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PROCESS

(57) **Abrégé/Abstract:**

The present invention relates to a supported catalyst composition and a method for making the supported catalyst composition and its use in a process for polymerizing olefin(s). In particular, the invention is directed to a method for making a supported catalyst composition by combining a heated bulky ligand metallocene-type catalyst system with a carrier or an optionally heated carrier.



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(54) Title: A METHOD FOR PREPARING A SUPPORTED CATALYST SYSTEM AND ITS USE IN A POLYMERIZATION PROCESS

(57) Abstract: The present invention relates to a supported catalyst composition and a method for making the supported catalyst composition and its use in a process for polymerizing olefin(s). In particular, the invention is directed to a method for making a supported catalyst composition by combining a heated bulky ligand metallocene-type catalyst system with a carrier or an optionally heated carrier.

**A METHOD FOR PREPARING A SUPPORTED CATALYST
SYSTEM AND ITS USE IN A POLYMERIZATION PROCESS**

FIELD OF THE INVENTION

5 The present invention relates to a method for preparing a supported catalyst system and for its use in a process for polymerizing olefin(s). In particular, the invention is directed to a method for preparing a supported bulky ligand metallocene-type catalyst system.

BACKGROUND OF THE INVENTION

10 Advances in polymerization and catalysis have resulted in the capability to produce many new polymers having improved physical and chemical properties useful in a wide variety of superior products and applications. With the development of new catalysts the choice of polymerization-type (solution, slurry, high pressure or gas phase) for producing a particular polymer has been greatly
15 expanded. Also, advances in polymerization technology have provided more efficient, highly productive and economically enhanced processes. Especially illustrative of these advances is the development of technology utilizing bulky ligand metallocene-type catalyst systems. In particular, in a slurry or gas phase process where typically a supported catalyst system is used, there are a variety of
20 different methods described in the art for supporting bulky ligand metallocene-type catalyst systems.

 Illustrative methods for producing supported bulky ligand metallocene-type catalyst systems include: U.S. Patent No. 5,332,706 and 5,473,028 have resorted to a particular technique for forming a catalyst by incipient impregnation;
25 U.S. Patent Nos. 5,427,991 and 5,643,847 describe the chemical bonding of non-coordinating anionic activators to supports; U.S. Patent No. 5,492,975 discusses polymer bound metallocene-type catalyst systems; PCT publication WO 97/06186 published February 20, 1997 teaches removing inorganic and organic impurities after formation of the metallocene-type catalyst itself; PCT publication WO
30 97/15602 published May 1, 1997 discusses readily supportable metal complexes; U.S. Patent No. 4,937,217 generally describes a mixture of trimethylaluminum and triethylaluminum added to an undehydrated silica then adding a metallocene catalyst; EP-308177-B1 generally describes adding a wet monomer to a reactor containing a metallocene, trialkylaluminum and undehydrated silica; U.S. Patent
35 Nos. 4,912,075, 4,935,397 and 4,937,301 generally relate to adding trimethylaluminum to an undehydrated silica and then adding a metallocene to

form a dry supported catalyst; U.S. Patent No. 4,914,253 describes adding trimethylaluminum to undehydrated silica, adding a metallocene and then drying the catalyst with an amount of hydrogen to produce a polyethylene wax; U.S. Patent Nos. 5,008,228, 5,086,025 and 5,147,949 generally describe forming a dry supported catalyst by the addition of trimethylaluminum to a water impregnated silica to form alumoxane in situ and then adding the metallocene; U.S. Patent Nos. 4,808,561, 4,897,455 and 4,701,432 describe techniques to form a supported catalyst where the inert carrier, typically silica, is calcined and contacted with a metallocene(s) and a activator/cocatalyst component; U.S. Patent No. 5,238,892 describes forming a dry supported catalyst by mixing a metallocene with an alkyl aluminum then adding undehydrated silica; and U.S. Patent No. 5,240,894 generally pertains to forming a supported metallocene/alumoxane catalyst system by forming a metallocene/alumoxane reaction solution, adding a porous carrier, and evaporating the resulting slurry to remove residual solvent from the carrier.

WO 96/35729 discusses making a supported catalyst system by reacting a metallocene with an alumoxane at a temperature of up to 50°C and then combining the reaction product with a support.

EP-A-878 486 describes the preparation of a supported metallocene catalyst using magnesium halide as an activator.

U.S. Patent No. 5,554,704 discusses making a supported catalyst system by adding the carrier in dry form or as a slurry to a reaction product solution of metallocene and alumoxane.

U.S. Patent No. 5,914,289 discusses making a supported catalyst system by combining a specific bulky ligand metallocene-type catalyst system with alumoxane to form a reaction product in the presence of a carrier and then heating the reaction product/carrier combination to a high temperature.

While all these methods have been described in the art, a need for an improved method for preparing a supported bulky-ligand metallocene-type catalysts has been discovered.

SUMMARY OF THE INVENTION

This invention provides a method of making a new and improved supported bulky ligand metallocene-type catalyst system and for its use in a polymerizing process.

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In one embodiment, the invention is directed to a method for making a supported catalyst system comprising the steps of (a) heating a composition comprising a bulky ligand metallocene-type catalyst compound and an activator to a temperature of from 75°C to 100°C; and (b) combining the heated composition of step (a) with a carrier.

In another embodiment, the invention is directed to a method for making a supported catalyst system comprising the steps of: (a) forming a reaction product comprising a bulky ligand metallocene-type catalyst compound and an activator selected from the group consisting of alumoxanes and non-coordinating activators; (b) heating the reaction product; (c) optionally heating a carrier; (d) combining the heated reaction product with a carrier or optionally the heated carrier.

In another embodiment, the invention is directed to a method for making a supported catalyst system comprising the steps of: (a) heating an activated bulky ligand metallocene-type catalyst to a temperature of between 75°C and 100°C; (b) heating a carrier; and (c) combining the heated carrier and the heated activated bulky ligand metallocene-type catalyst.

In another embodiment, the invention is directed to a method for preparing a supported catalyst system comprising the steps of: (a) heating a composition comprising a bulky ligand metallocene-type catalyst compound and an activator selected from the group consisting of alumoxanes and non-coordinating activators at a first temperature of from 60°C to 100°C; (b) heating a carrier at a second temperature; and (c) combining (a) and (b) at a third temperature.

In another embodiment, the invention is directed to a process for polymerizing olefin(s) in the presence of a supported catalyst system, the supported catalyst system made by (a) heating a solution comprising at least one bulky ligand metallocene-type catalyst compound and an activator at a temperature in the range of from 75°C to 100°C; (b) introducing a carrier to the solution to form a mixture; (c) drying the mixture to form the supported catalyst system; and (d) polymerizing olefin(s) in the presence of the supported catalyst system.

In another embodiment, the invention is direct to a process for polymerizing olefin(s) in the presence of a supported catalyst system, the supported catalyst system made by (a) heating a reaction product comprising a bulky ligand metallocene-type catalyst compound and an activator selected from the group consisting of alumoxanes and

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non-coordinating activators to a temperature of 60°C to 100°C; (b) combining the reaction product with a carrier, optionally the carrier is heated; and polymerizing olefins in the presence of the supported catalyst system.

In another embodiment, the invention is directed to a method for preparing a supported catalyst system comprising: (a) heating a composition comprising a metallocene catalyst compound to a temperature of from 75°C to 125°C; and (b) combining the heated composition with a carrier.

In another embodiment, the invention is directed to a method for making a supported catalyst system comprising: (a) forming a reaction product comprising a metallocene catalyst compound and an activator; (b) heating the reaction product to a temperature of from 60°C to 125°C; (c) introducing a carrier; (d) combining the heated reaction product with the carrier.

In another embodiment, the invention is directed to a method for making a supported catalyst system comprising: (a) heating an activated metallocene catalyst product to a temperature of from 60°C to 125°C; (b) heating a carrier; and (c) combining the heated carrier and the heated activated metallocene catalyst.

In another embodiment, the invention is directed to a method for preparing a supported catalyst system comprising: (a) heating a composition comprising a metallocene catalyst compound to a first temperature, wherein the first temperature is in the range of from 60°C to 110°C; (b) heating a carrier at a second temperature; and (c) combining said metallocene catalyst, and said carrier, at a third temperature.

In another embodiment, the invention is directed to a method for preparing a supported catalyst composition comprising: (a) combining a metallocene catalyst compound and an activator at a temperature in the range of from 60°C to 125°C; and (b) introducing a carrier.

In yet another embodiment, the invention is directed to a method for making a supported catalyst system comprising the steps of (a) heating an activated bulky ligand metallocene-type catalyst; (b) heating a carrier; and (c) combining the heated carrier and the heated activated bulky ligand metallocene-type catalyst.

In a further embodiment, the invention relates to a method for preparing a supported catalyst system comprising the steps of (a) heating a composition comprising a bulky ligand metallocene-type catalyst compound at a first temperature; (b) heating a carrier at a second temperature; and (c) combining (a) and (b) at a third temperature. The first, second and third temperatures are the same or different.

In another embodiment, the invention is directed to a process for polymerizing olefin(s), particularly in a gas phase or slurry phase process, utilizing any one of the supported catalyst systems prepared above.

In one embodiment, there is provided a use in the polymerization of olefin(s) of a supported catalyst as disclosed herein.

DETAILED DESCRIPTION OF THE INVENTION

Introduction

The invention is directed toward a method for making a supported catalyst system. It has been surprisingly discovered that by combining a heated bulky ligand metallocene-type catalyst system with a carrier, optionally heating the carrier, results in an increase in catalyst productivity. This method is particularly enhanced when the bulky ligand metallocene-type catalyst compound has reduced solubility as compared for example with a very basic unsubstituted bulky ligand metallocene-type catalyst compound, i.e. bis(cyclopentadienyl)zirconium dichloride. The method of the invention is especially well suited for use with bridged bulky ligand metallocene-type catalyst compounds. Thus, as a result the improved method of the invention provides a way to increase catalyst productivities to a commercially acceptable level with improved reactor process operability.

