



(22) Date de dépôt/Filing Date: 2005/06/23

(41) Mise à la disp. pub./Open to Public Insp.: 2006/01/06

(45) Date de délivrance/Issue Date: 2014/02/11

(30) Priorité/Priority: 2004/07/06 (US10/885,267)

(51) Cl.Int./Int.Cl. *F23J 15/02* (2006.01),
B01D 53/56 (2006.01)

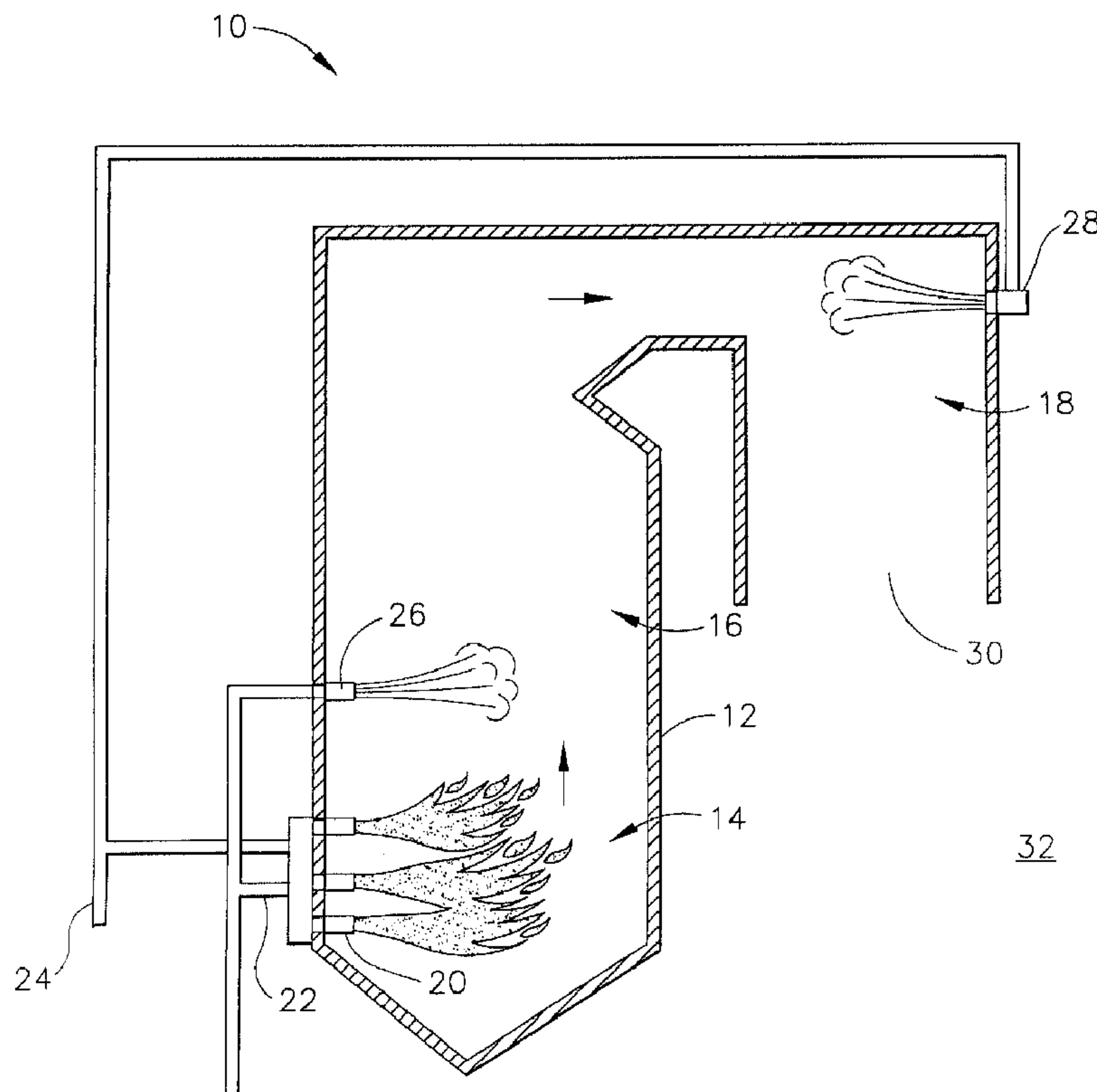
(72) Inventeurs/Inventors:
ZAMANSKY, VLADIMIR M., US;
LISSIANSKI, VITALI VICTOR, US;
EITENEER, BORIS NICKOLAEVICH, US

(73) Propriétaire/Owner:
GENERAL ELECTRIC COMPANY, US

(74) Agent: CRAIG WILSON AND COMPANY

(54) Titre : METHODES ET SYSTEMES D'EXPLOITATION DE DISPOSITIFS DE COMBUSTION

(54) Title: METHODS AND SYSTEMS FOR OPERATING COMBUSTION SYSTEMS



(57) Abrégé/Abstract:

Methods and systems for reducing nitrogen oxides in combustion flue gas is provided. The method includes combusting a fuel (22) in a main combustion zone (14) such that a flow of combustion flue gas is generated wherein the combustion flue gas includes at



(57) **Abrégé(suite)/Abstract(continued):**

least one nitrogen oxide species, establishing a fuel-rich zone, forming a plurality of reduced N-containing species in the fuel rich zone, injecting over-fire air into the combustion flue gas downstream of fuel rich zone, and controlling process parameters to provide conditions for the reduced N- containing species to react with the nitrogen oxides in the OFA zone to produce elemental nitrogen such that a concentration of nitrogen oxides is reduced.

METHODS AND SYSTEMS FOR OPERATING COMBUSTION SYSTEMS

ABSTRACT OF THE DISCLOSURE

Methods and systems for reducing nitrogen oxides in combustion flue gas is provided. The method includes combusting a fuel (22) in a main combustion zone (14) such that a flow of combustion flue gas is generated wherein the combustion flue gas includes at least one nitrogen oxide species, establishing a fuel-rich zone, forming a plurality of reduced N-containing species in the fuel rich zone, injecting over-fire air into the combustion flue gas downstream of fuel rich zone, and controlling process parameters to provide conditions for the reduced N-containing species to react with the nitrogen oxides in the OFA zone to produce elemental nitrogen such that a concentration of nitrogen oxides is reduced.

METHODS AND SYSTEMS FOR OPERATING COMBUSTION SYSTEMS

BACKGROUND OF THE INVENTION

This invention relates generally to operating combustion systems and, more particularly, to methods and systems for operating combustion systems to facilitate reducing NO_x emissions.

Typical boilers, furnaces, engines, incinerators, and other combustion sources emit exhaust gases that include nitrogen oxides. Nitrogen oxides include nitric oxide (NO), nitrogen dioxide (NO₂), and nitrous oxide (N₂O). Total NO+NO₂ concentration is usually referred to as NO_x. Nitrogen oxides produced by combustion are mainly in the form of NO. Some NO₂ and N₂O are also formed, but their concentrations are generally less than approximately 5% of the NO concentration, which generally ranges from 200 to 1000 ppm for coal-fired applications. Nitrogen oxide emissions are the subject of growing concern because they are alleged to be toxic compounds and precursors to acid rain and photochemical smog, and contributors to the greenhouse effect.

Several commercial technologies are available to reduce NO_x emissions from combustion sources. Currently, Selective Catalytic Reduction (SCR) is a commercial technology that is frequently used to facilitate NO_x control. With SCR, NO_x is reduced by reactions with Nitrogen Reducing Agents (N-agents, such as ammonia, urea, etc.) across the surface of a catalyst. Known SCR systems operate at temperatures of approximately 700 °F and routinely are able to achieve approximately 80% NO_x reduction. However, several inherent drawbacks of SCR, and most importantly, its high cost, may prevent it from being an all-encompassing solution to the problem of NO_x removal. Moreover, SCR requires the installation of a large amount of catalyst in the exhaust stream, and SCR catalyst life is limited. Specifically, catalyst deactivation, due to a number of mechanisms, generally limits catalyst life to about four years for coal-fired applications. Costs associated with system modifications, installation and operation, combined with the cost of catalyst material, render SCR quite expensive pollutant control technology. Furthermore,

because the spent catalysts are toxic, the catalysts also present disposal problems at the end of lifetime.

