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(54) Keksinnön nimitys - Uppfinningens benämning - Title of the invention

Menetelmä ja laite veden käsittelemiseksi

Förfarande och anordning för behandling för behandling av vatten

(57) Tiivistelmä - Sammandrag - Abstract

Valuvan kalvon monivaihehaihduttimessa tuotetaan puhdistettua vettä erityistarkoituksiin. Jokainen vaihe tuottaa syöttövedestä höyryfaasin ja vesifaasin. Höyryfaasi käytetään lämmityshöyrynä seuraavassa haihdutusvaiheessa, jolloin se lauhtuu tuotevedeksi, ja vesifaasi syötetään syöttövetenä seuraavaan haihdutusvaiheeseen. Prosessista poistetaan rejektivirta vedestä erotettujen epäpuhtauksien saattamiseksi ulos prosessista. Keksinnön mukaisesti rejektivirta poistetaan jokaisesta vaiheesta. Edullisesti kukin rejektivirta on kyseisessä vaiheessa synnytetyn höyryn lauhdutettu fraktio. Fig.1

I en flerstegsindunstare av fallande-film-typ produceras renat vatten för specialändamål. I varje steg produceras av matarvattnet en ångfas och en vattenfas. Ångfasen används som uppvärmningsånga i nästa indunstningssteg varvid den kondenserar till produktvatten, och vattenfasen utgör matarvatten för nästa indunstningssteg. En rejektström avlägsnas från processen för att avlägsna från vattnet avskiljda orenheter. Enligt uppfinningen avlägsnas en rejektström från varje steg. Företrädesvis är varje rejekt-ström en kondenserad fraktion av den ånga som uppstått i respektive steg.

Field of the invention

The invention relates to the production of highly purified water for special purposes. Particularly, the invention relates to the production of purified water using falling-film evaporators with subsequent condensation.

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Background of the invention

For the purpose of this text, "purified water" means generally water of greater purity than ordinary potable water available from e.g. a municipal water distribution system. Highly purified water is required e.g. for various medical purposes, such as production of pharmaceuticals, and in the production of "water for injection", the quality of which is defined in official pharmacopoeias. Plants for producing such purified water may be designed as so-called multi-effect stills, employing a series of falling film evaporators. A falling film evaporator comprises a vertical bundle of evaporation tubes enclosed into a heating jacket. Water fed into the evaporating tubes at their upper end flows down the inner surface of the tubes, thereby evaporating and forming steam, which emerges at the lower ends of the tube bundle together with any un-vaporized water. In many devices for producing highly purified steam or water, the flow of steam makes a 180° turn and flows upwards in a rising space provided therefore, while the remaining water collects at the bottom of the device.

The upward-flowing steam may, depending on the type of device, undergo various kinds of demisting and/or purification operations, whereby the separated droplets and impurities finally join the water phase at the bottom of the effect while the steam enters the heating jacket of the subsequent effect. The water phase becomes the feed water of the subsequent effect and the steam condenses, giving off its heat to cause more steam to evaporate from the feed water, and the cascade continues until the last effect is reached. The combined condensates from the heating jackets, together with the steam from the last effect, are cooled and condensed, respectively, in a final heat exchanger to form the purified product water.

In prior art multi-effect falling-film plants for producing purified water, the feed to each effect generates a steam phase and a residual leaving water phase. The residual water phase then, in its entirety, generates the feed for the next effect and so on, until the last effect is reached. The residual water in the last effect represents the reject fraction containing the impurities.

In this context, a reject stream is a stream of water, which is permanently removed from the process. Generally, the reject stream is liquid water, but may be a steam-liquid mixture. A continuous process for producing pure water by evaporation must include the removal of a sufficient amount of reject water to carry away the separated impurities. The ratio of reject water to product water is an important aspect of the efficiency of the process. It follows from the material balance, that if the reject stream is insufficient, the impurities either accumulate in the device or leave with the product, which both alternatives are highly undesirable.

