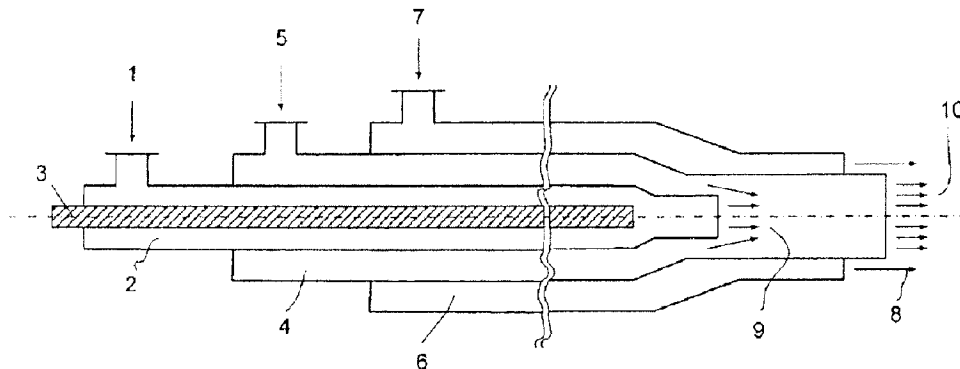




(86) **Date de dépôt PCT/PCT Filing Date:** 2013/08/08
(87) **Date publication PCT/PCT Publication Date:** 2014/02/20
(45) **Date de délivrance/Issue Date:** 2020/04/14
(85) **Entrée phase nationale/National Entry:** 2015/02/10
(86) **N° demande PCT/PCT Application No.:** EP 2013/002369
(87) **N° publication PCT/PCT Publication No.:** 2014/026748
(30) **Priorité/Priority:** 2012/08/14 (DE10 2012 016 086.0)

(51) **Cl.Int./Int.Cl. C10J 3/50** (2006.01),
C21C 5/46 (2006.01)
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(54) **Titre : DISPOSITIF ET PROCEDE POUR INJECTER DE L'OXYGENE DANS UN DISPOSITIF DE GAZEIFICATION EN LIT FLUIDISE PRESSURISE**
(54) **Title: DEVICE AND METHOD FOR INTRODUCING OXYGEN INTO A PRESSURIZED FLUIDIZED-BED GASIFICATION PROCESS**



(57) **Abbrégé/Abstract:**

The invention relates to an oxygen lance that has at least three mutually coaxial pipes, each of which delimits at least one annular gap. The outermost pipe is designed to conduct superheated steam and has a steam supply point, the central pipe is designed as an annular gap, and the innermost pipe is designed to conduct oxygen at a temperature of no higher than 180 °C and has an oxygen supply point. A temperature sensor is arranged within the innermost pipe, said temperature sensor extending to just in front of the opening of the innermost pipe. The innermost pipe tapers in the form of a nozzle before opening; the innermost pipe opens into the central pipe; and the opening of the central pipe protrudes farther relative to the opening of the outermost pipe.

ABSTRACT

The invention relates to an oxygen lance that has at least three mutually coaxial pipes, each of which delimits at least one annular gap. The outermost pipe is designed to conduct superheated steam and has a steam supply point, the central pipe is designed as an annular gap, and the innermost pipe is designed to conduct oxygen at a temperature of no higher than 180 °C and has an oxygen supply point. A temperature sensor is arranged within the innermost pipe, said temperature sensor extending to just in front of the opening of the innermost pipe. The innermost pipe tapers in the form of a nozzle before opening; the innermost pipe opens into the central pipe; and the opening of the central pipe protrudes farther relative to the opening of the outermost pipe.

Device and method for introducing oxygen into a pressurized
fluidized-bed gasification process

5 **[0001]** The invention relates to a method and a device for
introducing oxygen into a pressurized fluidized bed
gasification process which is typically employed in a
gasification reactor according to the high-pressure Winkler
method (HTW method).