To facilitate reducing costs compared to the SCR technology, the reaction of N-agents with NO_x can proceed without a catalyst at a higher temperature. This process is called the Selective Non-Catalytic Reduction (SNCR). SNCR is effective over a narrow range of temperatures, or "temperature window" centered about 1800 °F wherein the N-agent forms NH_i radicals that react with NO. Under ideal laboratory conditions, deep NO_x control may be possible; however, in practical full-scale installations, the non-uniformity of the temperature profile, difficulties of mixing the N-agent across the full combustor cross section, limited residence time for reactions, and ammonia slip (unreacted N-agent) may limit SNCR's effectiveness. Generally, NO_x control via SNCR is limited to between approximately 40% and approximately 50%. However, since SNCR does not require a catalyst and therefore has a relatively lower capital cost compared to SCR, it is a valuable option for NO_x control with a lower efficiency of NO_x control compared to SCR systems.

Other known combustion systems include combustion modifications such as Low NO_x Burners (LNB), reburning, and over-fire air (OFA) injection control of NO_x emissions via combustion staging. These technologies provide relatively moderate NO_x control of between approximately about 30% and approximately 60%. However, their capital costs are low and, since no injection of N-agents is required, their operating costs are generally reduced in comparison to SCR or SNCR systems. NO_x control in reburning is achieved by fuel staging wherein a main portion of the fuel, for example, approximately 80% to approximately 90% is fired through the conventional burners with a normal amount of air, for example, approximately 10% excess. A certain amount of NO_x is formed during the combustion process, and in a second stage, the remainder of the fuel (reburn fuel) is added into the secondary combustion zone, called the reburn zone, to maintain a fuel-rich environment. The reburn fuel can be coal, gas or other fuels. In the reducing atmosphere within the fuel-rich zone, both NO_x formation and NO_x removal reactions occur. Experimental results indicate that within a specific range of conditions (equivalence ratio, temperature, and residence time in the reburn zone), NO_x concentrations may typically be reduced by

approximately 50% to approximately 60%. Part of the reburn fuel is rapidly oxidized by oxygen to form CO and hydrogen, and the remaining reburn fuel provides a fuel-rich mixture with certain concentrations of carbon-containing radicals: CH_3 , CH_2 , CH , C , HCCO , etc. These active species can either form NO precursors in reactions with molecular nitrogen or consume NO in direct reactions with it. Many elementary reaction steps are involved in NO reduction. The carbon-containing radicals (CH_i) formed in the reburn zone are capable of reducing NO concentrations by converting it into various intermediate species with C-N bonds. These species, in turn, are converted into NH_i species (NH_2 , NH , and N), which later react with NO to form molecular nitrogen. Thus, NO can be removed by reactions with two types of radicals, namely species: CH_i and NH_i . However, reactions of intermediate N-containing species with NO are typically slow in the absence of O_2 and do not contribute significantly to NO reduction in the reburn zone. In the third stage OFA is injected to complete combustion of the fuel. Typically OFA is injected at a location where the flue gas temperature is about 1800 °F to about 2800 °F to facilitate achieving complete combustion. The temperature of the flue gas at a point where overfire air is injected is henceforth referred to as T_{OFA} . The OFA added in the last stage of the process oxidizes remaining CO, H_2 , HCN, and NH_i species as well as unreacted fuel and fuel fragments, to final products, which include H_2O , N_2 , and CO_2 . At this stage, the reduced N-containing species react mainly with oxygen and are oxidized either to elemental nitrogen or to NO_x . It is the undesired oxidation of N-containing species to NO_x that limits the efficiency of the reburning process.

Generally, reburning fuel is injected at flue gas temperatures of about 2300 °F to about 3000 °F. The efficiency of NO_x reduction in reburning may increase with an increase in injection temperature because of faster oxidation of the reburning fuel at higher temperatures, resulting in higher concentrations of carbon-containing radicals involved in NO_x reduction. For reburning fuel heat inputs up to about 20%, the efficiency of NO_x reduction increases with an increase in the amount of the reburning fuel. With larger amounts of reburning fuel, the efficiency of NO_x reduction flattens out and may even slightly decrease. Increasing residence time in the reburn zone also improves reductions in nitrogen oxides emissions by allowing more time for reburning chemistry to proceed.

Lastly, an Advanced Reburning (AR) process, which is a synergistic integration of reburning and SNCR, is also currently available. Using AR, the N-agent is injected along with the OFA and the reburning system is adjusted to facilitate optimizing NO_x reduction with an N-agent. By adjusting the reburning fuel injection rate to achieve near-stoichiometric conditions, instead of fuel-rich conditions normally used for reburn, the CO level is facilitated to be controlled, and the temperature window for effective SNCR chemistry may be broadened. With AR, NO_x reduction achieved from the N-agent injection is nearly doubled, compared with that of SNCR. Furthermore, with AR, the widening of the temperature window provides flexibility in locating the injection system and the NO_x control should be achievable over a broad boiler operating range.

However, although the technologies described above are available and capable of reducing NO_x concentrations from combustion sources, they are complex systems that are also expensive to install, operate, and maintain.

BRIEF DESCRIPTION OF THE INVENTION

In one embodiment, a method for reducing nitrogen oxides in combustion flue gas is provided. The method includes combusting a fuel in a main combustion zone such that a flow of combustion flue gas is generated wherein the combustion flue gas includes at least one nitrogen oxide species, establishing a fuel-rich zone, forming a plurality of reduced N-containing species in the fuel rich zone, injecting over-fire air into the combustion flue gas downstream of fuel rich zone, and controlling process parameters to provide conditions for the reduced N-containing species to react with the nitrogen oxides in the OFA zone to produce elemental nitrogen such that a concentration of nitrogen oxides is reduced.

In another embodiment, a furnace having a reduced NO_x emission is provided. The furnace includes a main combustion zone for combusting a fuel, a fuel rich zone located downstream from the main combustion zone, at least one over-fire air port for injecting over-fire air into a combustion flue gas stream at a respective OFA zone, a controller configured to control process conditions in the main combustion zone and the fuel rich zone such that a molar concentration of reduced N-containing species is

approximately equal to a molar concentration of NO_x when the combustion flue gas reaches said over-fire air zone.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a schematic view of a exemplary power generating boiler furnace system;

Figure 2 is a schematic view of a second exemplary power generating boiler furnace system;

Figure 3 is a schematic view of another exemplary power generating boiler furnace system;

Figure 4 is a graph illustrating exemplary traces of relative concentrations of N-containing species during operation of a furnace in accordance with the embodiment shown in Figure 1;

Figure 5 is a graph illustrating exemplary traces of NO concentration as a function of temperature T_{OFA} of the flue gas at a point where overfire air is injected using the system shown in Figure 1;

Figure 6 is a graph illustrating exemplary traces illustrating an effect of T_{OFA} on CO emissions;

Figure 7 is a graph illustrating a relationship between reburning heat input and CO concentration on an inlet side of the oxidation catalyst and an outlet side of the oxidation catalyst; and

Figure 8 is a graph that illustrates a prediction of an effect of T_{OFA} on NO, total fixed nitrogen (TFN), and CO concentrations at the end of a burnout zone.

DETAILED DESCRIPTION OF THE INVENTION

As used herein, the terms "nitrogen oxides" and " NO_x " are used interchangeably to refer to the chemical species nitric oxide (NO) and nitrogen dioxide (NO_2). Other oxides of nitrogen are known, such as N_2O , N_2O_3 , N_2O_4 and N_2O_5 , but these species are not emitted in significant quantities from stationary combustion sources, except

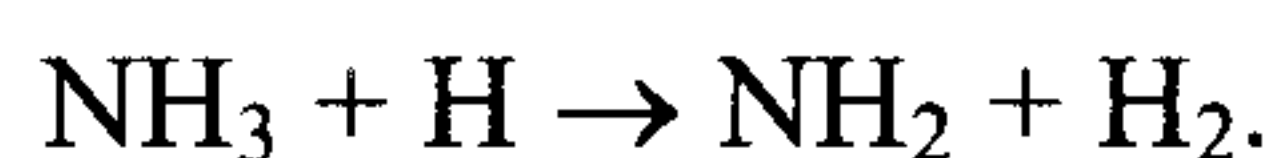
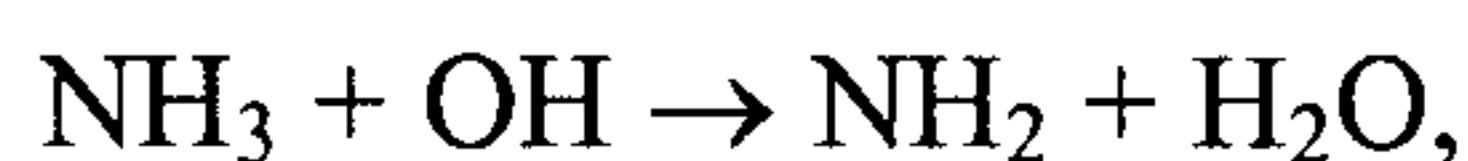
N₂O in some systems. Thus, while the term "nitrogen oxides" can be used more generally to encompass all binary N--O compounds, it is used herein to refer particularly to the NO and NO₂ (i.e., NO_x) species.

