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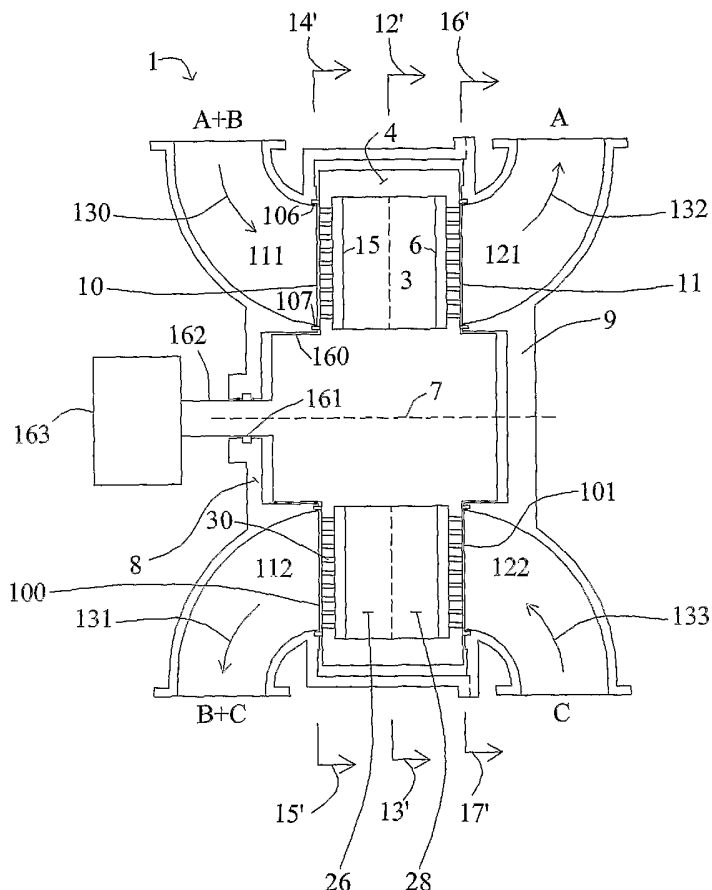
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(54) Title: HYDROGEN RECYCLE FOR HIGH TEMPERATURE FUEL CELLS



(57) Abstract: High temperature fuel cell electrical generation systems are provided that are adapted to enable selective generation of electrical power, and/or hydrogen fuel, and/or useable heat, allowing flexible operation of the generation system. In such embodiments, the high temperature fuel cell may be either a MCFC or a SOFC. The disclosed systems relate to high temperature fuel cells exploiting gas separation devices in which a first gas mixture is to be separated so that a first product of the separation is enriched in a first component, while a second component is mixed with a displacement purge stream to form a second gas mixture, with provision to prevent cross contamination of purge gas components into the first product stream. The invention may be applied to hydrogen (component A) enrichment from syngas mixtures such as fuel cell anode exhaust, where dilute carbon dioxide (component B) is to be rejected such as to the atmosphere or for recycle to the fuel cell cathode in the case of molten carbonate fuel cells, by purging with cathode exhaust oxygen-depleted air (as component C).



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HYDROGEN RECYCLE FOR HIGH TEMPERATURE FUEL CELLS

FIELD

This application is related to adsorptive gas separation, and in particular rotary pressure
5 swing adsorption (PSA), as well as fuel cell applications, and QuestAir Technologies' related
patent applications, including Nos. 09/591,275, 09/808,715, 60/323,169, and 60/351,798, the
disclosures of which are incorporated herein by reference.

The present disclosure relates to high temperature fuel cell systems, such as solid oxide
fuel cell (SOFC) and molten carbonate fuel cell (MCFC) systems exploiting gas separation
10 devices in which a first gas mixture comprising components A (e.g. hydrogen) and B (e.g.
carbon dioxide) is to be separated so that a first product of the separation is enriched in component
A, while component B is mixed with a third gas component C (e.g. air, oxygen-enriched air or
oxygen-depleted air) contained in a displacement purge stream to form a second gas mixture
including components B and C, and with provision to prevent cross contamination of
15 component C into the first product containing component A, or of component A into the second
gas mixture containing component C. The invention may be applied to hydrogen (as exemplary
gas component A) enrichment from high temperature fuel cell anode exhaust gas, where dilute
carbon dioxide (as exemplary gas component B) is to be rejected to the atmosphere by purging
with cathode exhaust oxygen-depleted air (as exemplary gas component C) for example in
20 SOFC embodiments or to be transferred to the cathode oxidant feed gas by purging with feed
air or oxygen-enriched air (as another exemplary gas component C) in MCFC embodiments.

BACKGROUND

Fuel cells provide an environmentally friendly source of electrical current. One
25 type of high temperature fuel cell used for generating electrical power, particularly envisaged
for larger scale stationary power generation, is the molten carbonate fuel cell (MCFC). The

MCFC typically includes an anode channel for receiving a flow of hydrogen gas (or a fuel gas which may react in the anode channel to generate hydrogen such as by steam reforming and water gas shift reactions), a cathode channel for receiving a flow of oxygen gas, and a porous matrix containing a molten carbonate electrolyte which separates the anode channel from the cathode channel. Oxygen and carbon dioxide in the cathode channel react to form carbonate ions, which cross the electrolyte to react with hydrogen in the anode channel to generate a flow of electrons. As the hydrogen is consumed, carbon monoxide is shifted by steam to generate additional hydrogen. Carbon dioxide and water vapor are produced in the anode channel by oxidation of fuel components, and by reduction of carbonate ions from the electrolyte. A typical operating temperature of molten carbonate fuel cells is about 650°C.

Another type of high temperature fuel cell is the solid oxide fuel cell (SOFC). The SOFC typically includes an anode channel for receiving a flow of hydrogen gas (or a fuel gas which reacts in the anode channel to generate hydrogen by steam reforming and water gas shift reactions), a cathode channel for receiving a flow of oxygen gas, and a solid electrolyte which is a ceramic membrane conductive to oxygen ions and separates the anode channel from the cathode channel. Oxygen in the cathode channel dissociates to oxygen ions, which cross the electrolyte to react with hydrogen in the anode channel to generate a flow of electrons. As the hydrogen is consumed, carbon monoxide may be oxidized directly or may be shifted by steam to generate additional hydrogen. Carbon dioxide and water vapor are produced in the anode channel by oxidation of fuel components. Typical operating temperatures of solid oxide fuel cells range between about 500° to about 1000°C.

Except in the rare instance that hydrogen (e.g. recovered from refinery or chemical process off-gases, or else generated from renewable energy by electrolysis of water) is directly available as fuel, hydrogen must be generated from fossil fuels by an appropriate fuel processing system. For stationary power generation, it is preferred to generate hydrogen from natural gas by steam reforming or partial oxidation to produce "syngas" comprising a mixture of

hydrogen, carbon monoxide, carbon dioxide, steam and some unreacted methane. As hydrogen is consumed in the fuel cell anode channel, much of the carbon monoxide reacts with steam by water gas shift to generate more hydrogen and more carbon dioxide. Other carbonaceous feedstocks (e.g. heavier hydrocarbons, coal, or biomass) may also be reacted with oxygen and steam to generate syngas by partial oxidation, gasification or autothermal reforming. The fuel cell may also be operated on hydrogen or syngas that has been generated externally.

A great advantage of MCFC and SOFC systems is that their high operating temperature facilitates close thermal integration between the fuel cell and the fuel processing system. The high temperature also allows the elimination of noble metal catalysts required by lower temperature fuel cells.

Prior art MCFC systems have limitations associated with their high temperature operation, and with their inherent need to supply carbon dioxide to the cathode while removing it from the anode. Prior art SOFC systems face even more challenging temperature regimes, and are disadvantaged by the degradation of cell voltages at very high temperatures under conventional operating conditions.

The lower heat of combustion of a fuel usefully defines the energy (enthalpy change of the reaction) that may be generated by oxidizing that fuel. The electrochemical energy that can be generated by an ideal fuel cell is however the free energy change of the reaction, which is smaller than the enthalpy change. The difference between the enthalpy change and the free energy change is the product of the entropy change of the reaction multiplied by the absolute temperature. This difference widens at higher temperatures, so higher temperature fuel cells inherently convert a lower fraction of the fuel energy to electrical power at high efficiency, while a larger fraction of the fuel energy is available only as heat which must be converted to electrical power by a thermodynamic bottoming cycle (e.g. steam or gas turbine plant) at lower efficiency.

Accumulation of reforming reaction products (carbon dioxide and steam) on the fuel cell anode opposes the electrochemical reaction, so that the free energy is reduced. Higher partial pressure of oxygen and carbon dioxide over the cathode, and higher partial pressure of hydrogen over the anode, drive the reaction forward so that the free energy is increased.

5 Unfortunately, the reaction depletes the oxygen and carbon dioxide in the cathode channel and depletes hydrogen in the anode channel while rapidly increasing the backpressure of carbon dioxide in the anode channel. Hence the free energy change is reduced, directly reducing the cell voltage of the fuel stack. This degrades the electrical efficiency of the system, while increasing the heat that must be converted at already lower efficiency by the thermal bottoming

10 cycle.

The free energy change is simply the product of the electromotive force (“ E ”) of the cell and the charge transferred per mole by the reaction (“ $2F$ ”), where the factor of two reflects the valency of the carbonate ion. The following Nernst relation for a MCFC expresses the above described sensitivity of the electromotive force to the partial pressures of the electrochemical

15 reactants in the anode and cathode channels, where the standard electromotive force (“ E_o ”) is referred to all components at standard conditions and with water as vapor.

$$E = E_o - \frac{RT}{2F} \ln \left[\frac{P_{H_2O(anode)} \cdot P_{CO_2(anode)}}{P_{H_2(anode)} \cdot P_{O_2(cathode)}^{0.5} \cdot P_{CO_2(cathode)}} \right]$$

20 Prior art MCFC systems do not provide any satisfactory solution for this problem which compromises attainable overall efficiency. Despite repeated attempts to devise an effective technology and method to maximize reactant concentrations, and minimize product accumulation in both the anode and cathode circuits that would be compatible with MCFC operating conditions, no such attempt has been adequately successful.

The accepted method for supplying carbon dioxide to the MCFC cathode has been to burn a fraction of the anode exhaust gas (including unreacted hydrogen and other fuel components) to provide carbon dioxide mixed with steam and nitrogen to be mixed with additional air providing oxygen to the cathode. This approach has limitations. Even more of
 5 the original fuel value is unavailable for relatively efficient electrochemical power generation, in view of additional combustion whose heat can only be absorbed usefully by the thermal bottoming cycle. Also, the oxygen/nitrogen ratio of the cathode gas is even more dilute than ambient air, further reducing cell voltage and hence transferring more power generation load less efficiently onto the thermal bottoming plant.

10 The following Nernst relation for a SOFC expresses the sensitivity of the electromotive force to the partial pressures of the electrochemical reactants in the anode and cathode channels, with the simplifying assumption that CO is converted by the water gas shift reaction. This sensitivity is of course greatest at the highest working temperatures of SOFC.

15

$$E = E_o - \frac{RT}{2F} \ln \left[\frac{P_{H_2O(anode)}}{P_{H_2(anode)} \cdot P_{O_2(cathode)}^{0.5}} \right]$$

Adsorption gas separation systems have been considered in the prior art for manipulating partial pressures of reactants in the fuel cell, so as to achieve higher fuel cell voltage E.

According to prior known adsorptive processes, for enriching a component A of a feed
 20 gas mixture containing components A and B, an adsorbent material over which component B is more readily adsorbed and component A is less readily adsorbed may be provided. The adsorbent material contacts flow channels in adsorbers or adsorbent beds. When the gas mixture is introduced at a feed pressure and temperature to a first end of the adsorber during a feed step of the process, component B is preferentially adsorbed and a first product enriched in
 25 component A may be delivered from the second end of the adsorber as it becomes loaded with

component B. The adsorber may then be regenerated to desorb component B in reverse flow so that the process may be repeated cyclically.

Regeneration of adsorbent materials may be achieved by alternative strategies including pressure swing, displacement purge, thermal swing, or combinations thereof, according to the prior art. It has also been claimed that regeneration of a carbon adsorbent loaded with carbon dioxide may be achieved by applying an electric current in so-called electric swing adsorption.

In existing pressure swing adsorption (PSA) systems or vacuum pressure swing adsorption systems (VPSA), the total pressure of the gas contacting the adsorber is reduced (pressure swing) following the feed step, thus reducing the partial pressure of component B contacting the adsorbent, and desorbing component B to be exhausted by purging with a reflux fraction of already enriched component A. The total pressure of the gas mixture in the adsorber is elevated while the gas flow in the adsorber is directed from the first end to the second end thereof, while the total pressure is reduced in the regeneration step while the gas flow in the adsorber is directed from the second end back to the first end. As a result, a "light" product (a gas fraction depleted in the more readily adsorbed component and enriched in the less readily adsorbed component A) is delivered from the second end of the adsorber, and a "heavy" product (a gas fraction enriched in the more strongly adsorbed component B) is exhausted from the first end of the adsorber.

Alternatively, the total pressure may be kept approximately constant in the regeneration step, while component B is desorbed by a third preferably less readily adsorbed component C, which was not part of the feed gas mixture, with component C introduced in reverse flow from the second end back to the first end of the adsorbers (displacement purge), thus reducing the partial pressure of component B contacting the adsorbent, and exhausting displaced component B from the first end of the adsorbers. As a result, a first or "light" product (a gas fraction depleted in the more readily adsorbed component B and enriched in the less readily adsorbed component A) is delivered from the second end of the adsorber, and a "heavy" product (a gas

mixture including the more strongly adsorbed component B and the displacement component C) is exhausted from the first end of the adsorber.

