coolant in the closed cooling circuit.

25

For a bypass valve that can fulfil the aforementioned
functions, it is known to use a type of valve known by the
name of 'hot gas bypass' (HGBP), and more specifically this
type of valve is a pressure-controlled bypass valve with a
30 valve element that is held in a closed position under the
influence of a spring element to close the bypass pipe, and

which is also provided with a pressure-sensitive element that acts on the aforementioned valve element, and which, when it is subject to a sufficient pressure drop, can open the valve against the spring force.

5

In the known devices, the pressure-sensitive element is exposed to a control pressure that is tapped off locally from a point downstream of the evaporator via an internal control pressure pipe in the circuit, more specifically at
10 the point where the bypass pipe leads into the cooling circuit.

When such a device changes from an unloaded state to a loaded state through a quantity of gas to be dried suddenly
15 being driven through the heat exchanger, the temperature in the evaporator increases due to the heat transfer from the gas to be dried to the cooler coolant in the evaporator, such that more coolant evaporates in the evaporator, which itself increases the pressure in the evaporator and also
20 downstream of the evaporator, and this pressure increase is felt by the bypass valve which will thereby close when the pressure increase is sufficient.

A feature of the control characteristic of an HGBP valve is
25 a given pressure difference of the control pressure between the unloaded and loaded state, which in known devices in a loaded state results in a relatively high pressure of the coolant at the outlet of the evaporator, and thus also in the evaporator where the pressure is even higher as a
30 result of the frictional losses that occur when coolant flows through the evaporator.

As the coolant in the closed cooling circuit is in a two-phase region, there is an unambiguous relationship between the pressure and temperature of the coolant: a higher
5 pressure in the evaporator also implies a higher temperature in the evaporator.

This leads to the disadvantage that the gas to be dried is not cooled optimally for drying by the evaporator, which
10 results in a higher pressure dew point of the gas at the outlet of the secondary part of the heat exchanger, whereby at this outlet the aim is for the lowest possible temperature (the lowest temperature of the gas to be dried is also called the LAT or 'Lowest Air Temperature' -
15 although the term LAT is also used for gases other than air) and corresponding pressure dew point of the gas for good drying.

The purpose of the present invention is to provide a
20 solution to one or more of the aforementioned and/or other disadvantages by providing a device for cool drying a gas that primarily consists of a closed cooling circuit that contains a coolant that can be circulated in the cooling circuit by a compressor, and which further in the direction
25 of flow of the coolant successively comprises a condenser connected to the outlet of the compressor; an expansion means followed by an evaporator connected to the inlet of the aforementioned compressor, whereby the evaporator constitutes the primary part of a heat exchanger with a
30 secondary part through which the gas to be dried is guided, and whereby there is a bypass pipe in the cooling circuit

that can be closed by means of a bypass valve with a valve element that is kept in a closed position under the influence of a spring element and with a pressure-sensitive element that acts on the valve element, and which, via a control pressure pipe, is exposed to a local control pressure in the circuit where the control pressure pipe is connected to the circuit, whereby the control pressure pipe is connected to the closed cooling circuit upstream of the outlet of the evaporator.

10

By connecting the control pressure pipe at a point of the cooling circuit upstream of the evaporator outlet, for example in the evaporator or upstream of the evaporator, instead of downstream as in the known devices, and this in a device that is otherwise identical, a number of important advantages are obtained.

15

An advantage is that when the cool dryer is loaded, the pressure and temperature of the coolant in the evaporator and at its outlet is less than with a conventional connection downstream, such that the gas to be dried can be cooled more intensively to a lower pressure dew point and thereby more liquid can be removed from the gas to be dried through condensation, with better drying as a result.

20

An advantage attached to this is that to dry a given flow of gas with a certain desired lowest air temperature (LAT) at the outlet of the secondary part of the heat exchanger, a smaller and more compact exchanger is sufficient, or that with a given heat exchanger the same flow rate can be cooled to a lower LAT.

25

30

Another advantage is that the pressure dew point only increases slightly during the transition from the unloaded to the loaded state, and that in the event of a varying
5 load the pressure dew point varies less and is thus more constant.

In a preferred embodiment, an additional restrictor can be placed in the cooling circuit upstream of the evaporator,
10 more specifically between the evaporator and the point upstream of the evaporator where the control pressure pipe is connected to the cooling circuit.

This has the beneficial effect that the average pressure in
15 the evaporator and at the outlet of the evaporator in a loaded state will decrease even more and come closer to the pressure in the unloaded state, such that the aforementioned advantages are amplified.

20 The invention also relates to a method for cool drying a gas by means of a device that primarily consists of a closed cooling circuit that contains a coolant that is circulated in the cooling circuit by a compressor and which further comprises, successively in the direction of flow of
25 the coolant, a condenser connected to the outlet of the compressor; an expansion means followed by an evaporator connected to the inlet of the aforementioned compressor, whereby the evaporator constitutes the primary part of a heat exchanger with a secondary part through which the gas
30 to be dried is guided and whereby there is a bypass pipe in the cooling circuit that can be closed by means of a bypass

valve with a valve element that is kept in a closed position under the influence of a spring element, whereby when the device is loaded, the bypass valve is opened against the spring force of the spring element when the
5 pressure in the closed cooling circuit, at a point upstream of the outlet of the evaporator, is higher than a set value.

With the intention of better showing the characteristics of
10 the invention, a preferred embodiment of a device according to the invention for cool drying a gas and a method applied with it is described hereinafter by way of an example, without any limiting nature, with reference to the accompanying drawings, wherein:

15

figure 1 schematically shows a device for cool drying of the known type in the fully loaded state;

figure 2 shows the section designated in figure 1 by the arrow F2 on a larger scale;

20 figure 3 shows the pressure curve of the coolant in the evaporator of figure 1;

figure 4 shows the device of figure 1 in the unloaded state;

25 figure 5 schematically shows a device according to the invention;

figure 6 shows the pressure curve of the coolant in the evaporator of figure 5;

figure 7 shows a variant of a device according to the invention;

30 figure 8 shows the pressure curve of the coolant in the evaporator of figure 7;

figure 9 shows a variant of a device according to the invention; and

figure 10 shows the pressure curve of the coolant in the evaporator of figure 9.

5

The known device 1 for cool drying gases shown in figure 1 comprises a cooling circuit 2 that contains a coolant that can be circulated in the circuit by a compressor 3 driven by means of a motor 4 or similar, preferably but not necessarily, a motor with a constant speed.

10

The direction of flow of the coolant in the circuit is indicated by the arrows M. Upstream and downstream are defined according to this direction of flow M.

15

Further the cooling circuit 2 contains, successively in the direction of flow of the coolant, a condenser 5 connected to an outlet of the compressor 3 and which for example is cooled by means of a fan 6; expansion means 7, for example in the form of an expansion valve; an evaporator 8 connected to an inlet of the aforementioned compressor 3 and which forms part of a heat exchanger 9 with a primary part that is formed by the evaporator 8 and a secondary part through which the gas to be dried is driven in the direction of the arrows L via a supply pipe 11 in order to be cooled by the evaporator 8.

20

25

The gas cooled in the heat exchanger 8 is first driven through a liquid separator 13 via an outlet pipe 12 and then through a heat exchanger 14 to again heat up the cooled gas.

30

In this case this heat exchanger 14 makes use of the recuperation heat contained in the supplied gas to be dried and to this end consists of a primary part 15 that is incorporated in the aforementioned supply pipe 11 and a secondary part 16 that is incorporated in the outlet pipe 12.

The presence of the liquid separator 13 and heat exchanger 14 is not necessary and can be omitted for certain applications in which the dried air is still partially or entirely saturated with water.

The cooling circuit 2 is further equipped with a bypass pipe 17 connected to the cooling circuit 2 in order to bypass the compressor 3, and which to this end is placed between the inlet and outlet of the compressor 3.

The bypass pipe 17 can be closed by means of a bypass valve 18 that is placed between a first section 17A of the bypass pipe 17 connected to the cooling circuit 2 on the outlet side of the compressor 3, and a second section 17B connected to the cooling circuit 2 along the inlet side of the compressor 3, more specifically downstream of the evaporator 8.

