THERMOPLASTIC SILICONE ELASTOMERS FORMED FROM NYLON RESINS

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U.S. PATENT DOCUMENTS

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4,695,602 A 9/1987 Crosby et al. 524/439
4,714,739 A 12/1987 Arkles 525/92
4,803,244 A 2/1989 Umpleby 525/105
4,831,071 A 5/1989 Ward et al. 524/401
4,849,469 A 7/1989 Crosby et al. 524/439
4,891,407 A 1/1990 Mitchell 525/104
4,970,263 A 11/1990 Arkles et al. 525/92
5,391,594 A 2/1995 Romenskos et al. 523/212
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6,013,715 A 1/2000 Gornowicz 524/492

FOREIGN PATENT DOCUMENTS

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JP 07-26147 1/1995
WO 96/01291 1/1996

OTHER PUBLICATIONS


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ABSTRACT

A method for preparing a thermoplastic elastomer is disclosed, said method comprising
(I) mixing
(A) a rheologically stable polyamide resin having a melting point or glass transition temperature of 25°C to 250°C,
(B) a silicone base comprising
(B1) 100 parts by weight of a diorganopolysiloxane gum having a plasticity of at least 30 and having an average of at least 2 alkenyl radicals in its molecule and
(B2) 5 to 200 parts by weight of a reinforcing filler, the weight ratio of said silicone base to said polyamide resin being greater than 35:65 to 85:15,
(C) 0.1 to 5 parts by weight of a hindered phenol compound for each 100 parts by weight of said polyamide and said silicone base,
(D) an organohydro silicon compound which contains an average of at least 2 silicon-bonded hydrogen groups in its molecule and
(E) a hydrosilation catalyst, components (D) and (E) being present in an amount sufficient to cure said diorganopolysiloxane (B); and
(II) dynamically curing said diorganopolysiloxane (B), wherein at least one property of the thermoplastic elastomer selected from tensile strength or elongation is at least 25% greater than the respective property for a corresponding simple blend wherein said diorganopolysiloxane is not cured and said thermoplastic elastomer has an elongation of at least 25%.

24 Claims, No Drawings
1. THERMOPLASTIC SILICONE ELASTOMERS FORMED FROM NYLON RESINS

FIELD OF THE INVENTION

The present invention relates to a thermoplastic elastomer composition wherein a silicone base and a hindered phenol are blended with a polyamide resin and a silicone gum contained in the base is dynamically vulcanized in the mixture.

BACKGROUND OF THE INVENTION

Thermoplastic elastomers (TPEs) are polymeric materials which possess both plastic and rubbery properties. They have elastomeric mechanical properties but, unlike conventional thermoset rubbers, they can be re-processed at elevated temperatures. This re-processability is a major advantage of TPEs over chemically crosslinked rubbers since it allows recycling of fabricated parts and results in a considerable reduction of scrap.

In general, two main types of thermoplastic elastomers are known. Block copolymer thermoplastic elastomers contain “hard” plastic segments which have a melting point or glass transition temperature above ambient as well as “soft” polymeric segments which have a glass transition or melt point considerably below room temperature. In these systems, the hard segments aggregate to form distinct microphases and act as physical crosslinks for the soft phase, thereby imparting a rubbery character at room temperature. At elevated temperatures, the hard segments melt or soften and allow the copolymer to flow and be processed like an ordinary thermoplastic resin.

Alternatively, a thermoplastic elastomer referred to as a simple blend (physical blend) can be obtained by uniformly mixing an elastomeric component with a thermoplastic resin. When the elastomeric component is also cross-linked during mixing, a thermoplastic elastomer known in the art as a thermoplastic vulcanize (TPV) results. Since the crosslinked elastomeric phase of a TPV is insoluble and non-flowable at elevated temperatures, TPVs generally exhibit improved oil and solvent resistance as well as reduced compression set relative to the simple blends.

Typically, a TPV is formed by a process known as dynamic vulcanization, wherein the elastomer and the thermoplastic matrix are mixed and the elastomer is cured with the aid of a crosslinking agent and/or catalyst during the mixing process. A number of such TPVs are known in the art, including some wherein the crosslinked elastomeric component can be a silicone polymer while the thermoplastic component is an organic, non-silicone polymer (i.e., a thermoplastic silicone vulcanize or TPSIV). In such a material, the elastomeric component can be cured by various mechanisms, but it has been shown that the use of a non-specific radical initiator, such as an organic peroxide, can also result in at least a partial cure of the thermoplastic resin itself, thereby reducing or completely destroying ability to re-process the composition (i.e., it no longer is a thermoplastic). In other cases, the peroxide can lead to the partial degradation of the thermoplastic resin. To address these problems, elastomer-specific crosslinkers, such as organohydrido silicon compounds, can be used to cure alkynyl-functional silicone elastomers.

Arkles, in U.S. Pat. No. 4,500,688, discloses semi-interpenetrating networks (IPN) wherein a vinyl-containing silicone fluid having a viscosity of 500 to 100,000 cS is dispersed in a conventional thermoplastic resin. Arkles only illustrates these IPNs at relatively low levels of silicone. The vinyl-containing silicone is vulcanized in the thermoplastic during melt mixing according to a chain extension or crosslinking mechanism which employs a silicone hydride-containing silicone component. This disclosure states that the chain extension procedure results in a thermoplastic composition when the vinyl-containing silicone has 2 to 4 vinyl groups and the hydride-containing silicone has 1 to 2 times the equivalent of the vinyl functionality. On the other hand, silicones which predominantly undergo crosslinking reaction result in thermoset compositions when the vinyl-containing silicone has 2 to 30 vinyl groups and the hydride-containing silicone has 2 to 10 times the equivalent of the vinyl functionality. Typical thermoplastics mentioned include polyamides, polycrylates, styrenes, polyacetals and polycarbonates. This disclosure is expanded by Arkles in U.S. Pat. No. 4,714,739 to include the use of hybrid silicones which contain unsaturated groups and are prepared by reacting a hydride-containing silicone with an organic polymer having unsaturated functionality. Although Arkles discloses a silicone fluid content ranging from 1 to 40 weight percent (1 to 60% in the case of the ’739 patent), there is no suggestion of any criticality as to these proportions or to the specific nature of the organic resin.

Publication WO 96/01291 to Advanced Elastomer Systems discloses thermoplastic elastomers having improved resistance to oil and compression set. These systems are prepared by first forming a cured rubber concentrate wherein a curable elastomeric copolymer is dispersed in a polymeric carrier not miscible therewith, the curable copolymer being dynamically vulcanized while this combination is mixed. The resulting rubber concentrate is, in turn, blended with an engineering thermoplastic to provide the desired TPE. Silicone rubber is disclosed as a possible elastomeric component, but no examples utilizing such a silicone are provided. Further, this publication specifically teaches that the polymeric carrier must not react with the cure agent for the curable copolymer.

Crorey et al. in U.S. Pat. No. 4,695,602 teach composites wherein a silicone semi-IPN vulcanized via a hydrosilation reaction is dispersed in a fiber-reinforced thermoplastic resin having a high flexural modulus. The silicones employed are of the type taught by Arkles, cited supra, and the composites are said to exhibit improved shrinkage and warpage characteristics relative to systems which omit the IPN.

Ward et al., in U.S. Pat. No. 4,831,071, disclose a method for improving the melt integrity and strength of a high modulus thermoplastic resin to provide smooth-surfaced, high tolerance profiles when the modified resin is melt-drawn. As in the case of the disclosures to Arkles et al., cited supra, a silicone mixture is cured via a hydrosilation reaction after being dispersed in the resin to form a semi-IPN, and the resulting composition is subsequently extruded and melt-drawn.

U.S. Pat. No. 6,013,715 to Gornowicz et al. teaches the preparation of TPSIV elastomers wherein a silicone gum (or filled silicone gum) is dispersed in either a polyolefin or a polyybutylene terephthalate) resins and the gum is subsequently dynamically vulcanized therein via a hydrosilation cure system. The resulting elastomers exhibit an ultimate elongation at break of at least 25% and have significantly improved mechanical properties over the corresponding simple blends of resin and silicone gum in which the gum is not cured (i.e., physical blends). This, of course, of great commercial significance since the vulcanization procedure, and the cure agents required therefor, add to both the complexity as well as the expense of the preparation and
vulcanization would be avoided in many applications if essentially identical mechanical properties could be obtained without its employ.

