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METHOD AND APPARATUS FOR PURIFICATION OF WASTE GASES
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- (57) Claim

1. A method of purification of gases produced in a process containing pollutants comprising adding to the gases in or after the process a reagent and/or an absorbent for reacting with the pollutants contained in the gases, introducing the gases into a wetting reactor for wetting the gases with water or steam in order to activate the reagent and/or the absorbent contained in the gases, separating the reagent and/or absorbent particles, reacted either completely or partly, from the gases, further comprising introducing the gases into the wetting reactor at at least two locations so that a first portion of the gases is fed into a wetting zone where a suspension formed of the gas in the reagent and/or the absorbent is wet with water and/or steam, and the second portion of the gases is fed into a second zone disposed below the wetting zone, maintaining a particle suspension in the wetting zone by recycling particles separated from the gas to the wetting

(11) AU-B-72565/91
(10) 645528

-2-

zone, the particle density of the particle suspension being higher than the particle density of the gas fed into the wetting reactor, and discharging the gases from the wetting reactor at a location above the wetting zone.

25. An apparatus for purification of waste gases having been produced in a process comprising a wetting reactor which is provided with an inlet for waste gases to which gases a reagent and/or absorbent has been added for removing pollutants contained in said gases, water or steam sprays which provide a wetting zone for activating the reagent and/or absorbent, a gas outlet above the wetting zone, and a filter disposed in the upper section of the wetting reactor, for separating solid particles from gases and for returning the solid particles to the lower section of the wetting reactor, and an outlet for the particles separated from the gases, disposed in the lower section of the wetting reactor, wherein the wetting reactor is provided with gas inlets disposed on at least two different elevations so that at least one gas inlet is disposed in the wetting zone and at least another gas inlet is disposed in a second zone below the wetting zone.

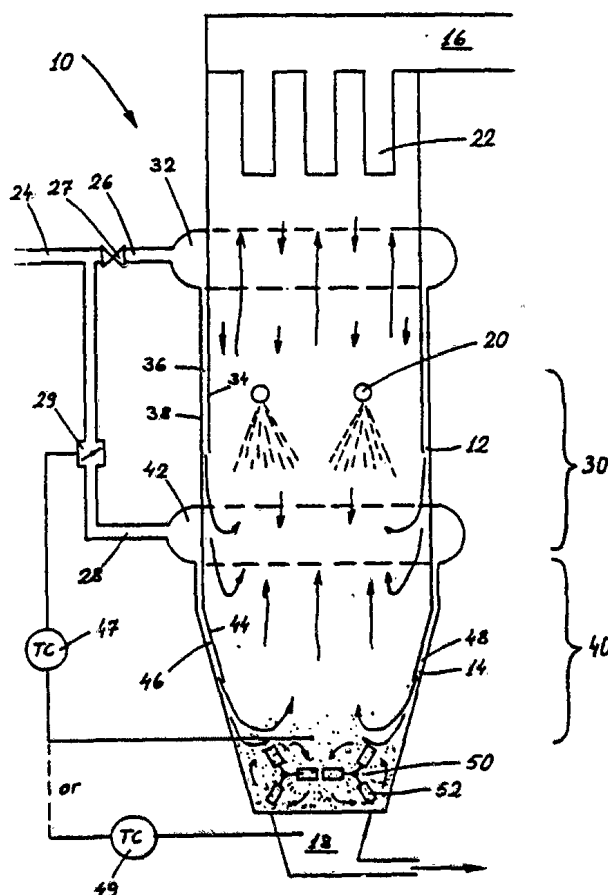
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(54) Title: METHOD AND APPARATUS FOR PURIFICATION OF WASTE GASES

(57) Abstract

Method and apparatus for purification of waste gases by adding reagent and/or absorbent, which reacts with the pollutants, to the gases and by introducing the gases into a wetting reactor (10) for activating the reagent or absorbent contained in the gases. Gases are conveyed to at least two levels through inlets (12, 14) in the wetting reactor so that a first portion of the gases is introduced into a wetting zone (30) and a second portion of the gases below the wetting zone. A high density of particles is maintained in the wetting zone by recycling particles separated from the gas to the wetting zone.



Method and apparatus for purification of waste gases

The present invention relates to a method of purification of waste gases which are produced in, for example, combustion, gasification, or some chemical or metallurgical processes. Sulfur dioxides, ammonia, chlorine and fluorine compounds and condensing hydrocarbon compounds are typical pollutants contained in these gases. The present invention especially relates to a method in which reagent or absorbent which reacts with pollutants contained in the gases is activated by leading the gases into a wetting reactor. The reagent or absorbent is added to the process itself or to the gases discharged from the process. The reagent or absorbent particles which have reacted either completely or partially are separated from the gases. Carbonates, oxides or hydroxides of, e.g., either alkali metals or alkaline earth metals are used as reagents or absorbents.

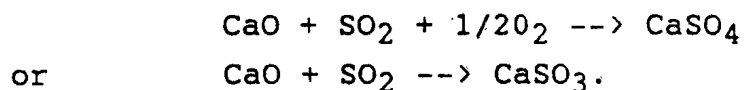
The present invention also relates to an apparatus for purification of waste gases. Especially, it relates to a wetting reactor which is provided with an inlet for waste gases and for reagent and/or absorbent, with spray means for water or steam, said spray means forming a wetting zone for activating the absorbent, with a filter disposed above the wetting zone in the upper section of the wetting reactor, for separating solid particles from the gases, and a gas outlet connected to the filter, and with an outlet or outlet duct for particles separated from the gases, disposed in the lower section of the wetting reactor.

As known, combustion of fossile fuels produces flue gases which contain sulfur dioxide and cause environmental acidification. The sulfur content of the flue gases varies depending on the sulfur content of the fuel. Efforts are made to find means for employing fuels which contain more and more sulfur even though the restrictions on sulfur emissions become tighter and tighter. Waste incineration plants, the number of which is continuously increasing,

also produce sulfur-containing flue gases which have to be purified so as to be within the set limits. The flue gases produced in waste incineration plants when, e.g., plastic compounds are burnt contain, besides SO₂ and SO₃ emissions, also hydrochloric and hydrofluoric acids and other harmful gaseous and solid compounds.

Process gases produced in various gasification processes may also contain harmful amounts of sulfuric or other compounds which have to be separated from the gases prior to further treatment thereof.

Several methods have been developed for cutting down sulfur emissions of combustion plants. The most common method used so far is wet scrubbing in which method the gases are scrubbed with a water suspension of a reagent, such as lime, reacting with, e.g., sulfur dioxides. The water suspension is sprayed into a gas flow in a scrubber arranged after a combustor, whereby sulfur is absorbed into the water suspension and sulfur dioxide reacts with lime, forming calcium sulphate or calcium sulphite



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Water suspension is sprayed in such an amount that sulfur compounds thus formed have not enough time to dry, but they are discharged as a slurry from the lower section of the scrubber. The wet scrubbing process is complicated as it requires means for preparing water suspension and means for after-treatment thereof. Furthermore, the method usually requires additional energy for drying the produced slurry in a slurry after-treatment plant. Therefore, the water suspension is usually fed into the system as dry as possible in order to minimize the energy requirement. Due to the considerable amount of water suspension used, the gas may be cooled to a relatively low temperature in the scrubber and, consequently, the gas discharged from the scrubber

may cause corrosion and clogging of filters. Further, energy is consumed for reheating the flue gases prior to leading them out of the system. In the wet scrubbing system, the separation degree of, for example, SO_2 , is about 95%.

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During the last few years, semi-dry scrubbing methods have been developed, in which a fine alkali suspension, e.g., calcium hydroxide suspension is sprayed through nozzles into a hot flue gas flow in a contact reactor where sulfur
10 oxides dissolve in water and, when the suspension dries, are bound to the lime compound. Water is evaporated in the contact reactor so as to form a solid waste, whereby reaction products of, for example, sulfur and lime are readily separable from the gases by means of a filter. It
15 is attempted to maintain the consistency of the calcium hydroxide suspension on such a level that the heat content of the flue gases is sufficient for evaporating the water therefrom. The thick lime suspension, however, easily deposits layers on the reactor walls and especially around
20 the spray nozzles, and may finally clog the nozzles entirely. The reactors have to be dimensioned relatively large for minimizing the drawbacks caused by deposits. Furthermore, as separate equipment is required for the production of lime suspension, a considerable amount of
25 equipment will be needed in the semi-dry scrubbing method as well, and the gas purification will be fairly expensive. A further drawback is the wearing effect of the lime suspension on the nozzles.

