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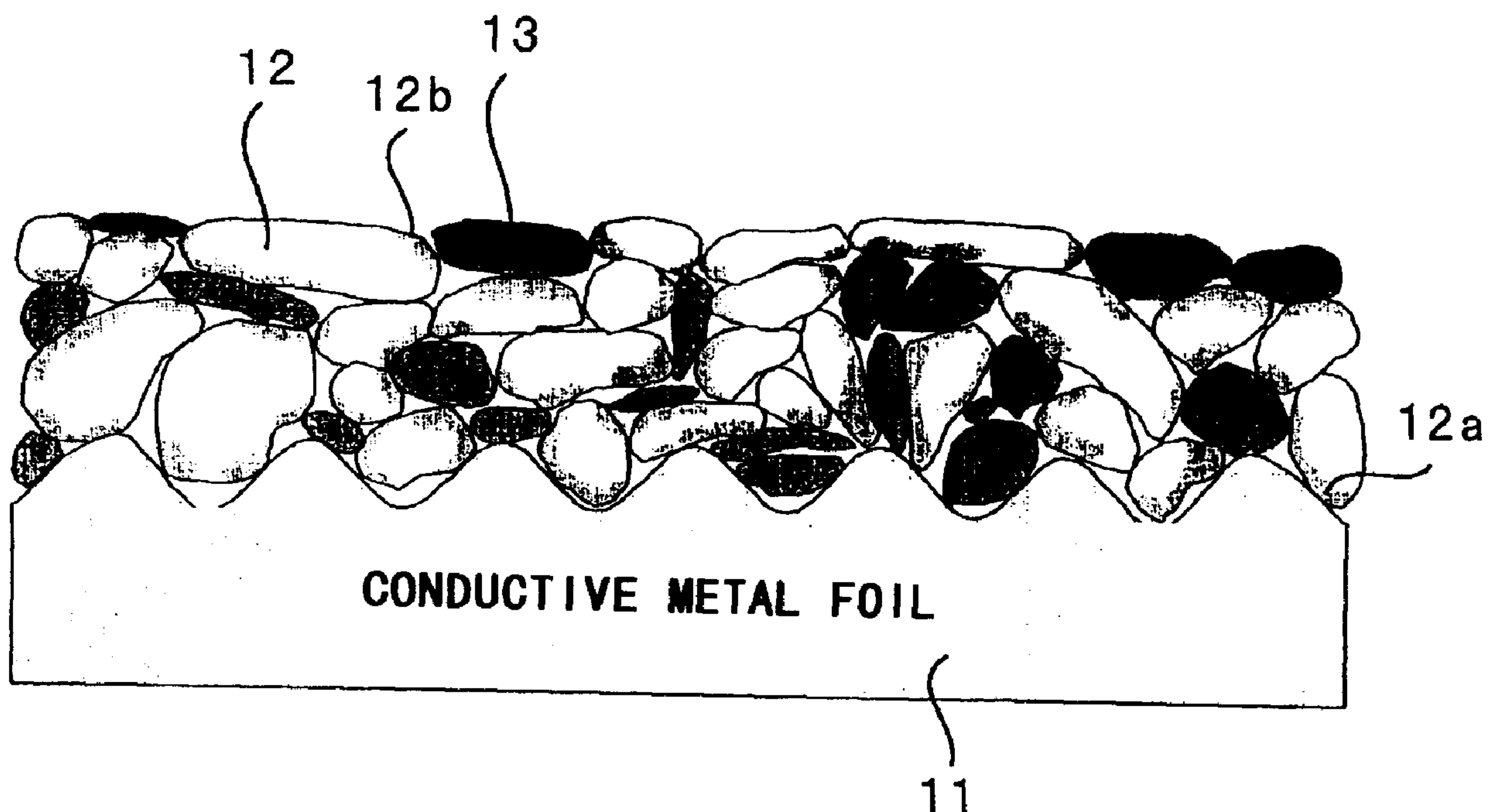
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(54) Titre : ELECTRODE NEGATIVE POUR ACCUMULATEUR AU LITHIUM ET PROCEDE DE PRODUCTION
(54) Title: NEGATIVE ELECTRODE FOR LITHIUM SECONDARY CELL AND METHOD FOR PRODUCING THE SAME



(57) Abrégé/Abstract:

A negative electrode for a lithium secondary cell, prepared by a method comprising providing a conductive metal foil having a surface roughness Ra of 0.2 μm or more as a current collector, and a mixture of active material particles containing silicon or a silicon alloy with a conductive metal powder, and sintering the mixture on the surface of the current collector; and a lithium secondary cell comprising the negative electrode.



ABSTRACT

A negative electrode for a lithium secondary cell, prepared by a method comprising providing a conductive metal foil having a surface roughness Ra of 0.2 μm or more as a current collector, and a mixture of active material particles containing silicon or a silicon alloy with a conductive metal powder, and sintering the mixture on the surface of the current collector; and a lithium secondary cell comprising the negative electrode.

**NEGATIVE ELECTRODE FOR LITHIUM SECONDARY CELL
AND METHOD FOR PRODUCING THE SAME**

5

TECHNICAL FIELD

The present invention relates to a negative electrode for a rechargeable lithium battery, a method for fabrication thereof and a rechargeable lithium battery.

10

BACKGROUND ART

The use of metallic lithium for a negative electrode enables construction of batteries which exhibit high charge-discharge capacities. However, the metallic lithium deposited on the negative electrode during charge grows into dendrites, which could cause problematic internal short-circuiting.

The use of lithium-alloying metals, such as Si, Sn and Al, as the negative active material may be expected to solve the above-described problem and achieve high charge-discharge capacities. Despite the expectation of higher capacities, the use of such alloying metals as the active material has resulted problematically in the separation or delamination of the active material from a current collector because such active materials undergo a large change in

25

volume during repetitive charge-discharge cycling and are consequently pulverized.

Japanese Patent Laying-Open No. Hei 11-339777 proposes a technique for reducing a contact resistance between a
5 current collector and active material by coating on the current collector a slurry containing silicon powder as the active material and then calcining the coating under a non-oxidizing atmosphere.

Japanese Patent Publication No. Hei 11-2948205
10 proposes using, as a negative electrode for a rechargeable lithium battery, a product prepared by coating silicon or a complex of silicon and carbon on a conductive substrate and then sintering the coating under a non-oxidizing atmosphere.

Japanese Patent Laying-Open No. Hei 2000-12089
15 proposes the use of a product prepared by sintering copper silicide, or a complex of silicon with conductive carbon or with a conductive metal, together with a conductive metal foil. Also, Japanese Patent Laying-Open No. Hei 2000-12088
20 proposes the use of a product prepared by bonding active material onto a current collector having an average roughness of 0.03 μm or larger by a binder.

However, the above-described conventional methods have resulted in the failure to obtain sufficiently good charge-discharge cycle performance characteristics and thus provide
25 practical negative electrodes for rechargeable lithium

batteries, which has been a problem.

DISCLOSURE OF THE INVENTION

It is an object of the present invention to provide
5 an electrode for a rechargeable lithium battery, which can
provide a high charge-discharge capacity and exhibit
excellent cycle performance characteristics, a method for
fabrication thereof and a rechargeable lithium battery
using the same.

10 In an aspect of the present invention, there is
provided a negative electrode for a rechargeable lithium
battery including a conductive metal foil having a surface
roughness Ra of 0.2 μm or larger used as a current
collector and a layer sinterized, under non-oxidizing
15 atmosphere, and including active material particles
containing silicon or a silicon alloy and a binder on a
surface of the current collector under such conditions that
the binder remains after a heat treatment for sintering,
wherein a metal component in the conductive metal foil is
20 diffused into the active material particles, and wherein a
detectable level of copper silicide does not exist in
regions of the active material particles where the metal
component is diffused, when analyzed by X-ray
diffractometry; and wherein the heat treatment for
25 sintering is carried out at a temperature within the range
of 400°C to 500°C.

In another aspect of the present invention, there is

provided a method for fabrication of a negative electrode for a rechargeable lithium battery, including the steps of providing a layer including active material particles containing silicon or a silicon alloy and a binder on a surface of a conductive metal foil having a surface roughness Ra of 0.2 μm or larger, and sintering, under non-oxidizing atmosphere, the layer of the active material particles and the binder while it is placed on the surface of the conductive metal foil under such conditions that the binder remains after a heat treatment, and wherein the sintering is achieved by the heat treatment at a temperature within the range of 200°C-500°C.

In a further aspect of the present invention, there is provided a negative electrode for a rechargeable lithium battery, wherein a layer of active material particles composed of silicon or a silicon alloy is provided on a current collector, the active material particles in the layer are sinter bonded to each other, and the layer of active material particles includes a binder which remains after a heat treatment for the sintering; wherein a nonlithium-alloying component is diffused from the current collector; and wherein a detectable level of an intermetallic compound between a lithium-alloying component and the nonlithium-alloying component does not exist in regions of the active material particles wherein the nonlithium-alloying component is diffused into the active material particles, when analyzed by X-ray diffractometry;

and wherein the heat treatment for sintering is carried out at a temperature within the range of 400°C to 500°C.

In yet another aspect of the present invention, there is provided a negative electrode for a rechargeable lithium battery including a conductive metal foil used as a current collector and a mixture of active material containing silicon or a silicon alloy sinterized under reducing atmosphere with conductive metal powder and a binder on a surface of the current collector under such conditions that the binder remains after a heat treatment; wherein a metal component in the conductive metal foil or the conductive metal powder is diffused into the active material; and wherein the ratio of the conductive metal powder to the active material particles is between 0.05 and 50 by weight; wherein a detectable level of an intermetallic compound between the metal component and the silicon does not exist in regions of the active material particles where the metal component is diffused, when analyzed by X-ray diffractometry; and wherein the heat treatment for sintering is carried out at a temperature within the range of 400°C to 500°C.

The invention also provides a method for fabrication of a negative electrode for a rechargeable lithium battery, including the steps of providing a mixture of active material containing silicon or a silicon alloy, conductive metal powder and a binder on a surface of a conductive metal foil, wherein the ratio by weight of the conductive metal powder to the active material particles is within

0.05 and 50, sintering, under reducing atmosphere, the mixture while it is placed on the surface of the conductive metal foil under such conditions that the binder remains after a heat treatment, and wherein sintering is achieved
5 at a temperature within 200°C and 500°C.

The matters common to the aspects of the present invention discussed above may be hereinafter referred to as those of the "present invention".

