



(72) SCHMIDT, MARC, DE

(71) CABOT CORPORATION, US

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(54) **PROCEDE DE COMPACTAGE D'AEROGELS**

(54) **METHOD FOR COMPACTING AEROGELS**

(57) L'invention concerne un procédé de compactage de particules d'aérogel dans lequel les particules d'aérogel sont introduites dans un dispositif de compression et comprimées.

(57) The invention relates to a method for compacting aerogel particles, according to which said aerogel particles are placed in a pressing device and are compressed.



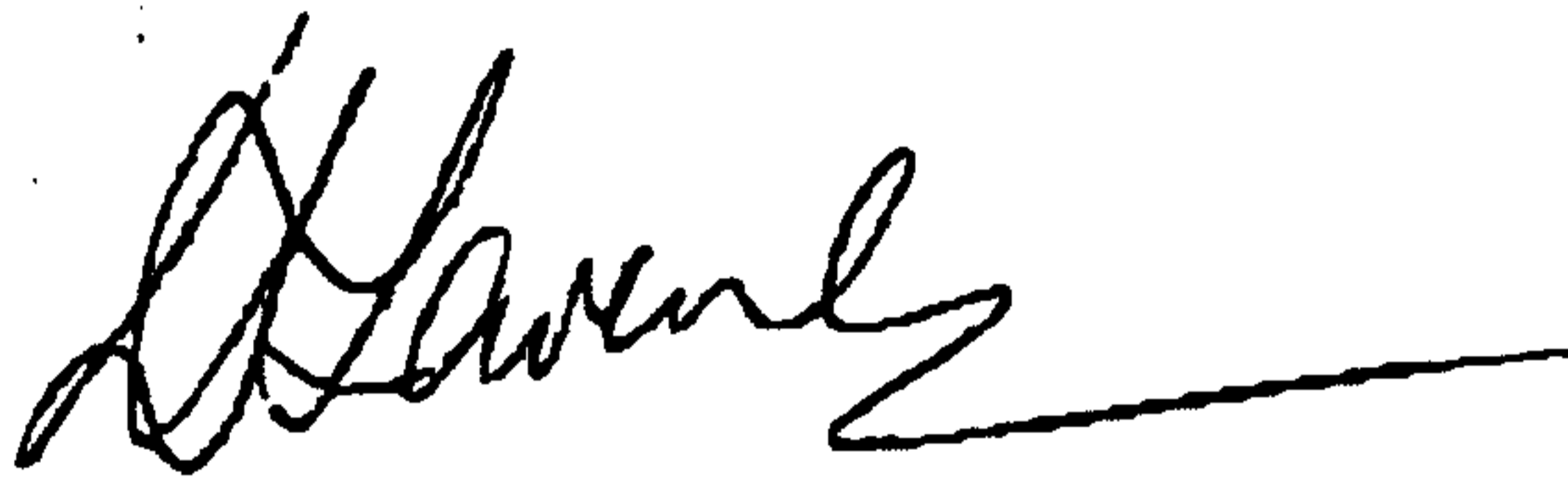
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<p>(21) Internationales Aktenzeichen: <b>PCT/EP98/02520</b> (22) Internationales Anmeldedatum: 29. April 1998 (29.04.98)  (30) Prioritätsdaten: 197 18 741.2 2. Mai 1997 (02.05.97) <b>DE</b>  (71) Anmelder (für alle Bestimmungsstaaten ausser US): <b>CABOT CORPORATION [US/US]; 75 State Street, Boston, MA 02109 (US).</b>  (72) Erfinder; und (75) Erfinder/Anmelder (nur für US): <b>SCHMIDT, Marc [DE/DE]; Raenthaler Weg 33, D-60529 Frankfurt (DE).</b>  (74) Anwälte: <b>MAI, Peter usw.; Luderschmidt, Schüler &amp; Partner, John-F.-Kennedy-Strasse 4, D-65189 Wiesbaden (DE).</b></p>	<p>(81) Bestimmungsstaaten: <b>CA, CN, JP, KR, MX, NO, US, europäisches Patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).</b></p> <p><b>Veröffentlicht</b> <i>Mit internationalem Recherchenbericht. Vor Ablauf der für Änderungen der Ansprüche zugelassenen Frist; Veröffentlichung wird wiederholt falls Änderungen eintreffen.</i></p>	
<p>(54) <b>Titel: METHOD FOR COMPACTING AEROGELS</b> (54) <b>Bezeichnung: VERFAHREN ZUR KOMPAKTIERUNG VON AEROGELN</b> (57) <b>Abstract</b> The invention relates to a method for compacting aerogel particles, according to which said aerogel particles are placed in a pressing device and are compressed. (57) <b>Zusammenfassung</b> Die vorliegende Erfindung betrifft ein Verfahren zur Kompaktierung von Aerogel-Partikeln, bei dem die Aerogel-Partikel in eine Preßvorrichtung gegeben und verpreßt werden.</p>		