30 The semi-dry scrubbing method is advantageous for the process because the pollutants in the gases may be removed as dry waste. The process has drawbacks of being difficult to control and providing a sulfur absorption below 90%, which is less than in wet scrubbing. A still further
35 drawback is that inexpensive limestone cannot be used in the semi-dry method because it is very slow to react with sulfur. Either calcium oxide or calcium hydroxide, which

are much more expensive, have to be used instead. In big combustion plants, the cost of absorbent is remarkable.

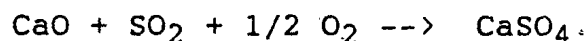
5 Addition of limestone already into the actual combustion or gasification stage has also been suggested. As a result of such addition, limestone is calcined into calcium oxide in accordance with the following reaction



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Calcium oxide is then capable of reacting already in the combustor with the sulfur oxides formed therein. The reaction takes place as follows:

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When the reactions proceed, calcium sulphate or calcium sulphite layers, however, cover the surface of the calcium oxide particles preventing sulfur from penetrating the particles, thereby slowing down and finally preventing the reactions between sulfur and lime. Thus, lime will not react completely and will not, therefore, be optimally utilized. Many other parameters, such as Ca/S mole ratio, temperature and retention time also affect sulfur
25 absorption.

The closer to the dew point the reactions take place, the higher the reactivity of alkali compounds becomes. Better reactivity is caused by the fact that, in a wetted particle, reactions take place in a water phase as fast ionic
30 reactions. Close to the dew point, the particles stay wetted and the reactivity also remains on a desired level for a longer time. The moistness of the particles is preferably maintained on such a high level that water surrounds the particles, also penetrating them. As the
35 water penetrates the lime particles, the sulphate or sulphite layer deposited on them will be broken, thereby revealing new reactive lime area. Sulfur dioxide contained

in the gases dissolves in the water surrounding the particles and reacts with calcium compounds in the liquid phase.

- 5 Finnish patent specification 78401 discloses a method in which sulfur dioxide of flue gases is caused to react in a reaction zone and to be thereby transformed into solid sulphates and sulphites separable from the flue gases. The flue gases are conducted into the lower section of a
10 vertical, lengthy contact reactor. Additionally, powdered lime and water are separately brought into the reactor from several points for the sulfur to be absorbed by lime. Flue gas suspensions are discharged from the upper section of the flow-through reactor and are further conducted to a
15 dust separation stage. By feeding the powdered lime and water separately into the reactor, production, treatment, and spraying of a water suspension are avoided. According to the specification, this method, when used in sulfur absorption with calcium oxide, results in about 80% SO₂
20 reduction with a mole ratio of Ca/S = 1.56 and about 90% SO₂ reduction with a mole ratio of Ca/S = 2.22. The 98% SO₂ reduction is not achieved until the mole ratio is Ca/S = 4. In this method either, the temperature of the flue gas flow must not be allowed to drop optimally close to
25 the dew point as the solids contained in the flue gas suspension then would deposit layers on the walls of the tubes and other equipment, thus causing troubles in dust separation.
- 30 European patent specification 0 104 335 discloses another two-phase, semi-dry flue gas purification system. In this method, dry reagent is fed into the flue gases in a contact reactor in a first stage and water or an aqueous solution, to which dissolved reagent has been added, in a second
35 stage. In the first stage, an inactive surface layer is formed on the reagent particles. The layer slows down or prevents reactions between the reagent and, e.g., sulfur oxide. By adding water in the second stage, the reagent

is reactivated. In this manner, the reagent is utilized more completely. The gas temperature is allowed to decrease to a level on which it always stays above the dew point, for example, to 105°C. The gas temperature must not, in this method either, be allowed to decrease too close to the dew point because any wetted particles possibly formed would cause difficulties in the long run, even if the reactivity of the reagent at a lower temperature would be much better. According to the method, the required amount of reagent may be reduced by recycling reagent-containing solid material which has been separated from the gas at a later stage and then regenerated by either grinding or some other way. A drawback of this method is, however, separate equipment needed for handling and storing of the recycled solids.

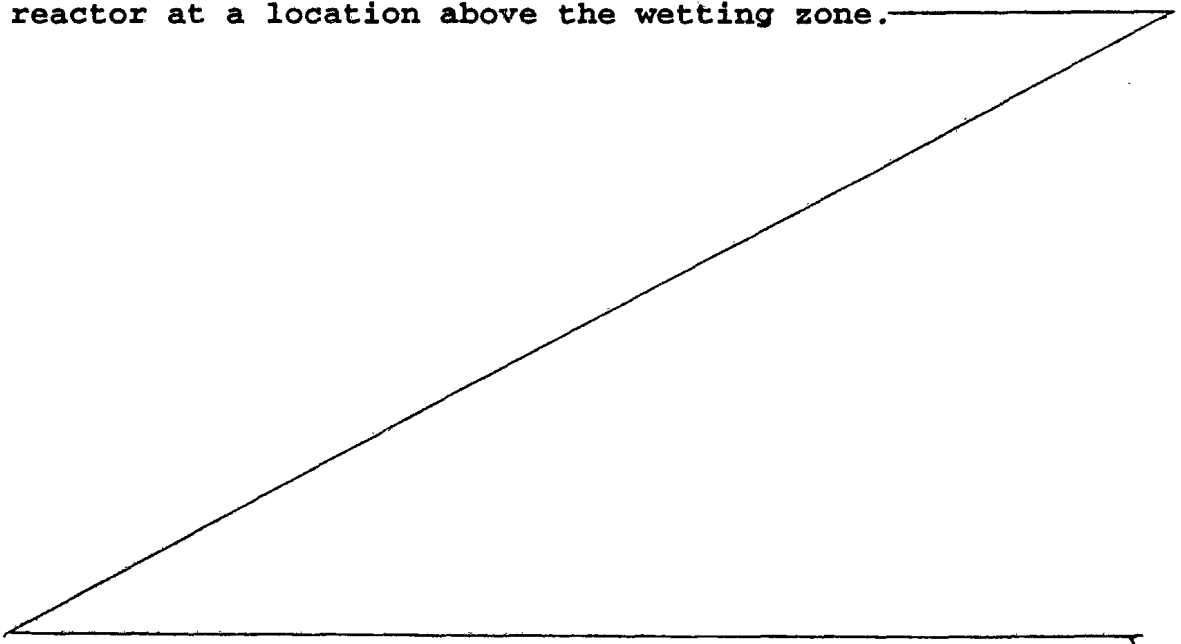
U.S. patent specification 4,509,049 suggests a dry gas purification system in which lime is added to flue gases in a boiler and the lime is then allowed to react with the flue gases in a reactor. The lime, which has partly reacted with the pollutants in the flue gases, is separated from the gases in a filter in the upper section of the reactor. The dry lime thus separated from the gases is accumulated in the base portion of the reactor or into a separate chamber where it is ground and treated with dry steam in order to increase the reactivity of the dry lime, whereafter the lime is recycled into the gas flow at a location prior to the reactor. The dry steam treatment of lime takes 2 to 24 hours, which is a long time involving high consumption of energy.

~~An object of the present invention is to provide an improved method of purification of waste gases, such as sulfur, chlorine and fluorine compounds or other condensable compounds.~~

~~Another object of the invention is to provide a method by which, e.g., sulfur reduction can be considerably improved,~~



According to the present invention there is provided a method of purification of gases produced in a process containing pollutants comprising adding to the gases in or after the process a reagent and/or an absorbent for
5 reacting with the pollutants contained in the gases, introducing the gases into a wetting reactor for wetting the gases with water or steam in order to activate the reagent and/or the absorbent contained in the gases, separating the reagent and/or absorbent particles, reacted
10 either completely or partly, from the gases, further comprising introducing the gases into the wetting reactor at at least two locations so that a first portion of the gases is fed into a wetting zone where a suspension formed of the gas in the reagent and/or the absorbent is wet with
15 water and/or steam, and the second portion of the gases is fed into a second zone disposed below the wetting zone, maintaining a particle suspension in the wetting zone by recycling particles separated from the gas to the wetting zone, the particle density of the particle suspension being
20 higher than the particle density of the gas fed into the wetting reactor, and discharging the gases from the wetting reactor at a location above the wetting zone.