Bulky Ligand Metallocene-Type Catalyst Compounds

Generally, bulky ligand metallocene-type catalyst compounds include half and full sandwich compounds having one or more bulky ligands bonded to at least one metal atom. Typical bulky ligand metallocene-type compounds are generally described as containing one or more bulky ligand(s) and one or more leaving group(s) bonded to at least one metal atom. In one preferred embodiment, at least

Bulky Ligand Metallocene-Type Catalyst Compounds

Generally, bulky ligand metallocene-type catalyst compounds include half and full sandwich compounds having one or more bulky ligands bonded to at least one metal atom. Typical bulky ligand metallocene-type compounds are generally
5 described as containing one or more bulky ligand(s) and one or more leaving group(s) bonded to at least one metal atom. In one preferred embodiment, at least one bulky ligands is η -bonded to the metal atom, most preferably η^5 -bonded to the metal atom.

The bulky ligands are generally represented by one or more open, acyclic,
10 or fused ring(s) or ring system(s) or a combination thereof. These bulky ligands, preferably the ring(s) or ring system(s) are typically composed of atoms selected from Groups 13 to 16 atoms of the Periodic Table of Elements, preferably the atoms are selected from the group consisting of carbon, nitrogen, oxygen, silicon, sulfur, phosphorous, germanium, boron and aluminum or a combination thereof.
15 Most preferably the ring(s) or ring system(s) are composed of carbon atoms such as but not limited to those cyclopentadienyl ligands or cyclopentadienyl-type ligand structures or other similar functioning ligand structure such as a pentadiene, a cyclooctatetraendiyl or an imide ligand. The metal atom is preferably selected from Groups 3 through 15 and the lanthanide or actinide series of the Periodic
20 Table of Elements. Preferably the metal is a transition metal from Groups 4 through 12, more preferably Groups 4, 5 and 6, and most preferably the transition metal is from Group 4.

In one embodiment, the bulky ligand metallocene-type catalyst compounds of the invention are represented by the formula:



where M is a metal atom from the Periodic Table of the Elements and may be a Group 3 to 12 metal or from the lanthanide or actinide series of the Periodic Table of Elements, preferably M is a Group 4, 5 or 6 transition metal, more preferably M is a Group 4 transition metal, even more preferably M is zirconium, hafnium or
30 titanium. The bulky ligands, L^A and L^B , are open, acyclic or fused ring(s) or ring system(s) and are any ancillary ligand system, including unsubstituted or substituted, cyclopentadienyl ligands or cyclopentadienyl-type ligands, heteroatom substituted and/or heteroatom containing cyclopentadienyl-type ligands. Non-limiting examples of bulky ligands include cyclopentadienyl ligands,
35 cyclopentaphenanthrene-yl ligands, indenyl ligands, benzindenyl ligands, fluorenyl

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ligands, octahydrofluorenyl ligands, cyclooctatetraendiyl ligands, cyclopentacyclododecene ligands, azenyl ligands, azulene ligands, pentalene ligands, phosphoyl ligands, phosphinimine (WO 99/40125), pyrrolyl ligands, pyrozolyl ligands, carbazolyl ligands, borabenzene ligands, including

5 hydrogenated versions thereof, for example tetrahydroindenyl ligands. In one embodiment, L^A and L^B may be any other ligand structure capable of η -bonding to M, preferably η^3 -bonding to M and most preferably η^5 -bonding. In yet another embodiment, the atomic molecular weight (MW) of L^A or L^B exceeds 60 a.m.u. (9.96×10^{-23} g), preferably greater than 65 a.m.u. (1.08×10^{-22} g). In another

10 embodiment, L^A and L^B may comprise one or more heteroatoms, for example, nitrogen, silicon, boron, germanium, sulfur and phosphorous, in combination with carbon atoms to form an open, acyclic, or preferably a fused, ring or ring system, for example, a hetero-cyclopentadienyl ancillary ligand. Other L^A and L^B bulky ligands include but are not limited to bulky amides, phosphides, alkoxides,

15 aryloxides, imides, carbolides, borollides, porphyrins, phthalocyanines, corrins and other polyazomacrocycles. Independently, each L^A and L^B may be the same or different type of bulky ligand that is bonded to M. In one embodiment of formula (I) only one of either L^A or L^B is present.

Independently, each L^A and L^B may be unsubstituted or substituted with a

20 combination of substituent groups R. Non-limiting examples of substituent groups R include one or more from the group selected from hydrogen, or linear, branched alkyl radicals, or alkenyl radicals, alkynyl radicals, cycloalkyl radicals or aryl radicals, acyl radicals, aroyl radicals, alkoxy radicals, aryloxy radicals, alkylthio radicals, dialkylamino radicals, alkoxycarbonyl radicals, aryloxycarbonyl

25 radicals, carbomoyl radicals, alkyl- or dialkyl- carbamoyl radicals, acyloxy radicals, acylamino radicals, aroylamino radicals, straight, branched or cyclic, alkylene radicals, or combination thereof. In a preferred embodiment, substituent groups R have up to 50 non-hydrogen atoms, preferably from 1 to 30 carbon, that can also be substituted with halogens or heteroatoms. Non-limiting examples of

30 alkyl substituents R include methyl, ethyl, propyl, butyl, pentyl, hexyl, cyclopentyl, cyclohexyl, benzyl or phenyl groups, including all their isomers, for example tertiary butyl and isopropyl. Other hydrocarbyl radicals include fluoromethyl, fluroethyl, difluroethyl, iodopropyl, bromohexyl, chlorobenzyl and hydrocarbyl substituted organometalloid radicals including trimethylsilyl,

35 trimethylgermyl, methyldiethylsilyl; and halocarbyl-substituted organometalloid

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radicals including tris(trifluoromethyl)-silyl, methyl-bis(difluoromethyl)silyl, bromomethyldimethylgermyl; and disubstituted boron radicals including dimethylboron for example; and disubstituted pnictogen radicals including dimethylamine, dimethylphosphine, diphenylamine, methylphenylphosphine, chalcogen radicals including methoxy, ethoxy, propoxy, phenoxy, methylsulfide and ethylsulfide. Non-hydrogen substituents R include the atoms carbon, silicon, boron, aluminum, nitrogen, phosphorous, oxygen, tin, sulfur, germanium, including olefins such as but not limited to olefinically unsaturated substituents including vinyl-terminated ligands, for example but-3-enyl, prop-2-enyl, hex-5-enyl. Also, at least two R groups, preferably two adjacent R groups, are joined to form a ring structure having from 3 to 30 atoms selected from carbon, nitrogen, oxygen, phosphorous, silicon, germanium, aluminum, boron or a combination thereof. Also, a substituent group R group such as 1-butanyl may form a carbon sigma bond to the metal M.

Other ligands may be bonded to the metal M, such as at least one leaving group Q. For the purposes of this patent specification and appended claims the term "leaving group" is any ligand that can be abstracted from a bulky ligand metallocene-type catalyst compound to form a bulky ligand metallocene-type catalyst cation capable of polymerizing one or more olefin(s). In one embodiment, Q is a monoanionic labile ligand having a sigma-bond to M. Depending on the oxidation state of the metal, the value for n is 0, 1 or 2 such that formula (I) above represents a neutral bulky ligand metallocene-type catalyst compound.

Non-limiting examples of Q ligands include weak bases such as amines, phosphines, ethers, carboxylates, dienes, hydrocarbyl radicals having from 1 to 20 carbon atoms, hydrides or halogens or a combination thereof. In another embodiment, two or more Q's form a part of a fused ring or ring system. Other examples of Q ligands include those substituents for R as described above and including cyclobutyl, cyclohexyl, heptyl, tolyl, trifluoromethyl, tetramethylene, pentamethylene, methylidene, methoxy, ethoxy, propoxy, phenoxy, bis(N-methylanilide), dimethylamide, dimethylphosphide radicals.

In one embodiment, the bulky ligand metallocene-type catalyst compounds of the invention include those of formula (I) where L^A and L^B are bridged to each other by at least one bridging group, A, such that the formula is represented by



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These bridged compounds represented by formula (II) are known as bridged, bulky ligand metallocene-type catalyst compounds. L^A , L^B , M, Q and n are as defined above. Non-limiting examples of bridging group A include bridging groups containing at least one Group 13 to 16 atom, often referred to as a
5 divalent moiety such as but not limited to at least one of a carbon, oxygen, nitrogen, silicon, aluminum, boron, germanium and tin atom or a combination thereof. Preferably bridging group A contains a carbon, silicon or germanium atom, most preferably A contains at least one silicon atom or at least one carbon atom. The bridging group A may also contain substituent groups R as defined
10 above including halogens and iron. Non-limiting examples of bridging group A may be represented by R'_2C , R'_2Si , $R'_2Si R'_2Si$, R'_2Ge , R'_2P , where R' is independently, a radical group which is hydride, hydrocarbyl, substituted hydrocarbyl, halocarbyl, substituted halocarbyl, hydrocarbyl-substituted organometalloid, halocarbyl-substituted organometalloid, disubstituted boron,
15 disubstituted pnictogen, substituted chalcogen, or halogen or two or more R' may be joined to form a ring or ring system. In one embodiment, the bridged, bulky ligand metallocene-type catalyst compounds of formula (II) have two or more bridging groups A (EP 664 301 B1).

