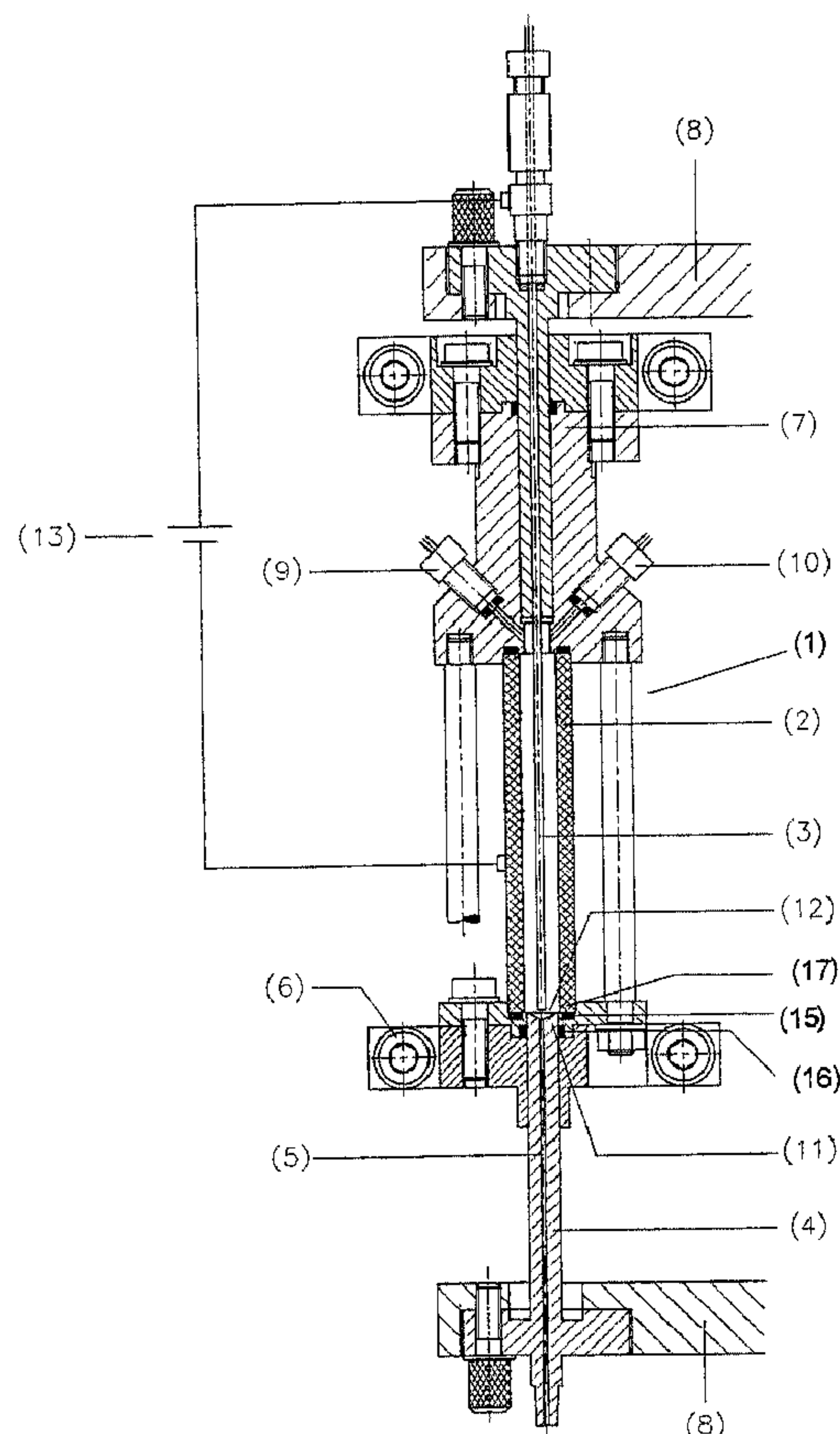




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(54) Titre : CELLULE D'ECOULEMENT ET PROCEDE DE SEPARATION DE RADIONUCLEIDES DEPOURVUS DE
PORTEURS, ET LEUR CONVERSION RADIOCHIMIQUE
(54) Title: FLOW CELL AND METHOD OF SEPARATING CARRIER-FREE RADIONUCLIDES AND THEIR
RADIOCHEMICAL REACTION