In a copending application (Ser. No. 09/393029 filed on Sep. 9, 1999) now U.S. Pat. No. 6,281,286 we disclose that the impact resistance of polyester and polyamide resins can be greatly augmented by preparing a thermoplastic silicone vulcanize therefrom wherein the elastomeric component is a silicone rubber base which comprises a silicone gum and a silica filler and the weight ratio of the base to the resin ranges from 10:90 to 35:65. Although the resulting thermoplastic materials have improved impact resistance, they do not exhibit sufficiently low modulus to be useful as elastomers.

While the above publications disclose the preparation of compositions using various thermoplastic resins as the matrix and a dispersed phase consisting of a silicone oil or elastomer which is dynamically vulcanized therein, neither these references, nor any art known to applicants, teach the preparation of TPSIV elastomers based on polyamide resins having superior tensile and elongation properties.

**SUMMARY OF THE INVENTION**

It has now been discovered that TPS IV elastomers of the type described in above cited U.S. Pat. No. 6,013,715 can be prepared from certain polyamide resins wherein the silicone component is a base comprising a diorganopolysiloxane gum and a reinforcing filler. As in the case of the teachings of U.S. Pat. No. 6,013,715, the elastomers disclosed herein generally also have good appearance, have an elongation of at least 25% and have a tensile strength and/or elongation at least 25% greater than that of the corresponding simple (physical) blend wherein the diorganopolysiloxane is not cured. However, it has been surprisingly found that such properties are significantly enhanced when a minor portion of a hindered phenol compound is incorporated in the formulation. Moreover, inclusion of the hindered phenol apparently also results in a lower melt viscosity of the instant thermoplastic elastomer vulcanizes, as reflected by process torque measurements during mixing. This reduction is of considerable value to fabricators since the elastomers of the present invention can be more readily processed in conventional equipment (e.g., extruders, injection molders) and results in lower energy consumption. Furthermore, unlike the teachings of Arkles, cited supra, and others, the silicone component which is dispersed in the thermoplastic resin, and dynamically cured therein, must include a high molecular weight gum, rather than a low viscosity silicone fluid, the latter resulting in compositions having poor uniformity.

The present invention, therefore, relates to a thermoplastic elastomer prepared by

(I) mixing

(A) an organohydrido silicon compound which contains an average of at least 2 silicon-bonded hydrogen groups in its molecule and

(B) a hindered phenol compound.

(D) an organohydrido silicon compound which contains an average of at least 2 silicon-bonded hydrogen groups in its molecule and

(E) a hydrosilation catalyst, components (D) and (E) being present in an amount sufficient to cure said diorganopolysiloxane (B); and

(II) dynamically curing said diorganopolysiloxane (B), wherein said thermoplastic elastomer has an elongation of at least 25%.

The invention further relates to a thermoplastic elastomer which is prepared by the above method.

**DETAILED DESCRIPTION OF THE INVENTION**

Component (A) of the present invention is a thermoplastic polyamide resin. These resins are well known by the generic term “nylon” and are long chain synthetic polymers containing amide (i.e., —CO—NH—) linkages along the main polymer chain. For the purposes of the present invention, the polyamide resin has a melt point (m.p.) or glass transition temperature (Tg) of room temperature (i.e., 25° C.) to 275° C. Attempts to prepare TPSIV elastomers from polyamides having higher melt points (e.g., nylon 4/6) resulted in poor physical properties, the ultimate elongation of such products being less than the required 25% according to the present invention. Furthermore, for the purposes of the present invention, the polyamide resin must be dry, this preferably being accomplished by passing a dry, inert gas over resin pellets or powder at elevated temperatures. Again, it has been found that TPSIVs prepared from as-supplied resins often do not meet the elongation requirements of the present invention. The degree of drying consistent with acceptable properties and processing depends on the particular polyamide and its value is generally recommended by the manufacturer or may be determined by a few simple experiments. It is generally preferred that the polyamide resin contains no more than about 0.1 weight percent of moisture. Finally, the polyamide must also be thermally stable under the mixing conditions required to prepare the TPSIV elastomer, as described infra. This stability is evaluated on the neat resin at the appropriate processing temperature and a change of more than 20% in melt viscosity (mixing torque) within the time generally required to prepare the corresponding TPSIVs (e.g., 10 to 30 minutes in a bowl mixer) indicates that the resin is outside the scope of the present invention. Thus, for example, a dried nylon 11 sample having a m.p. of 198° C. was mixed in a bowl mixer under a nitrogen gas purge at about 210 to 220° C. for about 15 minutes and the observed mixing torque increased by approximately 200%. Such a polyamide resin is not a suitable candidate for the instant method.

Other than the above mentioned limitations, resin (A) can be any thermoplastic crystalline or amorphous high molecular weight solid homopolymer, copolymer or terpolymer having recurring amide units within the polymer chain. In copolymer and terpolymer systems, more than 50 mole percent of the repeat units are amide-containing units.

Examples of suitable polyamides are polyamidates such as nylon 6, polycatenolactam (nylon 7), polycaprylactam (nylon 8), polylaurylactam (nylon 12), and the like; homopolymers of amino acids such as polyglycolalalaminone (nylon 4); copolyamides of dicarboxylic acid and diamine such as nylon 6/6, polyhexamethyleneazalamide (nylon 6/9), polyhexamethylenesalicamid (nylon 6/10), polyhexamethyleneisophthalamid (nylon 6/1), polyhexamethyleneadecanoic acid (nylon 6/12) and the like; aromatic and partially aromatic polyamides; copolyamides such as...
copolymers of caprolactam and hexamethyleneadipamide (nylon 6/6.6), or a terpolyamide, e.g., nylon 6/6,6/6.10; block copolymers such as polyether polyamides; or mixtures thereof. Preferred polyamide resins are nylon 6, nylon 12, nylon 6/12 and nylon 6/6.

Silicone base (B) is a uniform blend of a diorganopolysiloxane gum (B') a reinforcing filler (B'').

Diorganopolysiloxane (B') is a high consistency (gum) polymer or copolymer which contains at least 2 alkyl groups having 2 to 20 carbon atoms in its molecule. The alkyl group is specifically exemplified by vinyl, allyl, butenyl, pentenyl, hexenyl and decenyl. The position of the alkyl functionality is not critical and it may be bonded at the molecular chain terminals, in non-terminal positions on the molecular chain or at both positions. It is preferred that the alkyl group is vinyl or hexenyl and that this group is present at a level of 0.001 to 3 weight percent, preferably 0.01 to 1 weight percent, in the diorganopolysiloxane gum.

The remaining (i.e., non-alkyl) silicon-bonded organic groups in component (B') are independently selected from hydrocarbon or halogenated hydrocarbon groups which contain no aliphatic unsaturation. These may be specifically exemplified by alkyl groups having 1 to 20 carbon atoms, such as methyl, ethyl, propyl, butyl, pentyl and hexyl; cycloalkyl groups, such as cyclohexyl and cyclohexyl; aryl groups having 6 to 12 carbon atoms, such as phenyl, tolyl and xylol; aralkyl groups having 7 to 20 carbon atoms, such as benzyl and phenethyl; and halogenated alkyl groups having 1 to 20 carbon atoms, such as 3,3,3-trifluoropropyl and chloromethyl. It will be understood, or course, that these groups are selected such that the diorganopolysiloxane gum (B') has a glass temperature (or melt point) which is below room temperature and the gum is therefore elastomeric. Methyl preferably makes up at least 50, more preferably at least 90, mole percent of the non-saturated silicon-bonded organic groups in component (B').

Thus, polydiorganosiloxane (B') can be a homopolymer or a copolymer containing such organic groups. Examples include gums comprising dimethylosiloxane units and phenylmethylsiloxane units; dimethylosiloxane units and diphenylosiloxane units; and dimethylosiloxane units and phenylmethylsiloxane units, among others. The molecular structure is also not critical and is exemplified by straight-chain and partially branched straight-chain, linear structures being preferred.

