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(54) Titre : AGENTS D'INVERSION NON IONIQUES POUR LATEX EAU-DANS-HUILE ET PROCEDES D'UTILISATION
(54) Title: NONIONIC INVERSION AGENTS FOR WATER-IN-OIL LATICES AND METHODS OF USE

(57) **Abrégé/Abstract:**

Water-in-oil latices of water soluble or dispersible polymers and methods of using the same are presented. The latices include nonionic inversion agents that provide rapid and complete inversion of the latices under conditions wherein the water source used to invert the latex is provided at high temperature, or includes a high level of total dissolved solids, or is both high temperature and high total dissolved solids.

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(54) Title: NONIONIC INVERSION AGENTS FOR WATER-IN-OIL LATICES AND METHODS OF USE

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**NONIONIC INVERSION AGENTS FOR WATER-IN-OIL LATICES AND
METHODS OF USE**

CROSS-REFERENCE TO RELATED APPLICATION

This application claims priority to U.S. Patent Application Serial No. 62/202,197
5 filed on August 7, 2015, the disclosure of which is incorporated herein by reference in its
entirety.

TECHNICAL FIELD

The invention relates to water-in-oil latices of water dispersible polymers and
compositions that provide for rapid inversion of the latices when diluted.

10 **BACKGROUND**

Crude oil development and production can include up to three distinct phases:
primary, secondary, and tertiary (or enhanced) recovery. During primary recovery, the
natural pressure of the reservoir or gravity drives oil into the wellbore, combined with
artificial lift techniques (such as pumps) which bring the oil to the surface. But only about
15 10 percent of a reservoir's original oil in place is typically produced during primary
recovery. Secondary recovery techniques extend a field's productive life generally by
injecting water or gas to displace oil and drive it to a production wellbore, resulting in the
recovery of 20 to 40 percent of the original oil in place.

Enhanced oil recovery, or EOR, is a generic term encompassing techniques for
20 increasing the amount of crude oil that can be extracted from a subterranean formation
such as an oil field. EOR techniques offer prospects for ultimately producing 30 to 60
percent, or more, of the reservoir's original oil in place. Three major categories of EOR
have been found to be commercially successful to varying degrees:

Thermal recovery is the introduction of heat such as the injection of steam to lower
25 the viscosity of the oil and improve its ability to flow through the reservoir.

Gas injection is the injection of gases such as natural gas, nitrogen, or carbon
dioxide that expand in a reservoir to push additional oil to a production wellbore, or gases
that dissolve in the oil to lower its viscosity and improve flow rate.

Chemical injection is the injection of polymer dispersions to increase the effectiveness of waterfloods, or the use of detergent-like surfactants to help lower the surface tension that often prevents oil droplets from moving through a reservoir. Chemical injection of a polymer is also referred to as polymer flooding. This method improves the vertical and areal sweep efficiency as a consequence of improving the water/oil mobility ratio. In addition, the polymer reduces the contrasts in permeability by preferentially plugging the high permeability zones flooded. This forces the water to flood the lower permeability zones and increases the sweep efficiency. The art in this area is well-developed for conventional oil recovery applications.

Of these techniques, polymer flooding using water-in-oil (w/o) latex products is particularly favored for use in offshore reservoirs and other relatively isolated operations due to the ease of use and relatively simple equipment requirements. Polymer flooding is generally accomplished by dissolving the selected polymer in water and injecting the polymer solution into the reservoir. However, since the target concentration of polymer in the polymer dispersions is typically about 1 wt% or less, transport at the target concentration is not economically efficient. Transporting the dried polymers, while economically efficient for the supplier, is not favorable for field use due to limited space for dry polymer make-down equipment and difficulties in fully hydrating the polymers in the field. To address these issues, various formulations have been developed to allow economically feasible transportation and storage. Specialized methods have also been developed to convert the formulations to use concentrations of fully hydrated polymers in the field.

Organic polymers traditionally used in EOR include water soluble polymers such as polyacrylamide homopolymers and copolymers with acrylic acid or conjugate base thereof and/or one or more other water soluble monomers, and hydrophobically modified water soluble polymers, also called associative polymers or associative thickeners. Associative thickeners are typically copolymers of acrylamide, acrylic acid, or both with about 1 mole% or less of a hydrophobic monomer such as a C₈ - C₁₆ linear or branched ester of acrylic acid. Any of these water soluble polymers are deliverable as a dry powder, as a gel-like concentrate in water, or in the water phase of a w/o latex. Of these formats, water-in-oil latices have the advantage of being deliverable in a liquid format that is easily handled in the field because the latex viscosity is lower than that of a water solution of

comparable wt% polymer. The liquid products are also easy to make down with little equipment and a small space footprint compared to that of dry polymer products.

Commercial w/o latices are formulated for EOR by dissolving monomer(s) in a high-solids aqueous solution to form a water phase (or monomer phase), mixing one or more hydrocarbon solvents and a surfactant or a blend thereof having a hydrophilic-lipophilic balance (HLB) of about 2 to 10 to form an oil phase, mixing the two phases using techniques to result in a water-in-oil emulsion or latex, and polymerizing the monomer via a standard free-radical initiation. The w/o latex may be a macroemulsion, nanoemulsion, microemulsion, or combination thereof. The free radical initiation may be radiation, photo, thermal, or redox initiation, or any combination thereof. After polymerization is complete, a higher HLB surfactant (HLB > 10) or a blend thereof having an HLB > 10 is often added to facilitate latex inversion when water is added. “*Inversion*” is a term of art to describe the dilution of w/o latices with a water source, causing destabilization of the latex and subsequent dissolution of the concentrated polymer particles. In some cases, the higher HLB surfactant is added in the field, immediately prior to addition of water to dilute the latex; or is added in-line with the water source used to dilute the latex. In other cases, the higher HLB surfactant is added directly to the w/o latex after polymerization is complete, and the latex is stable or even shelf stable. In such cases, careful control of type and amount of surfactant is required to provide a sufficiently stable latex to facilitate storage and transportation, while providing for improved inversion performance in the field.

Recently, there has arisen the need to address polymer flooding in challenging conditions encountered in reservoirs wherein the ambient or produced water contacted by the polymer includes high total dissolved solids, such as a high saline or hardness content, in some cases involving total dissolved solids of up to about 30 wt%. In some cases the ambient or produced water is tap water, hard water, brackish water, municipal waste water, produced water, or seawater. Field operators strongly prefer to use such water sources to dilute polymer flooding formulations to final use concentrations rather than employ purified water sources. Reasons for the preference include reducing costs by diverting some or all of the water source already being injected into a reservoir to dilute the polymer flooding formulations and reducing the environmental impact associated with employing a purified water source. However, use of such water sources leads to

difficulties in dispersing the high molecular weight polymers to use concentrations. Inversion of w/o latices in such water sources can result in slow inversion times and/or the requirement of multistage dilution and mixing procedures; it can also result in coagulation, precipitation, or gross phase separation of polymer upon or after contact of the latex with
5 the diluted water environment. Thus there is a need to address inversion of w/o latices in field conditions where the use water source has high total dissolved solids.

Another need in the industry is to address reservoirs where the water source contacted by a w/o latex is at an extreme temperature, such as 30 °C to 100 °C or -10 °C to 10 °C. Extreme temperature water sources lead to difficulties in dispersing high molecular
10 weight, water soluble polymers delivered in w/o latices, similarly to the difficulties encountered in the use of high total dissolved solids water sources. In some cases, conditions of both extreme temperature and high total dissolved solids are encountered in the ambient or produced water source employed to dilute polymer flooding formulations to use concentrations. Such conditions cause instability of w/o latices during inversion,
15 evidenced by formation of gel particles, coagulum, polymer coated out on contact surfaces, and gross coalescence of phases (conventionally referred to as “separation”) and the like. The products of this instability cause plugged equipment in the field, reduced reservoir permeability, plugged formation, and ultimately failure to accomplish mobility control within the reservoir. These problems remain largely unaddressed by conventional
20 formulations, methods, and equipment developed for inversion of w/o latices in the field. For example, formulations described in US Patent Application Publication No. 2014/0051620 A1, which comprise an inversion agent such as glycerol, do not provide satisfactory performance under conditions using water sources having high total dissolved solids, extreme temperature, or both.

25 As a result, there is a substantial need in the industry to develop technologies suitable for carrying out enhanced oil recovery in reservoirs where high temperature water sources, high total dissolved solids water sources, or both are used in conjunction with EOR. There is a substantial need in the industry for w/o polymer latices that invert rapidly to form stable, fully hydrated or dissolved polymer solutions at water temperatures of 30
30 °C to 100 °C. There is a substantial need in the industry for w/o polymer latices that invert rapidly to form stable, fully hydrated or dissolved polymer solutions using water sources having up to 30 wt% total dissolved solids. There is a substantial need in the

industry for w/o polymer latices that invert rapidly to form stable, fully hydrated or dissolved polymer solutions at polymer concentrations of 1 wt% or less using water sources having high total dissolved solids, high temperature, or both.

SUMMARY

5 Described herein are water-in-oil (w/o) latices. The latices are formed by combining about 0.1 wt% to 20.0 wt% of a nonionic inversion agent with about 15 wt% to 70 wt% of a water soluble or dispersible polymer comprising 1 mol % to about 100 mol % acrylamide monomers; and about 0.1 wt% to 20.0 wt% of an inversion surfactant having a hydrophilic/lipophilic balance of 10 or greater. In some embodiments, the w/o latex
10 comprises about 0.1 wt% to 5.0 wt% of a nonionic inversion agent; about 15 wt% to 70 wt% of the water soluble polymer; about 0.1 wt% to 20.0 wt% of the inversion surfactant; about 3 wt% to 50 wt% water; about 10 wt% to 40 wt% of a compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C and is substantially a liquid over the range of 20 °C to 90 °C and comprising linear, branched, or cyclic hydrocarbon moieties;
15 and about 20 wt% or less of a latex surfactant characterized as having a hydrophilic/lipophilic balance of between 2 and 10.

Also described herein is a method of forming an invertible latex, the method comprising a) forming a water-in-oil latex comprising about 15 wt% to 70 wt% of a water soluble or dispersible polymer; about 3 wt% to 50 wt% water; about 10 wt% to 40 wt% of
20 a compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C and is substantially a liquid over the range of 20 °C to 90 °C and comprising linear, branched, or cyclic hydrocarbon moieties; and about 20 wt% or less of a latex surfactant characterized as having a hydrophilic/lipophilic balance of between 2 and 10; and b) adding to the latex about 0.1 wt% to 20.0 wt% of an inversion surfactant characterized as having a
25 hydrophilic/lipophilic balance of 10 or greater and about 0.1 wt% to 5.0 wt% of a nonionic inversion agent to form an invertible latex.

Also described herein is a method of recovering hydrocarbon compounds from a subterranean reservoir, the method comprising a) forming an invertible latex comprising about 15 wt% to 70 wt% of a water soluble or dispersible polymer, about 3 wt% to 50
30 wt% water, about 10 wt% to 40 wt% of a compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C and is substantially a liquid over the range of 20 °C to 90 °C

and comprising linear, branched, or cyclic hydrocarbon moieties, and about 20 wt% or less of a latex surfactant characterized as having a hydrophilic/lipophilic balance of between 2 and 10; and adding to the latex about 0.1 wt% to 20.0 wt% of an inversion surfactant characterized as having a hydrophilic/lipophilic balance of 10 or greater and about 0.1 wt% to 5.0 wt% of a nonionic functional inversion agent; b) adding a water source to the invertible latex in a single addition to form a polymer flooding solution comprising about 100 ppm to 10,000 ppm of the water soluble or dispersible polymer; c) injecting the polymer flooding solution into the subterranean reservoir; and d) recovering the hydrocarbon compounds.