In one embodiment, the bulky ligand metallocene-type catalyst
20 compounds are those where the R substituents on the bulky ligands L^A and L^B of formulas (I) and (II) are substituted with the same or different number of substituents on each of the bulky ligands. In another embodiment, the bulky ligands L^A and L^B of formulas (I) and (II) are different from each other.

Other bulky ligand metallocene-type catalyst compounds and catalyst
25 systems useful in the invention may include those described in U.S. Patent Nos. 5,064,802, 5,145,819, 5,149,819, 5,243,001, 5,239,022, 5,276,208, 5,296,434, 5,321,106, 5,329,031, 5,304,614, 5,677,401, 5,723,398, 5,753,578, 5,854,363, 5,856,547 5,858,903, 5,859,158, 5,900,517, 5,939,503 and 5,962,718 and PCT publications WO 93/08221, WO 93/08199, WO 95/07140, WO 98/11144, WO
30 98/41530, WO 98/41529, WO 98/46650, WO 99/02540 and WO 99/14221 and European publications EP-A-0 578 838, EP-A-0 638 595, EP-B-0 513 380, EP-A1-0 816 372, EP-A2-0 839 834, EP-B1-0 632 819, EP-B1-0 739 361, EP-B1-0 748 821 and EP-B1-0 757 996.

In one embodiment, bulky ligand metallocene-type catalysts compounds
35 useful in the invention include bridged heteroatom, mono-bulky ligand

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metallocene-type compounds. These types of catalysts and catalyst systems are described in, for example, PCT publication WO 92/00333, WO 94/07928, WO 91/04257, WO 94/03506, WO96/00244, WO 97/15602 and WO 99/20637 and U.S. Patent Nos. 5,057,475, 5,096,867, 5,055,438, 5,198,401, 5,227,440 and 5,264,405 and European publication EP-A-0 420 436.

In this embodiment, the bulky ligand metallocene-type catalyst compound is represented by the formula:



where M is a Group 3 to 16 metal atom or a metal selected from the Group of actinides and lanthanides of the Periodic Table of Elements, preferably M is a Group 4 to 12 transition metal, and more preferably M is a Group 4, 5 or 6 transition metal, and most preferably M is a Group 4 transition metal in any oxidation state, especially titanium; L^C is a substituted or unsubstituted bulky ligand bonded to M; J is bonded to M; A is bonded to M and J; J is a heteroatom ancillary ligand; and A is a bridging group; Q is a univalent anionic ligand; and n is the integer 0, 1 or 2. In formula (III) above, L^C , A and J form a fused ring system. In an embodiment, L^C of formula (III) is as defined above for L^A , A, M and Q of formula (I).

In formula (III) J is a heteroatom containing ligand in which J is an element with a coordination number of three from Group 15 or an element with a coordination number of two from Group 16 of the Periodic Table of Elements. Preferably J contains a nitrogen, phosphorus, oxygen or sulfur atom with nitrogen being most preferred.

In another embodiment, the bulky ligand type metallocene-type catalyst compound is a complex of a metal, preferably a transition metal, a bulky ligand, preferably a substituted or unsubstituted pi-bonded ligand, and one or more heteroallyl moieties, such as those described in U.S. Patent Nos. 5,527,752 and 5,747,406 and EP-B1-0 735 057.

In an embodiment, the bulky ligand metallocene-type catalyst compound is represented by the formula:



where M is a Group 3 to 16 metal, preferably a Group 4 to 12 transition metal, and most preferably a Group 4, 5 or 6 transition metal; L^D is a bulky ligand that is bonded to M; each Q is independently bonded to M and $Q_2(YZ)$ forms a uncharged polydentate ligand; A or Q is a univalent anionic

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ligand also bonded to M; X is a univalent anionic group when n is 2 or X is a divalent anionic group when n is 1; n is 1 or 2.

In formula (IV), L and M are as defined above for formula (I). Q is as defined above for formula (I), preferably Q is selected from the group consisting of -O-, -NR-, -CR₂- and -S-; Y is either C or S; Z is selected from the group consisting of OR, -NR₂, -CR₃, -SR, -SiR₃, -PR₂, -H, and substituted or unsubstituted aryl groups, with the proviso that when Q is -NR- then Z is selected from one of the group consisting of -OR, -NR₂, -SR, -SiR₃, -PR₂ and -H; R is selected from a group containing carbon, silicon, nitrogen, oxygen, and/or phosphorus, preferably where R is a hydrocarbon group containing from 1 to 20 carbon atoms, most preferably an alkyl, cycloalkyl, or an aryl group; n is an integer from 1 to 4, preferably 1 or 2; X is a univalent anionic group when n is 2 or X is a divalent anionic group when n is 1; preferably X is a carbamate, carboxylate, or other heteroallyl moiety described by the Q, Y and Z combination.

In another embodiment of the invention, the bulky ligand metallocene-type catalyst compounds are heterocyclic ligand complexes where the bulky ligands, the ring(s) or ring system(s), include one or more heteroatoms or a combination thereof. Non-limiting examples of heteroatoms include a Group 13 to 16 element, preferably nitrogen, boron, sulfur, oxygen, aluminum, silicon, phosphorous and tin. Examples of these bulky ligand metallocene-type catalyst compounds are described in WO 96/33202, WO 96/34021, WO 97/17379, WO 98/22486 and WO 99/40095 (dicarbamoyl metal complexes) and EP-A1-0 874 005 and U.S. Patent No. 5,637,660, 5,539,124, 5,554,775, 5,756,611, 5,233,049, 5,744,417, and 5,856,258.

In another embodiment, the bulky ligand metallocene-type catalyst compounds are those complexes known as transition metal catalysts based on bidentate ligands containing pyridine or quinoline moieties, such as those described in U.S. Patent No. 6,103,657. In another embodiment, the bulky ligand metallocene-type catalyst compounds are those described in PCT publications WO 99/01481 and WO 98/42664.

In one embodiment, the bulky ligand metallocene-type catalyst compound is represented by the formula:



where M is a metal selected from Group 3 to 13 or lanthanide and actinide series of the Periodic Table of Elements; Q is bonded to M and each Q is a monovalent, bivalent, or trivalent anion; X and Y are bonded to M; one or more of X and Y are heteroatoms, preferably both X and Y are heteroatoms; Y is contained in a heterocyclic ring J, where J comprises from 2 to 50 non-hydrogen atoms, preferably 2 to 30 carbon atoms; Z is bonded to X, where Z comprises 1 to 50 non-hydrogen atoms, preferably 1 to 50 carbon atoms, preferably Z is a cyclic group containing 3 to 50 atoms, preferably 3 to 30 carbon atoms; t is 0 or 1; when t is 1, A is a bridging group joined to at least one of X, Y or J, preferably X and J; q is 1 or 2; n is an integer from 1 to 4 depending on the oxidation state of M. In one embodiment, where X is oxygen or sulfur then Z is optional. In another embodiment, where X is nitrogen or phosphorous then Z is present. In an embodiment, Z is preferably an aryl group, more preferably a substituted aryl group.

Other Bulky Ligand Metallocene-Type Catalyst Compounds

It is within the scope of this invention, in one embodiment, that the bulky ligand metallocene-type catalyst compounds include complexes of Ni^{2+} and Pd^{2+} described in the articles Johnson, et al., "New Pd(II)- and Ni(II)-Based Catalysts for Polymerization of Ethylene and α -Olefins", J. Am. Chem. Soc. 1995, 117, 6414-6415 and Johnson, et al., "Copolymerization of Ethylene and Propylene with Functionalized Vinyl Monomers by Palladium(II) Catalysts", J. Am. Chem. Soc., 1996, 118, 267-268, and WO 96/23010 published August 1, 1996, WO 99/02472, U.S. Patent Nos. 5,852,145, 5,866,663 and 5,880,241. These complexes can be either dialkyl ether adducts, or alkylated reaction products of the described dihalide complexes that can be activated to a cationic state by the activators of this invention described below.

Also included as bulky ligand metallocene-type catalyst are those diimine based ligands of Group 8 to 10 metal compounds disclosed in PCT publications WO 96/23010 and WO 97/48735 and Gibson, et. al., Chem. Comm., pp. 849-850 (1998).

Other bulky ligand metallocene-type catalysts are those Group 5 and 6 metal imido complexes described in EP-A2-0 816 384 and U.S. Patent No. 5,851,945. In addition, bulky ligand metallocene-type catalysts include bridged bis(arylamido) Group 4 compounds described by D.H. McConville, et

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al., in *Organometallics* 1995, 14, 5478-5480. In addition, bridged bis(amido) catalyst compounds are described in WO 96/27439. Other bulky ligand metallocene-type catalysts are described as bis(hydroxy aromatic nitrogen ligands) in U.S. Patent No. 5,852,146. Other metallocene-type catalysts containing one or more Group 15 atoms include those described in WO 98/46651. Still another metallocene-type bulky ligand metallocene-type catalysts include those multinuclear bulky ligand metallocene-type catalysts as described in WO 99/20665.

It is also contemplated that in one embodiment, the bulky ligand metallocene-type catalysts of the invention described above include their structural or optical or enantiomeric isomers (meso and racemic isomers, for example see U.S. Patent No. 5,852,143) and mixtures thereof.

Activator and Activation Methods for the Bulky Ligand Metallocene-Type Catalyst Compounds

The above described bulky ligand metallocene-type catalyst compounds are typically activated in various ways to yield catalyst compounds having a vacant coordination site that will coordinate, insert, and polymerize olefin(s).