Figure 1 is a schematic view of an exemplary power generating boiler system 10 that includes, a furnace 12 including a main combustion zone 14, a reburn zone 16, and a burnout zone 18. Main combustion zone 14 may include a one or more fuel injectors and/or burners 20 that are supplied from a fuel source (not shown) with a predetermined and selectable amount of a fuel 22. In the exemplary embodiment, the fuel source may be, for example, a coal mill and exhauster. In alternative embodiments, the fuel source may be any fossil fuel including oil and natural gas, or any renewable fuel including biomass and waste. Burners 20 may also be supplied with a predetermined and selectable quantity of air 24. Burners 20 may be tangentially arranged in each corner of furnace 12, wall-fired, or have another arrangement.

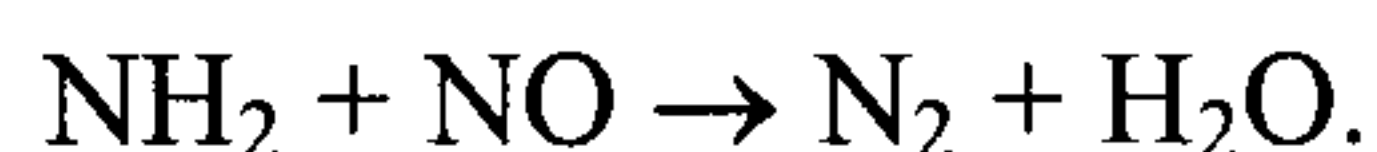
Reburn zone 16 may be supplied with a predetermined and selectable amount of a fuel 26. Although fuel 22 and fuel 26 are illustrated in Figure 1 as originating at a common source, it should be understood that fuel 22 and/or fuel 26 may be different types of fuel supplied from separate sources. For example, fuel to burners 20 may be pulverized coal that is supplied from a mill and exhauster, and fuel 26 may be natural gas. Over-fire air (OFA) may be supplied through OFA port 28, from air source 24, or from a separate source (not shown).

During operation, combustion by-products, including various oxides of nitrogen (NO_x) may be formed in main combustion zone 14 and carried through furnace 12 to a furnace exhaust flue 30, and ultimately to ambient 32. Removal of the NO_x emissions may be performed using a two-step process, henceforth referred to as in situ advanced reburning (AR) process. During a first step of the process, reburning fuel 26 may be injected into reburn zone 16 to provide a fuel-rich environment in which NO_x is partially reduced to N₂. Other reduced N-containing species including NH₃ and HCN are formed in reburn zone 16 as a result of this process. An amount of reduced N-containing species formed depends on process conditions in combustion zone 14 and reburn zone 16, and on a chemical composition of main fuel 22 and

reburning fuel 26. To facilitate optimizing NO_x reduction using the in-situ-AR process, conditions in main combustion zone 14 and in reburn zone 16 may be selected such that a molar concentration of reduced N-containing species is approximately equal to a NO_x concentration at the point of OFA injection. Reactions between reduced N-containing species such as NH₃, HCN, and NO typically proceed relatively slowly in the fuel-rich environment of reburn zone 16. During a second step, OFA may be injected downstream of reburn zone 16. If OFA is injected into NO-containing combustion flue gas within a specific temperature range, a chemical reaction between NO and reduced N-containing species occurs, and NO is converted to molecular nitrogen. The reaction starts with formation of NH₂ radicals in reactions of combustion radicals (OH, O and H) with NH₃:



The main elementary reaction of NO-to-N₂ conversion is:



Simultaneously, HCN is oxidized to NH₃ and N-containing radicals that in turn react with combustion radicals as indicated above. In a conventional SNCR process, reaction between NH-forming reducing agents (N-agents) and NO occurs in a narrow temperature range (temperature window), typically about 1750 °F to about 1950 °F. In the in-situ-AR process, oxidation of reburning fuel 26 in reburn zone 16 may not proceed to completion due to the lack of available oxygen. Accordingly, combustion flue gas exiting reburn zone 16 may contain relatively significant concentrations of unburned hydrocarbons, for example, H₂ and CO. The presence of these species in the combustion flue gas shifts the conventional SNCR temperature window of NO_x reduction toward lower temperatures. In the in-situ-AR process, the OFA is injected in combustion flue gas at temperatures relatively significantly lower than 1750 °F resulting in relatively significant additional NO_x reduction. Downstream of the OFA injection zone the reduced N-containing species react mainly with NO_x, producing

elemental nitrogen. As such deeper NO_x control is achieved as compared to traditional reburning, where the reduced N-containing species react mainly with oxygen downstream of the OFA injection zone.

Figure 2 is a schematic view of a second exemplary power generating boiler furnace system 200. In the exemplary embodiment, a concentration of NO may be reduced in a three-step process. In a first step, reburning fuel 26 may be injected to provide fuel-rich environment in which NO is partially reduced to N_2 . In a second step, OFA may be injected downstream of reburn zone 16 in a predetermined temperature range that results in a NO reduction by N-containing species formed in reburn zone 16. In a third step, combustion flue gas containing CO, remaining NO, and un-reacted N-containing species may be directed through an oxidation catalyst 202. CO is oxidized by catalyst 202 while N-containing species are partially oxidized and partially reduced to N_2 .

Figure 3 is a schematic view of another exemplary power generating boiler furnace system 300. The exemplary embodiment represents air staging wherein reburning fuel is not injected, and a fuel rich zone (302) is formed by fuel-rich combustion in main combustion zone 14. One or more additional OFA ports 28 may be used to stage the introduction of OFA to match conditions in furnace 12 at any time. Each of the additional OFA ports 28 may be independently controlled such that a OFA air flow may be modulated over a wide flow rate range as well as being substantially shut-off. As in other embodiments of the in-situ-AR process, the conditions may be selected to approximately meet $[\text{NH}_3] + [\text{HCN}] = [\text{NO}_x]$ at the point of OFA injection to facilitate optimizing NO_x removal. In the exemplary embodiment, oxidation catalyst 202 is used. In an alternative embodiment, oxidation catalyst 202 is not used.

Figure 4 is a graph 400 illustrating exemplary traces of relative concentrations of N-containing species during operation of a furnace in accordance with the embodiment shown in Figure 1. Graph 400 includes an x-axis 402 graduated in units of reburning fuel input as a percentage of the total heat input into the furnace. A y-axis 404 is graduated in percentage units of $X_N/[\text{NO}]_i$ wherein X_N represents a total concentration of N-containing species before reburning fuel injection and $[\text{NO}]_i$ represents an initial NO concentration measured without reburning fuel injection. A trace 406 represents

a concentration of NO. A trace 408 represents a concentration of NH_3 . A trace 410 represents a concentration of HCN, and a trace 412 represents a concentration of total fixed nitrogen (TFN). During operation, concentrations of NO, NH_3 , HCN and TFN were measured in furnace 12 while being fired on natural gas. TFN, as used herein is defined as a sum of NO, NH_3 , and HCN. In the exemplary embodiment, reburning fuel, for example, natural gas, and OFA were injected at locations where flue gas temperatures were 2500 °F and 2200 °F, respectively. The concentrations of NO, NH_3 , and HCN were measured at the end of reburn zone 16 (before OFA injection). Traces 406, 408, 410, and 412 illustrate NO, NH_3 , HCN and TFN as fractions of total concentration of N-containing species before reburning fuel injection. NH_3 and HCN are formed in reburn zone 16 as a result of reactions between CH_i radicals and NO.

Trace 406 illustrates that NO concentration at the end of reburn zone 16 depends on a relative heat input of the reburning fuel and decreases as relative heat input of the reburning fuel increases. For the range of relative heat inputs illustrated, the concentrations of NH_3 , trace 408, and HCN, trace 410 at the end of reburn zone 16 are considered. The TFN concentration, trace 412, at the end of reburn zone 16 is minimized at approximately 18% reburning fuel input. For the exemplary fuels and process conditions and 18% reburning fuel heat input, NO concentration, trace 406 at the end of reburn zone 16 is approximately equal to a sum of NH_3 and HCN concentrations.