(57) Abrégé/Abstract:

The invention relates to a flow cell, a method for separating carrier-free radionuclides from a liquid or liquefiable target material, and the radiochemical reaction thereof. According to prior art, flow cells are known which require reaction volumes corresponding to



(57) **Abrégé(suite)/Abstract(continued):**

the volume of the target material in order to carry out the desired reactions. The inventive flow cell (1) and method enable the reaction volume, and thus the quantity of starting material, to be reduced by a multiple by reducing the cylinder volume (= reaction volume). As the radioactively marked product is present in very small quantities (picomole to nanomole), the HPL-chromatographic separation of the non-reacted starting material is significantly improved. The economic efficiency of the method is increased due to the fact that small quantities of starting material can be used.

Abstract

The invention relates to a flow cell, a method for separating carrier-free radionuclides from a liquid or liquefiable target material, and the radiochemical reaction thereof. According to prior art, flow cells are known which require reaction volumes corresponding to the volume of the target material in order to carry out the desired reactions. The inventive flow cell (1) and method enable the reaction volume, and thus the quantity of starting material, to be reduced by a multiple by reducing the cylinder volume (= reaction volume). As the radioactively marked product is present in very small quantities (picomole to nanomole), the HPL-chromatographic separation of the non-reacted starting material is significantly improved. The economic efficiency of the method is increased due to the fact that small quantities of starting material can be used.

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T R A N S L A T I O N

D e s c r i p t i o n

5 *FLOW CELL AND METHOD OF SEPARATING CARRIER-FREE RADIONUCLIDES AND
THEIR RADIOCHEMICAL REACTION*

10

The invention relates to a flow cell as well as to a method of separating carrier-free radionuclides from liquids or liquifiable target material and their radiochemical reactions.

15

Radionuclides can be made by nuclear conversion processes in a cyclotron, for example by irradiating a suitable target with protons. An exact description of a method of separating carrier-free radionuclides from a target liquid is known, for example, from German patent DE 195 00 428, issued July 13, 1995.

20

From German patent document DE 195 00 428 a device is also known (a flow cell) for the separation of carrier-free radionuclides from a target liquid, which is comprised substantially of a cylinder of a glass carbon (Sigradur®) and an axial platinum canula through which a cylindrical vessel can be
25 filled or emptied through which the inert gas can be fed into the

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chamber. The system is fixed by means of a plastic support and is sealed. Into the lower end a flat funnel is worked which opens into the duct carrying off the water. In the head of the support, there is a gas feed line as well as an opening through which the gas can be discharge. The cylinder of glass carbon (Sigradur®) and the platinum canula are connected to a direct current source and can be switched to serve either as the cathode or anode. For the recovery of the desired radionuclide, for example, (^{18}F) fluoride from (^{18}O) H_2O , the flow cell is filled with (^{18}F) fluoride containing target water. The (^{18}F) fluoride is anodically deposited on the surface of the cylinder and the (^{18}O) water is transported out of the latter. The height of the zone at which the (^{18}F) fluoride is anodically fixed is identical with the level of the (^{18}O) water in the cell.

In order that the radioisotope fixed on the surface can be completely transferred to another liquid phase by reversal of the polarity of the electric filled, it is necessary to match the amount of the educt supplied to the level in the cell to which the latter was filled with the (^{18}O) water. For the subsequent (^{18}F) fluoridation, therefore, a reaction volume must be provided which corresponds to that of the target water. Thus it is necessary to match the quantity of the educt so that it corresponds at the optimal educt concentration to this volume (for example 1.3 ml). Because of the very small quantities or proportions of these products (picomols to nonomols) with respect to the proportion of

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unoriented educt (μmol), difficulties in separation occur during purification and especially during chromatographic purification. Since the mass of the educt significantly exceeds the mass of the product, an HPL-chromatographic separation can only be run with poor resolution.