In the present invention, a conductive metal foil
10 having a surface roughness Ra of 0.2 μm or larger is preferably used as a current collector. The value of surface roughness Ra is a value determined before the metal foil is sintered. The use of such a conductive metal foil having the specified surface roughness Ra increases a
15 contact area between the mixture of active material particles with conductive metal powder and the surface of the metal foil, and accordingly allows more effective sintering under a non-oxidizing or reducing atmosphere to result in the improved adhesion of the active material
20 particles and conductive metal powder to the current collector. This suppresses large volumetric expansion or shrinkage of the active material that occurs as it stores and releases lithium during a charge-discharge reaction and also prevents separation of the active material from the
25 current collector due to pulverization. Even when the conductive metal powder was excluded and thus only the active material particles were used, the use of such a

conductive metal foil as a current collector increases a contact area between the current collector and the active material particles to result in the improved adhesion of the active material particles to the current collector.

5 The upper limit of surface roughness Ra of the conductive metal foil is not particularly specified, but may preferably fall within the range of 10 - 100 μm , as will be described below. Accordingly, the substantial upper limit of surface roughness Ra may be 10 μm or below.

10 The surface roughness Ra and an average distance S between adjacent local peaks preferably satisfy the relationship $100\text{Ra} \geq \text{S}$. The surface roughness Ra and the average distance S between local peaks are defined in Japanese Industrial Standards (JIS B 0601-1994) and can be
15 measured as by a surface roughness meter.

 In the present invention, sintering of the conductive metal powder and active material particles while in a mixed condition results in the formation of a solid conductive network by the conductive metal powder that surrounds the
20 active material particles. This insures current collection capability even if pulverization occurs and thus suppresses an increase of contact resistance.

 The conductive metal foil for use as a current collector in the present invention may be composed of a
25 metal such as copper, nickel, iron, titanium or cobalt, or

an alloy containing any combination thereof. It is particularly preferred that the conductive metal foil contains a metal element that shows a tendency to diffuse into the active material particles. From this point of view, 5 the conductive metal foil preferably comprises a copper foil or a copper alloy foil. The copper element when heat treated shows a high tendency to diffuse into the active material particles. It is accordingly expected that such a conductive foil when sintered shows the improved adhesion to 10 the active material particles. The copper foil having a surface roughness Ra of 0.2 μm or larger may be exemplified by an electrolytic copper foil or an electrolytic copper alloy foil. Such an electrolytic copper or copper alloy foil can be made by electrolytically depositing copper or a 15 copper alloy on a copper foil surface. Other metal foils can also be used which carry copper or a copper alloy electrolytically deposited thereon. Such metal foils may be made by electrically depositing copper or a copper alloy on a surface of a nickel foil, for example.

20 In the present invention, the conductive metal powder for use in combination with the active material particles may be composed of the same material as the conductive metal foil. Specific examples of such materials include copper, nickel, iron, titanium, cobalt and their alloys and mixtures. 25 The particularly preferred conductive metal powder is

composed of copper. By sintering a mixture of the active material particles and the conductive metal powder on a surface of the current collector, a metal component present in the conductive metal foil and/or the conductive metal powder is believed to diffuse into the active material particles and localize around the active material particles. The use of copper or other nonlithium-alloying metal component suppresses volumetric expansion and shrinkage during a charge-discharge reaction in regions where the metal component is unevenly distributed. This prevents separation of the active material from the current collector and pulverization of the current collector material, resulting in the improved charge-discharge cycle characteristics.

The active material particles for use in the present invention may be composed of silicon and/or a silicon alloy. Examples of silicon alloys include solid solutions of silicon and other one or more elements, intermetallic compounds of silicon with other one or more elements and eutectic alloys of silicon and other one or more elements. Alloying can be achieved by such methods as arc melting, liquid quenching, mechanical alloying, sputtering, chemical vapor deposition and calcining. Examples of liquid quenching methods include a single roll quenching method, a twin roll quenching method and various atomizing methods

including gas atomizing, water atomizing and disk atomizing.

The active material particles for use in the present invention may also comprise silicon and/or silicon alloy particles with surfaces being coated with a metal or the
5 other. Coating can be achieved by such methods as electroless plating, electrolytic plating, chemical reduction, vapor deposition, sputtering and chemical vapor deposition. Preferably, the coating metal is the same type of metal as the conductive metal foil or the conductive
10 metal powder. In the sintering, the active material particles if coated with the metal identical in type to the conductive metal foil or conductive metal powder exhibit the marked improvement in adhesion to the current collector and the conductive metal powder, resulting in the provision of
15 further improved charge-discharge cycle characteristics.

The active material particles for use in the present invention may be composed of material that alloys with lithium. Examples of such lithium-alloying materials include the aforesaid silicon and silicon alloys, germanium,
20 tin, lead, zinc, magnesium, sodium, aluminum, gallium, indium and their alloys.

The mean particle diameter of the active material particles for use in the present invention is not particularly specified but may preferably be up to 100 μm ,
25 more preferably up to 50 μm , most preferably up to 10 μm , to

insure effective sintering. The better cycle performance characteristics can be obtained as the mean particle diameter of the active material particles becomes smaller. The mean particle diameter of the conductive metal powder
5 for use in the present invention is not particularly specified but may preferably be up to 100 μm , more preferably up to 50 μm , most preferably up to 10 μm .

In the present invention, a ratio by weight of the conductive metal powder to the active material particles is
10 preferably within the range of 0.05 - 50. If the ratio is too low, satisfactory charge-discharge cycle characteristics may not be obtained. On the other hand, if it becomes excessively high, the amount of the active material particles in the blend becomes relatively smaller to result
15 in the reduced charge-discharge capacity.

However, if the mean particle diameter of the active material particles is small, satisfactory charge-discharge cycle characteristics may be obtained even when the conductive metal powder is excluded, i.e., with the sole use
20 of the active material particles.

In the present invention, the thickness of the conductive metal foil is not particularly specified but may preferably be in the range of 10 μm - 100 μm . The thickness of the sintered layer overlying the conductive metal foil
25 and consisting of the active material particles or a mixture

of the active material particles and conductive metal powder is not particularly specified but may preferably be up to 100 μm , more preferably 10 μm - 100 μm .

In the present invention, sintering may be carried out under a non-oxidizing atmosphere such as a nitrogen, argon or other inert gas atmosphere. Alternatively, sintering may be carried out under a hydrogen or other reducing atmosphere. Preferably, sintering is accomplished by a heat treatment at a temperature that does not exceed any one of the melting points of the conductive metal foil, conductive metal powder and active material particles. In an exemplary case where the conductive metal foil and conductive metal powder are both composed of copper, the heat treatment temperature is preferably maintained not to exceed its melting temperature, i.e., 1083 $^{\circ}\text{C}$, more preferably at 200 - 500 $^{\circ}\text{C}$, further preferably 300 - 450 $^{\circ}\text{C}$. Sintering can be achieved by a spark plasma sintering or hot pressing technique.

In the case where a powder containing silicon and/or a silicon alloy is used as the active material particles and a copper element is diffused into such active material particles, if sintering is performed at a high heat treatment temperature, a large amount of copper element may diffuse into the active material particles to form therein an intermetallic compound of silicon and copper, i.e., copper silicide. The formation of copper silicide is likely

to decline charge-discharge cycle characteristics. It is therefore preferred that sintering is performed under such conditions that formation of copper silicide is not caused to occur in a level detectable by X-ray diffractometry.

5 In view of the preceding discussion, it is preferred that sintering is performed within the above-specified temperature range.

In the present invention, a slurry either containing the active material particles, conductive metal powder and a
10 binder or containing the active material particles and a binder may be coated on the conductive metal foil as a current collector to provide thereon a layer of the mixture or a layer of active material particles. The binder preferably remains fully undecomposed after the heat
15 treatment for sintering. As stated above, sintering improves adhesion between the active material particles and the current collector and between the active material particles themselves. If the binder remains undecomposed even after the heat treatment, the binding ability thereof
20 further improves adhesion therebetween. Accordingly, pulverization of the active material particles and separation of the active material particles from the current collector are suppressed to result in obtaining more satisfactory charge-discharge cycle characteristics.

25 A preferred example of the binder for use in the

present invention is polyimide. Polyimide can be obtained, for example, by subjecting polyamic acid to a heat treatment. The heat treatment causes polyamic acid to undergo dehydrocondensation to produce polyimide. In the present invention, polyimide preferably has an imidization level of at least 80 %. If the imidization level of polyimide is below 80 %, its adhesion to the active material particles and the current collector may become unsatisfactory. The imidization level, as used herein, refers to a mole % of the produced polyimide relative to a polyimide precursor. Polyimide with at least 80 % imidization level can be obtained, for example, by subjecting an NMP (N-methylpyrrolidone) solution of polyamic acid to a heat treatment at a temperature of 100 °C - 400 °C for over 1 hour. In an exemplary case where the heat treatment is carried out at 350 °C, the imidization level approaches 80 % in about 1 hour and 100 % in about 3 hours. In the case of using polyimide as a binder, sintering is preferably carried out at a temperature that does not cause full decomposition of polyimide, i.e., at 600 °C or below, since in the present invention the binder is preferred to remain fully undecomposed even after the heat treatment for sintering.

The use of a fluoro-containing binder is also preferred. Polyvinylidene fluoride and polytetrafluoroethylene are particularly preferred fluoro-

containing binders. It is preferred that
polytetrafluoroethylene or polyvinylidene fluoride is used
as a binder and the heat treatment for sintering is
performed at a temperature that does not cause full
5 decomposition of such a binder. This further improves
charge-discharge cycle performance characteristics.

In view of the above discussion, the heat treatment
for sintering is preferably carried out at 200 - 500 °C, more
preferably at 300 °C - 450 °C.

10 In the present invention, a layer of a mixture of the
active material particles and the conductive metal powder or
a layer of the active material particles is provided on the
conductive metal foil as a current collector. Preferably,
such a layer, together with the underlying conductive metal
15 foil, is subjected to calendering or rolling, prior to being
sintered. Rolling increases a packing density of the layer
comprising the mixture or the active material particles and
thus improves adhesion between the active material particles
and the current collector or between the active material
20 particles themselves, resulting in obtaining improved
charge-discharge cycle performance characteristics.