Specific illustrations of organopolysiloxane (B') include: trimethylsiloxy-endblocked dimethylsiloxane-methylhexenylosiloxano copolymers; dimethylhexenylosiloxane-endblocked dimethylsiloxano copolymers; trimethylsiloxy-endblocked dimethylsiloxano-methylenylvinylsiloxano copolymers; trimethylsiloxy-endblocked methylphenylsiloxano-dimethylsiloxano-methylenylvinylsiloxano copolymers; dimethylnvinylsiloxano-endblocked dimethylnvinylsiloxano; dimethylnvinylsiloxano-endblocked dimethylnvinylsiloxano copolymers; dimethylnvinylsiloxano-endblocked methylphenylsiloxano copolymers and similar copolymers wherein at least one end group is dimethylhydroxyisiloxo. Preferred systems for low temperature applications include methylphenylsiloxane-dimethylsiloxano-methylvinylsiloxano copolymers and dimethylnvinylsiloxano-dimethylnvinylsiloxano methylvinylsiloxano copolymers, particularly wherein the molar content of the dimethylsiloxane units is about 93%.

Component (B') may also consist of combinations of two or more organopolysiloxanes. Most preferably, component (B') is a polydimethylsiloxane homopolymer which is terminated with a vinyl group at each end of its molecule or is such a homopolymer which also contains at least one vinyl group along its main chain.

For the purposes of the present invention, the molecular weight of the diorganopolysiloxane gum is sufficient to impart a Williams plasticity number of at least about 30 as determined by the American Society for Testing and Materials (ASTM) test method 926. The plasticity number, as used herein, is defined as the thickness in millimeters of a cylindrical test specimen 2 cm² in volume and approximately 10 mm in height after the specimen has been subjected to a compressive load of 49 Newtons for three minutes at 25°C. When the plasticity of this component is less than about 30, as in the case of low viscosity siloxanes employed by Arkles, cited supra, the TPSIVs prepared by dynamic vulcanization according to the instant method exhibit poor uniformity such that at high silicone contents (e.g., 50 to 70 weight percent) there are regions of essentially only silicone and those of essentially only thermoplastic resin, and the blends are weak and friable. The gums of the present invention are considerably more viscous than the silicone fluids employed in the prior art. For example, silicones contemplated by Arkles, cited supra, have an upper viscosity limit of 100,000 cP (0.1 m²/s) and, although the plasticity of fluids of such low viscosity are not readily measured by the ASTM D 926 procedure, it was determined that this corresponds to a plasticity of approximately 24. Although there is no absolute upper limit on the plasticity of component (B'), practical considerations of processability in conventional mixing equipment generally restrict this value. Preferably, the plasticity number should be about 100 to 200, most preferably about 120 to 185.

Methods for preparing high consistency unsaturated group-containing polydiorganosiloxanes are well known and they do not require a detailed discussion in this specification. For example, a typical method for preparing an alkyl-functional polymer comprises the base-catalyzed equilibration of cyclic and/or linear diorganopolysiloxanes in the presence of similar alkyl-functional species.

Component (B'') is a finely divided filler which is known to reinforce diorganopolysiloxane (B') and is preferably selected from finely divided, heat stable minerals such as fumed and precipitated forms of silica, silica aerogels and titanium dioxide having a specific surface area of at least about 50 m²/g. The fumed form of silica is a preferred reinforcing filler based on its high surface area, which can be up to 450 m²/g and a fumed silica having a surface area of 50 to 400 m²/g, most preferably 200 to 380 m²/g, is highly preferred. Preferably, the fumed silica filler is treated to render its surface hydrophobic, as typically practiced in the silicone rubber art. This can be accomplished by reacting the silica with a liquid organosilicon compound which contains silanol groups or hydrolyzable precursors of silanol groups. Compounds that can be used as filler treating agents, also referred to as anti-creeping agents or plasticizers in the silicone rubber art, include such ingredients as low molecular weight liquid hydroxy- or alkoxy-terminated polydiorganosiloxanes, hexaorganosiloxanes, cyclo-dim-


ethylsilazanes and hexorganodisilazanes. It is preferred that the treating compound is an oligomeric hydroxy-terminated diorganopolsiloxane having an average degree of polymerization (DP) of 2 to about 100, more preferably about 2 to about 10 and it is used at a level of about 5 to 50 parts by weight for each 100 parts by weight of the silica filler. When component (B) is the preferred vinyl-functional or hexenyl-functional polydimethylsiloxane, this treating agent is preferably a hydroxy-terminated polydimethylsiloxane.

For the purposes of the present invention, 5 to 200 parts by weight, preferably 5 to 150 and most preferably 20 to 100 parts by weight, of the reinforcing filler (B') are uniformly blended with 100 parts by weight of gum (B') to prepare silicone base (B). This blending is typically carried out at room temperature using a two-roll mill, internal mixer or other suitable device, as well known in the silicone rubber art. Alternatively, the silicone base can be formed in-situ during mixing prior to dynamic vulcanization of the gum, as further described infra. In the latter case, the temperature of mixing is kept below the softening point or melting point of the polyamide resin until the reinforcing filler is well dispersed in the diorganopolsiloxane gum.

 Hindered phenol (C) is an organic compound having at least one group of the structure in its molecule. In the above formula, R is an alkyl group having one to four carbon atoms and R' is a hydrocarbon group having four to eight carbon atoms. For the purposes of the present invention, a group according to formula (i) can be attached to hydrogen to form a 1,5-di-organophenol. Preferably, one to four of these groups are attached to an organic moiety of corresponding valence such that the contemplated compound has a molecular weight (MW) of less than about 1,500. Most preferably, four such groups are present in component (C) and this compound has a molecular weight of less than 1,200. This monovalent (or polyvalent) organic moiety can contain heteroatoms such as nitrogen, oxygen, phosphorus, and sulfur. The R' groups in the above formula may be illustrated by t-butil, n-pentyl, butylxyl, hexylxyl, cyclopropyl, cyclohexyl and phenyl. It is preferred that both R and R' are t-butil.

Non-limiting specific examples of component (C) include various hindered phenols marketed by Ciba Specialty Chemicals Corporation under the tradename Irganox™:

- Irganox™ 1076 octadecyl 3,5-di-tert-butyl-4-hydroxyphenoxybenzylate
- Irganox™ 1035 ethylenediamine bis(3,5-di-tert-butyl-4-hydroxyphenoxybenzylate)
- Irganox™ MD1024 1,2-bis(3,5-di-tert-butyl-4-hydroxyphenoxybenzylamine) hydroxydiphenylmethane
- Irganox™ 1330 1,3,5-trimethyl-2,4,6-tris(3,5-di-tert-butyl-4-hydroxyphenoxybenzyl)benzene
- Irganox™ 1425 WLC calcium bis(monoethyl(3,5-di-tert-butyl-4-hydroxyphenoxybenzyl)phosphonate) and Irganox™ 3114 1,3,5-tris(3,5-di-tert-butyl-4-hydroxyphenoxybenzyl)-1,3,5-triazine-2,4,6(1H,3H,5H)-trione.

Preferred hindered phenols are Irganox™ 245 [triethylenglycol bis (3,3’-tert-butyl-4’-hydroxy-5’-methylphenyl) propionate], Irganox™ 1098 [N,N’-hexamethylenbis(3,5-di-tert-butyl-4-hydroxyphenoxybenzylamine)] and Irganox™ 1010 [tetrakis(methylene(3,5-di-tert-butyl-4-hydroxyphenoxybenzyl) methane).

From 0.1 to 5 parts by weight of hindered phenol (C) are employed for each 100 parts by weight of polyamide (A) plus silicone base (B). Preferably 0.1 to 0.75 parts by weight, more preferably 0.475 to 0.525 parts by weight, of (C) are added for each 100 parts by weight of (A) plus (B).

The organohyridro silcone compound (D) is a crosslinker (cure agent) for diorganopolsiloxane (B) of present composition and is an organopolsiloxane which contains at least 2 silicon-bonded hydrogen atoms in each molecule, but having at least about 0.1 weight percent hydrogen, preferably 0.2 to 2 and most preferably 0.5 to 1.7, percent hydrogen bonded to silicon. Those skilled in the art will, of course, appreciate that either component (B') or component (D), or both, must have a functionality greater than 2 if diorganopolsiloxane (B) is to be cured (i.e., the sum of these functionalities must be greater than 4 on average). The position of the silicon-bonded hydrogen component (D) is not critical, and it may be bonded at the molecular chain terminals, in non-terminal positions along the molecular chain or at both positions. The silicon-bonded organic groups of component (D) are independently selected from any of the hydrocarbon or halogenated hydrocarbon groups described above in connection with diorganopolsiloxane (B), including preferred embodiments thereof. The molecular structure of component (D) is also not critical and is exemplified by straight-chain, partially branched straight- chain, branched, cyclic and network structures, linear polymers or copolymers being preferred, this component should be compatible with diorganopolsiloxane (B) (i.e., it is effective in curing component (B)).