Additional advantages and novel features of the invention will be set forth in part in the description that follows, and in part will become apparent to those skilled in the art upon examination of the following, or may be learned through routine experimentation upon practice of the invention.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 is a line graph of torque monitor data at 60 °C showing the invertibility of w/o latices comprising 3 wt% of a nonionic inversion agent and 3.3% of TDA-12 as an inverting surfactant ([polymer] = 10000 ppm in 3.5 % SSW).

Figure 2 is a line graph of torque monitor data at 60 °C showing the invertibility of w/o latices comprising 3 wt% of a nonionic inversion agent and 3.3% of TDA-12 as an inverting surfactant ([polymer] = 10000 ppm in 3.5 % SSW).

Figure 3 is a line graph of torque monitor data at room temperature showing the invertibility of w/o latices comprising 3 wt% of a nonionic inversion agent and 3.3% of TDA-12 as an inverting surfactant ([polymer] = 10000 ppm in 3.5 % SSW).

Figure 4 is a line graph of torque monitor data at 4° C showing the invertibility of w/o latices comprising 3 wt% of a nonionic inversion agent and 3.3% of TDA-12 as an inverting surfactant ([polymer] = 10000 ppm in 3.5 % SSW).

DETAILED DESCRIPTION

Although the present disclosure provides references to preferred embodiments, persons skilled in the art will recognize that changes may be made in form and detail without departing from the spirit and scope of the invention. Various embodiments will be described in detail with reference to the drawings. Reference to various embodiments does not limit the scope of the claims attached hereto. Additionally, any examples set forth in this specification are not intended to be limiting and merely set forth some of the many possible embodiments for the appended claims.

Definitions

As used herein, the term “*polymer*” means a water soluble or water dispersible polymer. The term “polymer” encompasses and includes homopolymers, copolymers, terpolymers and polymers with more than 3 monomers, crosslinked or partially crosslinked polymers, and combinations or blends of these.

The term “*monomer*” is used in context to mean an ethylenically unsaturated polymerizable compound or the polymerized residue thereof. As used herein, the term “*anionic monomer*” means an unsaturated compound or polymerized residue thereof bearing an acidic group, or a salt thereof. As used herein, the term “*cationic monomer*” means an unsaturated compound or polymerized residue thereof bearing a positive charge, or a salt thereof.

As used herein, the term “*polymer solution*” or “*polymer dispersion*” means a polymer composition substantially dispersed or dissolved in water, a water source, or a water-based solution. The polymer solution is a solution as formed, or in the case of some EOR applications the solution before injection, during injection, or after injection as determined by context. Water-based solutions include one or more dissolved salts, buffers, acids, bases, surfactants, or other dissolved, dispersed, or emulsified compounds, materials, components, or combinations thereof.

As used herein, the term “*water source*” means a source of water comprising, consisting essentially of, or consisting of fresh water, deionized water, distilled water, produced water, municipal water, waste water such as runoff water or municipal waste water, treated or partially treated waste water, well water, brackish water, “gray water”, sea water, or a combination of two or more such water sources as determined by context.

In some embodiments, a water source includes one or more salts, ions, buffers, acids, bases, surfactants, or other dissolved, dispersed, or emulsified compounds, materials, components, or combinations thereof. In some embodiments, a water source includes about 0 wt% to 30 wt% total dissolved solids. Generally and as determined by context, the term “water source” includes high total dissolved solids water sources, high temperature water sources, and water sources that are both high total dissolved solids and high temperature water sources.

As used herein, the term “*high temperature*” means about 30 °C to 100 °C, as specified or determined by context.

As used herein, the term “*high total dissolved solids*” refers to a water source having at least 1 wt% non-polymeric solids dissolved therein, and in embodiments up to about 30 wt% non-polymeric solids dissolved therein. In general, “*saline*” or “*salinity*” refers to a water source wherein a portion, in some embodiments a substantial portion, of the total dissolved solids are salts, as determined by context.

As used herein, the terms “*water-in-oil latex*” or “*w/o latex*” mean a discontinuous internal water phase within a continuous oil phase, wherein the water phase includes at least one monomer or polymer. In general and as determined by context, these terms denote a latex prior to addition of inverting surfactants.

As used herein, the term “*oil*” or “*hydrocarbon solvent*” as applied to an oil phase of a water-in-oil latex, means any compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C, is substantially chemically inert within a w/o latex as described herein, and is a liquid over at least the range of 20 °C to 100 °C.

As used herein, the term “*water phase*” means a water source having at least a monomer or polymer dispersed or dissolved therein, further wherein the dispersion or solution is a discontinuous phase within a w/o latex.

As used herein, the term “*stable*” as applied to a latex or emulsion means a kinetically stable latex or emulsion that absent any force applied, temperature change, or chemical added to a latex, the latex is or is capable of being substantially free of coagulation, plating out, precipitation, gross coalescence of phases (conventionally referred to as “separation”) or any other evidence of instability conventionally associated with water-in-oil latices for at least about 24 hours at about 20 °C. As used herein, the

term “*shelf stable*” means stable for at least 2 months. As used herein, the term “freeze-thaw stable” means stable after at least 1 freeze-thaw cycle.

As used herein, the term “*invertible latex*” means a w/o latex additionally including at least one inversion surfactant and at least one inversion agent, the inversion agent
5 comprising at least one nonionic compound.

As used herein, the term “*invert*” or “*inversion*” as applied to the w/o latices of the invention means to contact an invertible latex with a water source in an amount sufficient to form a polymer flooding solution.

As used herein, the term “*polymer flooding solution*” or “*polymer solution*” means
10 a polymer solution or dispersion of about 100 ppm (0.01 wt%) to 10,000 ppm (1.00 wt%) resulting from the inversion of an invertible latex.

As used herein, the term “*single component*” as applied to the w/o latices of the invention means that at least one inversion surfactant and at least one inversion agent are added to an existing w/o latex and the combination is shelf stable. The term is used in
15 contrast to inversion surfactants or other compounds added in-line during injection and inversion.

As used herein, the term “*optional*” or “*optionally*” means that the subsequently described component, event or circumstance may be, but need not be present or occur. The description therefore discloses and includes instances in which the event or
20 circumstance occurs and instances in which it does not, or instances in which the described component is present and instances in which it is not.

As used herein, the term “*about*” modifying, for example, the quantity of an ingredient in a composition, concentration, volume, temperature, time, yield, flow rate, pressure, and like values, and ranges thereof, employed in describing the embodiments of
25 the disclosure, refers to variation in the numerical quantity that can occur, for example, through typical measuring and handling procedures used for making compounds, compositions, concentrates or use formulations; through inadvertent error in these procedures; through differences in the manufacture, source, or purity of starting materials or ingredients used to carry out the methods, through standard operating machine error,
30 and like proximate considerations. The term “*about*” also encompasses amounts that differ due to aging of a formulation with a particular initial concentration or mixture, and

amounts that differ due to mixing or processing a formulation with a particular initial concentration or mixture. Where modified by the term "about" the claims appended hereto include equivalents according to this definition.

As used herein, the term "*substantially*" means "consisting essentially of", as that term is construed in U.S. patent law, and includes "consisting of" as that term is construed in U.S. patent law. For example, a solution that is "substantially free" of a specified compound or material may be free of that compound or material, or may have a minor amount of that compound or material present, such as through unintended contamination or incomplete purification. A "minor amount" may be a trace, an unmeasurable amount, an amount that does not interfere with a value or property, or some other amount as provided in context. A composition that has "substantially only" a provided list of components may consist of only those components, or have a trace amount of some other component present, or have one or more additional components that do not materially affect the properties of the composition. Additionally, "substantially" modifying, for example, the type or quantity of an ingredient in a composition, a property, a measurable quantity, a method, a value, or a range, employed in describing the embodiments of the disclosure, refers to a variation that does not affect the overall recited composition, property, quantity, method, value, or range thereof in a manner that negates an intended composition, property, quantity, method, value, or range. Where modified by the term "substantially" the claims appended hereto include equivalents according to this definition.

Water-in-oil Latices

We have found inversion agents that provide rapid and complete inversion of water-in-oil (w/o) latices of water soluble polymers under conditions wherein the water source used to invert the latex is provided at high temperature, or includes a high level of total dissolved solids, or is both high temperature and high total dissolved solids. The w/o latices useful in conjunction with the compositions and methods of the invention are conventional latices employed in one or more EOR applications, wherein the inversion agents are added to the w/o latices to facilitate inversion to yield a polymer solution for EOR. Polymer solutions for EOR conventionally target a concentration of about 1.00 wt% or less. The compositions and methods of the invention are easily carried out using conventional materials and equipment familiar to one of skill in w/o latex formation for EOR.

Polymers useful in the w/o latices include conventional EOR polymers as well as variations, mixtures, or derivatives thereof. The invention is not particularly limited as to the polymer employed in the water phase of the w/o latices, however, in embodiments the polymer is water soluble or fully dispersible to result in increased viscosity suitable for one or more EOR applications at concentrations of 1 wt% or less. Thus, polyacrylamides, polyacrylates, copolymers thereof, and hydrophobically modified derivatives of these (associative thickeners) are the most commonly employed EOR polymers; all are usefully employed in the w/o latices. Associative thickeners typically include about 1 wt% or less, based on total weight of dry polymer, of a monomer having a long-chain hydrocarbon functionality intended to produce physical or associative crosslinking in a water-based polymer dispersion. Such hydrophobically associating moieties are well known in the industry. In some embodiments, the hydrocarbyl functionality includes 8 to 20 carbons, or 10 to 20 carbons, or 12 to 20 carbons arranged in a linear, branched, or cyclic conformation. In some embodiments, the hydrophobically associating monomers are present in the polymer compositions at about 1 wt% or less of the total weight of the polymer composition, for example about 0.01 wt% to 1.00 wt%, or about 0.1 wt% to 1.00 wt%, or about 0.20 wt% to 1.00 wt% of the total weight of the polymer composition.

Other monomers usefully incorporated into the polymers and copolymers with acrylamide, acrylic acid, or both include cationic monomers, anionic monomers, and nonionic monomers. Nonlimiting examples of cationic monomers include N,N-diallyl-N,N-dimethylammonium chloride (DADMAC), N-alkyl ammonium salts of 2-methyl-1-vinyl imidazole, N-alkyl ammonium salts of 2-vinyl pyridine or 4-vinyl pyridine, N-vinyl pyridine, and trialkylammonium alkyl esters and amides derived from acrylic acid or acrylamide, respectively. Nonlimiting examples of anionic monomers include methacrylic acid, 2-acrylamido-2-methylpropane sulfonic acid (AMS), vinylphosphonic acid, and vinyl sulfonic acid and conjugate bases or neutralized forms thereof (salts). Nonlimiting examples of nonionic monomers include methacrylamide and alkyl ester or amide derivatives of acrylic acid or acrylamide, such as N-methyl acrylamide or butyl acrylate.