In the present invention, it is also preferred that
the active material particles and/or the binder penetrates
into minute pits on a surface of the conductive metal foil.
25 This penetration of the active material particles and/or the

binder into minute pits on the conductive metal foil surface further improves adhesion between the current collector and the layer of the mixture or the active material particles.

A rechargeable lithium battery of the present invention is characterized as including a negative electrode comprising either the negative electrode of the present invention or the electrode of the present invention or the negative electrode fabricated by the practice of the method of the present invention; a positive electrode containing positive active material and a nonaqueous electrolyte.

An electrolyte solvent for use in the rechargeable lithium battery of the present invention is not particularly specified in type but can be illustrated by a mixed solvent which contains cyclic carbonate such as ethylene carbonate, propylene carbonate or butylene carbonate and also contains chain carbonate such as dimethyl carbonate, methyl ethyl carbonate or diethyl carbonate. Also applicable is a mixed solvent of the above-listed cyclic carbonate and an ether solvent such as 1,2-dimethoxyethane or 1,2-diethoxyethane. Examples of electrolyte solutes include LiPF_6 , LiBF_4 , LiCF_3SO_3 , $\text{LiN}(\text{CF}_3\text{SO}_2)_2$, $\text{LiN}(\text{C}_2\text{F}_5\text{SO}_2)_2$, $\text{LiN}(\text{CF}_3\text{SO}_2)(\text{C}_4\text{F}_9\text{SO}_2)$, $\text{LiC}(\text{CF}_3\text{SO}_2)_3$, $\text{LiC}(\text{C}_2\text{F}_5\text{SO}_2)_3$ and mixtures thereof. Other applicable electrolytes include gelled polymer electrolytes comprised of an electrolyte solution impregnated into polymer electrolytes such as polyethylene oxide and

polyacrylonitrile; and inorganic solid electrolytes such as LiI and Li_3N , for example. The electrolyte for the rechargeable lithium battery of the present invention can be used without limitation, so long as a lithium compound as
5 its solute that imparts ionic conductivity, together with its solvent that dissolves and retains the lithium compound, remain undecomposed at voltages during charge, discharge and storage of the battery.

Examples of useful active materials for the positive
10 electrode of the rechargeable lithium battery of the present invention include lithium-containing transition metal oxides such as LiCoO_2 , LiNiO_2 , LiMn_2O_4 , LiMnO_2 , $\text{LiCo}_{0.5}\text{Ni}_{0.5}\text{O}_2$ and $\text{LiNi}_{0.7}\text{Co}_{0.2}\text{Mn}_{0.1}\text{O}_2$; and lithium-free metal oxides such as MnO_2 . Other substances can also be used, without limitation, if
15 they are capable of electrochemical lithium insertion and deinsertion.

Figure 2 is a schematic sectional view, illustrating one embodiment of the negative electrode for a rechargeable lithium battery in accordance with the present invention.
20 Provided on a conductive metal foil 11 are active material particles 12 and conductive metal powder 13, with all having been already sintered. Formed in the active material particles 12 are a region 12a into which a metal component from the conductive metal foil 11 has diffused and a region
25 12b into which a metal component from the conductive metal

powder 13 has diffused. In the case where the respective metal components diffused from the conductive metal foil 11 and from the conductive metal powder 13 are of the type that does not alloy with lithium, volumetric expansion of the active material particles 12 that occurs as they store lithium becomes smaller in those diffusion regions 12a and 12b. This is believed to suppress separation of the active material particles 12 from the conductive metal foil 11 and the conductive metal powder 13 and also prevent pulverization of the active material particles 12 themselves and accordingly results in the improved charge-discharge cycle performance characteristics.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a schematic sectional view showing a construction of a rechargeable lithium battery made in Examples in accordance with the present invention;

Figure 2 is a schematic sectional view showing one embodiment of a negative electrode for a rechargeable lithium battery in accordance with the present invention;

Figure 3 is a graph showing X-ray diffraction profiles of the respective negative electrodes of the batteries A18 and A20 fabricated in Examples;

Figure 4 is a photomicrograph taken using a scanning electron microscope (at a magnification of 1,000X), showing

a section of the negative electrode of the battery A20
fabricated in Example;

Figure 5 is a photomicrograph taken using a scanning
electron microscope (at a magnification of 5,000X), showing
5 a section of the negative electrode of the battery A20
fabricated in Example;

Figure 6 is a graph showing X-ray diffraction profiles
of the respective negative electrodes of the batteries C1
and C3 fabricated in Examples;

10

BEST MODE FOR CARRYING OUT THE INVENTION

The present invention is below described in more
detail by way of Examples. It will be recognized that the
following examples merely illustrate the practice of the
15 present invention but are not intended to be limiting
thereof. Suitable changes and modifications can be effected
without departing from the scope of the present invention.

EXPERIMENT 1

(Fabrication of Negative Electrode)

20 Copper powder in the form of flaky particles having a
mean particle diameter of 10 μm , as the conductive metal
powder, and silicon powder having a mean particle diameter
of 50 μm as the active material particles were weighed such
that a ratio by weight of the former to the latter was
25 brought to 4:1 (= 1:0.25) and then dry mixed in a mortar.

90 parts by weight of the mixture was added to an 8 wt.% N-methylpyrrolidone solution containing 10 parts by weight of polyvinylidene fluoride as a binder to provide a negative electrode mix slurry.

5 The negative electrode mix slurry was coated on one surface of an electrolytic copper foil (15 μm thick) having a surface roughness R_a of 0.5 μm and serving as a current collector, dried and then rolled. A 20 mm diameter disc was cut out from the coated copper foil and then sintered by a
10 heat treatment under argon atmosphere at 700 $^{\circ}\text{C}$ for 10 hours to provide a negative electrode. The thickness of the sintered electrode (excluding the current collector) was determined to be 50 μm .

(Fabrication of Positive Electrode)

15 Starting materials, Li_2CO_3 and CoCO_3 , were weighed such that a ratio of numbers of Li and Co atoms, Li:Co, was brought to 1:1, and then mixed in a mortar. The mixture was pressed in a 17 mm diameter mold and calcined in the air at 800 $^{\circ}\text{C}$ for 24 hours to obtain a calcined product consisting
20 of LiCoO_2 . This product was then ground into particles with a mean particle diameter of 20 μm .

 90 parts by weight of the resulting LiCoO_2 powder and 5 parts by weight of artificial graphite as an electric conductor were added to a 5 wt.% N-methylpyrrolidone
25 solution containing 5 parts by weight of polyvinylidene

fluoride as a binder to provide a positive electrode mix slurry.

The positive electrode mix slurry was coated on an aluminum foil as a current collector, dried and then rolled.

5 A 20 mm diameter disc was cut out from the coated aluminum foil to provide a positive electrode.

(Preparation of Electrolyte Solution)

1 mole/liter of LiPF_6 was dissolved in a mixed solvent containing an equivolume of ethylene carbonate and diethyl
10 carbonate to prepare an electrolyte solution.

(Construction of Battery)

Using the above-prepared positive electrode, negative electrode and electrolyte solution, a flat-type rechargeable lithium battery A1 was constructed.

15 Figure 1 is a schematic sectional view of the constructed rechargeable lithium battery. The battery includes a positive electrode 1, a negative electrode 2, a separator 3, a positive can 4, a negative can 5, a positive current collector 6, a negative current collector 7 and an
20 insulative gasket 8 made of polypropylene.

The positive electrode 1 and the negative electrode 2 were placed on opposite sides of the separator 3. These were housed in a battery case comprising the positive can 4 and the negative can 5. The positive current collector 6
25 connects the positive electrode 1 to the positive can 4 and

the negative current collector 6 connects the negative electrode 2 to the negative can 5. Accordingly, a battery construction is provided which is capable of charge and discharge, i.e., rechargeable.

5 EXPERIMENT 2

 Silicon and nickel or copper were mixed such that a ratio in number of silicon to nickel or copper atoms was brought to 9:1, and then made into an Si_9Ni or Si_9Cu alloy by a single roll quenching process. These alloys were ground
10 in a mortar into particles with a mean particle diameter of 50 μm . The procedure of Experiment 1 was followed, except that the silicon powder was replaced by these alloy powders, to construct batteries A2 and A3. The battery A2 was constructed using the Si_9Ni alloy and the battery A3 using
15 the Si_9Cu alloy.

 EXPERIMENT 3

 An electroless plating process was utilized to provide nickel coating on surfaces of silicon powder particles having a mean particle diameter of 50 μm . By atomic
20 absorption spectrometry (ICP), a weight of nickel coated on the silicon powder particles was found to be 0.5 % of a total weight.

 The procedure of Experiment 1 was followed, except that the silicon powder was replaced by the nickel-coated
25 silicon powder, to construct a battery A4.

EXPERIMENT 4

An electrolytic process was utilized to deposit copper on a nickel foil and a stainless steel foil so that a copper coated nickel foil (15 μm thick) and a copper coated stainless steel foil (15 μm thick) were prepared. Each of these copper coated foils was determined to have a surface roughness R_a of 0.5 μm .

The procedure of Experiment 1 was followed, except that the electrolytic copper foil was replaced by the copper coated nickel or stainless steel foil, to construct batteries A5 and A6. The battery A5 resulted from the use of the copper coated nickel foil and the battery A6 from the use of the copper coated stainless steel foil.

The procedure of Experiment 1 was followed, except that the electrolytic copper foil was replaced by an electrolytic nickel or iron foil having a surface roughness R_a of 0.5 μm , to construct batteries A7 and A8. The battery A7 resulted from the use of the electrolytic nickel foil and the battery A8 from the use of the electrolytic iron foil.

EXPERIMENT 5

The procedure of Experiment 1 was followed, except that the flaky copper powder was replaced by flaky nickel or iron powder having a mean particle diameter of 10 μm , to construct batteries A9 and A10. The battery A9 resulted from the use of the flaky nickel powder and the battery A10

from the use of the flaky iron powder.

The procedure of Experiment 1 was followed, except that the flaky copper powder was replaced by an equiweight mixture of the flaky copper powder used in Experiment 1 and
5 flaky nickel powder having a mean particle diameter of 10 μm , to construct a battery A11.

EXPERIMENT 6

The procedure of Experiment 1 was followed, except that the electrolytic copper foil having a surface roughness
10 Ra of 0.5 μm was replaced by an electrolytic copper foil having a surface roughness Ra of 0.2 μm , to construct a battery A12.

The procedure of Experiment 1 was followed, except that the electrolytic copper foil having a surface roughness
15 Ra of 0.5 μm was replaced by a rolled copper foil having a surface roughness Ra of 0.1 μm , to construct a battery B1.

