The invention relates to a method of combustion of fuel using an oxygen containing gas and at least one mainly inert gas, in which:

- the said oxygen containing gas comprises at least 80% of oxygen in volume;
- the said fuel and the said oxygen containing gas are injected in such a way as to create a flame;
- the said mainly inert gas is injected in such a way that it is contiguous to and surrounds the flame created by the said fuel and the said oxygen containing gas and that it has a divergent swirl with regard to the flame.
Effect of fumes repartition on Temperature profile

- Convergent distribution
- Intermediary distribution
- Divergent distribution

Fig. 2
The present invention relates to a burner and a combustion method which can make use of a high-oxygen-content gas.

With the increasingly stringent environmental restrictions, particularly in terms of the production of CO₂ and NOₓ, the combustion of a fuel using oxygen or a high-oxygen-content gas is becoming increasingly attractive for the combustion of fossil fuels in all kinds of industry fields, where thermal fluids such as steam, hot water or hot oil, and/or electricity and/or mechanical work are needed. However, the conventional combustion devices using air as oxidizer do not always have the geometry, nor the requisite materials, for operating with oxygen or a high-oxygen-content gas. This is because the absence of the nitrogen ballast in high-oxygen or all-oxygen combustion significantly modifies the heat transfer modes, the species concentrations, and the pressure conditions in the combustion chamber.

In order to operate with all-oxygen combustion in these installations, one proposed solution is to reinject flue gas produced by the said combustion or another combustion to partly make up for the absence of nitrogen. This procedure serves to avoid a high production of NOₓ due both to the absence of nitrogen, and also to a lower flame temperature than in all-oxygen combustion. However, the reinjected flue gas often nullifies the benefits of oxycombustion, such as, in particular, the lower proportion of unburns from heavy oil residues, or the decrease of part of the ash, these unburns and this ash then causing complications in the downstream flue gas treatment method.

This flue gas injection can be made essentially in two ways. First, by mixing the said flue gas with oxygen before its introduction into the burner, so as to reconstitute an oxidizer comprising about 21 to 27% oxygen and the remainder essentially consisting of CO₂ instead of nitrogen. One advantage that can be found for this solution in the case of a conversion of an air boiler is the possibility of retaining the air burners with minor operating adjustments. On the contrary, the premixing of the flue gases with the oxygen before their introduction into the burner may give rise to safety problems. To avoid this problem, in a second alternative, the flue gas can also be injected separately, either at a location of the combustion chamber, or through the burner. In the latter case, the flue gas is injected at a velocity such as to lengthen the flame, which may overheat the elements of the combustion chamber (opposite wall or tubes, in the case of a boiler). To avoid this problem, the flue gas injection velocities must be low, which has the effect of increasing the size of the burner and of creating layout problems, whereas it is well known that the surface areas of the combustion chamber must be maximized.

The preceding problems therefore imply the need to improve the methods and the oxycombustion burners making use of flue gas recycling.

Furthermore, practice demonstrates the utility of being able to use the combustion burners in flexible mode, that is, alternately in oxycombustion and in air combustion. In fact, owing to the restrictions in oxygen availability and/or safety problems, it may be useful to be able to convert an oxycombustion into air combustion without replacing the burner. Similarly, for certain types of combustion, it is preferable to start the combustion with air and then switch to oxycombustion for safety reasons.

It is therefore the object of the present invention to propose a device suitable for implementing an oxycombustion with flue gas recycle in a device designed for an air combustion.

A further object of the present invention is to propose a combustion device suitable for implementing an oxycombustion with flue gas recycle.

A further object of the present invention is to propose a combustion device suitable for implementing an oxycombustion with air combustion.

For this purpose, the invention relates to a method of combustion of at least one fuel using at least one oxygen containing gas and at least one mainly inert gas, in which:

- the said oxygen containing gas comprises at least 80% of oxygen in volume,
- the said fuel and the said oxygen containing gas are injected in such a way as to create a flame,
- the said mainly inert gas is injected in such a way that it is contiguous to and surrounds the flame created by the said fuel and the said oxygen containing gas and that it has a divergent swirl with regard to the flame.