10 **[0002]** The HTW method has been known for a long time and is
tried-and-tested technology whereby both particulate and
liquid or pasty carbon-containing fuels are converted into
synthesis gas. The fuels used are also heavy fuels with a very
high ash content and also biomass-based fuels and carbon-
15 containing waste materials. These are introduced into a
fluidized bed, which is operated as a bubbling fluidized bed,
and are gasified by means of oxygen, steam and CO₂. In contrast
to other gasification methods, the HTW method works at
moderate temperatures at which the ash which occurs does not
20 melt. This has operational benefits particularly in the case
of corrosive ashes.

25 **[0003]** The addition of oxygen has to be metered very
accurately, since excessive metering would lead to increased
burn-out and therefore to an increase in the CO₂ content in the
synthesis gas, which must be avoided. Also, excessive metering
would lead, in the immediate surroundings of the oxygen inlet
points, to a meltdown of the ash particles, with the result
that caking with the fluidized bed material may occur and
would lead in turn to material adhering to the oxygen lances.
Accurate, quick and fine regulation of the oxygen feed is
30 therefore necessary because the fuels are partly fed
discontinuously under pressure. This leads to especially
stringent requirements to be fulfilled by the oxygen lances

which are typically used for introducing the required oxygen into the fluidized bed reactor.

5 **[0004]** Corresponding oxygen lances are described, for example, in DE 34 39 404 C2 and DE 44 07 651 C1 which correspond to the hitherto existing prior art. In these, the problem of possible caking is solved in that, at the point of exit of the oxygen, steam addition is arranged in such a way as to form a steam film which envelops the emerging oxygen jet. The turbulences generated at the same time in the
10 emerging gas jet have a very high steam content which prevents overheating of the entrained fluidized bed particles and thus considerably reduces the tendency to caking.

15 **[0005]** However, this technology presents problems at pressures above 8 to 10 bar. Before being added to the oxygen lance, the oxygen is usually preheated. For safety reasons, however, it would be preferable not to carry out heating above 180°C, since in this case equipment parts, in particular seals, which are customary in the industry are attacked. Above 200°C, there are statutory licensing restrictions in the use
20 of material. If the preheated oxygen is introduced into the oxygen lance at 180°C and if superheated steam is applied in an enveloping pipe, condensates are formed at a pressure of above 8 to 10 bar on the steam side of the oxygen-carrying pipe. These condensates change the flow conditions of the gas
25 outlet to such a great extent that an enveloping steam film is no longer formed around the oxygen lance. This leads to the failure of the oxygen lances.

30 **[0006]** The object of the invention is, therefore, to make available a device and a method for introducing oxygen into a pressurized fluidized bed gasification process which is also suitable for operating pressures of above 10 bar and, along with high safety and availability, is efficient.

[0007] The object is achieved by means of an oxygen lance having at least three pipes arranged coaxially one in the other and at least in each case delimiting an annular gap,

- 5 • the outermost pipe being designed for the conduction of superheated steam and having a steam feed point,
- the middle pipe being designed as an annular gap,
- the innermost pipe being designed for the conduction of oxygen with a temperature of at most 180°C and having an oxygen feed point,
- 10 • there being arranged inside the innermost pipe a temperature probe which reaches to just short of the mouth of the innermost pipe,
- the innermost pipe tapering in a nozzle-like manner upstream of its mouth,
- 15 • the innermost pipe issuing into the middle pipe, and
- the mouth of the middle pipe projecting further in relation to the mouth of the outermost pipe.

[0008] In one refinement, the middle pipe may be designed as a blind pipe closed on both sides, and in this case the term
20 "mouth" used in the preceding paragraph is intended in this limiting instance to refer merely to the pipe end in the vicinity of the mouth of the outermost pipe. In another refinement, the middle pipe is open on the mouth side of the oxygen lance. In a further refinement, the middle pipe is
25 designed for the conduction of dry gas and has a gas introduction point. In this case, in a further refinement, there may be provision whereby the middle pipe tapers in a

nozzle-like manner upstream of the mouth of the innermost pipe issuing into the middle pipe.