Component (D) is exemplified by the following:

low molecular siloxanes, such as PhSi(OSMe)3H;
trimethylsiloxy-endblocked methylhydridopolysiloxanes;
trimethylenesiloxy-endblocked dimethyldisiloxy-methylhydridopolysiloxane copolymers;
dimethyldisiloxy-endblocked dimethylpolysiloxanes;
dimethylhydrogensiloxy-endblocked methylhydrogenpolysiloxanes;
dimethyldisiloxy-endblocked dimethylhydrogendisiloxane copolymers;
cyclical methylhydrogenpolysiloxanes;
cyclic dimethylsiloxane-methylhydridopolysiloxane copolymers;
tetrasil(dimethylhydrogensiloxy)silane;
silicone resins composed of (CH3)2H2SiO1/2, (CH3)3 SiO1/2, and SiO2/3 units and silicone resins composed of (CH3)2H2SiO1/2, (CH3)3 SiO1/2, CH3SiO3/2, PhSiO3/2, and SiO2/3 units, wherein Me and Ph hereinafter denote methyl and phenyl groups, respectively.

Particularly preferred organohyridro silicone compounds are polymers or copolymers comprising RH3O units ended with either R′3SiO1/2 or HR′3SiO1/2 wherein R is independently selected from alkyl groups having 1 to 20 carbon atoms, phenyl or trifluoroisopropyl, preferably methyl. It is also preferred that the viscosity of component (D) is about 0.5 to 1,000 mPa-s at 25° C., preferably 2 to 500 mPa-s. Further, this component preferably has 0.5 to 1.7 weight percent hydrogen bonded to silicon. It is highly preferred that
Component (D) is selected from a polymer consisting essentially of methylhydridosiloxane units or a copolymer consisting essentially of dimethylsiloxane units and methylhydridosiloxane units, having 0.5 to 1.7 percent hydrogen bonded to silicon and having a viscosity of 2 to 500 mPa·s at 25°C. It is understood that such a highly preferred system will have terminal groups selected from trimethylsiloxy or dimethylhydridosiloxane groups.

Component (D) may also be a combination of two or more of the above described systems. The organohydroxy silcon compound (D) is used at a level such that the molar ratio of SiH vinyl siloxane units to Si-enethyl in component (B) is greater than 1 and preferably below about 50, more preferably 3 to 30, most preferably 4 to 20.

These SiH-functional materials are well known in the art and many of them are commercially available.

Hydrosilation catalyst (E) is a catalyst that accelerates the cure of diorganopolysiloxane (B) in the present composition. This hydrosilation catalyst is exemplified by platinum catalysts, such as platinum black, platinum supported on silica, platinum supported on carbon, chloroplatinic acid, alcohol solutions of chloroplatinic acid, platinum/cellulose complex, platinum/alumina complex, platinum/beta-diketone complexes, platinum/phosphine complexes and the like; rhodium catalysts, such as rhodium chloride and rhodium chloride/di(n-butyl)sulfide complex and the like; and palladium catalysts, such as palladium on carbon, palladium chloride and the like. Component (E) is preferably a platinum-based catalyst such as chloroplatinic acid; platinum dichloride; platinum tetrachloride; a platinum complex catalyst produced by reacting chloroplatinic acid and divinyltetramethyldisiloxane which is diluted with dimethylvinylsiloxane or a platinum silane reagent prepared according to U.S. Pat. No. 3,419,593 to Willing; and a neutralized complex of platinous chloride and divinyltetramethylsiloxane, prepared according to U.S. Pat. No. 5,175,325 to Brown et al., these patents being hereby incorporated by reference. Most preferably, catalyst (E) is a neutralized complex of platinous chloride and divinyltetramethylsiloxane.

Component (E) is added to the present composition in a catalytic quantity sufficient to promote the reaction of components (B) and (D) and thereby cure the diorganopolysiloxane elastomer which is typically added so as to provide about 0.1 to 500 parts per million (ppm) of metal atoms based on the total weight of the thermoplastic elastomer composition, preferably 0.25 to 100 ppm.

In addition to the above mentioned major components (A) through (E), a minor amount (i.e., less than about 40 weight percent of the total composition, preferably less than 20 weight percent) of an optional additive (F) can be incorporated in the compositions of the present invention. This optional additive can be illustrated by, but not limited to, reinforcing fillers for polyamide resins, such as glass fibers and carbon fibers; extending fillers such as asphalt, calcium carbonate, and diatomaceous earth; pigments such as iron oxide and titanium oxide, electrically conducting fillers such as carbon black and finely divided metals, heat stabilizers such as hydrated ceric oxide, antioxidants, flame retardants such as halogenated hydrocarbons, alumina trihydrate, magnesium hydroxide, organophosphorus compounds and other fire retardant (FR) materials. A preferred FR additive is calcium silicate particulate, preferably a wollastonite having an average particle size of 2 to 30 μm. Further, this optional component can be a plasticizer for the silicone gum component, such as polymethylsiloxane oil, and/or a plasticizer for the polyamide component. Examples of the latter include phthalate esters such as decyclohexyl phthalate, dimethyl phthalate, diethyl phthalate, butyl benzyl phthalate and benzyl phthalate; trimellitate esters such as C_10-C_15 alkyl trimellitate; sulfonamides such as N-cyclohexyl-2-toluenesulfonamide, N-ethyl-o,p-toluenesulfonamide and o-toluenesulfonamide, and liquid oligomeric plasticizers. Preferred plasticizers are liquids with low volatility to avoid emissions of plasticizer at the common melt temperatures of polyamides.

The above additives are typically added to the final thermoplastic composition after drying cure, but they may also be added at any point in the preparation provided they do not interfere with the dynamic vulcanization mechanism. Of course, the above additional ingredients are only used at levels which do not significantly detract from the desired properties of the final composition.

According to the method of the present invention, the thermoplastic elastomer is prepared by thoroughly dispersing silicone base (B) and hindered phenol (C) in polyamide (A) and dynamically vulcanizing the diorganopolysiloxane using organohydroxy silcon compound (D) and catalyst (E). For the purposes of the present invention, the weight ratio of silicone base (B) to polyamide (A) is greater than 35:65. It has been found that when this ratio is 35:65 or less, the resulting vulcanizate generally has a modulus more resembling the polyamide resin than a thermoplastic elastomer. On the other hand, the above mentioned ratio should be no more than about 85:15 since the compositions tend to be weak and resemble cured silicone elastomers above this value. Notwithstanding this upper limit, the maximum ratio of (B) to (A) for any given combination of components is also limited by processability considerations since too high a silicone base content results in at least a partially crosslinked continuous phase which is no longer thermoplastic. For the purposes of the present invention, this practical limit is readily determined by routine experimentation and represents the highest level of component (B) which allows the TPSIV to be compression molded. It is, however, preferred that the final thermoplastic elastomer can also be readily processed in other conventional plastic operations, such as injection molding and extrusion and, in this case, the weight ratio of components (B) to (A) should be no more than about 75:25. Such a preferred thermoplastic elastomer which is subsequently re-processed generally has a tensile strength and elongation which are within 10% of the corresponding values for the original TPSIV (i.e., the thermoplastic elastomer is little changed by re-processing). Although the amount of silicone base consistent with the above mentioned requirements depends upon the particular polyamide resin and other components selected, it is preferred that the weight ratio of components (B) to (A) is 40:60 to 75:25, more preferably 40:60 to 70:30.