The second portion of the gases preferably serves as a drying gas and is brought into contact with and to dry wetted particles flowing downwardly from the wetting zone. At least a part of the downwardly flowing particles is then
5 carried away by the upwardly flowing drying gas and conveyed back upwards into the wetting zone in order to activate the still unreacted reagent or absorbent. In the upper section of the wetting reactor, the particles are separated from the gases by means of a filter and are then returned
10 to the lower section of the reactor. In this way, an internal circulation of reagent or absorbent particles is brought about in the wetting reactor and a relatively high density of particles is maintained therein.

15 The particles are separated from the gas in a fabric filter, electric filter or some other equivalent type of separator. Particles are detached from the filter either intermittently or continuously, e.g., by pulse flushing, backwash or shaking, whereby the particles drop either separately or
20 in lumps downwards in the wetting reactor.

At least a part of the particles stick to each other in the wetting zone or at the filter and form bigger agglomerates and pass thereafter downwards through the wetting zone all
25 the way to the lower section of the reactor, whereas single small particles are easily carried away by the upwardly flowing gas and are conveyed from the wetting zone into the upper section of the reactor. Bigger lumps of particles and wet, heavy particles are dried and ground into finer
30 particulates by the drying gas or by other mixing when they reach the lower section of the reactor.

The drying gas is preferably introduced into the lower section of the reactor, first as downwardly directed sprays.
35 The drying gas dries, grinds and causes whirling of the particles accumulated in the lower section of the reactor. Thorough mixing of the particles in the lower section of the reactor gives a positive effect, equalizing heat and

moistness in the particle suspension. As the particles are ground smaller, their reactive area increases. After this, at least a part of the particles are carried away with the drying gases, passing again through the wetting zone, whereby the particles are activated and will again be capable of absorbing sulfur in the reaction zone.

Mixing and recycling of the particles increases the retention time, dust density, Ca/S mole ratio and total surface area of the lime particles in the reaction zone, thereby decreasing the need for new reagent. According to the invention, an average particle density is maintained by internal circulation in the wetting reactor, which density is clearly higher than the particle density in the gas introduced into the reactor. The internal circulation can be controlled by regulating the amount and velocity of the gas introduced into the drying section. The location of the feeding point of the drying gas also has an effect on the recycling. The shorter the distance from which the gas spray is directed to the particle layer, the stronger the whirling effect of the spray.

Part of the particles is preferably removed from the reactor through an outlet disposed in the lower section of the wetting reactor below the drying zone. Part of the discharged particles may be returned to the wetting reactor if desired. Thus, external circulation of particles may also be provided in connection with the wetting reactor. Particles may be treated outside the reactor, for example, to regenerate some reagent. The particle density may also be controlled in the reactor by regulating the amount of particles removed from the lower section of the reactor.

External particle circulation in the wetting reactor may be provided by connecting a filter or an equivalent particle separator, which is either totally or partly disposed outside the reactor, to the upper section of the wetting reactor. In such a filter or particle separator, reacted

- and still unreacted absorbent particles are separated from the gases, at least part of which particles is directly returned to the lower section of the wetting reactor, preferably to the drying zone. Particles may be detached from the filter either continuously or intermittently and be returned to the lower section of the wetting reactor. Part of the material separated by means of the particle separator may be totally removed from the system.
- 10 By the method according to the invention, it is possible to decrease the average temperature of the gases in the wetting reactor to a level which is about 0 - 20°C, preferably 0 - 10°C, from the dew point, and even to the actual dew point, and still to avoid the drawbacks caused by too wet particles in the upper or lower sections of the reactor. The particles wetted in the wetting zone and falling downwardly are dried by the drying gas in the drying zone, thereby not causing any trouble in the lower section of the reactor. Due to recycling, the differences in temperature and moistness are very small also above the wetting zone, at various cross-sectional points of the reactor. In this way, local troubles caused by wetted particles or water drops are avoided.
- 25 The relative amounts of gas introduced into different zones of the wetting reactor may vary according to the temperature and composition of the gases. The ratio of the amount of gas introduced into the wetting zone to the amount of drying gas is about 10:1 - 1:5. Mostly, it is advantageous to introduce more gas into the wetting zone than into the drying zone, e.g., so that about 60 % of the gas is fed into the wetting zone. A small part of the gas, preferably < 10 %, may be fed to a zone above the wetting zone to make sure that the upwardly flowing gas suspension is dry enough when entering the filter. The absorbent cake or absorbent layer formed on the filter contains partly reactive absorbent, which is capable of absorbing a significant part of the sulfur contained in this added gas.

In accordance with a preferred embodiment of the invention, layers formed by wetted particles on the walls of the wetting reactor may be avoided in such a manner that at least a part of the gas fed into the wetting zone is conducted into the wetting reactor as jacket flow so that the gases, either indirectly or directly, heat the reactor walls. The gas is conducted into the reactor through ducts disposed, e.g., in the walls, whereby the hot gas flowing in the ducts prevents the walls from cooling and thereby solids from depositing layers on the walls. The gases may also be injected directly to the inside of the reactor and caused to flow downwardly along the walls, protecting the walls. Thereby, the wetted particles are either directed away from the wall or they dry when passing through the jacket flow prior to touching the wall. The jacket flow is brought about by feeding gas, e.g., into a cylindrical reactor via an annular opening in its wall.

Removing of deposits from the walls may also be intensified by shaking or by constructing the walls of flexible material, whereby pressure fluctuations normally occurring in the system will shake the walls, causing the deposits to fall down.

Especially in big reactors, gas may also be introduced into the inner part of the wetting zone for providing a gas distribution as even as possible in the reactor. Gas may be fed, e.g., through a plurality of nozzles or slots disposed in the gas duct in the middle part of the reactor. Gas may also be fed into the wetting reactor from more than two levels.

Gas may be introduced also into the drying zone as jacket flow or it may be introduced into the inner part of the drying section for ensuring even distribution of the gas.

By sprays of water or steam, a wetting zone is provided in the upper or middle section of the wetting reactor. Water is preferably sprayed into the flue gases, mainly downwards from above the gas inlets. Sprays of water or steam are preferably so arranged that as much as possible of the gas flow is evenly covered.

An apparatus for implementing the method of the invention is preferably a wetting reactor, which is characterized in that gas inlets are disposed in the wetting reactor at least at two different elevations. At least one inlet, e.g., an annular or rectangular opening following the outer wall of the reactor, is disposed in the wetting zone. The wetting zone may also be provided with one or more inlets into the inner part of the reactor so that gas will be distributed evenly over the entire cross-sectional area of the reactor. At least one second inlet for the reactor is disposed below the wetting zone in the drying or mixing zone. This second inlet opening may be disposed in the reactor wall or inside the reactor, or in both of them.

The wetting reactor may be either totally or partly double-walled so that in the wall there is formed an inlet duct or inlet ducts for the gas to be fed into the reactor.

The wetting zone of the wetting reactor is preferably provided with downwardly directed water or water vapor nozzles, disposed, for example, in the support members running horizontally through the wetting reactor.

The filter disposed in the upper section of the wetting reactor is preferably a fabric filter such as a hose or cassette filter, or possibly an electric or some other equivalent type of filter, wherefrom particles are returned to the lower section of the reactor by shaking or back-blowing the filter.

The lower section of the reactor is preferably provided with a mechanical mixer, mixing solid material accumulated in the lower section of the reactor. Mixing of solid material intensifies the equalization of the moistness and heat of the particles, whereby the particles which are still wet will be dried when coming into contact with drier and hotter particles. At the same time, the mixer breaks the lumps of particles so as to facilitate them to be conveyed upwards in the reactor by the gas flow. Thus, the mixer intensifies the effect of the drying gas for bringing about internal circulation of particles in the reactor. The speed of the mixer is adjustable, and together with the gas flow entering the mixing area, a wide range of adjustment of particle circulation is thereby provided.

