



(51) International Patent Classification:
C08J 7/00 (2006.01)

(21) International Application Number:
PCT/EP2013/076706

(22) International Filing Date:
16 December 2013 (16.12.2013)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
12198387.8 20 December 2012 (20.12.2012) EP
61/748,141 2 January 2013 (02.01.2013) US

(71) Applicant: AGFA-GEVAERT [BE/BE]; IP Department
3622, Septestraat 27, B-2640 Mortsel (BE).

(72) Inventors: DEPLA, Anouschka; c/o Agfa-Gevaert, IP Department 3622, Septestraat 27, B-2640 Mortsel (BE). MUES, Willem; c/o Agfa-Gevaert, IP Department 3622, Septestraat 27, B-2640 Mortsel (BE). BRIES, Peter; c/o Agfa-Gevaert, IP Department 3622, Septestraat 27, B-2640 Mortsel (BE). QUINTENS, Dirk; c/o Agfa-Gevaert, IP Department 3622, Septestraat 27, B-2640 Mortsel (BE).

(74) Agent: VIAENE, Kris; Agfa-Gevaert, IP Department 3622, Septestraat 27, B-2640 Mortsel (BE).

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM, AO, AT, AU, AZ, BA, BB, BG, BH, BN, BR, BW, BY, BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DK, DM, DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IR, IS, JP, KE, KG, KN, KP, KR, KZ, LA, LC, LK, LR, LS, LT, LU, LY, MA, MD, ME, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PA, PE, PG, PH, PL, PT, QA, RO, RS, RU, RW, SA, SC, SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LR, LS, MW, MZ, NA, RW, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, RU, TJ, TM), European (AL, AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU, LV, MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK, SM, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, KM, ML, MR, NE, SN, TD, TG).

Published:

— with international search report (Art. 21(3))

(54) Title: METHOD OF PREPARING A BARRIER FILM FOR BLISTER PACKS

(57) Abstract: A method for preparing a barrier film comprising the steps of: (i) providing a substrate; (ii) applying in a single coating step an polymer latex on the substrate to form a single layer of the polymer on the substrate (iii) drying the single layer of the polymer; characterized in that the single layer has a dry coating weight (DCW) of at least 20 g/m² of polymer and is dried at a dry temperature (Td) of at least the film formation temperature (Tf) the polymer latex at a relative humidity (RH) according to the following formula: RH = 15 + 1.25 * DCW.



Method of preparing a barrier film for blister packs

[DESCRIPTION]

5

FIELD OF THE INVENTION

The present invention relates to a method of making a barrier film and to its use in blister packs.

10

BACKGROUND OF THE INVENTION

A blister pack is a term for several types of pre-formed plastic packaging used for consumer goods, food and pharmaceuticals. The primary component of a blister pack is a cavity, often referred to as "pocket" or "blister", holding the product. The blister is typically obtained by thermoforming a flat, preferably transparent, plastic film. The blisters holding the product are then sealed by a lidding foil.

When used for pharmaceuticals, blister packs are designed to protect the product from the environment (moisture, O₂, light) to guarantee physical and chemical stability of the product. The type of thermoformable plastic film and lidding foil used to prepare the blister pack determines its "barrier" properties against water vapor and oxygen. The lidding foil is typically made of aluminium.

This invention relates to the preparation of a barrier film used as thermoformable plastic film in the preparation of a blister pack for pharmaceuticals. Such barrier films typically comprise a thermoformable polymeric substrate on which one or more barrier layers may be provided to increase the barrier properties.

Typical barrier films used are for example a polyvinylchloride (PVC) substrate having a thickness of 250 µm, a PVC substrate on which a coating of polyvinylidenechloride copolymers (PVDC) is provided,

and a PVC substrate onto which a polychlorotrifluoroethylene (PCTFE) film is laminated.

A barrier film comprising a PVDC coating has the advantage that it exhibits good barrier properties not only with respect to oxygen but also with respect to water vapor.