(Evaluation of Charge-Discharge Cycle Characteristics)

The above-constructed batteries A1 - A12 and B1 were evaluated for charge-discharge cycle characteristics. Each
20 battery was charged at 25 °C at a current of 1 mA to 4.2 V and then discharged at a current of 1 mA to 2.7 V. This was recorded as a unit cycle of charge and discharge. The battery was cycled to determine the number of cycles after which its discharge capacity fell down to 80 % of its first-
25 cycle discharge capacity and the determined cycle number was

recorded as a cycle life. The results are shown in Table 1. The cycle life of each battery is indicated therein by an index when that of the battery A1 is taken as 100.

5

Table 1

Battery	Cycle Life
A1 (Surface Roughness Ra : 0.5 μm)	100
A2 (Surface Roughness Ra : 0.5 μm)	110
A3 (Surface Roughness Ra : 0.5 μm)	115
A4 (Surface Roughness Ra : 0.5 μm)	112
A5 (Surface Roughness Ra : 0.5 μm)	97
A6 (Surface Roughness Ra : 0.5 μm)	94
A7 (Surface Roughness Ra : 0.5 μm)	96
A8 (Surface Roughness Ra : 0.5 μm)	97
A9 (Surface Roughness Ra : 0.5 μm)	95
A10 (Surface Roughness Ra : 0.5 μm)	93
A11 (Surface Roughness Ra : 0.5 μm)	97
A12 (Surface Roughness Ra : 0.2 μm)	85
B1 (Surface Roughness Ra : 0.1 μm)	65

As can be clearly seen from Table 1, the batteries A1 - A12 using metal foils having a surface roughness Ra of 0.2 μm or larger exhibit the extended cycle lives relative to the battery B1 using a metal foil having a surface roughness Ra of 0.1 μm . The use of a metal foil having a surface roughness Ra of 0.2 μm or larger is believed to have caused more effective sintering of the overlying active material particles and conductive metal powder and improved adhesion of the active material particles to the current collector.

EXPERIMENT 7

In this Experiment, the effect of sintering on the cycle characteristics was studied.

Following Experiment 1, the negative electrode mix slurry was coated on an electrolytic copper foil, dried and rolled. However, in the fabrication of a negative electrode, the coated copper foil was not subjected to a heat treatment. Using this negative electrode, a battery B2 was constructed. This battery was evaluated for cycle characteristics in the same manner as above. Its cycle life was given by an index when that of the battery A1 was taken as 100. In Table 2, the cycle life of the battery A1 is also shown.

Table 2

Battery	Cycle Life
A1	100
B2	20

As apparent from Table 2, the battery A1 incorporating the negative electrode made with heat treatment exhibits far superior cycle characteristics compared to the battery B2 incorporating the negative electrode with heat treatment. This is believed to have resulted from the heat treatment which improved adhesion of the active material particles to the conductive metal powder and the conductive metal foil and induced metal components in the conductive metal foil and the conductive metal powder to diffuse into the active material particles to form therein a network of diffusion

regions that improved the capability of current collection.

EXPERIMENT 8

In this Experiment, the effect of the amount of the loaded conductive metal powder on the cycle characteristics was studied.

The procedure of Experiment 1 was followed, except that the weight of the flaky copper powder loaded per unit weight of the silicon powder was varied to 1 (50 % by weight of copper powder), 0.5 (33.3 % by weight of copper powder), 0.125 (11.1 % by weight of copper powder) and 0 (0 % by weight of copper powder), to construct batteries A13, A14, A15 and A16.

These batteries were evaluated for cycle characteristics in the same manner as described above. The results are given in Table 3. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100.

Table 3

Battery	Cycle Life
A1 (Copper Powder Content : 20 Weight %)	100
A13 (Copper Powder Content : 50 Weight %)	143
A14 (Copper Powder Content : 33.3 Weight %)	127
A15 (Copper Powder Content : 11.1 Weight %)	91
A16 (Copper Powder Content : 0 Weight %)	29

As can be clearly seen from Table 3, the batteries A1

and A13 - A15 with the negative electrodes containing the flaky copper powder exhibit far superior cycle characteristics compared to the battery A16 with the negative electrode excluding the flaky copper powder. This
5 is believed to have resulted from the addition of the copper powder that improved adhesion between the silicon powder particles as the active material particles, led to the formation of a solid conductive network surrounding the silicon powder particles, and as a result, improved the
10 capability of current collection.

EXPERIMENT 9

In this Experiment, the effects of the heat treatment temperature, mean particle diameter of the silicon powder and mean particle diameter of the conductive metal powder on
15 the cycle life were studied.

The procedure of Experiment 1 was followed, except that the heat treatment temperature, mean particle diameter of the silicon powder, and mean particle diameter and type of the conductive metal powder were altered as specified in
20 Table 4, to construct batteries A17 - A24. These batteries were evaluated for cycle characteristics according to the procedure used in Experiment 1. The cycle life of each battery was indicated by an index when that of the battery A1 was taken as 100.

Table 4

Battery	Heat Treatment Conditions	Mean Particle Diameter of Silicon Powder (μm)	Mean Particle Diameter of Conductive Metal Powder (μm)	Cycle Life
A1	700 °C, 10 Hours	50	15 Flaky Copper Powder	100
A17	400 °C, 30 Hours	50	15 Flaky Copper Powder	130
A18	700 °C, 10 Hours	3	15 Flaky Copper Powder	330
A19	500 °C, 10 Hours	3	15 Flaky Copper Powder	360
A20	400 °C, 30 Hours	3	15 Flaky Copper Powder	750
A21	400 °C, 10 Hours	3	15 Flaky Copper Powder	733
A22	300 °C, 30 Hours	3	15 Flaky Copper Powder	740
A23	200 °C, 20 Hours	3	15 Flaky Copper Powder	305
A24	400 °C, 30 Hours	3	3 Flaky Brass (Cu-10wt%Zn) Powder	800

As can be clearly seen from Table 4, maintaining the heat treatment temperature within the range of 200 °C - 500 °C results in the marked improvement of cycle characteristics. The particularly preferred heat treatment temperature is found to be about 400 °C. As apparent from the comparison between the batteries A1 and A18 and between the batteries A17 and A20, the cycle characteristics is markedly improved when the mean particle diameter of the silicon powder is reduced to 3 μm from 50 μm .

Figure 3 is a graph showing X-ray diffraction profiles of the respective negative electrodes of the batteries A18 and A20. As apparent from Figure 3, the electrode made via

heat treatment at 700 °C for the battery A18 exhibits a copper silicide peak, while no copper silicide peak existed for the electrode made via heat treatment at 400 °C for the battery A20. This appears to demonstrate that the heat
5 treatment at 700 °C induces diffusion of excess copper element into the silicon powder to result in the deposition of copper silicide. This accordingly suggests that sintering is preferably carried out under such heat treatment conditions that cause no deposition of copper
10 silicide in order to improve cycle characteristics.

Figures 4 and 5 are photomicrographs taken using a scanning electron microscope (SEM), each showing a section of the negative electrode incorporated in the battery A20. Figure 4 is a photomicrograph taken at a magnification of
15 1,000X and Figure 5 is a photomicrograph taken at a magnification of 5,000X. These negative electrodes were resin-embedded and then sliced before they were used as samples for observation.

As can be clearly seen from Figures 4 and 5, the
20 silicon powder and the conductive powder while both in a closely packed condition are brought into contact with a surface of the electrolytic copper foil.

It is also observed that the silicon powder and the binder penetrate densely into pits on the surface of the
25 electrolytic copper foil.

Polyvinylidene fluoride (PVdF) for use as the binder was subjected to a heat treatment at 400 °C and 700 °C and then to observation by infrared absorption spectrum (IR spectrum). Peaks for PVdF and its decomposition product appeared in the IR spectrum of PVdF when heat treated at 400 °C. However, the PVdF peak disappeared completely in the IR spectrum of PVdF when heat treated at 700 °C. Accordingly, the improved cycle characteristics obtained for the battery incorporating the negative electrode made via heat treatment at 400 °C is conceivably attributed not only to the sintering that improved adhesion between the silicon powder particles and between the silicon powder particles and the copper foil, but also to the action of a binding force of the remaining binder that further improved adhesion between the silicon powder particles and between the silicon powder particles and the copper foil.

EXPERIMENT 10

In this Experiment, the effect of the binder type on the cycle life was studied.

The procedure of Experiment 1 was followed, except that polyvinylpyrrolidone (PVP) was used as the binder, the silicon powder was used having a mean particle diameter of 3 μm and the heat treatment was carried out at 400 °C for 10 hours, to construct a battery A25. This battery was evaluated for cycle characteristics according to the

procedure used in Experiment 1. The results are given in Table 5. In Table 5, the results for the batteries A1 and A21 are also given. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100.

Table 5

Battery	Binder	Heat Treatment Conditions	Mean Particle Diameter of Silicon Powder (μm)	Cycle Life
A1	PVdF	700 °C, 10 Hours	50	100
A21	PVdF	400 °C, 10 Hours	3	733
A25	PVP	400 °C, 10 Hours	3	50

As can be clearly seen from Table 5, the use of fluoro-containing PVdF as the binder results in the improved cycle characteristics.

In this Experiment, the presence of a fluoride of silicon on particle surfaces of the silicon powder as the active material was confirmed by electron spectroscopic analysis (XPS) for the negative electrode of the battery A21 which incorporated PVdF as the binder and experienced a heat treatment at 400 °C.

EXPERIMENT 11

In this Experiment, the effect of the type of the conductive metal powder on the cycle life was studied.

The procedure of Experiment 1 was followed, except that the silicon powder was used having a mean particle

diameter of 3 μm , the conductive metal powder specified in Table 6 was used and the heat treatment was carried out at 400 $^{\circ}\text{C}$ for 30 hours, to construct batteries A26 - A32. A battery B3 was also constructed using ketchen black in the place of the conductive metal powder. These batteries were evaluated for cycle characteristics according to the procedure used in Experiment 1. The results are given in Table 6. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100. In Table 6, the results for the batteries A19 and A24 are also given.