Other features and advantages of the invention will appear from a reading of the description that follows. Embodiments of the invention are provided as non-limiting examples, illustrated by the Fig. 1 which is a schematic view of a burner according to the invention.

The method according to the invention implements the main combustion of a fuel by an oxygen containing gas. The fuel may be any gaseous, liquid, solid, slurry, emulsion, or any combination thereof. If it is a gas, the fuel may be, but is not limited to, natural gas, mine gas, coke oven gas, blast furnace gas, refinery gas, low heating value gas, gassified solid fuel, or syngas. If it is a liquid, the fuel may be, but is not limited to, home-heating oil, heavy fuel oil, asphalt, refinery residue or crude oil. If it is a solid, the fuel may be, but is not limited to, coal, coke, petroleum coke, biomass, peat, solid asphalt, or solid refinery residue. These various types of fuels are injected in such a way as to form a flame with the oxygen containing gas. The injections of the fuel or fuels and the oxygen containing gas can be made in any manner known to a person skilled in the art in order to produce a flame. According to the method of the invention, a mainly inert gas is also injected. The mainly inert gas comprises at least one of the following compounds: CO₂, H₂O, Ar, in a molar quantity of at least 50%. The mainly inert gas may be or comprise a flue gas.

The mainly inert gas is preferably injected in the form of a single jet. This single jet surrounds the flame created by the fuel and the oxygen containing gas. In the context of the present invention, “surround” means the fact that this jet of mainly inert gas encircles the central flame of the fuel and the oxygen containing gas. According to a preferred embodiment, the jet of mainly inert gas has the shape of a ring centred on the flame of fuel and oxygen containing gas.

According to the invention, the single peripheral jet has a divergent swirl with regard to the flame of fuel and oxygen containing gas. In the context of the present invention, swirl of a jet means a swirl movement of the jet about itself. The single peripheral jet is therefore a jet swirling about itself. Since the said jet surrounds the flame of fuel and oxygen containing gas, the said single peripheral jet is also swirling...
about the said flame. According to the invention, this swirl is divergent, that is, in the single peripheral jet, the mainly inert gas moves away from the flame of fuel and oxygen containing gas as it is injected.

For the single peripheral jet, the swirl rate of each of this jet of mainly inert gas is advantageously between 0.26 and 1.73. The swirl rate $S$ is defined as follows: $S = \frac{v}{u_0}$, where $v$ is the velocity, and $u_0$ is the angular velocity of the fluid swirled in a jet.

The method is particularly suited for use in boilers.

In the context of the present invention, oxygen-containing gas preferably means a gas having an oxygen concentration above 90% in volume. According to this embodiment, the oxidizer is an oxygen-containing gas and the mainly inert gas is composed of the flue gases from a combustion. The flue gases from a combustion generally comprise mainly, if not exclusively, CO$_2$. These gases may also comprise H$_2$O. Preferably, the mainly inert gas consists at least partly of the gases issuing from the combustion of the present method and which are recycled during the combustion method. In this case, the flue gases are recycled outside the combustion chamber in which the present method is implemented. They may be treated before being recycled. In general, at least 4 Sm$^3$ of flue gases are recycled during the method according to the invention.

According to this embodiment, it is preferable for the flow rate of mainly inert gas injected into the single peripheral jet of mainly inert gas to account for 100% of the total flow rate of mainly inert gas injected. Furthermore, the gases issuing from a combustion injected in the form of the single peripheral jet does not disturb the flame issuing from the combustion of the fuel and of the oxygen-containing gas, but creates a corridor close to the nozzle of the burner which protects the walls of the combustion chamber from excessively intense radiation. Beyond the burner nose, the gases issuing from a combustion and injected in the form of the single peripheral jet and the hot gases issuing from the actual combustion of the method, are mixed to form only one uniform mixture. According to a first embodiment, gases issuing from a combustion may also be injected into at least one point of the combustion chamber that is different from the injection points of the single peripheral jet.