Regeneration may also be achieved by cyclically raising the temperature (temperature swing) of the adsorbent so as to reduce the adsorptive affinity for all gas species, resulting in
5 desorption of component B which can then be purged in reverse flow by a purge stream either as a reflux of previously enriched component A or by displacement purge with a component C. Thermal swing adsorption (TSA) requires bulk heating and cooling of the adsorbent on a cyclic basis, so is limited to relatively low cycle frequencies. The heating step may be achieved by heating the purge stream before admission to the second end of the adsorbers.

10 According to the prior art, pressure swing and displacement purge may be combined, so that a displacement purge regeneration step is achieved at a lower total pressure than the feed pressure. When relatively low cycle frequency necessary for operation of thermal swing adsorption processes may be acceptable, thermal swing may be combined with pressure swing and/or displacement purge regeneration strategies. The distinction of displacement purge
15 processes in the present context is that the displacement purge stream is externally provided and includes a component C that is not contained in the feed gas mixture to be separated, unlike conventional PSA or TSA processes where the purge stream is obtained internally as a fraction of the feed gas mixture undergoing separation.

Previously, application of displacement purge processes has been limited by
20 compatibility of components A, B and C. Even within the context of an overall separation being achieved, some intimate mixing will take place due to axial dispersion in the adsorbers, fluid holdup in gas cavities, and leakage across fluid seals and valves. While components B and C must obviously be compatible as they will be mixed as an intended outcome of the process, cross-contamination between components B and C would also take place so as to require
25 compatibility of those components as well.

PSA is widely applied in hydrogen purification (e.g. from syngas generated by steam reforming or gasification of a hydrocarbon feedstock, after water gas shifting to minimize carbon monoxide concentration), with components A and B representing carbon dioxide and hydrogen. In that application, displacement purge using air (or any oxygen-containing gas with
5 oxygen appearing as a component C) would in the prior art have been impracticable owing to unacceptable hazards of cross-contamination between hydrogen and oxygen.

SUMMARY OF THE DISCLOSURE

10 The present disclosure addresses some of the limitations of the prior art in the application of gas separation systems to high temperature fuel cell systems.

In an embodiment of the present disclosure, a high temperature fuel cell electrical generation system is provided that is adapted to enable selective generation of electrical power, and/or hydrogen fuel, and/or useable heat, allowing flexible operation of the generation system
15 wherein the generation system may additionally incorporate means for mitigation of "greenhouse" gas and other environmentally deleterious gas emissions, and for enhancing overall efficiency of operation to increase sustainability of fuel resource use. In such an embodiment, the high temperature fuel cell may be either a MCFC or a SOFC.

According to a first embodiment of the disclosed systems and processes, there is
20 provided an electrical current generating system that includes at least one fuel cell operating at a temperature of at least about 250°C, a hydrogen gas separation system and/or oxygen gas delivery system that includes at least one device selected from a compressor or vacuum pump, and a drive system for the device that includes means for recovering energy from at least one of the hydrogen gas separation system, oxygen gas delivery system, or heat of the fuel cell.
25 According to a second embodiment of an electrical current generating system according to the present disclosure, that also includes a high temperature fuel cell, a gas turbine system may be

coupled to the hydrogen gas separation system or oxygen gas delivery system, wherein the gas turbine system may be powered by energy recovered from at least one of the hydrogen gas separation system, oxygen gas delivery system, or heat of the fuel cell. The hydrogen gas separation system or the oxygen gas delivery system may include an adsorption module, such as
5 a pressure swing adsorption module. These generating systems are particularly useful for use in conjunction with molten carbonate fuel cells and solid oxide fuel cells.

The present disclosure is concerned with gas separation for application within a high temperature fuel cell system, and more particularly with adsorptive separation of a first gas mixture containing less readily adsorbed first component (or fraction) A and more readily
10 adsorbed second component (or fraction) B, with adsorber regeneration achieved by displacement purge, preferably in combination with pressure swing or thermal swing regeneration techniques. The displacement purge stream includes a preferably less readily adsorbed third component (or fraction) C which may be mixed with component B in the regeneration step. A particular requirement for safe use of a gas separation system for use in a
15 high temperature fuel cell system is to provide means to avoid or strictly minimise any mixing between components A and C in externally delivered or discharged gas streams. This requirement arises in fuel cell and other applications where components A and C may be mutually chemically reactive, as when component A is a combustible fuel and component C is an oxidant.

20 Thus, a first gas mixture including components A and B is be separated so that a first product of the separation is enriched in component A, while component B is mixed with a third gas component C contained in a displacement purge stream to form a second gas mixture including components A and B, and with provision to prevent cross contamination of component C into the first product containing component A, or of component A into the second
25 gas mixture containing component C. It is desirable that such cross contamination be avoided

or at least strictly minimised for safety or other reasons. Component C may be a major or minor constituent of the purge gas stream.

An exemplary apparatus embodiment according to the present disclosure includes a co-operating set of N adsorbers, each adsorber having a flow path between first and second ends of the adsorber, and a flow path contacting an adsorbent material within the adsorber, with
5 component B being more readily adsorbed relative to components A and C which are less readily adsorbed by the adsorbent material. The adsorbers may be subjected to a cyclic adsorption process with process steps as set forth below, with a cycle period T. Further, the N adsorbers may be arranged so as to sequentially undergo the steps of the cycle sequentially in
10 staggered phase so that the process may proceed in a substantially continuous fashion.

The process for each adsorber includes a feed step in which the first gas mixture is admitted at a first total pressure to the first end of the adsorber, while a first or "light" product gas enriched in component A is delivered from the second end of the adsorber as component B is preferentially adsorbed on the adsorbent contacting the flow channel(s) of the flow path within the adsorber.
15 The process also includes a displacement purge step in which displacement purge gas containing component C is admitted to the second end of the adsorber, while a second gas mixture (or "heavy" product gas) is delivered at a second total pressure from the first end of the adsorbers as component B desorbs from the adsorbent. The first and second pressures may be substantially similar, or the second pressure may be substantially less than the first pressure so
20 as to utilize a pressure swing in the performance of the separation process.

Immediately prior to the displacement purge step, a first "buffer" step may be performed in the presently disclosed process, in order to substantially remove interstitial and adsorbed component A accumulated in the adsorber from the previous feed step, so as to avoid contamination of the second gas mixture to be produced in the imminent displacement purge
25 step by component A. Likewise, immediately following the displacement purge step, a second "buffer" step may be performed in the inventive process, in order to substantially remove

interstitial and adsorbed component C accumulated in the adsorber from the previous feed step, so as to avoid contamination of the first product gas to be produced in the following feed step by component C.

The optional buffer steps of an aspect of the present invention may be accomplished in several ways, including applications of the displacement purge principle by introducing a buffer sweep stream, optionally assisted by reducing the total pressure relative to the pressure during the displacement purge step in the adsorber during the buffer steps. Typically, each buffer step will generate an exhaust stream, in which there may be some admixture of components A and C; and such buffer step exhaust streams may be subjected to further processing (such as combustion to eliminate any unreacted mixture of A and C) for disposal. Buffer sweep gas to achieve displacement purge in the buffer steps may be provided as any less readily adsorbed gas stream. The first buffer sweep gas for a first buffer step preferably should not contain unbound component A, and the second buffer sweep gas for a second buffer step preferably should not contain unbound component C. The first buffer sweep gas may be or may contain displacement purge gas containing component C. The second buffer sweep gas may be or may contain first gas mixture containing component A.

The buffer sweep gas for either buffer step may be selected to be an inert gas, which may be flue gas recycled from combustion of the buffer sweep gas under combustion conditions for each stream such that A is removed from sweep gas for a first buffer step, and C is removed from sweep gas for a second buffer step. For higher temperature applications, steam may be used as buffer sweep gas.

Reducing the total pressure (e.g. below the second pressure at which the displacement purge step is conducted) during the buffer steps may be desirable to assist the removal of components A or C to be purged, and also to avoid any leakage (external to the adsorbers) of components A or C between process steps preceding and following each buffer step. With reduced total pressure in a first buffer step, desorbing component B may assist the purging of

component A during that first buffer step. Hence, a minor pressure swing to reduce the total pressure during buffer steps, for example by a modest level of vacuum if the second pressure is substantially atmospheric, may be used to enhance the reliability of the buffer steps, independently of whether a larger pressure swing is applied to assist the enrichment of component A.

If the first pressure is much larger than the second pressure, the process may include additional steps as provided in well-known pressure swing adsorption processes for the depressurization of the adsorber after a feed step and before the first buffer step, and for repressurization of the adsorber after the second buffer step and before the next feed step.

Depressurization steps may include co-current and/or countercurrent blowdown steps. Repressurization steps may include backfill and feed pressurization steps. Depressurization and repressurization steps may be achieved by single or plural pressure equalization steps performed between out-of-phase adsorbers by providing fluid communication between the first or second ends of adsorbers undergoing a pressure equalization step.

In the case that pressure swing is combined with displacement purge in the present invention, it may be understood for greatest generality that any of the steps known for PSA and VPSA processes may be incorporated in the present process, which is characterised by the first and second buffer steps respectively just before and just after the displacement purge step. If desired, a purge step using light product gas or cocurrent blowdown gas as purge gas may be conducted in addition to (and before or after) the displacement purge step.

In order to perform the buffer steps with minimal losses of components A and C during those steps, it may be desirable that components A and C (and any buffer sweep component D) be weakly adsorbed, and that the number N of adsorbers be large with each adsorber thus having a small inventory of adsorbent material, so that the buffer steps may occupy only a small fraction of the cycle period T.

The apparatus of the present disclosure may include a first valve means communicating to the first end and a second valve means communicating to the second end of each adsorber, so as to perform in sequence for each adsorber the complete cycle of the feed step, any optional depressurization steps, a first optional buffer step, a displacement purge step, a second optional buffer step, and any optional repressurization steps.

Many potential directional valve configurations (e.g. as used in PSA systems) may be used; an exemplary embodiment of the present invention may include rotary distributor valves as the first and second valve means. In such an embodiment the N adsorbers may be mounted as an array in a rotor engaged in fluid sealing contact on first and second valve faces with a stator. The gas separation apparatus of the invention may then be referred to as a rotary adsorption module ("RAM").

According to a second exemplary embodiment of the present disclosure, the rotor of a rotary adsorption module in a gas separation system for use in the disclosed systems and processes may include a number of flow paths for receiving adsorbent material therein for preferentially adsorbing a first gas component in response to increasing pressure in the flow paths relative to a second gas component. The gas separation system also may include compression machinery coupled to the rotary module for facilitating gas flow through the flow paths for separating the first gas component from the second gas component. The stator may include a first stator valve surface, a second stator valve surface, and plurality of function compartments opening into the stator valve surfaces. The function compartments may include a gas feed compartment, a light reflux exit compartment and a light reflux return compartment.

In the above exemplary embodiment the rotary adsorption module may itself operate at an elevated working temperature. For example, the operating temperature of the adsorbers may range from approximately ambient temperature to an elevated temperature up to about 450°C, as may be facilitated by recuperative or regenerative heat exchange between the feed gas mixture and the displacement purge stream. The rotary adsorption module may be operated to

support a temperature gradient along the length of the flow channels, so that for example the temperature at the first end of the adsorbers is higher than the temperature at the second end of the adsorbers. As used herein, "operating temperature of the adsorbers" denotes the temperature of a gas flowing through the adsorbers and/or the temperature of the adsorber beds.

5 The systems and processes of the present disclosure may be applied to hydrogen (component A) enrichment from syngas mixtures as the first gas mixture, where dilute carbon dioxide (component B) is to be rejected such as directly to the atmosphere, and the displacement purge stream containing oxygen (component C) may be air or advantageously nitrogen-enriched air. The adsorbent material may be selected from those known in the art as
10 effective to separate carbon dioxide in the presence of significant levels of water vapor, particularly in applications where the separation is performed at elevated temperature.

For operation near ambient temperature, suitable adsorbents may include (but are not limited to) alumina gel, activated carbons, carbon molecular sieves, hydrophilic zeolites (e.g. type 13X zeolite and many other zeolites known in the art), other molecular sieves, and more
15 preferably hydrophobic zeolites (e.g. type Y zeolite or silicalite). If the displacement purge stream is itself humid, it may be necessary to use relatively hydrophobic adsorbents such as active carbons and zeolites such as Y-zeolite or silicalite. Alternatively, the adsorbent in the rotary adsorption module may be chosen to be selective at an elevated operating temperature (e.g., about 250°C to about 400°C) for carbon dioxide in preference to water vapor. Suitable
20 such adsorbents known in the art include alkali-promoted materials. Illustrative alkali-promoted materials include those containing cations of alkali metals such as Li, Na, K, Cs, Rb, and/or alkaline earth metals such as Ca, Sr, and Ba. The materials typically may be provided as the hydroxide, carbonate, bicarbonate, acetate, phosphate, nitrate or organic acid salt compound of the alkali or alkaline earth metals. Such compounds may be deposited on any suitable substrate
25 such as alumina. Examples of specific materials for elevated temperature operation may

include alumina impregnated with potassium carbonate and hydrotalcite promoted with potassium carbonate, as disclosed in the prior art.

For use in the inventive systems, the adsorbent material may be a conventional granular adsorbent, or may advantageously be an adsorbent material supported in a parallel passage monolith of high surface area, so that the process may be conducted at relatively high cycle frequency (e.g. cycle period of about 1 second to about 10 seconds) in a compact apparatus which contains only a small inventory of adsorbent and consequently of components A and C which may be mutually chemically reactive. An exemplary such supported parallel passage adsorbent material may be a formed adsorbent sheet structure, supported on a support substrate (known suitable support substrates include thin fibreglass, wire mesh, expanded metal, and carbon matrices). It may be particularly preferred that the adsorbent be supported as a formed sheet structure ("structured adsorbent") on thin metallic sheets (e.g. of a stainless steel wire mesh or expanded metal foil approximately 150 to 250 microns thick) with metallic spacers (e.g. of a similar wire mesh or foil) between the sheets so that the adsorbent laminate may additionally function as an effective flame arrestor structure to suppress any accidental reaction between mutually reactive components A and C that may occur as the result of any mechanical or structural failure of fluid sealing.