5 **[0009]** Dry gas is understood here, as is customary in combustion technology in contrast to steam generation technology, to mean an industrial gas without steam fractions. By contrast, moist gas is understood below to mean an industrial gas which also contains steam fractions, although this is not intended to mean that a multiphase mixture has been formed. Superheated steam is therefore to be considered
10 as moist gas, even though it is dry in the sense that wet steam has not occurred.

15 **[0010]** The object is also achieved, as described above, by means of a method for introducing oxygen into a fluidized bed gasification reactor, operated according to the HTW method, by means of an oxygen lance,

- moist gas being fed into the outermost pipe at a pressure above the pressure in the fluidized bed gasification reactor,
- 20 • oxygen being conducted into the innermost pipe at a temperature of at most 180°C and with a pressure above the pressure in the fluidized bed gasification reactor,
- 25 • moist gas emerging from the mouth of the outermost pipe as a cladding flow around the mouth of the middle pipe and the emerging free jet, the flow velocity of the emerging moist gas being set higher than that of the emerging gas from the innermost pipe.

[0011] In refinements of the method, there may be provision whereby dry gas is introduced into the middle pipe at a pressure above the pressure in the fluidized bed gasification

reactor, and thereby oxygen and dry gas are intermixed upstream of the mouth of the middle pipe.

[0012] In further refinements of the method, there is provision whereby the moist gas is superheated steam or a
5 mixture of carbon dioxide and of superheated steam.

[0013] In further refinements of the method, there is provision whereby the dry gas is carbon dioxide, nitrogen or a mixture of carbon dioxide and of air or a mixture of carbon dioxide and of nitrogen. Moreover, insofar as is desirable in
10 the gasification process, operation without dry gas is possible, the positive effects upon the temperature of the moist gas being maintained. The minimum feed temperature of the dry gas into the middle pipe arises from the dew point of the moist gas used in the outermost pipe, this corresponding
15 in the case of pure steam to the saturated steam temperature.

[0014] It became apparent that this technical solution is especially beneficial economically, since the supply lines for carbon dioxide can be used due to the need to ensure inertization of the oxygen lances during rapid shutdowns, and
20 the insertion of a further pipe into the oxygen lances entails only little outlay. The choice of a dry gas with high specific heat capacity and the additional shielding of the hot moist gas against the cooler oxygen prevent an appreciable lowering of temperature in the steam-carrying outermost pipe and
25 therefore the condensation of steam in the outermost pipe.

[0015] The invention is explained in more detail below by means of 2 sketches. Fig. 1 in this case shows diagrammatically a section through an oxygen lance, the mouth of which issues into the fluidized bed of an HTW gasification reactor, not shown, and Fig. 2 shows the circuitry of the
30 supply lines for oxygen, carbon dioxide and steam.

[0016] Oxygen 1 is conducted into the innermost pipe 2 in which the temperature measuring device 3 is arranged. The temperature amounts to 180 degrees Celsius and the pressure at the inlet to approximately 28 bar. The exact pressure is
5 determined by means of the quantity control which feeds the reactor with exactly the quantity of oxygen just required instantaneously for gasification. Carbon dioxide 5 at 230 degrees Celsius is added to the middle pipe 4. Superheated steam 7 with a pressure of approximately 29 bar and a
10 temperature of 410 degrees Celsius is introduced into the outermost pipe 6. This steam heats the carbon dioxide to a temperature of approximately 270 degrees Celsius, the oxygen likewise being heated slightly. Since the dew point of the steam is not in this case undershot, steam is not condensed
15 out and no droplets are formed at the mouth 8 of the outermost pipe, so that a homogenous steam film can be formed around the tip of the oxygen lance.