Figure 5 is a graph 500 illustrating exemplary traces of NO concentration as a function of temperature T_{OFA} of the flue gas at a point where overfire air is injected using system 10 (shown in Figure 1). Graph 500 includes an x-axis 502 graduated in divisions of °F and a y-axis 504 graduated in divisions of percent NO reduction. A trace 506 illustrates the NO concentration with an amount of reburning fuel of about 10% heat input. A trace 508 illustrates the NO concentration with an amount of reburning fuel of about 15% heat input. A trace 510 illustrates the NO concentration with an amount of reburning fuel of about 20% heat input. In the exemplary embodiment, NO_i was 310 ppm at 0% O_2 . Natural gas was used as main combustion fuel and reburning fuel. As illustrated, NO reduction increased as T_{OFA} decreased at each of the exemplary heat inputs. The increase in NO reduction is approximately

linear as T_{OFA} decreases from 2200 °F to about 1600 °F. This improvement in NO reduction may be due to an increased residence time in reburn zone 16. Further temperature decrease to lower than 1600 °F resulted in a relatively greater increase in NO reduction efficiency. NO reduction for a 15% reburning at T_{OFA} of approximately 1050 °F to approximately 1150 °F reached approximately 90% and NO reduction for a 20% reburning at T_{OFA} of approximately 1050 °F to approximately 1150 °F reached approximately 95%.

Figure 6 is a graph 600 illustrating exemplary traces demonstrating an effect of T_{OFA} on CO emissions. Graph 600 includes an x-axis 602 divided in graduations of °F and a y-axis 604 divided into units of parts per million (PPM) CO concentration at zero percent O_2 . Trace 606 illustrates CO concentration at 10% reburning heat input. Trace 608 illustrates CO concentration at 15% reburning heat input. Trace 610 illustrates CO concentration at 20% reburning heat input. The CO emissions illustrated by traces 606, 608, and 610 are less than 15 ppm at T_{OFA} above 1350 °F and sharply increase at lower temperatures. The sharp increase in CO concentration at relatively low temperature may be a consequence of low temperature chemistry of CO oxidation that occurs relatively slowly such that CO oxidation is not completed within an amount of time available in the OFA zone. Accordingly, operation demonstrates that OFA injection in the temperature range of approximately 1050 °F to approximately 1150 °F results in an NO reduction of up to 95%. However, CO oxidation in this temperature range may be incomplete.

Figure 7 is a graph 700 illustrating a relationship between reburning heat input and CO concentration on an inlet side of oxidation catalyst 202 and an outlet side of oxidation catalyst 202. Graph 700 includes a x-axis 702 that is divided into a 15% reburning portion and a 20 reburning portion 706, and an y-axis 708 that is divided into graduations of CO concentration in ppm at 0% O_2 . A temperature of the combustion flue gas at the catalyst location was approximately 500 °F. During operation with approximately 15% reburning, a bar 710 illustrates a CO concentration of approximately 14,000 ppm upstream of catalyst 202 and a bar 712 illustrates a CO concentration of approximately 4,500 ppm after the combustion flue gas has passed through catalyst 202. During operation with 20% reburning, a bar 714 illustrates a

CO concentration of approximately 25,000 ppm upstream of catalyst 202 and a bar 716 illustrates a CO concentration of approximately 8,500 ppm after the combustion flue gas has passed through catalyst 202. As illustrated CO emissions significantly decrease as a result of CO oxidation across catalyst 202. A more efficient CO oxidation can be achieved with lower space velocity through the catalyst.

The results above illustrate that significant concentrations of NH_3 and HCN may be present in reburn zone 16. These species may react with NO and may facilitate substantially reducing NO emissions. A greater reduction in NO concentration may be realized when OFA is injected at combustion flue gas temperatures of approximately 1050 °F to approximately 1750 °F. Because CO oxidation at lower temperatures of this range may not be complete, installation of downstream oxidation catalyst 202 may facilitate complete oxidation of CO.

Figure 8 is a graph 800 that illustrates a prediction of an effect of T_{OFA} on NO, TFN, and CO concentrations at the end of burnout zone 18. Graph 800 includes a x-axis 802 divided in graduations of an injection temperature of OFA and an y-axis 804 that is divided in graduations of reagent concentration in units of ppm. A process model may be used to predict NO_x control efficiency. The process model was developed to include a detailed kinetic mechanism of natural gas reburning combined with gas dynamic parameters characterizing mixing of reagents. Process modeling facilitates understanding the effects of system components and conditions on NO_x control performance. In modeling, a set of homogeneous reactions representing the interaction of reactive species was assembled. Each reaction was assigned a certain rate constant and heat release or heat loss parameters. A plurality of numerical solutions of differential equations for time-dependent concentrations of the reagents facilitates predicting the concentration-time curves for all reacting species under selected process conditions. During modeled operation, the process conditions that facilitate significant improvements in NO_x removal may be determined.

The chemical kinetic code ODF, for “One Dimensional Flame” (Kau, C. J., Heap, M. P., Seeker, W. R., and Tyson, T. J., Fundamental Combustion Research Applied to Pollution Formation. U.S. Environmental Protection Agency Report No. EPA-6000/7-87-027, Volume IV: Engineering Analysis, 1987), was employed to model

experimental data. ODF is designed to progress through a series of well-stirred or plug-flow reactors, solving a detailed chemical mechanism. The kinetic mechanism (Glarborg, P., Alzueta, M.U., Dam-Johansen, K., and Miller, J.A., Combust. Flame 115:1-27 (1998)) consisted of 447 reactions of 65 C-H-O-N chemical species.

The model was used to predict NO_x reduction in natural gas reburning as a function of flue gas temperature at which OFA was injected (T_{OFA}). Initial NO_x (NO_i) and the amount of reburning fuel were assumed to be 300 ppm and 18%, respectively. This amount of the reburning fuel was chosen for modeling because, as illustrated in Figure 4, at 18% reburning heat input, NO concentration in the combustion flue gas at the end of reburn zone 16 is approximately equal to the sum of NH_3 , and HCN. This resulted in a nitrogen stoichiometric ratio (NSR) of 1.0. As used herein, NSR is defined as a molar ratio of $\text{NH}_3 + \text{HCN}$ to NO. Modeling was conducted for the final excess O_2 after OFA injection of 3%, which may be typical for industrial boilers. The temperature of the combustion flue gas decreased at a substantially linear rate of approximately 550 °F per second, which may also be typical for industrial boilers.

Process model output graph 800 includes a trace 806 that illustrates a prediction of NO concentration in the combustion flue gas decreasing as T_{OFA} decreases. This NO reduction may be due to reactions of NO with NH_3 and HCN. These reactions are similar to reactions that take place in a SNCR process. Optimum temperatures for the SNCR process are in the range of approximately 1750 °F to approximately 1950 °F without significant amounts of combustibles present in flue gas and decrease as CO concentration in flue gas increases. At temperatures higher than optimum some NH_3 and HCN may be oxidized and form NO. At temperatures lower than optimum not all NH_3 and HCN are consumed in reactions with NO and O_2 resulting in “ammonia slip”.

A trace 808 illustrates a model prediction of CO concentration in flue gas at the end of reburn zone 16 at 18% reburning fuel heat input is about 2%. Optimum temperatures for the SNCR process at this CO concentration are in the range of approximately 1300 °F to 1400 °F. A trace 810 of the model prediction illustrates that TFN reaches a minimum at a T_{OFA} of about 1350 °F. Although NO continued to be reduced further

at temperatures below approximately 1350 °F, not all NH_3 and HCN were consumed in this process resulting in an increase in TFN.

Trace 808 illustrates a model prediction that CO was substantially completely oxidized to CO_2 at a T_{OFA} in a range of approximately 1350 °F to approximately 1900 °F. The CO concentration in the combustion flue gas increased as T_{OFA} decreased below approximately 1350 °F. This may be due to low temperature CO oxidation becoming too slow and may not be substantially completed within time available in burnout zone 18.

Trace 810 illustrates a model prediction of OFA injection of approximately 1350 °F resulted in TFN reduction from 300 ppm to about 60 ppm. CO is substantially completely oxidized at T_{OFA} of approximately 1350 °F and greater. When compared to empirical results the model results illustrated in graph 800 exhibited a close correlation.

It is contemplated that the benefits of the various embodiments of the invention accrue to all combustion systems, such as, for example, but not limited to, a stoker furnace, a fluidized bed furnace, and a cyclone furnace.

The above-described nitrogen oxide reducing methods and systems provide a cost-effective and reliable means for reducing nitrogen oxide concentration in combustion flue gas emissions without injecting N-reducing agents into the combustion flue gas stream. More specifically, empirical results show that significant concentrations of NH_3 and HCN can be present in the reburn zone. These species may react with NO and significantly reduce NO emissions if OFA is injected at combustion flue gas temperatures of about 1050 °F to about 1750 °F. Because CO oxidation at lower temperatures of this range is not complete, installation of a downstream oxidation catalyst may permit complete CO oxidation. Accordingly, controlling process conditions that promote the formation of N-containing agents and injecting OFA at temperatures in a range that facilitates the combination of NH_3 and NO to form N_2 provides a cost-effective methods and systems for reducing nitrogen oxide emissions.