IN THE MATTER OF  
International Patent Application PCT/EP98/02520  
filed 29<sup>th</sup> April 1998  
in the name of  
CABOT CORPORATION

I, DENNIS STANLEY TAVENER, Fellow of the Institute of Linguists and Member of the Institute of Translating and Interpreting, of 52 Garden Wood Road, East Grinstead, West Sussex RH19 1JU, hereby certify that I am the translator of the attached document and that it is a true translation to the best of my knowledge and belief of the original authentic text to be granted of the above-mentioned PCT application.

Signed this 23<sup>rd</sup> day of October 1999



(Dennis S. Tavener, FIL, MITI.)

The object of the present invention is a method of compacting aerogels.

Aerogels, particularly those with a porosity above 60% and a density of less than 0.6 g/cu.cm display extremely low thermal conductivity and are therefore used as a heat insulating material, as is described in EP-A-0 171 722, as catalysts or as catalyst carriers and also as adsorption material. Furthermore, by virtue of their very low refraction index for solid substances, it is known to use them for Cerenkov detectors. Furthermore, by reason of their particular acoustic impedance, the literature describes a possible use as an impedance adaptation means, for example in the ultrasound range.

It is also possible for them to be used as carriers for effective substances in pharmacy or agriculture.

Aerogels in the broader sense, e.g. in the sense of "gel with air as the dispersion agent" are produced by the drying of a suitable gel. The term "aerogel" in this sense embraces aerogels in the narrower sense, xerogels and cryogels. In this respect, a dried gel is termed an aerogel in the narrower sense when the liquid of the gel is eliminated at above critical temperature and starting from pressures above critical pressure. On the other hand, if the liquid is eliminated from the gel under sub-critical conditions, for example with the formation of a liquid/vapour interphase, then the resulting gel is frequently referred to also as a xerogel.

When the term aerogels is used in the present invention, these are aerogels in the broader sense, i.e. in the sense of "gel with air as the dispersion medium"

The term does not include aerogels known from earlier literature and which are obtained for example by precipitation of silicic acid (e.g. DE 3025437, DD 296 898) or which occur as pyrogenic silicic acid, e.g. Aerosil<sup>TM</sup>. In these cases, during manufacture, no three-dimensional gel lattice develops which is homogeneous over relatively great distances

Where aerogels are concerned, it is possible basically to differentiate between inorganic and organic aerogels.

Inorganic aerogels have already been known since 1931 (S. S. Kistler, Nature 1931, 127, 741). Since then, aerogels have been forthcoming from various starting materials. In this respect, for example  $\text{SiO}_2$ -,  $\text{Al}_2\text{O}_3$ -,  $\text{TiO}_2$ -,  $\text{ZrO}_2$ -,  $\text{SnO}_2$ -,  $\text{Li}_2\text{O}$ -,  $\text{CeO}_2$ -,  $\text{V}_2\text{O}_5$ -aerogels and mixtures of these were produced (H. D. Gesser, P. C. Goswami, Chem. Rev. 1989, 89, 765 et seq.).

For some years, organic aerogels have also been known which are derived from the most widely diverse starting materials, e.g. melamine formaldehyde (R. W. Pekala, J. Mater. Sci. 1989, 24, 3221).

