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<p>(21) International Application Number: PCT/US96/19280</p> <p>(22) International Filing Date: 5 December 1996 (05.12.96)</p> <p>(30) Priority Data: 60/008,209 5 December 1995 (05.12.95) US</p> <p>(71) Applicant (for all designated States except US): THE DOW CHEMICAL COMPANY [US/US]; 2030 Dow Center, Midland, MI 48674 (US).</p> <p>(72) Inventors; and (75) Inventors/Applicants (for US only): FINLAYSON, Malcolm, F. [IE/US]; 731 East 12 1/2 Street, Houston, TX 77008 (US). SPRINGS, Kenneth, E. [US/US]; 341 North Shanks, Clute, TX 77561 (US). GATHERS, John, J. [US/US]; 3615 Hanover Circle, Pearland, TX 77584 (US). COOPER, James, L. [US/US]; 54 Yaupon Court, Lake Jackson, TX 77566 (US). VAUGHN, Walter, L. [US/US]; Route 3, Box 68B, Brenham, TX 77833 (US). SCHUMANN, Brian, H. [US/US]; Apartment 1410, 201 Dixie Drive, Clute, TX 77531 (US). OLIVER, Stephen, M. [GB/CH]; Erlenstrasse 99, CH-8832 Wollerau (CH).</p>	<p>(74) Agent: MCKINNEY, Osborne, K.; The Dow Chemical Company, Patent Dept., B-1211, 2301 Brazosport Boulevard, Freeport, TX 77541 (US).</p> <p>(81) Designated States: AL, AM, AT, AU, AZ, BB, BG, BR, BY, CA, CH, CN, CZ, DE, DK, EE, ES, FI, GB, GE, HU, IL, IS, JP, KE, KG, KR, KZ, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, TJ, TM, TR, TT, UA, UG, US, UZ, ARIPO patent (KE, LS, MW, SD, SZ, UG), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG).</p> <p><b>Published</b> <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i></p>	
<p>(54) Title: METHOD FOR EXTERNALLY SIZING FIBROUS MATERIALS</p>		
<p>(57) Abstract</p> <p>Fibrous product is externally sized by applying to the material a basic aqueous dispersion of an interpolymer of an ethylenically unsaturated monomer and an ethylenically unsaturated carboxylic acid comonomer. The preferred dispersions which have lower initial viscosities provide dispersion/starch dilute solutions with higher viscosities and improved external sizing effectiveness. Resulting fibrous products are adequately sized and exhibit excellent printability and strength properties.</p>		

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## METHOD FOR EXTERNALLY SIZING FIBROUS MATERIALS

The present invention relates to the external  
5 sizing of fibrous materials, particularly cellulose  
such as paper. The external sizing agent is an  
interpolymer of an ethylenically unsaturated monomer and  
an ethylenically unsaturated carboxylic acid comonomer.

Sizing is the process of providing fibrous  
10 materials such as cellulose (e.g., paper) and textiles  
(e.g., fabrics) with resistance to penetration by  
liquids. Sizing may be accomplished via an internal  
sizing process, an external sizing process, or as is  
usually the case, a combination of both.

15 The processes of internal sizing and external  
sizing are very different from each other in many  
respects. Many materials that are known to be effective  
as internal sizing are generally not effective as  
external sizing agent and vice versa. Internal sizing  
20 is a method by which the sizing is initiated before the  
fibrous material is formed. This is usually  
accomplished by adding an internal sizing agent, in  
conjunction with a retention aid, directly to a fiber  
slurry to precipitate the sizing agent upon the fibers.  
25 Internal sizing agents are generally hydrophobic in  
nature, i.e., the sizing agents will have their nonpolar  
portions oriented about the surface of the fibers  
forming a protective layer wherein the penetration of  
liquids is retarded once the fibers are fabricated into  
30 a finished fibrous product such as paper and a fabric.  
See Biermann, C. J., Essentials of Pulping and  
Papermaking, Academic Press, Inc., 1993, p. 197.