5 It is thus an object of embodiments of the invention to provide a device and a method whereby the reaction volume can be reduced. It is a further object of the invention to reduce the amount of material of the educt by a multiple while maintaining the optimum educt concentration.

10 In one broad aspect of the invention, there is provided a flow cell for separating carrier-free radionuclides from liquid or liquefiable target material and effecting a radiochemical reaction with the separated radionuclides, the flow cell comprising: a cylinder extending along and centered on an axis and having upper and lower ends; a cannula extending axially in the cylinder from one of the cylinder ends and having a cannula end in the cylinder; a piston extending axially
15 in the cylinder from the other of the cylinder ends and having a piston end spacedly juxtaposed with the cannula end, the piston having an outer surface separated from an inner surface of the cylinder by a gap between the cylinder and the piston, a volume ratio between the cylinder and the gap being equal to between 4.1 and 10.1; and supply means for applying a voltage differential
20 between the inner surface of the cylinder and the cannula.

 With the flow cell according to embodiments of the invention and the method, it is possible directly to reduce the cylinder volume (= reaction volume) and thereby reduce the quantity of the educt also by a multiple. The reduction of the quantity of the educt simplifies the chromatographic purification and enables a
25 quantitative separation of the carrier-poor marker compound (product) from the educt. Since reduced educt quantities can be used, the costs are reduced and the economy of the method enhanced.

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The drawing shows an embodiment of the method and the device according to the invention by way of example.

In the drawing:

FIG. 1 is a cross section through the flow cell in position I;

5 FIG. 2 is a cross section through the flow cell in position II; and

FIG. 3 is a cross-section taken along line A-A of Fig. 2.

FIG. 1 shows the flow cell 1 with a cylinder 2 receiving a canula 3 which is bounded from below by a piston 4 with a bore 5 connected by a yoke 6 with a canula holder 7. The cylinder 2 can be filled with liquid or inert gas through
10 the canula 3. The flow cell 1 is fixed by a support 8 and sealed. In the head part of the support 8, there are two feed lines 9 and 10 through which the gases can be fed to the device or carried away. In the head of the piston 11, there is a flat funnel 12 which opens into a bore 5. The cylinder 2 and the canula 3 are connected to a direct current source 13 and can be selectively switched for use as
15 the cathode or

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anode. In position I, the canula 3 is located at the lower end of the cylinder 2. The piston 4 is located outside the cylinder 2. In the lower region 17 of the cylinder, two sealing rings 15 and 16 seal the piston 4 with respect to the cylinder 2.

5

In FIG. 2 the same features of the device have been represented by the same reference numerals. FIG. 2 shows the arrangement of the components of the flow cell 1 in Position II, with the piston 4 shifted into the cylinder 2. The canula 3 is pushed out of the cylinder 2 by the amount to which the piston 4 projects into the cylinder 2. Between the piston 4 and the cylinder 2, an annular gap 14 is formed. In FIG. 2 at the lower portion of the cylinder, a section plane has been marked by the reference character "A".

15

FIG. 3 shows the flow cell 1 in position II in a section along the section plane A. The annular gap 14 can be seen between the piston 4 and the cylinder 2.

20

The invention is described by way of example below.

25

At the beginning of the reaction the components of the flow cell 1 are arranged, for example, as follows (see also FIG. 1; Position I); the lower opening of the canula 3, which is preferably made from platinum is located at the lower end 17 of the cylinder 2 and the piston 4 is located externally of the cylinder 2. The flow

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cell 1 is filled through the bore 5 or the duct 3 with the (^{18}F) fluoride containing target water, whereby the (^{18}F) fluoride is anodically deposited on the surface of the cylinder 2 to which a DC voltage of, for example, 20 volts is applied via the DC voltage source 13. The canula 3 here serves as the cathode. The cylinder 2 is made in an advantageous embodiment of the device of a pore-free inert material, like for example carbon glass (Sigradur®), a noble metal or platinum.