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The lower section of the wetting reactor is provided with means for discharging particles from the reactor. Particles are preferably discharged by the mixer described above. The blades of the mixer can be directed askew so that they gradually move particles to one end of the lower section of the reactor, wherefrom the particles can be removed dry through a suitable sealing means. They may also be removed by a separate discharge screw or a discharge conveyor. Particles are discharged from the wetting reactor preferably in such a dry state that they can be further conveyed, for example, pneumatically.

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If necessary, the lower section of the wetting reactor may be provided with a separate feeding point for reagent or absorbent. Several different reagents may be introduced into the wetting reactor for removing harmful substances from the gases in one stage.

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The arrangement according to the invention provides e.g. the following advantages over the earlier known arrangements:

- Several functions, such as sulfur absorption, wetting of reagent, particle separation and drying, may be concentrated in one apparatus. Wetting of gas may be

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arranged in the same space as the existing ash separation, whereby neither extra devices nor separate reactors are needed for each partial process.

- By the present invention, it is possible to operate very close to the dew point, even almost at the dew point, as the filter is directly arranged in the reactor, and no gas ducts are needed, whereby the problem of layers depositing on the walls of such gas ducts is avoided in conveyance of gas which becomes wet when close to the dew point. The possibility of operating close to the dew point results in a highly efficient elimination of SO_2 , SO_3 , HCl and HF emissions.

- Internal circulation of particles through the wetting zone cuts down the consumption of reagent or absorbent. By this method, the retention time of the absorbent in the reactor becomes essentially longer, preferably about 2 to 10 times longer in comparison with earlier known once-through reactors.

- Fine ash is also separated from the gases in this apparatus. Ash and consumed absorbent may be recovered dry and in a common step. Only one ash removal system and ash treatment is needed. Dry ash and absorbent may be conveyed pneumatically.

- In the earlier known methods, only if the SO_2 content of the inlet gas has been < 40 ppm, almost complete sulfur absorption has been provided in the wetting stage with SO_2 containing gases. By the method of the invention, complete sulfur removal is possible even though the SO_2 content of the inlet gas is > 100 ppm.

- The method and the apparatus are simple.

In the arrangement according to the invention, three main factors having an positive effect on absorbing reactions may be used simultaneously and optimally:

- cooling of gas to a temperature level which is close to the dew point in order to provide fast reactions;
- high Ca/S mole ratio in the reaction zone; and

- long retention time for optimal utilization of the absorbent.

The invention is further described below, by way of example, with reference to the accompanying schematic drawings, in which

Fig. 1 is a schematic illustration of a preferred apparatus for implementing the method of the invention.

Figs. 2 and 3 are schematic illustrations of two other apparatuses for implementing the method of the invention, and

Fig. 4 shows the ratio of SO₂ reduction to Ca/S mole ratio in an embodiment of the invention.

Fig. 1 discloses a wetting reactor 10 provided with gas inlets 12 and 14, a gas outlet duct 16 and a discharge duct 18 for particles separated from the gas. The wetting reactor is also provided with nozzles 20 for spraying water or steam into the wetting reactor above the gas inlets. The upper section of the reactor is provided with a filter 22 for separating particles from the upwardly flowing gas.

The wetting reactor according to the invention may be disposed in the flue gas duct after the combustion chamber of a grate furnace, pulverized fuel combustor or fluidized bed combustor, such as a circulating fluidized bed reactor, whereby the wetting reactor is preferably disposed after the heat recovery boiler. Prior to entering the wetting reactor, the flue gases are cooled to < 300°C, preferably to < 150°C. For removing sulfur oxides from the flue gases, absorbent, such as limestone, has been fed into the combustion chamber or fluidized bed reactor or thereafter. The absorbent is at least partly calcined in hot flue gas to calcium oxide, which absorbs sulfur as calcium sulphate

and calcium sulphite. The lime/sulfur ratio of 1.5 - 2.1 produces about 80 to 95 % sulfur reduction in a circulating fluidized bed reactor. The flue gases still contain sulfur as well as unreacted lime when entering the wetting reactor.

5 An important object of the wetting reactor according to the invention is to activate lime or other absorbent in the flue gases so that the rest of the sulfur will also be removable from the flue gases.

10 In the arrangement shown in Fig. 1, flue gases containing sulfur and lime are conveyed through pipe 24 into the wetting reactor. Prior to feeding the flue gases into the reactor, they are divided into two separate flue gas flows in ducts 26 and 28. The flue gas flow in duct 26 is
15 conducted into the reactor, substantially to the same level as the water sprays 20. The flue gas flow in duct 28 is conducted to a substantially lower level.

The main flue gas flow is conducted into the wetting reactor
20 substantially to the same level as the water sprays, either above or below or to exactly the same level as the water sprays. It is essential that the gas fed into the reactor is well mixed with the water spray. Both the gas and the water are preferably fed into the reactor as a downwardly
25 flowing spray, which, at a small distance from the inlet, turns upwards. In this manner, vortices of gas and water spray are provided in the wetting zone and thereby also a good mixing effect.

30 The water sprays constitute a wetting zone 30 in the wetting reactor. In this wetting zone, the flue gases are wetted and cooled as close to the dew point thereof as possible, preferably to about 0 - 3°C therefrom. In the wetting zone, the lime particles are wetted, whereby sulfur is
35 absorbed by the particles and fast ionic reactions between sulfur and calcium can take place in the liquid phase.

Water is preferably sprayed from nozzles; which produce small drops, preferably $< 100 \mu\text{m}$ in size, and which are large-angled so that the reactor cross-section and the gas flow are well covered. Water is sprayed downwardly. The wetting zone covers the vertical zone of the reactor which preferably equals the hydraulic diameter of the reactor.

In the embodiment shown in Fig. 1, flue gas is introduced into the reactor as jacket flow. From duct 26 the gas is first conveyed into a tubular duct 32 surrounding the reactor. From the tubular duct, the gases are further conveyed into one or more downwardly directed ducts 36 defined by the reactor wall 34. The reactor is double-walled so as to form an inlet duct 36 for flue gas between the walls 34 and 38. From ducts 36, the flue gases are conveyed through inlets 12 into the wetting zone 30 in the reactor.

Correspondingly, gas is conducted from the lower gas duct 28 to a tubular duct 42 surrounding the reactor and therefrom further to a downwardly directed duct 46 defined by the reactor walls 44. From that duct 46, the flue gases flow into the lower section i.e. the drying or mixing zone 40, of the reactor.

Introduction of gas into the wetting reactor is controllable, e.g., by means of dampers 27 and 29 in ducts 26 and 28. Introduction of gas is also controllable by means of an adjustable slot 48 in the duct 46.

Drying gas can be fed into the drying section to such an extent that the particles accumulated in the lower section of the reactor stay mainly dry. The temperature in the lower section of the reactor is then maintained above the dew point for providing efficient drying. The gases flow from the drying zone upwards, thereby drying particles flowing downwardly from the filter and the wetting zone. The flow of drying gas is automatically adjustable by

members 47 and 49, in accordance with the temperature of the gas in the lower section of the reactor or the temperature of the particles to be discharged.

5 Further, the lower section of the reactor is equipped with mechanical mixers 50. The embodiment shown in Fig. 1 has two such mixers lying on the bottom of the reactor and being provided with blades 52. The mixers break the lumps of particles falling down to the lower section of the
10 reactor. At the same time, they equalize the temperature and moistness between the particles. The mixer blades are preferably so disposed that they, when rotating, move particles to one end of the lower section of the reactor, said end being provided with a discharge duct 18 for
15 particles. The particles preferably flow over an over-flow plate, not disclosed, into the discharge duct. In this manner, a "buffer" of particles, which equalizes the temperature and moistness of the down-flowing particles, is always maintained in the reactor.

20

Fig. 2 shows a wetting reactor 10 similar to that of Fig. 1, except that gas is introduced into the drying section via a gas inlet duct 54 disposed inside the reactor. The gas inlet duct is provided with downwardly directed nozzles
25 56, through which the gas first flows towards the particles accumulated in the lower section of the reactor and thereafter upwards. In this way, mixing is provided among the particles accumulated in the lower section of the reactor.