Table 6

Battery	Conductive Metal Powder (Mean Particle Diameter μm)	Cycle Life
A19	Flaky Cu Powder (15)	750
A24	Flaky Brass (Cu-10wt%Zn) Powder (3)	800
A26	Co Powder (5)	810
A27	Fe Powder (3)	820
A28	Mo Powder (0.7)	770
A29	Flaky Ni Powder (13)	820
A30	Ti Powder (10)	820
A31	W Powder (0.6)	780
A32	Zn Powder (7)	720
B3	Ketchen Black (0.3)	280

As can be clearly seen from Table 6, the electrode using any type of the conductive metal powder exhibits excellent cycle characteristics. This is probably because the conductive metal powder forms a conductive network surrounding the silicon powder particles to result in

obtaining the increased current collecting capability.
 However, the use of kitchen black in the place of the
 conductive metal powder apparently shortens a cycle life.
 This is believed likely due to the low density and high bulk
 5 of the kitchen black which made it insufficient for the
 binder present in the same amount as in the other electrodes
 to provide adhesion between the particles.

EXPERIMENT 12

In this Experiment, the effect of rolling in the
 10 electrode fabrication step on the cycle life was studied.

The procedure of Experiment 1 was followed, except
 that coating of the negative electrode mix slurry on the
 electrolytic copper foil surface was not followed by rolling,
 to construct a battery A33. This battery was evaluated for
 15 cycle characteristics according to the procedure used in
 Experiment 1. The evaluation results are given in Table 7.
 The cycle life of each battery is indicated by an index when
 that of the battery A1 is taken as 100.

20

Table 7

Battery	Rolling	Cycle Life
A1	Present	100
A33	Absent	50

As can be clearly seen from Figure 7, the practice of
 rolling in the electrode fabrication step improves cycle
 characteristics. This is probably because the practice of

rolling has led not only to further dense packing of the active material particles that improves contact therebetween but also to the increased contact area between the active material particles, the conductive metal powder and the current collector that enables more effective sintering, resulting in the improved current collecting performance characteristics.

EXPERIMENT 13

In the fabrication of electrodes, the flaky copper powder as the conductive metal powder was excluded and only the silicon powder was used. Specifically, the copper foils specified in Table 8, the silicon powders having the mean particle diameters specified in Table 8 and the heat treatment conditions specified in Table 8 were used.

Otherwise, the procedure of Experiment 1 was followed to construct batteries C1 - C3 and B4. These batteries were evaluated for cycle characteristics according to the procedure used in Experiment 1. The results are given in Table 8. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100.

Table 8

Battery	Copper Foil	Heat Treatment Conditions	Mean Particle Diameter of Silicon Powder(μm)	Cycle Life
A1	Electrolytic Copper Foil (Surface Roughness Ra : 0.5 μm)	700 °C, 10 Hours	50	100
C1	Electrolytic Copper Foil (Surface Roughness Ra : 0.5 μm)	400 °C, 10 Hours	3	720
C2	Electrolytic Copper Foil (Surface Roughness Ra : 0.5 μm)	400 °C, 10 Hours	50	125
C3	Electrolytic Copper Foil (Surface Roughness Ra : 0.5 μm)	700 °C, 10 Hours	3	200
B4	Rolled Copper Foil (Surface Roughness Ra : 0.1 μm)	400 °C, 10 Hours	3	95

As can be clearly seen from Figure 8, the use of the electrode incorporating the silicon powder with a smaller mean particle diameter and made via heat treatment at 400 °C results in the marked improvement of cycle characteristics. This is likely because the use of the silicon powder having a smaller mean particle diameter has led to the effective sintering that improves adhesion between the silicon powder particles and between the silicon powder particles and the copper foil.

As also apparent from comparison between the batteries C1 and B4, the use of the metal foil having a surface roughness Ra of 0.2 μm or larger results in the improved cycle performance characteristics.

Figure 6 is a graph showing X-ray diffraction profiles

of the respective negative electrodes of the batteries C1 and C3. As apparent from Figure 6, the electrode made via heat treatment at 700 °C for the battery C3 exhibits a copper silicide peak, while no copper silicide peak existed for the electrode made via heat treatment at 400 °C for the battery C1. This demonstrates that even in the case where the conductive metal powder was excluded and only the silicon powder was used in the fabrication of electrodes, sintering is preferably carried out at such a heat treatment temperature that no deposition of copper silicide is caused to occur in a level detectable by X-ray diffractometry.

EXPERIMENT 14

The effect of the type of the binder in the electrode made by incorporating the silicon powder but excluding the flaky copper powder as the conductive metal powder on the cycle life was studied. In Experiment 1, the silicon powder having a mean particle diameter of 3 μm was used, the flaky copper powder was excluded, and the heat treatment condition and the binder respectively specified in Table 9 were used. Otherwise, the procedure of Experiment 1 was followed to construct batteries D1 - D5. Where polyimide was used as the binder, an electrode was fabricated by adding 90 parts by weight of silicon powder to an 18 wt. % N-methylpyrrolidone solution containing 10 parts by weight of polyamic acid to provide a negative electrode mix slurry,

coating and heat treating the negative electrode mix slurry. The electrode, subsequent to the heat treatment at 400 °C, was found to have an imidization level of 100 %. Where styrene-butadiene rubber (SBR) or polytetrafluoroethylene (PTFE) was used as the binder, an electrode was fabricated by adding 90 parts by weight of silicon powder to a mixture of a 3 wt.% aqueous solution containing 1 part by weight of a carboxymethylcellulose (CMC) thickener with a 48 wt.% aqueous dispersion containing 10 parts by weight of styrene-butadiene rubber (SBR) or with a 60 wt.% aqueous dispersion containing 10 parts by weight of polytetrafluoroethylene (PTFE) to provide a negative electrode mix slurry. Where polyvinylpyrrolidone (PVP) was used as the binder, an electrode was fabricated by adding 90 parts by weight of silicon powder to a 8 wt.% N-methylpyrrolidone solution containing 10 parts by weight of polyvinylpyrrolidone (PVP) to provide a negative electrode mix slurry.

The batteries D1 - D5 were fabricated using these electrodes according to the procedure used in Experiment 1 and then evaluated for cycle characteristics. The results are given in Table 9. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100.

The temperature at which the weight of the binder showed a declining tendency in thermogravimetry was recorded as a thermal decomposition initiation temperature of the

binder.

Table 9

Battery	Binder	Decomposition Initiating Temp. of Binder (°C)	Heat Treatment Conditions	Cycle Life
A1	Polyvinylidene Fluoride (PVdF)	380	700 °C, 10 Hours	100
D1	Polyvinylidene Fluoride (PVdF)	380	400 °C, 30 Hours	820
D2	Polyimide (PI)	500	400 °C, 30 Hours	980
D3	Polyvinyl- pyrrolidone (PVP)	260	400 °C, 10 Hours	55
D4	Polytetrafluoro- ethylene (PTFE)	450	400 °C, 30 Hours	710
D5	Styrene-Butadiene Rubber (SBR)	240	400 °C, 10 Hours	40

5 As can be seen from Figure 9, the use of the binder
having a higher decomposition initiation temperature results
in the improved cycle characteristics. This is believed
likely due to the binder left undecomposed after the heat
treatment, which served during sintering to improve adhesion
10 between the active material and the current collector and
between the active material particles, exhibited a binding
force that further improved adhesion therebetween and, as a
result, provided a further adherent electrode.

EXPERIMENT 15

15 The effect of the mean particle diameter of the
silicon powder in the electrode made by incorporating the
silicon powder but excluding the flaky copper powder as the
conductive metal powder on the cycle life was studied. The

case of using polyimide as the binder in Experiment 14 was followed, except that the mean particle diameter of the silicon powder was varied as specified in Table 10, to construct batteries D6 - D10. These batteries were

5 evaluated for cycle characteristics according to the procedure used in Experiment 1. The results are given in Table 10. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100. In Table 10, the results for the batteries A1 and C2 are also shown.

10

Table 10

Battery	Mean Particle Diameter of Silicon Powder (μm)	Heat Treatment Conditions	Binder	Cycle Life
A1	50	700 °C, 10 Hours	PVdF	100
C2	50	400 °C, 10 Hours	PVdF	125
D6	0.3	400 °C, 30 Hours	PI	250
D2	3	400 °C, 30 Hours	PI	980
D7	4	400 °C, 30 Hours	PI	710
D8	5	400 °C, 30 Hours	PI	450
D9	7.5	400 °C, 30 Hours	PI	460
D10	50	400 °C, 30 Hours	PI	120

As can be clearly seen from Table 10, the use of the silicon powder having a mean particle diameter of 10 μm or

15 below results in the improved cycle performance characteristics.

EXPERIMENT 16

In this Experiment, the effect of the amount of the binder in the electrode made by incorporating the silicon

powder but excluding the flaky copper powder as the conductive metal powder on the cycle characteristics was studied. The silicon powder having a mean particle diameter of 3 μm was used but the flaky copper powder was excluded.

5 The heat treatment and the binder used are specified in Table 11, respectively. Otherwise, the procedure of Experiment 1 was followed to construct batteries D11 - D16. Where polyimide was used as the binder, a battery was
10 fabricated by following the case of using polyimide as the binder in Experiment 14. These batteries were evaluated for cycle characteristics according to the procedure used in Experiment 1. The results are given in Table 11. The cycle life of each battery is indicated by an index when that of the battery A1 is taken as 100. In Table 11, the results
15 for the batteries A1, D1 and D2 are also shown.

Table 11

Battery	Binder	Binder Content (Weight %)	Heat Treatment Conditions	Cycle Life
A1	PVdF	10	700 °C, 10 Hours	100
D11	PVdF	3.2	400 °C, 30 Hours	520
D1	PVdF	10	400 °C, 30 Hours	820
D12	PVdF	18	400 °C, 30 Hours	830
D13	PVdF	25	400 °C, 30 Hours	810
D14	PI	1.1	400 °C, 30 Hours	200
D15	PI	5.3	400 °C, 30 Hours	480
D2	PI	10	400 °C, 30 Hours	980
D16	PI	18	400 °C, 30 Hours	970

As apparent from Table 11, the electrode if containing the binder in the amount of at least 5.3 % by weight, preferably at least 10 % by weight, provides the improved battery cycle characteristics. This is believed due to the presence of the binder in the amount sufficient to maintain good adhesion between the active material particles and the current collector and between the active material particles.

The following examples illustrate the sixth and seventh aspects of the present invention.