The invention also relates to a burner suitable for implementing the said method, which comprises:

- At least one means for injecting said fuel and at least one means for injecting said oxygen-containing gas comprising at least 80% of oxygen in volume, the said means being placed with regard to one another in such a way that the oxygen-containing gas and the fuel are capable of producing a flame,

- A means for injecting said mainly inert gas;

- Said means for injecting the said mainly inert gas being suitable for injecting it in the form of a jet contiguous to and surrounding the flame produced by the said oxygen-containing gas and the said fuel, and said means for injecting the said mainly inert gas comprising a means suitable for divergently swirling the flow of said mainly inert gas passing through it.

The burner according to the invention therefore comprises a first central part comprising at least one means for injecting fuel and at least one means for injecting the oxygen-containing gas. These two injection means must be positioned with regard to one another in such a way that the oxygen-containing gas and fuel are capable of producing a flame when the burner operates. Thus, the means for injecting fuel and oxygen-containing gas may be coaxial tubes or separate tubes. Any known technique for injecting fuel and oxygen-containing gas in order to form a flame can be used.

The burner comprises a second peripheral part consisting of a means for injecting mainly inert gas. Preferably, the means suitable for divergently swirling the flows of mainly inert gas passing through the injection means causes the said flow to swirl with a swirl rate of between 0.26 and 1.73. The said means suitable for divergent swirling is generally a deflector.

According to a particular embodiment, the burner is such that:

- The means for injecting mainly inert gas comprises two coaxial tubes centred around the means for injecting fuel and the means for injecting an oxygen-containing gas, the space between the two tubes allowing the passage of part of the mainly inert gas and comprising the means suitable for divergently swirling the flow of mainly inert gas passing through it.

According to this particular embodiment, the burner may also comprise two means for injecting oxygen-containing gas, the said means being coaxial tubes, and the means for injecting fuel may be a metal ring drilled with at least one ring of orifices, the said metal ring being coaxial with the oxygen-containing gas injection tubes and placed between the said tubes. The burner is then composed of four coaxial tubes and the metal ring drilled with orifices arranged in a ring, the said ring being placed between the smallest tube and the tube having the immediately larger diameter.

According to the invention, the burner may comprise two distinct means for injecting fuel for the injection of two different fuels.

FIG. 1 shows the end of a burner according to the invention. It comprises a first central part consisting of:

- Fuel injection means 1 which is a tube,

- Oxygen containing gas injection means 2 which comprises two tubes 21 and 22; one 21 is placed at the centre of the fuel injection tube 1 and the other 22 around the same fuel injection tube 1.

The burner also comprises a second part which is a means for injecting mainly inert gas; it comprises two coaxial tubes 22, 31, centred on the first central part, the smallest tube corresponding to the tube 22 for injecting fuel 1. The space between the intermediate tube 31 and the smallest tube 22 comprises means 5 (fans) suitable for divergently swirling the flow of mainly inert gas passing through it.

One advantage of the invention is that it may serve to modify a burner normally operating with air in such a way that it operates with an oxygen-containing gas and oxygen-containing flue gases. It suffices to supplement the air burner corresponding to the first part of the burner according to the invention with the second part of the burner according to the invention suitable for injecting the recycled flue gases. The oxygen-containing gas is then injected into the first part of the burner and the flue gases are injected into the second part.

One advantage of the burner and of the combustion method according to the invention is that they produce a flame having a controlled size, which is useful in confined vessels, such as boiler combustion chambers in which the direct contact of the excessively long flame with bare steel tubes is fatal. In this latter case, the geometry of the flame produced by the burner according to the invention allows a uniform distribution of the heat flux on all the inner surfaces of the boiler, a boiler equipped with this burner operating in oxycombustion
can withstand an energy density of up to 0.600 MW/m³ depending on the proportion of flue gas recycled.

[0037] A further advantage of the burner and of the combustion method according to the invention operating with an oxygen-containing gas is that they produce a flame having a high core temperature, whereby the unburnts are significantly decreased.

[0038] This invention may comprise one or more of the following features:

[0039] The fuel may be gaseous, liquid, solid, a slurry, an emulsion, solid in gas suspension, or any combination of the above. Three or more different fuels may be simultaneously injected. The fuel is injected through two or more orifices and the oxygen containing gasses injected through two or more orifices. The oxygen containing gasses injected through two or more orifices. The injection of the oxygen containing gasses staged between primary and secondary oxygen. A single set of orifices may be utilized to inject two or more different fuels. The flue gas temperature is maintained at a temperature greater than the acid dew point temperature.