Polymers employed for EOR are desirably high molecular weight, as conventionally employed in EOR applications. Higher molecular weight increases the efficacy of the polymers in viscosifying water. However, higher molecular weight also increases difficulty in dissolution due to the high level of chain entanglement between

polymer strands as well as strong hydrogen bonding between polymer functionalities such as amides and carboxylates. In embodiments, the polymers usefully incorporated in the w/o latices have a weight average molecular weight (M_w) of about 5×10^5 to 1×10^8 g/mol, or about 1×10^6 to 5×10^7 g/mol, or about 5×10^6 to 2×10^7 g/mol.

5 In embodiments, any polymer(s) useful in the w/o latices disclosed herein includes a cross-linking monomer or polymer. The crosslinker may be labile, non-labile, or a combination thereof. The labile crosslinker may be a glyoxal cross-linking monomer as described in U.S. Patent Application Publication No. 2014/0209304, which is incorporated by reference herein in its entirety. The non-labile crosslinker may be methylene
10 bis(acrylamide) as described in U.S. Patent No. 7,300,973, which is incorporated by reference herein in its entirety. In embodiments, the polymer comprises about 1 mol % to about 100 mol % acrylamide monomers, or about 1 mol % to about 90 mol %, or about 1 mol % to about 80 mol %, or about 1 mol % to about 70 mol %, or about 1 mol % to about 60 mol %, or about 1 mol % to about 50 mol %, or about 1 mol % to about 40 mol %, or
15 about 1 mol % to about 30 mol %, or about 1 mol % to about 20 mol %, or about 1 mol % to about 10 mol %, or about 10 mol % to about 100 mol %, or about 20 mol % to about 100 mol %, or about 30 mol % to about 100 mol %, or about 40 mol % to about 100 mol %, or about 50 mol % to about 100 mol %, or about 60 mol % to about 100 mol %, or about 70 mol % to about 100 mol %, or about 80 mol % to about 100 mol %, or about 90
20 mol % to about 100 mol %, or about 20 mol % to about 80 mol %, or about 30 mol % to about 70 mol %, or about 40 mol % to about 60 mol %, or about 60 mol % to about 80 mol % acrylamide monomers.

In embodiments, the polymer comprises about 0.1 ppm to about 20000 ppm labile or non-labile cross-linked monomer units based on the weight of the polymer, or about 0.1
25 ppm to about 10000 ppm, or about 0.1 ppm to about 5000 ppm, or about 0.1 ppm to about 1000 ppm, or about 0.1 ppm to about 100 ppm, or about 1 ppm to about 20000 ppm, or about 10 ppm to about 20000 ppm, or about 100 ppm to about 20000 ppm, or about 1000 ppm to about 20000 ppm, or about 5000 ppm to about 20000 ppm, or about 10000 ppm to about 20000 ppm, or about 100 ppm to about 10000 ppm, or about 1000 ppm to about
30 5000 ppm cross-linked monomer units based on the weight of the polymer. In embodiments, the cross-linking monomer is glyoxal bis(acrylamide).

In embodiments, the polymer including the cross-linking monomer comprises about 100 ppm to about 10000 ppm of a w/o latex, or about 100 ppm to about 5000 ppm, or about 100 ppm to about 1000 ppm, or about 100 ppm to about 500 ppm, or about 500 ppm to about 10000 ppm, or about 1000 ppm to about 10000 ppm, or about 5000 ppm to about 10000 ppm, or about 500 ppm to about 5000 ppm, or about 100 ppm to about 1000 ppm, of a w/o latex.

In embodiments, one or more polymers are present substantially within the water phase in an w/o latex. In embodiments, the polymers are present within the w/o latices at about 15 wt% to 70 wt% based on the total weight of the latex, or about 17 wt% to 70 wt%, or about 19 wt% to 70 wt%, or about 21 wt% to 70 wt%, or about 23 wt% to 70 wt%, or about 25 wt% to 70 wt%, or about 15 wt% to 68 wt%, or about 15 wt% to 66 wt%, or about 15 wt% to 64 wt%, or about 15 wt% to 62 wt%, or about 15 wt% to 60 wt%, or about 15 wt% to 58 wt%, or about 15 wt% to 56 wt%, or about 25 wt% to 65 wt%, or about 30 wt% to 60 wt%, or about 30 wt% to 60 wt% based on the total weight of the latex.

The polymers present within the water phase of a w/o latex are often, though not exclusively, formed in situ by dissolving one or more monomers in the water phase, then adding a water phase into an oil phase bearing a surfactant to form the emulsion, followed by polymerization of the monomers to form a polymer w/o latex. Such latices are used for EOR applications.

Also present in the w/o latex is an amount of water sufficient to form a water phase within the latex. Water is present in the w/o latex at about 3 wt% to 50 wt% based on the total weight of the latex, or about 5 wt% to 50 wt%, or about 10 wt% to 50 wt%, or about 15 wt% to 50 wt%, or about 20 wt% to 50 wt%, or about 25 wt% to 50 wt%, or about 3 wt% to 45 wt%, or about 3 wt% to 40 wt%, or about 3 wt% to 35 wt%, or about 3 wt% to 30 wt%, or about 3 wt% to 25 wt%, or about 5 wt% to 45 wt%, or about 5 wt% to 40 wt%, or about 5 wt% to 35 wt%, or about 5 wt% to 30 wt%, or about 5 wt% to 25 wt% based on the total weight of the w/o latex. In some embodiments, the water is a water source.

Also present in the w/o latex is an amount of oil sufficient to form an oil phase within the latex. In some embodiments, the oil is not flammable at temperatures less than about 90 °C, or less than about 80 °C, or less than about 70 °C. In some embodiments, the oil is a mixture of compounds, wherein the mixture is less than 0.1 wt% soluble in water at

25 °C and is substantially a liquid over the range of 20 °C to 90 °C. In some embodiments, the oil comprises, consists essentially of, or consists of one or more linear, branched, or cyclic hydrocarbon moieties, aryl or alkaryl moieties, or combinations of two or more such moieties. In some embodiments, the oil has a density of about 0.8 g/L to 1.0 g/L, for example about 0.8 g/L to 0.9 g/L. Examples of suitable oils include decane, dodecane, isotridecane, cyclohexane, toluene, xylene, and mixed paraffin solvents such as those sold under the trade name ISOPAR® by ExxonMobil Corp. of Irving, TX. In embodiments, the oil is present in the w/o latex at about 10 wt% to 40 wt% based on the total weight of the w/o latex, or about 15 wt% to 40 wt%, or about 20 wt% to 40 wt%, or about 22 wt% to 40 wt%, or about 24 wt% to 40 wt%, or about 26 wt% to 40 wt%, or about 28 wt% to 40 wt%, or about 30 wt% to 40 wt%, or about 10 wt% to 38 wt%, or about 10 wt% to 36 wt%, or about 10 wt% to 34 wt%, or about 10 wt% to 32 wt%, or about 10 wt% to 30 wt%, or about 10 wt% to 25 wt%, or about 10 wt% to 20 wt%, or about 15 wt% to 35 wt%, or about 20 wt% to 30 wt% based on the total weight of the w/o latex.

Also present in the w/o latex is one or more latex surfactants. Latex surfactants are employed to form and stabilize the w/o latices during polymerization and to maintain latex stability until inversion. Generally the latex surfactant is present at about 20 wt% or less based on the weight of the latex. Conventionally employed surfactants for w/o latices used for EOR applications include nonionic ethoxylated fatty acid esters, ethoxylated sorbitan fatty acid esters, sorbitan esters of fatty acids such as sorbitan monolaurate, sorbitan monostearate, and sorbitan monooleate, block copolymers of ethylene oxide and hydroxyacids having a C₁₀ - C₃₀ linear or branched hydrocarbon chain, and blends of two or more of these targeted to achieve a selected hydrophilic/lipophilic balance (HLB). Those of skill will understand that a plethora of surfactants are employed throughout the industry to form and stabilize w/o latices, serving as emulsifiers for polymerization of monomers and further maintaining emulsion stability of the polymer formed therein until subsequent use in the field. Any nonionic surfactants and blends thereof conventionally employed in w/o latices for EOR applications are suitably employed in conjunction with the present invention. In embodiments, the latex surfactant is a single nonionic surfactant or blend thereof having a combined HLB value of about 2 to 10, for example about 3 to 10, or about 4 to 10, or about 5 to 10, or about 6 to 10, or about 7 to 10, or about 8 to 10,

or about 2 to 9, or about 2 to 8, or about 2 to 7, or about 2 to 6, or about 2 to 5, or about 3 to 9, or about 4 to 8.

Representative amounts of the above listed materials are suitably included in one or more w/o latices useful to stabilize one or more EOR applications, wherein the amounts are suitably selected to provide optimal kinetic stability of the emulsion. In some embodiments, amounts of the above listed materials are suitably employed in one or more w/o latices to form a microemulsion or a nanoemulsion, wherein such emulsions are characterized by one or more properties of thermodynamic stability and optical transparency. Representative amounts of these materials are shown below, wherein these amounts are intended to be representative of the w/o latices useful in conjunction with the methods and materials of the invention. Useful w/o latices are not limited to those shown below. A specific example of a w/o latex formulation is provided in Example 2. Where amounts listed below do not add up to 100 wt%, one or more additional components are also present in the latex.

Phase	Material	Amount in a w/o Latex, wt%				
		Latex 1	Latex 2	Latex 3	Latex 4	Latex 5
Oil	Oil (solvent)	25	30	10	20	25
	Latex Surfactant	15	5	3	5	20
Water	Monomer or Polymer	50	25	50	35	40
	Water	5	40	10	3	10

15

The w/o latices optionally include one or more additives. Salts, buffers, acids, bases, dyes, thermal stabilizers, metal chelators, coalescing solvents, and the like are optionally included in the w/o latices. In some embodiments, the additives include one or more corrosion inhibitors, scale inhibitors, emulsifiers, water clarifiers, hydrogen sulfide scavengers, gas hydrate inhibitors, biocides, pH modifiers, antioxidants, asphaltene

20

inhibitors, or paraffin inhibitors. While the amount of an additive usefully employed in the w/o latex depends on the additive and the intended application, in general the amount of any individual additive is about 0 wt% to 5 wt% based on the total weight of the w/o latex, or about 0 wt% to 4 wt%, or about 0 wt% to 3 wt%, or about 0 wt% to 2 wt%, or about 0
5 wt% to 1 wt% based on the total weight of the latex.

In embodiments, the w/o latices are made using conventional equipment and methodology. Thus, in embodiments a w/o latex containing the monomers is formed and the polymerization is conducted within the water phase of the latex. In other embodiments the polymer is formed in a water solution, and the solution is used to form a w/o latex. In
10 such embodiments, the w/o latex is formed after polymerization is complete by adding one or more surfactants and one or more oils to the water-based polymer composition and emulsifying the combined components as described above.

In embodiments, the water in the w/o latex is substantially removed after polymerization to produce a more concentrated latex product by distillation, vacuum
15 drying, spray drying, or a combination thereof. In embodiments, the oil in the w/o latex is substantially removed and recycled after polymerization to produce a more concentrated latex product by distillation, vacuum drying, spray drying, or any combination thereof.