The piston 4 should preferably be made from an inert material. As suitable material, for example PEEK (polyetheretherketon), quartz glass or implement glass have been found to be suitable. It is, however, also possible to use a piston of an electrically conductive material which can then also be used as an electrode. The gap width or the difference in radius between the cylinder 2 and the piston 4 is dependent upon the fabrication method. Preferred is a radius difference between the cylinder 2 and the piston 4 of 0.4 mm. Suitable however also are gap widths of ≤ 0.2 mm. For the ratio of the radii between the cylinder (r_1) and the piston (r_2), the following equations can apply:

$$F_1 = r_1^2 * \pi$$

where F_1 = the area of the cylinder 2

$$F_2 = r_2^2 * \pi$$

where F_2 = the area of the piston 4

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$$F_3 = F_1 - F_2 = \pi(r_1^2 - r_2^2) \quad \text{where } F_3 = \text{the area of the gap 14}$$

$$V_3 = r_1^2 - r_2^2 = (r_1 + r_2)(r_1 - r_2) \quad \text{where } V_3 = \text{the volume of the gap 14}$$

$$5 \quad V_1/V_3 = r_1^2/r_1^2 - r_2^2 = r_1^2/(r_1 + r_2)(r_1 - r_2)$$

where V_1 = the volume of the cylinders 2.

After the filling of the flow cell with the target solution (for example ^{18}O water), the radio isotope (for example ^{18}F fluoride) is deposited on the inner surface of the cylinder 2 and the ^{18}O water is transported out of the flow cell 1 through the bore 5 in the piston 4. The height of the zone in which the (^{18}F) fluoride is anodically fixed, corresponds to the filling level of the ^{18}O water in the cylinder 2. The (^{18}F) fluoride fixed on the surface of the cylinder 2 is then completely dissolved in another liquid phase, like for example an organic phase transfer catalyst containing solution ($(\text{K}2.2.2)_2\text{C}_2\text{O}_4$ in dimethylsulfoxide = DMSO) by reversal of the electrical field. For that purpose it is necessary that the fill level of this liquid phase in the cylinder 2 match the filling state of the ^{18}O water which was previously set. To avoid the need for a reaction volume corresponding in amount to the target water volume for the subsequent nucleophilic (^{18}F) fluoridation, a displacement effect of the piston 4 is used. The piston 4 is shifted upwardly by a movement of the yoke 6 in this direction. Simultaneously the canula 3 is shifted in the cylinder

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2 corresponding to the height of the piston 4 out of the cylinder
2. The volume that thus must be introduced into the cylinder 2
must correspond to the volume of the gap 14 that is formed when the
piston 4 projects into the cell 1 (see FIG. 2, Position II) such
5 that the upper end of the piston 4 coincides with the fill level
which has been determined by the (^{18}F) fluoride fixed on the surface
of the cylinder 2. In an advantageous configuration of the device,
the ratio of the volume (V_1) of the cylinder 2 to the volume (V_3) of
the gap amounts to 4:1 to 10:1. In an especially preferred
10 configuration of the device, it amounts to 4:1. With an ^{18}O water
volume of, for example 1.3 ml, the volume of the gap 14 at a
fill level can amount to about 0.29 ml. When the piston is
shifted upwardly sufficiently that the upper end of the piston 4
coincides with the fill level determined by the (^{18}F) fluoride
15 fixed on the surface of the cylinder (see FIG. 2, piston B), the
(^{18}F) fluoride can be transferred to the reaction solution by
applying an electric belt (with the (Sigradur® as the cathode). In
this position, only the gap volume 14 is filled. The solution is
sealed at the lower end by two annular cylinders 15 and 16 (for
20 example O-rings) with respect to the piston 4 so that a lateral
outflow of liquid from the lower end of the cylinder is prevented.

For emptying the reaction vessel, the vessel 4 is again
lowered and the liquid transported outwardly through the canula 3
25 or the bore 5 of the piston 4.

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Transl. of PCT/DE03/00332

5 In an advantageous configuration of the device and the method, the feed or the evacuation of the (^{18}F) fluoride-containing target water and the organic solvent are effected through different conduits. When, for example, the supply of the (^{18}F) fluoride-
10 containing target water is effected through the conduit 3, the transport of the organic solvent which is used for desorption of the product is effected through the bore 5 to avoid a contamination of the conduit 3. Thus a high effort cleaning of the conduit for the target water can be avoided. The transport of the target water
15 will be self-understood to be possible also through the bore 5 and the transport of the organic solvent correspondingly through the conduit 3. It is important for a device which can be easily manipulated and the method that a separate conduit is provided for each of the different liquids.