An exemplary embodiment of the presently disclosed adsorptive separation module includes the use of a parallel passage adsorbent structure with narrow spacers (and correspondingly narrow channels) relative to the adsorbent sheet thickness. Preferably, the channel voidage ratio (ratio of channel volume to the volume of the active adsorbent plus channels) may be in the approximate range of 20% to 35%, e.g. less than the typical 35% voidage volume of conventional granular adsorbent, which may not achieve adequate selectivity for CO₂ separation from humid gas in this application. It is also noted that conventional rotary adsorber technology (as used for removal of strongly adsorbed water vapour or volatile organic compounds from air) is based on adsorber wheels with monolithic parallel channel adsorbent

supports (using corrugated sheet adsorbent or honeycomb extrudates) whose channel voidage ratio may be of the order of 60% to 80%, so that such adsorbers would be ineffective for separation of relatively less strongly adsorbed gases such as CO₂.

In another application of the presently disclosed systems and processes, anode exhaust
5 gas from solid oxide fuel cells (SOFC) typically contains carbon dioxide and steam with unreacted fuel components including hydrogen and carbon monoxide. A SOFC power plant also has an available stream of nitrogen-enriched air as the cathode exhaust stream, or from a vacuum exhaust of an oxygen VPSA unit which may be used to deliver enriched oxygen to the cathode inlet for enhanced voltage efficiency and other benefits. In such a SOFC system, it is
10 desirable to improve overall efficiency by recycling hydrogen to the fuel cell anode inlet. In an embodiment of the present disclosure, after water gas shifting to convert most carbon monoxide to hydrogen (component A) and carbon dioxide (component B), and preferably after partial removal of water vapor, the SOFC anode exhaust gas may be introduced to a rotary adsorption module (as described above) as first gas mixture, while air or nitrogen-enriched air may be used
15 as displacement purge gas. If the nitrogen-enriched air as displacement purge is the exhaust from an oxygen VPSA providing enriched oxygen to the SOFC cathode, a single vacuum pump may be used to draw the second gas mixture (comprising exhaust carbon dioxide and oxygen-depleted air) from the second end of the rotary adsorption module, thus providing a pressure swing vacuum for both the oxygen VPSA and the hydrogen-enrichment rotary adsorption
20 module.

Industrial H₂ PSA is normally conducted at considerably elevated pressures (> 10 bars) to achieve simultaneous high purity and high recovery (~ 80%-85%). The feed gas mixture must be supplied at elevated pressure in order to deliver hydrogen (component A) at substantially the feed pressure, while also delivering carbon dioxide (component B) at an
25 exhaust partial pressure of approximately one bar. If the carbon dioxide is being exhausted to

the atmosphere, this represents a major loss of energy due to lost free energy of mixing as the carbon dioxide is diluted to its ambient partial pressure of about 0.00035 bars.

The presently disclosed systems and processes exploit the fact that air contains only trace quantities of carbon dioxide to use air or nitrogen-enriched air as the displacement purge stream
5 to strip carbon dioxide from a syngas stream at low pressure, and thus achieve useful hydrogen enrichment without requiring compression to elevated pressures. Free energy is thus captured from dilution of carbon dioxide which may be discharged directly into the atmosphere.

In application to advanced power generation technologies such as high temperature fuel cells, it will be appreciated that overall efficiency can be unexpectedly increased by the
10 disclosed systems and processes, which may be used to enable recycle of enriched hydrogen to the anode while diluting carbon dioxide into the atmosphere, thus capturing extra free energy beyond that normally credited to a combustion process with carbon dioxide delivered at a reference pressure of one bar. In the particular case where the high temperature fuel cell is a MCFC, the above principles of enrichment of anode exhaust gas in hydrogen using a
15 displacement purge adsorption process, for recycle to the anode inlet are directly applicable, with the further benefit that the purge desorption gas stream enriched in carbon dioxide may be recycled to the cathode inlet to desirably increase the concentration of carbon dioxide in the cathode inlet gas relative to that of air, as opposed to discharged into the atmosphere. Optionally, the purge gas stream enriched in carbon dioxide may be further treated prior to
20 supply to the cathode inlet, such as by combustion or other process.

Without the buffer steps and other features of the disclosed systems and processes to prevent cross-contamination between oxidant and fuel components including hydrogen, use of air or even nitrogen-enriched air to purge hydrogen enrichment adsorbers would not usually be contemplated in view of safety concerns.

According to an embodiment of the disclosure, there is provided an electrical current generating system that includes a high temperature fuel cell, and a H₂ enrichment rotary adsorption module coupled to the fuel cell.

Solid oxide and molten carbonate fuel cells may be designed to operate at a range of pressures, with working pressures between about 1 bar to 10 bars being common in the disclosed systems. The disclosed systems and processes particularly apply to high temperature SOFC and MCFC fuel cell power plants using a hydrocarbon fuel such as natural gas. According to an embodiment of the disclosure, before being admitted to the fuel cell anode channel inlet, the fuel may be mixed with hydrogen rich gas separated by a first rotary adsorption module from the anode exhaust gas, with the separation optionally performed after the anode exhaust gas has been subjected to post-reforming and/or water gas shift reaction steps so as to elevate the hydrogen concentration therein while oxidizing carbon monoxide to carbon dioxide.

In the important case of natural gas as the hydrocarbon fuel, the anode feed gas desirably comprises a mixture including methane and a large excess of recycled hydrogen. The excess hydrogen inhibits soot deposition by the methane cracking reaction, thus allowing safe operation with a minimum amount of steam in the anode feed gas. The amount of steam in the anode feed gas may be very low or even substantially zero if the recycle hydrogen concentration is maintained at a high level (e.g. about 85 - 90% of the anode feed gas). Benefits of minimum steam concentration in the anode feed gas include:

1. high initial ratio of H₂ to H₂O elevates the Nernst potential to improve voltage efficiency and output.
2. methane acts as a chemical sink for fuel cell reaction H₂O by steam reforming, thus helping maintain a high ratio of H₂ to H₂O along the anode channel.

3. methane conversion to CO and H₂ is delayed along the anode channel as H₂O is supplied by the fuel cell oxidation reaction, thus alleviating steep temperature gradients that would result from overly rapid endothermic steam reforming at the anode entrance.

4. low steam concentration inhibits conversion of CH₄ and CO to CO₂, thus ensuring that the steam reforming reaction within the anode channel is most highly endothermic to take up fuel cell waste heat for improved overall heat balance.

By contrast, prior art internally reforming MCFC and SOFC fuel cells typically operate with a substantial steam/carbon ratio in the anode feed gas to suppress carbon deposition, thus depressing fuel cell voltage performance. This prior art approach typically requires pre-reforming of a substantial fraction of the fuel natural gas to avoid excessive cooling at the anode entrance and steep temperature gradients, that would result from overly rapid endothermic steam reforming as the fuel enters the anode channel.

The anode exhaust gas typically contains some unreacted methane as well as a considerable fraction of carbon monoxide. The systems and processes of the present disclosure provide optionally that steam may be added to the anode exhaust gas which may then be admitted at elevated temperature to an adiabatic post-reformer, simultaneously performing the endothermic steam reforming reaction with the exothermic water gas shift reaction so that external heat exchange for the post-reformer may not be needed.

The foregoing features and advantages will become more apparent from the following detailed description of several embodiments that proceeds with reference to the accompanying figures.

BRIEF DESCRIPTION OF THE DRAWINGS

Certain embodiments are described below with reference to the following figures:

FIG. 1 shows an axial section of a rotary adsorption module.

FIGS. 2 through 4 show transverse sections of the module of FIG. 1.

FIGS. 5 through 10 show alternative buffer step purge configurations for the module of FIG. 1.

FIGS. 11 through 16 show simplified schematics of alternative SOFC power plant embodiments using the rotary adsorption module for enrichment and recycling of hydrogen
5 from the anode exhaust gas.

FIGS. 17 through 19 show simplified schematics of alternative MCFC power plant embodiments using the rotary adsorption module with supplementary thermal swing regeneration for enrichment and recycling of hydrogen from the anode exhaust gas.

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DETAILED DESCRIPTION OF SEVERAL EMBODIMENTS

FIGS. 1-4

A hydrogen-enrichment rotary adsorption module with displacement purge regeneration is described below in connection with FIGS. 1-4. As used herein, a "rotary adsorption module"
15 includes, but is not limited to, either a device wherein an array of adsorbers rotates relative to a fixed valve face or stator or a device wherein the valve face or stator rotates relative to an array of adsorbers. Illustrated embodiments have the adsorbers mounted in a rotor, with the rotor in a housing which is a stator with fixed valve faces.

FIG. 1 shows a rotary adsorption module 1, which includes a number "N" of adsorbers
20 3 or adsorber channels 3 in adsorber housing body 4. Each adsorber has a first end 5 and a second end 6, with a flow path therebetween contacting an adsorbent over which a gas component B is more readily adsorbed relative to a component A and a component C which are less readily adsorbed. The adsorbers are deployed in an axisymmetric array about axis 7 of the adsorber housing body. The housing body 4 is in relative rotary motion about axis 7 with first
25 and second functional bodies 8 and 9, being engaged across a first valve face 10 with the first functional body 8 to which a first gas mixture containing components A and B is supplied in a

first sector and from which a second gas mixture containing components B and C is withdrawn from a second sector, and across a second valve face 11 with the second functional body 9 from which a first or light product enriched in component A is withdrawn in a first sector and to which a displacement purge stream containing component C is supplied in a second sector.

5 In embodiments as particularly depicted in FIGS. 1-5, the adsorber housing 4 rotates and shall henceforth be referred to as the adsorber rotor 4, while the first and second functional bodies are stationary and together constitute a stator assembly 12 of the module. The first functional body shall henceforth be referred to as the first valve stator 8, and the second functional body shall henceforth be referred to as the second valve stator 9. In other
10 embodiments, the adsorber housing 4 may be stationary, while the first and second functional bodies are rotary distributor valve rotors.

In the embodiment shown in FIGS. 1-4, the flow path through the adsorbers is parallel to axis 7, so that the flow direction is axial, while the first and second valve faces are shown as flat annular discs normal to axis 7. However, more generally the flow direction in the adsorbers
15 may be axial or radial or a combination thereof, and the first and second valve faces may be any figure of revolution centred on axis 7, such as planar, conical, cylindrical, etc. The steps of the process and the functional compartments to be defined will be in the same angular relationship regardless of a radial or axial flow direction in the adsorbers.

FIGS. 2-4 are cross-sections of module 1 in the planes defined by arrows 12'-13', 14'-
20 15', and 16'-17'. Arrow 20 in each section shows the direction of rotation of the rotor 4.

FIG. 2 shows section 12'-13' across FIG.1, which crosses the adsorber rotor. Here, "N"=72. The adsorbers 3 are mounted between outer wall 21 and inner wall 22 of adsorber wheel 208. Each adsorber in the particular embodiment depicted comprises a rectangular flat pack 3 of adsorbent sheets 23, with spacers 24 between the sheets to define flow channels here
25 in the axial direction. Separators 25 are provided between the adsorbers to fill void space and prevent leakage between the adsorbers. The packs 3 may be radially tapered to improve the

volume packing of adsorbent. In alternative embodiments, the adsorbers may comprise multiple layers of adsorbent laminate oriented in a concentric spirally wrapped configuration, or other suitable monolithic structure, or alternatively may compose beaded or other particulate adsorbent arrangements.

- 5 As shown in FIG. 1, the adsorbers 3 may include a plurality of distinct zones between the first end 5 and the second end 6 of the flow channels, here shown as two zones respectively a first zone 26 adjacent the first end 5 and a second zone 28 adjacent the second end 6. As an alternative to distinct zones of adsorbents, the different adsorbents may be provided in layers or mixtures that include varying gradients of adsorbent concentrations along the gas flow path.
- 10 The transition from one adsorbent to another may also be a blended mixture of the two adsorbents rather than a distinct transition. A further option is to provide a mixture of the different adsorbents that may or may not be homogeneous.

 In the case of a H₂ adsorption separator operating at ambient temperature up to about 250°C, the first zone may contain an adsorbent or desiccant selected for removing very strongly
15 adsorbed components of the feed gas mixture, such as water or methanol vapor, and some carbon dioxide. The second zone may contain an adsorbent typically selected for bulk separation of carbon dioxide.

 In the case of a H₂ PSA operating at about 250°C to about 500°C, the first zone may contain an adsorbent that preferentially adsorbs CO₂ relative to water vapor as described above.
20 The second zone may contain an adsorbent (e.g., zeolite, Cu(I)-containing material, or Ag(I)-containing material) that preferentially adsorbs CO relative to water vapor. According to one version, the CO₂-selective adsorbent and the CO-selective adsorbent may be included or mixed together in a single zone rather than in two distinct zones.

 The adsorbent sheets typically comprise a reinforcement material (e.g., glass fibre,
25 metal foil or metal or carbon mesh) to which the adsorbent material is attached or impregnated. Satisfactory adsorbent sheets have been made by coating a slurry of adsorbent crystals with

binder constituents onto the reinforcement material, with successful examples including nonwoven fibreglass scrims, woven metal (wire mesh) or carbon-based fabrics, and expanded metal foils. Spacers are provided by printing or embossing the adsorbent sheet with a raised pattern, or by placing a fabricated spacer between adjacent pairs of adsorbent sheets.

- 5 Alternative satisfactory spacers have been provided as woven metal (wire mesh) screens, non-woven fibreglass scrims, and metal foils with etched flow channels in a photolithographic pattern. Adsorbers of the layered adsorbent sheet material may be formed by stacking flat or curved sheets; or by forming a spiral roll, with the flow channels between the sheets extending from the first end of the adsorber to the second end thereof; to fill the volume of the adsorber
- 10 housing of the desired shape. Examples of methods and structures with packed, spirally wound adsorbents are disclosed in commonly owned, co-pending U.S. provisional application No. 60/285,527, filed April 20, 2001, and incorporated herein by reference.