Inversion Surfactants

Inversion of the presently disclosed w/o latices is facilitated by an inversion
20 surfactant. Useful inversion surfactants comprise, consist essentially of, or consist of surfactants or blends thereof having an HLB of about 10 to 40, or about 10 to 35, or about 10 to 30, or about 10 to 25, or about 10 to 20, or about 10 to 15, or about 15 to 40, or about 20 to 40, or about 25 to 40, or about 30 to 40, or about 35 to 40, or about 15 to 35, or about 20 to 30. In some embodiments, the inversion surfactant is nonionic and includes one or
25 more compounds comprising one or more ethoxy groups, propoxy groups, or a combination thereof. In some embodiments, the inversion surfactant is ionic and includes one or more carboxylate, sulfonate, phosphate, phosphonate, phosphonium, or ammonium moieties. In some embodiments, the inversion surfactant includes a linear or branched C₈ - C₂₀ hydrocarbyl moiety. In some such embodiments, the inversion surfactant is an
30 alkoxyated alcohol such as an ethoxyated, propoxyated, or ethoxyated/propoxyated alcohol, wherein the alcohol includes a linear or branched C₈ - C₂₀ hydrocarbyl moiety. In some such embodiments, the inversion surfactant includes about 4 and 40 ethylene oxide

repeat units and 0 to about 10 propylene oxide repeat units. In some embodiments, the inversion surfactant includes a sorbitan moiety. In some embodiments, the inversion surfactant is a block copolymer. In some such embodiments, the block copolymer is linear, branched, or hyperbranched. Examples of suitable inversion surfactants are listed
 5 in *McCutcheon's Emulsifiers & Detergents*, MC Publishing Co., 2015 edition.

The inversion surfactant may be added before, concurrently with, or after addition of an inversion agent, described below, to a w/o latex. In embodiments, in order to facilitate inversion of a w/o latex, the inversion surfactant is added to a latex at about 0.1 wt% to 20 wt% based on the total weight of the w/o latex, or about 0.1 wt% to 15 wt%,
 10 0.1 wt% to 10 wt%, or about 0.1 wt% to 7.5 wt%, 0.1 wt% to 6.0 wt% based on the total weight of the w/o latex, or about 0.5 wt% to 5.5 wt%, or about 1.0 wt% to 5.0 wt%, or about 1.5 wt% to 4.5 wt%, or about 2.0 wt% to 4.0 wt%, or about 2.5 wt% to 3.5 wt%, or about 0.1 wt% to 5.5 wt%, or about 0.1 wt% to 5.0 wt%, or about 0.1 wt% to 4.5 wt%, or about 0.1 wt% to 4.0 wt%, or about 0.1 wt% to 3.5 wt%, or about 0.5 wt% to 6.0 wt%, or
 15 about 1.0 wt% to 6.0 wt%, or about 1.5 wt% to 6.0 wt%, or about 2.0 wt% to 6.0 wt%, or about 2.5 wt% to 6.0 wt%, or about 3.0 wt% to 6.0 wt%, based on the total weight of the w/o latex.

The amount of inversion surfactant may be reduced when an inversion agent (described below) is added to a w/o latex. In embodiments, an inversion agent is added to
 20 a w/o latex and the amount of inversion surfactant is reduced by up to 50% compared to a w/o latex that does not include an inversion agent. In embodiments, the inversion agent is added to a latex at about 0.1 wt% to 10 wt% based on the total weight of the w/o latex, or about 0.1 wt% to 7.5 wt%, 0.1 wt% to 5.0 wt% based on the total weight of the w/o latex, or about 1.5 wt% to 4.5 wt%, or about 2.0 wt% to 4.0 wt%, or about 2.5 wt% to 3.5 wt%,
 25 or about 0.1 wt% to 4.5 wt%, or about 0.1 wt% to 4.0 wt%, or about 0.1 wt% to 3.5 wt%, or about 0.5 wt% to 5.0 wt%, or about 1.0 wt% to 5.0 wt%, or about 1.5 wt% to 5.0 wt%, or about 2.0 wt% to 5.0 wt%, or about 2.5 wt% to 5.0 wt%, or about 3.0 wt% to 5.0 wt%, based on the total weight of the w/o latex.

Inversion Agents

30 We have found inversion agents that when added to conventional w/o latices of water soluble polymers in the presence of an inverting surfactant form invertible latices. The invertible latices are characterized by the rapid and complete inversion thereof under

conditions wherein the water source used to invert the latex is about 30 °C to 100 °C, or about 40 °C to 100 °C, or about 50 °C to 100 °C, or about 60 °C to 100 °C. Further, the invertible latices are characterized by the rapid and complete inversion thereof under conditions wherein the water source used to invert the latex includes about 0.1 to 30 wt% total dissolved solids. Still further, the invertible latices are characterized by the rapid and complete inversion thereof under conditions wherein the water source used to invert the latex is about 30 °C to 100 °C and further includes about 0.1 to 30 wt% total dissolved solids.

In embodiments, inversion agents of the invention comprise, consist essentially of, or consist of a nonionic compound. As used herein, a nonionic compound is a branched alkylene oxide oligomer or polymer. The oligomer is at least a dimer. In some embodiments, the branched polymer is a hyperbranched polymer. In some embodiments, the nonionic compound is a mixture of two or more nonionic compounds.

In embodiments, the nonionic compounds are not surface active agents in w/o latices. That is, they do not tend to lower the surface tension between water and oil phases in a w/o latex. As used herein, a compound that is not a surfactant is one that reduces the surface tension of water in a 0.5% active solution at room temperature by 35% or less, by 30% or less, by 25% or less, by 20% or less, or by 10% or less, or by 5% or less. (Example 8.)

In embodiments, inversion agents of the invention comprise, consist essentially of, or consist of compounds with an HLB as calculated by the Griffin formula:

$$\text{HLB} = 20 \times \text{MW}_H / (\text{MW}_H + \text{MW}_L),$$

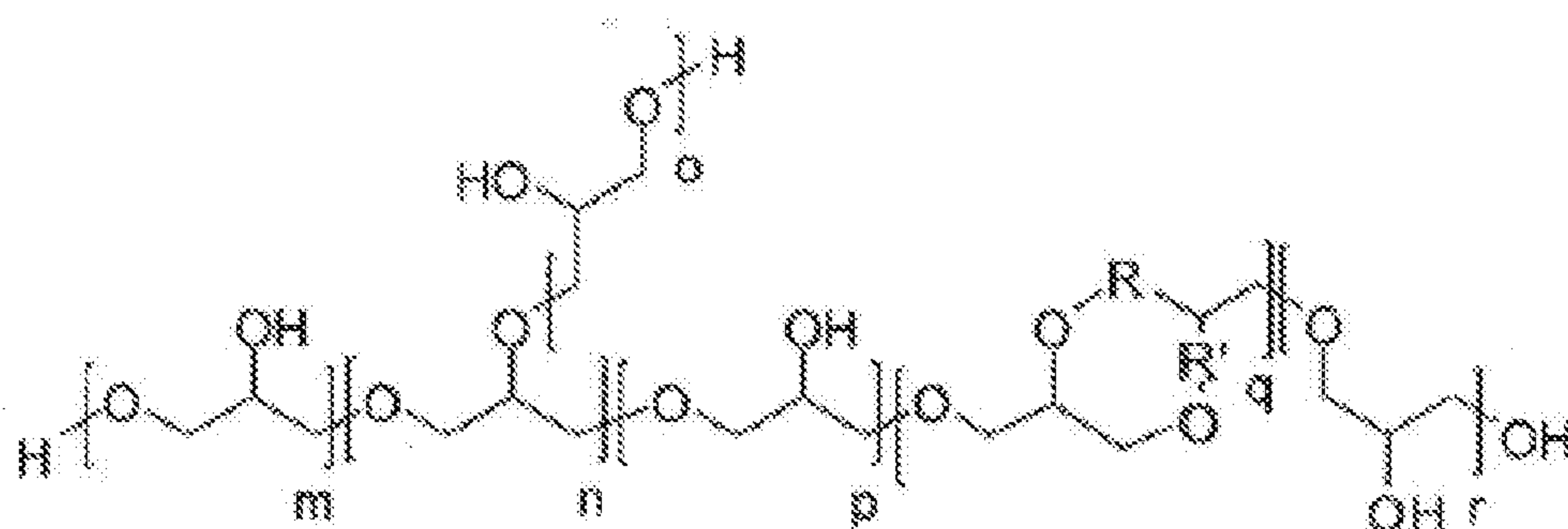
where MW_H = mol. wt. of hydrophile and MW_L = mol. wt. of hydrophobe,

of greater than about 10, of greater than about 15, or greater than about 16, or greater than about 17, or greater than about 18, or greater than about 19, or about 16 to 20, or about 17 to 20, or about 18 to 20. As calculated herein, ethoxylate values were used as a proxy for glycerol values; pentaerythritol and propylene oxide were considered lipophilic; and ethylene oxide, glycerol, and glycidol were considered hydrophilic.

Examples of nonionic inversion agents comprise, consist essentially of, or consist of structured polyols, branched glycols, and branched, cyclic glycerol-based polyols.

Examples of structured polyols include polyalkoxylates of organic compounds having three or more hydroxyl moieties, such as sugar alcohols. Thus, ethoxylates of glycerol, pentaerythritol, or sorbitol, and propoxylate ethoxylates of glycerol, pentaerythritol, or sorbitol having an average of 1 to 20 alkoxylate repeat units per hydroxyl moiety are
 5 examples of suitable structured polyols.