The coating weight of a PVDC coating on a substrate is usually from 40 up to 180 g/m² PVDC, depending on the barrier properties strived for. Such PVDC coatings are typically coated from aqueous latex dispersions and dried at high temperatures (70-130°C) and low relative humidities (RH < 5%). Under such drying conditions, the maximum dry coating weight in one single pass is limited to ± 17 g/m² PVDC. To achieve a final dry layer thickness of for example 180 g/m² PVDC, 10 or more repetitive coating/drying steps are necessary. This implies several passes through an industrial coating alley.

The coating weight is limited to 17 g/m² PVDC because higher coating weights results in the formation of so-called "mud cracks" upon drying of the coating. Mud cracks in the top surface of the coating are due to skinning of the surface layer(s) of the coating while the sub layers still contain large amounts of water which needs to be evaporated. These mobile sublayers create cracks in the tensed skinned toplayer. Such mud cracks may decrease the barrier properties of the PVDC coating.

EP-A 1148084 discloses a process for preparing a barrier film wherein a homogeneous layer of at least 20 g/m² PVDC is coated on a thermoplastic base. The process comprises a thermal pretreatment at a temperature ranging from 60 to 100°C of the coated layer followed by drying the coated layer at a temperature ranging from 70 to 120 °C and cooling at a temperature ranging from 30 to 50°C.

It would be advantageous to have a method of preparing a barrier film comprising a PVDC coating on a substrate, wherein the dry coating weight after a single coating and drying step is at least 20 g/m² and wherein the PVDC coating is free from mud cracks. Such a method results in a substantial cost price reduction as less coating and drying steps have to be performed to produce the film.

SUMMARY OF THE INVENTION

It is an object of the invention to provide a method of preparing a barrier film characterized by a substantial cost price reduction while the barrier properties of the obtained barrier film are maintained.

A method for preparing a barrier film comprising the steps of:

(i) providing a substrate;

(ii) applying in a single coating step a polymer latex having on the substrate to form a single layer of the polymer on the substrate;

(iii) drying the single layer;

characterized in that the single layer has a dry coating weight (DCW) of at least 20 g/m² of the polymer and is dried at a dry temperature (Td) of at least the film formation temperature (Tf) of the polymer latex at a relative humidity (RH) according to the following formula:

$$RH = 15 + 1.25 * DCW.$$

Further objects of the invention will become apparent from the description hereinafter and the dependent claims.

5

DETAILED DESCRIPTION OF THE INVENTION

The method for preparing a barrier film according to the present invention comprises the steps of:

- 10 (i) providing a substrate;
(ii) applying in a single coating step a polymer latex having on the substrate to form a single layer of the polymer on the substrate;
(iii) drying the single layer;
characterized in that the single layer has a dry coating weight
15 (DCW) of at least 20 g/m² of the polymer and is dried at a dry temperature (Td) of at least the film formation temperature (Tf) of the polymer latex at a relative humidity (RH) according to the following formula:

20
$$RH = 15 + 1.25 * DCW.$$

Substrate

- 25 The substrate of the barrier film is preferably a transparent thermoformable polymeric film. The polymeric film may be selected from the group consisting of polyvinyl chloride (PVC), copolymers made of vinyl chloride units and of one or more other monomers (VC copolymers), polyesters, polyolefins, polyacrylonitrile,
30 copolymers made of acrylonitrile units and one or more other monomers, and mixtures made of PVC and VC copolymers.
Substrates based on polylactic acid may also be of interest in view of their biodegradability. Polyethylenefuranoate (PEF) substrates may also be of interest as they are 100 % biobased and recyclable.

35

The most widely used substrate is PVC. The main advantages of PVC are the low cost and the ease of thermoforming. The main

disadvantages are the poor barrier properties and a negative environmental connotation due to its chlorine content.

The polyesters preferably comprise polyethylene terephthalate (PET),
5 in particular amorphous PET, and copolymers made of ethylene terephthalate units and one or more other monomers. A particular preferred copolymer is PETG, which is composed of ethylene terephthalate units and cyclohexanedimethanol units.