External sizing, which is also referred to as  
surface, tub, or calender sizing, is substantially  
35 different from internal sizing in that external sizing

agents are applied to one or both surfaces of already-formed fibrous products in the absence of retention aids. Because external sizing is accomplished by a different mechanism than internal sizing, certain hydrophobic materials as well as non-hydrophobic materials, such as starch, can be effectively used as external sizing agents. Whereas internal sizing takes place on a substantial portion of the fibers throughout the three dimensional matrix of the paper or fabric and generally involves modification of the surface energy of the fibers, external sizing occurs when an external sizing agent is applied to a surface of a fabricated fibrous product and either fills the capillaries and voids between individual fibers, or acts to modify the surface energy of the fibers nearest the surface rather than all the fibers throughout the matrix, rendering liquid penetration more difficult. See Biermann, p. 197. Because of the requirement of filling surface capillaries, the surface tension or energy of the external sizing agent is an important factor in successful external sizing of fibrous products.

Interpolymers of an ethylenically unsaturated monomer and an ethylenically unsaturated carboxylic acid comonomers have been used for internal sizing of paper previously. See, for example, U.S. Patent Nos. 3,872,039; 3,899,389; and 4,181,566. However, heretofore, such interpolymers have not been employed as external sizing agents. That is, these disclosures by Vaughn et al. teach the use of such interpolymers as internal sizing agents.

For internal sizing of paper, Vaughn et al. in US Patent Nos. 3,872,039; 3,899,389; and 4,181,566, described the combination of an ammoniated copolymer of ethylene and an ethylenically unsaturated carboxylic acid comonomer and a cationic retention aid. The

advantage of the internal sizing systems disclosed by Vaughn et al. is said to be their utility over the complete range of pH conditions found in paper-making operations. For these systems, Vaughn et al. taught the order of addition of the sizing agent and the retention aid to a conventional paper making process was non-critical, however, Vaughn et al. preferred to introduce their sizing agent prior to the addition of a retention aid.

10 Rowland et al. in US Patent Nos. 5,206,279 and 5,387,635 disclosed aqueous dispersions of interpolymers of ethylene and an ethylenically unsaturated carboxylic acid comonomer. Rowland et al. described the combination of two bases, one as a weak cation and the other as a strong cation. Rowland et al. teach that this combination permits the preparation of stable dispersions of interpolymers having relatively low carboxylic acid concentrations (e.g. less than 15 weight percent acrylic acid content). However, Rowland et al. did not disclose that their dispersions were useful as external sizing agents for fibrous materials.

While there are a variety of known sizing systems and alleged solutions, there is still a need for an external sizing system that provides improved sizing performance, i.e., higher Hercules Size Test (HST) values as measured by accordance with TAPPI method T 530 pm-89. Higher HST values translate into improved hydrophobicity and liquid penetration resistance.

To fulfill these objects, we have discovered a novel process for external sizing fibrous materials and products. The process comprises applying a basic aqueous dispersion of an interpolymer of an ethylenically unsaturated monomer and an ethylenically unsaturated carboxylic acid to a fibrous material after the fibrous material has been finished or fabricated

into its final form. In one preferred embodiment, the basic aqueous dispersion is prepared at a controlled reduced viscosity to provide dilute solution with a starch having higher viscosities.

5           The present process is particularly suitable for external sizing of paper and paper products. Further, in addition to providing improved external sizing, the present process provides fibrous products with improved cohesive strength and improved  
10           printability. An advantage of the inventive process is now processors and mills can employ the same or similar basic aqueous dispersions for purposes of external sizing and internal sizing, thereby eliminating the need to buy, receive, store and use different substances for  
15           internal sizing and external sizing. Another advantage provided by the present process is the use of basic aqueous dispersions which are stable and do not require the use of surface active ingredients.

          The term "external sizing," is used herein, to  
20           refer to a method of sizing in which a sizing material is contacted with fabricated finished fibrous material under conditions effective to size the fibrous material, i.e., deposit the sizing agent on the fibrous material and increase the hydrophobicity of the fibrous material  
25           as measured in seconds by the Hercules Size Test, TAPPI method T 530 pm-89. Accordingly, the term "external sizing" is used herein generically and as such is inclusive of such terms as "surface sizing," "tub sizing," "calender sizing" and the like.

30           The term "water-dispersible," as used herein, refers to a material which can exist in the form of a stable aqueous colloidal dispersion in the absence of a surface active agent or surfactant.