[0017] The oxygen of the innermost pipe and the carbon dioxide of the middle pipe are brought together at the mixing
20 point 9 into a common gas stream, the feed point already lying inside the fluidized bed in the HTW gasification reactor. The mixture is conducted as a free jet 10 into the fluidized bed, the steam film preventing the oxygen from forming vortices around the nozzle tip and thus preventing possible local
25 overheating with the result of ash softening and caking at the nozzle tip. The fluidized bed reactor can thereby be operated at a pressure of 28 bar.

[0018] Fig. 2 shows a circuit diagram with supply lines for oxygen 11, carbon dioxide 12 and superheated steam 13 and also
30 with the most important shut-off and regulating valves. In an emergency, carbon dioxide can be introduced into the oxygen line via the scavenging valve 14 and into the steam line via the regulating valve 15. As a rule, the two valves are closed.

As a function of the oxygen quantity required, the regulating valve 16 serves for the oxygen supply, regulating valve 17 serves for regulating the quantity of carbon dioxide and the regulating valve 18 serves for the introduction of steam.
5 Oxygen 11 can also be distributed to other nozzle levels via the oxygen distributor 19.

[0019] The following computing and design examples illustrate the invention:

- 10 • In example 1, the outermost pipe is subjected to steam and the middle pipe to nitrogen.
- In example 2, the outermost pipe is subjected to steam and the middle pipe to carbon dioxide.
- 15 • In example 3, the outermost pipe is subjected to a mixture which is composed in equal proportions by mass of carbon dioxide and of steam and the middle pipe is subjected to carbon dioxide.
- In example 4, the outermost pipe is subjected to steam and the middle pipe is left without any throughflow.

20 **[0020]** In all the examples, the innermost pipe is subjected to oxygen, the inside diameter amounting to approximately 25 mm and a thermocouple with a thickness of 11 mm being arranged inside. All the indications of dimension are approximate indications obtained from design calculations.

	Ex. 1	Ex. 2	Ex. 3	Ex. 4
gap of the outermost pipe [mm]	9	15	15	15
gap of the middle pipe [mm]	10	4	4	4
mass throughflow through the outermost pipe [kg/s]	0.039	0.039	0.039	0.039
mass throughflow through the middle pipe [kg/s]	0.0039	0.0039	0.0039	-
mass throughflow through the innermost pipe [kg/s]	0.225	0.225	0.225	0.225
inlet temperature into the outermost pipe [°C]	410	410	410	410
inlet temperature into the middle pipe [°C]	230	230	230	-
inlet temperature into the innermost pipe [°C]	180	180	180	180
outlet temperature from the outermost pipe [°C]	400	390	390	390
outlet temperature from the middle pipe [°C]	270	270	270	-
outlet temperature from the innermost pipe [°C]	182	182	182	182

In all instances, the saturated steam temperature of the moist gas of the outermost pipe is at no point undershot in the middle pipe, and therefore condensation cannot occur.

5 [0021] The invention is not restricted to the examples illustrated, and, furthermore, it is also possible, in the case of different load situations or operating situations, to adapt the respective throughflows to the requirements in a flexible way.

List of reference symbols:

- 1 oxygen
- 2 innermost pipe
- 3 temperature measuring device
- 5 4 middle pipe
- 5 carbon dioxide
- 6 outermost pipe
- 7 steam
- 8 mouth of the outermost pipe
- 10 9 mixing point
- 10 free jet
- 11 oxygen
- 12 carbon dioxide
- 13 steam
- 15 14 scavenging valve
- 15 regulating valve
- 16 regulating valve
- 17 regulating valve
- 18 regulating valve
- 20 19 oxygen distributor

CLAIMS:

1. An oxygen lance, having at least three pipes arranged coaxially to one another and at least in each case delimiting an annular gap,

the outermost pipe being designed for the conduction of superheated steam and having a steam feed point,

the middle pipe being designed as an annular gap,

the innermost pipe being designed for the conduction of oxygen with a temperature of at most 180°C and having an oxygen feed point,

there being arranged inside the innermost pipe a temperature probe which reaches to just short of the mouth of the innermost pipe,

the innermost pipe tapering in a nozzle-like manner upstream of its mouth,

the innermost pipe issuing into the middle pipe, and

the mouth of the middle pipe projecting further in relation to the mouth of the outermost pipe.