Mixing is carried out in any device which is capable of uniformly dispersing the components in the polyamide resin, such as an internal mixer or a twin-screw extruder, the latter being preferred for commercial preparations. The temperature is preferably kept as low as practical consistent with good mixing so as not to degrade the resin. Depending upon the particular system, order of mixing is generally not critical and, for example, components (A), (C) and (D) can be added to (B) at a temperature above the softening point (melt point) of (A), catalyst (E) then being introduced to initiate dynamic vulcanization. However, components (B) through (D) should be polyamide resin (A) before dynamic vulcanization begins. As previously mentioned, it is also contemplated that the silicone base can be formed in-situ. For example, the reinforcing filler may be added to
a mixer already containing the polyamide resin and diorganopolysiloxane gum at a temperature below the softening point (melt point) of the resin to thoroughly disperse the filler in the gum. The temperature is then raised to melt the resin, the other ingredients are added and mixing/dynamic Vulcanization are carried out. Optimum temperatures, mixing times and other conditions of the mixing operation depend upon the particular resin and other components under consideration and these may be determined by routine experimentation by those skilled in the art. It is, however, preferred to carry out the mixing and dynamic Vulcanization under a dry, inert atmosphere (i.e., one that does not adversely react with the components or otherwise interfere with the hydrolysis cure), such as dry nitrogen, helium or argon. It has been observed that there is actually a preferred dry gas flow rate with respect to mechanical properties of the final TPSIV as well as the melt viscosity thereof (see examples, infra).

When the melting point or glass temperature of the polyamide is considerably higher than room temperature (e.g., greater than 100°C), a preferred procedure comprises preparing a pre-mix by blending dried polyamide resin (A), silicone base (B), hindered phenol (C) and organohydroxil silicone gum (D) below the melt temperature of the resin (e.g., at ambient conditions). This pre-mix is then melted in a bowl mixer or internal mixer using a dry inert gas purge and at a controlled temperature which is just above the melt point to about 35°C above the melt point of the polyamide (e.g., 210°C to 215°C) for nylon 12 which, depending on molecular weight, has a melt point of about 175°C~180°C) and catalyst (E) is mixed therewith. Mixing is continued until the melt viscosity (mixing torque) reaches a steady state value, thereby indicating that dynamic vulcanization of the diorganopolysiloxane of component (B) is complete.

As noted above, in order to be within the scope of the present invention, the tensile strength or elongation, or both, of the TPSIVs must be at least 25% greater than that of a corresponding simple blend. A further requirement of the invention is that the TPSIV has at least 25% elongation, as determined by the test described infra. In this context, the term “simple blend” denotes a composition wherein the weight proportions of resin (A), base (B) and hindered phenol (C) are identical to the proportions in the TPSIV, but no silicone compound (D) below the melt temperature (or component (E), or both, are omitted and the gum is therefore not cured). In order to determine if a particular composition meets the above criterion, the tensile strength of the TPSIV is measured on dumbbells having a length of 25.4 mm and a width of 3.2 mm and a typical thickness of 1 to 2 mm, according to ASTM method D 412, at an extension rate of 50 mm/min. At least three such samples are evaluated and the results averaged after removing obvious low readings due to sample inhomogeneity (e.g., such as voids, contamination or inclusions). These values are then compared to the corresponding average tensile and elongation values of a sample prepared from the simple blend composition. When at least a 25% improvement in tensile and/or elongation over the simple blend is not realized there is no benefit derived from the dynamic vulcanization and such TPSIVs are not within the scope of the present invention.

The thermoplastic elastomer prepared by the above described method can then be processed by conventional techniques such as extrusion, vacuum forming, injection molding, blow molding, overmolding or compression molding. Moreover, these compositions can be re-processed (recycled) with little or no degradation of mechanical properties.

The novel thermoplastic elastomers of the present invention can be used for fabricating wire and cable insulation, electrical connectors, automotive and appliance components such as belts, hoses, air ducts, boots, bellows, gaskets and fuel line components, architectural seals, bottle closures, medical devises, sporting goods and general rubber parts.

EXAMPLES

The following examples are presented to further illustrate the compositions and method of this invention, but are not to be construed as limiting the invention, which is delineated in the appended claims. All parts and percentages in the examples are on a weight basis and all measurements were obtained at 25°C, unless indicated to the contrary.

Materials

The following materials, listed alphabetically for ease of reference, were employed in the examples.

BASE 1 is a silicone rubber base made from 68.7% PDMS 1, defined infra, 25.8% of a fumed silica having a surface area of about 250 m²/g (Cab-O-Sil® MS-75 by Cabot Corp., Tuscola, Ill.), 5.4% of a hydroxy-terminated diorganopolysiloxane having an average degree of polymerization (DP) of about 8 and 0.02% of ammonia.

BASE 2 is a silicone rubber base made from 76.6% PDMS 1, defined infra, 17.6% of a fumed silica having a surface area of about 250 m²/g, 5.7% of a hydroxy-terminated diorganopolysiloxane having an average degree of polymerization (DP) of about 8 and 0.02% of ammonia.

BASE 3 is similar to BASE 1 wherein only 5% of fumed silica is present.

CATALYST 1 is a 1.5% platinum complex of 1,3-dienylidene-1,1,3,3-tetramethyldisiloxane; 6.0% tetramethylvinylidimethyldisiloxane; 92% dimethylvinyl ended polydimethylsiloxane and 0.5% dimethylcyclopolsiloxanes having 6 or greater dimethylsiloxane units.

IRGANOX™ 245 is a hindered phenol marketed by Ciba Specialty Chemicals Corporation, Tarrytown, N.Y., and described as triethylene glycol bis [3-(3,5-di-tert-butyl-4'-hydroxy-5'-methylphenyl)propionate],

IRGANOX™ 1010 is a hindered phenol stabilizer marketed by Ciba Specialty Chemicals Corporation and described as tetrakis (methylene(3,5-di-tert-butyl-4'-hydroxyphenyl)methyl)methane.

IRGANOX™ 1098 is a hindered phenol described as N,N'-hexamethylene-bis (3,5-di-tert-butyl-4'-hydroxyhydrocinnamamide) and marketed by Ciba Specialty Chemicals Corporation.

NYLON 11 is nylon 11 obtained from Aldrich Chemical Co., Milwaukee, Wis.; m.p.=198°C.

NYLON 12-A is nylon 12 obtained from Aldrich Chemical Co.; m.p.=178°C.

NYLON 12-B is Rilsan™ AMNO, a nylon 12 marketed by Elf Atochem NA, Inc., Philadelphia, Pa.; m.p.=175°C.

NYLON 4/6 is nylon 4/6 obtained from Aldrich Chemical Co.; m.p.=295°C.

NYLON 6 is nylon 6 obtained from Aldrich Chemical Co. m.p.=228.5°C.

NYLON 6/6-A is Zytel™ E42 A NC 010 nylon 6/6 obtained from DuPont.; m.p.=262°C.

NYLON 6/6-B is nylon 6/6 obtained from Aldrich Chemical Co.; m.p.=267°C.

NYLON 6/6-C is nylon 6/6 marketed by Solutia, Inc. (St. Louis, Mo.) under the tradename Vydrene™ 66B; m.p.=260°C.

NYLON 6/12 is nylon 6/12 obtained from Aldrich Chemical Co.; m.p.=218°C.
PDMS 1 is a gum consisting of 99.81 wt % MeSiO units, 0.16% MeViSiO units and 0.03% MeViSiO\(_{1/2}\) units, wherein Vi hereinafter represents a vinyl group. Prepared by potassium catalyzed equilibration of cyclic siloxanes wherein the catalyst is neutralized with carbon dioxide. This gum has plasticity of about 150.

PDMS 2 is a gum similar to PDMS 1 but having 99.97 wt % MeSiO units, and 0.03% MeViSiO\(_{1/2}\) units and plasticity of about 150.

PDMS 3 is a gum similar to PDMS 1 but having 97.70 wt % MeSiO units, 2.27% MeViSiO units and 0.03% MeViSiO\(_{1/2}\) units and plasticity of about 150.

PDMS 4 is a gum similar to PDMS 1 but having 87.05 wt % MeSiO units, 12.76% PhMeSiO units, 0.16% MeViSiO units and 0.03% Me\(_2\)ViSiO\(_{1/2}\) units and plasticity of about 150.

X-LINKER 1 is an SiH-functional crosslinker consisting essentially of 68.4% MeHSiO units, 28.1% MeSiO units and 3.5% MeSiO\(_{1/2}\) units and has a viscosity of approximately 29 mPa.s. This corresponds to the average formula MD\(_1\)D\(_{2/3}\)M, in which (hereinafter) M is (CH\(_3\))\(_3\)Si—O—, D is —Si(CH\(_3\))—O—and D’ is —Si(H)(CH\(_3\))—O—.