- Typical experimental sheet thicknesses have included the range of about 50-300 microns, with spacer heights in the range of 100 to 200 microns, and adsorber flow channel
- 15 length in the range of 10 cm to approximately 20 cm. Alternative dimensions and lengths have also proven successful.

In other embodiments of the invention, the adsorbers may be provided as an array of spiral rolls of adsorbent sheet and spacers as described above, with the array supported in a rotor.

- 20 Alternatively, the adsorbers may be formed by winding a single spiral roll of adsorbent sheet around the rotor hub and filling the annulus to wall 21. Spacers between adjacent adsorbent sheet layers may be formed by longitudinal spacers or corrugations, establishing axial flow channels between the sheets and extending between the first end 5 and second end 6, while the spacers or corrugations prevent flow transverse to the flow channels or between adjacent
- 25 flow channels. Consequently, each such flow channel may be isolated from neighbouring flow

channels through the adsorbent mass, and serves as a small independent adsorber. With this approach, the number N of independent adsorbers may be extremely large.

Also alternatively, the adsorbers may be provided as flow channels in a monolith, for example a honeycomb cordierite extrudate with adsorbent washcoated onto the cell walls of the honeycomb. The rotor may be formed from a single extrudate section, or from an array of such sections supported on the rotor.

In all cases, the adsorbers and rotor may be assembled with co-operating fluid sealing means so that substantially all fluid flow between the first and second ends of the adsorbers passes through the flow channels in the adsorbers, so that bypass leakage is avoided.

FIG. 3 shows the porting of rotor 4 in the first and second valve faces respectively in the planes defined by arrows 14'-15', and 16'-17'. An adsorber port 30 provides fluid communication directly from the first or second end of each adsorber to respectively the first or second valve face. Each such port 30 may be equivalently provided by a number of small ports for each adsorber.

FIG. 4 shows a typical stator valve face 100 of the first stator 8 in the first valve face 10 and in the plane defined by arrows 14'-15', similar to a valve face 101 of the second stator 9 in the second valve face 11 and in the plane defined by arrows 16'-17'. Arrow 20 indicates the direction of rotation by the adsorber rotor. In the annular valve face between circumferential seals 106 and 107, the open area of first stator valve face 100 ported to external conduits is indicated by clear angular sectors 111-116, which are separated by radial seals 118 corresponding to the first functional ports communicating directly to functional compartments identified by the same reference numerals 111-116. Sector 113 is used for the first buffer step, and sector 114 is used for the second buffer step. If pressure swing is used to augment displacement purge regeneration, a sector 115 may be provided for a pressurization step and a sector 116 may be provided for a depressurization step. Similarly, the open area of second stator valve face 101 (as shown in FIGS. 5, 7 and 9) ported to external conduits is indicated by

clear angular sectors 121-126, which are also separated by radial seals 118 corresponding to the first functional ports communicating directly to functional compartments identified by the same reference numerals 111-116. Typical radial seal 118 provides a transition for an adsorber between being open to adjacent sectors. A gradual opening may be provided by a tapering clearance channel between the slipper and the sealing face, so as to achieve gentle pressure equalization of an adsorber being opened to a new compartment. Much wider closed sectors may be provided to substantially stop flow to or from one end of the adsorbers when pressurization or depressurization steps are being performed from the other end.

Turning back to FIG. 1, in the first valve face 100 feed gas (the first gas mixture including components A and B) is supplied to first sector 111 as indicated by arrow 125, while heavy product (the second gas mixture including components B and C) is exhausted from second sector 112 as indicated by arrow 126. In the second valve face 101, the first or light product gas (enriched in component A) is delivered from first sector 211 as indicated by arrow 127, while displacement purge gas (including component C) is supplied to second sector 122 as indicated by arrow 128.

The rotor is supported by bearing 160 with shaft seal 161 on rotor drive shaft 162 in the first stator 8, which is integrally assembled with the first and second valve stators. The adsorber rotor is driven by motor 163 as an exemplary rotor drive means.

FIGS. 5 and 6

FIG. 5 shows the first and second stator valve faces 100 and 101 of an embodiment with displacement purge gas as the first buffer purge gas, and the feed or first gas mixture as the second buffer gas. In FIG. 5 and also FIGS. 7 and 9, the first and second stator valve faces are being viewed in one direction as indicated by section arrows 14'-17' so that the first stator valve face is being viewed from behind while the second valve face is being viewed from in front.

FIG. 6 shows the flow pattern through the adsorbers, in a circumferential section including the angular range of 0° to 360° about axis 7.

The first buffer purge gas is admitted by valve 180 to sector 123 in the second valve face 101, and displaces gas from sector 113 in the first valve face to burner 182 with co-
operating heat recovery means 183. The second buffer purge gas is admitted by valve 185 to
sector 114 in the first valve face 100, and displaces gas from sector 123 in the second valve face
to burner 182 with co-operating heat recovery means 183. The heat recovery means may be a
heat exchanger to preheat oxidant and fuel streams being supplied to the fuel cell, or a steam
generator, or an internal combustion engine, or a gas turbine, or a Stirling engine.

10

FIGS. 7 and 8

FIG. 7 shows the first and second stator valve faces 100 and 101 of an embodiment
with recycled flue gas as the first and second buffer purge gases, with this flue gas obtained by
combustion of the buffer purge gases so that unbound component C is removed from the first
buffer purge gas and unbound component A is removed from the second buffer purge gas. FIG.
8 shows the flow pattern through the adsorbers, in a circumferential section including the
angular range of 0° to 360° about axis 7.

The buffer gas streams are admitted to the first valve face 10, with the first buffer
stream through sector 113 and the second buffer stream through sector 114. A portion of the
first buffer stream is recirculated from sector 113' back to sector 113, after being displaced by
the initially entering displacement purge stream.

The first buffer stream is withdrawn from sector 123 by blower or vacuum pump 187,
and the second buffer stream is withdrawn from sector 124 by blower or vacuum pump 187'.
The buffer streams are passed through burner 182 with co-operating heat recovery means 183,
and then through condenser 189 to reject excess water through discharge conduit 190.
Complete or partial separation of the first and second buffer streams may be maintained through

burner 182 and condenser 189, as indicated by dashed partitions 191 and 192, so that combustion conditions on each side of partition 191 may be maintained appropriately fuel rich on the first buffer stream side in order to remove unbound component C from the first buffer purge gas, and lean on the second buffer stream side to remove unbound component A from the second buffer purge gas. Alternatively, the first and second buffer streams may be mingled through a single blower and vacuum pump 187, and through the burner and condenser, by maintaining closely stoichiometric combustion conditions in the burner so that unbound components A and C are both extinguished. The burner may be a catalytic combustor in order to achieve satisfactory and sufficiently complete combustion under all conditions.

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FIGS. 9 and 10

FIG. 9 shows the first and second stator valve faces 100 and 101 of an embodiment with combined pressure swing and displacement purge regeneration and with recycled flue gas as the first and second buffer purge gases. FIG. 10 shows the flow pattern through the adsorbers, in a circumferential section including the angular range of 0° to 360° about axis 7.

15

In the first stator valve face 100, sector 115 is used for a feed pressurization step, with feed gas mixture introduced through an orifice or pressure reduction restrictor 193, while sector 116 is used for a countercurrent blowdown step for depressurization preceding the first buffer step. In the second stator valve face 101, sector 125 provides a repressurization step by light reflux (pressure equalization) through conduit 195 and restrictor 196 with sector 126 which provides the corresponding depressurization step. Sector 125' provides another repressurization step by light reflux (pressure equalization) through conduit 195' and restrictor 196' with sector 126' which provides the corresponding depressurization step.

20

Extended closed sectors of valve face 100 are provided as wide radial seals (e.g. 197, 197') opposite the light reflux sectors 125, 125', 126 and 126' of face 101. Similarly wide radial seals (e.g. 198, 198') are provided in closed sectors of valve face 101 opposite the feed

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pressurization sector 115 and the countercurrent blowdown sector 116 of face 100. It may also be noted in FIG. 10 that the radial seals leading sectors 111, 115, 116, 125, 125', 126, and 126' have tapered clearance gaps (e.g. 199) between the rotor face and the respective seal entering those sectors, so as to provide smooth pressurization and depressurization transitions by flow throttling in the tapered clearance as each adsorber comes into registration with the corresponding sector.

If desired, a purge step using light reflux of enriched component B may be included in addition to a displacement purge step including component C.

10 FIGS. 11-16

The following embodiments illustrate application of the invention to solid oxide fuel cell power plants. SOFC stack 302 includes a solid oxide electrolyte membrane 310 interposed between anode channel 312 and cathode channel 314. The anode channel has an inlet 316 and an outlet 318 connected by anode loop including anode exhaust conduit 319 and anode return conduit 319', while the cathode channel 314 has an inlet 320 and an outlet 321. If the fuel is natural gas, it is internally reformed within the anode channel 312, while a suitable excess concentration of recycled hydrogen and preferably some steam is maintained in anode loop 319 so as to prevent carbon deposition.

A first rotary adsorption module 1 according to the invention receives water gas shifted and cooled anode exhaust gas from anode outlet 318, first recuperator 322, water gas shift reactor 324, second recuperator 326, and water removal condenser 328 as feed gas mixture in conduit 130. The water gas shift reactor would typically have an exit temperature in the range of about 200°C to about 400°C. Excess water is discharged by conduit 329. Hydrogen enriched gas as the light product of the first rotary adsorption module 1 is delivered by conduit 132 to recycle fan 330, after which the enriched hydrogen recycle stream is joined by feed

natural gas supplied to the anode loop by infeed conduit 336. The anode recycle gas is reheated in recuperators 326 and 322 before being admitted to the anode inlet 316.

Feed air is admitted by infeed conduit 340 to air feed blower 341, and thence by recuperator 342 to cathode inlet 320. Vitiated (nitrogen-enriched) cathode exhaust air is discharged from cathode outlet to optional heat hat recovery heat exchanger 344, and back
5 through recuperator 342 by conduit 346 which communicates to displacement purge inlet conduit 133 of the first rotary adsorption module. Spent displacement purge gas, including vitiated air and carbon dioxide, is discharged by conduit 131 to exhaust 350.

In FIG. 11, the buffer purge streams are supplied from the feed gas mixture and the
10 displacement purge gas as described for FIGS. 5 and 6 above. The buffer exhaust is schematically indicated by conduit 352 from module 1. The spent buffer purge gas is burned in burner 182 with heat recovery means 183, and discharged by flue conduit 355.

FIG. 12 illustrates a similar embodiment using recycled flue gas as the buffer purge gas, as described for FIGS. 7 and 8 above. The spent buffer purge gas is burned in burner 182 with
15 heat recovery means 183, excess water is removed by condenser 189 and water discharge conduit 190, and the flue gas is recycle to buffer inlet sectors in module 1 by schematically depicted return conduit 360.

FIG. 13 shows two independent alternative features, including use of a second rotary adsorption module 380 to transfer a fraction of water vapor (remaining in the anode exhaust
20 stream after the water gas shift step in reactor 324) from conduit 319 to anode return conduit 319', and use of a VPSA unit to provide enriched oxygen to the cathode and nitrogen-enriched exhaust to be used under vacuum as displacement purge gas. In this example, the buffer purge gas is provided from the feed gas mixture in conduit 130 and the displacement purge gas (which will be the oxygen vitiated exhaust of the oxygen VPSA) in conduit 133.

25 The second rotary adsorption module 380 includes an adsorber rotor 381 engaged at first and second ends with rotary valve faces 382 and 383. It uses an adsorbent with high

selectivity for water vapor relative to carbon dioxide and other anode gas constituents at the operating temperature, which may be that of the water gas shift reactor exit.

In FIG. 13, enriched oxygen is delivered from oxygen VPSA unit 400 and optionally an oxygen product compressor directly to the cathode channel inlet 321 by conduit 402 through recuperators 326 and 322. The VPSA unit includes a rotary adsorber module 404 and a light
5 reflux loop 406 to achieve high oxygen purity. The nitrogen enriched exhaust is delivered under vacuum by conduit 408 communicating to conduit 133. Motor or engine 410 drives feed blower 341 and a vacuum pump 412 which draws the nitrogen-enriched exhaust with exhaust carbon dioxide as spend displacement purge gas from conduit 131.

10 The vacuum pump discharge may be passed by discharge conduit 414 through a catalytic burner 416 (co-operating with heat recovery means 183) to remove any residual combustible components. Exhaust cathode gas is conveyed from the cathode channel exit 320 by conduit 440 to combustor 182, thus providing the buffer gas burner with enriched oxidant as well as heat recovery from the cathode channel.

15 In FIGS. 11-13, the first rotary adsorption module would operate just above ambient temperature, after condensation of excess water from the feed gas mixture. FIGS. 14-16 illustrate embodiments in which the first rotary adsorption module would operate at an elevated temperature corresponding to that of the water shift reactor exit. The adsorbent would be selected for carbon dioxide selectivity and insensitivity to water vapor. An example of a
20 suitable adsorbent is potassium promoted hydrotalcite. Carbon dioxide removal at a relatively elevated temperature will reduce the flows and heat exchange load in recuperator 326.

In FIGS. 14-16, the light product stream (enriched hydrogen) in conduit 132 is split into a first and a second recycle streams, which are recombined in ejector 500. Ejector 500 has a nozzle 501, a suction inlet 502, a mixing zone 503, and a diffuser 504. The first recycle stream
25 is conveyed directly to suction inlet 502 by conduit 510. The second recycle stream is passed through recuperator 326, condenser 328, recycle blower 330, and with feed from infeed conduit

336 back through recuperator 326 to ejector nozzle 501. It will be seen that blower 330 provides the driving energy through nozzle 501 to operate the ejector 500.

