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(54) **LUMEN LOADING OF MINERAL FILLER INTO CELLULOSE FIBERS FOR PAPERMAKING**

FÜLLEN VON ZELLSTOFFFASERHOHLRAUM MIT MINERALISCHEM FÜLLSTOFF ZUR
PAPIERHERSTELLUNG

REMPLISSAGE DE LUMIERE DE FIBRES CELLULOSIQUES PAR UNE CHARGE MINERALE EN
VUE DE LA FABRICATION DE PAPIER

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- **"Pulp and Paper Manufacture, Vol. 6 "Stock Preparation" 3rd. ed 1983, The Joint Textbook Committee of the Paper Industry, TAPPI Atlanta USA**

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Description

[0001] The present invention relates to a process for the preparation of mineral filled paper wherein the filler is dispersed within the lumens of the pulp fiber and wherein a chemical flocculant is added to the furnish, in order to bind the filler inside the lumens as well as to the use of certain flocculants. By using the process of the present invention, the filler is retained within the lumens even under dilute, high shear conditions of papermaking.

[0002] Any fibrous raw material such as wood, straw, bamboo, hemp, bagasse, sisal, flax, cotton, jute and ramie, can be used in the manufacture of paper. Separation of the fibers of such materials is called pulping. The separated fibers which are used to make paper, are called pulp. Due to the fact that wood is plentiful and readily available, paper consists primarily of wood pulp fiber and insoluble particulate mineral fillers. Most fillers are considerably less expensive than the fibers, and as such, are added during papermaking to reduce the overall cost of producing the paper. Fillers are also added to the pulp fiber to impart certain mechanical properties such as bulk and stiffness, and optical properties such as brightness and opacity to the paper. Kaolin clays, chalk, talc, titanium dioxide, calcium carbonates including precipitated calcium carbonate (PCC) and ground calcium carbonate (GCC) are commonly used as mineral fillers in paper production.

[0003] Precipitated calcium carbonate (PCC) has been widely used as a preferred paper filling mineral over the last decade. The versatility of PCC has been one of the major catalysts for its success. For example, PCC can be prepared in a variety of particle sizes and crystal shapes or morphologies. PCC generally exhibits high brightness, resulting in high sheet brightness. Some PCC morphologies are particularly effective at increasing sheet opacity, which is desirable when both sides of the sheet are printed. Other PCC morphologies are effective in controlling the thickness (caliper) of the sheet, which is related to sheet stiffness. PCC can also affect sheet porosity, which can influence the ability of certain pneumatic devices to physically handle the sheet during papermaking. There are also other advantages in using PCC in paper production.

[0004] The material costs of producing paper generally decrease in direct proportion with increasing amounts of mineral filler in the filled paper. Therefore, maximizing the mineral content of paper is a major objective of the paper maker. Optical properties of the filled paper, such as brightness and opacity, also tend to improve by increasing the filler content. These benefits are offset however, by a reduction in mechanical strength that generally occurs as the level of mineral filler in the sheet is increased. Paper derives its mechanical strength from bonding between adjacent pulp fibers. Fillers that are dispersed throughout the pulp fibers will disrupt the intimate contact that allows bonding between adjacent pulp fibers, to occur. The greater the amount of filler in the paper, the greater will be the tendency toward disruption of fiber to fiber bonds, resulting in lower sheet strength.

[0005] Several methods have been proffered to resolve the problem of decreased sheet strength caused by increased filler loading. Some of these techniques have involved chemical modification of the filler surface using agents commonly utilized as retention aids. These generally are polyelectronic synthetic polymers that act mainly through the mechanism of flocculation. Most common are polyamines and polyacrylamides.

[0006] Supplemental bonding agents are also well known as a means of improving the strength of filler loaded papers. These bonding agents can be natural or synthetic polymeric substances that are added at the wet-end of a paper machine to improve the mechanical strength of the dried paper. These materials are typically starches derived from various plants such as corn, tapioca, potato and wheat, or gums derived from locust bean or guar seeds. Such gums and starches are "cooked" or otherwise prehydrated to promote swelling before they are used. Gums and starches also are commonly used in papermaking as surface coatings to improve the sizing (i.e., resistance to penetration by water) of paper.

[0007] Another means of improving the strength of filled papers is through a technique called lumen loading. This involves placing the fillers directly inside the hollow spaces (i.e. lumens) of the pulp fibers. Fillers that reside inside the lumens of pulp fibers do not interfere with inter-fiber bonding, and therefore have less negative impact on the mechanical strength of filled papers. Lumen loading can be accomplished through simple mechanical mixing. However, just as fillers will migrate into these lumens, they can also diffuse out. Using known techniques, loading of the lumens and diffusion of the filler loaded lumens during the papermaking process, continues to be a problem for papermakers. What has been found to be novel and unanticipated by the prior art is a product and process for lumen loading pulp fibers wherein a substantial level of a mineral filler can be loaded into the lumens, while paper strength reduction, is minimized.