          The term "ethylenically unsaturated monomer,"  
35           as used herein, refers to any water-immiscible monomer

containing a terminal double bond capable of polymerization under normal conditions of free-radical addition polymerization to form a water-insoluble homopolymer having a polyethylenic backbone.

5           The term "ethylenically unsaturated carboxylic acid comonomer" is used herein to refer to a comonomer containing alpha-beta unsaturation and a carboxylic acid group and which is capable of free-radical addition interpolymerization through the ethylenically  
10 unsaturated group with ethylenically unsaturated monomers.

          The term "interpolymer", as used herein, refers to polymers prepared by the polymerization or interpolymerization of at least two different types of  
15 monomers. The generic term "interpolymer" is inclusive of the term "copolymer" and the term "terpolymer." The term "copolymer" is usually employed to refer to a polymer prepared from two different monomers such as an ethylene-acrylic acid (EAA) copolymer. Conversely, the  
20 term "terpolymer" is usually employed to refer to a polymer prepared from three different types of monomers such as an ethylene-acrylic acid-vinyl acetate (EAA/VA) terpolymer.

          The term "dilute solution" is used herein to  
25 refer to external sizing solutions wherein a dispersion is prepared at a higher solids concentration and then is diluted to some substantially lower solids concentration by the addition of water. Dilute solutions used in the present inventive process are admixtures of at least one  
30 basic aqueous dispersion and at least one starch. Generally, the dilute solution will have a total dispersion/starch solids concentration of less than about 20 weight percent.

          The amount of size imparted to the fibrous  
35 material may be controlled by the amount of basic

aqueous dispersion applied. Generally, the amount of basic aqueous dispersion applied will be in the range of 0.1 to 50 pounds per ton of fibrous material, preferably in the range of 1 to 25 pounds per ton of fibrous material.

The amount of sizing required or the desired HST value will depend on specific end-use application requirements. For example, fine printing and writing grade paper typically requires an HST value of about 50 seconds, whereas water repellent outdoor apparel can require substantially higher HST values. That is, the higher the HST value, the better the hydrophobicity and water resistance. Thus, where improved hydrophobicity is the primary performance requirement, the present process provides a HST value greater than 45, preferably greater than about 100, more preferably greater than about 200 and most preferably greater than about 500.

Also, in the present process, the basic aqueous dispersions and dilute solutions provide improved hydrophobicity at fairly moderate loadings, i.e., excessive sizing quantities are not required for higher HST value relative to conventional external sizing agents such as styrene maleic anhydride (SMA) systems.

The external sizing agents suitably employed in the practice of this invention are interpolymers of an ethylenically unsaturated monomer and at least one ethylenically unsaturated carboxylic acid comonomer. These interpolymers are generally solid or semi-solid, often in the form of pellets, and water-dispersible.

The surface sizing agent is a normally solid, water-insoluble and alkali-insoluble thermoplastic addition polymer in the form of an aqueous colloidal dispersion. The ethylenically unsaturated carboxylic acid comonomer groups of the interpolymer should be

neutralized with ammonia, alkali metal hydroxides, alkaline earth metal hydroxides, or mixtures thereof to form active salt groups. This is normally accomplished by dispersing the interpolymer in aqueous solutions of  
5 the above bases or mixtures thereof to form a basic aqueous dispersion of the interpolymer. However, it is understood that an ethylenically unsaturated carboxylic acid in active salt form may be interpolymerized with the ethylenically unsaturated monomer in order to  
10 prepare a suitable interpolymer having active salt groups. In any event, the occurrence of active salt groups formed on the interpolymer should be generally throughout the macromolecules thereof so that each macromolecule contains a minimum number of active salt  
15 groups sufficient to render the polymer water-dispersible as hereinbefore. The maximum number of acid groups which have been converted into active salt groups that may be present in the macromolecules is fixed by the requirement that the molecule be substantially  
20 water-insoluble. Generally speaking, such interpolymers contain from about 1 to about 99 weight percent of acid comonomer, with preferred interpolymers containing from about 6 to about 40 weight percent of acid comonomer and especially preferred interpolymers containing from about  
25 10 to about 25 weight percent comonomer.