For the purposes of this patent specification and appended claims, the term "activator" is defined to be any compound or component or method which can activate any of the bulky ligand metallocene-type catalyst compounds of the invention as described above. Non-limiting activators, for example may include a Lewis acid or a non-coordinating ionic activator or ionizing activator or any other compound including Lewis bases, aluminum alkyls, conventional-type cocatalysts and combinations thereof that can convert a neutral bulky ligand metallocene-type catalyst compound to a catalytically active bulky ligand metallocene cation. It is within the scope of this invention to use alumoxane or modified alumoxane as an activator, and/or to also use ionizing activators, neutral or ionic, such as tri (n-butyl) ammonium tetrakis (pentafluorophenyl) boron, a trisperfluorophenyl boron metalloid precursor or a trisperfluoronaphthyl boron metalloid precursor, polyhalogenated heteroborane anions (WO 98/43983) or combination thereof, that would ionize the neutral bulky ligand metallocene-type catalyst compound.

In one embodiment, an activation method using ionizing ionic compounds not containing an active proton but capable of producing both a bulky ligand metallocene-type catalyst cation and a non-coordinating anion are also

contemplated, and are described in EP-A- 0 426 637, EP-A- 0 573 403 and U.S. Patent No. 5,387,568.

There are a variety of methods for preparing alumoxane and modified alumoxanes, non-limiting examples of which are described in U.S. Patent No. 4,665,208, 4,952,540, 5,091,352, 5,206,199, 5,204,419, 4,874,734, 4,924,018, 4,908,463, 4,968,827, 5,308,815, 5,329,032, 5,248,801, 5,235,081, 5,157,137, 5,103,031, 5,391,793, 5,391,529, 5,693,838, 5,731,253, 5,731,451, 5,744,656, 5,847,177, 5,854,166, 5,856,256 and 5,939,346 and European publications EP-A-0 561 476, EP-B1-0 279 586, EP-A-0 594-218 and EP-B1-0 586 665, and PCT publication WO 94/10180.

Organoaluminum compounds include trimethylaluminum, triethylaluminum, triisobutylaluminum, tri-n-hexylaluminum, tri-n-octylaluminum.

Ionizing compounds may contain an active proton, or some other cation associated with but not coordinated to or only loosely coordinated to the remaining ion of the ionizing compound. Such compounds are described in European publications EP-A-0 570 982, EP-A-0 520 732, EP-A-0 495 375, EP-B1-0 500 944, EP-A-0 277 003 and EP-A-0 277 004, and U.S. Patent Nos. 5,153,157, 5,198,401, 5,066,741, 5,206,197, 5,241,025, 5,384,299 and 5,502,124.

Other activators include those described in PCT publication WO 98/07515 such as tris (2,2',2''-nonafluorobiphenyl) fluoroaluminate. Combinations of activators are also contemplated by the invention, for example, alumoxanes and ionizing activators in combinations, see for example, EP-B1 0 573 120, PCT publications WO 94/07928 and WO 95/14044 and U.S. Patent Nos. 5,153,157 and 5,453,410. WO 98/09996 describes activating bulky ligand metallocene-type catalyst compounds with perchlorates, periodates and iodates including their hydrates. WO 98/30602 and WO 98/30603 describe the use of lithium (2,2'-bisphenyl-ditrimethylsilicate) 4THF as an activator for a bulky ligand metallocene-type catalyst compound. WO 99/18135 describes the use of organoboron-aluminum activators. EP-B1-0 781 299 describes using a silylium salt in combination with a non-coordinating compatible anion. Also, methods of activation such as using radiation (see EP-B1-0 615 981) and electro-chemical oxidation are also contemplated as activating methods for the purposes of rendering the neutral bulky ligand metallocene-type catalyst compound or precursor to a bulky ligand metallocene-type cation capable of polymerizing olefins. Other activators or methods for activating a bulky ligand metallocene-type catalyst

compound are described in for example, U.S. Patent Nos. 5,849,852, 5,859,653 and 5,869,723 and WO 98/32775, WO 99/42467 (dioctadecylmethylammonium-bis(tris(pentafluorophenyl)borane)benzimidazolide).

It is also within the scope of this invention that the above described bulky ligand metallocene-type catalyst compounds can be combined with one or more of the catalyst compounds represented by formulas (I) through (V) with one or more activators or activation methods described above.

It is further contemplated by the invention that other catalysts can be combined with the bulky ligand metallocene-type catalyst compounds of the invention. For example, see U.S. Patent Nos. 4,937,299, 4,935,474, 5,281,679, 5,359,015, 5,470,811, and 5,719,241. It is also contemplated that any one of the bulky ligand metallocene-type catalyst compounds of the invention have at least one fluoride or fluorine containing leaving group as described in U.S. Patent No. 6,632,901.

In another embodiment of the invention one or more bulky ligand metallocene-type catalyst compounds or catalyst systems may be used in combination with one or more conventional-type catalyst compounds or catalyst systems. Non-limiting examples of mixed catalysts and catalyst systems are described in U.S. Patent Nos. 4,159,965, 4,325,837, 4,701,432, 5,124,418, 5,077,255, 5,183,867, 5,391,660, 5,395,810, 5,691,264, 5,723,399 and 5,767,031 and PCT Publication WO 96/23010 published August 1, 1996.

Supports, Carriers and General Supporting Techniques

The above described bulky ligand metallocene-type catalyst compounds and catalyst systems may be combined with one or more support materials or carriers using one of the support methods well known in the art or as described below. For example, in a most preferred embodiment, a bulky ligand metallocene-type catalyst compound or catalyst system is in a supported form, for example deposited on, contacted with, vaporized with, bonded to, or incorporated within, adsorbed or absorbed in, or on, a support or carrier.

The terms "support" or "carrier" are used interchangeably and are any support material, preferably a porous support material, including inorganic or organic support materials. Non-limiting examples of inorganic support materials include inorganic oxides and inorganic chlorides. Other carriers include resinous support materials such as polystyrene, functionalized or crosslinked organic supports, such as polystyrene divinyl

benzene polyolefins or polymeric compounds, or any other organic or inorganic support material, or mixtures thereof.

The preferred carriers are inorganic oxides that include those Group 2, 3, 4, 5, 13 or 14 metal oxides. The preferred supports include silica, alumina, silica-alumina and mixtures thereof. Other useful supports include magnesia, titania, zirconia, magnesium chloride, montmorillonite (EP-B1 0 511 665), phyllosilicate, zeolites, talc and clays. Also, combinations of these support materials may be used, for example, silica-chromium, silica-alumina and silica-titania. Additional support materials may include those porous acrylic polymers described in EP 0 767 184 B1. Other support materials include nanocomposites as described in PCT WO 99/47598.

It is preferred that the carrier, most preferably an inorganic oxide, has a surface area in the range of from about 10 to about 700 m²/g, pore volume in the range of from about 0.1 to about 4.0 cc/g and average particle size in the range of from about 5 to about 500 µm. More preferably, the surface area of the carrier is in the range of from about 50 to about 500 m²/g, pore volume of from about 0.5 to about 3.5 cc/g and average particle size of from about 10 to about 200 µm. Most preferably the surface area of the carrier is in the range from about 100 to about 1000 m²/g, pore volume from about 0.8 to about 5.0 cc/g and average particle size is from about 5 to about 100 µm. The average pore size of the carrier of the invention typically has pore size in the range of from 10 to 1000Å (1 x 10⁻⁷ to 1 x 10⁻⁵ cm), preferably 50 to about 500Å (5 x 10⁻⁷ to about 5 x 10⁻⁶ cm), and most preferably 75 to about 450Å (7.5 x 10⁻⁷ to about 4.5 x 10⁻⁶ cm).

Examples of supporting the bulky ligand metallocene-type catalyst systems of the invention are described in U.S. Patent Nos. 4,701,432, 4,808,561, 4,912,075, 4,925,821, 4,937,217, 5,008,228, 5,238,892, 5,240,894, 5,332,706, 5,346,925, 5,422,325, 5,466,649, 5,466,766, 5,468,702, 5,529,965, 5,554,704, 5,629,253, 5,639,835, 5,625,015, 5,643,847, 5,665,665, 5,698,487, 5,714,424, 5,723,400, 5,723,402, 5,731,261, 5,759,940, 5,767,032, 5,770,664, 5,846,895, 5,939,348, 5,468,702 and 6,090,740, and PCT publications WO 95/32995, WO 95/14044, WO 96/06187 and WO 97/02297, and EP-B1-0 685 494.

There are various other methods in the art for supporting a polymerization catalyst compound or catalyst system of the invention. For example, the bulky ligand metallocene-type catalyst compound of the invention may contain a polymer bound ligand as described in U.S. Patent Nos. 5,473,202 and 5,770,755; the bulky ligand metallocene-type catalyst

system of the invention may be spray dried as described in U.S. Patent No. 5,648,310; the support used with the bulky ligand metallocene-type catalyst system of the invention is functionalized as described in European publication EP-A-0 802 203, or at least one substituent or leaving group is selected as described in U.S. Patent No. 5,688,880.

In a preferred embodiment, the invention provides for a supported bulky ligand metallocene-type catalyst system that includes a surface modifier that is used in the preparation of the supported catalyst system as described in PCT publication WO 96/11960. The catalyst systems of the invention can be prepared in the presence of an olefin, for example hexane-1.

In another embodiment, the bulky ligand metallocene-type catalyst system can be combined with a carboxylic acid salt of a metal ester, for example aluminum carboxylates such as aluminum mono, di- and tri- stearates, aluminum octoates, oleates and cyclohexylbutyrates, as described in U.S. Application Serial No. 09/113,216, filed July 10, 1998, published as US 2002 000448A1 published on January 10, 2002.