The bypass valve 18 is equipped with a flow-through channel 19 with an inlet 20 connected to the first section 17A of the bypass pipe 17 and an outlet 21 connected to the second section 17B of the bypass pipe 17.

As shown in more detail in figure 2, the inlet 20 is separated from the outlet 21 by a passage 22 that can be closed off by means of a valve element 23.

- 5 The bypass valve 18 further comprises a closed pressure chamber 24 that is separated from the flow-through channel 19 by a separating wall 25 with a wall passage 26.

10 The valve element 23 has a valve stem 27 that partially extends through the aforementioned wall passage 26 into the pressure chamber 24, and which at its end has a spring seat 28 for a spring 29 that is compressed between the aforementioned separating wall 25 and the spring seat 28 and which keeps the valve element 23 in a closed state.

15

The pressure chamber 24 has a pressure-sensitive element, for example in the form of a membrane 30 that closes off the pressure chamber 24 and which is in contact with the aforementioned spring seat 28.

20

The aforementioned membrane 30 forms a separation between the aforementioned pressure chamber 24 and a second pressure chamber 31 that is connected to a 'bulb' 33 via a capillary tube 32. As this bulb 33 is of no further
25 importance for the invention, its role shall not be explained further.

The bypass valve 18 also has, in this case, an internal control pressure pipe 34 via which the pressure chamber 24
30 is connected to the outlet 21 in order to sense, via the section 17B of the bypass pipe 17, the pressure in the

cooling circuit 2 downstream of the evaporator 8. It goes without saying that the control pressure pipe 34 can also be constructed in the form of an external pipe.

- 5 The operation of the known device 1 described above is illustrated in the loaded state on the basis of figures 1 and 2 in which the bypass pipe 17 is closed by the bypass valve 18.
- 10 The motor 4 drives the compressor that circulates the coolant in the cooling circuit in the direction of the arrows M.

The compressed gaseous coolant is then cooled in the
15 condenser 5, such that it changes from the gas phase to the liquid phase.

The coolant then undergoes an expansion by the expansion means 7, such that the temperature of the coolant falls
20 drastically.

This cooled coolant then flows through the evaporator 8 where it comes into thermal contact with the gas to be dried flowing through the secondary part 10 of the heat
25 exchanger 9, of which the evaporator forms the primary part.

As a result, the gas to be dried is cooled and is generally saturated with water vapour, whereby the moisture in the
30 gas condenses into droplets that can be removed via the liquid separator 13.

By heating up the cold gas after the liquid separator 13 in the heat exchanger 14, the relative humidity falls and the gas thus becomes dryer.

5

In the evaporator 8 the coolant that enters in the liquid phase evaporates due to the heat transfer from the gas to be dried to the coolant. The direction of the heat transfer in the heat exchangers is indicated by the arrows W.

10

The gas that leaves the evaporator 8 is again sucked in by the compressor 3 and is further pumped around the cooling circuit 2, so that the coolant can begin the next cooling cycle.

15

As a result of the evaporation of the coolant in the evaporator 8 the pressure in the evaporator, as well as downstream of the evaporator 8, increases, and thus also in the pressure chamber 24, which is connected to the cooling circuit 2 via the section 17B of the bypass pipe. Due to the relatively high pressure in the pressure chamber 24, the membrane 30 is loaded in the sense that it reinforces or counteracts less the action of the spring 29 on the valve element 23.

25

As a result the passage 22 is kept closed in loaded conditions by the valve element 23 and no coolant flows through the bypass pipe, such that the entire flow that is compressed by the compressor 3 also flows through the condenser 5, the expansion means 7 and the evaporator 8.

30

Because this entire flow flows through the evaporator 8, there is also a relatively large pressure drop across the evaporator 8 due to the frictional losses of the flow.

5 The change of the average pressure along the path of the coolant through the evaporator 8 in the cooling circuit 2 between a point A, which, as shown in figure 1, is situated at the inlet of the evaporator 8, through a point B in the evaporator 8 to a point C at the outlet of the evaporator
10 8, is shown as curve 35 in figure 3, whereby the pressure difference between A and C is due to the aforementioned pressure drop in the evaporator 8.

When the load is suddenly removed and no further gas to be
15 dried flows through the heat exchanger 9, as schematically shown in figure 4, then there is no further heat supply to the coolant in the evaporator 8.

The evaporation of the coolant thus partly stops, such that
20 the pressure in the evaporator decreases and thus also the pressure in the pressure chamber 24, and this pressure is in fact an underpressure that pulls the membrane 30 inwards into the pressure chamber 24. When the underpressure is sufficiently low, the force of the spring 29 is overcome by
25 the strong suction force on the membrane 30 and the valve element 23 of the passage 22 is pushed away such that it opens.

The bypass pipe 17 is now open, such that a part of the
30 flow compressed by the compressor 3 is immediately sucked in again by the compressor 3 without flowing through the

condenser 5, expansion valve 7 and the evaporator 8, while the remaining flow still flows through the entire cooling circuit 2.

- 5 The pressure curve between points A and C in the unloaded state is shown as curve 36 in figure 3, in which the curve 35 of the loaded state is already shown.

The curve 35 of the loaded state is situated completely
10 above the curve 36 of the unloaded state, which is due to the pressure increase that occurs in the evaporator 8 when loaded as a result of the heat transfer from the gas to be dried to the coolant in the evaporator 8 and due to the fact that the valve needs a certain pressure difference
15 Δp_{ref} to be able to act on the pressure increase.

The pressure curve according to the curve 35 in the loaded state is also steeper than the curve 36 in the unloaded state, which is the result of higher load losses in the
20 evaporator 8 on account of the fact that in the loaded state, the entire flow flows through the evaporator 8, while in the unloaded state only a part of this flow flows through the evaporator 8 as the other part is diverted through the bypass pipe 17.

25

It is a characteristic of the bypass valve 18 that the pressure difference between the unloaded and loaded state at the point where the control pressure is tapped off approaches the constant value Δp_{ref} . This value Δp_{ref} depends
30 on various factors such as the pressure losses, the relative capacity of the compressor, the expansion and

similar. In order to be able to bypass a certain power, a certain valve position difference is needed. A certain valve position difference always requires a fixed pressure difference: this is Δp_{ref} .

5

This Δp_{ref} can be read from figure 3 at the point C, as the control pressure in the case of the known device is tapped off downstream of the evaporator 8.

10 Figure 3 also schematically shows the 'freezing line' 37, which shows at what pressure there is a risk of freezing.

The device is generally set up so that the curve 36 in the unloaded state is just above this horizontal freezing line
15 37.

In the loaded state the curve 35 is situated far above the freezing line, which results in inefficient cooling with relatively high temperatures in the evaporator, and thus
20 inefficient drying.

The invention is explained hereinafter on the basis of the device of figure 5 that differs from the known device of figure 1 in the fact that the pressure chamber 24 of the
25 bypass valve 18 is connected via an external control pressure pipe 38 to the cooling circuit 2 at a point A upstream of the evaporator 8 instead of a point downstream of the evaporator 8.

30 The device 1 according to the invention, as was the case with the conventional device of figure 1, is set up such

that in the unloaded state the pressure curve in the evaporator 8 is just above the freezing line 37.

This pressure curve in the unloaded state is shown in figure 6 for the device of figure 5 as curve 39, whereby this curve 39, given the aforementioned setting, coincides with the curve 36 of the conventional device.

In the event of changing from the unloaded to the loaded state, the effect of the connection of the external control pressure pipe 38 at point A upstream of the evaporator 8 can be seen, as now the aforementioned characteristic pressure difference Δp_{ref} in the bypass valve 18 will be at point A instead of point C, as was the case in figure 3. This thus determines the pressure at point A when loaded.

The further change of pressure in the evaporator 8 when loaded is primarily determined by the load losses due to the flow of the coolant through the evaporator 8.

20

The pressure drop between A and C in the loaded state will be equal to the pressure drop between A and C in figure 3 for a cooling circuit with the same flow.

This results in the curve 40 when loaded, which is shown in figure 6 next to the corresponding curve 35 under a load for a conventional device.