Exemplary preferred interpolymers are the random polymer products of copolymerization of mixtures of one or more polymerizable ethylenically unsaturated carboxylic acids having 3 to 8 carbon atoms, inclusive  
30 of anhydrides and alkyl esters and half esters, such as acrylic acid, methacrylic acid, maleic acid and anhydride, itaconic acid, fumaric acid, crotonic acid and citraconic acid and anhydride, methyl hydrogen maleate, ethyl hydrogen maleate, and one or more  
35 ethylenically unsaturated hydrocarbon monomers such as

the aliphatic  $\alpha$ -olefin monomers, e.g., ethylene, propylene, butene-1 and isobutene; conjugated dienes, e.g., butadiene and isoprene; and monovinylidene aromatic carbocyclic monomers, e.g., styrene,  $\alpha$ -methylstyrene, toluene, and t-butylstyrene.

In addition, other ethylenically unsaturated monomers which are not entirely hydrocarbon can be interpolymerized with the aforementioned carboxylic acid comonomers. Examples of suitable monomers which are not entirely hydrocarbon include, but are not limited to, esters of ethylenically unsaturated carboxylic acids such as ethyl acrylate, methyl methacrylate, ethyl methacrylate, methyl acrylate, isobutyl acrylate, and methyl fumarate; unsaturated esters of non-polymerizable carboxylic acids such as vinyl acetate, vinyl propionate, and vinyl benzoate; vinyl halides such as vinyl and vinylidene chloride; vinyl ethers; ethylenically unsaturated amides and nitriles such as acrylamide, acrylonitrile, methacrylonitrile and fumaronitrile. It is understood that the aforementioned suitable monomers may be interpolymerized with the preferred hydrocarbon monomer and carboxylic acid comonomer in proportions such that a water and alkali-insoluble interpolymer is provided. Preferred interpolymers include interpolymers from about 70 to about 90 weight percent of ethylene, from about 10 to about 20 weight percent of one or more ethylenically unsaturated carboxylic acids, such as acrylic acid and methacrylic acid (unneutralized or neutralized to an active salt form) and from 0 to about 20 weight percent of another ethylenically unsaturated monomer as described hereinbefore such as acrylonitrile, ethyl acrylate and vinyl acetate. The above interpolymers may be made according to the methods and procedures of U.S.

Patent Nos. 3,436,363; 3,520,861; 4,599,392; and  
4,988,781.

Other suitable interpolymers can be made from  
pre-formed, non-acid polymers by subsequent chemical  
5 reactions carried out thereon. For example, the  
carboxylic acid group may be supplied by grafting a  
monomer such as acrylic acid or maleic acid onto a  
polymer substrate such as polyethylene. Additionally,  
interpolymers containing carboxylic anhydride, ester,  
10 amide, acylhalide and nitrile groups can be hydrolyzed  
to carboxylic acid groups which can then be neutralized  
to form the activated salt form of carboxylic acid.

In general, better external sizing is provided  
by dispersions made from interpolymers containing lower  
15 carboxylic acid comonomer concentrations. That is, for  
example, an ethylene acrylic acid (EAA) dispersion  
containing 15 weight percent acrylic acid will generally  
provide higher HST values than an ethylene acrylic acid  
(EAA) dispersion containing 20 weight percent acrylic  
20 acid prepared using the same method and procedures at  
the same percent solids level and diluted and added to  
the fibrous material at the same concentration.  
Aqueous dispersions of the above interpolymers employed  
in the invention may utilize amines (e.g., ammonia and  
25 monoethanolamine), alkali metal hydroxides, alkaline  
earth metal hydroxides or mixtures thereof. Dispersions  
of the interpolymer in aqueous ammonia to neutralize the  
carboxylic acid groups can be made according to U.S.  
Patent Nos. 3,389,109; 3,872,039; 3,899,389; and  
30 4,181,566. Dispersions of alkali metal hydroxides,  
alkaline earth metal hydroxides and mixtures with amine  
(i.e., mixed base dispersion) may suitably be made  
according to the methods and procedures of U.S. Patent  
Nos. 5,206,279 and 5,387,635.

With respect to the cation used to prepare the dispersions useful in the present invention, a mixed base system of potassium or sodium with ammonia provides higher HST values than potassium dispersions. Also, potassium dispersions generally provide higher HST values than ammonia dispersions. Further, potassium dispersions provide better print quality than mixed base or ammonia dispersions while ammonium dispersions provide better toner adhesion. However, mixed base dispersions are preferred, especially at lower interpolymer comonomer concentrations (e.g.,  $\leq 15$  weight percent).