10 The polyolefins are preferably polypropylene (PP), polyethylene (PE), cyclo-olefin copolymers (COCs), and cyclo-olefin polymers (COP).

The thickness of the substrate may be between 10 and 1000 μm , more
15 preferably between 50 and 500 μm .

The polymeric support may be surface treated, typically to enhance the adhesion between the support and layers provided thereon.

20 Examples of such a surface treatment include a corona discharge treatment, a flame treatment, a UV treatment, a low pressure plasma treatment, and an atmospheric plasma treatment. A preferred treatment is a corona discharge treatment.

25 Polymer latex

Any latex, capable of forming a film having sufficient barrier properties may be used in the method of the present invention.

30 A latex selected from a polyurethane latex, a poly(meth)acrylate latex and fluoro-polymer latex is preferred.

A particularly preferred latex is a a polyvinylidenechloride
35 copolymer (PVDC) latex.

PVDC

PVDC is a vinylidene polymer selected from the group consisting of
5 polyvinylidene chloride, copolymers made of vinylidene chloride
units and other monomers (VCD copolymers). A preferred PVDC is a
vinylidene chloride - methyl acrylate copolymer.

The PVDC is coated from aqueous latex dispersions. Such latex
10 dispersions are commercially available, for example from Solvay
Plastics (Diofan® A736, Diofan® 193D and Diofan® Super B), from
Asahi Kasei Chemicals (L801, L803, L803C, L817B), and from Dow
Chemical (Serfene® 195).

15 The dry coating weight of the single PVDC coating is at least 20
g/m², more preferably at least 30 g/m², most preferably at least 35
g/m². It has been observed that it is difficult to obtain mud crack
free coatings of PVDC when the dry coating weight is more than
50 g/m².

20 When the dry coating weight of PVDC has to be, for example more than
100 g/m², to achieve high barrier properties, it may be difficult to
achieve such high dry coating weight in a single coating step.
To achieve such high dry coating weights multiple coating steps may
25 be used.

Therefore, another embodiment of the invention provides a method for
preparing a barrier film comprising the steps of:

(i) providing a substrate;

30 (ii) applying in multiple coating steps a polymer latex on the
substrate to form multiple layers of the polymer on the substrate;

(iii) drying the applied polymer layers after each coating step;
characterized in that in at least one coating step a single layer of
polymer is applied having a dry coating weight (DCW) of at least 20
35 g/m² of the polymer and wherein said single layer is dried at a dry
temperature (Td) of at least the film formation temperature (Tf) of

the polymer latex at a relative humidity (RH) according to the following formula:

$$RH = 15 + 1.25 * DCW.$$

5

Preferably the polymer latex is a polyvinylidenechloride copolymer (PVDC) latex in all coating steps.

10

In a preferred method of this embodiment in all coating steps a single layer of polymer is applied having a dry coating weight (DCW) of at least 20 g/m² of the polymer and wherein said single layer is dried at a dry temperature (Td) of at least the film formation temperature (Tf) of the polymer latex at a relative humidity (RH) according to the following formula:

15

$$RH = 15 + 1.25 * DCW.$$

20

For example, a dry coating weight of 120 g/m² PVDC can be obtained with the method of the present invention by subsequently coating three layers of PDVC having a dry coating weight of 40 g/m² on top of each other or by coating four layers of PVDC having a dry coating weight of 30 g/m². With the methods known from the prior art, at least six subsequent coatings would be necessary to obtain such a high dry coating weight.

25

After each coating and drying step the obtained intermediate barrier film may be stored on roll. After unwinding the roll of film, a subsequent coating step may be carried out.

30

The drying step after each coating step may be characterized by the same or different drying conditions.

The PVDC coating solution preferably consists of the PVDC latex, i.e. no other ingredients are added to the coating solution.