An advantage of the invention is that the curve 39 in the case of the invention in the loaded state is lower with respect to the curve 35 for a similar conventional

30

situation, and is thus closer to the aforementioned horizontal freezing line 37, such that the coolant can cool the air to be dried more intensively, which results in better drying.

5

It can be derived from figure 6 that due to the application of the invention, the curve 39 in the unloaded state and the curve 40 in the loaded state are closer together, which points to lower pressure and temperature differences
10 occurring between a loaded and unloaded state, with a more constant pressure dew point of the dried air as a favourable result.

The second pressure chamber 31, the capillary tube 32 and
15 the bulb 33 are not strictly necessary for the invention and can thus be omitted, as shown in figure 5, although they can also be present as they do not interfere with the invention.

20 Alternatively with respect to the embodiment of figure 5, the pressure control pipe 38 can also be connected to the closed cooling circuit 2 at a point in the evaporator 8, which means at a point in the inlet or at a point between the inlet and outlet of the evaporator 8. The favourable
25 effect of the invention will then be all the greater as the point where the pressure control pipe 38 is connected to the closed cooling circuit 2 is located further upstream of the outlet of the evaporator 8.

30 What is important for obtaining the favourable effect of the invention is that the pressure control pipe 38 is

connected to the closed cooling circuit 2 at a point upstream of the outlet of the evaporator 8 and at a distance from this outlet and preferably upstream of the evaporator 8.

A variant of a device according to the invention is shown in figure 7, which differs from the device of figure 5 in that there is a restrictor 41 in the cooling circuit 2 upstream of the evaporator 8, more specifically between the inlet A of the evaporator 8 and the point R where the external control pressure pipe 38 is connected to the cooling circuit 2.

10 The result of such a restrictor 41 is clearly shown on the basis of figure 8, which shows the pressure curve between the points R and C as curve 42 in the loaded state and curve 43 in the unloaded state.

The effect of the restrictor 41, both in the loaded and unloaded state, can be seen as a sharp pressure drop between R and A that is larger in the loaded state than in the unloaded state, as in the loaded state the entire flow of compressed coolant flows through the restrictor 41, while in the unloaded state only a part of it.

The pressure drop across the evaporator 8, in other words between points A and C, is similar to the situation of figure 6 without the restrictor 41.

20 The distance between the curves 42 and 43 is determined this time by the pressure difference Δp_{ref} that is realised by the bypass valve 18 at the point R where the control pressure pipe 38 is connected to the cooling circuit 2.

It is clear from figure 8 that, thanks to the restrictor 41, the curves 42 and 43 are even closer together than the curves 39 and 40 of figure 6 for a situation without the restrictor 41, and the curve 42 is even closer to the freezing line 37 such that in the loaded state the cooling can be even deeper.

Through a suitable choice of the restrictor 41, it can be ensured that at point C at the outlet of the evaporator 8, the curves 42 and 43 coincide, such that at the outlet of the evaporator 8 there is no difference between a loaded and unloaded situation, or can even ensure that at this point the curve 42 is below the curve 43, and the loaded state enables cooling to a situation close to freezing.

Figure 9 shows another variant of the invention that also presents advantages with respect to the known devices as outlined in figure 1.

10 The device of figure 9 is analogous to that of figure 7, with the difference that the bypass pipe 17 not only bypasses the compressor 3, but also the evaporator 8 so that the same flow always flows through the evaporator 8, irrespective of whether the bypass valve 18 detects a loaded or unloaded state.

The pressure drop in the evaporator will be the same in the loaded and unloaded state, which is illustrated in figure 10 with the curves 44 and 45 respectively for a loaded and unloaded state.

This shows the favourable effect of the restrictor 41 that brings both curves closer together compared to the existing situations.

It is clear that in all cases the bypass valve 18 is adjustable if need be, for example by adjusting the force of the spring.

20 Referring now to figures 7 and 9, the restrictor 41 is chosen such that in the loaded state the pressure of the coolant in the cooling circuit 2 at the outlet of the evaporator 8 is chosen such that the corresponding temperature of the coolant at the outlet of the evaporator 8 is equal or approximately equal to 0°C.

The present invention is by no means limited to the embodiments described as an example and shown in the drawings, but a device and method for cool drying according to the invention can be realised in all kinds of variants.

CLAIMS:

1. Device for cool drying a gas that primarily consists of a closed cooling circuit (2) that contains a coolant that can be circulated in the cooling circuit (2) by means of a compressor (3), and which further in the direction of flow (M) of the coolant successively comprises a condenser (5) connected to the outlet of the compressor (3); an expansion means (7) followed by an evaporator (8) connected to the inlet of the aforementioned compressor (3), whereby the evaporator (8) constitutes the primary part of a heat exchanger (9) with a secondary part (10) through which the gas to be dried is guided, and whereby there is a bypass pipe (17) in the cooling circuit (2) that can be closed by means of a bypass valve (18) with a valve element (23) that is kept in a closed position under the influence of a spring element and with a pressure-sensitive element (30) that acts on the valve element (23), and which, via a control pressure pipe (38), is exposed to a local control pressure in the cooling circuit (2) where the control pressure pipe (38) is connected to the cooling circuit (2), characterised in that the control pressure pipe (38) is connected to the closed cooling circuit (2) upstream of the outlet of the evaporator (8).
2. Device according to claim 1, characterised in that the control pressure pipe (38) is connected to the closed cooling circuit (2) upstream of the evaporator (8).
3. Device according to claim 1 or 2, characterised in that one end of the bypass pipe (17) is connected to the cooling circuit (2) at a point located between the outlet of the compressor (3) and the condenser (5) and the other end is connected to a point of the cooling circuit (2) located between the outlet of the evaporator (8) and the inlet of the compressor (3).
4. Device according to claim 1 or 2, characterised in that one end of the bypass pipe (17) is connected to the cooling circuit (2) at a point located between the outlet of the compressor (3) and the condenser (5), and the other end is connected to a

point of the cooling circuit (2) located between the expansion means (7) and the inlet of the evaporator (8).

5. Device according to any one of the previous claims 1 to 4, characterised in that the bypass valve is such that when loaded the valve element (23) is opened against the force of the spring as of a set value of the aforementioned control pressure and that this value is adjustable.

6. Device according to any one of the previous claims 1 to 5, further characterised in that there is a restrictor (41) in the cooling circuit (2) between the expansion means (7) and the inlet of the evaporator (8).

7. Device according to claim 6, characterised in that the restrictor (41) is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is approximately equal to the pressure of the coolant at the outlet of the evaporator (8) in an unloaded state.

8. Device according to claim 6, characterised in that the restrictor (41) is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is less than or equal to the pressure of the coolant at the outlet of the evaporator (8) in an unloaded state.

9. Device according to any one of claims 6 to 8, characterised in that the restrictor (41) is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is chosen such that the corresponding temperature of the coolant at the outlet of the evaporator (8) is equal or approximately equal to 0°C.

10. Device according to any one of the previous claims 1 to 9, characterised in that the bypass valve (18) used is an 'HGBP' valve (Hot Gas Bypass) with the external control pressure pipe (38).

11. Device according to claim 10, characterised in that the bypass valve (18) has a flow-through channel (19) with a closable passage (26) and a closed pressure chamber (24) that is connected via the aforementioned control pressure pipe (38) to the cooling circuit (2), and that the pressure-sensitive element (30) is a membrane that closes an opening of the pressure chamber (24) and which is located opposite a separating wall (25) between the flow-through channel (19) and the pressure chamber (24), whereby the valve element (23) is equipped to close the aforementioned passage (26) and has a valve stem (27) that extends partly via the wall passage (26) in the aforementioned separating wall (25) into the pressure chamber (24), and which on the end located in the pressure chamber (24) has a spring seat (28) for a spring (29) that is compressed between the aforementioned separating wall (25) and the spring seat (28) and which keeps the valve element (23) in a closed position and the spring seat (28) in contact with the pressure-sensitive element (30).

12. Device according to claim 10, characterised in that the bypass valve (18) used is an 'HGBP' valve (Hot Gas Bypass) without a temperature-sensitive bulb (33).