A preferred method for producing a supported bulky ligand metallocene-type catalyst system is described below and is described in PCT publications WO 96/00245 and WO 96/00243 both published January 4, 1996. In this preferred method, the bulky ligand metallocene-type catalyst compound is slurried in a liquid to form a metallocene solution and a separate solution is formed containing an activator and a liquid. The liquid may be any compatible solvent or other liquid capable of forming a solution with the bulky ligand metallocene-type catalyst compounds and/or activator of the invention. In the most preferred embodiment the liquid is a cyclic aliphatic or aromatic hydrocarbon, most preferably toluene. The bulky ligand metallocene-type catalyst compound and activator solutions are mixed together heated and added to a porous support, optionally a heated porous support, or a porous support, optionally a heated porous support is added to the solutions such that the total

volume of the bulky ligand metallocene-type catalyst compound solution and the activator solution or the bulky ligand metallocene-type catalyst compound and activator solution is less than four times the pore volume of the porous support, more preferably less than three times, even more preferably less than two times; preferred ranges being from 1.1 times to 3.5 times range and most preferably in the 1.2 to 3 times range.

Procedures for measuring the total pore volume of a porous support are well known in the art. Details of one of these procedures is discussed in Volume 1, *Experimental Methods in Catalytic Research* (Academic Press, 1968) (specifically see pages 67-96). This preferred procedure involves the use of a classical BET apparatus for nitrogen absorption. Another method well known in the art is described in Innes, *Total Porosity and Particle Density of Fluid Catalysts By Liquid Titration*, Vol. 28, No. 3, Analytical Chemistry 332-334 (March, 1956).

The mole ratio of the metal of the activator component to the metal of the supported bulky ligand metallocene-type catalyst compounds are in the range of between 0.3:1 to 1000:1, preferably 20:1 to 800:1, and most preferably 50:1 to 500:1. Where the activator is an ionizing activator such as those based on the anion tetrakis(pentafluorophenyl)boron, the mole ratio of the metal of the activator component to the metal component of the bulky ligand metallocene-type catalyst is preferably in the range of between 0.3:1 to 3:1.

In one embodiment of the invention, olefin(s), preferably C₂ to C₃₀ olefin(s) or alpha-olefin(s), preferably ethylene or propylene or combinations thereof are prepolymerized in the presence of the supported bulky ligand metallocene-type catalyst system of the invention prior to the main polymerization. The prepolymerization can be carried out batchwise or continuously in gas, solution or slurry phase including at elevated pressures. The prepolymerization can take place with any olefin monomer or combination and/or in the presence of any molecular weight controlling agent such as hydrogen. For examples of prepolymerization procedures, see U.S. Patent Nos. 4,748,221, 4,789,359, 4,923,833, 4,921,825, 5,283,278 and 5,705,578 and European publication EP-B-0279 863 and PCT Publication WO 97/44371.

Method of Preparing the Supported Catalyst System of the Invention

The method for making the supported catalyst system of the invention generally involves the combining, contacting, vaporizing, blending, bonding

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and/or mixing any of the above described bulky ligand metallocene-type catalyst compounds using any of the above described methods of supporting them, wherein the bulky ligand metallocene-type catalyst compound and/or reaction product of an activator and a bulky ligand metallocene-type catalyst compound
5 and/ or an activated bulky ligand metallocene-type catalyst is heated and then combined with a carrier, optionally a heated carrier. In a preferred embodiment, the bulky ligand metallocene-type catalyst compound is combined with an activator to form a reaction product that is then heated and added to a carrier, optionally a heated carrier. The methods of heating supported catalyst system
10 components (including warming) are well known in the art.

In one preferred embodiment, at least one bulky ligand metallocene-type catalyst compound and at least one activator are combined to form a mixture; the mixture is heated to a first temperature from 25°C to 150°C, preferably from 50°C to 125°C, more preferably from 75°C to 100°C, most preferably from 80°C to
15 100°C; and the heated mixture is combined with a carrier, preferably the carrier is at ambient conditions, at a third temperature that is the same or different from the first and/or second temperature.

In another preferred embodiment, at least one bulky ligand metallocene-type catalyst compound and at least one activator are combined to form a mixture;
20 the mixture is heated to a first temperature from 25°C to 150°C, preferably from 50°C to 125°C, more preferably from 75°C to 100°C, most preferably from 80°C to 100°C; a carrier is heated to a second temperature in the range of from 30°C to 100°C, preferably from 40°C to 100°C, more preferably from 70°C to 100°C, most preferably from 85°C to 100°C; and the heated carrier and the heated
25 mixture are combined at a third temperature that is the same or different from the first and/or second temperature. Preferably in this embodiment, the first, second and third temperatures are substantially the same, in the range of from 50°C to 125°C, preferably from 65°C to 100°C, more preferably from 75°C to 100°C, most preferably from 85°C to 100°C. In one embodiment, the heated carrier and
30 the heated mixture after being combined are maintained at a temperature greater than 50°C, preferably greater than 70°C, more preferably greater than 80°C and most preferably greater than 85°C, for a period of time from about 30 seconds to about 12 hours, preferably from about 1 minute to about 6 hours, more preferably from 10 minutes to about 4 hours, and most preferably from about 30 minutes to
35 about 3 hours. In a further embodiment, after the heated mixture and carrier,

In another preferred embodiment, at least one bulky ligand metallocene-type catalyst compound and at least one activator are combined to form a mixture; the mixture is heated to a first temperature from 25°C to 150°C, preferably from 50°C to 125°C, more preferably from 75°C to 100°C, most preferably from 80°C to 100°C; a carrier is heated to a second temperature in the range of from 30°C to 100°C, preferably from 40°C to 100°C, more preferably from 70°C to 100°C, most preferably from 85°C to 100°C; and the heated carrier and the heated mixture are combined at a third temperature that is the same or different from the first and/or second temperature. Preferably in this embodiment, the first, second and third temperatures are substantially the same, in the range of from 50°C to 125°C, preferably from 65°C to 100°C, more preferably from 75°C to 100°C, most preferably from 85°C to 100°C. In one embodiment, the heated carrier and the heated mixture after being combined are maintained at a temperature greater than 50°C, preferably greater than 70°C, more preferably greater than 80°C and most preferably greater than 85°C, for a period of time from about 30 seconds to about 12 hours, preferably from about 1 minute to about 6 hours, more preferably from 10 minutes to about 4 hours, and most preferably from about 30 minutes to about 3 hours. In a further embodiment, after the heated mixture and carrier, optionally the heated carrier, have been combined at a specified temperature and time period, the combination is then dried to a free flowing powder by any of the techniques well known in the art.

Other embodiments are contemplated by the present invention, for example (1) heating a bulky ligand metallocene-type catalyst compound in a solution and adding it to a carrier that has been optionally heated, followed by then adding a activator that is optionally heated; (2) adding an activator, optionally heated and/or optionally in a solution, to a carrier that has been optionally heated, heating a bulky ligand metallocene-type catalyst compound in a liquid, heating the carrier if not already been heated, and combining the heated bulky ligand metallocene-type catalyst compound to the heated carrier; and (3) heating a bulky ligand metallocene catalyst compound solution; adding an activator to the heated solution; and then combining the heated solution with a carrier that has been optionally heated. In these embodiments, “heating” or “heated” means that what is “heated” or “heating” is maintained at substantially the same temperature “heated” or “heating” to.

In one embodiment the invention is directed to a supported catalyst composition comprising a bulky ligand metallocene-type catalyst compound and an activator that have been combined at a temperature in the range of from 30 °C to 125°C, preferably from 50°C to 110°C, more preferably from 60°C to 100°C, most preferably from 75°C to 100°C. The supported catalyst composition in one embodiment is dried or substantially dried to a free flowing powder composition for use in a polymerization or prepolymerization process as described later in this patent specification. In yet another embodiment, the free flowing composition is reslurried in a liquid such as mineral oil, toluene, or any the hydrocarbon prior to combining with the additional bulky ligand metallocene-type catalyst compound.

In another embodiment, the supported bulky ligand metallocene-type catalyst system of the invention particularly in a gas phase process has a productivity greater than 4000 grams of polymer per gram of catalyst, preferably greater than 5000 grams of polymer per gram of catalyst, more preferably greater than 6000 grams of polymer per gram of catalyst and most preferably greater than 7000 grams of polymer per gram of catalyst.

The preferred bulky ligand metallocene-type catalyst compounds are those having a low solubility in toluene, for example, less than 20 weight percent, preferably less than 15 weight percent, more preferably less than 10 weight percent, even more preferably less than 5 weight percent and most preferably less than about 3 weight percent, of the bulky ligand metallocene-type catalyst compound in toluene at room temperature (25°C).

Polymerization Process

The supported catalyst systems or compositions of the invention described above are suitable for use in any prepolymerization and/or polymerization process over a wide range of temperatures and pressures. The temperatures may be in the range of from -60 °C to about 280°C, preferably from 50°C to about 200°C, and the pressures employed may be in the range from 1 atmosphere to about 500 atmospheres or higher.

Polymerization processes include solution, gas phase, slurry phase and a high pressure process or a combination thereof. Particularly preferred is a gas phase or slurry phase polymerization of one or more olefins at least one of which is ethylene or propylene.

In one embodiment, the process of this invention is directed toward a solution, high pressure, slurry or gas phase polymerization process of one or more

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In one embodiment, the invention is directed to a polymerization process, particularly a gas phase or slurry phase process, for polymerizing propylene alone or with one or more other monomers including ethylene, and/or other olefins having from 4 to 12 carbon atoms. Polypropylene polymers may be produced
5 using the particularly bridged bulky ligand metallocene-type catalysts as described in U.S. Patent Nos. 5,296,434 and 5,278,264.