Also effective external sizing results are obtained with paper for both virgin fiber sources as well as for 100% recycled fibers. Moreover, external sizing effectiveness is independent of the application method of the dispersion sizing agent. For example, effective sizing is obtained for both continuous and batch sizing operations.

The basic aqueous interpolymer dispersion should contain an amount of solid interpolymer such that fibrous material sizes after application of the dispersion. This amount varies depending upon the particular interpolymer employed and, as discussed above, the particular end-use application. However, unlike typical internal sizing processes, in the present process, all of the interpolymer that is applied or introduced to the fibrous material will be retained on the surface and/or in the capillaries and voids of the fibrous product.

For use in the present invention, the dispersion solids concentration may be as high as 50 percent interpolymer by weight and as low as 1 percent interpolymer by weight. However, the dispersion or

dilute solution solids concentration should not be so high that the dispersion or dilute solution is too viscous to be effectively or sufficiently applied.

The degree of sizing obtained is controlled by  
5 the amount of solid interpolymer in the dispersion that is applied to the fibrous material. That is, the greater the amount of solid interpolymer applied, the greater the degree of sizing. Correspondingly, the lesser the amount of solid interpolymer applied, the  
10 lesser the degree of sizing. Therefore, although other means may be employed to control the degree of sizing, the most convenient means is to adjust the concentration of interpolymer in the dispersion and/or the total amount of dispersion that is actually applied to the  
15 fibrous material.

Surprisingly, however, the solids concentration at which the dispersion is initially prepared affects the sizing ability of the dilute solution even though the total final solids  
20 concentration of the dilute solution is the same. That is, we have discovered that dispersions prepared at higher percent solids concentrations and used in dilute solutions result in lower HST values all else being the same. Specifically, we have found for the same cation  
25 and the same interpolymer comonomer concentration, a 20 percent solids dispersion provides a HST value at least about 50 percent higher than a 35 percent solids dispersion. This discovery is surprising and unexpected in that one skilled in the art would not expect the  
30 initial dispersion solids concentration to affect the sizing performance with the applied solids concentration is unchanged.

As such, preferred basic aqueous dispersions for use in the invention have an interpolymer solids  
35 concentration less than 35 weight percent, more

preferably equal to or less than 25 weight percent, and most preferably equal to or less than 20 weight percent.

As an additional surprise, we have discovered that dilute solutions with higher viscosities result  
5 from dispersions initially prepared at lower viscosities and that higher HST values are achieved with dilute solutions having higher viscosities. This was found to be independent of whether deionized or ordinary tap water was employed to cook the starch before use in the  
10 dilute solutions. As such, in addition to (or as an alternative to) employing a dispersion prepared at a lower percent solids concentration (e.g., less than 35 percent) to accomplish improved external sizing, the basic aqueous dispersion itself can be prepared at a  
15 lower viscosity to effectuate improved hydrophobicity and liquid penetration resistance.

Any known method or technique can be employed to provide a basic aqueous dispersion with a lower initial viscosity including, for example, but not  
20 limited to, known methods and procedures that alter the interpolymer used to prepare the dispersion. As another viable technique for use in the present invention, the utilization of higher shear agitation during digestion and agitation during the preparation of dispersion is  
25 known to provide reduced dispersion viscosity.

Thus, in specific embodiments of the present invention, the basic aqueous dispersions will have a relatively low initial viscosity at 23°C, preferably less than about 700 centipoises, more preferably less than  
30 about 500 centipoises and most preferably less than about 300 centipoises as measured at 23°C using a Brookfield Viscometer, Model RVTD, equipped with a #3 spindle at 20 rpms.

The dilute solutions used in the present  
35 process will contain 1 to 30 weight percent basic

aqueous dispersion, preferably 5 to 20 weight percent basic aqueous dispersion and have a concentration in the range of 1 to 20 percent total solids by weight, preferably 2 to 15 percent total solids by weight. The dispersion/starch dilute solutions will have generally have a viscosity greater than about 50, however, in preferred embodiments of the present process, the dilute solution will have a relatively high viscosity at 23°C, preferably greater than 150 centipoises, more preferably greater than 175 centipoises, and more preferably greater than 200 centipoises as measured at 23°C using a Brookfield Viscometer, Model RVTD, equipped with a #3 spindle at 20 rpm.