However, to optimize the properties of the barrier film, additives, such as for example surfactants, may be added to the PVDC coating.

When more than one PVDC layer is coated, it may be advantageous to add such additives, for example antiblocking agents, only to the outermost PVDC layer.

Other layers

The barrier film may, besides PVDC layers, also comprise additional layers to further optimize its properties.

For example, an "anchor coating" or primer may be applied on the substrate to improve the adhesion between the PVDC coating and the substrate. Such a primer is preferably coated from an aqueous coating solution. Such primers typically comprise one or more binders, such as for example polyurethanes, polyacrylics, and polyesters. A preferred primer is a polyurethane based primer.

A barrier film comprising a substrate, a PVDC layer and a PCTFE layer, as disclosed in US2011/0210037, may also be prepared by the method according to the present invention. The PCTFE layer is laminated to the PVC/PVDC film. The PCTFE layer has typically a thickness of 15 μm to 152 μm , is typically applied to a PVC/PE laminate. Using both PVDC and PCTFE may further improve the barrier properties of the barrier film.

A widely used multilayer barrier film comprises in this order PVC/PE/PVDC. The PVDC layer in such a multilayer can be applied using the method of the present invention.

Coating

The PVDC latex is coated on the substrate using well known coating techniques such as air knife coating, dip coating, spray coating, reverse gravure roll coating, cascade coating, and curtain coating.

A preferred coating technique is cascade coating. The coating speed is determined by the coating weight and the drying conditions. For example, the coating speed may be up to 180 - 200 m/min for a coating weight of 20 g/m² and up to 100 - 120 m/min for a coating weight of 40 g/m².

Drying

In the drying process, heat is supplied to evaporate the water from the coated latex layer. Also, when the drying temperature is above the film forming temperature of the latex, the coated latex particles will coalesce to form a continuous film.

The main drying parameters are drying temperature (T_d), wet bulb temperature ($T_{\text{wet bulb}}$), relative humidity (RH) and air speed of drying (α). The wet bulb temperature is the temperature of the drying layer. Due to the evaporation of the water, this temperature is lower than the drying temperature. When the layer becomes dry, the $T_{\text{wet bulb}}$ and the drying temperature (T_d) are equal.

T_d , $T_{\text{wet bulb}}$ and RH are correlated with each other according to the well known Mollier diagram.

The drying conditions of the coated layers are set to meet the conditions of claim 1.

Drying of a coating is typically carried out in so called drying tunnels. The length of the drying tunnel will determine the speed at which the coating may pass through the tunnel: the speed may be increased when the length of the drying tunnel increases.

The heat for drying is usually supplied by convection from air that has been heated indirectly by a steam heat exchanger or by electric heaters or directly from hot flue gases from the combustion of natural gas.

The heat may also be supplied by conduction from heated rolls in drum dryers or from heated plates in a gap dryer.

The heat may also be supplied by infra-red or microwave radiation.

Preferably, the heat is supplied by convention. Infra-red heaters
5 may be used in addition to convection heaters to increase the drying capacity.

In the convention units, the drying air impinges on the coating. The temperature and the RH of the air are controlled.

10 Several drying zones (units) may be used, having the same or different drying conditions.

To monitor the drying process, the temperature of the coated layer
15 (wet bulb temperature, $T_{w \text{ bulb}}$) may be monitored, for example with an IR pyrometer. As long as the coated layer is not dry, the wet bulb temperature will be lower than the drying temperature (T_d). When the coating becomes dry, the layer temperature (T_n) evolves towards the drying temperature (T_d).

20 The drying temperature (T_d) is determined by measuring the temperature of the drying air with conventional thermometers. The Relative Humidity of the drying air is determined by conventional RH measurement instruments.

25

EXAMPLES

Materials

5 All materials used in the examples were readily available from standard sources such as Aldrich Chemical Co. (Belgium) and Acros (Belgium) unless otherwise specified.