X-LINKER 2 is a fluid similar to X-LINKER 1 having the average formula MD\(_1\)D\(_{2/3}\)M.

X-LINKER 3 is a fluid similar to X-LINKER 1 having the average formula MD\(_{10}\)D\(_{2/3}\)M.

X-LINKER 4 is a fluid similar to X-LINKER 1 having the average formula MD\(_{10}\)D\(_{2/3}\)M.

X-LINKER 5 is a fluid similar to X-LINKER 1 having the average formula MD\(_{10}\)D\(_{2/3}\)M.

X-LINKER 6 is a fluid similar to X-LINKER 1 containing about 68% D’ units and having a viscosity of approximately 100 mPa.s.

**EXAMPLES A1–A17**

NYLON 12-A (80.0 g) was dried at 120°C for two hours in a desiccating oven (i.e., a drying oven in which hot air is dried over a desiccant bed and then passed through a heated oven containing the sample to be dried in a continuous flow cycle). This resin was then melted at 210°C at 60 rpm in a Haake System 9000™ miniaturized internal mixer (310 ml bowl) under a dry nitrogen atmosphere using roller rotors. IRGANOX™ 1010 (0.24 g) was added and mixed for approximately 3.5 minutes and then BASE 1 (1200 g) was mixed in. After about 3 minutes, X-LINKER 1 (3.8 g) was added, at which point the mixer torque was approximately 1800 m-g. After another 3.5 minutes, CATALYST 1 (57 drops=0.855 g) was added and the torque started to rise sharply. After seven additional minutes, the torque increased to 16,400 m-g, mixing was stopped and the resulting nylon was filtered.

As can be seen from a comparison of Examples A1 and A3, increasing the hindered phenol content resulted in improved physical properties. Further, formulations based on NYLON 11 did not result in a product having sufficient elongation, this polyeamide exhibiting unstable rheology under these conditions. Likewise, NYLON 4/6 has a melt point above 275°C and, again, resulted in poor mechanical properties even at a higher hindered phenol content.

**TABLE A1**

<table>
<thead>
<tr>
<th>Example</th>
<th>IRGANOX™ Content (g)</th>
<th>Nylon Type</th>
<th>Set Process Temp. (°C)</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (m-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. A1</td>
<td>0.24</td>
<td>12</td>
<td>210</td>
<td>12.5</td>
<td>134</td>
<td>16,400</td>
</tr>
<tr>
<td>Comp. Ex. A2 (PB)</td>
<td>0.24</td>
<td>12</td>
<td>210</td>
<td>3.0</td>
<td>22</td>
<td>1,700</td>
</tr>
<tr>
<td>Ex. A3</td>
<td>1</td>
<td>12</td>
<td>210</td>
<td>14.5</td>
<td>200</td>
<td>15,000</td>
</tr>
<tr>
<td>Comp. Ex. A4</td>
<td>0.24</td>
<td>11</td>
<td>215</td>
<td>6.4</td>
<td>17</td>
<td>12,000</td>
</tr>
<tr>
<td>Comp. Ex. A5</td>
<td>0.24</td>
<td>6/12</td>
<td>240</td>
<td>8.0</td>
<td>19</td>
<td>4,200</td>
</tr>
<tr>
<td>Comp. Ex. A6 (PB)</td>
<td>0.24</td>
<td>6/12</td>
<td>240</td>
<td>1.9</td>
<td>7</td>
<td>1,000</td>
</tr>
<tr>
<td>Ex. A7</td>
<td>1</td>
<td>6/12</td>
<td>240</td>
<td>15.8</td>
<td>141</td>
<td>3,900</td>
</tr>
<tr>
<td>Ex. A8</td>
<td>1</td>
<td>6</td>
<td>245</td>
<td>11.0</td>
<td>99</td>
<td>5,200</td>
</tr>
<tr>
<td>Ex. A9</td>
<td>1</td>
<td>6</td>
<td>245</td>
<td>10.3</td>
<td>76</td>
<td>4,000</td>
</tr>
<tr>
<td>Ex. A10</td>
<td>0.24</td>
<td>6</td>
<td>245</td>
<td>12.7</td>
<td>84</td>
<td>5,000</td>
</tr>
<tr>
<td>Ex. A11</td>
<td>0.24</td>
<td>6</td>
<td>245</td>
<td>7.4</td>
<td>39</td>
<td>8,000</td>
</tr>
<tr>
<td>Comp. Ex. A12 (PB)</td>
<td>0.24</td>
<td>6/12</td>
<td>240</td>
<td>1.6</td>
<td>6</td>
<td>1,000</td>
</tr>
<tr>
<td>Comp. Ex. A13</td>
<td>0.24</td>
<td>6/6-B</td>
<td>275</td>
<td>8.8</td>
<td>22</td>
<td>4,000</td>
</tr>
<tr>
<td>Comp. Ex. A14</td>
<td>1.0</td>
<td>6/6-A</td>
<td>275</td>
<td>2.2</td>
<td>4</td>
<td>7,800</td>
</tr>
<tr>
<td>Comp. Ex. A15 (PB)</td>
<td>0</td>
<td>6/6-B</td>
<td>285</td>
<td>1.25</td>
<td>6</td>
<td>1,200</td>
</tr>
<tr>
<td>Comp. Ex. A16</td>
<td>1</td>
<td>4/6</td>
<td>300</td>
<td>5.4</td>
<td>10</td>
<td>3,800</td>
</tr>
<tr>
<td>Comp. Ex. A17 (PB)</td>
<td>0</td>
<td>4/6</td>
<td>300</td>
<td>1.3</td>
<td>4</td>
<td>800</td>
</tr>
</tbody>
</table>

**PB** = Physical blend (no crosslinking)

[X-LINKER 6 used instead of X-LINKER 1 at same level.]

TPSIVs based on NYLON 12-A were prepared according to the methods of Example A1 wherein the total amount of BASE 1 and NYLON 12-A was maintained at 200 g but the ratio of these two components, as well as IRGANOX™ 1010 content, were varied, as shown in Table A2. The X-LINKER 1 amount was also adjusted to maintain a constant SiH/Vi ratio. The respective mechanical properties are also presented in this table.

**EXAMPLES A18–A21**

As can be seen from a comparison of Examples A1 and A3, increasing the hindered phenol content resulted in improved physical properties. Further, formulations based on NYLON 11 did not result in a product having sufficient elongation, this polyeamide exhibiting unstable rheology under these conditions. Likewise, NYLON 4/6 has a melt point above 275°C and, again, resulted in poor mechanical properties even at a higher hindered phenol content.
TABLE A2

<table>
<thead>
<tr>
<th>Example</th>
<th>IRGANOXTM 1010 Content (g)</th>
<th>Ratio of BASE 1 to NYLON 12-A</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (m-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. A18</td>
<td>0.18</td>
<td>70/30</td>
<td>3.14</td>
<td>28</td>
<td>13,000</td>
</tr>
<tr>
<td>Comp. Ex. A19</td>
<td>0.15</td>
<td>75/25</td>
<td>1.1</td>
<td>14</td>
<td>12,200</td>
</tr>
<tr>
<td>Ex. A20</td>
<td>0.12</td>
<td>80/20</td>
<td>2.85</td>
<td>64</td>
<td>10,000</td>
</tr>
<tr>
<td>Ex. A21</td>
<td>0.09</td>
<td>85/15</td>
<td>3.35</td>
<td>116</td>
<td>9,000</td>
</tr>
</tbody>
</table>

EXEMPLARY A22–A32

The above experiments were repeated using an IRGANOXTM 1010 content of 1 g in otherwise similar formulations wherein the ratio of base to NYLON 12-A was varied, the results being shown in Table A3.