Before the basic aqueous dispersion or dilute solution is applied to the fibrous product, it is preferable that the product be substantially dry. By substantially dry is meant that the fibrous product has less than about 10 percent, preferably less than about 6 percent water. Conventional dryers known in the art, e.g. steam can, electrical can, or infrared dryers, may be employed to enhance the drying of the paper.

The basic aqueous dispersion or dilute solution may be applied to the fibrous product by any method sufficient to apply the interpolymer onto the product. For example, the fibrous product may be immersed or soaked in the dispersion or dilute solution for a time sufficient to apply the interpolymer onto the product. The dispersion or dilute solution may also be sprayed onto or rolled onto the fibrous product.

Conventional equipment well known in the art may be employed to apply the dispersion or dilute solution. Such equipment as roll coaters, air knives, and blade coaters may be employed. One suitable type of equipment is a size press having a bottom roller which rotates in a pan filled with the dispersion or dilute solution and

picks up the dispersion or dilute solution. The dispersion or dilute solution is applied to the fibrous product as the product rolls over the roller.

Additives may be applied to the fibrous material to modify the final properties of the fibrous product, e.g., increase the strength, so long as the additives do not nullify the sizing effect discovered by the applicants. Such additives may include starches, defoamers, dyes, anti-stats, brighteners, fillers, etc. Suitable additives may be either added directly to the dispersion or dilute solution or, alternatively, applied to the fibrous material before, during or after the application of dispersion or dilute solution.

In a preferred embodiment of the invention, starch is added with the external sizing agent. Preferred starches are ethylated and cationic starches. Examples of preferred starches include, but are not limited to, an ethylated corn starch (supplied by A. E. Staley Manufacturing Co. under the designation of Ethlex 2025 and supplied by Penford Products Co. under the designation of PG 280), a cationic corn starch supplied by National Starch and Chemical Co. under the designation of CatoSize 270 and quaternary ammonium cationic starch derivatives such as, for example, Stalock 400 available from A. E. Staley Manufacturing Company and Solvatox N available from Avebe Ltd. (Sweden). Other cationic starches useful in the present invention include primary, secondary and tertiary amine cationic starch derivatives and other cationic nitrogen substituted starch derivatives as well as cationic sulfonium and phosphonium starch derivatives. A person with ordinary skill in the art will appreciate that starches and starch derivatives should be employed as gelatins; as such, pre-cooking (e.g., 1 hour at 90-95°C)

may be required prior use although some starches are commercially available already gelatinized.

After the dispersion has been applied to the fibrous material, the fibrous material is allowed to dry at ambient. Alternatively, the sized fibrous material may be dried in a dryer. Typically, the fibrous material is dried to less than about 6 percent moisture content before use.

#### 10 EXAMPLE 1

A one gallon Parr reactor was configured to allow dispersions to be prepared at temperatures greater than 100°C and increased pressures. An amount to provide a 35 percent solids dispersion of ethylene-acrylic acid copolymer, EAA, (PRIMACOR™ 5990 available from The Dow Chemical Company, having a 20 weight percent acrylic acid content and a melt index of 1300 grams/10 minutes as measured by ASTM D-1238 Condition 190°C/2.16 kg) was added to a 0.42 mole ratio aqueous ammonium hydroxide (NH<sub>4</sub>OH) solution in the reactor under agitation. Agitation was provided by a magnetically coupled stirrer having two six-blade impellers( with the blades at a 45° pitched) set at 300 revolutions per minute. A Watlow™ temperature controller ramped the temperature of the reactor from ambient to 120°C for two hours, then cooled the reactor to ambient temperature. To confirm that the reactor integrity remained intact during the run, the system was pressured with 20 pounds per square inch gauge (psig) of nitrogen at the beginning of the run. After the run was completed, the reactor pressure was checked to confirm that it had returned to the original setting. The resulting 35 percent solids EAA dispersion was then diluted to 6 percent solids for use in external sizing.