- Diofan A736, a PVDC latex commercially available from Solvay,
10 characterized by a viscosity of 20 mPoise and a film formation temperature of 17°C.
- Diofan Super B, a PVDC latex commercially available from Solvay.

15

Example 1

For three different coating weights, i.e. 20, 30 and 40 g/m² PVDC,
20 the drying conditions were varied in order to find conditions wherein mud free coatings could be realized.

Prior to coating, the Diofan A736 latex is cooled (5-8°C), magnetically stirred and then filtered, using a 50 µm bag filter,
25 and a 1 µm porvair filter. Cooling of the latex is mandatory to prevent coagulation and film formation on the equipment. As the latex is shear sensitive, intense stirring is not recommended.

All coatings were performed using a cascade coating installation,
30 based on meniscus formation. In order to form a good meniscus, the wet layer thickness had to be ≥ 38 µm for low viscosity latices (15-25 mPoise). This implied dilution of the latex for the lowest coating weight application (20 g/m² dry weight). To see whether or not dilution of the PVDC latex had an influence on the obtained

results, the effect of dilution has been looked at for the coating weight of 30 g/m² (see Table 1).

Table 1

Coated Weight (g/m ²)	Wet Layer Thickness (μ m)	PVDC Latex
20	38	50% diluted
30	38	not diluted
30	58	50% diluted
40	51	not diluted

5

For each coating weight, different drying conditions were used. The main drying parameters are drying temperature (T_d), wet bulb temperature ($T_{\text{wet bulb}}$), relative humidity (RH) and air speed of drying (α). The first three are correlated with each other according to the Mollier diagram.

10

As the latex film formation temperature (T_f) of Diofan A736 is $\pm 17^\circ\text{C}$, the drying temperature has to be at least this temperature to ensure good film formation. The pilot drying installation used in these experiments imposed some limitations on the operating window that could be investigated: the maximum drying temperature was 55°C , the maximum relative humidity was 85 %. The air speed of drying was set at 6-8 m/s.

15

The quality of the coatings was evaluated by the number of mud cracks visually identified on multiple A4 samples of each coating. The following scores were used:

20

0: mud crack free

25

1: less than 50 mud cracks per A4

2: 50 - 80 mud cracks per A4

3: more than 80 mud cracks per A4

As the coatings are used as barrier coatings, only mud crack free coatings are considered to fulfil the barrier properties.

The results for all samples are given in Table 2.

5 Table 2

	[PVDC] (g/m ²)	Wet layer thickness (μm)	PVDC latex	Td (°C)	RH (%)	Tn (°C)	Mud Cracking
COMP-01	20	38	50 % diluted	50	< 5	20.3	3
COMP-02	20	38	50 % diluted	50	15.0	26.6	3
COMP-03	20	38	50 % diluted	50	23.3	30.0	3
COMP-04	20	38	50 % diluted	40	< 5	17.0	3
COMP-05	20	38	50 % diluted	40	15.0	20.7	3
COMP-06	20	38	50 % diluted	40	23.9	23.5	3
COMP-07	20	38	50 % diluted	40	30.0	25.3	1
COMP-08	20	38	50 % diluted	35	< 5	14.5	2
COMP-09	20	38	50 % diluted	35	20.0	19.1	3
COMP-10	20	38	50 % diluted	35	30.0	21.7	3
INV-01	20	38	50 % diluted	35	40.0	24.1	0
COMP-11	20	38	50 % diluted	25	35.0	15.5	2
INV-02	20	38	50 % diluted	25	50.0	18.0	0
INV-03	20	38	50 % diluted	25	65.0	21.0	0
INV-04	20	38	50 % diluted	20	80.0	18.8	0
COMP-12	30	38	not diluted	40	< 5	17.0	3
COMP-13	30	38	not diluted	40	15.0	20.7	3
COMP-14	30	38	not diluted	40	23.9	23.5	3
COMP-15	30	38	not diluted	40	30.0	25.3	2
COMP-16	30	38	not diluted	35	< 5	14.5	3
COMP-17	30	38	not diluted	35	20.0	19.1	3