10 In Finnish patent application 20021538, a unit for producing pure steam is disclosed. This device includes a particular purification section for the steam, having a rising spiral path following the evaporation section, which is a falling-film unit as described above. In the outer wall of the spiral path, apertures are provided, and outside said apertures a cool surface. This arrangement creates a pressure gradient across the apertures due to condensation of steam on the cool surface, causing impurity-containing droplets to migrate through the apertures and collect on the cool surface. The least pure component of the rising stream in the spiral path thus travels to the periphery and leaves through the apertures, condenses on the cool surface and forms a water phase rich in impurities, which flows down the cool surface. This water phase rich in impurities may be isolated and not returned to the process, but separated as a reject stream.

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Summary of the invention

The present invention relates to the production of purified water in a multi-effect still or evaporation plant utilizing the type of devices described above for purified steam production. A falling-film evaporation plant for the production of purified water may comprise a plurality of evaporation stages or effects. Water is fed to each effect, and water and steam leaves each effect. According to the present invention, a reject stream is withdrawn from each effect. Thus, each effect in a multi-effect falling-film evaporation plant for producing purified water comprises means for the withdrawal of a reject stream. In one embodiment of the present invention, the reject stream may be withdrawn as liquid water from the fraction of water that is not vaporized in an evaporation section, i.e. the residual water. A fraction of the residual water phase may thus be split off before it is conducted to the subsequent effect.

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According to a preferable embodiment, each effect comprises a rising channel for the steam phase generated in the effect, and means for separating an impurity-containing fraction from the rising steam. The “steam phase” in this context is a water vapor phase in the vicinity of its saturation point, and thus generally contains minute water droplets. The impurity-containing fraction, which may thus comprise steam and water droplets, is permanently separated from the process and not passed on to the next effect. Preferably, the fraction is essentially allowed to condense to be withdrawn in the form of liquid water.

The present invention provides several advantages, particularly in the embodiment described above. The total amount of reject water is decreased, as a smaller proportion is required to carry impurities. A greater proportion of water can be evaporated in each effect, compared to the prior art. The impurities separated from the feed in each effect are not carried over to the next effect, and do not come into contact with heat exchange surfaces further downstream. Scaling is thus avoided. The recycling of the residual water from the last effect is also made feasible, as this fraction does not contain such an increased level of impurities as in the prior art.

Brief description of the drawing

The invention is more thoroughly disclosed in the following, with reference to the appended figure, which schematically shows the main components of a plant according to the invention.

Disclosure of the invention

Figure 1 shows an embodiment of a four-effect production plant for pure water according to the invention. Feed water, preferably purified by means of filtering and ion exchange or other appropriate methods, enters at inlet 1. After passing heat recovery exchanger 4, the feed stream enters, through transfer line 5, the first falling-film evaporation unit 6. Transfer line 5 may be provided with additional heat exchange devices to improve the overall heat recovery, as the person skilled in the art may contemplate.

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Plant steam or another primary heat transfer medium entering at inlet 8 heats the shell side of the falling film evaporation section 7. As the feed water flows down as a film on the inner walls of the evaporating tubes (not shown), the water partly evaporates into steam, which emerges from the lower end of the tubes together with the remaining water. Within

separation section 9, the steam makes a 180° turn and enters a rising channel. After passing the rising channel, the steam is led through transfer line 10 to the shell side of the falling film evaporation unit of the subsequent effect 11. The water phase collects on the bottom of the effect, leaves the effect at outlet 2 and is conducted to the feed inlet 12 of the subsequent effect. A reject stream is withdrawn via conduit 13.

In each evaporation effect, the same sequence occurs. Feed water is partially evaporated to steam in the falling film section. The steam generated in each effect is carried over to heat the feed water in the subsequent effect, and the residual water that has not been converted into steam becomes the feed water of the next effect. The residual water from the last effect may be discarded or recycled.