Inorganic aerogels can thereby be produced in different ways.

On the one hand,  $\text{SiO}_2$  aerogels can for example be produced by acid hydrolysis and condensation of tetra-ethyl orthosilicate in ethanol. During this process, a gel is produced which can be dried by super-critical drying while its structure is maintained. Production methods based on this drying technique are known for example from EP-A-0 396 076, WO 92/03378 or WO 95/06617

The high pressure technique involved in the super-critical drying of aerogels is however an expensive process and involves a high security risk. In addition, however, super-critical drying of aerogels is a very cost-intensive production method

An alternative to super-critical drying is afforded by a method for the sub-critical drying of  $\text{SiO}_2$  gels.

The costs involved in sub-critical drying are substantially less by reason of the simpler technology, the lower energy costs and the lesser security risk.

The  $\text{SiO}_2$  gels can for example be obtained by acid hydrolysis of tetra-alkoxy silanes in a suitable organic solvent by means of water. Once the solvent has been exchanged for a suitable organic solvent, the gel obtained is in a further step reacted with a silylating agent. The  $\text{SiO}_2$  gel resulting from this can then, from an organic solvent, be dried in air. Thus, aerogels with densities of less than 0.4 g/cu.cm and porosities above 60% can be achieved. The production method based on this drying technique is described in detail in WO 94/25149

Furthermore, the above-described gels can, prior to drying and in the alcohol-aqueous solution, be mixed with tetra-alkoxy silanes and aged, in order to increase the gel lattice strength, as disclosed in WO 92/20623.

The tetra-alkoxy silanes used as starting materials in the above-described processes do, however, likewise represent an extremely high cost factor.

A not inconsiderable cost reduction can be achieved by using water-glass as a starting material for the production of  $\text{SiO}_2$  gels. To this end, it is possible for example to produce a silicic acid from an aqueous water-glass solution with the help of an ion exchange resin, the silicic acid then being polycondensed by the addition of a base to produce an  $\text{SiO}_2$  gel. After exchange of the aqueous medium for a suitable organic solvent, it is then possible in a further step to react the resulting gel with a silylating agent containing chlorine. The  $\text{SiO}_2$  gel which is surface modified for example with methyl silyl groups can then and likewise from an organic solvent, be dried in air. The production method based on this technique is known from DE-A-43 42 548

Alternative methods with regard to the production of an  $\text{SiO}_2$  aerogel on a basis of water-glass with subsequent sub-critical drying are described in German Patent Application 195 41 715.1 and 195 41 992.8

Furthermore, DE-A-195 02 453 describes a use of chlorine-free silylating agents during the production of sub-critically dried aerogels.

Furthermore, an organofunctionalisation by means of organofunctionalised silylating agents in the production of sub-critically dried aerogels is described in DE-A-195 34 198.

However, on grounds of procedural technology and manufacturing costs, the production of aerogel particles on a major industrial scale is limited to particle sizes less than 5 mm and preferably less than 2 mm.

According to the particular manner of producing the aerogels, so in principle a plurality of washing and solvent exchange stages are required. Since these are diffusion-dependent, the time required is increased by the square of the radius of the gel particles. Consequently, apart from the drying method, the costs of aerogel production also increase quite considerably from the particle size upwards. On grounds of cost, the result is an endeavour to produce the smallest possible aerogel particles.

On the other hand, the handling of very small particles is very complicated and thus the costs entailed are likewise unfavourable and not every industrial application of aerogels is independent of the particle size.

Therefore, from the point of view of handling and for many applications, larger aerogel particles are needed or at least advantageous.

Therefore, the object of the present invention is to provide a method by which small aerogel particles of less than 2 mm can be formed into larger aerogel particles.

This problem is resolved by a method in which the aerogel particles are delivered to a moulding apparatus in which they are compressed. In this way, it is particularly simple to form small aerogel particles into larger aerogel particles.

Advantageously, in order to achieve specific desired properties of the aerogel particles, additives, fillers and/or binders are added to the aerogel particles and may be in the form of particles and/or fibres or may possibly also be liquid or in paste form.