COMP-18	30	38	not diluted	35	30.0	21.7	3
COMP-19	30	38	not diluted	35	40.0	24.1	2
COMP-20	30	38	not diluted	25	35.0	15.5	2
COMP-21	30	38	not diluted	25	50.0	18.0	1
INV-05	30	38	not diluted	25	65.0	21.0	0
INV-06	30	38	not diluted	20	80.0	18.8	0
COMP-22	30	58	50 % diluted	40	< 5	17.0	3
COMP-23	30	58	50 % diluted	40	15.0	20.7	3
COMP-24	30	58	50 % diluted	40	23.9	23.5	3
COMP-25	30	58	50 % diluted	40	30.0	25.3	2
COMP-26	30	58	50 % diluted	35	< 5	14.5	3
COMP-27	30	58	50 % diluted	35	20.0	19.1	3
COMP-28	30	58	50 % diluted	35	30.0	21.7	3
COMP-29	30	58	50 % diluted	35	40.0	24.1	2
COMP-30	30	58	50 % diluted	25	35.0	15.5	2
INV-07	30	58	50 % diluted	25	50.0	18.0	1
INV-08	30	58	50 % diluted	25	65.0	21.0	0
INV-09	30	58	50 % diluted	20	80.0	18.8	0
COMP-31	40	51	not diluted	35	< 5	14.5	3
COMP-32	40	51	not diluted	35	20.0	19.1	3
COMP-33	40	51	not diluted	35	30.0	21.7	3
COMP-34	40	51	not diluted	35	40.0	24.1	3
COMP-35	40	51	not diluted	25	35.0	15.5	3
COMP-36	40	51	not diluted	25	50.0	18.0	3
INV-10	40	51	not diluted	25	65.0	21.0	0
INV-11	40	51	not diluted	20	80.0	18.8	0

The results of Table 2 clearly indicate that the RH has to be increased for the higher coating weight to obtain mud cracks free coatings. Based on these results it could be concluded that the relation between RH and the dry coating weight (DCW) can be represented by the following formula:

$$RH = 15 + 1.25 * DCW$$

As already stated above, the appearance of mud cracks is related to skin formation of the surface layer(s) while the sublayer(s) are still mobile. An increase of the humidity during drying up to 65 % RH is able to slow down skin formation and prevent subsequent mud cracks formation up to coating weights of 40 g/m² PVDC.

From Table 1 it is also clear that the effect of dilution of the latex (to obtain a higher wet coating thickness) on the results is minimal.

Example 2

In this example, multiple coating steps have been carried out to obtain a barrier film on PVC having high dry coating weights of PVDC.

The drying conditions in all coating steps were T_d = 25°C, RH = 65 %, and T_n = 21°C. The dry coating weight of PVDC in each coating step is given in Table 3.

Table 3

	Coating step 1	Coating step 2	Coating step 3	Coating step 4	Total coating
	[PVDC] g/m ²	[PVDC] g/m ²	[PVDC] g/m ²	[PVDC] g/m ²	Total [PVDC] g/m ²
INV-12	20	20	-	-	40
INV-13	30	30	-	-	60

INV-14	30	30	20	-	80
INV-15	25	25	20	20	90

The barrier properties, more specifically the vapor transmission rate (WVTR) of the mud crack free inventive PVDC coatings have been determined. Standard WVTR measurements were carried out in the "Xios Hogeschool Limburg" and in "Permlabs" in Wiesbaden in accordance with ASTM F 1249. The results are shown in Table 3. In Table 4, the WVTR values of commercially available barrier films (PVC/PVDC films from Bilcare) are shown (taken from the datasheets of these films).