In an embodiment of separation section 9, disclosed in greater detail in Finnish patent application 20021538 referred to above, the rising channel for steam generated in each effect has the form of a spiral pathway, causing the impurity-containing droplets entrained in the steam to travel to the periphery of the spiral, where they migrate through apertures in the outer wall of the rising channel. Outside the apertures, the droplets, along with steam, condense on a surface having a temperature sufficiently low for this to occur. The water film forming on this surface, containing the separated impurities, flows down by gravity and the water is collected in a separate, isolated shell space, from where a reject stream is withdrawn.

Thus, in an embodiment of this type having means for separating a fraction of the generated steam, the steam in each effect is depleted of a contaminant-enriched fraction in the corresponding separation section; these fractions are isolated in separate compartments and form reject streams, exiting via conduits 13 in Fig.1. Preferably, the reject lines are provided with steam traps 16. As impurities are removed from all effects from the first onwards, they are not accumulated in the final residual water as in the prior art.

The stream leaving the shell side of the falling film section of the first effect is commonly factory steam condensate, and is removed at outlet 3. The primary heat source can also be another heat transfer medium, whereby appropriate re-circulation is provided, or electrical heating elements.

Beginning from the second effect, the condensate from the shell side of the falling film section, which condensate stems from the evaporated part of the initial feed water, is collected and fed to the shell side of the falling film section of the next effect. Thus, the evaporated fractions are finally combined in the shell of the final effect, from which they
5 are taken out and cooled in a heat exchanger 4 together with the steam phase of the final effect. Preferably, this heat exchanger delivers heat to the initial feed water stream.

The temperature and pressure conditions in the individual effects are adjusted as required. In the first effect, the temperature corresponds to that of the primary heating medium, resulting in a corresponding steam pressure. Throttle devices may be provided between ef-
10 fects, and the pressure decreases sequentially until preferably being near atmospheric in the final effect.

From the last effect, a residual water phase is withdrawn at outlet 15 and may be discarded
15 as an additional reject stream, recycled, or split between these.

Claims

1. A method for producing purified water using a multi-effect falling-film evaporation process, whereby in each effect steam and water are produced from feed water, and residual water from each evaporation effect is supplied as feed water to the subsequent effect,
5 **characterized** in that from each evaporation effect, a fraction is removed as a reject stream.
2. The method according to claim 1, **characterized** in that the reject stream is a fraction
10 separated from the steam phase produced in the respective effect.
3. The method according to claim 2, **characterized** in that the fraction of the steam phase is essentially condensed to liquid water.
- 15 4. A device for the production of purified water comprising a plurality of effects, each effect having a falling film evaporation section and a separation section, the separation section having a channel for conducting steam from the unit and a channel for conducting liquid water to a subsequent unit, **characterized** in each unit having a conduit for conducting a reject stream out of the unit.
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5. The device according to claim 4, **characterized** in that the separation section comprises in the channel for conducting steam, means for separating a fraction of the steam.
6. The device according to claim 5, **characterized** in that the means for separating part of
25 the steam comprises a spiral channel.
7. The device according to claim 5 or 6, **characterized** in that the separation section comprises an isolated compartment for collecting the separated steam, and that the conduit for conducting a reject stream out of the effect is connected to said compartment.