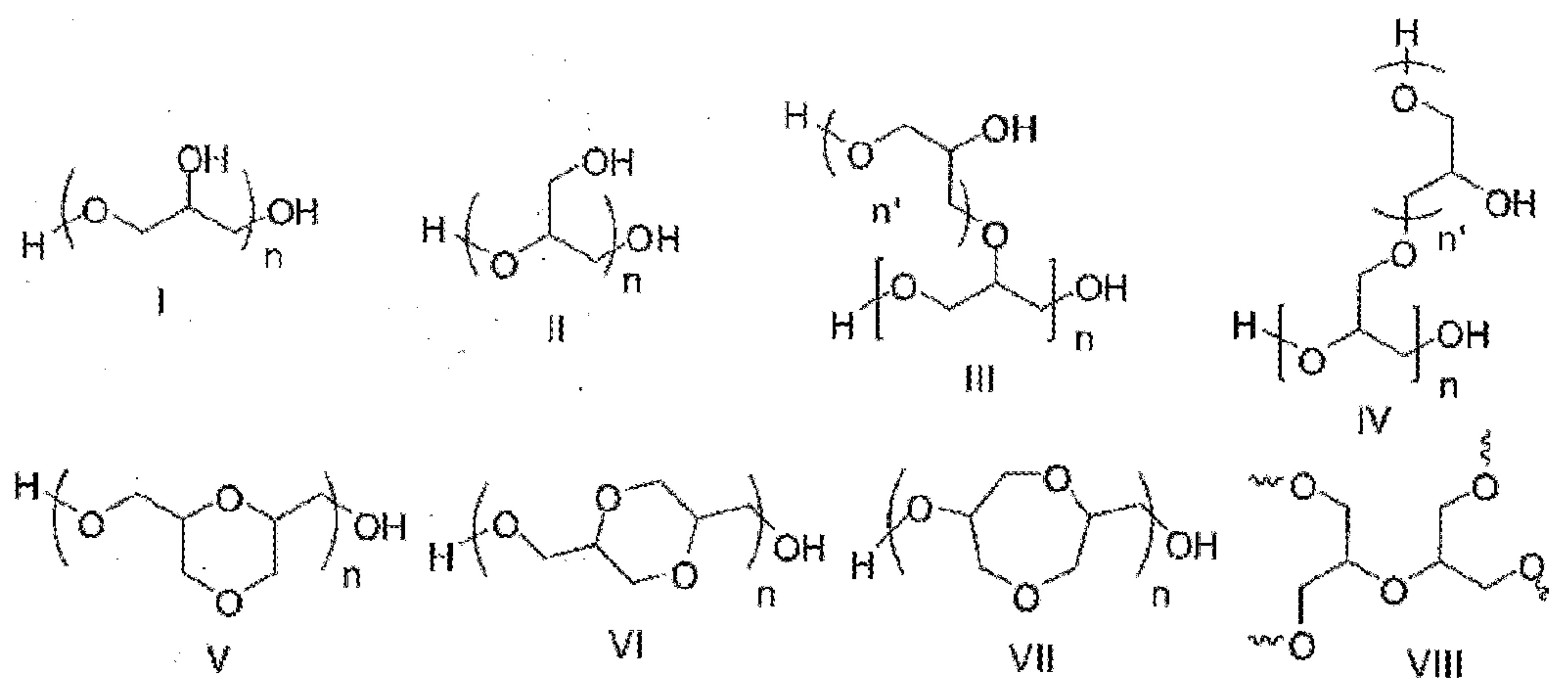
Branched, cyclic glycerol-based polyols are as described in U.S. Patent Application Publication No. 2011/092743, which is incorporated by reference herein in its entirety. In some embodiments, the glycerol-based polyols have the following structure:



where
 10 each m, n, o, p, q, and r is independently any integer; and R and R¹ are (CH₂)_n and n in (CH₂)_n is independently 0 or 1.

In some embodiments, the sum of m, n, o, p, q, and r is from 2 to 135, or from 5 to 135, or from 10 to 135, or from 20 to 135, or from 30 to 135, or from 40 to 135, or from 50 to 135, or from 60 to 135, or from 70 to 135, or from 80 to 135, or from 90 to 135, or
 15 from 100 to 135, or from 110 to 135, or from 120 to 135, or from 2 to 130, or from 2 to 120, or from 2 to 110, or from 2 to 100, or from 2 to 90, or from 2 to 80, or from 2 to 70, or from 2 to 60, or from 2 to 50, or from 2 to 40, or from 2 to 30, or from 2 to 20, or from 2 to 10.

The glycerol-based polyols may be polyglycerols, polyglycerol derivatives, polyols
 20 having glycerol-based monomer units and non-glycerol monomer units, or combinations thereof. The glycerol and glycerol-based monomer units may be selected from the following structures I-VIII:



where each n and n' is independently any integer.

Glycerol monomer units may self-condense to form the 6- or 7-membered structures V-VII. The non-glycerol monomer units may include polyols such as pentaerythritol and glycols, amines, other monomers capable of reacting with glycerol or glycerol-based polyol intermediates and any combination thereof. The glycerol-based polyols may have at least two hydroxyl groups.

In some embodiments, a glycerol-based polyol has a degree of branching of about 0.1 to about 0.5, or about 0.2 to about 0.5, or about 0.1 to about 0.4. As used herein, “degree of branching” means the mol fraction of monomer units at the base of a chain branching away from the main polymer chain relative to a perfectly branched dendrimer. The degree of branching is determined by ^{13}C NMR as described in *Macromolecules* (1999) 32:4240-4246. Cyclic units are not included in the degree of branching. In a perfect dendrimer the degree of branching is 1 or 100%.

In some embodiments, a glycerol-based polyol has a degree of cyclization of about 0.01 to about 0.19, or about 0.02 to about 0.19, or about 0.05 to about 0.19, or about 0.10 to about 0.19, or about 0.02 to about 0.18, or about 0.02 to about 0.15, or about 0.02 to about 0.10, or about 0.15 to about 0.18. As used herein, “degree of cyclization” means the mol fraction of cyclic structure units, such as structures V-VII above, relative to the total monomer units in a polymer. The degree of cyclization may be determined by ^{13}C NMR.

A glycerol-based polyol has an average molecular weight of at least about 166 Daltons. In some embodiments, a glycerol based polyol has an average molecular weight of about 166 Daltons to about 10,000 Daltons, or about 240 Daltons to about 10,000 Daltons, or about 314 Daltons to about 10,000 Daltons, or about 388 Daltons to about

10,000 Daltons, or about 462 Daltons to about 10,000 Daltons, or about 1,000 Daltons to about 10,000 Daltons, or about 2,000 Daltons to about 10,000 Daltons, or about 3,000 Daltons to about 10,000 Daltons, or about 4,000 Daltons to about 10,000 Daltons, or about 5,000 Daltons to about 10,000 Daltons, or about 166 Daltons to about 9,000 Daltons, or about 166 Daltons to about 8,000 Daltons, or about 166 Daltons to about 7,000 Daltons, or about 166 Daltons to about 6,000 Daltons, or about 166 Daltons to about 5,000 Daltons, or about 166 Daltons to about 4,000 Daltons, or about 166 Daltons to about 3,000 Daltons, or about 166 Daltons to about 2,000 Daltons, or about 166 Daltons to about 1,000 Daltons.

Examples of hyperbranched polymers include highly-branched glycidol-based polyols as disclosed in U.S. Patent No. 6,822,068 and poly(glycidol) multi-branched polymers as disclosed in Sunder et al, *Macromolecules* (1999) 32:4240-4246, each reference being incorporated by reference herein in its entirety. Examples of hyperbranched polymers also include dendrimers as disclosed in Garcia-Bernabé et al, *Chem. Eur. J.* (2004) 10:2822-2830; Siegers et al, *Chem. Eur. J.* (2004) 10:2831-2838; and Haag et al, *J. Am. Chem. Soc.* (2000) 122:2954-2955, each of which is incorporated by reference herein in its entirety.

Unexpectedly, the inversion agent, or the inversion agent in combination with the inversion surfactant, reduces the bulk viscosity of the invertible latex. In embodiments, reduced bulk viscosity provides better pumpability for pumping and transferring the invertible latex and/or the polymer flooding solution. The inversion agent, or the inversion agent in combination with the inversion surfactant, may increase the speed of the inversion process, increase the completeness of the inversion process, or both increase the speed and completeness. The resulting polymer flooding solution may thereby demonstrate improved performance.

In embodiments, the inversion agents, or the inversion agents in combination with an inversion surfactant, of the present disclosure facilitate inversion of an invertible latex compared to an invertible latex comprising no inversion agent and/or compared to an invertible latex comprising a known inversion agent such as glycerol. The inversion agents, or the inversion agents in combination with an inversion surfactant, of the present disclosure increase the speed and/or completeness of the inversion process compared to an invertible latex comprising no inversion agent and/or compared to an invertible latex comprising a known inversion agent such as glycerol.

In embodiments, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex is about 0 °C to 100 °C. In some examples, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex is about 4 °C, about 25 °C, or about 60 °C. (Examples 6 and 7.)

In embodiments, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex includes about 0.1 to 30 wt% total dissolved solids. In some examples, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex includes about 3.5% total dissolved solids. (Examples 6 and 7.)

In embodiments, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex is about 0 °C to 100 °C and includes about 0.1 to 30 wt% total dissolved solids. In some examples, the inversion agents, or the inversion agents in combination with an inversion surfactant, facilitate inversion of an invertible latex under conditions wherein the water source used to invert the latex is about 4 °C, about 25 °C, or about 60 °C and includes about 3.5% total dissolved solids. (Examples 6 and 7.)

Without being limited to any mechanism or mode of action, inversion agents may form hydrogen bonds and/or may affect the osmotic pressure of monomer- or polymer-comprising droplets of the discontinuous internal water phase within the continuous oil phase of a w/o latex. The inversion agents may increase the osmotic pressure of the droplets such that the droplets swell. When combined with a water source to form a polymer flooding solution, the swollen droplets may rupture more easily, facilitating the release of the monomer or polymer into the water. Separately from, or in addition to, the effect on osmotic pressure, the inversion agents may chelate ions within the droplets. Chelation may prevent or limit interaction of ions with the surfactant and thereby facilitate inversion. In embodiments, the branched structure of some inversion agents, such as

pentaerythritol ethoxylate and pentaerythritol propoxylate, may facilitate inversion compared to the inclusion of straight chain molecules, such as polyethylene glycol.

In embodiments, the inversion agent is added to a latex in an amount sufficient to facilitate the inversion of a w/o latex. The amount is not so high that it causes the emulsion to break or otherwise be unstable. In embodiments, the inversion agent is added to a latex in an amount less than amounts of known inversion agents. For example, the presently disclosed inversion agent may be added in an amount of from about 0.1 wt% to 5.0 wt% based on the total weight of the w/o latex. In contrast, and as disclosed in US 2014/0051620, glycerol is preferably added in an amount of from about 5 to about 20% by weight.

In embodiments, in order to facilitate inversion of a w/o latex, the inversion agent is added to a latex at about 0.1 wt% to 20.0 wt% based on the total weight of the w/o latex, or about 0.1 wt% to 15.0 wt%, or about 0.1 wt% to 10.0 wt%, or about 0.1 wt% to 7.5 wt%, or about 0.1 wt% to 5.0 wt%, or about 0.5 wt% to 4.5 wt%, or about 1.0 wt% to 4.0 wt%, or about 1.5 wt% to 3.5 wt%, or about 2.0 wt% to 3.0 wt%, or about 0.1 wt% to 4.5 wt%, or about 0.1 wt% to 4.0 wt%, or about 0.1 wt% to 3.5 wt%, or about 0.1 wt% to 3.0 wt%, or about 0.5 wt% to 5.0 wt%, or about 1.0 wt% to 5.0 wt%, or about 1.5 wt% to 5.0 wt%, or about 2.0 wt% to 5.0 wt%, based on the total weight of the w/o latex.

The inversion agent is added to a latex at an inversion surfactant:inversion agent wt:wt ratio of about 10:1, or about 7.5:1, or about 5:1, or about 2.5:1, or about 2:1, or about 1.75:1, or about 1.5:1, or about 1.25:1, or about 1:1, or about 1:10, or about 1:7.5, or about 1:5, or about 1:2.5, or about 1:2, or about 1:1.75, or about 1:1.5, or about 1:1.25.