Table 4

	Substrate	PVDC latex	PVDC (g/m ²)	WVTR
INV-12	PVC	Diofan A736	40	0.70
INV-13	PVC	Diofan A736	60	0.48
INV-14	PVC	Diofan A736	80	0.34
INV-15	PVC	Super B	90	0.13

Table 5

Substrate	PVDC (g/m ²)	WVTR
PVC	40	0.75
PVC	60	0.55
PVC	90	0.35

It is clear from Table 4 and 5 that the values obtained with the inventive barrier films are at least comparable with the state of the art PVDC coatings on PVC.

[CLAIMS]

1. A method for preparing a barrier film comprising the steps of:
 (i) providing a substrate;
 (ii) applying in a single coating step a polymer latex on the
5 substrate to form a single layer of the polymer on the substrate;
 (iii) drying the single layer;
characterized in that the single layer has a dry coating weight
(DCW) of at least 20 g/m² of the polymer and is dried at a dry
temperature (Td) of at least the film formation temperature (Tf)
10 of the polymer latex at a relative humidity (RH) according to the
following formula:

$$RH = 15 + 1.25 * DCW.$$

- 15 2. The method according to claim 1 wherein the polymer latex is a
polyvinylidenechloride copolymer (PVDC) latex.
3. The method according to claim 2 wherein the single layer contains
at least 40 g/m² of PVDC.
4. The method according to any of the preceding claims wherein the
20 RH is at least 65 %.
5. The method according to any of the preceding claims wherein the
substrate is made from polyvinylchloride (PVC), polyethylene-
terephthalate (PET), polypropylene (PP), polyethylene (PE), or
cyclic olefin copolymer (COC).
- 25 6. The method according to any of the preceding claims wherein a
primer is provided on the substrate before applying the polymer
latex.
7. A method for preparing a barrier film comprising the steps of:
 (i) providing a substrate;
30 (ii) applying in multiple coating steps a polymer latex on the
substrate to form multiple layers of the polymer on the

substrate;

(iii) drying the applied polymer layers after each coating step; characterized in that in at least one coating step a single layer of polymer is applied having a dry coating weight (DCW) of at least 20 g/m² of the polymer and wherein said single layer is dried at a dry temperature (Td) of at least the film formation temperature (Tf) of the polymer latex at a relative humidity (RH) according to the following formula:

$$RH = 15 + 1.25 * DCW.$$

8. The method according to claim 7 wherein the polymer latex is a polyvinylidenechloride copolymer (PVDC) latex in all coating steps.

9. The method according to any of the claims 7 or 8 wherein the multiple coating and drying steps results in a coating on the substrate having a dry coating weight of at least 60 g/m² of polymer.

10. The method according to any of the preceding claims wherein the barrier film obtained has a Water Vapor Transmission Rate (WVTR) measured in accordance with ASTM F 1249 of less than 0.80 g/m².d.b.

■

INTERNATIONAL SEARCH REPORT

International application No
PCT/EP2013/076706

A. CLASSIFICATION OF SUBJECT MATTER
INV. C08J7/00
ADD.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
C08J

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 2004/033379 A1 (GRUNLAN JAMIE C [US] ET AL) 19 February 2004 (2004-02-19) paragraph [0018] - paragraph [0025] page 53 - page 57 page 64 - page 72 claims 1, 3, 5-8, 10; figures 1-12; example 1	1-10
X	JP 63 307055 A (NORDSON KK) 14 December 1988 (1988-12-14) the whole document	1-10
X	JP 58 158247 A (UNITIKA LTD) 20 September 1983 (1983-09-20) the whole document	1-10
X	JP 55 059961 A (ASAHI DOW LTD) 6 May 1980 (1980-05-06) the whole document	1-10



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier application or patent but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

8 January 2014

Date of mailing of the international search report

15/01/2014

Name and mailing address of the ISA/

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040,
Fax: (+31-70) 340-3016

Authorized officer

Glomm, Bernhard

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/EP2013/076706

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
US 2004033379	A1	19-02-2004	NONE	
JP 63307055	A	14-12-1988	-----	
JP 58158247	A	20-09-1983	-----	
JP 55059961	A	06-05-1980	-----	