Typically in a gas phase polymerization process a continuous cycle is employed where in one part of the cycle of a reactor system, a cycling gas stream, otherwise known as a recycle stream or fluidizing medium, is heated in the reactor
10 by the heat of polymerization. This heat is removed from the recycle composition in another part of the cycle by a cooling system external to the reactor. Generally, in a gas fluidized bed process for producing polymers, a gaseous stream containing one or more monomers is continuously cycled through a fluidized bed in the presence of a catalyst under reactive conditions. The gaseous stream is
15 withdrawn from the fluidized bed and recycled back into the reactor.

Simultaneously, polymer product is withdrawn from the reactor and fresh monomer is added to replace the polymerized monomer. (See for example U.S. Patent Nos. 4,543,399, 4,588,790, 5,028,670, 5,317,036, 5,352,749, 5,405,922, 5,436,304, 5,453,471, 5,462,999, 5,616,661 and 5,668,228.)

20 The reactor pressure in a gas phase process may vary from about 100 psig (690 kPa) to about 500 psig (3448 kPa), preferably in the range of from about 200 psig (1379 kPa) to about 400 psig (2759 kPa), more preferably in the range of from about 250 psig (1724 kPa) to about 350 psig (2414 kPa).

The reactor temperature in a gas phase process may vary from about 30°C
25 to about 120°C, preferably from about 60°C to about 115°C, more preferably in the range of from about 70°C to 110°C, and most preferably in the range of from about 70°C to about 95°C.

Other gas phase processes contemplated by the process of the invention include series or multistage polymerization processes. Also gas phase processes
30 contemplated by the invention include those described in U.S. Patent Nos. 5,627,242, 5,665,818 and 5,677,375, and European publications EP-A- 0 794 200 EP-B1-0 649 992, EP-A- 0 802 202 and EP-B- 634 421.

In a preferred embodiment, the reactor utilized in the present invention is capable and the process of the invention is producing greater than 500 lbs of
35 polymer per hour (227 Kg/hr) to about 200,000 lbs/hr (90,900 Kg/hr) or higher of

polymer, preferably greater than 1000 lbs/hr (455 Kg/hr), more preferably greater than 10,000 lbs/hr (4540 Kg/hr), even more preferably greater than 25,000 lbs/hr (11,300 Kg/hr), still more preferably greater than 35,000 lbs/hr (15,900 Kg/hr), still even more preferably greater than 50,000 lbs/hr (22,700 Kg/hr) and most preferably greater than 65,000 lbs/hr (29,000 Kg/hr) to greater than 100,000 lbs/hr (45,500 Kg/hr).

A slurry polymerization process generally uses pressures in the range of from about 1 to about 50 atmospheres and even greater and temperatures in the range of 0°C to about 120°C. In a slurry polymerization, a suspension of solid, particulate polymer is formed in a liquid polymerization diluent medium to which ethylene and comonomers and often hydrogen along with catalyst are added. The suspension including diluent is intermittently or continuously removed from the reactor where the volatile components are separated from the polymer and recycled, optionally after a distillation, to the reactor. The liquid diluent employed in the polymerization medium is typically an alkane having from 3 to 7 carbon atoms, preferably a branched alkane. The medium employed should be liquid under the conditions of polymerization and relatively inert. When a propane medium is used the process must be operated above the reaction diluent critical temperature and pressure. Preferably, a hexane or an isobutane medium is employed.

A preferred polymerization technique of the invention is referred to as a particle form polymerization, or a slurry process where the temperature is kept below the temperature at which the polymer goes into solution. Such technique is well known in the art, and described in for instance U.S. Patent No. 3,248,179. Other slurry processes include those employing a loop reactor and those utilizing a plurality of stirred reactors in series, parallel, or combinations thereof. Non-limiting examples of slurry processes include continuous loop or stirred tank processes. Also, other examples of slurry processes are described in U.S. Patent No. 4,613,484.

In an embodiment the reactor used in the slurry process of the invention is capable of and the process of the invention is producing greater than 2000 lbs of polymer per hour (907 Kg/hr), more preferably greater than 5000 lbs/hr (2268 Kg/hr), and most preferably greater than 10,000 lbs/hr (4540 Kg/hr). In another embodiment the slurry reactor used in the process of the invention is producing

greater than 15,000 lbs of polymer per hour (6804 Kg/hr), preferably greater than 25,000 lbs/hr (11,340 Kg/hr) to about 100,000 lbs/hr (45,500 Kg/hr).

Examples of solution processes are described in U.S. Patent Nos. 4,271,060, 5,001,205, 5,236,998 and 5,589,555 and PCT WO 99/32525.

5 A preferred process of the invention is where the process, preferably a slurry or gas phase process is operated in the presence of a bulky ligand metallocene-type catalyst system of the invention and in the absence of or essentially free of any scavengers, such as triethylaluminum, trimethylaluminum, tri-isobutylaluminum and tri-n-hexylaluminum and diethyl aluminum chloride and
10 dibutyl zinc. This preferred process is described in PCT publication WO 96/08520 and U.S. Patent No. 5,712,352 and 5,763,543.

Polymer Products

The polymers produced by the process of the invention can be used in a wide variety of products and end-use applications. The polymers produced by the
15 process of the invention include linear low density polyethylene, elastomers, plastomers, high density polyethylenes, medium density polyethylenes, low density polyethylenes, polypropylene and polypropylene copolymers.

The polymers, typically ethylene based polymers, have a density in the range of from 0.86g/cc to 0.97 g/cc, preferably in the range of from 0.88 g/cc to
20 0.965 g/cc, more preferably in the range of from 0.900 g/cc to 0.96 g/cc, even more preferably in the range of from 0.905 g/cc to 0.95 g/cc, yet even more preferably in the range from 0.910 g/cc to 0.940 g/cc, and most preferably greater than 0.915 g/cc, preferably greater than 0.920 g/cc, and most preferably greater than 0.925 g/cc. Density is measured in accordance with ASTM-D-1238.

25 The polymers produced by the process of the invention typically have a molecular weight distribution, a weight average molecular weight to number average molecular weight (M_w/M_n) of greater than 1.5 to about 15, particularly greater than 2 to about 10, more preferably greater than about 2.2 to less than about 8, and most preferably from 2.5 to 8.

30 Also, the polymers of the invention typically have a narrow composition distribution as measured by Composition Distribution Breadth Index (CDBI). Further details of determining the CDBI of a copolymer are known to those skilled in the art. See, for example, PCT Patent Application WO 93/03093, published February 18, 1993.

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The bulky ligand metallocene-type catalyzed polymers of the invention in one embodiment have CDBI's generally in the range of greater than 50% to 100%, preferably 99%, preferably in the range of 55% to 85%, and more preferably 60% to 80%, even more preferably greater than 60%, still even more preferably greater than 65%.

In another embodiment, polymers produced using a bulky ligand metallocene-type catalyst system of the invention have a CDBI less than 50%, more preferably less than 40%, and most preferably less than 30%.

The polymers of the present invention in one embodiment have a melt index (MI) or (I_2) as measured by ASTM-D-1238-E in the range from 0.01 dg/min to 1000 dg/min, more preferably from about 0.01 dg/min to about 100 dg/min, even more preferably from about 0.1 dg/min to about 50 dg/min, and most preferably from about 0.1 dg/min to about 10 dg/min.

The polymers of the invention in an embodiment have a melt index ratio (I_{21}/I_2) (I_{21} is measured by ASTM-D-1238-F) of from 10 to less than 25, more preferably from about 15 to less than 25.

The polymers of the invention in a preferred embodiment have a melt index ratio (I_{21}/I_2) (I_{21} is measured by ASTM-D-1238-F) of from preferably greater than 25, more preferably greater than 30, even more preferably greater than 40, still even more preferably greater than 50 and most preferably greater than 65. In an embodiment, the polymer of the invention may have a narrow molecular weight distribution and a broad composition distribution or vice-versa, and may be those polymers described in U.S. Patent No. 5,798,427.

In yet another embodiment, propylene based polymers are produced in the process of the invention. These polymers include atactic polypropylene, isotactic polypropylene, hemi-isotactic and syndiotactic polypropylene. Other propylene polymers include propylene block or impact copolymers. Propylene polymers of these types are well known in the art see for example U.S. Patent Nos. 4,794,096, 3,248,455, 4,376,851, 5,036,034 and 5,459,117.

The polymers of the invention may be blended and/or coextruded with any other polymer. Non-limiting examples of other polymers include linear low density polyethylenes produced via conventional Ziegler-Natta and/or bulky ligand metallocene-type catalysis, elastomers, plastomers, high pressure low density polyethylene, high density polyethylenes and polypropylenes.

AMENDED SHEET

Polymers produced by the process of the invention and blends thereof are useful in such forming operations as film, sheet, and fiber extrusion and co-extrusion as well as blow molding, injection molding and rotary molding. Films include blown or cast films formed by coextrusion or by lamination useful as shrink film, cling film, stretch film, sealing films, oriented films, snack packaging, heavy duty bags, grocery sacks, baked and frozen food packaging, medical packaging, industrial liners, membranes, etc. in food-contact and non-food contact applications. Fibers include melt spinning, solution spinning and melt blown fiber operations for use in woven or non-woven form to make filters, diaper fabrics, medical garments, geotextiles, etc. Extruded articles include medical tubing, wire and cable coatings, pipe, geomembranes, and pond liners. Molded articles include single and multi-layered constructions in the form of bottles, tanks, large hollow articles, rigid food containers and toys, etc.

15

EXAMPLES

In order to provide a better understanding of the present invention including representative advantages thereof, the following examples are offered.

Density is measured in accordance with ASTM-D-1238.

20

I₂ is measured by ASTM-D-1238-E.

I₂₁ is measured by ASTM-D-1238-F.