[0008] It is therefore an object of the present invention to provide a process wherein the mineral content of paper is increased. Another object of the present invention is to reduce the cost of the papermaking process by reducing the amount of pulp necessary to obtain the same quality paper by increasing the level of mineral filler. A further object of the present invention is to increase the filler content of the paper so that substantially less of the filler is lost with the drainage water, also known as "white water", during sheet formation on the paper machine. A final object is to produce a filled paper that has no deficiencies in mechanical and/or optical properties.

RELATED ART

[0009] U.S. Pat. No. 5223090 discloses a method of loading cellulose fibers with calcium carbonate filler by reacting calcium hydroxide with carbon dioxide in the presence of cellulosic fibrous material.

[0010] U.S. Pat. No. 5,096,539 discloses a process for preparing a filled paper wherein the filler comprises an insoluble precipitate that is precipitated in situ within the cell wall of the fibers.

[0011] U.S. Pat. No. 4,510,020 discloses a process for preparing a filled paper wherein substantially all of the filler present is within the lumens of the cellulosic fibers.

[0012] None of the related art references, either individually or in combination, disclose the present novel product and process for increasing the filler content of paper.

SUMMARY OF THE INVENTION

[0013] The present invention provides a process for adding a mineral filler to wood pulp fiber in a papermaking process wherein a chemical additive is used to flocculate the filler particles inside of the lumens of the fibers as defined in claim 1. The filler is maintained inside the lumens of the fibers during the dilute, high shear conditions of papermaking. The present invention further provides a use as defined in claim 12.

[0014] The present invention provides a process for producing filled paper by loading the lumens of the pulp fiber with a mineral filler. The filler is added to the papermaking process at a point where the concentration of the pulp is from 1.0 to 5.0 weight percent. By the subsequent addition of a chemical flocculant down-stream of the filler addition point, the filler is fixed and remains within the lumens during papermaking. Optionally, additional filler may be added to the papermaking process at a second addition point, in order to achieve fine control of the filler content of the final paper. By using the process of the present invention, filler is loaded within the lumens of the pulp fibers and protected from drainage forces which normally cause filler dislodgement during papermaking. According to the process of the present invention, the filler is loaded into the pulp fiber lumens by mixing or agitating the pulp fiber, the filler, and a flocculant at a point in the papermaking process when the pulp concentration is from about 1.0 to about 5.0 weight percent. Dilution of the filler/pulp fiber mixture may be necessary to obtain the desired furnish consistency of usually from about 0.3 to about 1.0 percent, preferably about 0.5 percent, prior to delivery to the paper machine.

[0015] An integral aspect of the process of the present invention is the structure of the papermaking fiber. The strength of paper is highly dependent upon the fibers of the pulp, used to make paper, becoming bonded extensively to one another during papermaking. The most widely used fibers are those derived from wood and, as liberated by pulping, the majority appear under the microscope as long hollow tubes. uniform in size for most of the length but tapered at each end. Along the length of the fiber, the fiber wall is perforated by small apertures(pits) which connect the central cavity(lumen) to the fiber exterior. The process for placing mineral fillers within the lumens is called lumen loading and is applicable to a wide range of papermaking fibers.

[0016] The present process can be carried out on fibers derived from many species of wood, by any of the common pulping and bleaching procedures. The fiber may be hardwood fiber, softwood fiber or a mixture of both hard and soft wood fibers. However, in order to realize maximum loading of the lumens with filler, the pulp fiber should enter the process of the present invention in "never-dried" form. Drying the pulp fiber irreversibly collapses a large portion of the lumens and renders them inaccessible to the mineral filler. Reslurrying of dried pulp fiber is less susceptible to the full benefit of the novel process for lumen loading of the present invention, but having full knowledge of this limitation, may be used.

[0017] The concentration or consistency of the pulp fiber slurry is preferably in the range of from about one percent to about five percent, based on the total weight of the slurry. In a preferred embodiment of the invention, the consistency of the pulp fiber slurry is preferably in the range of from about two percent to about four percent, based on the total weight of the slurry.

[0018] Kaolin clays, chalk, talc, titanium dioxide, alumina, silica, precipitated calcium carbonate (PCC) and ground calcium carbonate (GCC) are commonly used as mineral fillers in paper production. A filler consists of fine particles of an insoluble solid, usually of a mineral origin. By virtue of the high surface area and sometimes high refractive index, fillers confer improved optical properties such as opacity and brightness to the paper. Enhancement of the optical properties of the mineral filled paper is a principal objective in adding fillers to the paper furnish, although other advantages, such as improved smoothness, improved printability and improved durability, can be imparted to the paper.