EXPERIMENT 17

(Fabrication of Negative Electrode)

Copper powder in the form of flaky particles having a mean particle diameter of 10 μm , as the conductive metal powder, and silicon powder having a mean particle diameter of 50 μm as the active material particles were weighed such that a ratio by weight of the former to the latter was brought to 4:1 (= 1:0.25) and then dry mixed in a mortar. 90 parts by weight of the mixture was added to an 8 wt.% N-methylpyrrolidone solution containing 10 parts by weight of polyvinylidene fluoride as a binder to provide a negative electrode mix slurry.

The negative electrode mix slurry was coated on one surface of an electrolytic copper foil (15 μm thick) having a surface roughness Ra of 0.5 μm and serving as a current collector, dried and then rolled. A 20 mm diameter disc was

cut out from the resulting coated copper foil and then sintered by a heat treatment under hydrogen atmosphere at 600 °C for 10 hours to provide a negative electrode. The thickness of the sintered electrode (excluding the current collector) was determined to be 50 µm.

(Fabrication of Positive Electrode)

Starting materials, Li_2CO_3 and CoCO_3 , were weighed such that a ratio of numbers of Li and Co atoms, Li:Co, was brought to 1:1, and then mixed in a mortar. The mixture was pressed in a 17 mm diameter mold and calcined in the air at 800 °C for 24 hours to obtain a calcined product consisting of LiCoO_2 . This product was then ground into particles with a mean particle diameter of 20 µm.

90 parts by weight of the resulting LiCoO_2 powder and 5 parts by weight of artificial graphite powder as an electric conductor were added to a 5 wt.% N-methylpyrrolidone solution containing 5 parts by weight of polyvinylidene fluoride as a binder to provide a positive electrode mix slurry.

The positive electrode mix slurry was coated on an aluminum foil as a current collector, dried and then rolled. A 20 mm diameter disc was cut out from the coated aluminum foil to provide a positive electrode.

(Preparation of Electrolyte Solution)

1 mole/liter of LiPF_6 was dissolved in a mixed solvent

containing an equivolume of ethylene carbonate and diethyl carbonate to prepare an electrolyte solution.

(Construction of Battery)

Using the above-prepared positive electrode, negative
5 electrode and electrolyte solution, a flat-type rechargeable lithium battery E1 shown in Figure 1 was constructed.

EXPERIMENT 18

Silicon and nickel or copper were mixed such that a ratio in number of silicon to nickel or copper atoms was
10 brought to 9:1, and then made into an Si_9Ni or Si_9Cu alloy by a single roll quenching process. These alloys were ground in a mortar into particles with a mean particle diameter of 50 μm . The procedure of Experiment 17 was followed, except that the silicon powder was replaced by these alloy powders,
15 to construct batteries E2 and E3. The battery E2 was constructed using the Si_9Ni alloy and the battery E3 using the Si_9Cu alloy.

EXPERIMENT 19

An electroless plating process was utilized to provide
20 nickel coating on surfaces of silicon powder particles having a mean particle diameter of 50 μm . By atomic absorption spectrometry (ICP), a weight of nickel coated on the silicon powder was found to be 0.5 % of a total weight.

The procedure of Experiment 17 was followed, except
25 that the silicon powder was replaced by the nickel-coated

silicon powder, to construct a battery E4.

EXPERIMENT 20

An electrolytic process was utilized to deposit copper on a nickel foil and a stainless steel foil so that a copper
5 coated nickel foil (15 μm thick) and a copper coated stainless steel foil (15 μm thick) were prepared. Each of these copper coated foils was determined to have a surface roughness Ra of 0.5 μm .

The procedure of Experiment 17 was followed, except
10 that the electrolytic copper foil was replaced by the copper coated nickel or stainless steel foil, to construct batteries E5 and E6. The battery E5 resulted from the use of the copper coated nickel foil and the battery E6 from the use of the copper coated stainless steel foil.

15 The procedure of Experiment 17 was followed, except that the electrolytic copper foil was replaced by an electrolytic nickel foil having a surface roughness Ra of 0.5 μm , to construct a battery E7.

EXPERIMENT 21

20 The procedure of Experiment 17 was followed, except that the flaky copper powder was replaced by flaky nickel or iron powder having a mean particle diameter of 10 μm , to construct batteries E8 and E9. The battery E8 resulted from the use of the flaky nickel powder and the battery E9 from
25 the use of the flaky iron powder.

The procedure of Experiment 17 was followed, except that the flaky copper powder was replaced by an equiweight mixture of the flaky copper powder used in Experiment 17 and flaky nickel powder having a mean particle diameter of 10 μm ,
5 to construct a battery E10.

EXPERIMENT 22

The procedure of Experiment 17 was followed, except that the heat treatment for sintering was carried out under argon atmosphere at 600 $^{\circ}\text{C}$ for 10 hours, to fabricate a
10 negative electrode and then a battery F1. Also following the procedure 17, the negative electrode mix slurry was coated on an electrolytic copper foil, dried and rolled. However, in the fabrication of a negative electrode, the coated copper foil was not subjected to a heat treatment.
15 Using this negative electrode, a battery F2 was constructed in the same manner as in Experiment 17.

(Evaluation of Charge-Discharge Cycle Characteristics)

The above-constructed batteries E1 - E10 and F1 - F2 were evaluated for charge-discharge cycle characteristics.
20 Each battery was charged at 25 $^{\circ}\text{C}$ at a current of 1 mA to 4.2 V and then discharged at a current of 1 mA to 2.7 V. This was recorded as a unit cycle of charge and discharge. The battery was cycled to determine the number of cycles after which its discharge capacity fell down to 80 % of its first-
25 cycle discharge capacity and the determined cycle number was

recorded as a cycle life. The results are shown in Table 12. The cycle life of each battery is indicated therein by an index when that of the battery E1 is taken as 100.

5

Table 12

Battery	Cycle Life
E1 (Under Hydrogen Atmosphere)	100
E2 (Under Hydrogen Atmosphere)	113
E3 (Under Hydrogen Atmosphere)	120
E4 (Under Hydrogen Atmosphere)	112
E5 (Under Hydrogen Atmosphere)	99
E6 (Under Hydrogen Atmosphere)	97
E7 (Under Hydrogen Atmosphere)	99
E8 (Under Hydrogen Atmosphere)	96
E9 (Under Hydrogen Atmosphere)	92
E10 (Under Hydrogen Atmosphere)	97
F1 (Under Argon Atmosphere)	75
F2 (Without Heat Treatment)	15

As apparent from Table 12, the battery E1 with the negative electrode made via the heat treatment under hydrogen atmosphere shows the improved cycle characteristics compared to the battery F1 with the negative electrode made via the heat treatment under argon atmosphere and the battery F2 with the negative electrode made without the heat treatment. This is probably because the heat treatment under hydrogen atmosphere has improved adhesion between the copper foil, active material and copper powder and as a result improved current collecting capability.

EXPERIMENT 23

The effect of the surface roughness Ra of the current collector on the cycle characteristic was studied in this Experiment.

5 The procedure of Experiment 17 was followed, except that the electrolytic copper foil with a surface roughness Ra of 0.5 μm was replaced by an electrolytic copper foil having a surface roughness Ra of 0.2 μm or a rolled copper foil having a surface roughness Ra of 0.1 μm , to construct
10 batteries E11 and E12. These batteries were evaluated for cycle characteristics in the same manner as described above. The cycle life of each battery is indicated by an index when that of the battery E1 is taken as 100. In Table 13, the cycle life of the battery E1 is also shown.

15

Table 13

Battery	Cycle Life
E1 (Surface Roughness Ra : 0.5 μm)	100
E11 (Surface Roughness Ra : 0.2 μm)	83
E12 (Surface Roughness Ra : 0.1 μm)	62

As can be clearly seen from Table 13, the batteries E1 and E11 with the negative electrode using the copper foil
20 having a surface roughness Ra of 0.2 μm or larger exhibit the longer cycle lives compared to the battery E12 with the negative electrode using the copper foil having the smaller surface roughness Ra. These are believed to suggest that

the use of a metal foil having a larger surface roughness Ra as a current collector results in the more effective sintering between the metal foil, active material and copper powder that improves adhesion therebetween.

5 EXPERIMENT 24

 In this Experiment, the effect of the loadings of the conductive metal powder on the cycle characteristics was studied.

 The procedure of Experiment 17 was followed, except
10 that the weight of the flaky copper powder loaded per unit weight of the silicon powder was varied to 1 (50 % by weight of copper powder), 0.5 (33.3 % by weight of copper powder) and 0.125 (11.1 % by weight of copper powder), to construct batteries E13, E14 and E15. For a comparative purpose, the
15 procedure of Experiment 17 was followed, except that the flaky copper powder was excluded and only the silicon powder was used, to construct a battery F3.

 These batteries were evaluated for cycle characteristics in the same manner as described above. The
20 results are given in Table 14. The cycle life of each battery is indicated by an index when that of the battery E1 is taken as 100.

Table 14

Battery	Cycle Life
E1 (Copper Powder Content : 20 Weight %)	100
E13 (Copper Powder Content : 50 Weight %)	145
E14 (Copper Powder Content : 30.3 Weight %)	124
E15 (Copper Powder Content : 11.1 Weight %)	90
F3 (Copper Powder Content : 0 Weight %)	31

As can be clearly seen from Table 14, the batteries E1 and E13 - E15 with the negative electrodes containing the flaky copper powder exhibit far superior cycle characteristics compared to the battery F3 with the negative electrode excluding the flaky copper powder. This is believed to have resulted from the addition of the copper powder that improved adhesion between the silicon powder particles as the active material particles, led to the formation of a solid conductive network surrounding the silicon powder particles and as a result improved the capability of current collection.

UTILITY IN INDUSTRY

In accordance with the present invention, a negative electrode for a rechargeable lithium battery, as well as a rechargeable lithium battery, can be provided which exhibits a high discharge capacity and excellent cycle characteristics.

THE EMBODIMENTS OF THE PRESENT INVENTION IN WHICH AN EXCLUSIVE PROPERTY OR PRIVILEGE IS CLAIMED ARE DEFINED AS FOLLOWS:

1. A negative electrode for a rechargeable lithium battery including a conductive metal foil having a surface roughness Ra of 0.2 μm or larger used as a current collector and a layer sinterized, under non-oxidizing or reducing atmosphere, and including active material particles containing silicon or a silicon alloy and a binder on a surface of said current collector under such conditions that said binder remains, after a heat treatment for sintering, without being fully decomposed, wherein a metal component in said conductive metal foil is diffused into said active material particles, and wherein a detectable level of copper silicide does not exist in regions of said active material particles where the metal component is diffused, when analyzed by X-ray diffractometry; and

wherein said heat treatment for sintering is carried out at a temperature within the range of 400°C to 500°C.