[0040] The pressure drop that either the fuel stream, oxygen containing gas stream, or both, experiences upon passing through the burner may be no more than 200 mbar. The pressure drop that the main inert gas experiences when passing through the burner may be between 4 mbar and 10 mbar. The main inert gas injection means may be fabricated from HR 160, or another Hastelloy-type alloy, if the fuel has a high sulphur content. The main inert gas injection means may be fabricated from 316 stainless steel if the fuel is relative sulphur free. The means for injecting oxidant and fuel may be fabricated from inconel 600. A boiler may comprise at least one burner in accordance with this design.

[0041] The oxidizer is an oxygen-containing gas and the main inert gas is composed of the gases issuing from a combustion of said method and recycled, wherein the rate of recycling varies from 0.1 to 5.0, preferably 1.5. In this document, the rate of recycling is defined as the ratio (x/y) of the volume flowrate of the flue gas that is recycled (x) to the volume flowrate of the flue gas that exists the system through the stack (y).

[0042] In another embodiment, the method of combustion according to the invention is used to produce at least one thermal fluid, for example steam, hot water or hot oil and/or electricity and for mechanical work.

1-12. (canceled)

13. A method of combustion of at least one fuel using at least one oxygen containing gas and at least one main inert gas, comprising injecting the said main inert gas in such a way that the injected main inert gas is contiguous to and surrounds the flame created by combustion of the fuel and the oxygen containing gas and that the injected main inert gas has a divergent swirl with regard to the flame, wherein the oxygen containing gas comprises at least 80% of oxygen by volume.

14. The method of claim 13, wherein the fuel is gaseous, liquid, solid, a slurry, an emulsion, solid in gas suspension, or any combination thereof.

15. The method of claim 13, wherein 3 or more different fuels are simultaneously injected.

16. The method of claim 13, wherein the fuel is injected through two or more orifices and the oxygen containing gas is injected through two or more orifices.

17. The method of claim 13, wherein the oxygen containing gas is injected through two or more orifices.

18. The method of claim 13, wherein the injection of the oxygen containing gas is staged between primary oxygen and secondary oxygen.

19. The method of claim 13, wherein a single set of orifices is to inject two or more different fuels.

20. The method of claim 13, wherein:

- the mainly inert gas essentially consists of recycled flue gas resulting from combustion of the fuel and the oxygen containing gas;
- and a rate of recycling of the flue gas varies from 0.1 to 5.0, the rate of recycling being defined as a ratio (x/y) of a volume flowrate (x) of the flue gas that is recycled to the volume flowrate (y) of the flue gas that is not recycled.

21. The method of claim 13, wherein:

- the mainly inert gas essentially consists of recycled flue gas resulting from combustion of the fuel and the oxygen containing gas;
- and the flue gas temperature is maintained at a temperature greater than the acid dew point temperature.

22. The method of claim 13, wherein the rate of recycling of the flue gas varies from 0.1 to 1.5.

23. A burner comprising:

- at least one fuel tube adapted to inject fuel; and
- at least one oxygen containing gas tube adapted to inject an oxygen containing gas comprising at least 80% of oxygen in volume, the fuel and oxygen containing gas tubes being placed with regard to one another in such a way that the oxygen containing gas and the fuel are capable of producing a flame upon injection;
- a divergent swirler adapted to inject a mainly inert gas in the form of a divergently swirling jet contiguous to and surrounding a flame produced by combustion of the injected oxygen containing gas and fuel.

24. A boiler comprising at least one of the burner according to claim 23.

25. The method of claim 13, further comprising the step of utilizing the combustion of the fuel and the oxygen containing gas to produce at least one thermal fluid.

26. The method of claim 25, wherein the thermal fluid is selected from the group consisting of steam, hot water and hot oil.

27. The method of claim 13, further comprising the step of utilizing the combustion of the fuel and the oxygen containing gas to produce electricity.

28. The method of claim 13 further comprising the step of utilizing the combustion of the fuel and the oxygen containing gas to produce mechanical work.

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