[0019] Although kaolin clays, chalk talc, titanium dioxide, alumina, silica, PCC, GCC and the like, may be used in the process of the present invention, the preferred filler is precipitated calcium carbonate (PCC). The PCC has an average particle size in the range from about 0.5 to about 2.0 microns(μm). In a preferred embodiment of the present invention, the average size of the PCC is in the range of from about 0.7 μm to about 1.4 μm . The PCC morphology may be orthorhombic, rhombic or scalenohedral. Other fillers, such as ultrafine ground limestone (UFGL) also may be used in the process of the present invention.

[0020] According to one embodiment of the present invention, an aqueous slurry of mineral filler is mixed, by any known mechanical means, into an aqueous slurry of wood pulp fiber. For loading of the lumens, the pulp is in a never-dried state, in order to obtain the maximum loading benefit. The filler is added to the pulp as an aqueous slurry, so that the filler solids, after mixing with the pulp fiber, represent from about 5 weight percent to about 80 weight percent based on the total solids. In a preferred embodiment of the invention, the filler solids represents from about 20 weight percent to about 40 weight percent based on the total solids.

[0021] The filler and fiber components are mixed under agitation for a period of time to allow maximum loading of the lumens. It has been found that a minimum of five minutes of agitation is necessary to obtain maximum loading. Shorter mixing times do not provide maximum lumen loading benefits. In a preferred embodiment of the present invention, the period of mixing or agitation can range from about 10 minutes to about 30 minutes. There is no known upper limit on the time of mixing, outside of that imposed by practicality and economics. During the time that the fiber and filler components are mixed together, some of the filler becomes dispersed within the fiber lumens. This occurs by mechanical diffusion.

[0022] Certain factors strongly influence the level of filler that can be practically loaded into the fiber lumens. One such factor is the average particle size of the mineral filler. Fillers having smaller average particle sizes will more easily diffuse into the lumens than larger particle size fillers. In addition, the relative concentrations of fiber and filler that are present when the two components are mixed, will also determine the extent to which lumen loading occurs. Finally, the period of time the filler and fiber components are mixed, influence how much lumen loading will occur in the paper furnish.

[0023] According to the present invention, the amount of filler that diffuses into the lumens, is from about 0.5 percent to about 10 percent of the combined weight of fiber and filler. In a preferred embodiment of the invention from about 3 percent to about 6 percent of the total weight of fiber and filler is lumen loaded filler.

[0024] Another integral aspect of the process of lumen loading of the present invention requires that a flocculating chemical be added to the pulp fiber-filler mixture, after the pulp fiber-filler components have been sufficiently mixed. The use of such a flocculant causes any filler that resides within the fiber lumens to form agglomerates of sufficient size to prevent diffusion outside the lumens during paper production. This also causes filler outside the lumens to also form agglomerates. The formation of agglomerates reduces the tendency of filler particles to interfere with inter-fiber bonding, fixes and holds the filler inside and outside the lumens, thus preventing dislodgement of the filler during papermaking.

[0025] The flocculating chemical is selected from that group of materials that are polymers of glucose derived from plants, called starches. Plants from which starches are principally obtained are corn, tapioca, potato and wheat. Before it is used as a chemical flocculant in the present produces, the starch is "cooked", in a manner consistent with the manufacturer's recommendation, to promote dissolution and swelling. This is an important aspect of the present invention since the formation of agglomerates both inside the lumens and outside of the lumens result in maximum lumen loading.

[0026] The starches to be used according to the invention are chemically modified to render the starch cationic, anionic or amphoteric. According to the process of the present invention. the starch is preferably an amphoteric waxy corn starch.

[0027] The flocculating agent is selected from those materials that exhibit a stronger chemical affinity for PCC than for wood pulp fiber. The chemical affinity is measured using the technique of batch calorimetry. When a chemical agent is brought into contact with the mineral surface, adsorption of the chemical agent will occur at the mineral surface only if sufficient affinity exists between the two materials. Adsorption is an exothermic process that liberates heat. Adsorption also can occur for a chemical agent that is brought into contact with wood pulp fibers. The magnitude of the interaction between a flocculating agent and the mineral filler is measured to determine which provides maximum benefit. A separate measurement is made to determine the magnitude of the interaction between the flocculating agent and a microcrystalline cellulose that is chemically similar to wood pulp.