TABLE A3

<table>
<thead>
<tr>
<th>Example</th>
<th>IRGANOXTM 1010 Content (g)</th>
<th>Ratio of BASE 1 to NYLON 12-A</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (m-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. A22</td>
<td>1</td>
<td>60/40</td>
<td>14.9</td>
<td>200</td>
<td>15,000</td>
</tr>
<tr>
<td>Comp. Ex. A23 (PB)</td>
<td>1</td>
<td>65/35</td>
<td>19.1</td>
<td>150</td>
<td>1,500</td>
</tr>
<tr>
<td>Ex. A24</td>
<td>1</td>
<td>70/30</td>
<td>11.5</td>
<td>19</td>
<td>12,000</td>
</tr>
<tr>
<td>Comp. Ex. A25 (PB)</td>
<td>1</td>
<td>75/25</td>
<td>9.4</td>
<td>14</td>
<td>2,000</td>
</tr>
<tr>
<td>Ex. A26</td>
<td>1</td>
<td>80/20</td>
<td>6.8</td>
<td>24</td>
<td>1,800</td>
</tr>
<tr>
<td>Ex. A27 (PB)</td>
<td>1</td>
<td>85/15</td>
<td>5.9</td>
<td>14</td>
<td>1,400</td>
</tr>
</tbody>
</table>

PB = Physical blend (no crosslinking)

It is clear from Table A4 that the combination of drying, dry nitrogen purge and inclusion of IRGANOXTM 1010 provides the best mechanical properties.

EXAMPLES A39–A43

TPSIVs based on dried NYLON 12-B were prepared according to the methods of Example A1 wherein the flow rate of dry nitrogen to the mixer was varied. The results are shown in Table A5, wherein the flow rate is reported in m³/min.

TABLE A4

<table>
<thead>
<tr>
<th>Example</th>
<th>Drying/Nitrogen/</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (m-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. A33</td>
<td>+/+/+</td>
<td>5.0</td>
<td>21</td>
<td>550</td>
</tr>
<tr>
<td>Ex. A34</td>
<td>+/-/+</td>
<td>6.67</td>
<td>25</td>
<td>550</td>
</tr>
<tr>
<td>Ex. A35</td>
<td>*/ */+</td>
<td>33.6</td>
<td>115</td>
<td>&gt;3,150</td>
</tr>
<tr>
<td>Comp. Ex. A36</td>
<td>*/ */+</td>
<td>4.96</td>
<td>15</td>
<td>650</td>
</tr>
<tr>
<td>Comp. Ex. A37</td>
<td>*/ */+</td>
<td>5.77</td>
<td>19</td>
<td>3,200</td>
</tr>
<tr>
<td>Comp. Ex. A38</td>
<td>*/ */+</td>
<td>2.58</td>
<td>14</td>
<td>1,200</td>
</tr>
</tbody>
</table>

It can be seen that the sample prepared without the nitrogen purge (Example A43) had relatively poor mechanical properties, although within the requirements of the invention. Additionally, there is an apparent optimum nitrogen flow rate with respect to good mechanical properties and low process viscosity (i.e., low torque).

EXAMPLES A44–A51

NYLON 6/6-B (80.0 g) was dried at 120°C for two hours in a desiccating oven (i.e., hot air is dried over a desiccant bed and then passed through a heated oven containing the sample in a continuous flow cycle). The resin was melted at 275°C at 60 rpm in a Haake System 9000® miniaturized internal mixer (310 ml bowl) under a dry nitrogen atmosphere using roller rotors. BASE 1 (120.0 g) was added 4 minutes after addition of polyamide. IRGANOXTM 1010 (1.0 gram) was added 2.5 minutes later and mixed for approximatively 2.5 minutes. X-LINKER 1 (3.8 g) was added, at which point the mixer torque was approximately 1,100 m-g. After another 3.5 minutes, CATALYST 1 (57 drops = 0.855 g) was added and the torque started to rise. After 18 additional minutes, the torque increased to 5,800 m-g, mixing was stopped and the resulting nylon TPSIV sample was removed from the bowl. The resulting TPSIV was molded at 285°C and tested, as described above, the results being shown in Table A6 (Example A44).

Similar compositions were prepared using NYLON 6/6-A and NYLON 6/6-C, these results also being presented in
Table A6. In these examples the order of mixing was varied, as shown in the second column of Table A6, wherein N, Irg. and Base denote the nylon, IRGANOX™ 1010 and BASE 1, respectively.

<table>
<thead>
<tr>
<th>Example</th>
<th>Order of addition</th>
<th>Torque (mN)</th>
<th>Nylon Type</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. A44</td>
<td>N/Base/Irg.</td>
<td>5,800</td>
<td>NYLON 6/6-B</td>
<td>14.8</td>
<td>81</td>
</tr>
<tr>
<td></td>
<td>(Comp.) Base/Irg.</td>
<td>8,000</td>
<td>NYLON 6/6-A</td>
<td>5.57</td>
<td>10</td>
</tr>
<tr>
<td>Ex. A45</td>
<td>N/1rg./Base</td>
<td>8,000</td>
<td>NYLON 6/6-B</td>
<td>14.8</td>
<td>81</td>
</tr>
<tr>
<td></td>
<td>(Comp.) Irg./N</td>
<td>8,000</td>
<td>NYLON 6/6-A</td>
<td>5.57</td>
<td>10</td>
</tr>
<tr>
<td>Ex. A46</td>
<td>Base/Irg./N</td>
<td>10,200</td>
<td>NYLON 6/6-A</td>
<td>8.70</td>
<td>26</td>
</tr>
<tr>
<td></td>
<td>(Comp.) Base/N/Irg.</td>
<td>7,900</td>
<td>NYLON 6/6-A</td>
<td>5.41</td>
<td>9</td>
</tr>
<tr>
<td>Ex. A47</td>
<td>N/Irg./Base</td>
<td>8,400</td>
<td>NYLON 6/6-C</td>
<td>9.33</td>
<td>33</td>
</tr>
<tr>
<td></td>
<td>(Comp.) Irg./N</td>
<td>10,000</td>
<td>NYLON 6/6-C</td>
<td>7.66</td>
<td>23</td>
</tr>
<tr>
<td>Ex. A49</td>
<td>N/1rg./Base</td>
<td>9,800</td>
<td>NYLON 6/6-C</td>
<td>7.45</td>
<td>16</td>
</tr>
<tr>
<td></td>
<td>(Comp.) Irg./N</td>
<td>15,000</td>
<td>NYLON 6/6-C</td>
<td>6.86</td>
<td>14</td>
</tr>
</tbody>
</table>

Table A6 illustrates our observation that it is more difficult to prepare TPSiVs having high tensile/elongation properties as the melting point of the polyamide approaches 275°C. Nevertheless, routine experimentation does provide compositions within the scope of the present invention.

**EXAMPLES B1**

NYLON 12-B was dried at 120°C for 18 hours in a dessicating oven, as described above in Example A1. A pre-mix of this dried polyamide was prepared by blending the following components in a Haake Rheomix™ 3000 mounted on a PolyLab™ miniaturized internal mixer using sigma blade rotors (free volume=541 cm³):

- 210.4 g BASE 1
- 6.60 g X-LINKER 1
- 1.75 g IRGANOX™ 1010
- 140.0 g NYLON 12-B

Blending was carried out at 20°C and a rotor speed of 60 rpm, until a stable torque reading was observed. The resulting pre-mix (210.8 g) was fed to a Rheomix™ 3000 bowl fitted with roller rotors (free volume=310 cm³) at 210°C, 60 rpm using a dry nitrogen purge at a flow rate of 0.5 standard cubic feet per minute (236 cm³/s). As previously noted, mixing torques observed in this series should not be compared with those obtained using the above described Haake System 9000™ mixer. The set temperature was reduced to 200°C, and when the mixing torque began to level out, indicating that the nylon had melted and the pre-mix had reached the set temperature, 57 drops (0.912 g) of CATALYST 1 were added. When the torque again reached a steady state value (5,800 mN-g), the resulting TPSiV was removed.

The above process was compression molded at 225°C, for 5 minutes and exhibited a tensile strength of 2631 psi (18.1 MPa) and an elongation of 298% according to ASTM method D 412, as described in Example A1 with the exception that at least 5 tensile measurements were averaged.

**EXAMPLES B2–B5**

The procedures of Example B1 were followed wherein NYLON 12-A served as the polyamide resin and the type of hindered phenol was varied. In each case, 120.0 g of the polyamide, 80.0 g of BASE 1 and 3.8 g of X-LINKER 1 were pre-mixed using sigma blades. This premix was dynamically cured by adding 1 g of the hindered phenol indicated in Table B1 and 0.912 g of CATALYST 1. This table also shows the respective mechanical properties of molded test specimens.