In FIG. 14, a fraction of the water condensate in conduit 329 is conveyed through recuperator 520 by conduit 522, and thence to steam generator coil 524 in the water gas shift reactor 324, and as steam to be used as the buffer purge via conduit 360. The spent buffer purge steam is carried by conduit 352 to burner 182.

In FIGS. 15 and 16, a portion of the steam from steam generator coil 524 is recycled by conduit 530 to the anode gas loop. In FIG. 15, conduit 530 conveys steam through recuperator 322 to a post-reformer reactor 540 which adiabatically converts a portion of unreacted methane and unreacted carbon monoxide in the anode exhaust gas from outlet 318. The post-reformer uses any of the known catalysts effective for steam methane reforming or high temperature water gas shift. Alternatively, conduit 530 may simply introduce the steam to the inlet of water gas shift reactor 524, without having passed through recuperator 322. This steam addition, and the consequent greater extent of water gas shift achieved, is highly desirable to maximize hydrogen recovery, to assist in water removal from the anode loop, and also to elevate the carbon dioxide concentration in conduit 130 for more effective removal. A further important advantage is the maximal removal of carbon monoxide from the anode return conduit 319', as highly desirable to reduce the risk of carbon deposition in the anode channel and to facilitate carbon-free operation with a minimal concentration of steam in the anode inlet.

FIG. 16 shows the steam from conduit 530 being supplied to a pre-reformer 550 for partially converting the feed fuel to syngas (hydrogen and carbon monoxide) as well as methanating part of that syngas, so that higher hydrocarbons are at least partially converted to methane in order to reduce the risk of soot deposition in the fuel cell anode channel. The pre-reformer also re-establishes the water gas shift equilibrium to minimize carbon monoxide after carbon dioxide removal in the first rotary adsorption module, so as to widen the margin of safety against carbon deposition. The pre-reformer will use a steam reforming catalyst that may

be selected for tolerance to feed impurities, and may operate at a relatively low temperature in the range of about 400°C to about 600°C so as to promote the methanation reaction. The pre-reformer may operate adiabatically, with at least partial heat balance between the endothermic steam reforming reaction and the exothermic methanation reaction. In the present invention, methane is a desirable component of the anode feed since it will act as a scavenger (by steam reforming) for water generated by the fuel cell reaction. Recycle hydrogen from the first rotary adsorption module may be passed through the pre-reformer with the feed fuel as shown in FIG. 16, or alternatively may be bypassed directly to the anode inlet 316 without passing through the pre-reformer.

Steam must be added to the inlet of pre-reformer 550 at a sufficient concentration for steam reforming and coking suppression in the pre-reformer.

Water vapor may be transferred across the anode loop in any of the embodiments by a second rotary adsorption module 380 (as shown in FIG. 13) operating as a desiccant humidity exchanger coupled between conduits 319 and 319'.

A heat engine may be used as the thermal bottoming system to recover waste heat available from heat recovery means 183 associated with buffer gas combustion, or waste heat from the fuel cell stack heat exchanger 344, or waste heat from the exothermic water gas shift reactor. While some waste heat will be used to preheat reactants and to overcome heat exchanger losses, there may be useful scope for a supplemental heat engine, to drive plant auxiliaries such as fans, blowers and vacuum pumps, and possibly to deliver supplemental power for export.

As hydrogen enrichment and optional oxygen enrichment features of the present invention serve to elevate the fuel cell voltage efficiency and stack power output, it may be preferred that all export power be exported by the fuel cell stack, and that the heat engine(s) therefore be used solely to drive plant auxiliaries.

Engine 410 may be a gas turbine using air as its working fluid (as in some embodiments of copending patent application "Energy Efficient Gas Separation for Fuel Cells" filed October 26, 2001, whose entire disclosure is incorporated herein), heated by indirect heat exchange with the anode and/or cathode gases and by combustion of the heavy product exhaust gas from the first PSA unit and/or by combustion of supplemental natural gas fuel.

Alternatively, the anode gas mixture may be used directly as the working fluid for a fuel cell stack heat recovery thermodynamic cycle, e.g. by a recuperative gas turbine. This is particularly attractive when an oxygen VPSA unit is used to concentrate enriched oxygen as the cathode oxidant stream. The gas turbine may then serve as engine 410 to operate the oxygen separation unit, and would preferably be applied in turbocharger configurations.

Engine 410 may be an internal combustion engine fuelled by spent buffer gas containing hydrogen and other fuel values, and/or by supplemental natural gas fuel. Alternatively, engine 410 may be any type of external combustion engine, e.g. a steam engine or a Stirling engine. Since the first rotary adsorption module generates enriched hydrogen, the heat recovery means may advantageously be a Stirling engine with hydrogen working fluid.

Figs. 17 – 19

Figs. 17 – 19 show particular MCFC embodiments of the disclosure, in which supplementary thermal swing regeneration is applied to assist in desorption of CO₂ from the adsorbent material. In each of the embodiments illustrated in these figures, air (rather than cathode exhaust gas as in the case of the above SOFC embodiments) may be used as a displacement purge gas to remove CO₂ from the rotary adsorber module, and the CO₂-laden air is advantageously recycled for use as oxidant in the molten carbonate fuel cell cathode. Somewhat oxygen-enriched air or other suitable purge gas stream may alternatively be used instead of air.

In the embodiments shown in Figs. 17, 18 and 19, a cooling coil 501 is shown in water condenser 328 for the purpose of cooling the anode exhaust stream prior to entry into rotary adsorption module 1, to enhance adsorption of CO₂ by the adsorbent material inside module 1. A suitable displacement purge gas stream such as air or somewhat oxygen-enriched air is introduced from inlet recuperator 510 by blower 515, and is preheated by the final cooling of cathode exhaust gas in recuperator 520, so as to provide preheated purge gas to assist in the desorption of CO₂ from the adsorbent material in rotary adsorption module 1. Components are identified in Figs. 17 – 19 by the same reference numerals as in preceding Figs. 11 – 16 applicable to SOFC embodiments. Water vapor may also be transferred across the anode loop in any of the MCFC embodiments of the invention by a second rotary adsorption module 380 (as shown in FIG. 18 and 19) operating as a desiccant humidity exchanger as similarly shown and described in the above SOFC embodiments.

In the above disclosed systems for both SOFC and MCFC fuel cells, the systems may optionally be modified to allow for at least a portion of the enriched H₂ product gas stream produced by the rotary adsorption module 1 to be exported from the high temperature fuel cell system for use as H₂ fuel for other applications, such as PEM fuel cells. A second gas

separation system, such as an additional displacement purge or pressure swing adsorption system may be included to further enrich the H₂ concentration of the exported H₂-containing gas stream, so as to purify the H₂ fuel for use in other applications requiring high purity H₂. Rotary displacement purge or pressure swing adsorption systems may advantageously be used for such purification purposes. Other separation systems suitable to purify the export H₂ stream may also be used, such as membrane separation systems. In the case where a pressure swing adsorption system is used as a second separation system for purification of the export H₂ stream, a feed compressor may be required to compress the export H₂ gas stream to an appropriate feed pressure for PSA separation, as is conventionally known in the PSA field.

Such H₂ export gas stream may optionally then be stored for further use as H₂ fuel, such as by a high pressure H₂ storage system. In such applications therefore, the disclosed inventive high temperature fuel cell systems may be used to selectively produce electrical current directly in the high temperature fuel cell, H₂ for export as fuel, and/or heat for additional power generation or other uses – and the relative production of these three “products” may be varied and determined by the control of the adsorptive separation system(s) and recycled gas streams used in combination with the high temperature fuel cell.

It will be evident that there may be many other alternatives and variations of the disclosed systems and processes, particularly for application to molten carbonate and solid oxide fuel cell generation systems.

For SOFC and MCFC power plants, the disclosed systems and processes may enhance power generation performance by increasing the ratio of hydrogen to steam partial pressure in the anode. Estimated efficiencies based on fuel lower heating value are in the range of about 65% to about 75% for natural gas fuelled fuel cell power plants. The presently disclosed systems and processes also facilitate cogeneration of efficiently generated electrical power, purified hydrogen, and low-grade waste heat suitable for building heating or domestic hot water utilities.

Having illustrated and described the principles of the disclosure with reference to several embodiments, it should be apparent to those of ordinary skill in the art that the specifically disclosed embodiments may be modified in arrangement and detail without departing from such principles.

What is claimed is:

1. An electrical current generation system comprising:
a high temperature fuel cell having an anode inlet and an anode exhaust outlet; and
a rotary adsorption module fluidly connected to the anode exhaust outlet and the anode inlet, and operable to receive exhaust gas from the anode exhaust outlet, to separate and enrich usable fuel gas from the exhaust gas by displacement purge adsorptive means, and to deliver at least a portion of such enriched usable fuel gas for export from the generation system as fuel for external use in a downstream system.
2. The electrical current generation system according to claim 1, additionally comprising:
a second gas separation system fluidly connected to the rotary adsorption module operable to further purify the usable fuel gas component in the exported portion of the enriched fuel gas, for external use in a downstream system.
3. The electrical current generation system according to claim 1 wherein the high temperature fuel cell is a solid oxide fuel cell.
4. The electrical current generation system according to claim 1 wherein the high temperature fuel cell is a molten carbonate fuel cell.
5. The electrical current generation system according to claim 1 wherein the rotary adsorption module is additionally operable to deliver at least a portion of the enriched usable fuel gas to the anode inlet.

6. The electrical current generation system according to claim 2 wherein the second gas separation system is a pressure swing adsorption system.
7. The electrical current generation system according to claim 6 wherein downstream system comprises a high pressure hydrogen storage system operable to store purified hydrogen fuel for dispensing to hydrogen vehicles.
8. An electrical current generation system comprising:
 - a molten carbonate fuel cell comprising an anode inlet and an anode exhaust outlet;
 - a rotary adsorption module, containing adsorbent material, fluidly connected to the anode exhaust outlet and the anode inlet, and operable to receive exhaust gas from anode exhaust outlet, to separate and enrich usable fuel gas from the exhaust gas by displacement purge adsorptive means to leave a fuel depleted waste gas stream, and to deliver at least a portion of such enriched usable fuel gas to the anode inlet; and
 - a heat exchange means operable to increase the temperature of a displacement purge gas, and to deliver such heated displacement purge gas to the displacement purge rotary adsorption module to assist desorption of the fuel depleted waste gas stream from the adsorbent material.
9. The electrical current generation system according to claim 8, wherein the molten carbonate fuel cell further comprises a cathode inlet, and the rotary adsorption module is further operable to deliver at least a portion of the fuel depleted waste gas to the cathode inlet.
10. The electrical current generation system according to claim 8 wherein the rotary adsorption module is further operable to deliver at least a portion of the enriched usable fuel gas for export from the generation system as fuel for external use in a downstream system.

11. The electrical current generation system according to claim 8 additionally comprising a second heat exchange means operable to receive anode exhaust gas from the anode exhaust gas outlet, to reduce the temperature of the anode exhaust gas and to provide the cooled anode exhaust gas to the rotary adsorption module to enhance the adsorption of the fuel depleted waste gas from the anode exhaust gas.
12. A process for generating electrical current comprising:
- providing a high temperature fuel cell having an anode inlet and an anode exhaust outlet, and a rotary adsorption module;
 - providing anode exhaust gas from the anode exhaust outlet as a feed gas mixture to the rotary adsorption module;
 - separating and enriching usable fuel gas from the anode exhaust gas by adsorptive means in the rotary adsorption module;
 - providing at least a portion of such enriched usable fuel gas for export from the generation system for use as fuel for external use in a downstream system.
13. The process according to claim 12 additionally comprising providing at least a portion of the enriched usable fuel gas for recycle to the anode inlet.
14. The process according to claim 12 wherein the high temperature fuel cell is a solid oxide fuel cell.
15. The process according to claim 12 wherein the high temperature fuel cell is a molten carbonate fuel cell.