[0028] In a preferred embodiment of the current invention, the magnitude of the flocculant-mineral interaction, expressed in calories, is at least equal to the magnitude of the flocculant-cellulose interaction for equal proportions of materials. More preferably, the magnitude of the flocculant-mineral interaction is at least 50 percent greater than the interaction between flocculant and cellulose. Most preferably, the magnitude of the flocculant-cellulose interaction is zero (0). The current invention is advantageous over other lumen loading techniques in that it offers a means of preventing diffusion of filler particles outside the fiber lumens without the need for a drying step. This results in a reduction in energy cost and an increase margin of profit for the papermaker.

[0029] Figure I demonstrates an aspect of how the process of the present invention could be used in a typical papermaking process. The filler addition is split such that filler may be added to the furnish at the blend chest and again at the head box. Between these two addition points, but after the first addition point, a chemical flocculant is added to the pre-mixed fiber-filler components in order to fix or hold the filler where it resides inside and outside of the fiber lumens.

[0030] The following examples are presented to further illustrate the present invention.

EXAMPLES

[0031] In the following examples, one or more processes are described which involve addition of a mineral filler to a high-consistency slurry of wood pulp fiber. After the filler and fiber are mixed, a flocculating chemical is added so that filler particles that have diffused into the fiber lumens are agglomerated and prevented from diffusing outside the lumens. The flocculating agent is selected from those chemicals that exhibit greater chemical affinity for the filler than for cellulose fiber. Chemical affinity is quantified using the technique of batch calorimetry. Alternately, the mineral filler and flocculating chemical are mixed and then added to a high consistency slurry of wood pulp fiber slurry. The resulting mixture is formed into paper exhibiting good mechanical strength at high filler loading levels.

Example 1

[0032] Into a 4-liter glass reactor was placed 200 milliliters (ml) of 4 weight percent consistency (solids) never-dried hardwood pulp. The pulp was mixed at 300 rpm with a large flat blade such that a gentle churning action occurs. Scalenohedral calcium carbonate slurry having 20 weight percent solids content was added to the mixing hardwood pulp in such an amount that the dry calcium carbonate content represented 40 weight percent of the total solids of the mixture. The calcium carbonate/pulp aqueous slurry was stirred for an additional 30 minutes. An amphoteric waxy corn starch (CATO 225 from National Starch Corporation) which was cooked at 93.3°C (200°F) for 30 minutes at 1 weight percent solids was added to the calcium carbonate/pulp aqueous slurry. The quantity of starch corresponds to a 4.0 weight percent on a dry calcium carbonate basis. The calcium carbonate/pulp/starch aqueous slurry was stirred for 30 minutes. The mixture was made into a paper sheet on a stainless steel wire using a Formax unit. The basis weight of the sheet approximates 170 grams per meter square (g/m^2). The sheet was pressed between felts at $1.7 \cdot 10^5$ pascal (25 psi) and dried on a drum drier at 265°C. These dried sheets represent the commercial hardwood dry lap containing calcium carbonate, which was combined with softwood dry lap in the desired proportions. The percent calcium carbonate of the hardwood dry lap is measured so as to definitively determine the amount of dry hardwood present. The hardwood containing sheets were refined by combining 360 grams hardwood (from the hardwood dry lap) and 24 liters of water and stirring the mixture in a Valley Beater to 360 Canadian Standard Freeness (CSF). A mixture was prepared by combining 360 grams of untreated softwood pulp and 24 liters of water. The mixture was refined by mixing in a Valley Beater to 400 CSF. The refined hardwood and the refined softwood were combined such that a 60 percent hardwood/40 percent softwood mixture results. Water was added to the mixture to adjust the solids to 0.3 weight percent on a dry pulp basis.

[0033] Handsheets were prepared (60 g/m^2) using a Formax Sheet Former (Noble and Wood type, from Adirondack Machine Corp) from a furnish of 60 percent hardwood (containing calcium carbonate in the lumen) and 40 percent bleached softwood pulps beaten to 400 CFS at pH 7 in distilled water. The pulp consistency was 0.3 percent. A retention aid (high molecular weight cationic polyacrylamide) Percol® from Allied Colloids was added to the pulp furnish in an amount equal to 0.05 percent (0.5 kg/ton ~ 1lb./ton of paper). Synthetic sizing agent (alkyl ketene dimer) was added to the pulp furnish at a level of 0.25 percent (2.5 kg/ton ~ 5lbs./ton of paper). The mixture was made into a paper sheet on a stainless steel wire using a Formax unit. The sheet was pressed between felts at $1.7 \cdot 10^5$ pascal (25p.s.i) and dried on a drum dryer at 265°C. The sheets were conditioned at 50 percent relative humidity and 23°C. prior to testing.