15 Through the method of the invention and the device it is possible to reduce the educt quantity. This reduction in the mass of the educt is especially advantageous for the subsequent chromatographic separation of the carrier-poor ^{18}F -labeled product from the educt. In previously known methods and with previously
20 known devices for the separation of the carrier-free radionuclide and its radiochemical reaction, the educt quantity is significantly greater. Through the method and device according to the invention, the volume of the educt solution and thus the quantity of the educt is reduced by a multiple (at least 3 to 4 times) so that the

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chromatographic separation of educt and the ^{18}F -labeled product is significantly improved.

The reduction of the absolute educt quantity thus gives rise to a cost saving and therewith an improvement in the economy
5 of the method.

Example:

^{18}F -Labeling of N-Methylbenperidol

The (^{18}F) fluoride-containing ^{18}O water (1.3 ml) coming from the target of the cyclotron is transported into the flow cell
10 1 through the bore 5 of the piston 4. Upon application of an electrical voltage of 20 volts from a direct current source 13 (anode = cylinder (2) of carbon glass), the carrier-poor radio isotope is identically adsorbed within about 8 minutes on the surface of the cylinder 2. The ^{18}O water is driven out through the
15 bore 5 by means of helium. To dry the cylinder wall, the flow cell is filled once or twice each with 1.6 ml of water-free dimethylsulfoxide (DMSO) and emptied through the canula 3 serving as the counterelectrode. Through the canula 3, a solution of 5 mg Kryptate ($[\text{KC}2.2.2]_2\text{CO}_3$ in 300 μl DMSO) is introduced into the flow
20 cell 1 and piston 4 shifted by a motor so that the liquid surface reaches the upper boundary of the anodically deposited ^{18}F fluoride. The potential is reversed (-2V) and the cylinder is heated for 5 minutes to 100°C. After depolarization of the flow cell, the

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piston is brought into its lower position and through the canula 3 of a solution of 2 mg of N-methyl-desfluor-nitro-benperidol in 150 μ l of DMSO is supplied. The piston 4 is shifted again into the upper position and the flow cell is heated for 10 minutes to 150°C.

5 Then the flow cell is cooled with compressed air to ambient temperature. The flow cell is emptied through the canula 3, is washed with about 0.8 ml acetonitrile at 50°C and this solution is mixed with the DMSO product solution by a subsequent HPL-

10 chromatography, the radiotracer (^{18}F) N-methylbenperidol is purified and isolated.

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CLAIMS:

1. A flow cell for separating carrier-free radionuclides from liquid or liquefiable target material and effecting a radiochemical reaction with the separated radionuclides, the flow cell comprising:
 - 5 a cylinder extending along and centered on an axis and having upper and lower ends;
 - a cannula extending axially in the cylinder from one of the cylinder ends and having a cannula end in the cylinder;
 - a piston extending axially in the cylinder from the other of the
 10 cylinder ends and having a piston end spacedly juxtaposed with the cannula end, the piston having an outer surface separated from an inner surface of the cylinder by a gap between the cylinder and the piston, a volume ratio between the cylinder and the gap being equal to between 4.1 and 10.1; and
 - supply means for applying a voltage differential between the inner
 15 surface of the cylinder and the cannula.
 2. The flow cell according to claim 1 wherein the piston is comprised of chemically inert material.
 3. The flow cell according to claim 1 wherein the piston is composed of one of PEEK, implement glass and quartz glass.
 - 20 4. The flow cell according to claim 1 wherein the piston has a bore, the cell further comprising means for feeding a fluid through the bore.
 5. The flow cell according to claim 1 wherein the piston has a central bore, the cell further comprising means for feeding a fluid through the central bore.
 6. The flow cell according to claim 1 wherein the cylinder has a pore-
 25 free inert surface.