While there have been described herein what are considered to be preferred and exemplary embodiments of the present invention, other modifications of these embodiments falling within the invention described herein shall be apparent to those skilled in the art.

WHAT IS CLAIMED IS:

1. A method for reducing nitrogen oxides in combustion flue gas comprising:

firing a furnace to generate a main combustion zone, a fuel rich zone, and combustion flue gas containing nitrogen oxides and reduced N-containing species;

injecting over-fire air into the combustion flue gas from at least one location wherein a ratio of a molar concentration of reduced N-containing species in the combustion flue gas to the molar concentration of nitrogen oxides in the combustion flue gas is in the range of approximately 0.5 to approximately 2.0 at the over-fire air injection location; and

injecting a reburning fuel in a reburn zone.

2. A method in accordance with claim 1 wherein injecting over-fire air into the combustion flue gas from at least one location comprises injecting over-fire air into the combustion flue gas from at least one location such that the ratio of the molar concentration of reduced N-containing species in the combustion flue gas to the molar concentration of nitrogen oxides in the combustion flue gas is in the range of approximately 0.8 to approximately 1.2 at the over-fire air injection location.

3. A method in accordance with claim 1 further comprising measuring the concentration of at least one of NH_3 , HCN , and NO_x in the combustion flue gas.

4. A method in accordance with claim 3 wherein measuring the concentration of at least one of NH_3 , HCN , and NO_x in the combustion flue gas comprises using the measured concentration of the at least one of NH_3 , HCN , and NO_x to facilitate optimizing the reduction of nitrogen oxides.

5. A method in accordance with claim 1 wherein firing a furnace to generate a main combustion zone and a fuel rich zone comprises combusting a main combustion fuel in a main combustion zone.

6. A method in accordance with claim 1 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air at an exhaust gas temperature of about 1050 degrees Fahrenheit to about 1750 degrees Fahrenheit.

7. A method in accordance with claim 6 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air at an exhaust gas temperature of about 1150 degrees Fahrenheit to about 1500 degrees Fahrenheit.

8. A method for reducing nitrogen oxides in combustion flue gas, said method comprising:

combusting a fuel in a main combustion zone such that a flow of combustion flue gas is generated, said gas comprising at least one nitrogen oxide;

adding a reburning fuel to the flow of combustion flue gas downstream from the main combustion zone to establish a fuel-rich zone;

forming a plurality of reduced N-containing species in the fuel rich zone;

injecting a flow of over-fire air into the flow of combustion flue gas to form an over fire air zone downstream of the fuel rich zone;

controlling process parameters to provide conditions for the reduced N-containing species to react with the nitrogen oxides in the over-fire air zone to produce elemental nitrogen such that a concentration of nitrogen oxides is reduced and such that a molar concentration of reduced N-containing species is facilitated to be maintained approximately equal to the molar concentration of nitrogen oxides when the combustion flue gas reaches the over fire air zone; and,

wherein controlling process parameters comprises controlling process conditions in the main combustion zone and the fuel-rich zone to maintain the ratio of molar concentration of reduced N-containing species to the molar concentration of nitrogen oxides in the range of approximately 0.5 to approximately 2.0 when the combustion flue gas reaches location of over-fire air injection.

9. A method in accordance with claim 8 wherein establishing a fuel-rich zone comprises establishing the fuel-rich zone within the main combustion zone.

10. A method in accordance with claim 8 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air into the combustion flue gas at an exhaust gas temperature in a range of between about 900 degrees Fahrenheit to about 2800 degrees Fahrenheit.

11. A method in accordance with claim 8 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air into the combustion flue gas at an exhaust gas temperature in a range of between about 1050 degrees Fahrenheit to about 1750 degrees Fahrenheit.

12. A method in accordance with claim 8 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air into the combustion flue gas at an exhaust gas temperature in a range of between about 1150 degrees Fahrenheit to about 1500 degrees Fahrenheit.

13. A method in accordance with claim 8 wherein controlling process parameters comprises controlling process conditions in the main combustion zone and the fuel-rich zone to maintain the ratio of molar concentration of reduced N-containing species to the molar concentration of nitrogen oxides in the range of approximately 0.8 to approximately 1.2 when the combustion flue gas reaches location of over-fire air injection.

14. A method in accordance with claim 8 wherein injecting over-fire air into the combustion flue gas comprises injecting over-fire air into the combustion flue gas at a plurality of locations.

15. A method in accordance with claim 14 wherein injecting over-fire air into the combustion flue gas comprises controlling the injection of over-fire air into the combustion flue gas to maintain the molar concentration of reduced N-containing species approximately equal to the molar concentration of nitrogen oxides when the combustion flue gas reaches each of the plurality of over-fire air locations.

16. A method in accordance with claim 8 wherein forming a plurality of reduced N-containing species comprises forming a plurality of reduced N-containing species including at least one of NH_3 and HCN.

17. A method in accordance with claim 8 wherein combusting a main combustion fuel in a main combustion zone comprises combusting at least one of coal, natural gas, oil, biomass, municipal waste products, and industrial waste products in the main combustion zone.

18. A method in accordance with claim 8 further comprising injecting a reburning fuel into the flow of combustion flue gas downstream of the main combustion zone such that a fuel rich zone is created, the combustion flue gas including a concentration of nitrogen oxides.

19. A method in accordance with claim 18 wherein injecting a reburning fuel into the flow of combustion flue gas comprises injecting at least one of coal, products of gasification of coal, natural gas, oil, biomass, municipal waste products, and industrial waste products into the flow of combustion flue gas.

20. A method in accordance with claim 8 further comprising generating carbon monoxide in the combustion fuel gas.

21. A method in accordance with claim 20 wherein concentration of generated carbon monoxide affects a temperature range in which nitrogen oxides react with the reduced N-containing species.

22. A method in accordance with claim 8 further comprising providing an oxidation catalyst to facilitate reducing a concentration of carbon monoxide (CO) in the combustion flue gas.

23. A combustion system comprising:
a main combustion zone for combusting a fuel;
a fuel rich zone located downstream from said main combustion zone;
at least one over-fire air port for injecting over-fire air into a combustion flue gas stream at a respective over-fire air zone;
a catalyst zone for reducing a concentration of carbon monoxide in said combustion gas stream;
a controller configured to control process conditions in the main combustion zone and the fuel rich zone such that a molar concentration of reduced N-containing species is approximately equal to a molar concentration of NO_x when the combustion flue gas reaches said over-fire air zone; and,
wherein said controller is configured to control process conditions in the main combustion zone and the fuel rich zone such that a ratio of molar concentration

of reduced N-containing species to the molar concentration of nitrogen oxides is in the range of approximately 0.8 to approximately 1.2 when the combustion flue gas reaches location of over-fire air injection location.

24. A combustion system in accordance with claim 23 wherein said main combustion zone is configured for fuel rich combustion such that said fuel rich zone is generated by fuel rich combustion in said main combustion zone.

25. A combustion system in accordance with claim 23 further comprising a reburn zone wherein a reburning fuel is injected into said combustion flue gas stream to generate a fuel rich zone downstream of said main combustion zone.

26. A combustion system in accordance with claim 23 wherein said controller facilitates controlling at least one over-fire air port.

27. A combustion system in accordance with claim 23 wherein said controller is configured to control over-fire injection temperature to a temperature of about 1050 degrees Fahrenheit to about 1750 degrees Fahrenheit.

28. A combustion system in accordance with claim 27 wherein said controller is configured to control a temperature at the over-fire air injection location to a temperature of about 1150 degrees Fahrenheit to about 1550 degrees Fahrenheit.

29. A combustion system in accordance with claim 23 configured to combust at least one of coal, products of gasification of coal, natural gas, oil, biomass, municipal waste products, and industrial waste products into the flow of combustion flue gas.