The inversion surfactant and inversion agent are added to a latex in a combined amount ([inversion surfactant + inversion agent]) of about 0.1 wt% to 20.0 wt% based on the total weight of the w/o latex, or about 0.5 wt% to 18.0 wt%, or about 1.0 wt% to 16.0 wt%, or about 1.5 wt% to 14.0 wt%, or about 2.0 wt% to 12.0 wt%, or about 2.5 wt% to 10.0 wt%, or about 3.0 wt% to 8.0 wt%, or about 3.5 wt% to 7.5 wt%, or about 4.0 wt% to 7.0 wt%, or about 4.5 wt% to 6.5 wt%, or about 0.1 wt% to 18.0 wt%, or about 0.1 wt% to 16.0 wt%, or about 0.1 wt% to 14.0 wt%, or about 0.1 wt% to 12.0 wt%, or about 0.1 wt% to 10.0 wt%, or about 0.1 wt% to 8.0 wt%, or about 0.1 wt% to 7.5 wt%, or about 0.1 wt% to 7.0 wt%, or about 0.1 wt% to 6.5 wt%, or about 0.5 wt% to 20.0 wt%, or about 1.0 wt% to 20.0 wt%, or about 1.5 wt% to 20.0 wt%, or about 2.0 wt% to 20.0 wt%, or about 2.5

wt% to 20.0 wt%, or about 3.0 wt% to 20.0 wt%, or about 3.5 wt% to 20.0 wt%, or about 4.0 wt% to 20.0 wt%, or about 4.5 wt% to 20.0 wt%, or about 5.0 wt% to 20.0 wt%, or about 5.5 wt% to 20.0 wt%, or about 6.0 wt% to 20.0 wt%, or about 6.5 wt% to 20.0 wt%, or about 7.0 wt% to 20.0 wt%, or about 7.5 wt% to 20.0 wt%, or about 8.0 wt% to 20.0 wt%, based on the total weight of the w/o latex.

Invertible latices

Addition of an inversion agent of the present disclosure to a conventional w/o latex in the presence of an inverting surfactant, results in an invertible latex of the invention. The inversion agents may be added to the w/o latex before or after polymerization. The inversion agents may be added to a w/o latex before or after addition of an inverting surfactant. In some embodiments, the inversion agents are characterized as not being surfactants, that is, they are not surface active. Thus, in some embodiments, the invertible latices of the invention comprise, consist essentially of, or consist of a conventional w/o latex as described above, an inversion surfactant, and an inversion agent. In embodiments, the inversion agent is added to the w/o latex before polymerizing the monomer via a conventional free-radical or redox initiation. In other embodiments, the inversion agent is added directly to the w/o latex after polymerization is complete.

The invertible latices of the invention are stable or even shelf stable. That is, the invertible latices do not exhibit any observed signs of gross phase separation, coagulation, or precipitation for at least 24 hours at ambient laboratory temperatures. In embodiments, the invertible latex is stable under common ambient conditions for at least 1 day at 20 °C – 25 °C, or for at least 2 days at 20 °C – 25 °C, or for at least 1 week at 20 °C – 25 °C, or for at least 2 weeks at 20 °C – 25 °C, or for at least 1 month at 20 °C – 25 °C, or for at least 2 months at 20 °C – 25 °C, or for at least 1 day at 50 °C, or for at least 2 days at 50 °C, or for at least 5 days at 50 °C, or for at least 10 days at 50 °C, or for at least 30 days at 50 °C.

Inversion of the invertible latices

The invertible latices of the invention invert rapidly and completely when contacted with a water source having high temperature, high total dissolved solids, or both to yield a polymer flooding solution. Numerous advantages are realized by use of the invertible latices of the invention; principal of these is the time savings realized when rapid and complete inversion replaces multi-step, slow, or incomplete inversion in the field. Both the invertible latices and the resulting polymer flooding solutions are

characterized by the absence of the manifestations of latex or inversion instability; avoiding latex or inversion instability prevents downtime in the field necessitated by plugged or fouled equipment and avoids damages to reservoirs and plugging the formation.

5 During inversion, a water source is contacted with an invertible latex in one or more steps including one or more mixing and/or shearing processes to result in a polymer flooding solution having 1 wt% polymer or less. In some embodiments, the invertible latices of the invention provide for a simple, one-step inversion process characterized by absence of instabilities manifested as coagulation or precipitation of polymer or gross
10 phase separation of the water phase from the oil phase prior to dissolution. It is a feature of the invention that the invertible latices of the invention provide for a simple, one-step inversion process in the presence of water sources contacted with the invertible latex at temperatures of about 30 °C to 100 °C, or about 40 °C to 100 °C, or about 50 °C to 100 °C, or about 60 °C to 100 °C. It is a feature of the invention that the invertible latices of
15 the invention provide for a simple, one-step inversion process in the presence of water sources contacted with the invertible latex wherein the water source contacting the invertible latex includes about 0.1 to 30 wt% total dissolved solids. It is a feature of the invention that the invertible latices of the invention provide for a simple, one-step inversion process wherein the water source contacting the invertible latex includes about
20 0.1 to 30 wt% total dissolved solids and further contacts the inversion composition at about 30 °C to 100 °C.

 During the inversion process, the presence of the inversion agent reduces or prevents the coagulation of the polymer in the polymer flooding solution; reduces or prevents "hardening" or "raincycle" (evaporation, condensation) during storage that leads
25 to formation of viscous masses on the surface and in the bulk; and prevents formation of lumps, skin, crust, or "waxing" due to the sensitivity of the invertible latex to shear during the pumping, filtration and stirring steps to which the latices are subjected in EOR applications, which in turn leads to the breakage of the mechanical seals of the pumps or the plugging of the filters, valves and check valves.

30 The polymer flooding solution typically includes about 1 wt% or less of polymer, other (residual) compounds from the inverted latex, and any dissolved solids present in the water source. The polymer flooding solutions of the invention are characterized by

absence of gel particles, absence of gross phase separation, and/or absence other manifestations of inversion instability of w/o latices.

Inversion of the invertible latices to form the polymer flooding solutions is accomplished using conventional techniques and equipment, which is an unexpected
 5 benefit of employing the inversion agent of the invention using water sources that are high temperature, high total dissolved solids, or both high temperature/high total dissolved solids water sources. In some embodiments, inversion of invertible latices to form the polymer flooding solutions is suitably accomplished in a single step including dilution and
 10 mixing of the invertible latex with the water source to the target polymer concentration in the polymer flooding solution. In other embodiments, inversion of invertible latices to form the polymer flooding solutions is suitably accomplished in two dilution/mixing steps to reach the target polymer concentration. In some embodiments, the inversion and dilution to a target concentration of less than 1 wt% is accomplished in about 1 to 15 minutes, for example about 1 to 14, 1 to 13, 1 to 12, 1 to 11, 1 to 10, 1 to 9, 1 to 8, 1 to 7, 1
 15 to 6, 1 to 5, 2 to 15, 3 to 15, 4 to 15, 5 to 15, 6 to 15, 7 to 15, 8 to 15, 9 to 15, 10 to 15, 2 to 10, 2 to 9, 2 to 8, 3 to 10, 3 to 9, 3 to 8, 4 to 10, 4 to 9, 4 to 8, or 4 to 7 minutes.

After inversion, the polymer flooding solutions comprise about 100 ppm to 10,000 ppm (0.01 wt% to 1.00 wt%) polymer, or about 200 ppm to 5000 ppm, or about 200 ppm to 4000 ppm, or about 200 ppm to 3000 ppm, or about 200 ppm to 2500 ppm polymer. In
 20 some embodiments the water source contacts the invertible latex at a temperature of about 30 °C to 100 °C, or about 40 °C to 100 °C, or about 50 °C to 100 °C, or about 60 °C to 100 °C. In other embodiments, the water source includes about 0.1 to 30 wt% total dissolved solids. In still other embodiments, the water source includes about 0.1 to 30 wt% total dissolved solids and further contacts the inversion composition at about 30 °C to
 25 100 °C.

A water source is water or a water solution having up to about 30.0 wt% total dissolved solids (TDS), or about 0.1 wt% to 29.0 wt%, or about 0.5 wt% to 28.0 wt%, or about 1.0 wt% to 27.0 wt%, or about 2.0 wt% to 25.0 wt%, or about 3.0 wt% to 20.0 wt% TDS. “High TDS” water sources have TDS of at least about 1 wt%. Thus in
 30 embodiments a water source includes one or more dissolved solid materials including but not limited to salts, ions, buffers, acids, bases, surfactants, compounds employed in the water used in mining operations, or other dissolved, dispersed, or emulsified compounds,

materials, components, or combinations thereof. Nonlimiting examples of water sources include hard water, produced water from mining operations, brackish water, sea water, municipal waste water, tap water, “gray water”, and the like. Water sources having high TDS and high temperature are often encountered in use for EOR applications. For example, hydraulic fracturing and conventional oil recovery often results in produced water having high TDS, temperatures in excess of 60 °C, or both; rather than use fresh water, in such situations it is economical to reuse the produced water as the water source for inversion processes.

In some embodiments, the method of inverting the invertible latices involves conventional inverting equipment. While inverting a latex is often accomplished in the field using high shear, stepwise dilution for efficiency in achieving full dilution and hydration of a polymer at the desired use level, we have found that relatively low shear mixing is advantageous in some embodiments for inverting the invertible latices of the invention. Such techniques are advantageous because avoiding some or all shear on the polymer chains during dissolution results in a higher final viscosity of the polymer flooding solution by reducing or eliminating chain scission of the high molecular weight polymers. It is a feature of the invertible latices of the invention that low-shear techniques that avoid substantial amounts of chain scission are suitably used in rapid inversion to result in polymer flooding solutions characterized by lack of manifestations of instability as discussed above.

Low shear inverting equipment employed to invert the invertible latices of the invention include static mixers. For example, U.S. Patent No. 8,383,560 describes an apparatus employing a two-step inversion apparatus. In the first step, a w/o polymer latex is diluted to yield a polymer solution having about 5000 ppm to 20,000 ppm polymer solids employing a first static mixer having a pressure drop of at least 2 bars between the inlet and outlet thereof. In the second step, the partially diluted latex is applied to a second static mixer having a pressure drop of at least 1 bar between the inlet and outlet, and is further diluted to result in a polymer solution having between 500 and 3000 ppm, in practice between 1000 and 2000 ppm polymer solids. Such a two-step dilution system is usefully employed in conjunction with the invertible latices of the present invention. Conventional static mixers, as described in U.S. Patent No. 8,383,560 are usefully

employed; other low shear mixers and pumps are used in addition to, or as a replacement for, one or more static mixers described in U.S. Patent No. 8,383,560.

Unexpectedly, we have further found that it is possible to employ a single stage inversion of the invertible latices by employing the inversion agents of the invention: that is, a single dilution step with a water source is usefully employed to dilute the invertible latices to form a polymer flooding solution at the final use concentration of about 100 ppm to 10,000 ppm. No intermediate or step-down dilution is required to form the polymer flooding solution. The polymer flooding solutions of the invention are characterized by the substantial absence of gels and solution instabilities in the field. This finding is significant because conventional w/o latices, subjected to a single dilution step in the field, result in substantial gel particles and/or solution instabilities that cause plating out or plugging of equipment used to carry out EOR by polymer flooding. Conventional water-in-oil EOR latices require two or more dilution steps and several hours to complete inversion to result in a polymer solution.

In some embodiments, after the invertible latices are contacted with water source to form a polymer flooding solution in a single dilution step, the polymer continues to build viscosity for about 0.5 minute to 120 minutes, or about 0.75 minute to 115 minutes, or about 1 minute to 110 minutes, or about 2 minutes to 105 minutes, or about 5 minutes to 100 minutes, or about 10 minutes to 90 minutes, or about 15 minutes to 80 minutes, or about 5 minutes to 70 minutes, or about 10 minutes to 70 minutes, or about 20 minutes to 70 minutes, or about 30 minutes to 70 minutes, or about 40 minutes to 70 minutes, or about 50 minutes to 70 minutes, or about 5 minutes to 60 minutes, or about 10 minutes to 60 minutes, or about 20 minutes to 60 minutes, or about 30 minutes to 60 minutes, or about 40 minutes to 60 minutes.