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7. The flow cell according to claim 1 wherein the cylinder is composed of chemically inert material.
8. The flow cell according to claim 1 wherein the cylinder is composed of carbon glass, a noble metal or platinum.
- 5 9. The flow cell according to claim 1 wherein the inner surface of the cylinder is electrically charged by the supply means.
10. The flow cell according to claim 1 wherein the cannula is electrically charged by the supply means.
11. The flow cell according to claim 9 wherein the cannula is a counter
10 electrode to the electrically charged cylinder.

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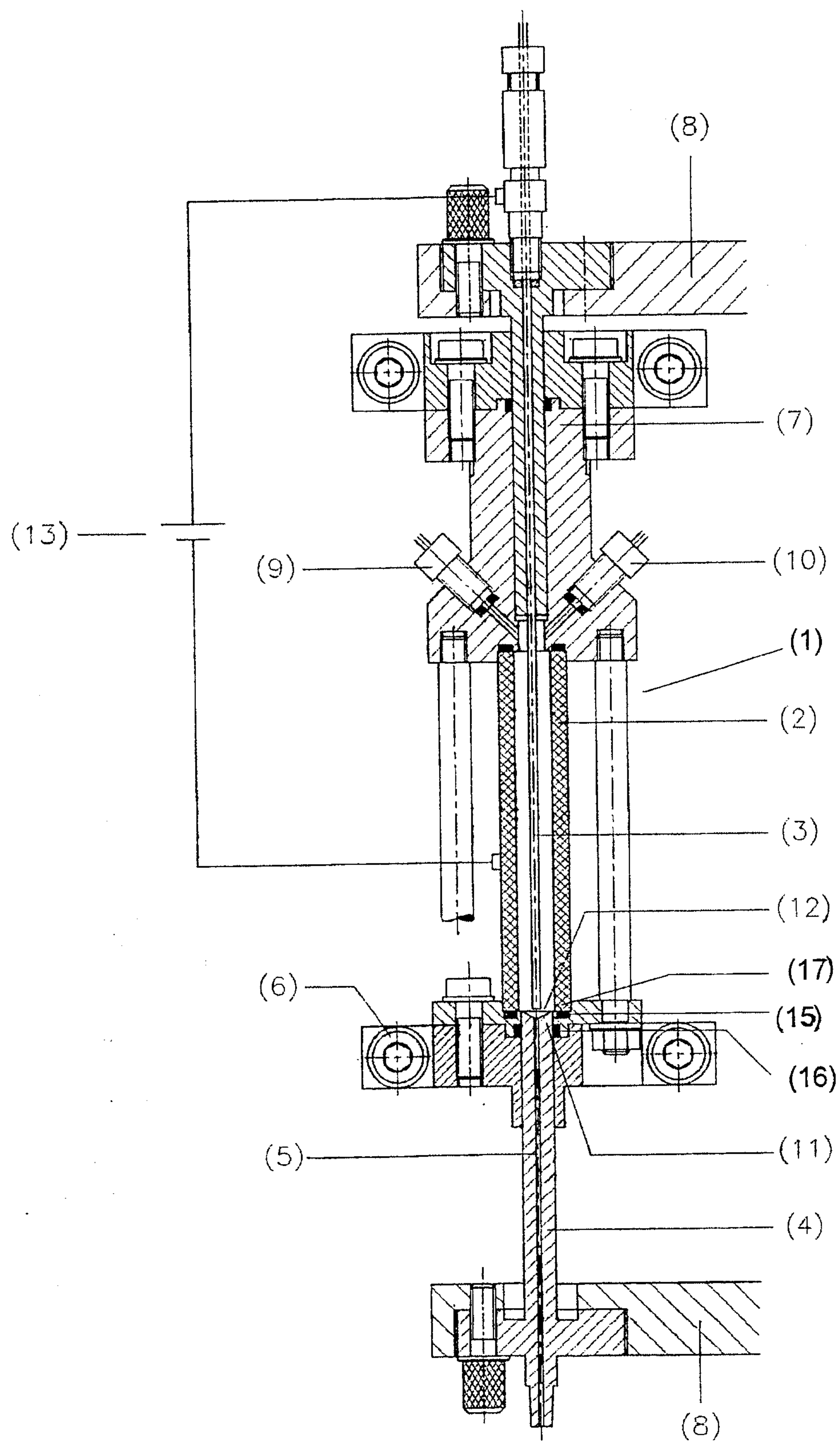