Fig. 1

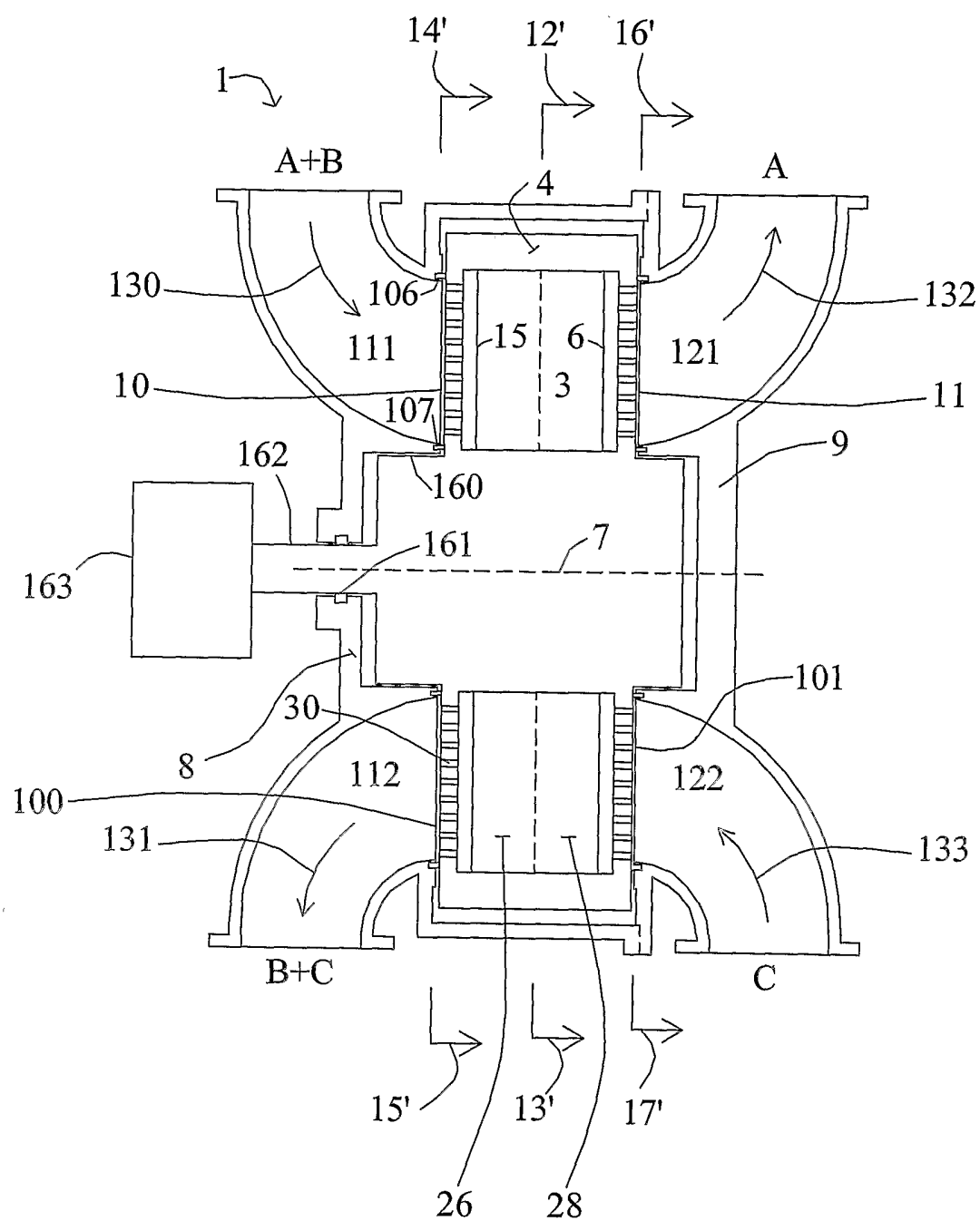


Fig. 2

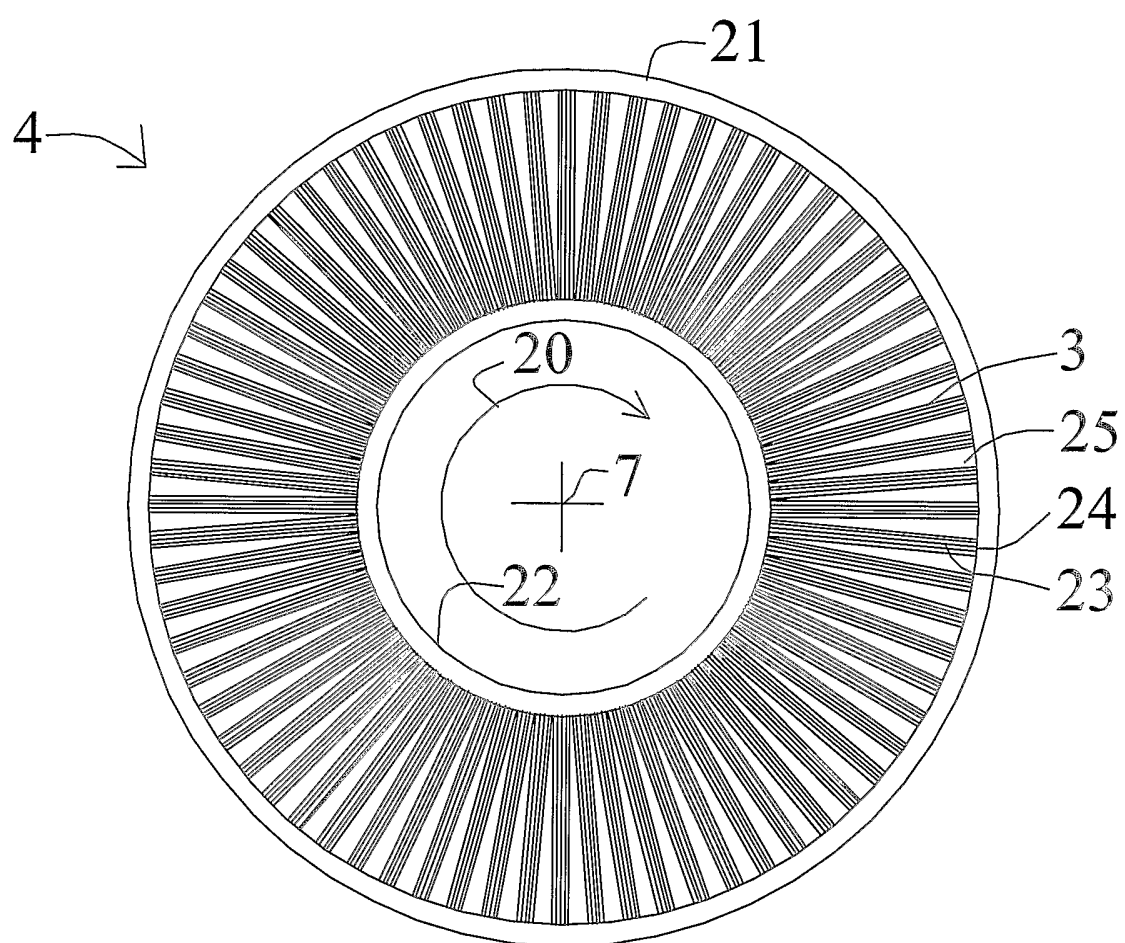


Fig. 3

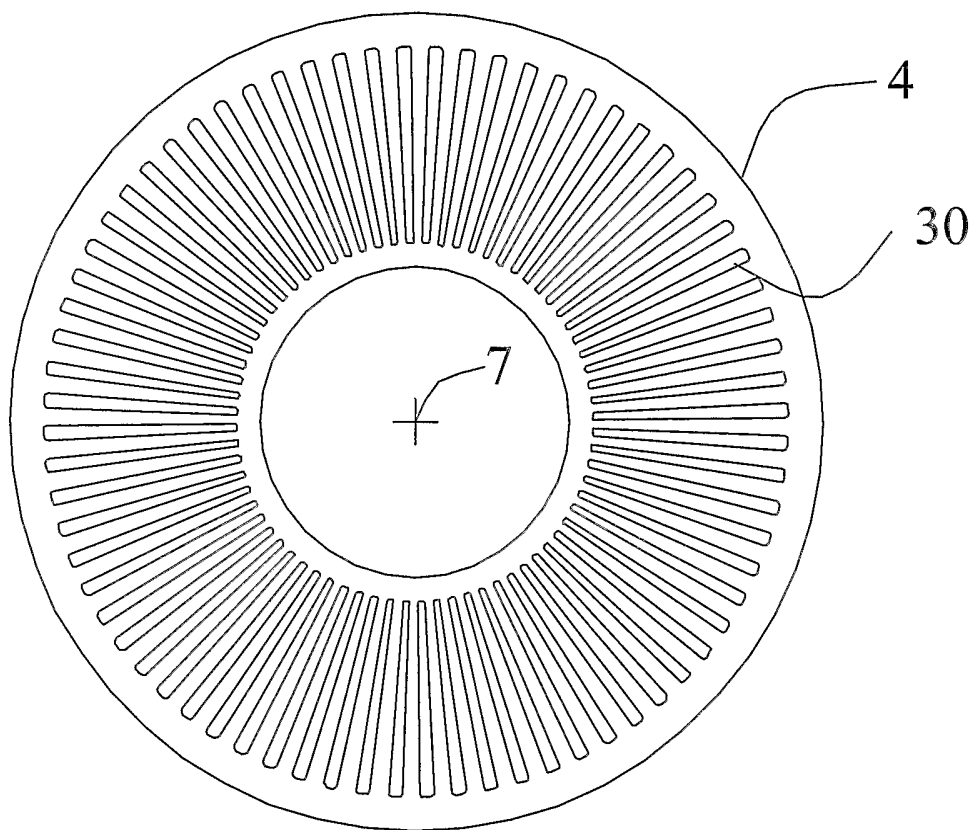


Fig. 4

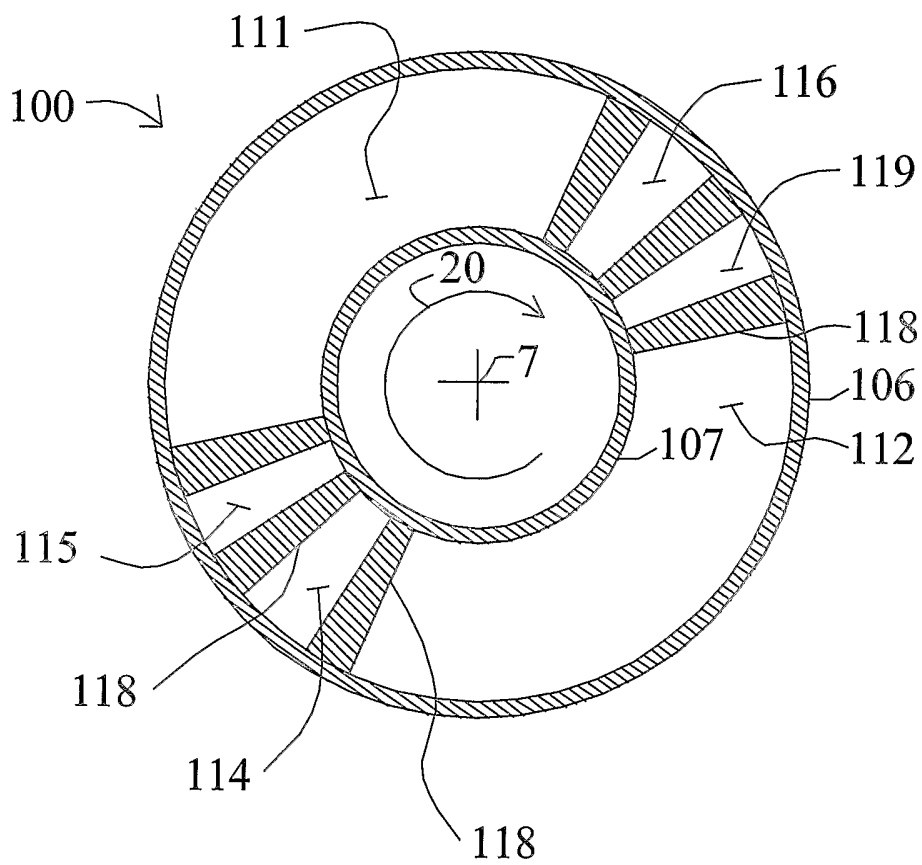


Fig. 5

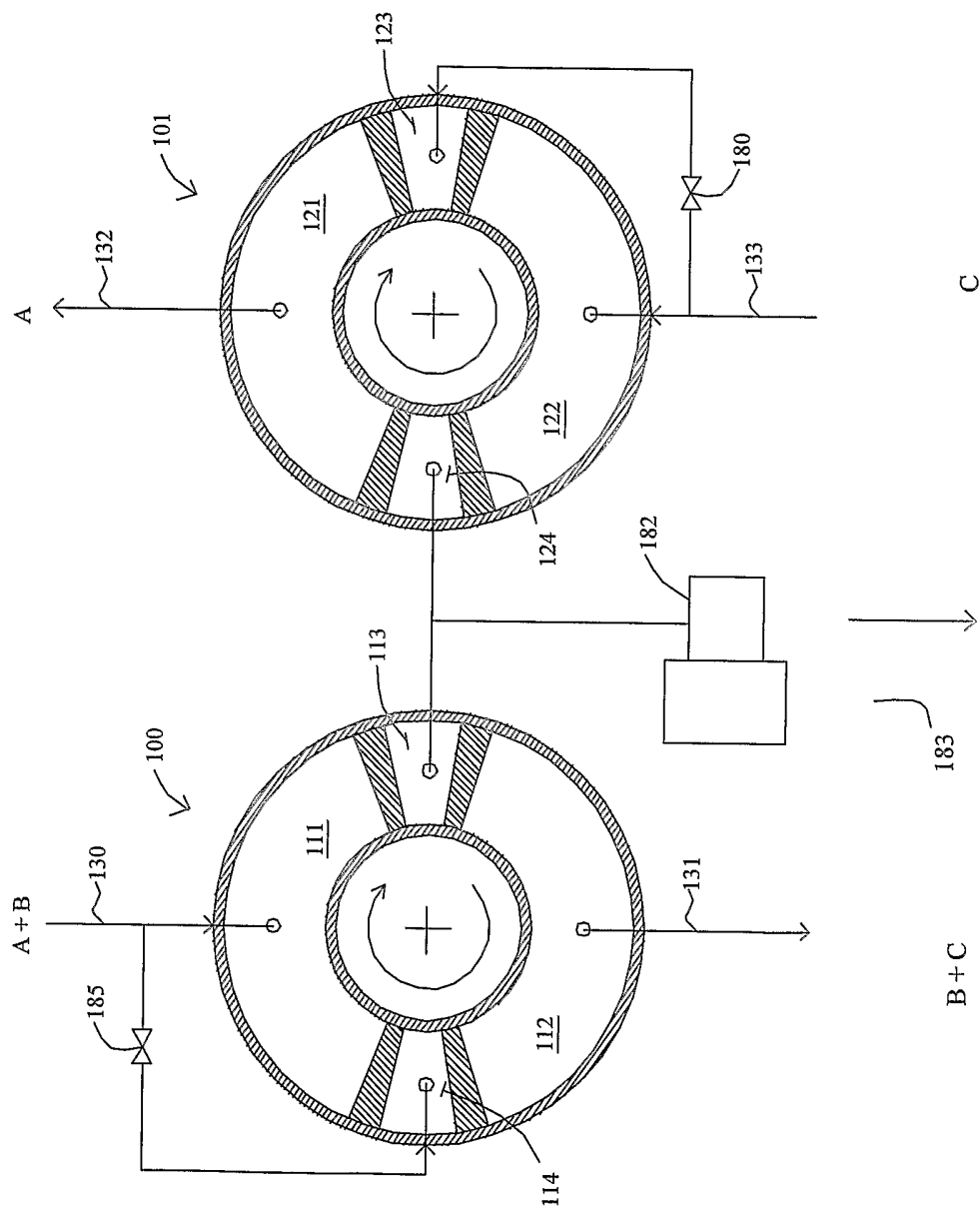