13. Device according to any one of the previous claims 1 to 12, characterised in that the compressor (3) is equipped with a drive with a constant speed.

14. Method for cool drying a gas by means of a device that primarily consists of a closed cooling circuit (2) that contains a coolant that is circulated in the cooling circuit (2) by means of a compressor (3) and which further contains, successively in the direction of flow (M) of the coolant, a condenser (5) connected to the outlet of the compressor (3); an expansion means (7) followed by an evaporator (8) connected to the inlet of the aforementioned compressor (3), whereby the evaporator (8) constitutes the primary part of a heat exchanger (9) with a secondary part (10) through which the gas to be dried is guided and whereby there is a bypass pipe (17) in the cooling circuit (2) that can be closed by means of a bypass valve

(18) with a valve element (23) that is kept in a closed position under the influence of a spring element, characterised in that when the device is loaded, the bypass valve is opened against the spring force of the spring element when the pressure in the closed cooling circuit (2) at a point upstream of the outlet of the evaporator (8) is higher than a set value.

15. Method according to claim 14, characterised in that the bypass valve is opened against the spring force of the spring element when the pressure in the closed cooling circuit (2) at a point upstream of the evaporator (8) is higher than a set value.

16. Method according to claim 14 or 15, further characterised in that there is a restrictor (41) in the cooling circuit (2) between the expansion means (7) and the inlet of the evaporator (8) that is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is approximately equal to the pressure of the coolant at the outlet of the evaporator (8) in an unloaded state.

17. Method according to claim 14 or 15, characterised in that there is a restrictor (41) in the cooling circuit (2) between the expansion means (7) and the inlet of the evaporator (8) that is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is less than or equal to the pressure of the coolant at the outlet of the evaporator (8) in an unloaded state.

18. Method according to claim 16 or 17, characterised in that the restrictor (41) is chosen such that in the loaded state the pressure of the coolant in the cooling circuit (2) at the outlet of the evaporator (8) is chosen such that the corresponding temperature of the coolant at the outlet of the evaporator (8) is equal or approximately equal to 0°C.