[0034] The paper strength was determined by testing the breaking length (TAPPI test method T-494 OM-88) and the Scott Bond (TAPPI test method UM 403). The paper brightness was measured according to TAPPI test method T452-OM92 and the paper opacity was measured according to TAPPI test method T425-OM-91 (corrected to 60.5 grams/ m^2 basis weight).

[0035] The strength of the paper, using as filler the lumen containing calcium carbonate in accordance with the present invention, is greater than that of the control paper (not lumen loaded. but having an equivalent amount of filler added in the conventional manner).

	CONTROL (Not Lumen Loaded)	PRESENT INVENTION (Lumen Loaded)
Weight Filler (Percent)	24	24
Breaking Length (Meters)	2127	3128
Scott Bond (Foot lbs in Thousandths)	34.2	53.6
TAPPI Brightness (Percent)	89.3	89
TAPPI Opacity (Percent)	87.6	87.6

Example 2

[0036] A mixture of 270 grams of hardwood pulp and 90 grams of softwood pulp (75 percent hardwood/25 percent softwood) was combined with 24 liters of water and refined in a Valley Beater to 400 CSF. The pulp consistency was 1.5 percent. Water was removed by screening the pulp through a 100 mesh screen to raise the consistency of the pulp to 3.8 percent. The pulp fine water was set aside for later use. The 3.8 percent consistency was used to simulate the solids of pulp in an integrated mill. An integrated paper mill is one that prepares its own pulp as opposed to acquiring pulp from the open market.

[0037] Into a 4-liter glass reactor was placed 1000 ml of the previously described 3.8 percent consistency pulp. The pulp was mixed at 100 rpm with a large flat blade such that a gentle churning action occurred. Scalenoedral calcium carbonate slurry at 20 weight percent solids was added to the mixing hardwood/softwood pulp in such an amount that the dry calcium carbonate represented 15 weight percent of the total solids of the mixture. The calcium carbonate/pulp aqueous slurry was stirred 10 minutes. A cationic potato starch (STA-LOK® 400 from A.E. Staley Manufacturing Company) which was cooked at 93.3°C (200°F), for 30 minutes at 1 percent solids was added to the calcium carbonate/pulp aqueous slurry. The quantity of starch corresponds to 4.0 weight percent on a dry calcium carbonate basis. The calcium carbonate/pulp/starch aqueous slurry was then stirred for 10 minutes. The mixture was then diluted with 1622 ml of the pulp fine water so as to re-introduce all fines that were removed during the screening process. The mixture was further diluted with 9500 ml water to adjust the final consistency to approximately 0.3 percent.

[0038] Paper handsheets were then prepared from the above-described hardwood/softwood pulp containing the calcium carbonate and hardwood/softwood pulp containing no calcium carbonate loaded in the lumen. The handsheets were prepared and tested as described in Example 1. Hercules Size Test (HST) was used to measure the penetration of liquid through the handsheets. The test was performed on a Hercules Sizing Tester Model KA or KC and the test method employed is TAPPI Test Method T-530 PM-89 (Revised 1989).

[0039] The paper strength, i.e. Breaking Length and Scott Bond of the paper, which contains the calcium carbonate loaded lumen in accordance with the present invention is greater than that of the control paper (not lumen loaded). The paper which contains the calcium carbonate loaded lumen also exhibits improved sizing.

	CONTROL (Not Lumen Loaded)	PRESENT INVENTION (Lumen Loaded)
Weight Filler (Percent)	16	16
Breaking Length (Meters)	2970	3350
Scott Bond (Foot lbs in Thousandths)	49.2	58.2
HST Sizing (Percent)	23	103
TAPPI Opacity (Percent)	88.1	88.2
TAPPI Opacity (Percent)	87.5	88