30

In the reactor according to Fig. 2, the amount of water fed into the wetting zone is regulated by a member 21 according to the temperature of the gas in the upper section of the reactor. The wetting reactor may be provided with water
35 nozzles on several different levels if required for the gas to be evenly wetted.

In Figs. 1 and 2, the reactors are made up of hose filter chambers, each of which has a standard filter and, in the lower section of the chamber, a wetting zone and a drying zone.

5

Fig. 3 illustrates a reactor in which a filter 60 is disposed immediately outside the reactor chamber. Thus, in addition to internal circulation, also external circulation of particles is effected in the reactor. Some of the particles wetted in the wetting zone 30 separate from the gases by themselves and flow, because of their weight, down to the drying section, where they become under the influence of the drying gas. After drying, the particles again flow upwards, entrained with the gases, thereby constituting internal circulation. Part of the wetted particles follow the gases to the upper section of the reactor and to the filter 60 and will be returned via duct 62 to the drying section 40. If necessary, particles may be removed from the circulation by outlet means 64, which may be closed by a valve 66. Particles may also be wetted outside the wetting reactor.

In Fig. 3, the flue gas inlet ducts 26 and 28 may be connected to different points of the combustion processes, for example so that, the gas brought into the reactor via duct 26 has been more cooled than the gas brought via duct 28, which duct may bring hotter gas for ensuring the drying process.

Compared with the prior art, the invention provides much better sulfur absorption of flue gases with much lower lime consumption, as indicated by the accompanying results of tests made on certain coal and limestone grades.

35 Example

Means in accordance with Fig. 1 was used in the test run. The wetting reactor was supplied with flue gases of about

870°C from a circulating fluidized bed reactor, which had been supplied with limestone the mole ratio Ca/S being 1.41 - 2.33. The theoretic SO₂ content of the flue gases was 860 to 960 ppm. The sulfur contained in the flue gases reacted already in the circulating fluidized bed reactor prior to the wetting reactor in such a manner that the SO₂ content of the flue gases entering the wetting reactor was about 60 to 201 ppm. The gases were conducted into the wetting reactor at a temperature of about 130 to 160°C. The theoretic dew point of the gases in the wetting reactor was about 54°C.

The test results are shown by the table below.

	Ca/S	Temp. after reactor mol/mol	SO ₂ before reactor ppm	SO ₂ after reactor ppm	SO ₂ abs. %
15		°C			
20	1.88	55	201	27	97
	1.91	55	111	2	100
	1.95	55	107	0	100
	1.94	57	105	0	100
	2.33	57	129	2	100
25	1.93	59	60	0	100
	1.41	61	183	83	91
	1.87	63	121	25	97
	2.00	66	136	61	93
	2.08	81	77	53	95
30	-----				

The test results clearly indicate that, by the method according to the invention, sulfur absorption is almost complete even with very low Ca/S mole ratios when the final reactions take place nearly at the dew point, i.e. 1-5°C from the dew point. Very good results are achieved even with the highest temperatures, i.e. 10-30°C from the

dew point, and with much lower lime consumption than in earlier known methods.

According to information in literature, the wetting reactors
5 of prior art have given about 90% SO₂ reduction with a mole ratio of Ca/S = 2.22. About 98% SO₂ reduction has not been achieved until the mole ratio has been Ca/S = 4.

Fig. 4 shows the ratio of SO₂ reduction to Ca/S mole ratio
10 received in the above described series of test runs when applying the method according to the invention. As a comparison, the figure also shows the ratio of SO₂ reduction to the Ca/S mole ratio when the test run is performed without the wetting reactor.

15

As a conclusion, the present invention enables combining of various stages of several different processes into a whole:

- A wetting reactor, made up of the space below the filter cassettes or the like. A nozzle system disposed in this
20 space sprays water for wetting the ash and absorbent particles and for dropping the flue gas temperature close to the dew point, i.e. 0-20°C therefrom.
- A fabric filter or the like, which operates either on the ordinary counterflow cleaning principle, with pressure
25 pulses, backwash or shaking.
- Combined mixing and transfer means for ash and absorbent, disposed, for example, in the receiving hopper at the bottom of the reactor. The mixing means preferably rotates at such a high velocity that it breaks the
30 deposits which, when wet, fall down from the walls and filter, and which are dried by the hot gas flow.
- Circulation of ash and absorbent, which is brought about by blowing part of the incoming flue gas into the reactor via the lower section thereof. Gas may also be blown
35 into the reactor from below the mixers in such a manner that the gas fluidizes the particle mass accumulated in the lower section of the reactor. The gas introduced into the reactor from the lower section thereof together

with the main gas flow coming from the side walls dries the wet lumps of particles falling down from the upper section of the wetting reactor. The gases catch part of the particles back into the wetting zone, thereby
5 resulting in an internal circulation of particles in the wetting reactor.

THE CLAIMS DEFINING THE INVENTION ARE AS FOLLOWS:

1. A method of purification of gases produced in a process containing pollutants comprising adding to the gases in or after the process a reagent and/or an absorbent for reacting with the pollutants contained in the gases, introducing the gases into a wetting reactor for wetting the gases with water or steam in order to activate the reagent and/or the absorbent contained in the gases, separating the reagent and/or absorbent particles, reacted either completely or partly, from the gases, further comprising introducing the gases into the wetting reactor at at least two locations so that a first portion of the gases is fed into a wetting zone where a suspension formed of the gas in the reagent and/or the absorbent is wet with water and/or steam, and the second portion of the gases is fed into a second zone disposed below the wetting zone, maintaining a particle suspension in the wetting zone by recycling particles separated from the gas to the wetting zone, the particle density of the particle suspension being higher than the particle density of the gas fed into the wetting reactor, and discharging the gases from the wetting reactor at a location above the wetting zone.
2. A method as claimed in claim 1, further comprising separating solid particles from the gases discharged from the wetting reactor in a filter disposed in the upper section of the wetting reactor, from which filter the separated particles are detached so that the particles may descend to the wetting zone and/or to the lower section of the wetting reactor.
3. A method as claimed in claim 2, in which particles are detached from the filter intermittently.



4. A method as claimed in claim 1, further comprising separating solid particles from the gases discharged from the wetting reactor in a separator disposed outside the wetting reactor, from which separator particles are recycled into the wetting reactor.

5. A method as claimed in any preceding claim in which the first portion of the gases is brought into contact with particles flowing downwardly from the wetting zone and is caused to dry them.

6. A method as claimed in any preceding claim in which the second portion of the gas, fed into the space below the wetting zone is caused to recycle part of the particles accumulated in the lower section of the reactor into the upper section thereof.

7. A method as claimed in any one of claims 1 to 5 in which the second portion of the gas fed into the space below the wetting zone is fed as one or more sprays which are at least partly directed downwardly so that the gas spray breaks lumps of particles accumulated in the lower section of the reactor and mixes particles.

8. A method as claimed in any preceding claim further comprising discharging particles from the lower section of the wetting reactor.

9. A method as claimed in claim 8, in which a part of the particles discharged from the lower section of the wetting reactor are recycled into the wetting reactor.

10. A method as claimed in claim 9, in which the



particles are wetted outside the wetting reactor prior to recycling them.

11. A method as claimed in any preceding claim
5 further comprising cooling the gases in the wetting reactor to a temperature of 0-20°C from the dew point.

12. A method as claimed in claim 11, in which the
10 gases are cooled to a temperature of 1-10°C from the dew point.

13. A method as claimed in any preceding claim in
which the ratio of the amount of gas fed into the wetting
zone to the amount of gas fed into a second zone is 10:1-
15 1:5.

14. A method as claimed in claim 13 in which the
amount of gas fed into the wetting zone is higher than the
amount of gas fed into the second zone.

20 15. A method as claimed in claim 14, in which about 60% of the gas is introduced into the wetting zone.

16. A method as claimed in any preceding claim
25 further comprising feeding at least a part of the gas to be introduced into the wetting zone into the wetting reactor as jacket flow so that the gas flows into the wetting zone through ducts disposed in the walls of the wetting reactor and/or along the walls of the wetting reactor as a
30 downwardly flowing spray, whereby the jacket flow prevents the walls from cooling and layers of solids from depositing on the walls.