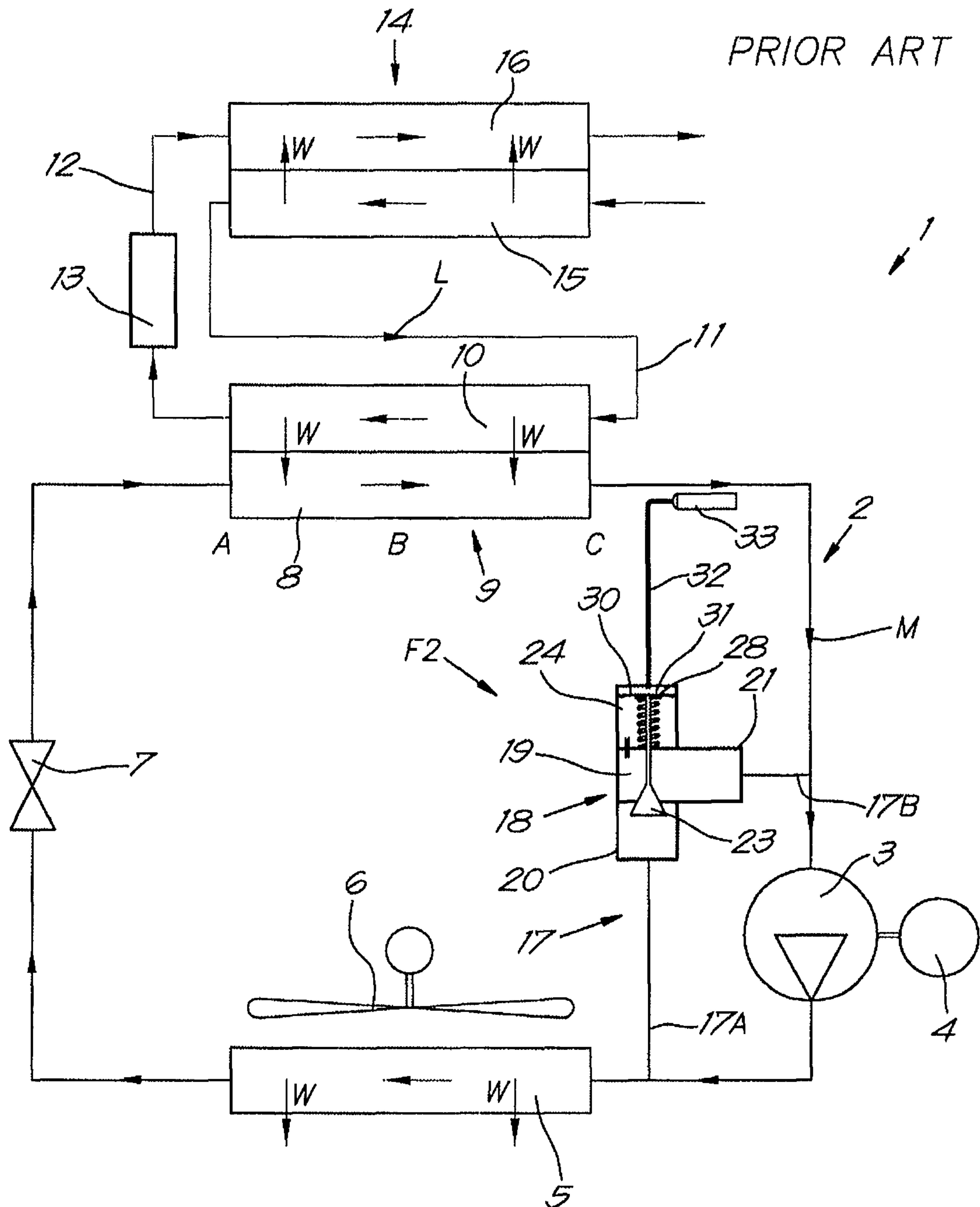


Fig. 1

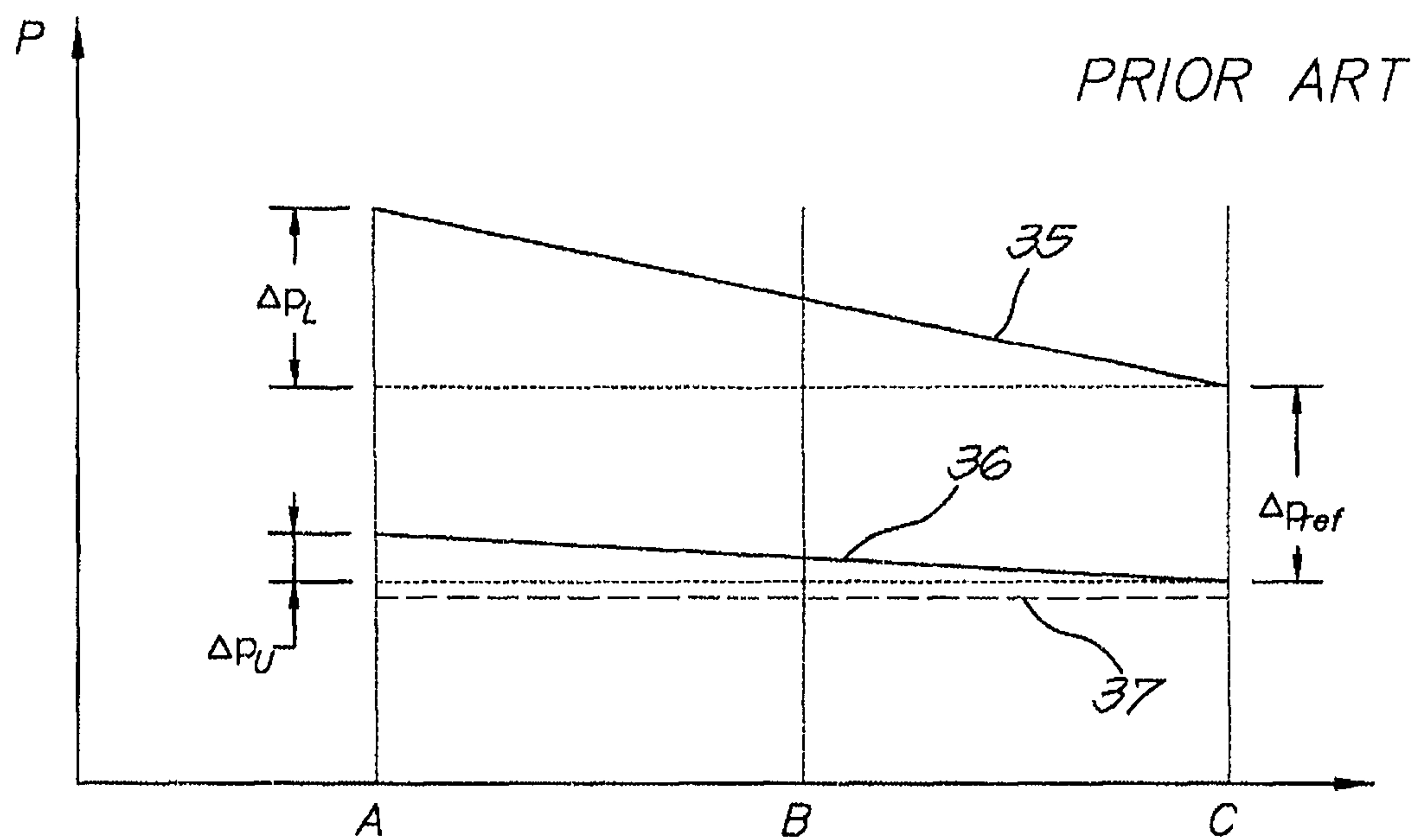
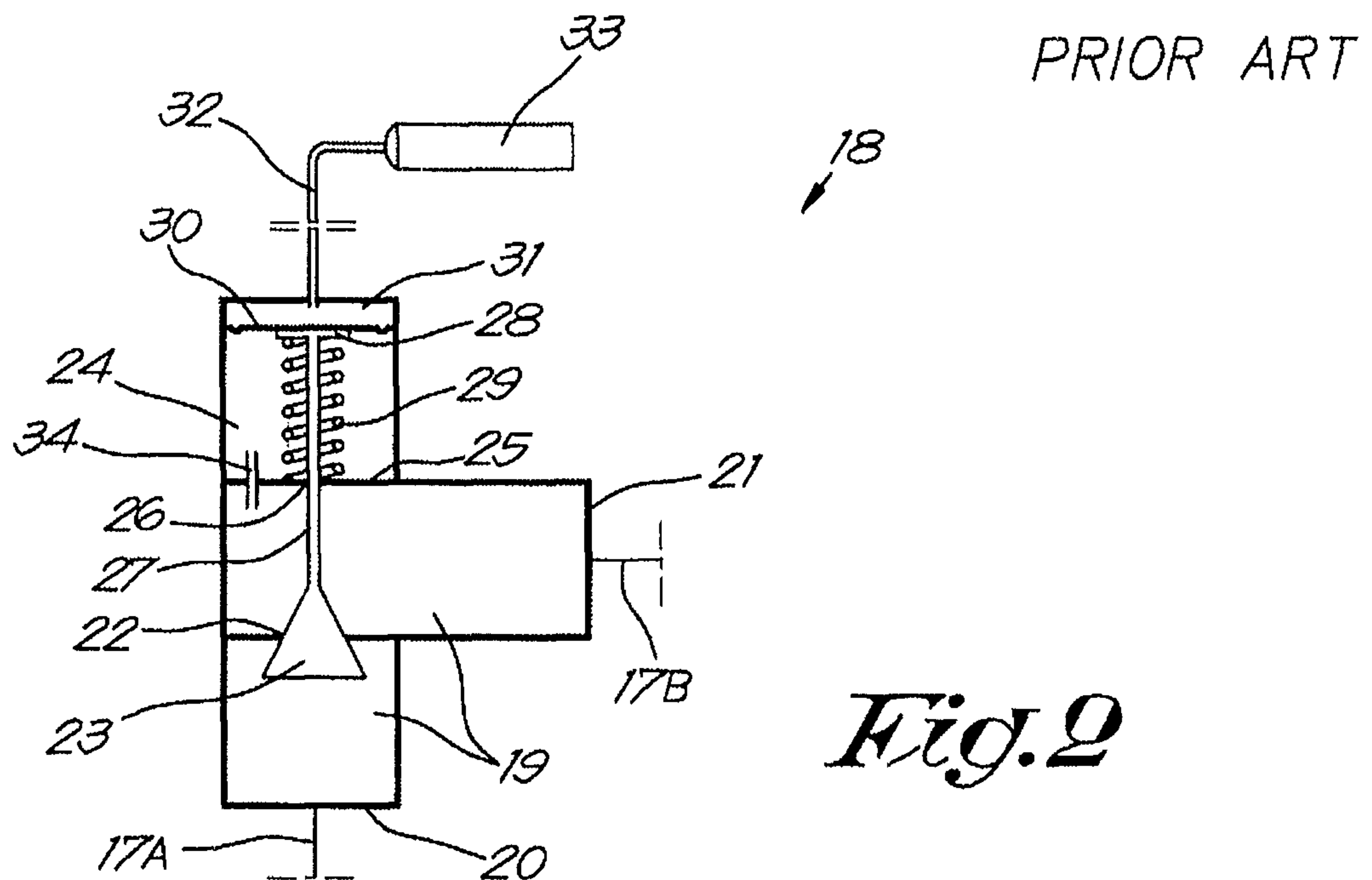