Claims

1. A process for producing a mineral filled paper which comprises adding an aqueous slurry of mineral filler particles to an aqueous slurry of never dried wood pulp fibre, wherein the concentration of the wood pulp fibre is from 1.0 wt % to 5.0 wt %, based on the weight of the slurry of never dried wood pulp fibre, wherein the filler solids, after mixing with the pulp fibre, is present from 5 to 80 wt % based on the total solids, wherein the filler and fibre components are mixed under agitation for at least 5 minutes, adding an amphoteric, anionic or cationic starch flocculent to fix the mineral filler inside the lumens and to produce paper wherein from 0.5 to 10 wt % of filler, based on the combined weight of filler and fibre, is located inside the lumens.
2. A process according to Claim 1 in which from 3 to 6 wt % of the total weight of fibre and filler is lumen loaded.
3. The process as claimed in Claim 1 or Claim 2 wherein the mixture of filler and pulp is diluted to a pulp concentration of from 0.3 wt % to 1.0 wt % prior to delivery to the paper machine.
4. The process as claimed in any of the preceding Claims wherein the mineral filler is calcium carbonate.
5. The process as claimed in Claim 4, wherein the calcium carbonate is precipitated calcium carbonate.
6. The process as claimed in Claim 5, wherein the precipitated calcium carbonate has an average particle size of from 0.5 microns to 2.0 microns.
7. The process as claimed in Claim 6, wherein the average particle size is from 0.7 microns to 1.4 microns.
8. The process as claimed in any of Claims 4 to 7, wherein the calcium carbonate is from 20 wt % to 40 wt % of the total solids of the filler pulp mixture.
9. The process as claimed in any of the preceding Claims, wherein the concentration of the wood pulp fibre is from 2.0 wt % to 4.0 wt %, based on the total weight of slurry.
10. The process as claimed in any of the preceding Claims, wherein the aqueous slurry of mineral filler and the aqueous slurry of fibre are mixed for from 10 to 30 minutes.
11. The process of any of the preceding Claims, wherein the starch is amphoteric waxy corn starch.
12. The use of an amphoteric, anionic or cationic starch flocculent in a papermaking furnish of never dried wood pulp fibre and mineral filler to fix the mineral filler inside the lumens of the wood pulp.

13. The use according to Claim 12, to fix from 0.5 to 10 % of filler, based on the combined weight of filler and fibre inside the lumens.
14. The use according to Claim 12 or 13, wherein the mineral filler is calcium carbonate.
15. The use according to any of Claims 12 to 14, wherein the calcium carbonate is precipitated calcium carbonate.
16. The use according to any of Claims 12 to 15 in a system wherein the concentration of the wood pulp fibre is from 1.0 wt % to 5.0 wt %, based on the total weight of the slurry.
17. The use according to any of Claims 12 to 16, wherein the starch is amphoteric waxy corn starch.

Patentansprüche

1. Verfahren zur Herstellung eines mineralisch gefüllten Papiers, bei welchem eine wässrige Aufschlämmung mineralischer Füllstoffpartikel zu einer wässrigen Aufschlämmung zwischenzeitlich nicht getrockneter Holzpulpefasern hinzugefügt wird, wobei die Konzentration der Holzpulpefasern von 1,0 Gew.-% bis 5,0 Gew.-% beträgt, bezogen auf das Gewicht der Aufschlämmung der zwischenzeitlich nicht getrockneten Holzpulpefasern und wobei die festen Füllstoffe nach der Vermischung mit der Pulpefaser in einen Anteil von 5 bis 80 Gew.-%, bezogen auf die Gesamtmenge an Feststoffen, zugegen ist, wobei der Füllstoff und die Faserkomponenten unter Rühren für mindestens fünf Minuten miteinander vermischt werden, und bei welchem ein amphoterer, anionischer oder kationischer Stärke-Flockungsmittel hinzugefügt wird, um den mineralischen Füllstoff innerhalb des Lumens zu fixieren und um ein Papier herzustellen, bei dem von 0,5 bis 10 Gew.-% des Füllstoffes, bezogen auf das Gesamtgewicht von Füllstoff und Fasern, innerhalb der Lumina sich befindet.
2. Verfahren nach Anspruch 1, bei welchem 3 bis 6 Gew.-% des Gesamtgewichts von Fasern und Füllstoff sich in der Lumina befindet.
3. Verfahren nach Anspruch 1 oder 2, bei welchem die Mischung aus Füllstoff und Pulpe auf eine Pulpekonzentration von 0,3 bis 1,0 Gew.-% verdünnt wird, bevor sie der Papiermaschine zugeführt wird.
4. Verfahren nach einem der vorangehenden Ansprüche, bei welchem der mineralische Füllstoff Calciumcarbonat ist.
5. Verfahren nach Anspruch 4, bei welchem das Calciumcarbonat ausgefälltes Calciumcarbonat ist.
6. Verfahren nach Anspruch 5, bei welchem das ausgefällte Calciumcarbonat eine mittlere Partikelgröße von 0,5 bis 2,0 Mikron aufweist.
7. Verfahren nach Anspruch 6, bei welchem die mittlere Partikelgröße 0,7 bis 1,4 Mikron beträgt.
8. Verfahren nach einem der Ansprüche 4 bis 7, bei welchem das Calciumcarbonat 20 bis 40 Gew.-% der Gesamtmenge der Mischung aus Füllstoff und Pulpe ausmacht.
9. Verfahren nach einem der vorangehenden Ansprüche, bei welchem die Konzentration der Holzpulpefaser von bis 4,0 Gew.-% beträgt, bezogen auf die Gesamtmenge der Aufschlämmung.
10. Verfahren nach einem der vorangehenden Ansprüche, bei welchem die wässrige Aufschlämmung des mineralischen Füllstoffs und die wässrige Aufschlämmung der Fasern 10 bis 30 Minuten miteinander vermischt werden.
11. Verfahren nach einem der vorangehenden Ansprüche, bei welchem die Stärke amphotere wachsartige Maisstärke ist.
12. Die Verwendung eines amphoterer, anionischen oder kationischen Stärke-Flockungsmittels in einem Papierstoff aus zwischenzeitlich nicht getrockneter Holzpulpefaser und mineralischem Füllstoff, um den mineralischen Füllstoff innerhalb der Lumina der Holzpulpe zu fixieren.
13. Verwendung nach Anspruch 12, um 0,5% bis 10 % des Füllstoffs, bezogen auf das Gesamtgewicht des Füllstoffs