The above 6 percent solids dispersion of EAA was applied with a size press at an amount of 15 pounds of solids EAA per ton of paper to paper having an initial Hercules Size Test value of 33 seconds at 85 percent reflectance according to TAPPI method T 530 pm-89. The final Hercules Size Test value of the paper according to TAPPI method T 530 pm-89 after application of EAA and drying was 707 seconds at 85 percent reflectance.

10 EXAMPLE 2

An equivalent dispersion of 6 percent solids EAA as employed in Example 1 was applied with a size press to paper having an initial Hercules Size Test value of 33 seconds at 85 percent reflectance according to TAPPI method T 530 pm-89 except that the amount of solid EAA applied was 4.85 pounds per ton of paper. The final Hercules Size Test value of the paper according to TAPPI method T 530 pm-89 after application of EAA and drying was 507 seconds at 85 percent reflectance.

20 The paper of Examples 1 and 2 exhibited excellent properties including good strength and printability.

Examples 3-6

25 In another evaluation, four different dispersions were prepared based on ammonium and potassium at a 0.42 mole ratio and at 20 and 35 percent solids concentrations. The interpolymer employed for the four dispersions was an experimental ethylene acrylic acid interpolymer containing 20 weight acrylic acid and having a 1300 g/10 minute melt index as measured in accordance with ASTM D-1238 Condition 190°C/2.16 kg., supplied by The Dow Chemical Company under the designation of XU-60751.16. The degree of  
30 sizing for each system was measured on alkaline paper  
35

sheets (copier grade paper having a basis weight of 75  
 grams/square meter) for 8 weight percent total solids  
 dilute solutions based on dispersion loadings of 4 lbs.  
 dispersion per ton of paper and cationic starch loadings  
 5 of 40 lbs. per ton of paper. Application of the  
 dispersion was at room temperature using a paper padder.  
 The padder settings were 2.2 meters/minute and 2.5 Bars.  
 The sheets were dipped into a pan containing about 400  
 milliliters of dispersion one to three times with one  
 10 padder nip following each dip. The sheets were dried  
 for about two minutes in an Adirondack Drum Dryer set at  
 105°C. The HST values for the four systems are shown in  
 Table 1.

15

Table 1

Example	Cation Type	Percent Solids	HST Value, seconds
3	Potassium	20	130
4	Potassium	35	109
5	Ammonium	20	71
6	Ammonium	35	42

The results in Table 1 indicates that  
 potassium based external sizing agents are more  
 effective than ammonium based sizing agents and that  
 20 surprisingly preparation of the dispersion at lower  
 solids concentrations can significantly improve sizing  
 efficiency.

Examples 7-9

25

In another evaluation, three different  
 dispersions were prepared at 35 percent solids  
 concentrations using the same experimental interpolymer

employed for Example 3-6 above. The three dispersions were prepared using shear intensities during digestion and agitation and as such resulted in different initial viscosities for the final dispersions as shown in Table 2 below. The three dispersions were all prepared using potassium as the cation at a 0.42 mole ratio. After the dispersion were prepared, each was admixed with cationic starch and diluted to an 8 percent total solids dilute solution (i.e., 7.08% cationic starch/0.92% interpolymer). The degree of sizing for each dilute solution was measured using Dalum paper (100% recycled grade paper having a basis weight of 93 grams/square meter) at loadings of 10 lbs. dilute solution per ton of paper. Application of the sizing solutions was the same as described for Examples 3-6. Table 2 shows the HST values for each system.

Table 2

Example	Dispersion Viscosity, cP	Dilute Solution Viscosity, cP	HST Value, seconds
7	700	145	42
8	440	198	78
9	260	234	131

Table 2 indicates, surprisingly, that dispersions with higher viscosities provide dilute solutions with lower viscosities and lower viscosity dilute solutions provide higher HST values.

Examples 10 and 11

In another evaluation, two different dispersions were prepared at 20 percent interpolymer solids concentrations using an ethylene acrylic acid copolymer containing 15 weight percent acrylic acid and having a 1300 g/10 minute melt index measured in

accordance with ASTM D-1238 Condition 190°C/2.16 kg.  
Both dispersions were mixed base dispersions. Example  
10 was a 0.5 mole ratio potassium/0.7 mole ratio  
ammonium dispersion and Example 11 was a 0.5 mole ratio  
5 sodium/0.7 mole ratio ammonium dispersion. The degree  
of sizing for the two systems was measured on alkaline  
paper sheets for dispersion loadings of 4 lbs.  
dispersion per ton of paper. Application of the  
dispersions was the same as described for Examples 3-6.  
10 The HST values for the two systems are shown in Table 3.