Fig.3

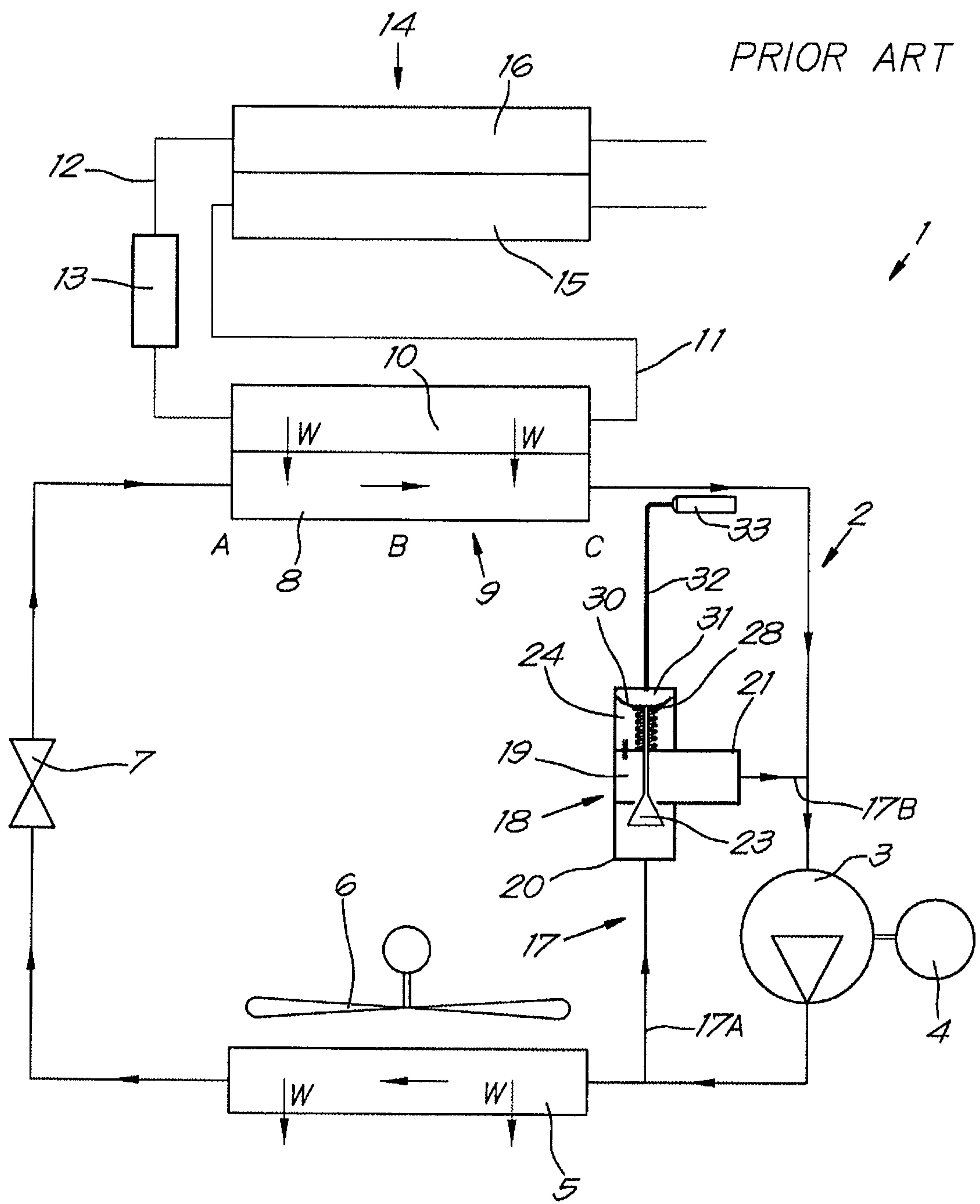


Fig. 4

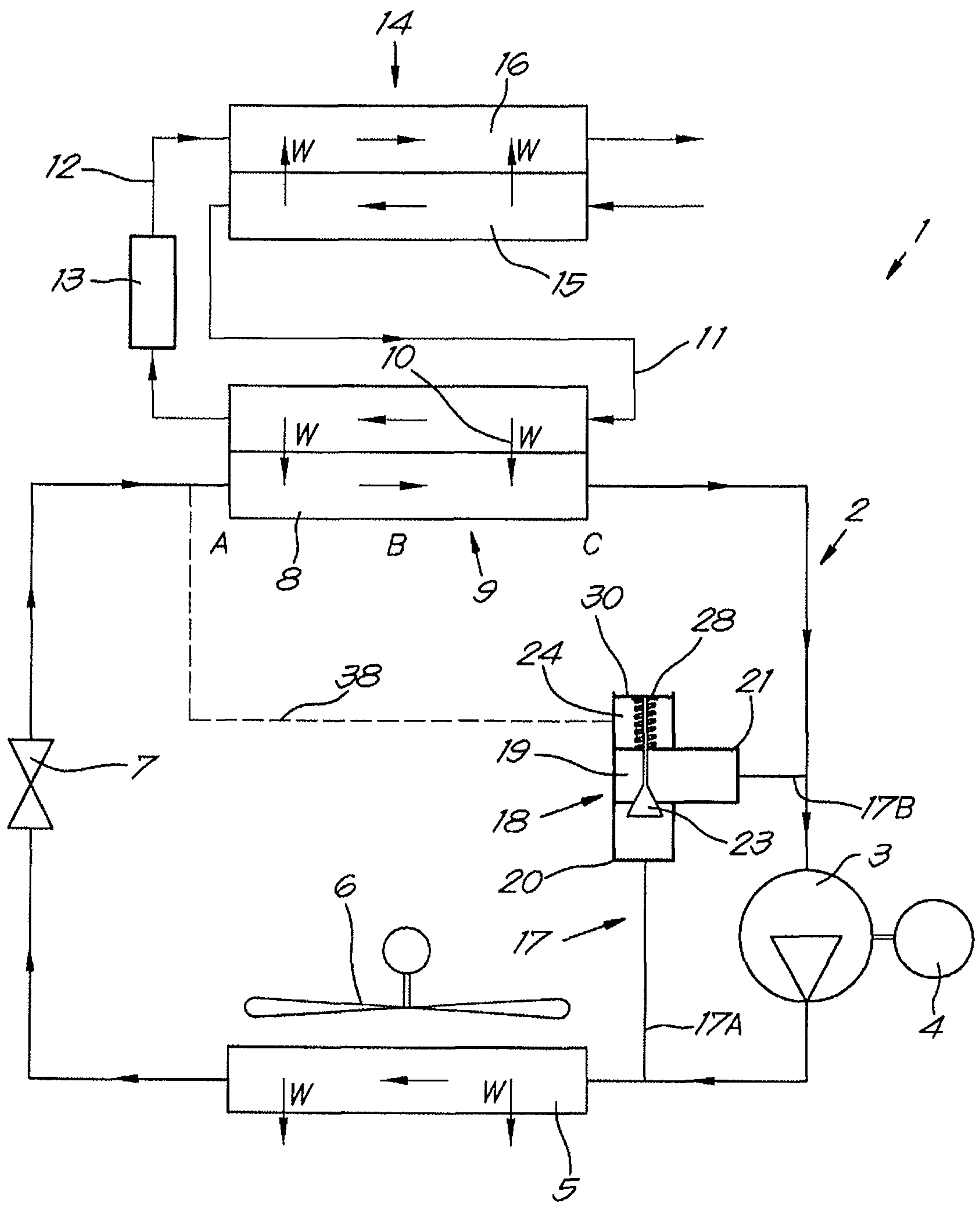


Fig.5