Fig. 6

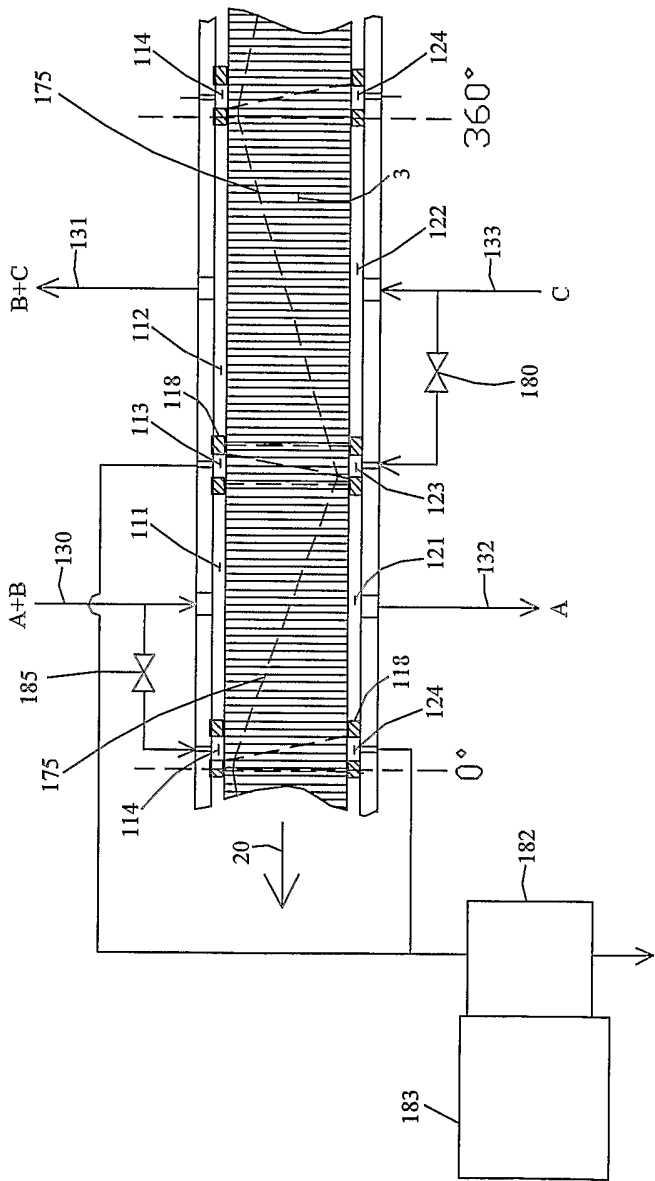


Fig. 7

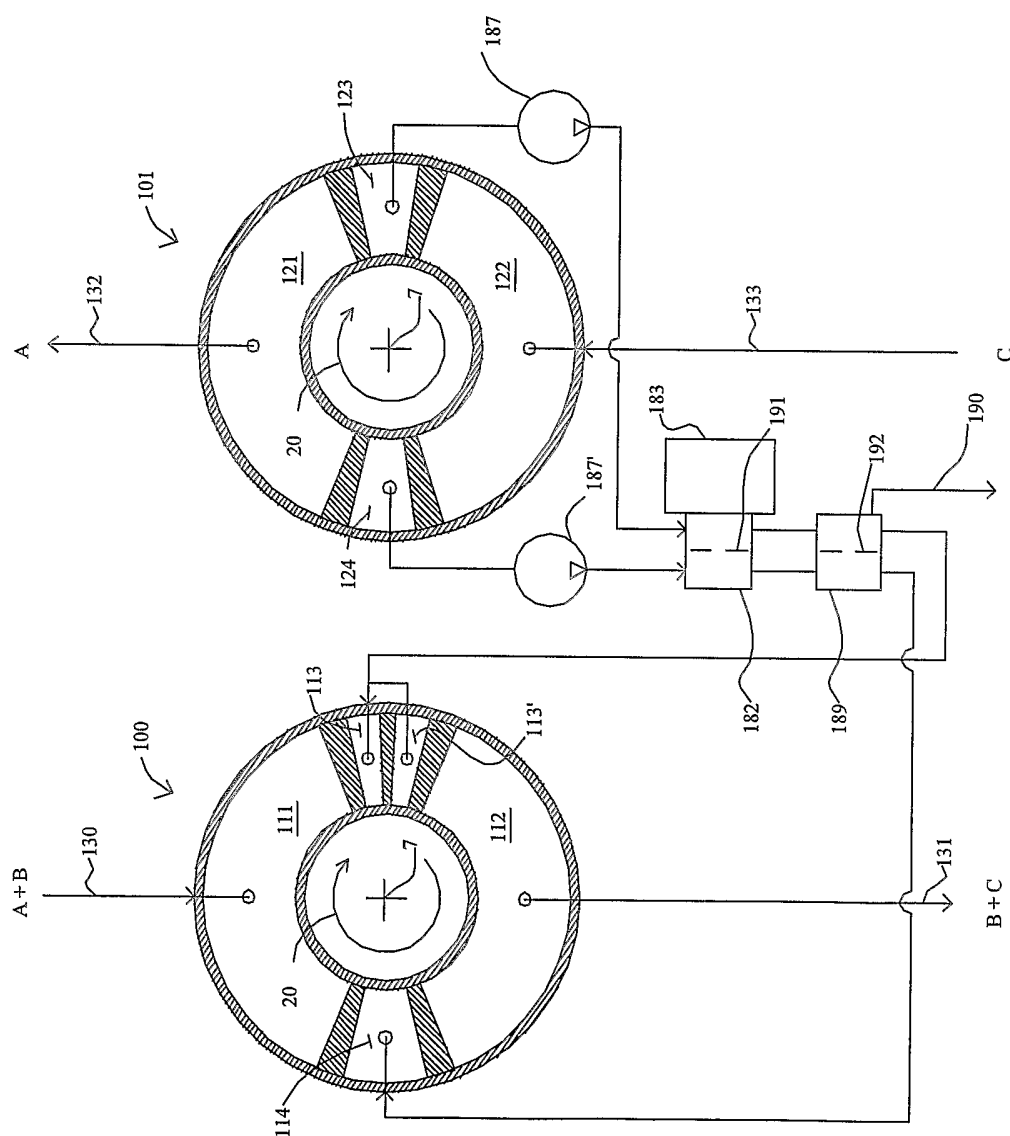


Fig. 8

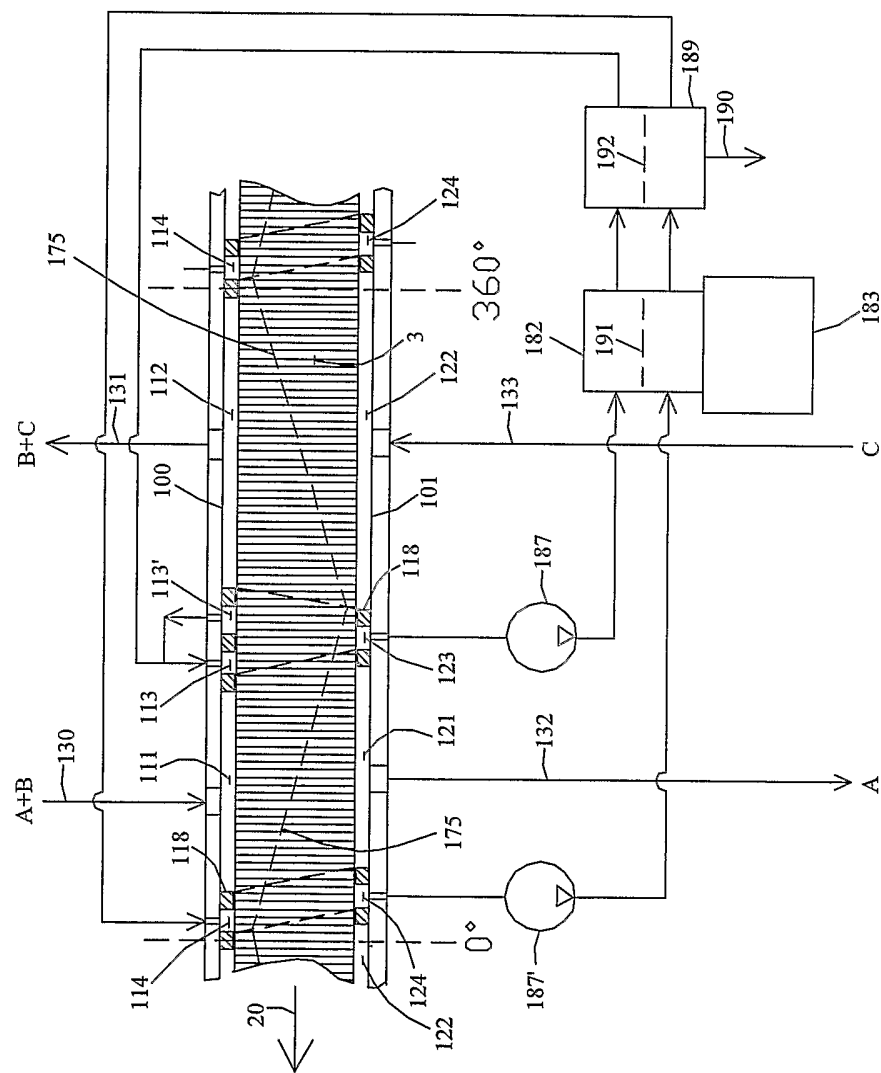


Fig. 9

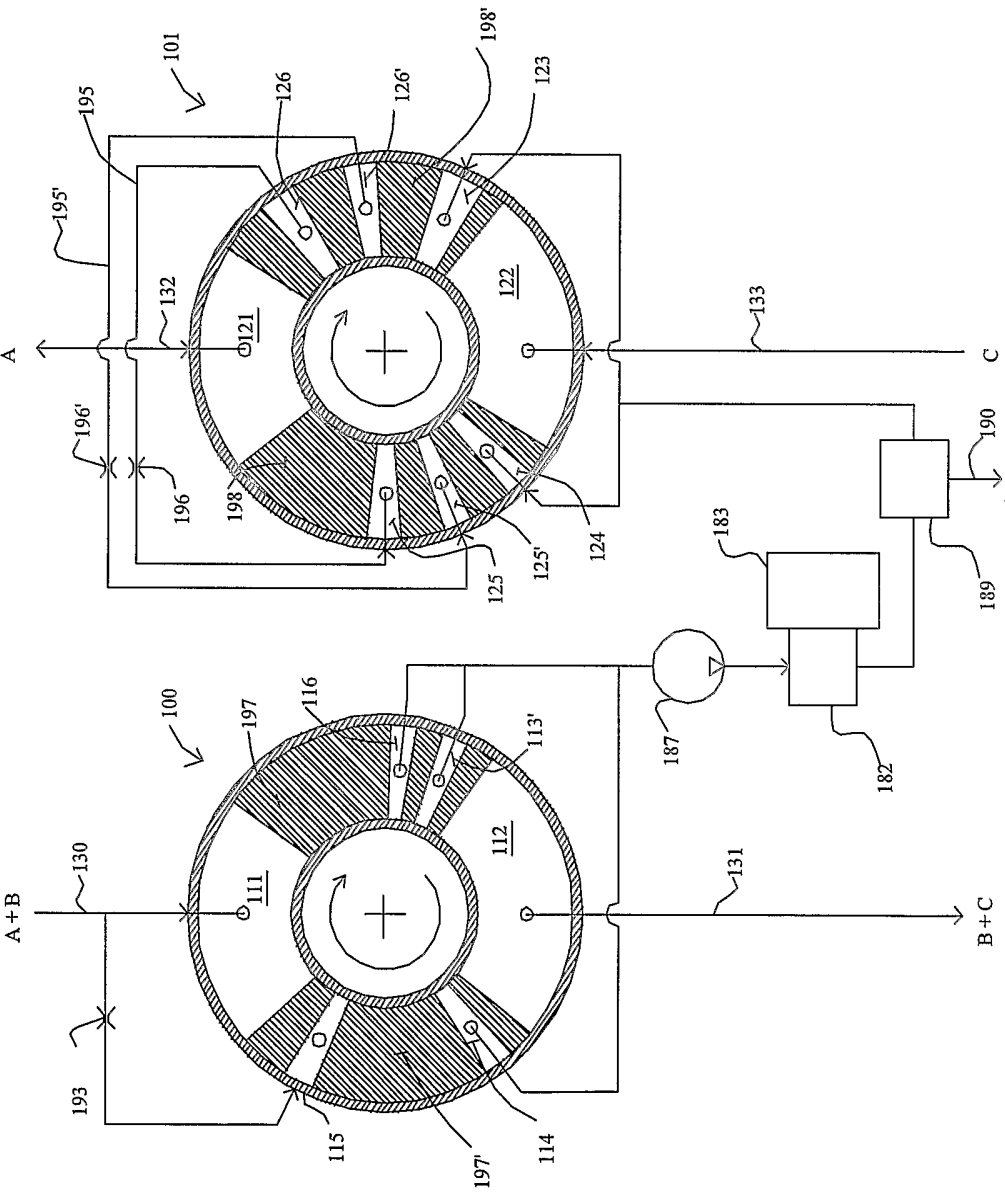


Fig. 10