Table 3

Example	Cation Type	HST Value, seconds
10	Potassium/Ammoniu m	110
11	Sodium/Ammonium	102

The results in Table 3 indicates that mixed  
15 based dispersions provide very effective external sizing  
systems.

WHAT IS CLAIMED IS:

1. A method of externally sizing a fibrous material which comprises applying to the material a  
5 basic aqueous dispersion of an interpolymer of an ethylenically unsaturated monomer and an ethylenically unsaturated carboxylic acid.
2. The method of Claim 1 wherein the fibrous  
10 material is a cellulosic material.
3. The method of Claim 1 wherein the fibrous material is a textile material.
- 15 4. The method of Claim 2 wherein the cellulosic material is paper.
5. The method of Claim 3 wherein the textile material is a fabric.  
20
6. The method of any one of the preceding claims wherein at least one starch is admixed with the basic aqueous dispersion.
- 25 7. The method of Claim 6 wherein the interpolymer is a copolymer of ethylene and acrylic acid.
8. The method of Claim 7 wherein the acrylic  
30 acid content is from about 10 to about 25 weight percent of the copolymer.
9. The method of Claim 4 wherein the interpolymer is applied to the paper with a size press.

10. The method of any one of the preceding claims wherein the cation of the dispersion is aqueous ammonia, alkali metal hydroxide, alkaline earth metal hydroxide, or mixtures thereof.

11. The method of Claim 10 wherein the dispersion is mixed base dispersion.

12. The method of Claim 11 wherein the mixed base dispersion employs ammonium and potassium as cations.

13. The method of Claim 10 wherein the dispersion is a potassium dispersion.

14. The method of Claim 10 wherein the dispersion is a sodium dispersion.

15. The method of Claim 1 wherein the fibrous material is internally sized before applying the dispersion.

16. The method of Claim 4 wherein the paper contains a filler.

17. The method of any one of the preceding claims wherein the dispersion has an interpolymer solids concentration less than 35 weight percent.

18. The method of any one of the preceding claims wherein the dispersion is admixed with starch and the dispersion/starch dilute solution has a 23°C Brookfield viscosity of equal to or greater than 150 centipoises as measured with a #3 spindle at 20 rpms.

19. The method of any one of the preceding claims wherein the dispersion has an initial 23°C Brookfield viscosity of less than or equal to 500  
5 centipoises as measured with a #3 spindle at 20 rpms.

20. The method of Claim 6 wherein the starch is a cationic or ethylated starch.

# INTERNATIONAL SEARCH REPORT

International Application No  
PCT/US 96/19280

A. CLASSIFICATION OF SUBJECT MATTER  
IPC 6 D21H23/22 D06M15/263 //D21H21:16,17:43

According to International Patent Classification (IPC) or to both national classification and IPC:

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
IPC 6 D21H D06M

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	DATABASE WPI Section Ch, Week 9236 Derwent Publications Ltd., London, GB; Class A89, AN 92-296371 XP002030458 & JP 04 204 746 A (MITSUBISHI PAPER MILLS LTD) , 27 July 1992 see abstract ---	1,2,4,6, 7,15,16
X	US 4 070 319 A (CAREL PHILIPPE ROBERT RAYMOND ET AL) 24 January 1978 see claim 1 ---	1-3,7
Y	US 3 872 039 A (VAUGHN WALTER LEE ET AL) 18 March 1975 cited in the application see column 1, line 20 - line 25; example I --- -/--	1,2,4,7, 15



Further documents are listed in the continuation of box C.



Patent family members are listed in annex.

\* Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
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- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- "&" document member of the same patent family

Date of the actual completion of the international search

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# INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 96/19280

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

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A	US 3 919 149 A (CUSHMAN DONALD R ET AL) 11 November 1975 see column 2, line 35 - column 4, line 62 ---	1,2,4
A	EP 0 171 670 A (PPG INDUSTRIES INC) 19 February 1986 see whole document -----	

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