Fig. 1

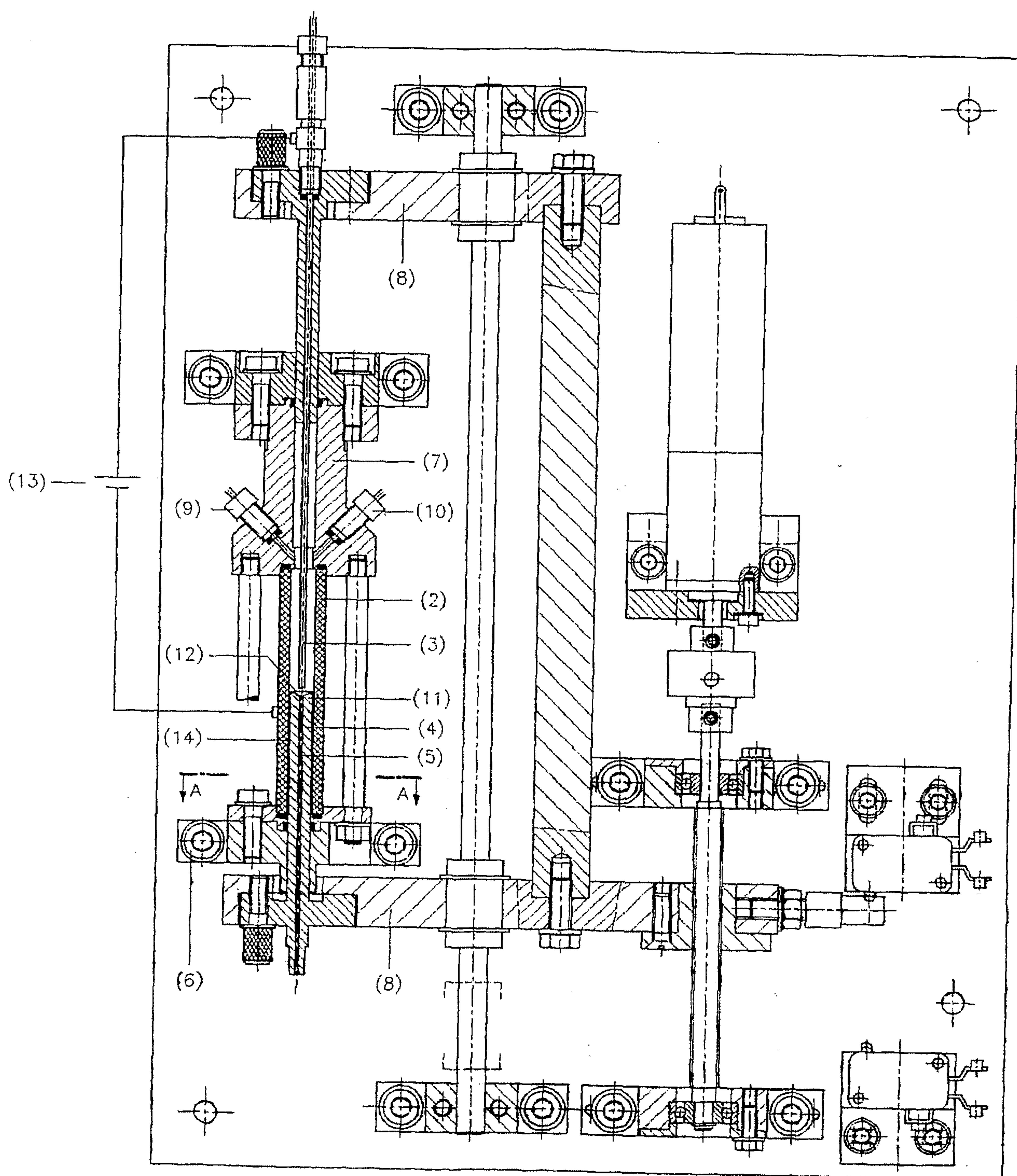


Fig. 2