In accordance with a preferred embodiment, the starting material is degassed prior to moulding. This is advantageous particularly when the starting material is in loose bulk form, since then a certain proportion of the gas present between the aerogel particles has to be removed prior to compacting.

Expediently, the starting material is subjected to a negative pressure for degassing, whereby, according to another embodiment, degassing can also take place during the moulding.

The aerogel particles or the starting material can be moulded into the form of granulate, after which they are then advantageously separated according to their size. For example, this can happen by screening off the desired ranges of granular size in order to arrive at the desired target fraction. Granulate which is below the desired granular range is advantageously recycled to the moulding apparatus while granulate which is above the desired range is ideally comminuted so that it comes into the desired granular range. However, after comminution it can also be fed back directly to the moulding apparatus to be compacted once again.

Prior to further processing, the granulate is then, in accordance with another embodiment, dried in order to remove any residual humidity which is undesirable or harmful to further processing.

However, the starting material can also be moulded to produce a slab, in which case this is then likewise and in accordance with a further embodiment, dried prior to any further procedural step.

Moulding of the aerogel particles or aerogel particles with possible additives can take place using conventional and suitable moulding apparatus.

In accordance with a further embodiment, the starting material was moulded in a female die by means of a male die. The mouldings produced in this way can then possibly be cut by a knife, a scraper or the like to reduce them to the desired size.

Another embodiment envisages the starting material being moulded between a female die and a roller which slides or rolls over it. In this case, the female die may be perforated in which case, the mouldings produced are advantageously, on the output side, cut to the desired size by means of a knife, a scraper or the like.

According to a preferred embodiment, the starting material is moulded between two rollers of which at least one but preferably both rotate. Expediently, the starting material is then pressed into the roller gap by a tamping screw.

In accordance with a further development of this embodiment, at least one of the rollers is constructed as a perforated hollow roller. The mouldings produced in this case by moulding are advantageously cut to the desired size on the output side by some suitable device, for example a knife or a scraper.

Another further development envisages at least one of the rollers being profiled. By a suitable selection of the profiles, the starting material can then be moulded directly either into the form of granules or into some cohesive product strip, a so-called scab.

**Parent claims**

1. **A method of compacting aerogel particles, characterised in that the aerogel particles are fed into and moulded in a moulding apparatus.**
2. **A method according to claim 1, characterised in that additives, fillers and/or binders are added to the aerogel particles.**
3. **A method according to claim 2, characterised in that the components are in particulate or fibre form.**
4. **A method according to claim 2, characterised in that the components are liquid or pasty.**
5. **A method according to at least one of the preceding claims, characterised in that the starting material is degassed prior to and/or during moulding.**
6. **A method according to claim 5, characterised in that the starting material is subjected to a negative pressure.**
7. **A method according to at least one of the preceding claims, characterised in that the starting material is moulded into granules**
8. **A method according to claim 7, characterised in that the granulates are sorted according to their size**
9. **A method according to claim 8, characterised in that the granules which are below the desired granular range are returned to the moulding apparatus.**

10. A method according to claim 8, characterised in that the granules which are above the desired granular range are comminuted.
11. A method according to at least one of claims 7 to 10, characterised in that the granules are dried prior to further processing
12. A method according to at least one of claims 1 to 6, characterised in that the starting material is moulded into a scab.
13. A method according to claim 12, characterised in that the scab is dried prior to further processing.
14. A method according to at least one of the preceding claims, characterised in that a male die moulds the starting material in a female die.
15. A method according to at least one of claims 1 to 13, characterised in that the starting material is moulded between a roller and a female die.
16. A method according to claim 5, characterised in that the female die is perforated and in that the mouldings are cut off on the output side
17. A method according to at least one of claims 1 to 13, characterised in that the starting material is moulded between two rollers.
18. A method according to claim 17, characterised in that at least one of the rollers is a perforated hollow roller, the mouldings being cut off on the output side.
19. A method according to at least one of claims 1 to 13, characterised in that the starting material is moulded between two rollers, at least one of which is profiled.