The Fouling Index in the Tables below illustrates operability of the catalyst. The higher the value the greater the fouling observed. A Fouling Index of zero means substantially no or no visible fouling. A Fouling Index of 1 is indicative of light fouling, where a very light partial coating of polymer on the stirrer blades of a 2 liter slurry isobutane polymerization reactor and/or no reactor body sheeting. A Fouling Index of 2 is indicative of more than light fouling, where the stirrer blades have a heavier, painted-like, coating of polymer and/or the reactor body wall has some sheeting in a band of 1 to 2 inches (2.54 to 5.08 cm) wide on the reactor wall. A Fouling Index of 3 is considered medium fouling, where the stirrer blade has a thicker, latex-like, coating of polymer on the stirrer blade, some soft chunks in the reactor, and/or some reactor body sheeting with a band of 2 to 3 inch (5.08 to 7.62 cm) wide on the reactor wall. A Fouling Index of 4 is evidence of more than medium fouling, where the stirrer has a thick, latex-

like, coating, some harder chunks/balls of polymer, and/or the reactor body wall sheeting band is from 3 to 4 inches (7.62 to 10.2 cm) wide.

Activity in the Tables below is measured in grams of polyethylene(PE) per gram of polymerization catalyst-hour (gPE/gCat.h).

5 **Example 1**

 Into a 2 gallon (7.6 L) jacketed reactor was added 449 g, 7.74 moles of 30 wt% methylaluminoxane (MAO) (available from Albemarle Corporation, Baton Rouge, Louisiana). Toluene (2 L) was then added to the reactor while stirring, followed by the addition of 22.0 g of silacyclopentyl (tetra-methyl-
10 cyclopentadienyl) (cyclopentadienyl) zirconium dichloride ("the bridged bulky

ligand metallocene-type catalyst compound”), dissolved in 250 ml of toluene, forming the metallocene solution. The mixture was stirred for 1 hour (“Mixing Time”) at 68°C (“Mixing Temperature”). Davison 948 silica (Davison 948 is available from W.R. Grace, Davison Division, Baltimore, Maryland) was
5 dehydrated at 600°C and used as a support. The Davison 948 silica (1000 g) was added slowly to the MAO/metallocene solution, allowing time for good mixing and distribution of the solids into the liquid. After all of the silica was added, the slurry was mixed for an additional 20 minutes at 49°C. A 10% toluene solution of Kemamine AS-990 (available from Witco Corporation, Memphis, Tennessee)
10 (30.2 g) was finally added to the reactor and the mixture stirred for 30 min. after which the catalyst was dried at 49 °C to a free flowing solid.

Example 2

Under anaerobic conditions, into a 125 ml glass vial containing a magnetic stir bar were added 20 cm³ of toluene and 2.25 g (0.039 moles) of
15 methylaluminoxane (MAO) (available from Albemarle Corporation, Baton Rouge, Louisiana) as a 30 wt% solution in toluene. While stirring 0.11 g of silacyclopentyl (tetra-methyl-cyclopentadienyl) (cyclopentadienyl) zirconium dichloride and 2 cm³ of toluene were added to the vial. The mixture was stirred for 20 min. at 25°C after which 5 grams of Davison 948 silica (dehydrated at
20 600°C) (available from W.R. Grace, Davison Division, Baltimore, Maryland) was added and stirring continued for 15 more minutes. Kemamine AS-990 (0.15 grams) (available from Witco Corporation, Memphis, Tennessee) in 2 ml of toluene was finally added and mixed for 10 min. at room temperature. Finally the mixture was dried at 75°C to a free flowing solid.

Example 3

As in Example 2 with the exception that Crosfield ES-70 grade silica (available from Crosfield Limited, Warrington, England) was used instead of Davison 948 silica.

Example 4

30 Under anaerobic conditions, into a 125 ml Serum vial with a stir bar, were added 20 ml of toluene and 2.25 g (0.039 moles) of MAO (available from Albemarle Corporation, Baton Rouge, Louisiana) as a 30 wt% toluene solution. While stirring 0.11 g of the same bridged bulky ligand metallocene-type catalyst compound used in Example 2 was added to the MAO solution and the mixture
35 heated in an oil bath, equilibrated at 65°C, for 1 hour. Silica (600°C), 5.0 g, of

- Crosfield ES-70 grade (available from Crosfield Limited, Warrington, England), was poured into the solution while the temperature was at 65°C. The slurry was allowed to react for 60 minutes at 65°C after which the catalyst was dried to a free flowing solid. To the free flowing solid 3 weight percent of Witco Aluminum
- 5 Stearate #22 (AlSt #22) $(\text{CH}_3(\text{CH}_2)_{16}\text{COO})_2\text{Al-OH}$ available from Witco Corporation, Memphis, Tennessee, was dried under vacuum at 85°C and was added to the flask and the contents tumbled/mixed for 20 minutes at room temperature.

Example 5

In this example the same catalyst was prepared as described in Example 4 with the exception that the MAO/metallocene solution and the silica reaction temperatures were 75°C and the catalyst was dried at 75°C instead of 65°C.

Example 6

In this example the catalyst was prepared as described in Example 4 with the exception that the MAO/metallocene solution and the silica reaction temperatures were 85°C, the MAO/ metallocene was reacted for 15 min. and the catalyst was dried at 75°C instead of 65°C.

Example 7

As in Example 6 except that reaction temperatures were 100°C and drying temperature was 75°C.

Example 8

As in Example 7 except that reaction temperatures were 120°C and drying temperature was 75°C.

Polymerization for Examples 1 to 8

A 2 liter autoclave reactor under a nitrogen purge was charged with 0.16 mmoles triethylaluminum (TEAL), followed by 40 cc of hexene-1 comonomer and 800 cc of isobutane diluent. The contents of the reactor were heated to 80°C, after which, 100 mg of each of the supported polymerization catalysts prepared above in Example 1 to 8, were each separately polymerized as follows: Each polymerization catalyst was introduced concurrently with ethylene into the reactor to make up a total reactor pressure of 325 psig (2240 kPa). The reactor temperature was maintained at 85°C and the polymerization was allowed to proceed for 40 min. After 40 minutes the reactor was cooled, ethylene was vented off and the polymer dried and weighed to obtain the polymer yield. Table 1 below provides the yield data, as well as the fouling characteristics observed, and other physical properties of the polymers.

TABLE 1A

Example	Mixing Temperature (°C)	Mixing Time (minutes)	Fouling Index	Yield (g)	Activity
1	68	60	0	53	795
2	25	20	1.0	58	870
3	25	20	2.0	64	960

TABLE 1B

5

Example ¹	Mixing Temperature (°C)	Mixing Time (minutes)	Yield ² (g)	Fouling Index	I ₂ (dg/min)	I ₂₁ /I ₂
4	65	60	115	2	0.60	56
5	75	60	175	1.0	0.44	62
6	85	15	192	0.5	0.16	106
7	100	15	215	0.5	0.33	76
8	115	15	163	0.5	0.45	66

(1) All catalysts prepared on ES-70 silicas dried at 75° C, and blended with 3% MPS-1

(2) Isobutane slurry polymerization conditions using 40 ml hexene-1 as comonomer.

10 These examples show that by heating the MAO/ metallocene between 75°C to 100°C both activity and fouling characteristics of the catalyst are improved.

Example 9

15 Into a 125 ml glass vial was added 15 ml of dried and sparged toluene followed by the addition of 6.2 g of a 30 wt% MAO solution (available from Albemarle Corporation, Baton Rouge, Louisiana) in toluene equivalent to 0.032 moles of Al. While stirring, 0.123 grams of dimethylsilyl-bis (tetrahydroindenyl) zirconium dichloride was added to the vial and the mixture brought to 85°C at which temperature it was stirred for 15 minutes. Silica Crosfield ES-70 (available from Crosfield Limited, Warrington, England) dehydrated at 600°C was then
20 added to the vial and the slurry mixed for an additional 15 min. at 85°C under a nitrogen purge.

Comparative Example 10 (CEX 10)

Into a 125ml glass vial was added 15 ml of dried and sparged toluene followed by the addition of 6.2 g of a 30 wt% MAO solution (available from Albemarle Corporation, Baton Rouge, Louisiana) in toluene equivalent to 0.032 moles of Al. While stirring, 0.123 g of dimethylsilyl-bis (tetrahydroindenyl) zirconium dichloride was added to the vial and the mixture was allowed to stir for 15 min. at room temperature. Silica Crosfield ES-70 (available from Crosfield Limited, Warrington, England) dehydrated at 600°C was then added to the vial and the slurry mixed for an additional 15 min. at room temperature. The catalyst was then dried to a free flowing solid at 75°C ("Drying Temperature").

The polymerizations for Example 9 and Comparative Example 10 were the same as described above.

TABLE 2

Example	Mixing Temperature (°C)	Mixing Time (minutes)	Drying Temperature (°C)	Yield (g)	Activity
9	85	15	85	175	2625
CEX 10	25	15	75	122	1830

Comparative Example 10 is a control preparation showing normal activity. The method of the invention utilized in Example 9 exhibited 43% higher activity.

Example 11

Into a 10 gallon (44 L) reactor was added 4988 g (25.8 moles MAO) of a 30 wt% solution of MAO (available from Albemarle Corporation, Baton Rouge, Louisiana). Dried and sparged toluene (9.0 L) was then added followed by a solution of 93.2 g of dimethylsilylbis (tetrahydroindenyl) zirconium dichloride in 1 L of toluene. The reaction mixture was heated to 85°C and kept at this temperature for 1 hour while stirring. Crosfield ES-70 silica dehydrated at 600°C (available from Crosfield Limited, Warrington, England) was used as a support. The silica 4.0 kg was added slowly to the MAO/metallocene solution, allowing time for good mixing and complete distribution of the solids into the liquid. After all of the silica was added, the slurry was mixed for an additional 60 minutes at 85°C. The catalyst was then dried to a free flowing solid at 85°C under vacuum.