und der Fasern, innerhalb der Lumina zu fixieren.

14. Verwendung nach Anspruch 12 oder 13, bei welcher der mineralische Füllstoff Calciumcarbonat ist.

15. Verwendung nach einem der Ansprüche 12 bis 14, bei welcher das Calciumcarbonat ausgefälltes Calciumcarbonat ist.

16. Verwendung nach einem der Ansprüche 12 bis 15 in einem System, in welchem die Konzentration der Holzpulpefasern 1,0 bis 5,0 Gew.-% beträgt, bezogen auf das Gesamtgewicht der Aufschlämmung.

17. Verwendung nach einem der Ansprüche 12 bis 16, bei welcher die Stärke eine amphotere wachsartige Maisstärke ist.

Revendications

1. Procédé pour la production d'un papier renfermant une charge minérale, qui comprend les étapes consistant à ajouter une suspension aqueuse de particules d'une charge minérale à une suspension aqueuse de fibres de pâte de bois n'ayant jamais été déshydratée, la concentration des fibres de pâte de bois étant comprise dans l'intervalle de 1,0% en poids à 5,0% en poids sur la base du poids de la suspension de fibres de pâte de bois n'ayant jamais été déshydratée, les matières solides de charge, après le mélange aux fibres de pâte, étant présentes en une quantité de 5 à 80% en poids sur la base des matières solides totales, à mélanger la charge et les fibres sous agitation pendant au moins 5 minutes, à ajouter un agent flocculant du type amidon amphotère, anionique ou cationique pour fixer la charge minérale à l'intérieur des lumens et pour produire du papier dans lequel une quantité de 0,5 à 10% en poids de charge, sur la base de la somme des poids de la charge et des fibres, est située à l'intérieur des lumens.

2. Procédé suivant la revendication 1, dans lequel une quantité de 3 à 6% en poids du poids total des fibres et de la charge est incorporée aux lumens.

3. Procédé suivant la revendication 1 ou la revendication 2, dans lequel le mélange de charge et de pâte est dilué à une concentration en pâte de 0,3% en poids à 1,0% en poids avant d'être amené à la machine à papier.

4. Procédé suivant l'une quelconque des revendications précédentes, dans lequel la charge minérale consiste en carbonate de calcium.

5. Procédé suivant la revendication 4, dans lequel le carbonate de calcium consiste en carbonate de calcium précipité.

6. Procédé suivant la revendication 5, dans lequel le carbonate de calcium précipité a un diamètre moyen de particule de 0,5 micromètre à 2,0 micromètres.

7. Procédé suivant la revendication 6, dans lequel le diamètre moyen de particule est compris dans l'intervalle de 0,7 micromètre à 1,4 micromètre.

8. Procédé suivant l'une quelconque des revendications 4 à 7, dans lequel le carbonate de calcium est présent en une quantité de 20% en poids à 40% en poids de matières solides totales du mélange de charge et de pâte.

9. Procédé suivant l'une quelconque des revendications précédentes, dans lequel la concentration des fibres de pâte de bois est comprise dans l'intervalle de 2,0% en poids à 4,0% en poids, sur la base du poids total de la suspension.

10. Procédé suivant l'une quelconque des revendications précédentes, dans lequel la suspension aqueuse de charge minérale et la suspension aqueuse de fibres sont mélangées pendant un temps de 10 à 30 minutes.

11. Procédé suivant l'une quelconque des revendications précédentes, dans lequel l'amidon consiste en amidon amphotère de maïs cireux.

12. Utilisation d'un agent flocculant du type amidon amphotère anionique ou cationique dans une composition de fabrication de papier constituée de fibres de pâte de bois n'ayant jamais été déshydratée et d'une charge minérale

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pour fixer la charge minérale à l'intérieur des lumens de la pâte de bois.