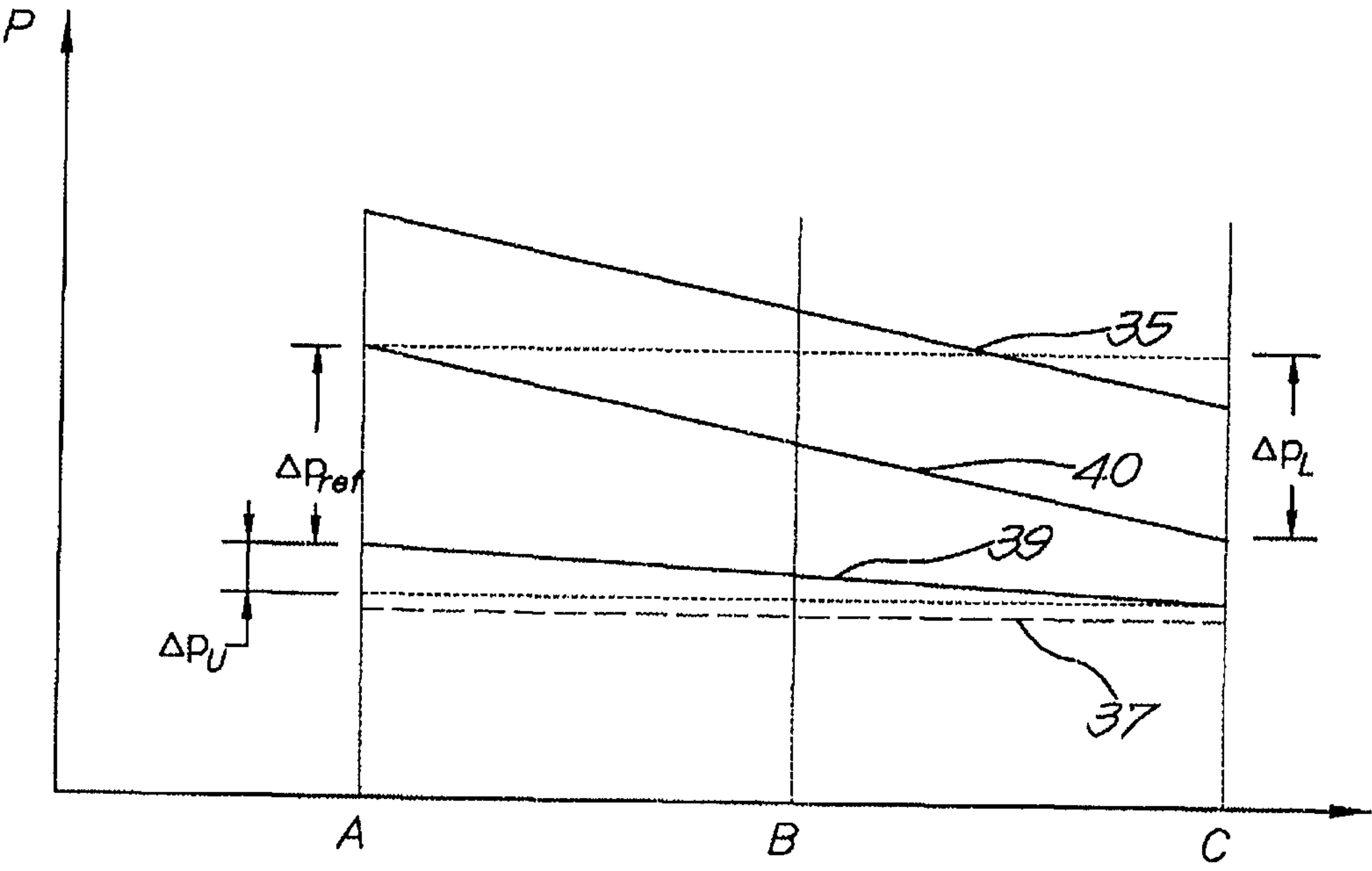


Fig. 6

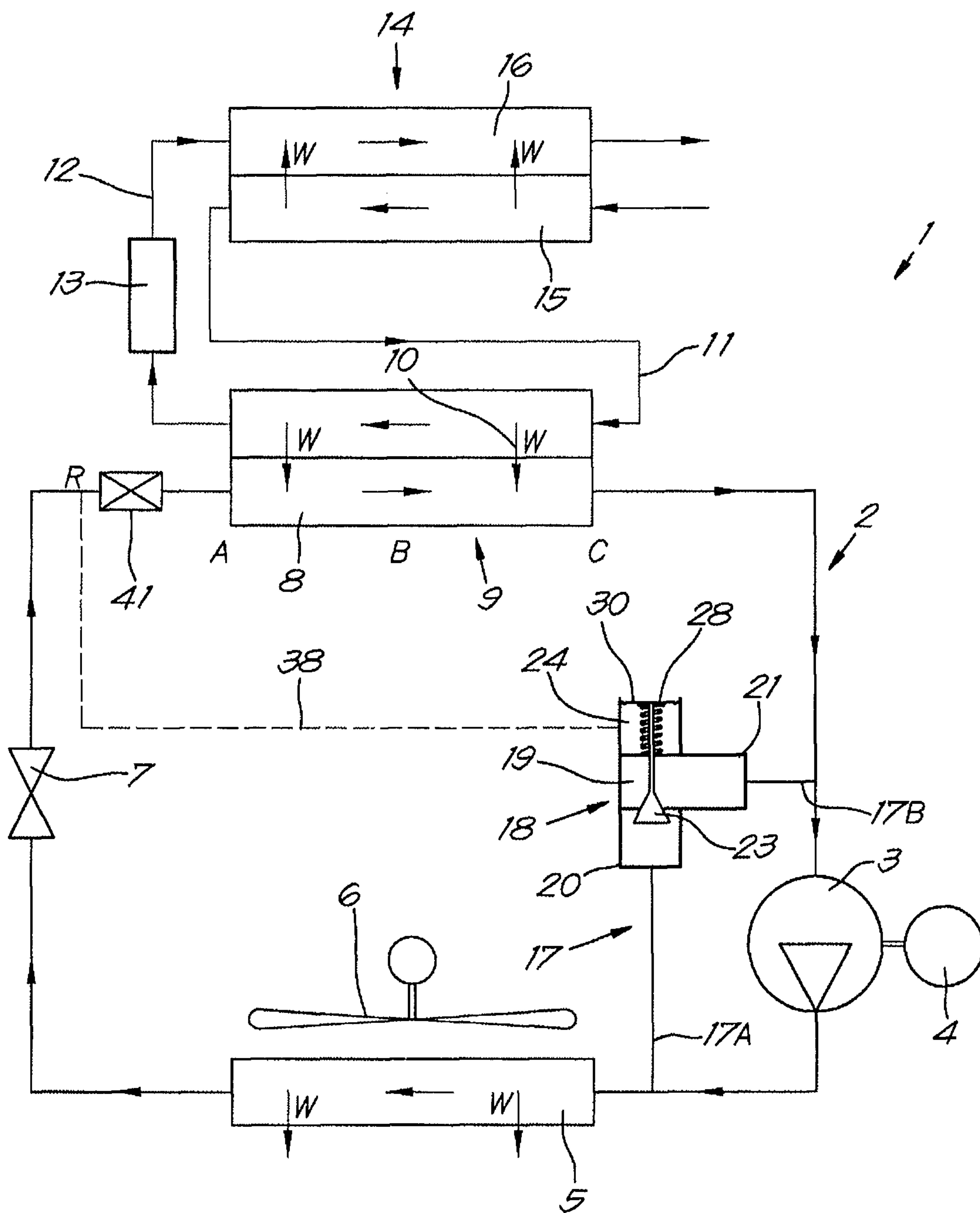


Fig. 7

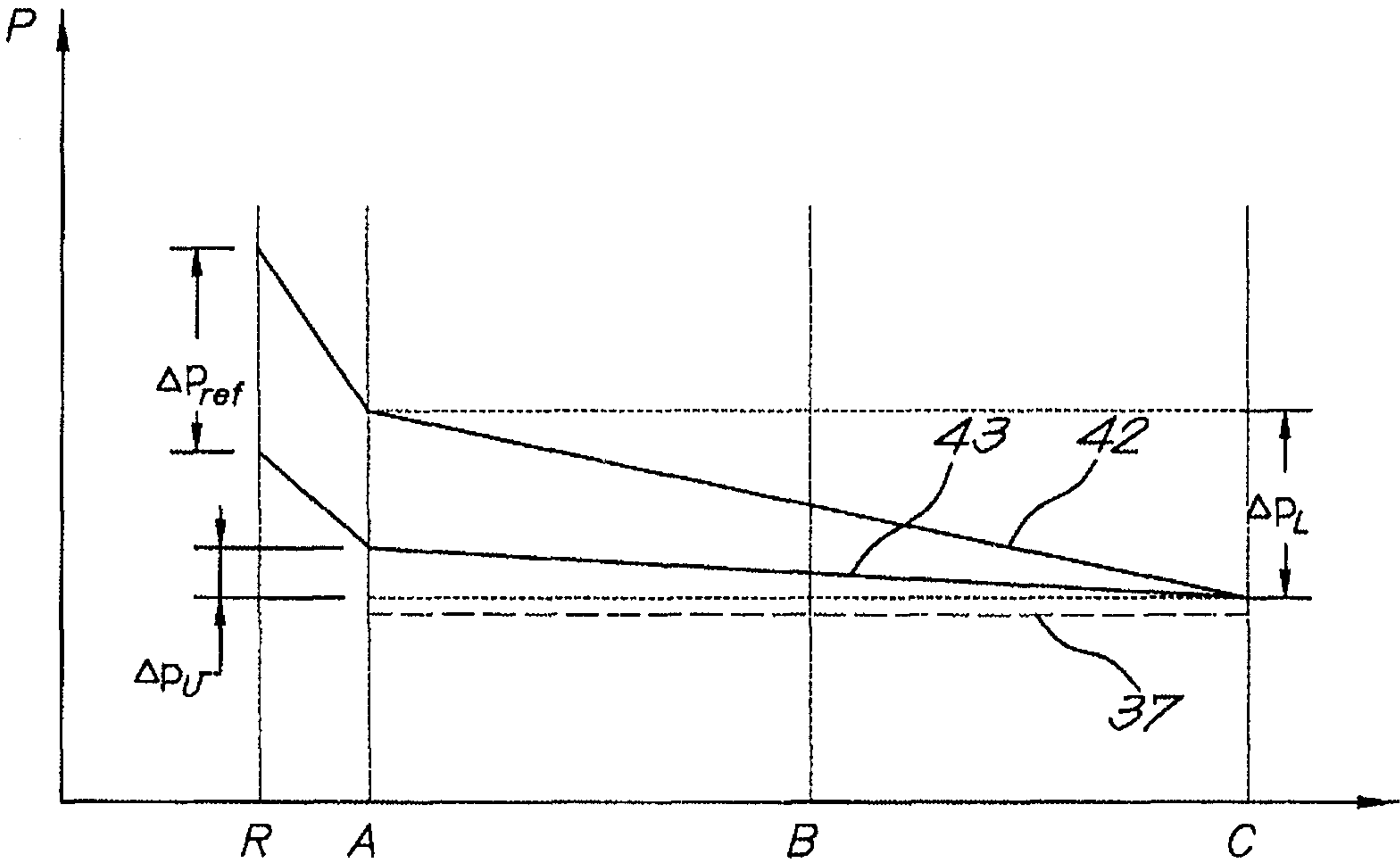