The inverted w/o latices, that is, the polymer flooding solutions of the invention, are characterized by a substantial freedom from gel particles and subsequent final polymer solution instability. The test for gel particle formation consists of measuring the time taken to filter given masses of solution containing 1000 ppm (0.1 wt%) polymer. The solution is contained in a steel bell filter ratio housing pressurized to and maintained at 20 psi. The filter has a diameter of 90 mm and a pore size of 5 microns.

The times required to obtain 90 g ($t_{90\text{ g}}$); 120 g ($t_{120\text{ g}}$); 180 g ($t_{180\text{ g}}$) and 210 g ($t_{210\text{ g}}$) of filtrate are therefore measured and a filtration quotient (or filter ratio denoted "FR") is defined, expressed as:

$$FR = \frac{t_{210\text{ g}} - t_{180\text{ g}}}{t_{120\text{ g}} - t_{90\text{ g}}}$$

The time measurement accuracy is 0.1 second.

5 The FR thus represents the capacity of the polymer solution to plug the filter for two equivalent consecutive mass samples. A typical acceptability criterion of the industry is $FR < 1.5$. Conventional w/o latices employed for formation of polymer flooding solutions cannot achieve this level of filterability even after several hours of stirring in the laboratory. However, the invertible latices of the invention are characterized in that
10 $FR < 1.5$ is suitably achieved in about 5 minutes or less when a water source is contacted with a invertible latex of the invention, for example about 1 to 5 minutes, or about 2 to 5 minutes, or about 3 to 5 minutes, or about 4 to 5 minutes, or about 1 to 4 minutes, or about 1 to 3 minutes.

In a nonlimiting example of an EOR application, a w/o latex is applied to a
15 reservoir as follows. An invertible latex is introduced to a mixing apparatus, wherein a water source is contemporaneously introduced into the apparatus in an amount suitable to form a polymer solution of the desired concentration. A water source, such as a high temperature water source, a high total dissolved solids water source, or a high temperature/high total dissolved solids water source is added to the invertible latex in an
20 amount suitable to target the selected final polymer concentration. The water source is added prior to or contemporaneously with the carrying out of one or more mixing processes to thoroughly mix the invertible latex with the water source and accomplish the inversion.

In some embodiments, inversion of the invertible latices is suitably carried out
25 using conventional equipment and methods used to invert latices in the field. Employing conventional equipment and methods familiar to those of skill in inverting w/o latices for EOR applications, it is possible to invert the invertible latex in less than 5 minutes, for example about 1 second to 5 minutes, or about 20 seconds to 5 minutes, or about 30 seconds to 5 minutes, or about 1 minute to 5 minutes, or about 2 minutes to 5 minutes, or
30 about 1 second to 4 minutes, or about 1 second to 3 minutes, or about 1 second to 2 minutes, or about 1 second to 1 minute.

In some embodiments, inversion is suitably carried out by subjecting the invertible latices of the invention to a single-step inversion by diluting the latices with a water source and efficiently mixing the water source and the invertible latex in a single step. Devices suitable to achieve a one-step inversion include static mixers, paddle or blade mixers, mixing pumps, and the like. Any devices conventionally employed for w/o latex inversion are suitably employed to invert the invertible latices of the invention.

While the foregoing description is centered on EOR applications, water soluble polymers and latices thereof are also usefully employed in one or more papermaking applications using a Fourdrinier or inclined Fourdrinier apparatus, wherein water-based furnishes dispensed onto a wire can include an EOR-type polymer to improve the rheological profile of the furnish as dictated by machine or application parameters. In such applications, the invertible latices of the invention are advantageously employed due to rapid inversion upon addition to a furnish (a water-based dispersion of fibers) to result in a polymer solution similar to the polymer flooding solutions as described above. In papermaking applications, it is desirable to use tap water or another water-based solution to form the furnish and the w/o latices of the invention are suitable for use with water-based furnishes employing water-based solutions having high TDS, at elevated temperatures, or both. Papermaking includes making paper—that is, cellulose based mats—as well as other nonwoven fibrous mats such as filtration media that employ e.g. thermoplastic and glass fibers in addition to or instead of cellulose based fibers. One of skill will appreciate that other industrial uses, such as in wastewater treatment, mining services, or energy services, of the w/o latices of the invention are similarly envisioned.

EXAMPLES

Abbreviations

- PEG – Polyethylene glycol
- PEO – Pentaerythritol ethoxylate
- PG – Polyglycerol
- PPO – Pentaerythritol propoxylate

Example 1

The nonionic inversion agents used in the following examples were purchased from Sigma Aldrich (St. Louis, MO) except for the polyglycerols, which were synthesized according to the method described in U.S. Patent Application Publication No.

2011/092743. Briefly, a reaction mixture of glycerol and a strong base catalyst at a concentration greater than 2% was stirred and gradually heated to between 230 °C and 260 °C under inert gas flow for up to 16 hours.

Example 2

- 5 Water-in-oil latices were prepared using the components of Table 1.

Table 1. Components of w/o latices.

<u>Material</u>	<u>Wt%</u>
<u>Water Phase</u>	
Acrylamide 49.5%	38.2953
DI water	15.0941
Acrylic acid	7.6437
Sodium hydroxide	8.2524
Sodium formate	0.0340
VERSENEX® 80 (pentasodium diethylenetriaminepentaacetate)	0.0300
<u>Oil Phase</u>	
Hydrocarbon solvent (hydrotreated light distillate)	27.1845
Sorbitan sesquioleate (Span 83™ or Arlacel 83™, Croda International PLC, Yorkshire, United Kingdom)	0.8234
Polyoxyethylene (40-50) sorbitol hexaoleate	2.5747
HYPERMER® B210 (Croda International PLC, Yorkshire, United Kingdom)	0.0194
<u>Initiator</u>	
2,2'-azobisisobutyronitrile	0.0288
<u>Post treatment/reduction of acrylamide residual</u>	
TBHP (tertiary butyl hydroperoxide) 70%	0.0064
Sodium metabisulfite	0.0133

Polymerization of the components of Table 1 was conducted at 38 to 44 °C for 3 to 4 hours and post heated for 57 °C for 30 minutes. The latex polymer (an acrylic acid and acrylamide copolymer) was then agitated at 800 rpm using a cage stirrer at room temperature. A nonionic inversion agent (2-3 wt%, neutralized to pH 7), then a stabilizer (ammonium thiocyanate, 0.125 %), and then an inverting surfactant (tridecyl alcohol ethoxylate (TDA-12), 3.3 %) were added with agitation. Control latices did not include an inversion agent. The resulting blend was stirred at room temperature for 30 minutes to produce a w/o latex for the invertibility analysis of Examples 6 and 7.

Example 3

The stability of the w/o latices produced in Example 2 was evaluated and stability data is presented in Table 2. Stability was assessed by allowing the latices to stand at ambient laboratory temperatures for the indicated amount of time, and the amount of oil phase that separates from the latex (oil split) was observed as an indication of latex stability; the bulk viscosity (BV) of the lattices was also measured before and after standing.

Table 2. Stability data of the w/o latices of Example 2.

Inversion Agent (3 wt %)	Oil Split (%)	Latex BV (initial, cP)	Latex BV (Final, cP)	Aging Time
Polyglycerol 1	4.76	1012	886	2 months
Polyglycerol 2	4.76	960	869	2 months

The stability data presented in Table 2 demonstrates that w/o latices comprising nonionic inversion agents remained stable after 2 months. The oil split was low and no significant change in the latex BV was observed.

Example 4

Water-in-oil latices were prepared using the components of Table 3.

Table 3. Components of w/o latices.

<u>Material</u>	<u>Wt %</u>
Acrylamide 49.5%	38.2953
DI water	13.1717
Acrylic acid	7.6437
Sodium hydroxide 50%	8.3457
Sodium formate	0.0340
Glyoxal 40%	0.0117
VERSENEX® 80 (pentasodium diethylenetriaminepentaacetate)	0.0300
Hydrocarbon solvent (hydrotreated light distillate)	29.0000
Sorbitan sesquiolate	0.8892
Polyoxyethylene (40-50) sorbitol hexaoleate	2.5108
HYPERMER® B210 (Croda International PLC, Yorkshire, United Kingdom)	0.0194
2,2'-azobisisobutyronitrile	0.0288
TBHP (tert-butyl hydroperoxide) 70%	0.0064
Sodium metabisulfite	0.0133

The w/o latices were prepared as in Example 2. The stability of the w/o latices was evaluated and stability data is presented in Table 4. Stability was assessed by placing the latices in a 50 °C oven for 4.5 months, and the amount of oil phase that separates from the latex (oil split) was observed as an indication of latex stability; the bulk viscosity (BV) of the lattices was also measured before and after standing.

Table 4. Stability data of the w/o latices of Table 3.

Inversion Agent (2 wt %)	Inversion Agent (1 wt %)	Oil Split (%)	Latex BV (initial, cP)	Latex BV (Final, cP)
Polyglycerol 2	Lactic acid	14.63	812	988

The stability data presented in Table 4 demonstrates that w/o latices comprising nonionic inversion agents remained stable after 4.5 months.

10 Example 5

The bulk viscosity (BV) of each of the w/o latices produced in Example 2 was measured at room temperature using a Brookfield DV-E viscometer. BV data for w/o latices comprising 3 wt% of a nonionic inversion agent are presented in Table 5.

15 Table 5. Bulk viscosity data of w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent.

Inversion Agent (3 wt %)	MW of polyglycerols (Da)	BV (cps)
None (Control)	N/A	2432
Glycerol	N/A	2152
Polyglycerol 1	260	1012
Polyglycerol 2	960	960
Pentaerythritol ethoxylate	N/A	1960
Pentaerythritol propoxylate	N/A	480
Polyethylene glycol	N/A	1400

The data of Table 5 demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent had bulk viscosities lower than w/o latices comprising no inversion agent (control SC latices) and lower than w/o latices comprising 3 wt% glycerol. The inclusion of a nonionic inversion agent in w/o latices decreased bulk viscosity 19% to 80% over control latices and 9% to 78% over w/o latices comprising glycerol. The inclusion of 3 wt% glycerol in w/o latices had a negligible effect on bulk

viscosity. The lower BVs of the w/o latices comprising a nonionic inversion agent provide better pumpability for pumping and transferring the invertible latices.

Example 6

The invertibility of the w/o latices of Example 2 was determined by torque monitor
 5 technique. A torque monitor is a qualitative analytical tool comprising a DC stir motor, a controller that can report the torque (DC voltage) required to maintain a constant stir speed, and a computer to record the torque reading as a function of time. In a typical experiment, the w/o latex was added to a stirring solution of 3.5% synthetic sea water (Glas-Col Precision Stirrer, obtained from Glas-Col LLC of Terre Haute, IN), and the
 10 generated torque was monitored as a function of time ([polymer] = 10000 ppm, 400 rpm). The analysis was run for 20-30 min to confirm the torque remained stable. Experiments were conducted at 60 °C with high salinity conditions to evaluate the performance of w/o latices under high stress conditions.