13. Utilisation suivant la revendication 12, pour fixer 0,5 à 10% de charge, sur la base de la somme des poids de la charge et des fibres à l'intérieur des lumens.

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14. Utilisation suivant la revendication 12 ou 13, dans laquelle la charge minérale consiste en carbonate de calcium.

15. Utilisation suivant l'une quelconque des revendications 12 à 14, dans laquelle le carbonate de calcium consiste en carbonate de calcium précipité.

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16. Utilisation suivant l'une quelconque des revendications 12 à 15, dans un système dans lequel la concentration de fibres de pâte de bois est comprise dans l'intervalle de 1,0% en poids à 5,0% en poids, sur la base du poids total de la suspension.

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17. Utilisation suivant l'une quelconque des revendications 12 à 16, dans laquelle l'amidon consiste en amidon amphotère de maïs cireux.

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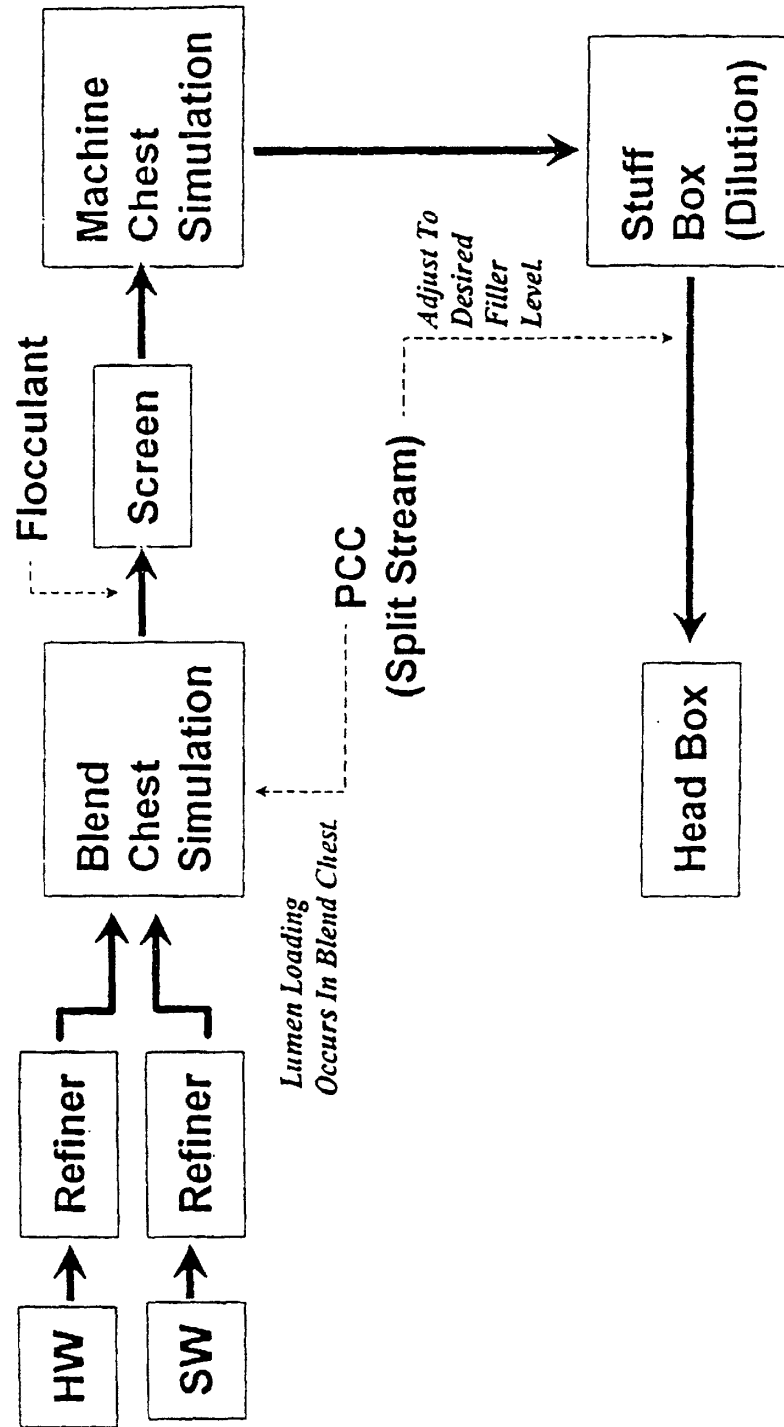
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**FIGURE 1 - LUMEN LOADING IN TYPICAL
PAPERMAKING PROCESS**



HW - Hardwood
SW - Softwood