2. The oxygen lance as claimed in claim 1, wherein the middle pipe is designed to be open on the mouth side of the oxygen lance.

3. The oxygen lance as claimed in claim 1, wherein the middle pipe is designed for the conduction of dry gas and has a gas introduction point.

4. The oxygen lance as claimed in claim 3, wherein the middle pipe tapers in a nozzle-like manner upstream of the mouth of the innermost pipe issuing into the middle pipe.

5. A method for introducing oxygen into a fluidized bed gasification reactor, operated according to the HTW method, by means of an oxygen lance according to any one of claims 1 to 4,

moist gas being fed into the outermost pipe at a pressure above the pressure in the fluidized bed gasification reactor,

oxygen being conducted into the innermost pipe at a temperature of at most 180°C and with a pressure above the pressure in the fluidized bed gasification reactor,

moist gas emerging from the mouth of the outermost pipe as a cladding flow around the mouth of the middle pipe and the emerging free jet, the flow velocity of the emerging moist gas being set higher than that of the emerging gas from the innermost pipe.

6. The method as claimed in claim 5, wherein

the middle pipe is subjected to dry gas,

oxygen and dry gas are intermixed upstream of the mouth of the middle pipe,

moist gas emerges from the mouth of the outermost pipe as a cladding flow around the mouth of the middle pipe and the emerging free jet, the flow velocity of the emerging moist gas being set higher than that of the emerging mixture of dry gas and of oxygen.

7. The method as claimed in either one of claims 5 or 6, wherein the moist gas is superheated steam.
8. The method as claimed in either one of claims 5 or 6, wherein the moist gas is a mixture of carbon dioxide and of superheated steam.
9. The method as claimed in claim 6, wherein the dry gas is carbon dioxide.
10. The method as claimed in claim 6, wherein the dry gas is nitrogen.
11. The method as claimed in claim 6, wherein the dry gas is a mixture of carbon dioxide and of air.
12. The method as claimed in claim 6, wherein the dry gas is a mixture of carbon dioxide and of nitrogen.
13. The method as claimed in claim 6, wherein the dry gas is not moved during operation.

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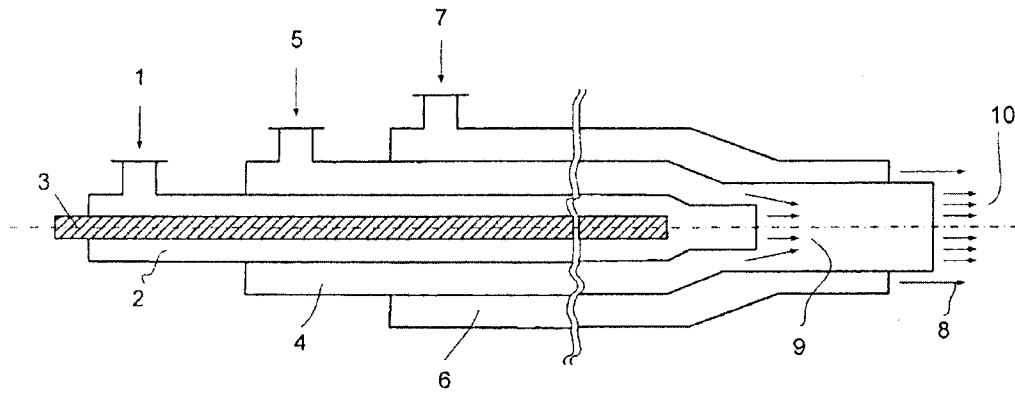
Fig. 1

Fig. 2