Example 12

Into a 10 gallon (44 L) reactor was added 3991 g (20.6 moles) of a 30 wt% solution of MAO (available from Albemarle Corporation, Baton Rouge, Louisiana). Dried and

5 sparged toluene (10.0 L) was then added, followed by a solution of 74.6 g of dimethylsilyl

bis (tetrahydroindenyl) zirconium dichloride in 1 L of toluene. The reaction mixture was

heated to 85°C and kept at this temperature for 1 hour while stirring.

10 **Example 13**

The catalyst in this example was prepared as in Example 11 with the exception that in this example 4489 g (23.2 moles MAO) of a 30 wt% MAO solution (available from Albemarle Corporation, Baton Rouge, Louisiana), 9.5 L of toluene and 65.2 g of dimethylsilyl bis-(tetrahydroindenyl) zirconium

15 dichloride was used.

Comparative Example 14 (CEX 14)

This catalyst was prepared as in Example 11 with the exception that the MAO/metallocene reaction temperature was kept at 25°C and drying was conducted at 68°C.

20 The polymerizations for the supported catalyst systems of Examples 11 to 13 and Comparative Example 14 were as described above.

TABLE 3

25

Example	Mixing Temperature (°C)	Mixing Time (Min)	MAO (wt%)	Metallocene (wt%)	Activity
11	85	60	100	100	2855
12	85	60	80	80	2700
13	85	60	90	70	2500
CEX 14	25	60	100	100	1800

Examples 11,12 and 13 illustrate that metal loadings on the catalyst can be reduced using the method of the invention, thus, providing a substantial cost advantage. Even more importantly, the activity is retained relative to room

30 temperature catalyst of Comparative Example 14.

Example 15

In a 125 ml glass vial equipped with a stirring bar and under anaerobic conditions was added 20 ml of toluene, 6.64 ml of a 30 wt% methylaluminoxane (MAO) solution (2.25 g MAO, 0.039 moles) (available from Albemarle Corporation, Baton Rouge, Louisiana). While stirring, 0.136 g of bis (1-methyl-3-n-butyl cyclopentadienyl) zirconium dichloride dissolved in 2 ml of toluene were added to the glass vial. The mixture was stirred at room temperature (25°C) for 15 minutes, after which 5 g of silica of Davison 948 silica (dehydrated at 600°C) (available from W.R. Grace, Davison Division, Baltimore, Maryland) was added to the solution. The mixture was then stirred for 15 minutes after which it was dried at 75°C until the solid was free flowing.

Example 16

The catalyst was prepared as in Example 15 with the exception that the pre-mix solution reaction and the silica/pre-mix reaction were conducted at 100°C for 15 minutes instead of at room temperature. All other conditions were the same as in Example 15.

The supported catalyst systems prepared in Example 15 and 16 were then used in the polymerization process described above for Examples 1 to 14 except that 20 ml of hexene-1 was used.

TABLE 5

Example	Mixing Temperature (°C)	Mixing Time (Min)	Silica Reaction Temperature (°C)	Yield (grams)	Fouling Index
15	25	15	25	199	0
16	100	15	100	157	0

Examples 15 and 16 illustrate that this specific unbridged metallocene catalyst while does not show any fouling, the overall yield is lower where the silica was heated to a higher temperature. While not wishing to be bound to any theory it is

suspected that one contributing factor is the solubility difference between the catalyst compounds used in Example 15 versus Example 1 and Example 11.

While the present invention has been described and illustrated by reference to particular embodiments, those of ordinary skill in the art will appreciate that the invention lends itself to variations not necessarily illustrated herein. For example,
5 it is contemplated that two or more supported catalyst compositions of the invention can be used. Also, that two or more bulky ligand metallocene-type catalyst compounds having different solubilities can be supported using the method of the invention. For this reason, then, reference should be made solely to
10 the appended claims for purposes of determining the true scope of the present invention.

CLAIMS:

1. A method for preparing a supported catalyst system comprising the steps of:
 - (a) heating a composition comprising a bulky ligand metallocene-type catalyst compound and an activator to a temperature of from 75°C to 100°C; and
 - (b) combining the heated composition of step (a) with a carrier.
2. A method for making a supported catalyst system comprising the steps of:
 - (a) forming a reaction product comprising a bulky ligand metallocene-type catalyst compound and an activator, the activator being an alumoxane or a non-coordinating activator;
 - (b) heating the reaction product to a temperature in the range from 65°C to 100°C;
 - (c) optionally heating a carrier; and
 - (d) combining the heated reaction product with a carrier or optionally the heated carrier.
3. The method of claim 1 wherein the activator is alumoxane.
4. The method of claim 2 wherein the activator is alumoxane.
5. The method of any one of claims 1 to 4 wherein the bulky ligand metallocene-type catalyst compound has a solubility less than 20 weight percent of the bulky ligand metallocene-type catalyst compound in toluene at 25°C.
6. A method for making a supported catalyst system comprising the steps of:
 - (a) heating an activated bulky ligand metallocene-type catalyst to a temperature of between 75°C and 100°C;
 - (b) heating a carrier; and
 - (c) combining the heated carrier and the heated activated bulky ligand metallocene-type catalyst.

7. A method for preparing a supported catalyst system comprising the steps of:
 - (a) heating a composition comprising a bulky ligand metallocene-type catalyst compound and an activator, the activator being an alumoxane or a non-coordinating activator at a first temperature of from 65°C to 100°C;
 - (b) heating a carrier at a second temperature; and
 - (c) combining (a) and (b) at a third temperature.
8. The method of claim 7 wherein the first, second and third temperatures are the same, or wherein the first and second temperatures are the same, or wherein the first temperature is in the range of 75°C to 100°C.
9. A use in the polymerization of olefin(s) of the supported catalyst system prepared according to the method as defined in claim 1, claim 6 or claim 7.
10. A process for polymerizing olefin(s) in the presence of a supported catalyst system, the supported catalyst system made by (a) heating a solution comprising at least one bulky ligand metallocene-type catalyst compound and an activator at a temperature in the range of from 75°C to 100°C; (b) introducing a carrier to the solution to form a mixture; (c) drying the mixture to form the supported catalyst system; and (d) polymerizing olefin(s) in the presence of the supported catalyst system.
11. A process for polymerizing olefin(s) in the presence of a supported catalyst system, the supported catalyst system made by (a) heating a reaction product comprising a bulky ligand metallocene-type catalyst compound and an activator, the activator being an alumoxane or a non-coordinating activator to a temperature of 65°C to 100°C; (b) combining the reaction product with a carrier, optionally the carrier is heated; and (c) polymerizing olefins in the presence of the supported catalyst system.
12. The process of claim 10 or 11 wherein the process is a continuous gas phase process.

13. A method for preparing a supported catalyst system comprising:
 - (a) heating a composition comprising a metallocene catalyst compound to a temperature of from 75°C to 125°C; and
 - (b) combining the heated composition with a carrier.
14. The method of claim 13 wherein the carrier is heated.
15. The method of claim 13 or 14 wherein in step (a) the composition is heated to a temperature in the range of from 75°C to 100°C.
16. The method of claim 14 wherein the carrier is heated to a temperature in the range of from 26°C to 150°C.
17. The method of any one of claims 1 to 8 and 13 to 16 wherein the metallocene catalyst compound has a solubility less than 20 weight percent of metallocene catalyst compound in toluene at 25°C.
18. A method for making a supported catalyst system comprising:
 - (a) forming a reaction product comprising a metallocene catalyst compound and an activator;
 - (b) heating the reaction product to a temperature of from 65°C to 125°C;
 - (c) introducing a carrier; and
 - (d) combining the heated reaction product with the carrier.
19. A method according to claim 18, wherein the carrier is heated.
20. The method of claim 18 or 19 wherein the reaction product is heated to a temperature in the range from 75°C to 100°C.
21. A method for making a supported catalyst system comprising:

- (a) heating an activated metallocene catalyst product to a temperature of from 65°C to 125°C;
 - (b) heating a carrier; and
 - (c) combining the heated carrier and the heated activated metallocene catalyst.
22. The method of claim 21 wherein the activated metallocene catalyst is heated to a temperature of from 75°C to 100°C.
23. A method for preparing a supported catalyst system comprising:
- (a) heating a composition comprising a metallocene catalyst compound to a first temperature, wherein the first temperature is in the range of from 65°C to 110°C;
 - (b) heating a carrier at a second temperature; and
 - (c) combining said metallocene catalyst, and said carrier, at a third temperature.
24. The method of claim 23 wherein the first, second and third temperatures are the same.
25. The method of claim 23 wherein the first and second temperatures are the same.
26. A method for preparing a supported catalyst composition comprising:
- (a) combining a metallocene catalyst compound and an activator at a temperature in the range of from 65°C to 125°C; and
 - (b) introducing a carrier.
27. The method of claim 26 wherein the supported catalyst composition is dried or substantially dried to a free flowing powder composition.
28. The method of claim 27 wherein the free flowing composition is reslurried in a liquid.

29. The method of claim 28 wherein the liquid is mineral oil.
30. The method of any one of claims 26 to 29 wherein the metallocene catalyst compound and activator are combined at a temperature of from 65°C to 110°C.
31. The method of any one of claims 26 to 30 wherein the metallocene catalyst compound and activator are combined at a temperature of from 65°C to 100°C.
32. The method of any one of claims 26 to 31 wherein the metallocene catalyst compound and activator are combined at a temperature of from 75°C to 100°C.
33. The process of any one of claims 9 to 12 wherein the metallocene catalyst compound has a solubility less than 20 weight percent of metallocene catalyst compound in toluene at 25°C.