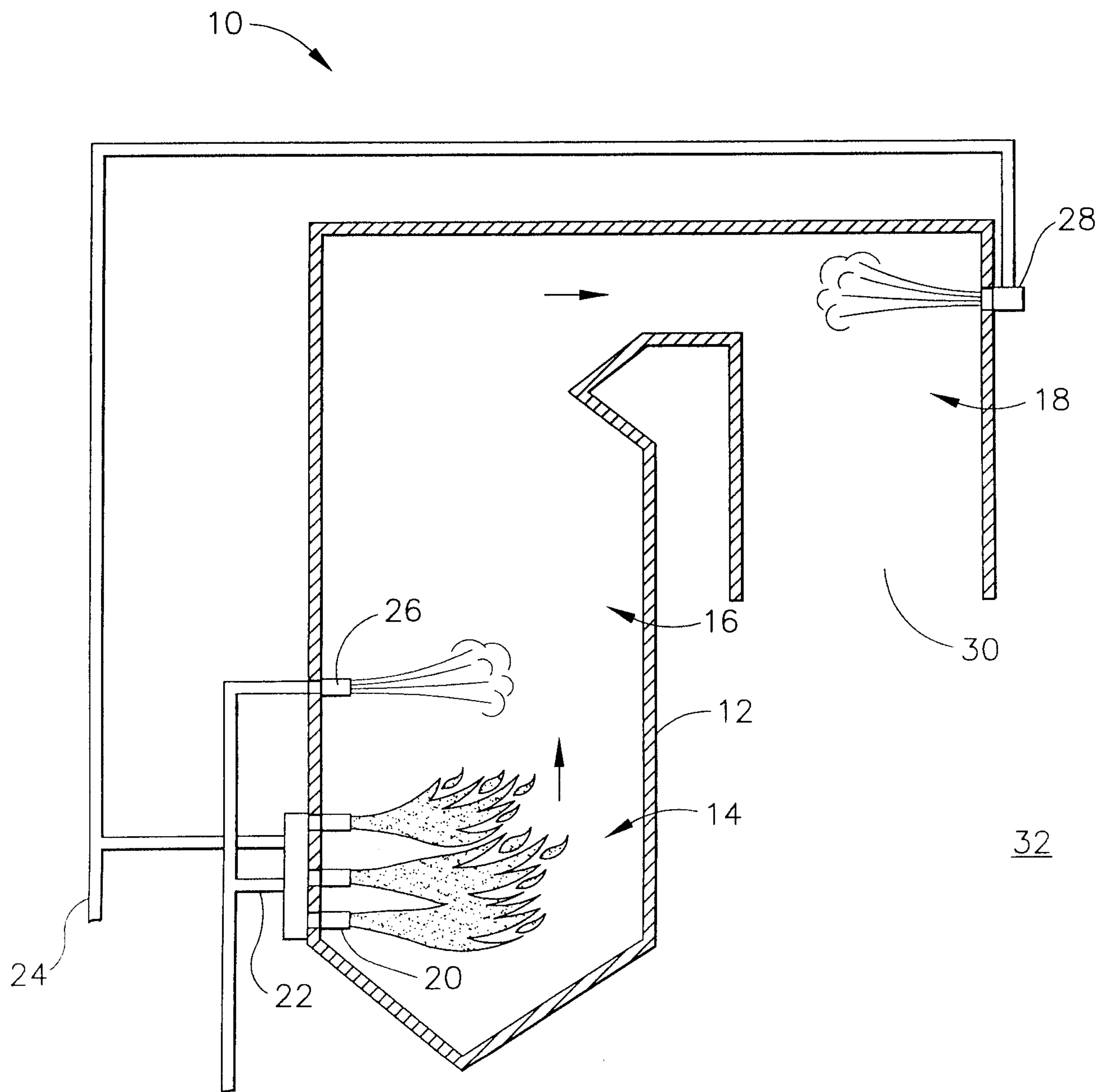


FIG. 1

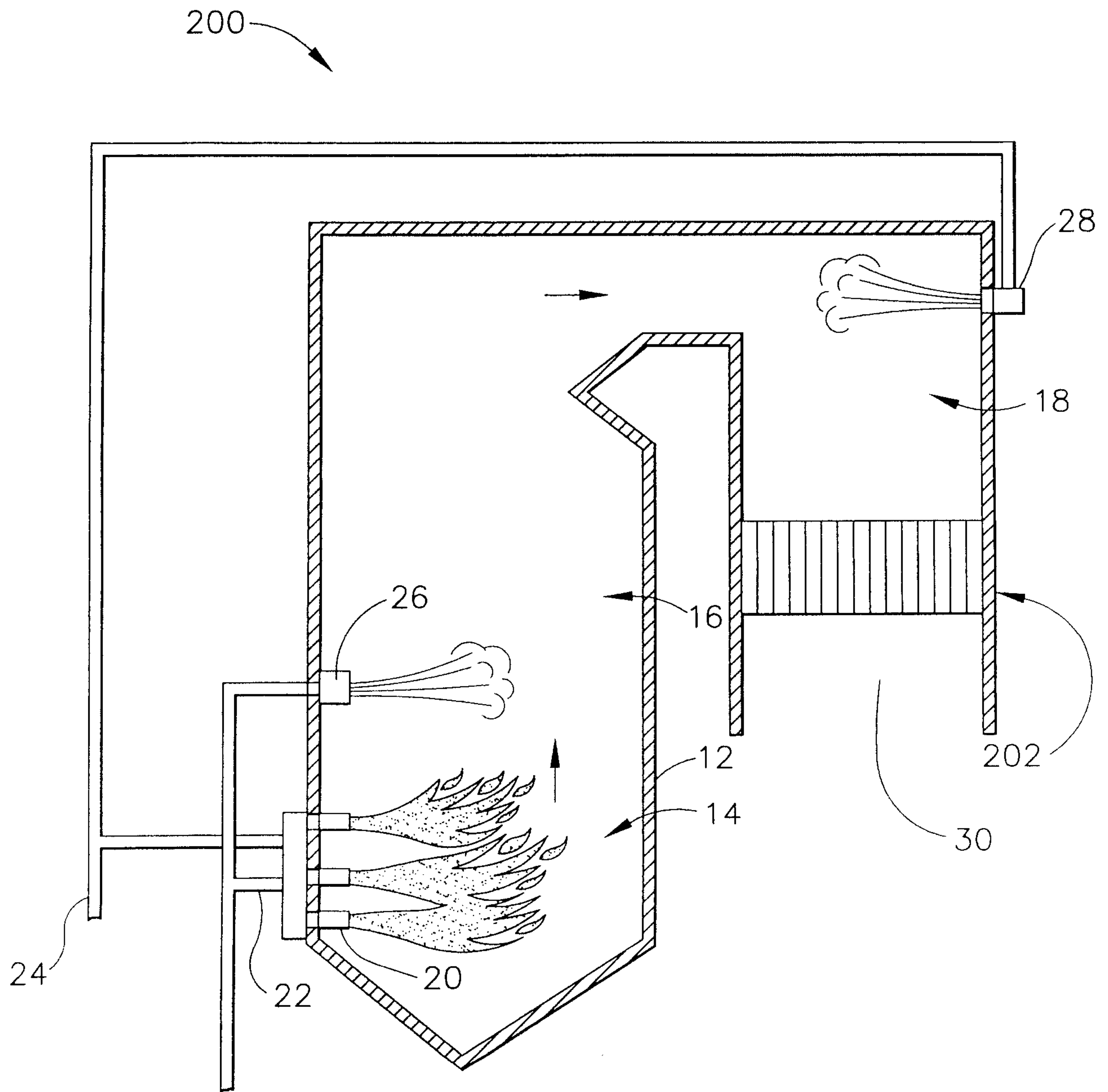


FIG. 2

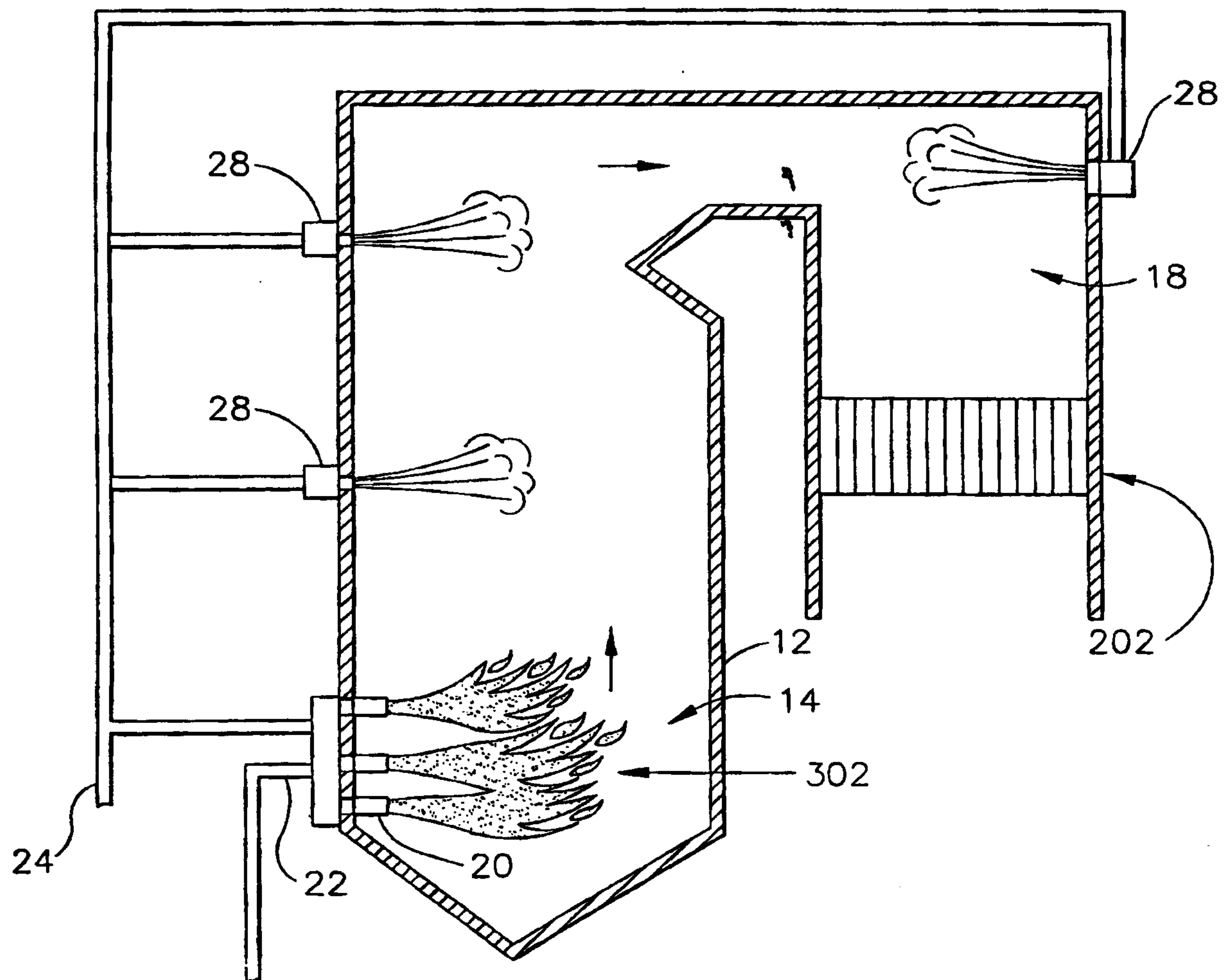