17. A method as claimed in any one of claims 1 to 15



further comprising conducting at least a part of the gas to be introduced into the drying zone into the wetting reactor as jacket flow so that the gas flows into the drying zone via ducts disposed in the walls of the wetting reactor,
5 whereby cooling of the walls is prevented.

18. A method as claimed in any one of claims 1 to 15 further comprising conducting at least part of the drying gas to be introduced into the drying zone into the wetting
10 reactor through one or more nozzles disposed substantially in the middle of the cross-sectional surface of the wetting reactor so that the drying gas is evenly distributed along the entire cross-sectional surface thereof.

15 19. A method as claimed in any preceding claim further comprising feeding water or steam as downwardly directed sprays into the wetting zone.

20 20. A method as claimed in any preceding claim further comprising feeding water or steam into a plurality of zones in the wetting reactor.

21. A method as claimed in any preceding claim further comprising controlling recycling or internal
25 particle circulation in the wetting reactor by adjusting the amount of gas fed into the second zone.

22. A method as claimed in any preceding claim in which carbonates, oxides or hydroxides of alkali metals or
30 alkali earths are used as the reagent and/or absorbent.

23. A method as claimed in any preceding claim in which the process is a combustion process, a gasification process or a chemical process.



24. A method as claimed in any preceding claim in which the pollutant is sulphur oxides, chlorine or fluorine compounds.

5

25. An apparatus for purification of waste gases having been produced in a process comprising a wetting reactor which is provided with an inlet for waste gases to which gases a reagent and/or absorbent has been added for removing pollutants contained in said gases, water or steam sprays which provide a wetting zone for activating the reagent and/or absorbent, a gas outlet above the wetting zone, and a filter disposed in the upper section of the wetting reactor, for separating solid particles from gases and for returning the solid particles to the lower section of the wetting reactor, and an outlet for the particles separated from the gases, disposed in the lower section of the wetting reactor, wherein the wetting reactor is provided with gas inlets disposed on at least two different elevations so that at least one gas inlet is disposed in the wetting zone and at least another gas inlet is disposed in a second zone below the wetting zone.

26. An apparatus as claimed in claim 25 in which the upper section of the wetting reactor is provided with a fabric filter.

27. An apparatus as claimed in claim 25 or 26 in which at least part of the wetting reactor wall in the wetting zone is a double wall so that an inlet duct is formed in the wall for the gas to be introduced into the wetting zone.

28. An apparatus as claimed in any one of claims 25



to 27 in which several gas inlets are formed in the walls of the wetting reactor in the wetting zone.

29. An apparatus as claimed in any one of claims 25
5 to 28 in which at least part of the wetting reactor wall in the second zone is formed of double-wall so that an inlet duct is formed in the wall for the gas to be introduced into the second zone.

10 30. An apparatus as claimed in any one of claims 25 to 29 in which gas inlets are formed in the wetting reactor walls in the second zone.

15 31. An apparatus as claimed in any one of claims 25 to 30 in which gas feed means are disposed approximately in the middle of the cross-sectional surface of the wetting reactor in the second zone.

20 32. An apparatus as claimed in any one of claims 25 to 31 in which the lower section of the wetting reactor is provided with a mechanical mixer for mixing the solids accumulated in said lower section of the wetting reactor and for breaking the lumps of particles formed therein.

25 33. An apparatus as claimed in any one of claims 25 to 32 in which the lower section of the wetting reactor is provided with a solids discharge screw or conveyor.

30 34. An apparatus as claimed in any one of claims 25 to 33 in which the wetting zone of the wetting reactor is provided with water or water vapor nozzles which are directed downwardly and disposed substantially on the same level as the gas inlets.



35. An apparatus as claimed in claim 34, in which water or steam nozzles are disposed in horizontal support means running through the wetting reactor.

5 36. An apparatus as claimed in any one of claims 25 to 35 in which the process is a combustion process, a gasification process, or a chemical process.

10 37. A method of purification of gases produced in a process substantially as hereinbefore described with reference to any one of the accompanying drawings.

15 38. A method of purification of gases produced in a process substantially as hereinbefore described with reference to any one of the foregoing examples.

20 39. An apparatus for purification of waste gases having been produced in a process substantially as hereinbefore described with reference to any one of the accompanying drawings.

25 40. An apparatus for purification of waste gases having been produced in a process substantially as hereinbefore described with reference to any one of the foregoing examples.

Dated this 15th day of October 1993

A AHLSTROM CORPORATION

By its Patent Attorneys:

30 GRIFFITH HACK & CO

Fellows Institute of Patent Attorneys of Australia



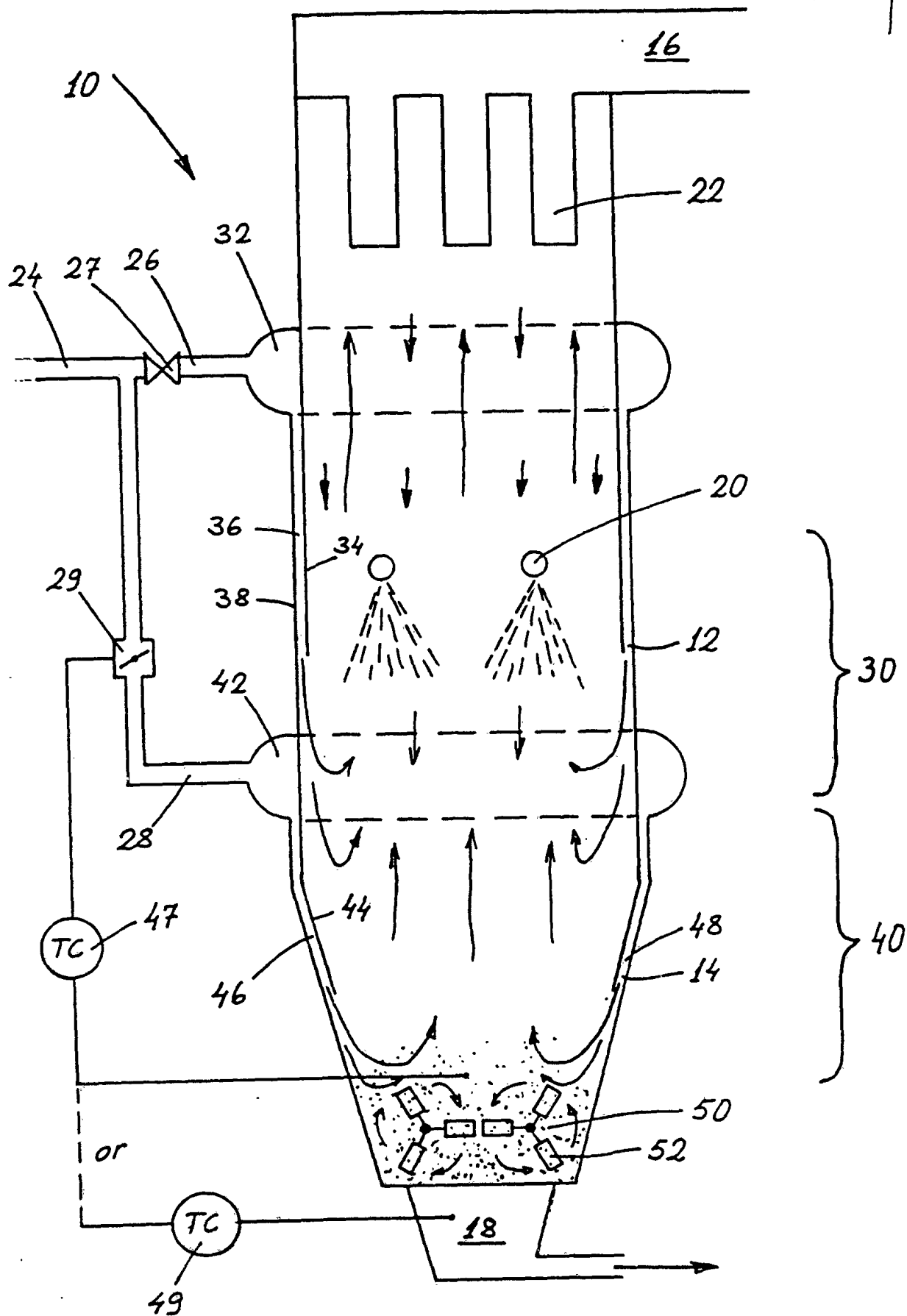
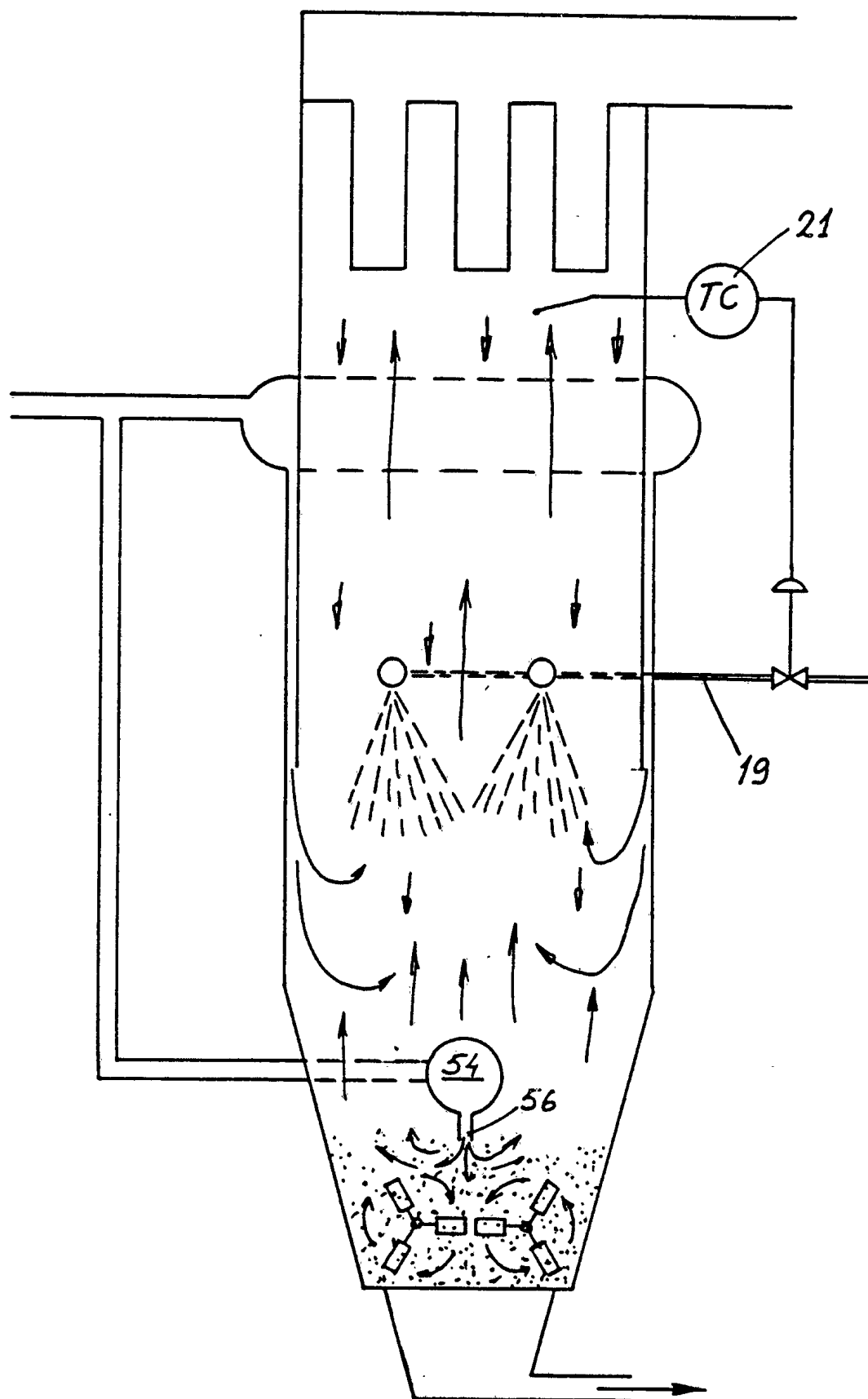


Fig 1.

*Fig 2.*

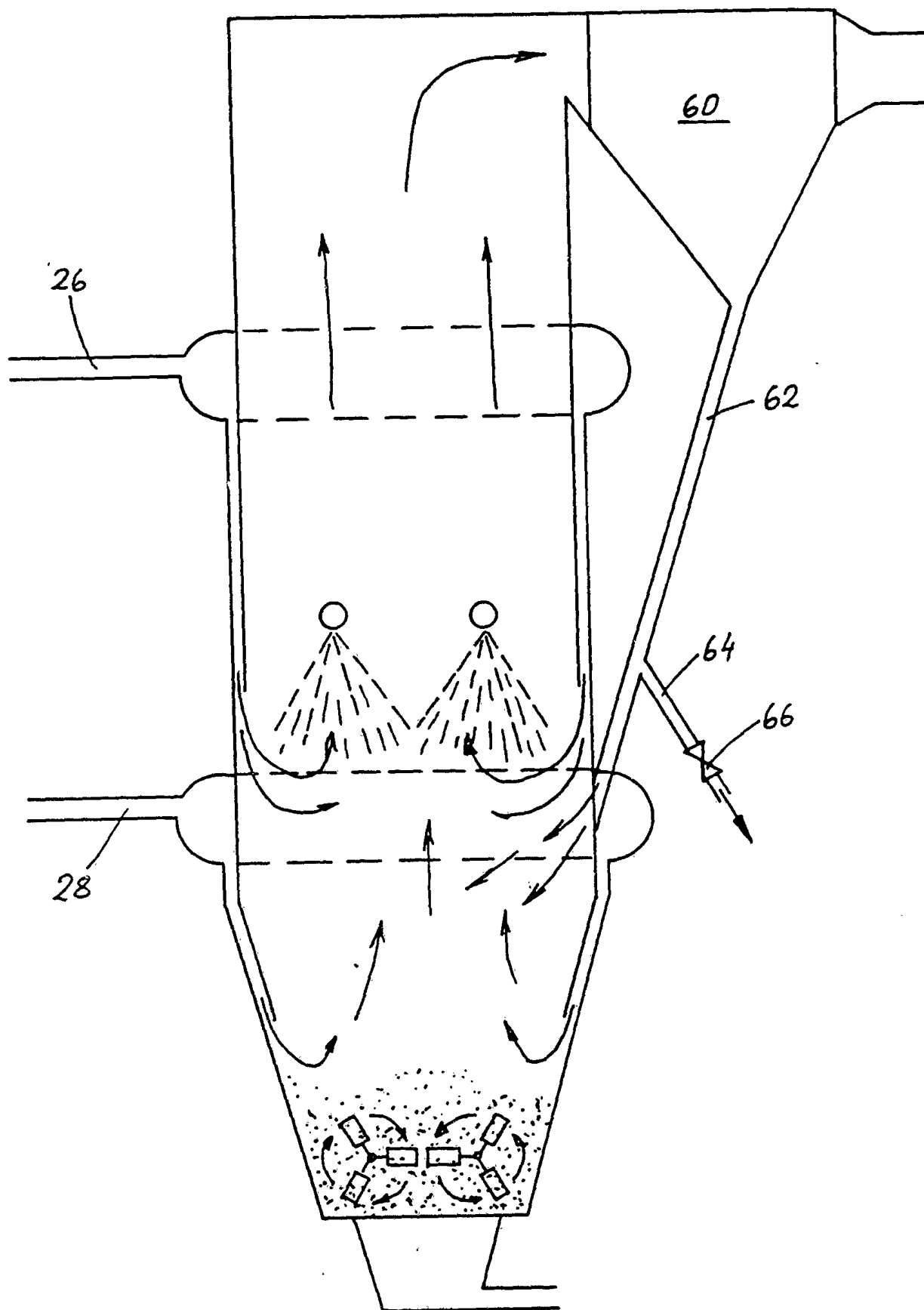


Fig 3.