2. A negative electrode for a rechargeable lithium battery according to claim 1, wherein the layer including active material particles further includes a conductive metal powder in a ratio of 0.05 to 50 by weight to the active material particles.

3. The negative electrode for a rechargeable lithium battery as defined in claim 2, wherein said metal component

in said conductive metal powder is diffused into said active material particles.

4. The negative electrode for a rechargeable lithium battery as defined in claim 2 or 3, wherein said conductive metal powder contains copper or a copper alloy.

5. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 4, wherein said conductive metal foil comprises a copper foil, a copper alloy foil, a metal foil having a copper surface layer, or a metal foil having a copper alloy surface layer.

6. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 5, wherein said conductive metal foil comprises an electrolytic copper foil, an electrolytic copper alloy foil, a metal foil having an electrolytic copper surface, or a metal foil having an electrolytic copper alloy surface.

7. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 6, wherein said metal component diffused into the active material particles is copper.

8. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 7, wherein said active material particles penetrate into pits on said surface of the conductive metal foil.

9. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 8, wherein said binder is polyimide.

10. The negative electrode for a rechargeable lithium battery as defined in claim 9, wherein said polyimide is a condensate obtained by subjecting polyamic acid to a heat treatment for condensation.

11. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 8, wherein said binder is a fluoro-containing binder remaining after said heat treatment for the sintering.

12. The negative electrode for a rechargeable lithium battery as defined in claim 11, wherein said binder is polyvinylidene fluoride or polytetrafluoroethylene remaining after said heat treatment for the sintering.

13. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 12, wherein said binder penetrates into pits on said surface of the conductive metal foil.

14. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 13, wherein said active material particles have a mean particle diameter of up to 10 μm .

15. The negative electrode for a rechargeable lithium battery as defined in any one of claims 1 to 14, wherein said active material particles are composed of silicon.

16. A method for fabrication of a negative electrode for a rechargeable lithium battery, including the steps of:
providing a layer including active material particles containing silicon or a silicon alloy and a binder on a

surface of a conductive metal foil having a surface roughness Ra of 0.2 μm or larger; and

sintering, under non-oxidizing or reducing atmosphere, said layer of the active material particles and the binder while it is placed on the surface of the conductive metal foil under such conditions that said binder remains after a heat treatment without being fully decomposed; and

wherein said sintering is achieved by said heat treatment at a temperature within the range of 200°C-500°C.

17. A method for fabrication of a negative electrode for a rechargeable lithium battery according to claim 16, including the further step of:

providing a conductive metal powder in said layer of the active material particles and the binder, in a ratio of 0.05 to 50 by weight of the conductive metal powder to the active material particles.

18. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 17, wherein provision of a mixture layer on the surface of the conductive metal foil is achieved by coating a slurry containing the active material particles, the conductive metal powder and the binder on the surface of the conductive metal foil.

19. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 17 or 18, wherein said conductive metal powder contains copper or a copper alloy.

20. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 16, wherein provision of said layer of the active material particles and the binder on said surface of the conductive metal foil is achieved by coating a slurry containing the active material particles and the binder on the surface of the conductive metal foil.

21. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 16 or 17, wherein prior to the sintering step, said layer of the active material particles and the binder is rolled while it is placed on said surface of the conductive metal foil.

22. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 16 or 20, wherein prior to the sintering step, said layer of the active material particles and the binder is rolled while it is placed on said surface of the conductive metal foil.

23. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 22, wherein said conductive metal foil comprises a copper foil, a copper alloy foil, a metal foil having a copper surface layer, or a metal foil having a copper alloy surface layer.

24. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 23, wherein said conductive metal foil comprises an electrolytic copper foil, an electrolytic copper alloy foil, a metal foil having an electrolytic

copper surface, or a metal foil having an electrolytic copper alloy surface.

25. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 19, wherein said sintering causes a metal component in said conductive metal foil or said conductive metal powder to diffuse into said active material particles.

26. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 19 to 24, wherein said sintering causes a metal component in said conductive metal foil to diffuse into said active material particles.

27. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 25 or 26, wherein said sintering is carried out under such conditions that formation of an intermetallic compound between said metal component and silicon is not caused to occur in a level detectable by X-ray diffractometry.

28. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 25 to 27, wherein said metal component diffused into the active material particles is a copper element.

29. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 28, wherein said sintering is carried out under such conditions that formation of copper silicide is not caused to occur in a level detectable by X-ray diffractometry.

30. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 29, wherein said binder is polyimide.

31. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 30, wherein said polyimide is a condensate obtained by subjecting polyamic acid to a heat treatment for condensation.

32. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 29, wherein said binder is a fluoro-containing binder.

33. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in claim 32, wherein said binder is polyvinylidene fluoride or polytetrafluoroethylene.

34. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 33, wherein said active material particles have a mean particle diameter of up to 10 μm .

35. The method for fabrication of a negative electrode for a rechargeable lithium battery as defined in any one of claims 17 to 32, wherein said active material particles are composed of silicon.

36. A rechargeable lithium battery comprising the negative electrode defined in any one of claims 1 to 15 or a negative electrode fabricated by the practice of the method defined in any one of claims 16 to 35, a positive electrode

containing positive active material and a nonaqueous electrolyte.

37. The negative electrode for a rechargeable lithium battery as defined in claim 1, wherein said reducing atmosphere is hydrogen-containing atmosphere.

38. A method for fabricating a negative electrode for a rechargeable lithium battery according to claim 16, wherein said reducing atmosphere is hydrogen-containing atmosphere.