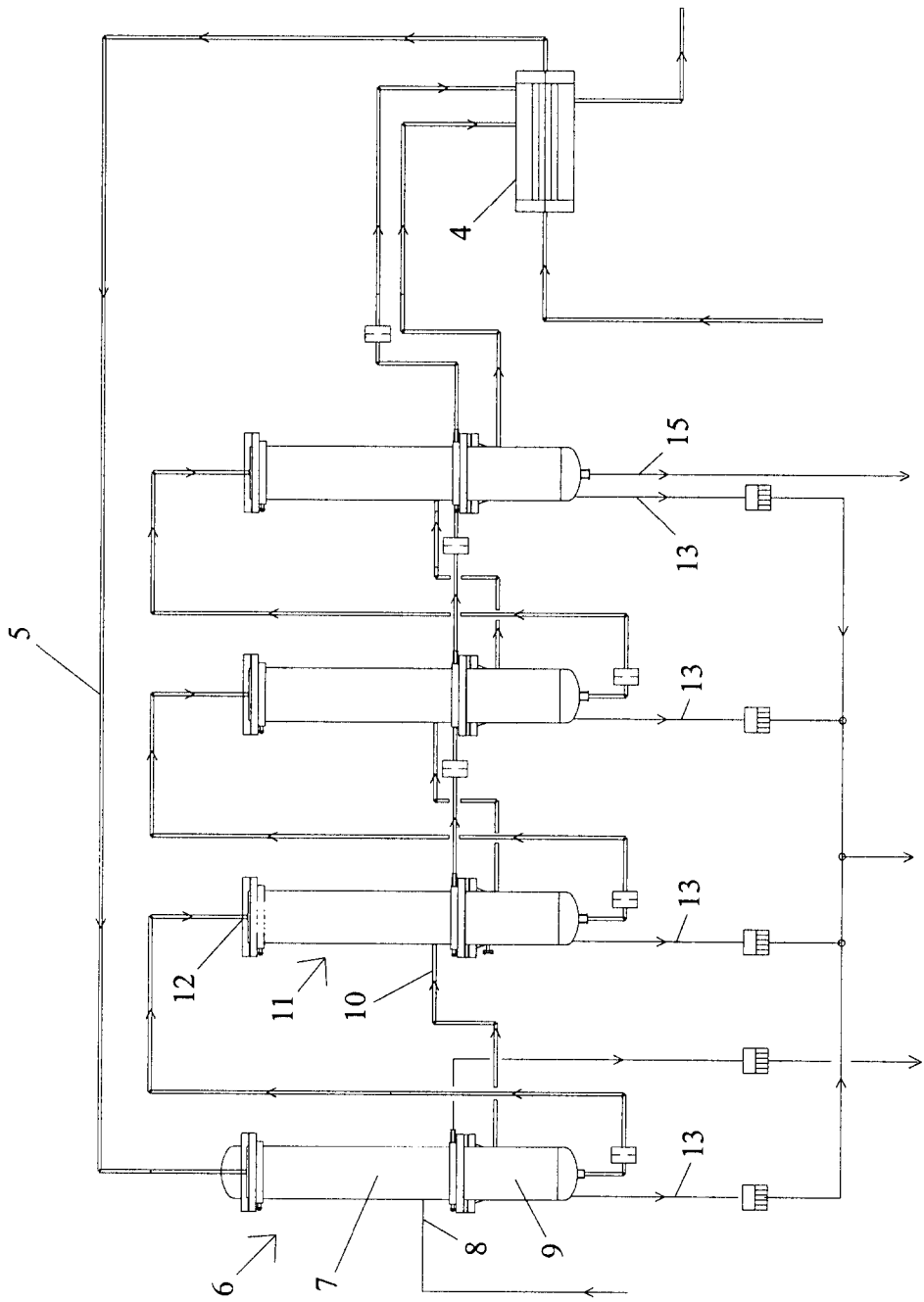


Fig. 1

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TUTKITUT PATENTTILUOKAT (luokitusjärjestelmät ja luokkatiedot)
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EPODOC, WPI,PAJ**VIITEJULKAISUT**

Kategoria*)	Julkaisun tunnistetiedot ja tiedot sen olennaisista kohdista	Koskee vaatimuksia
X	JP A 10328501 (KIMURA CHEM PLANTS CO LTD), 15.12.1998, ENGL. TIIVISTELMÄ (KAPPALE [0022]) JA KUVIO 1	1-7
A	EP A 0 042 605 (A/S NIRO ATOMIZER) 30.12.1981, KOKO JULKAISU	1-7
A	FI 20002104 A (STERIS EUROPE INC, SUOMEN SIVULIIKE), 26.03.2002, KOKO JULKAISU	6

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