**TABLE B1**

<table>
<thead>
<tr>
<th>Example</th>
<th>Hindered Phenol</th>
<th>Terminal Torque (mN-g)</th>
<th>Ultimate Tensile Strength (MPa)</th>
<th>Elongation at Break (%)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. B2</td>
<td>IRGANOX™ 1010</td>
<td>7,150</td>
<td>16.2</td>
<td>251</td>
</tr>
<tr>
<td>Ex. B3</td>
<td>IRGANOX™ 1010</td>
<td>9,090</td>
<td>16.3</td>
<td>237</td>
</tr>
<tr>
<td>Ex. B4</td>
<td>IRGANOX™ 1010</td>
<td>10,000</td>
<td>13.2</td>
<td>151</td>
</tr>
<tr>
<td>Comp. Ex. B5</td>
<td>none</td>
<td></td>
<td>10,000</td>
<td>12.2</td>
</tr>
</tbody>
</table>

It can be seen from Table B1 that omitting the hindered phenol reduces ultimate mechanical properties.

**EXAMPLES C1–C4**

Nylon TPSiVs were prepared according to the methods of Example B1 wherein different siloxane gums having various vinyl contents were used. In each case, the respective gum shown in Table C1 was used in place of PDMS 1 in the formulation of BASE 1 to prepare a similar silicone base, the latter then being used in the following proportions to provide the final TPSiV:

**TABLE C1**

<table>
<thead>
<tr>
<th>Example</th>
<th>Gum</th>
<th>Content of Vinyl (wt %)</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (mN-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. C1</td>
<td>PDMS 2</td>
<td>0.012</td>
<td>10.9</td>
<td>100</td>
<td>12,000</td>
</tr>
<tr>
<td>Ex. C2</td>
<td>PDMS 1</td>
<td>0.0562</td>
<td>15.7</td>
<td>150</td>
<td>20,000</td>
</tr>
<tr>
<td>Ex. C3</td>
<td>PDMS 3</td>
<td>0.753</td>
<td>10.8</td>
<td>30</td>
<td>6,000</td>
</tr>
<tr>
<td>Ex. C4</td>
<td>PDMS 4</td>
<td>0.0596</td>
<td>14.5</td>
<td>150</td>
<td>6,000</td>
</tr>
</tbody>
</table>

**EXAMPLES C5–C7**

Nylon TPSiVs were prepared according to the methods of Example C1 wherein different silicone bases having various levels of silica filler were used. In each case, the respective base shown in Table C2 was used in the following formulation to provide the final TPSiV:

<table>
<thead>
<tr>
<th>Example</th>
<th>Gum</th>
<th>Content of Vinyl (wt %)</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (mN-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>NYLON 12-A</td>
<td>80 g</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>IRGANOX™ 1010</td>
<td>1 g</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>SILICONE BASE</td>
<td>120 g</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>X-LINKER 1</td>
<td>3.0 g</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>CATALYST 1</td>
<td>0.86 g</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
</tbody>
</table>
TABLE C2

<table>
<thead>
<tr>
<th>Example</th>
<th>Silicone Base</th>
<th>Tensile (MPa)</th>
<th>Elongation (%)</th>
<th>Torque (m-g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ex. C5</td>
<td>BASE 1</td>
<td>13.5</td>
<td>160</td>
<td>17,500</td>
</tr>
<tr>
<td>Ex. C6</td>
<td>BASE 2</td>
<td>10.9</td>
<td>107</td>
<td>11,000</td>
</tr>
<tr>
<td>Ex. C7</td>
<td>BASE 3</td>
<td>4.11</td>
<td>30</td>
<td>1,800</td>
</tr>
</tbody>
</table>

From Table C3 it is seen that X-LINKER 1 provides the best overall mechanical properties while X-LINKER 5 is does not meet the requirements of the invention under the conditions of this series of experiments.

What is claimed is:

1. A method for preparing a thermoplastic elastomer, said method comprising:

(I) mixing

(A) a rheologically stable polyamide resin having a melting point or glass transition temperature of 25°C to 275°C,

(B) a silicone base comprising

(B) 100 parts by weight of a diorganopolysiloxane having a plasticity of at least 30 and having an average of at least 2 alkynyl radicals in its molecule and

(B') 5 to 200 parts by weight of a reinforcing filler, the weight ratio of said silicone base to said polyamide resin being greater than 35:65 to 85:15,

(C) 0.1 to 5 parts by weight of a hindered phenol compound for each 100 parts by weight of said polyamide and said silicone base,

(D) an organohydril silicone compound which contains an average of at least 2 silicon-bonded hydrogen groups in its molecule and

(E) a hydroisolation catalyst, components (D) and (E) being present in an amount sufficient to cure said diorganopolysiloxane (B'); and

(II) dynamically curing said diorganopolysiloxane (B'), wherein at least one property of the thermoplastic elastomer selected from tensile strength or elongation is at least 25% greater than the respective property for a corresponding simple blend wherein said diorganopolysiloxane is not cured and said thermoplastic elastomer has an elongation of at least 25%.

2. The method according to claim 1, wherein the weight ratio of said silicone base (B) to said polyamide resin (A) is greater than 35:65 to 75:25.

3. The method according to claim 2, wherein said polyamide is selected from the group consisting of nylon 6, nylon 6/6, nylon 6/12 and nylon 12.

4. The method according to claim 2, wherein said diorganopolysiloxane (B') is a gum selected from the group consisting of a copolymer consisting essentially of dimethylsiloxane units and methylvinylsiloxane units and a copolymer consisting essentially of dimethylsiloxane units and methylhexenylsiloxane units and said reinforcing filler (B') is a fumed silica.

5. The method according to claim 4, wherein said organohydril silicone component (D) is selected from the group consisting of a polymer consisting essentially of methylhydridosiloxane units and a copolymer consisting essentially of dimethylsiloxane units and methylhydridosiloxane units, having 0.5 to 1.7 weight percent hydrogen bonded to silicon and having a viscosity of 2 to 500 mPa·s at 25°C. and said catalyst (E) is a neutralized complex of platinous chloride and divinyltetramethyldisiloxane.

6. The method according to claim 3, wherein the weight ratio of said silicone base (B) to said polyamide resin (A) is 40:60 to 70:30.

7. The method according to claim 2, wherein said hindered phenol has a molecular weight of less than 1,200 and contains 2 to 4 groups of the formula

\[
\text{R} - \text{OH}
\]

in which R and R' are tert-butyl groups.

8. The method according to claim 4, wherein said fumed silica is present at a level of 20 to 100 parts by weight for each 100 parts by weight of said diorganopolysiloxane (B').

9. The method according to claim 8, wherein said polyamide resin is selected from the group consisting of nylon 6, nylon 6/6, nylon 6/12 and nylon 12.

10. The method according to claim 3, wherein said hindered phenol is selected from the group consisting of trihydroxybenzaldehyde (3,3'-tert-butyl-4'-hydroxy-5'-methylphenylpropionate), N,N'-hexamethylenebis(3,5-di-tert-butyl-4-hydroxyhydrocinnamamide) and tetrakis (methylene(3,5-di-tert-butyl-4-hydroxy-hydrocinnamate)) methane.

11. The method according to claim 10, wherein the weight ratio of said silicone base (B) to said polyamide resin (A) is 40:60 to 70:30.

12. The method according to claim 4, wherein said polyamide has a melt point greater than 100°C. and wherein a pre-mix of components (A) through (D) is first prepared at a temperature below the melting point of the polyamide, said catalyst (E) is subsequently added to said pre-mix at a temperature above the melt point and said diorganopolysiloxane (B') is then dynamically vulcanized.


15. A thermoplastic elastomer prepared by the method of claim 3.

A thermoplastic elastomer prepared by the method of claim 5.
A thermoplastic elastomer prepared by the method of claim 6.
A thermoplastic elastomer prepared by the method of claim 7.
A thermoplastic elastomer prepared by the method of claim 8.
A thermoplastic elastomer prepared by the method of claim 9.

A thermoplastic elastomer prepared by the method of claim 10.
A thermoplastic elastomer prepared by the method of claim 11.
A thermoplastic elastomer prepared by the method of claim 12.