FIG. 1

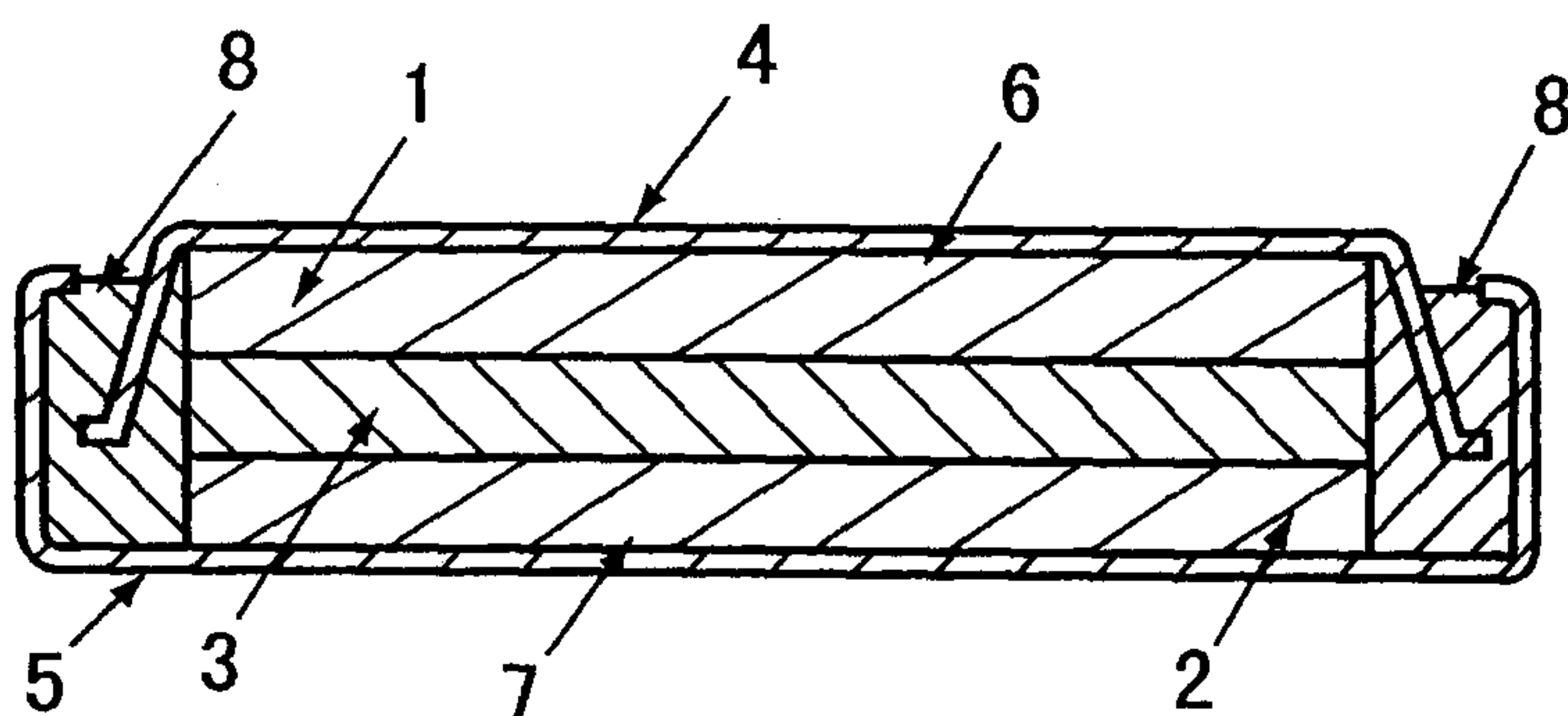


FIG. 2

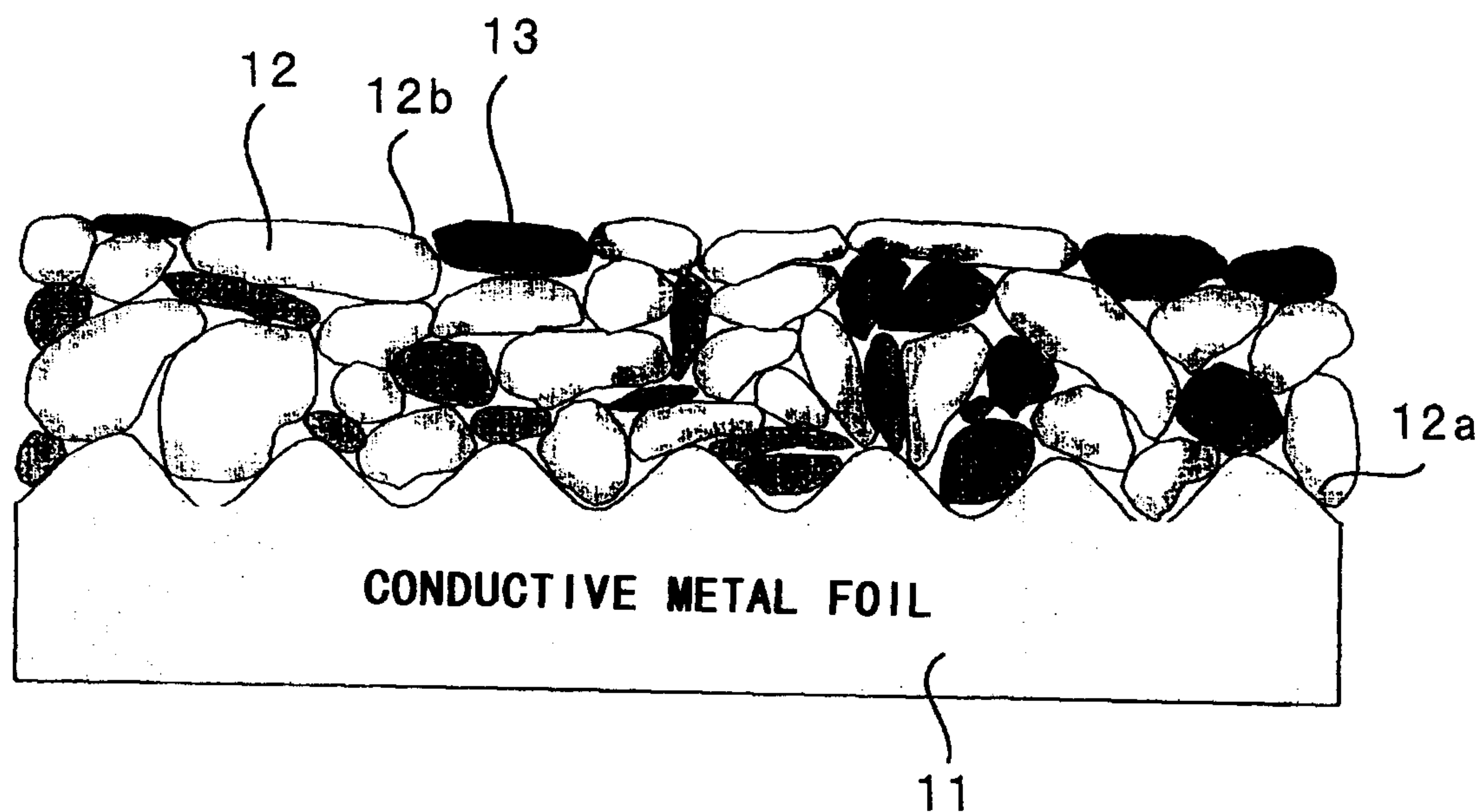


FIG. 3

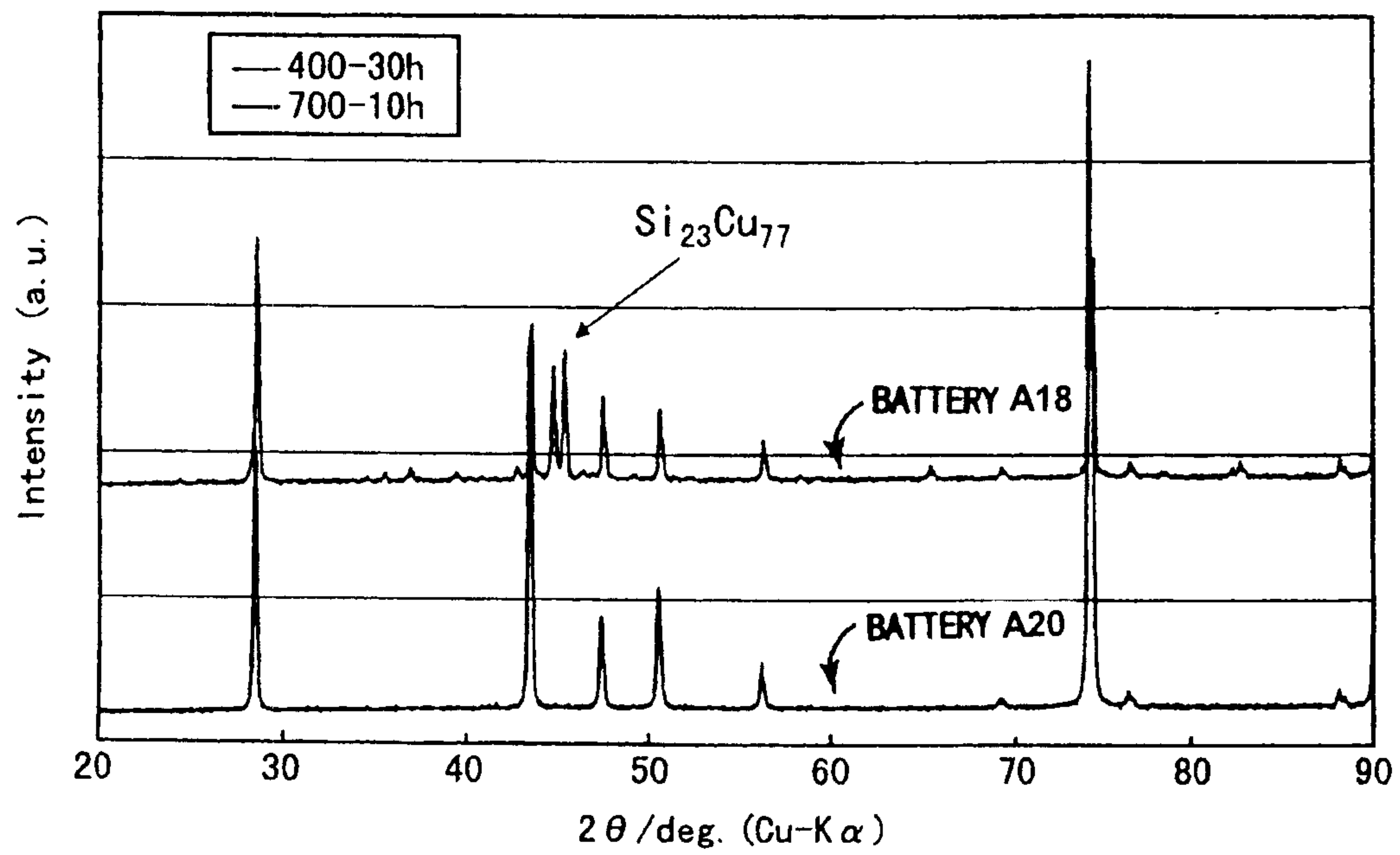
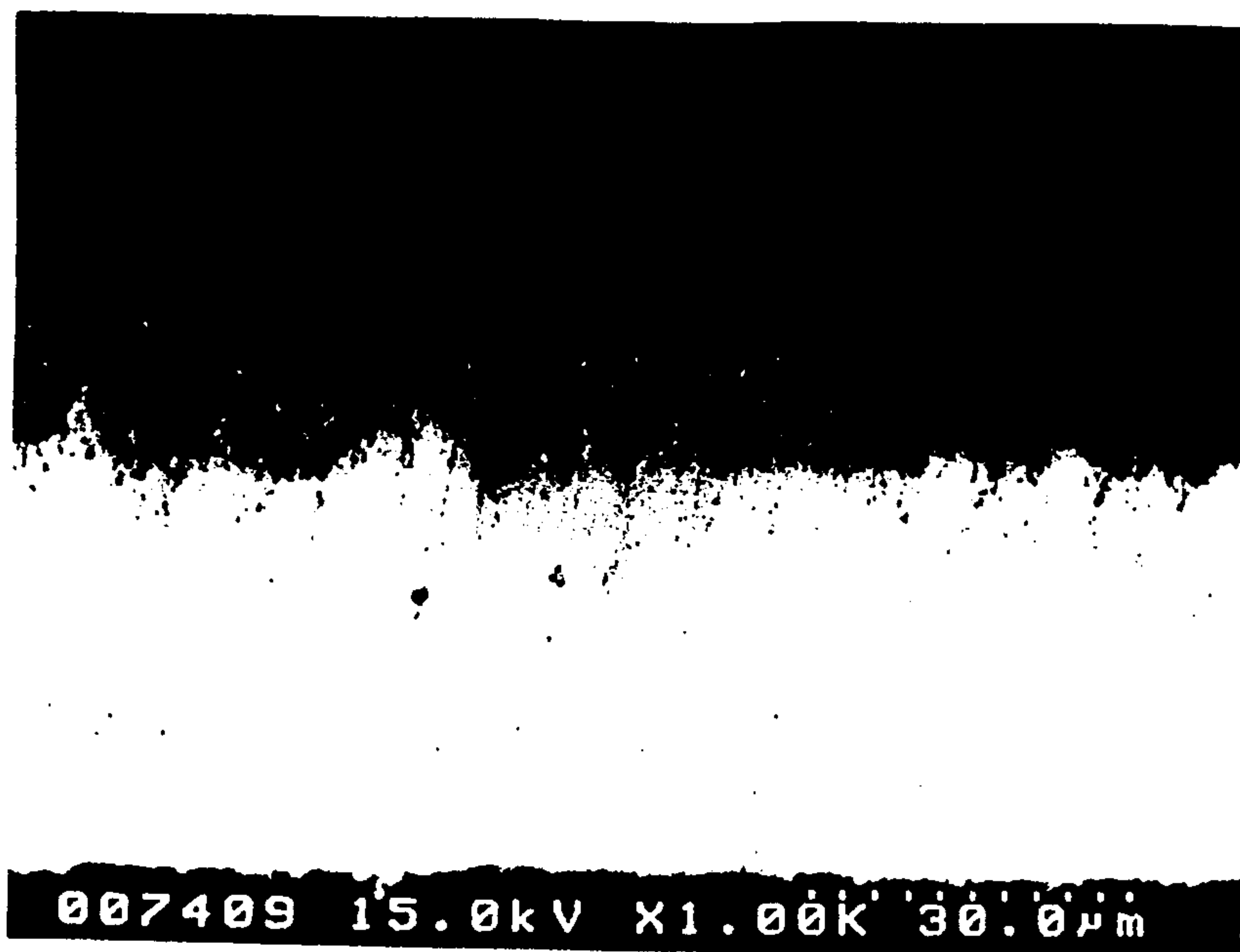


FIG. 4



REFLECTION ELECTRON IMAGE

× 1,000

FIG. 5



REFLECTION ELECTRON IMAGE

× 5,000

FIG. 6