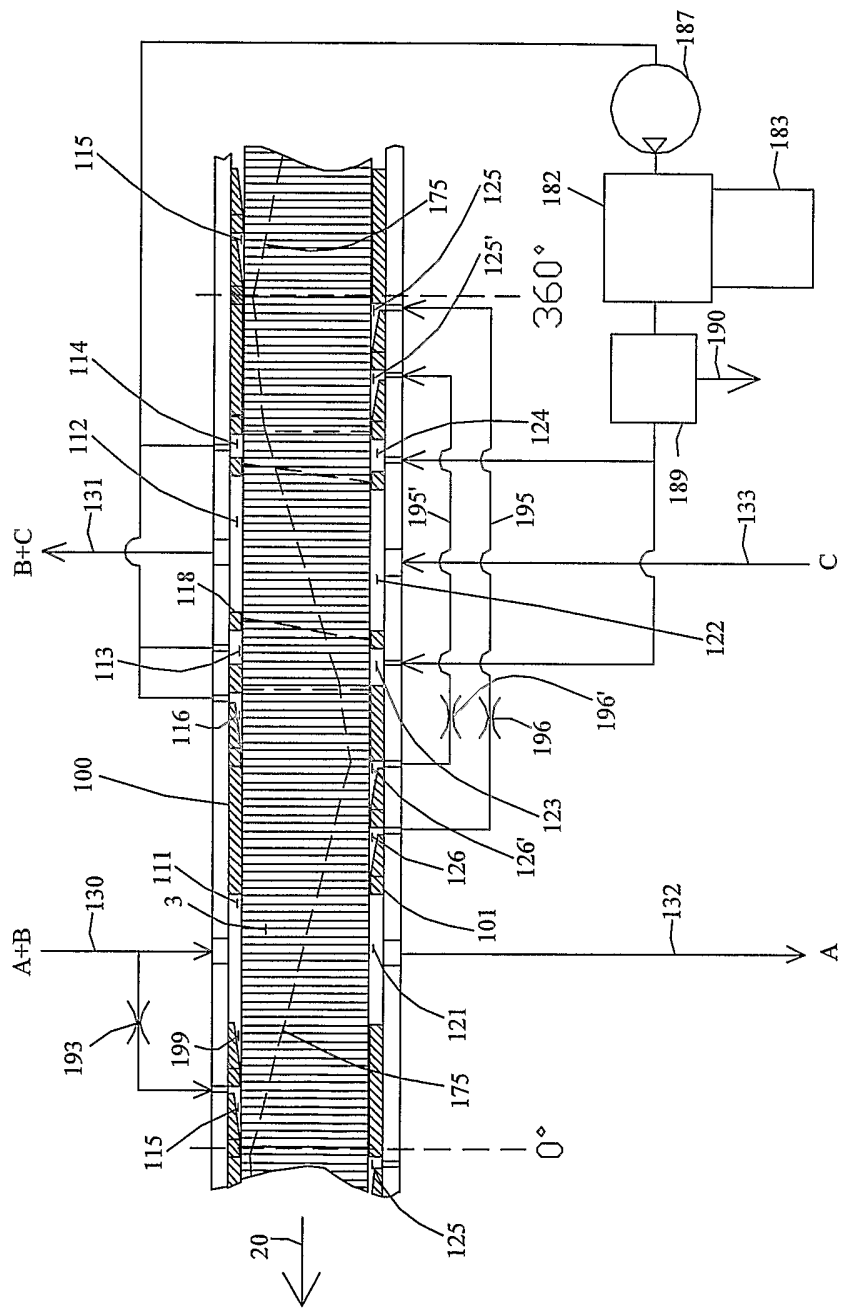


Fig. 11

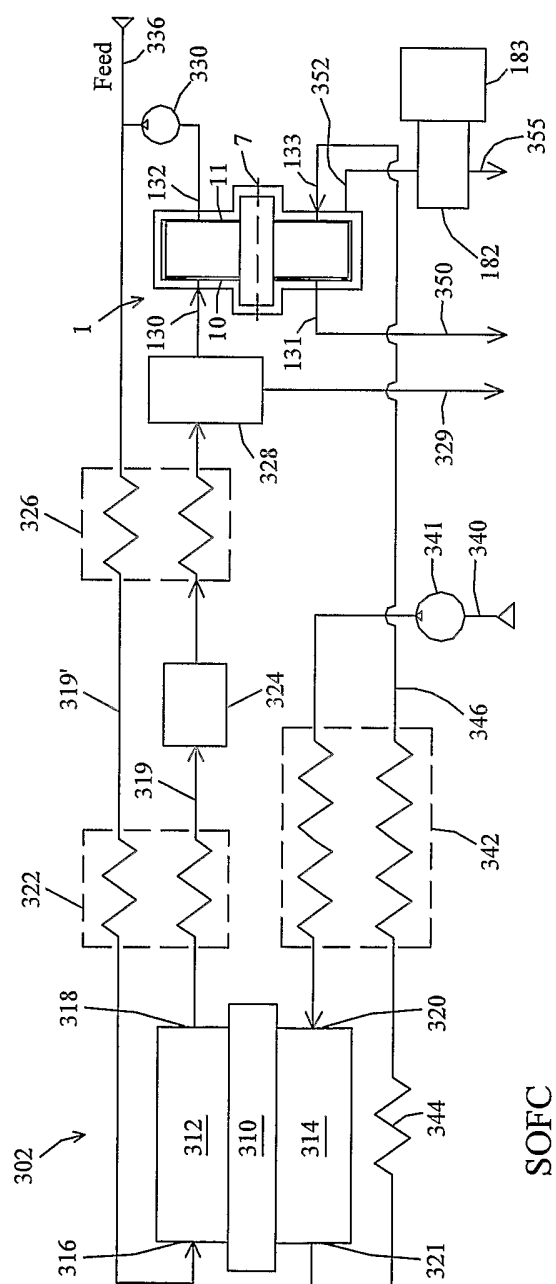


Fig. 13

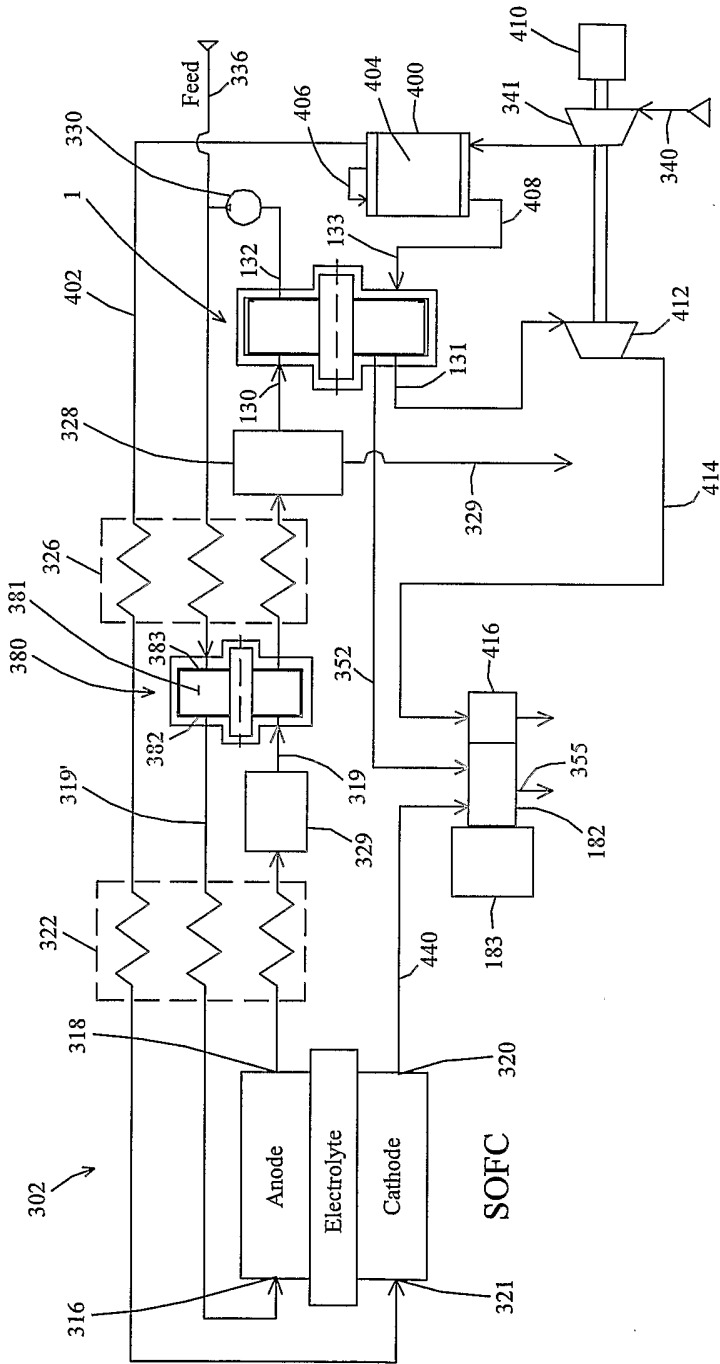


Fig. 16

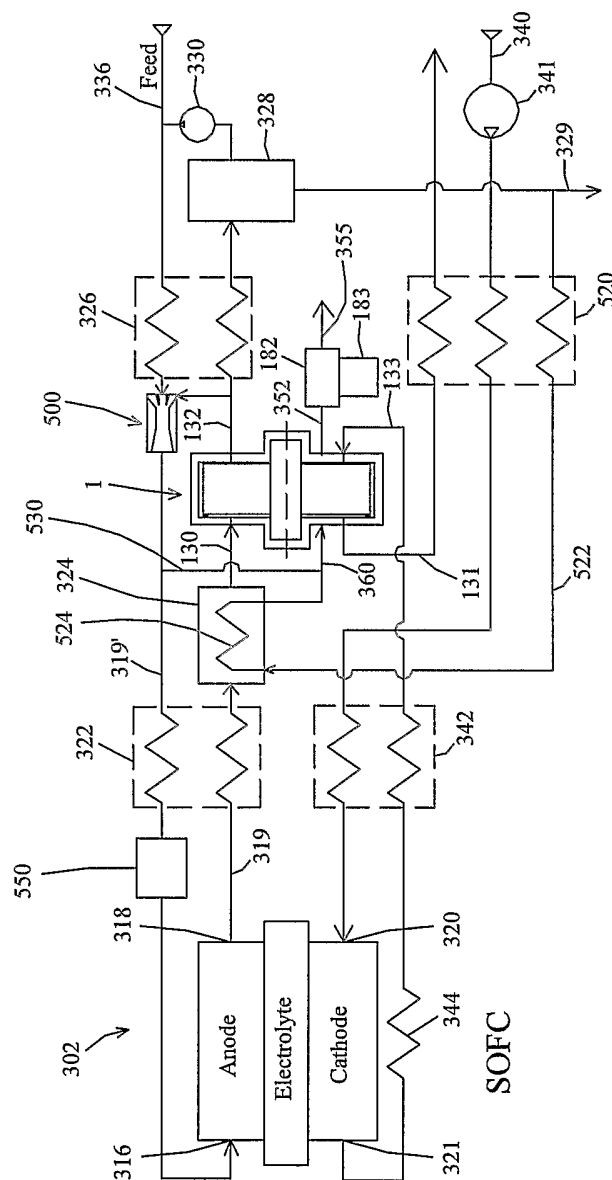


Figure 17

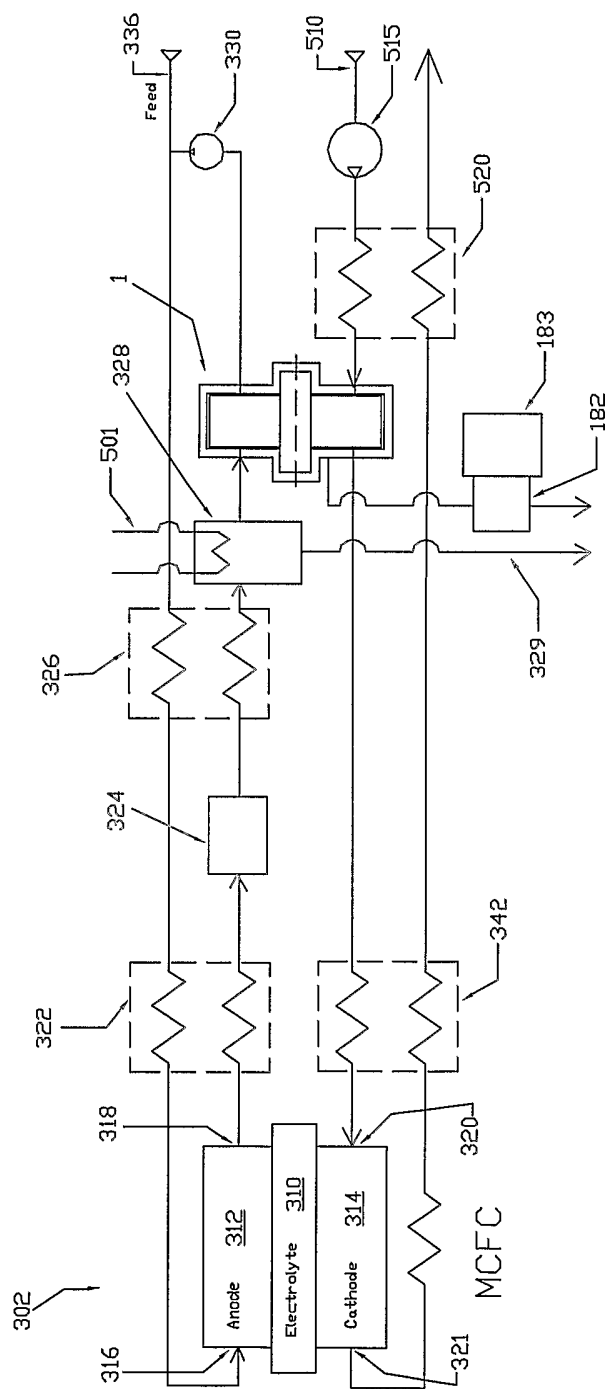


Figure 18