FIG. 3

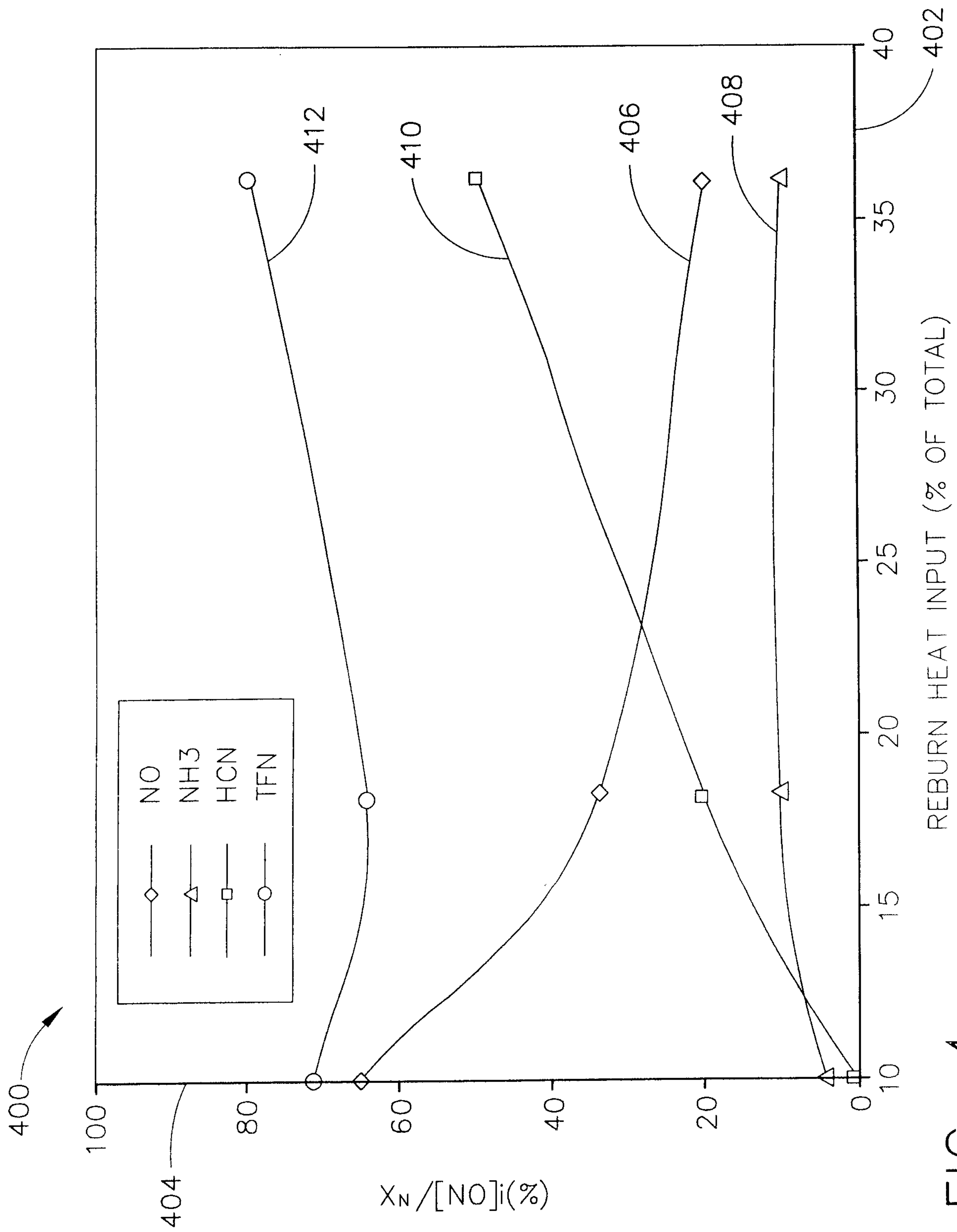
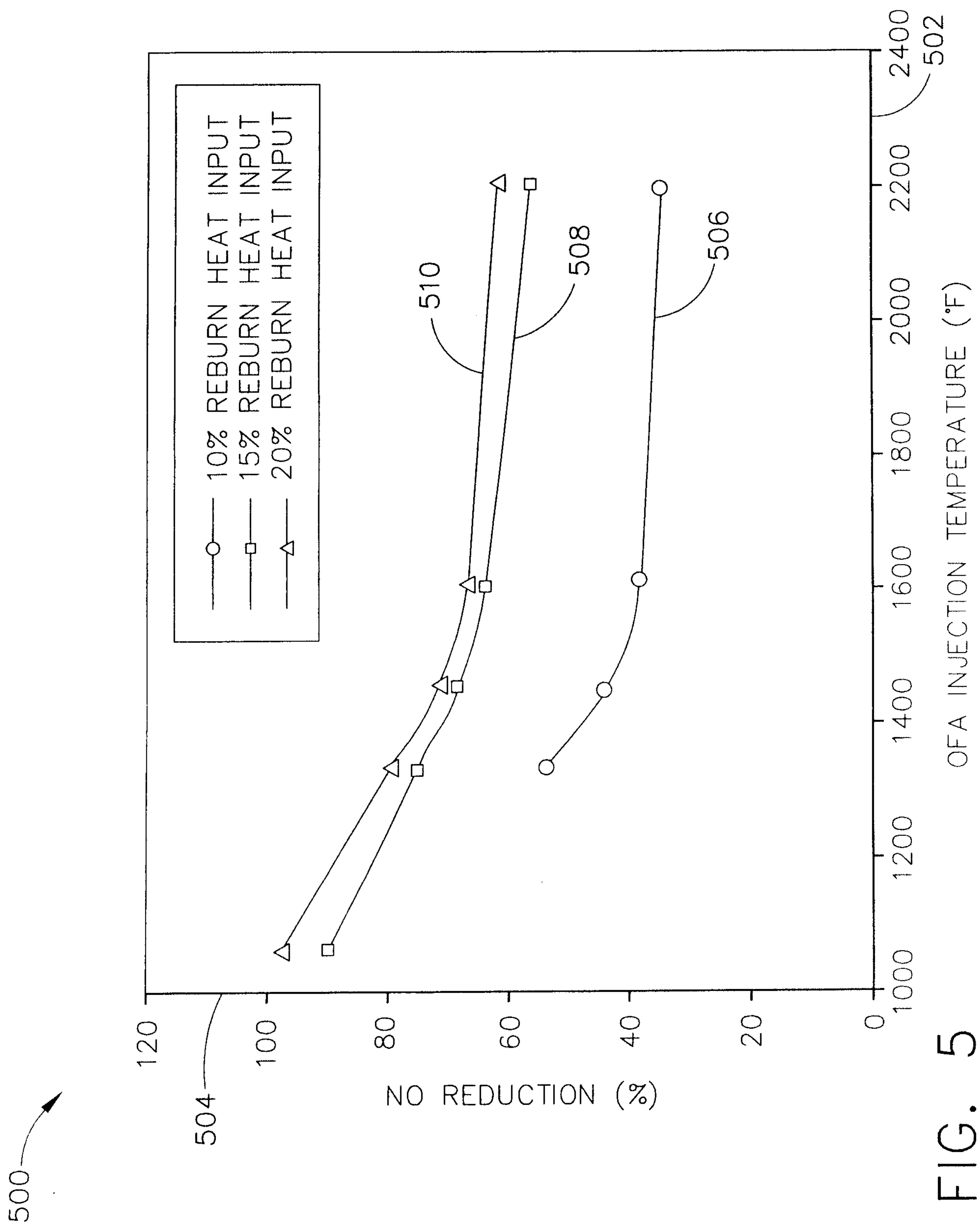
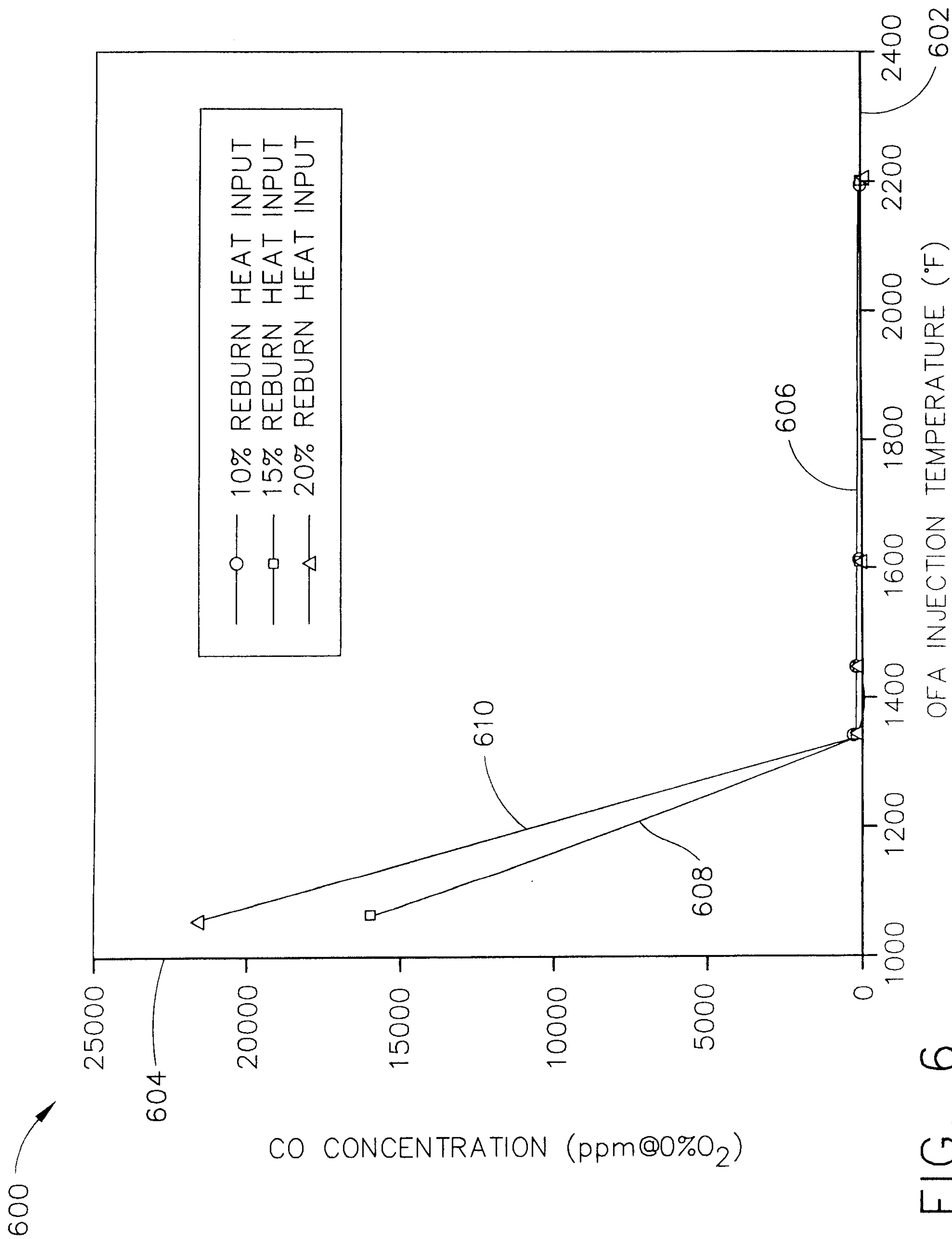