Fig. 8

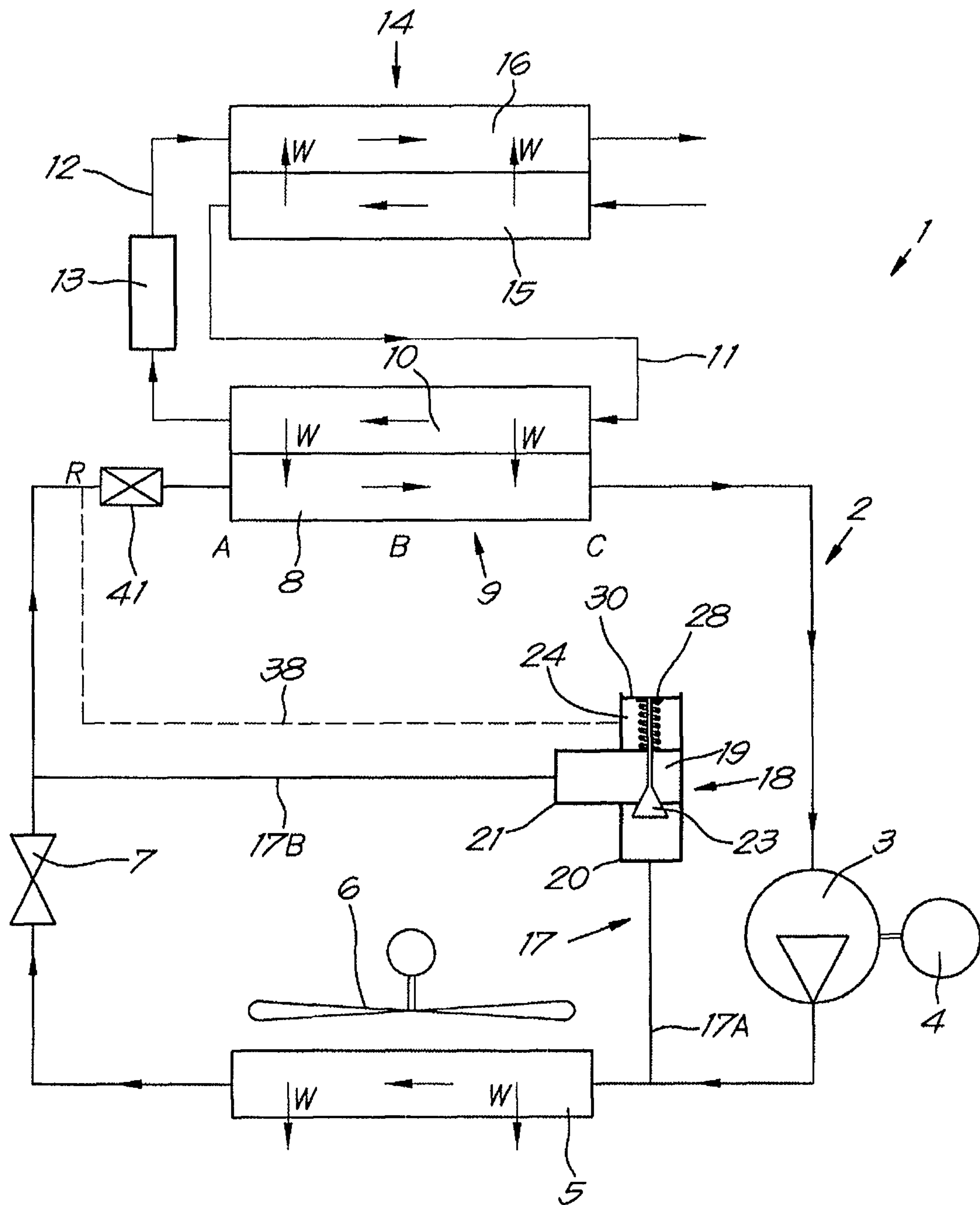


Fig. 9

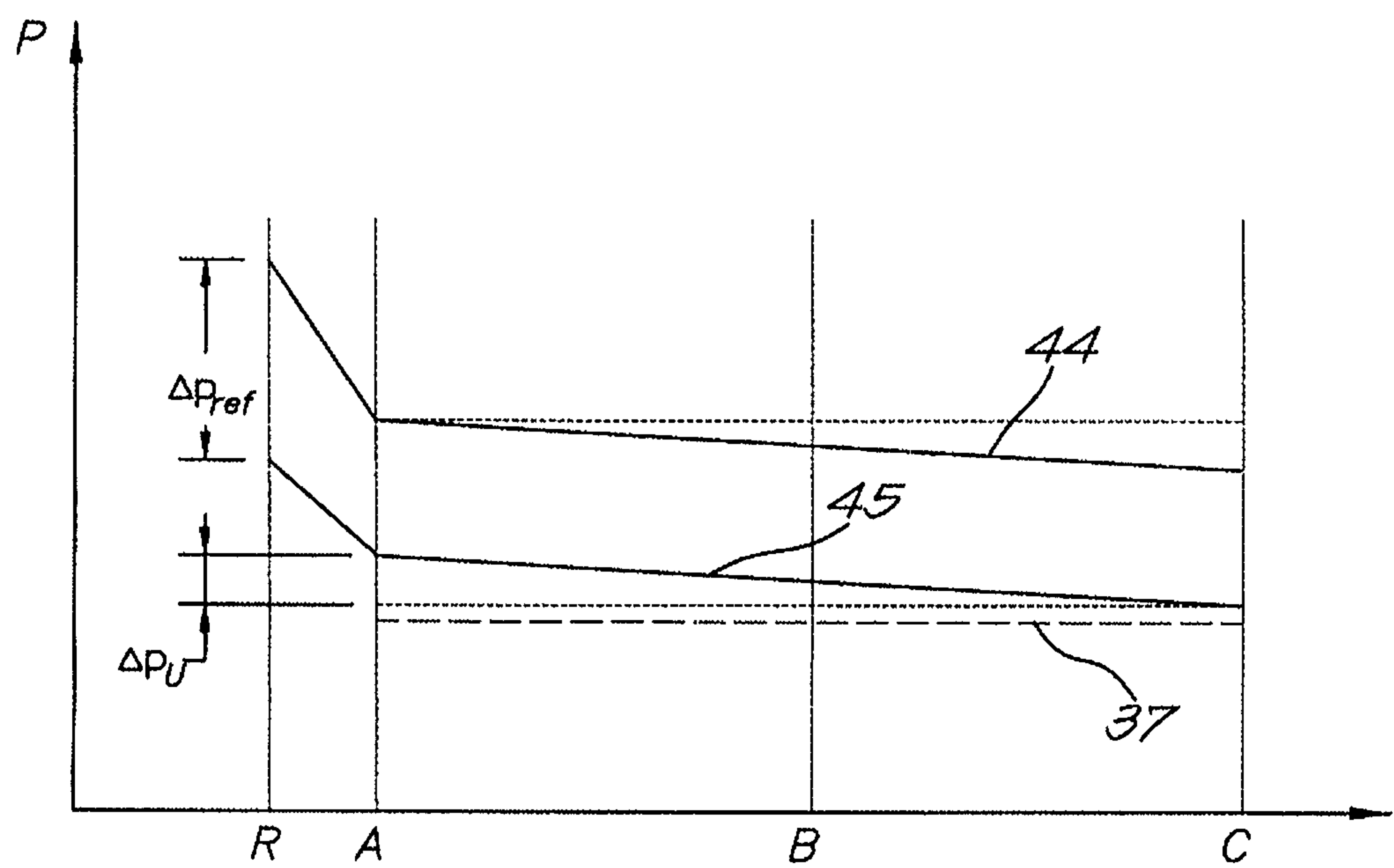


Fig.10