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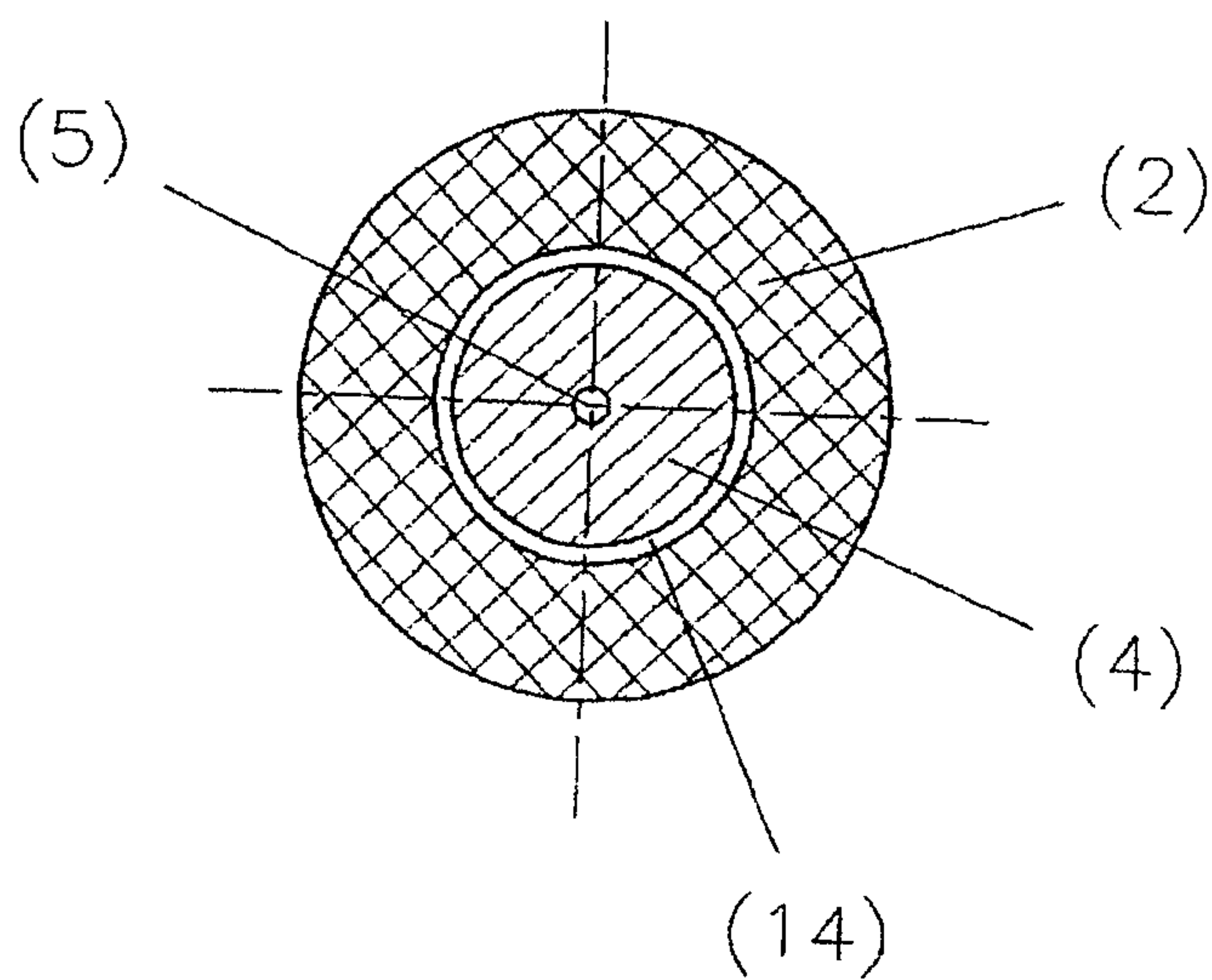


Fig. 3