SO₂ - ABSORB. [%]

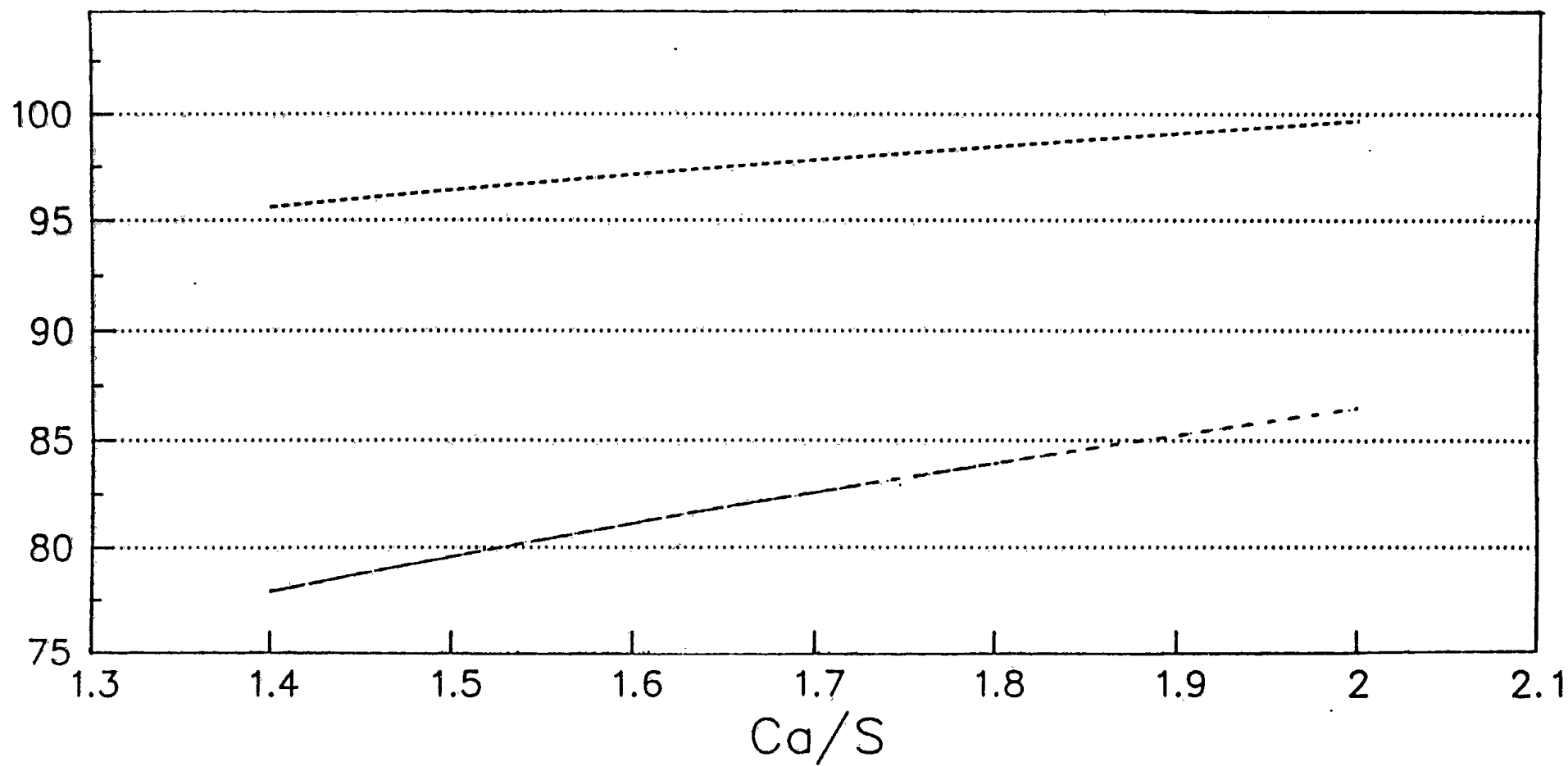


Fig 4

INTERNATIONAL SEARCH REPORT

International Application No PCT/FI 91/00051

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ⁶ According to International Patent Classification (IPC) or to both National Classification and IPC IPC5: B 01 D 53/34																	
II. FIELDS SEARCHED Minimum Documentation Searched⁷ <table style="width: 100%; border-collapse: collapse;"> <tr> <th style="width: 25%; border: 1px solid black; padding: 2px;">Classification System</th> <th style="width: 75%; border: 1px solid black; padding: 2px;">Classification Symbols</th> </tr> <tr> <td style="border: 1px solid black; padding: 5px; text-align: center;">IPC5</td> <td style="border: 1px solid black; padding: 5px; text-align: center;">B 01 D</td> </tr> </table> Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in Fields Searched⁸ SE,DK,FI,NO classes as above			Classification System	Classification Symbols	IPC5	B 01 D											
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III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹ <table border="1" style="width: 100%; border-collapse: collapse;"> <thead> <tr> <th style="width: 10%; padding: 2px;">Category *</th> <th style="width: 60%; padding: 2px;">Citation of Document,¹¹ with indication, where appropriate, of the relevant passages¹²</th> <th style="width: 30%; padding: 2px;">Relevant to Claim No.¹³</th> </tr> </thead> <tbody> <tr> <td style="text-align: center; vertical-align: top; padding: 5px;">X</td> <td style="padding: 5px;">DK, B, 146214 (ANHYDRO A/S) 1 August 1983, see page 4, line 14 - line 24; page 5, line 5 - page 6, line 17 --</td> <td style="text-align: center; vertical-align: top; padding: 5px;">1,23</td> </tr> <tr> <td style="text-align: center; vertical-align: top; padding: 5px;">Y</td> <td style="padding: 5px;">Derwent's abstract, No. 84-281 336/45, SU 1 080 836, publ. week 8445 --</td> <td style="text-align: center; vertical-align: top; padding: 5px;">1,23</td> </tr> <tr> <td style="text-align: center; vertical-align: top; padding: 5px;">A</td> <td style="padding: 5px;">FI, B, 78401 (OY TAMPELLA AB) 28 April 1989, see the whole document --</td> <td style="text-align: center; vertical-align: top; padding: 5px;">1,23</td> </tr> <tr> <td style="text-align: center; vertical-align: top; padding: 5px;">A</td> <td style="padding: 5px;">EP, A2, 0104335 (DEUTSCHE BABCOCK ANLAGEN AKTIENGESELLSCHAFT) 4 April 1984, see the whole document -- -----</td> <td style="text-align: center; vertical-align: top; padding: 5px;">1,23</td> </tr> </tbody> </table>			Category *	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³	X	DK, B, 146214 (ANHYDRO A/S) 1 August 1983, see page 4, line 14 - line 24; page 5, line 5 - page 6, line 17 --	1,23	Y	Derwent's abstract, No. 84-281 336/45, SU 1 080 836, publ. week 8445 --	1,23	A	FI, B, 78401 (OY TAMPELLA AB) 28 April 1989, see the whole document --	1,23	A	EP, A2, 0104335 (DEUTSCHE BABCOCK ANLAGEN AKTIENGESELLSCHAFT) 4 April 1984, see the whole document -- -----	1,23
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* Special categories of cited documents:¹⁰ "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance, the claimed invention cannot be considered novel or cannot be considered to involve an inventive step "Y" document of particular relevance, the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "&" document member of the same patent family																	
IV. CERTIFICATION <table style="width: 100%; border-collapse: collapse;"> <tr> <td style="width: 50%; border: 1px solid black; padding: 5px;"> Date of the Actual Completion of the International Search 15th April 1991 </td> <td style="width: 50%; border: 1px solid black; padding: 5px;"> Date of Mailing of this International Search Report 13 </td> </tr> <tr> <td style="border: 1px solid black; padding: 5px;"> International Searching Authority SWEDISH PATENT OFFICE </td> <td style="border: 1px solid black; padding: 5px;"> Signature of Authorized Officer Britt-Marie Lundell </td> </tr> </table>			Date of the Actual Completion of the International Search 15th April 1991	Date of Mailing of this International Search Report 13	International Searching Authority SWEDISH PATENT OFFICE	Signature of Authorized Officer Britt-Marie Lundell											
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