FIG. 4





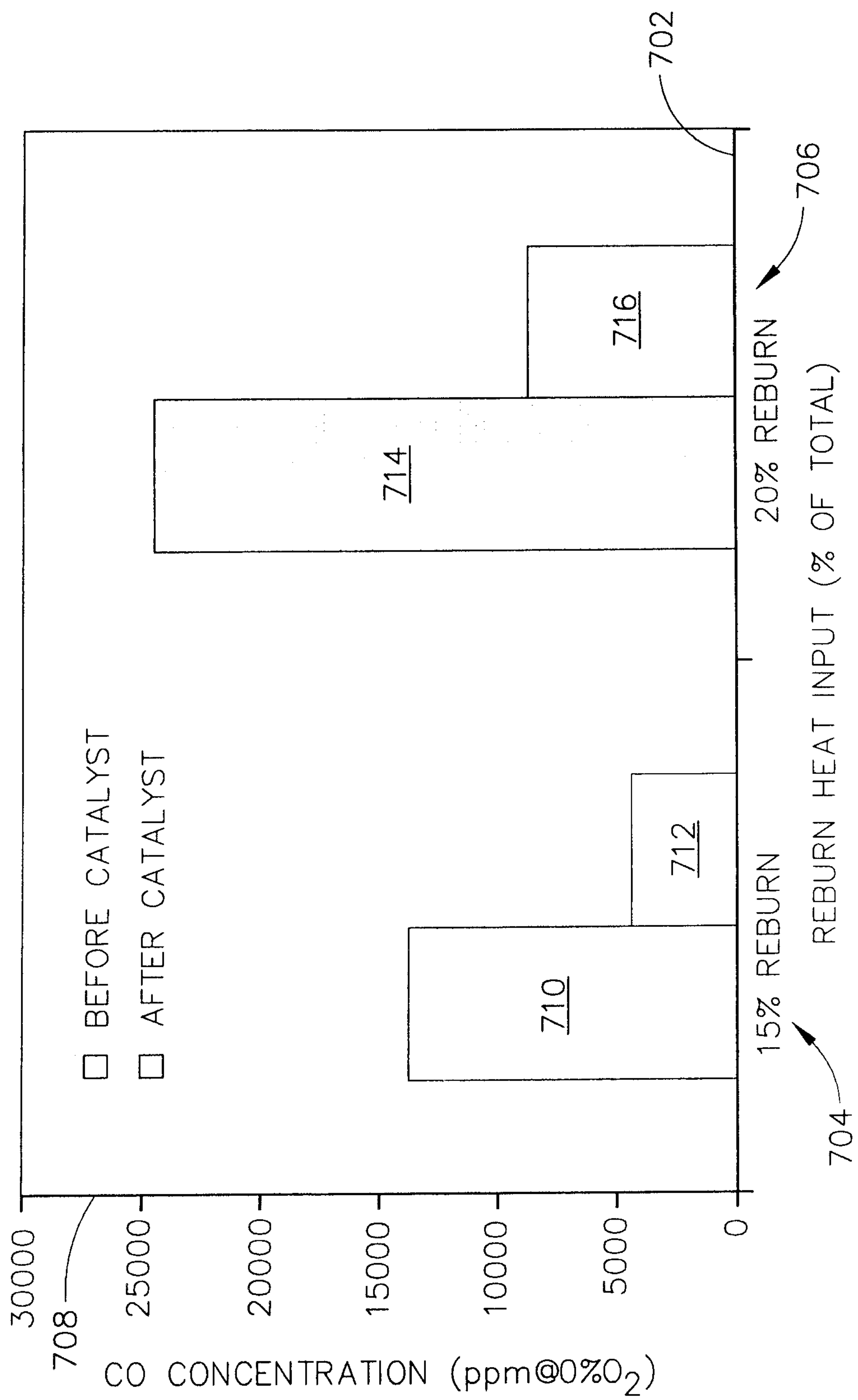


FIG. 7