The 3.5% synthetic seawater used in the present Example was formed by blending
 15 the components of Table 6.

Table 6. Components of 3.5% synthetic seawater.

Reagent	Amount (g)
Deionized water	957.99
Sodium bicarbonate (NaHCO ₃)	0.01
Calcium chloride CaCl ₂ ·2H ₂ O	1.57
Sodium sulfate (Na ₂ SO ₄)	4.38
Magnesium chloride (MgCl ₂ ·6H ₂ O)	11.39
Sodium chloride (NaCl)	24.65

Example 6A

Torque data at 60 °C for w/o latices comprising 3 wt% of a nonionic inversion
 20 agent are presented in Table 7 and Figure 1.

Table 7. Torque data at 60 °C of w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent.

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
0	-0.3713	0.5544	1.1393229	0.4985
20	13.7685	101.3641	52.71403	87.4736

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
40	116.7145	162.0941	142.84261	155.7312
60	164.8305	173.2839	142.13053	180.7556
80	185.1756	187.7289	147.31852	193.2678
100	191.3808	214.5844	178.243	243.6218
120	169.1030	234.2173	170.10498	243.2149
140	209.6914	197.4945	168.68083	247.3857
160	234.4106	202.4790	212.01579	279.6326
180	193.4153	206.8532	227.88493	268.8497
200	216.6087	227.8086	256.7749	306.8949
220	255.1626	236.2518	254.43522	303.7415
240	250.9918	273.1781	243.85579	309.1329
260	222.6105	295.9646	272.03369	369.8629
280	234.8175	309.6975	304.17887	344.2281
300	284.1543	336.4512	315.5721	369.5577
320	329.1168	318.1407	323.71012	333.8521
340	346.0032	334.3150	324.62565	365.9973
360	319.2495	331.9753	301.33057	340.4643
380	385.7778	344.6910	344.36035	357.1472
400	377.5380	403.3864	315.47038	322.8658
420	286.7991	358.5256	299.49951	323.9848
440	381.7088	329.0253	357.48291	331.1056
460	363.2965	330.0425	319.33594	323.9848
480	370.2138	378.7689	331.23779	328.4607
500	325.6582	329.0253	314.96175	333.7504
520	377.1311	341.2323	372.43652	346.9747
540	361.9741	329.6356	310.99447	324.3917
560	319.4529	339.1978	324.21875	337.2091
580	373.4690	322.8200	331.33952	351.5523
600	321.2840	323.2269	341.41032	321.2382
620	374.3846	360.0515	350.76904	322.1537
640	356.5826	313.8682	347.00521	342.2953
660	350.2757	355.6773	359.92432	313.9140
680	312.6373	371.1395	320.35319	334.3608
700	311.2132	335.4340	353.31217	353.2817
720	363.0931	287.2162	351.68457	328.0538
740	320.2667	376.8361	334.8999	339.3453
760	331.9651	347.3358	316.28418	308.0139
780	332.4738	320.6838	337.84993	318.5933
800	370.0104	355.4738	339.17236	351.0437
820	348.7498	354.4566	350.76904	352.2644
840	326.3702	324.5494	341.51204	318.0847
860	342.9515	330.9580	344.46208	342.4988
880	368.9931	337.8754	286.1735	321.4417
900	354.7516	343.6737	299.90641	302.8259
920	307.4493	305.6285	338.76546	304.2501
940	309.5856	309.7992	331.74642	296.4172
960	309.4838	333.3995	297.66846	332.4280
980	366.4500	345.8099	303.16162	327.1383

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
1000	347.3256	358.9325	332.76367	324.3917
1020	306.6355	351.2014	343.44482	309.1329
1040	366.3483	307.8664	329.71191	319.0002
1060	294.9371	357.8135	319.43766	353.4851
1080	302.1596	331.6701	307.63753	356.3334
1100	324.0306	342.8599	304.48405	305.6742
1120	299.3113	350.2858	290.95459	334.7677
1140	331.9651	343.2668	331.03434	338.0229
1160	338.6790	350.8962	295.8374	315.6433
1180	358.3120	360.4584	349.24316	282.5826
1200	329.7272	320.0734	289.32699	325.1038

The data of Table 7 and Figure 1 demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert as fast as or faster than w/o latices comprising no inversion agent (control w/o latices) at 60 °C in 3.5% SSW and as fast as or faster than w/o latices comprising 3 wt% glycerol at 60 °C in 3.5% SSW. The data of Table 7 and Figure 1 also demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert to a greater extent than w/o latices comprising no inversion agent (control w/o latices) at 60 °C in 3.5% SSW and as well as or to a greater extent than w/o latices comprising 3 wt% glycerol at 60 °C in 3.5% SSW. The faster inversion rates and greater extent of inversion of some of the w/o latices comprising a nonionic inversion agent provide better performance of the invertible latices than control w/o latices and w/o latices comprising glycerol under high stress conditions such as high TDS and elevated temperature.

Example 6B

Torque data at 60 °C for w/o latices comprising 3 wt% of a nonionic inversion agent or PEG are presented in Table 8 and Figure 2.

Table 8. Torque data at 60 °C of w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent or PEG.

Time (sec)	Torque (g.cm)				
	Control	Glycerol	PEO	PPO	PEG
0	-0.3713	0.5544	-0.4018	1.0986	-0.1780
20	13.7685	101.3641	21.8760	82.9875	62.8916
40	116.7145	162.0941	70.1955	162.0280	129.1148
60	164.8305	173.2839	108.3425	164.2660	153.3254
80	185.1756	187.7289	128.3824	184.5093	153.9358

Time (sec)	Torque (g.cm)				
	Control	Glycerol	PEO	PPO	PEG
100	191.3808	214.5844	140.5894	220.9269	152.8168
120	169.1030	234.2173	156.8654	230.8960	148.0357
140	209.6914	197.4945	184.7382	235.1685	175.6032
160	234.4106	202.4790	187.5865	261.6170	185.2671
180	193.4153	206.8532	241.2974	282.1655	146.0012
200	216.6087	227.8086	242.7216	255.2083	158.0048
220	255.1626	236.2518	274.4598	292.3381	174.3825
240	250.9918	273.1781	288.3962	293.0501	198.2880
260	222.6105	295.9646	329.5949	309.4279	188.1154
280	234.8175	309.6975	312.6068	329.7729	196.5586
300	284.1543	336.4512	318.4052	330.3833	174.9929
320	329.1168	318.1407	338.0381	297.9329	183.3344
340	346.0032	334.3150	305.3843	350.2197	204.7984
360	319.2495	331.9753	302.6377	337.0972	206.6294
380	385.7778	344.6910	361.9436	341.9800	208.6639
400	377.5380	403.3864	361.9436	329.9764	231.8573
420	286.7991	358.5256	325.0173	331.4006	259.9335
440	381.7088	329.0253	284.2255	338.8265	255.5593
460	363.2965	330.0425	330.5105	302.8158	266.2404
480	370.2138	378.7689	319.6259	312.7848	282.4148
500	325.6582	329.0253	291.0411	315.4297	288.0096
520	377.1311	341.2323	315.2517	352.2542	288.8234
540	361.9741	329.6356	317.2862	330.6885	299.1994
560	319.4529	339.1978	352.6866	316.5487	337.9567
580	373.4690	322.8200	367.0298	322.0418	309.6771
600	321.2840	323.2269	360.1125	335.0627	348.4344
620	374.3846	360.0515	329.0863	350.3215	310.6944
640	356.5826	313.8682	363.5712	328.6540	338.7705
660	350.2757	355.6773	357.9763	304.7485	305.2012
680	312.6373	371.1395	311.5896	340.9627	345.6879
700	311.2132	335.4340	356.5521	357.3405	312.1185
720	363.0931	287.2162	354.5176	330.4850	340.8051
740	320.2667	376.8361	347.9055	334.2489	309.1685
760	331.9651	347.3358	307.9274	290.5070	328.3946
780	332.4738	320.6838	347.4986	336.7920	309.3719
800	370.0104	355.4738	355.5349	315.2262	314.2548
820	348.7498	354.4566	317.6931	297.4243	339.4826
840	326.3702	324.5494	336.5122	347.4731	308.7616
860	342.9515	330.9580	311.8947	314.8193	330.8360
880	368.9931	337.8754	355.6366	347.3714	326.0549
900	354.7516	343.6737	329.0863	342.4886	305.5064
920	307.4493	305.6285	325.6276	334.4523	293.0959
940	309.5856	309.7992	355.9418	341.2679	325.9532
960	309.4838	333.3995	268.7632	337.7075	296.9615
980	366.4500	345.8099	303.8584	288.9811	301.0305
1000	347.3256	358.9325	310.0637	295.0846	299.5046
1020	306.6355	351.2014	331.1208	315.2262	301.1322
1040	366.3483	307.8664	303.4515	308.7158	308.4564
1060	294.9371	357.8135	317.2862	305.3589	337.0412

Time (sec)	Torque (g.cm)				
	Control	Glycerol	PEO	PPO	PEG
1080	302.1596	331.6701	322.7793	308.1055	323.3083
1100	324.0306	342.8599	342.2089	299.2554	321.4773
1120	299.3113	350.2858	299.5860	329.6712	295.9442
1140	331.9651	343.2668	299.9929	317.3625	336.2274
1160	338.6790	350.8962	305.0791	316.2435	335.3119
1180	358.3120	360.4584	344.5485	335.7747	289.6372
1200	329.7272	320.0734	333.3588	310.6486	288.7217

The data of Table 8 and Figure 2 demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert faster than w/o latices comprising no inversion agent (control w/o latices) at 60 °C in 3.5% SSW and faster than w/o latices comprising 3 wt% glycerol at 60 °C in 3.5% SSW. The data of Table 8 and Figure 2 also demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert to a greater extent than w/o latices comprising no inversion agent (control w/o latices) at 60 °C in 3.5% SSW and to a greater extent than w/o latices comprising 3 wt% glycerol at 60 °C in 3.5% SSW. The faster inversion rates and greater extent of inversion of the w/o latices comprising a nonionic inversion agent provide better performance of the invertible latices than control w/o latices and w/o latices comprising glycerol under high stress conditions such as high TDS and elevated temperature.

Example 7

The invertibility of the w/o latices of Example 2 was determined by torque monitor technique as described in Example 6 with the following modifications. Experiments were conducted at room temperature (*ca* 25° C) or 4° C to evaluate the performance of w/o latices across a range of temperatures.

Example 7A

Torque data at room temperate for w/o latices comprising 3 wt% of a nonionic inversion agent are presented in Table 9 and Figure 3.

Table 9. Torque data at room temperature of w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent.

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
0	-0.0712	-0.0865	0.0916	-0.5137
20	2.0650	26.2604	7.8227	4.5726

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
40	141.0217	284.3374	240.7735	248.6115
60	295.6441	424.2096	400.0753	400.9959
80	382.3140	531.7332	493.3573	495.7021
100	475.9013	557.2662	497.3246	486.4451
120	447.4182	545.4661	532.7250	471.1863
140	488.6169	518.0003	511.9731	538.1215
160	518.6259	586.9700	551.4425	521.1334
180	498.6877	588.0890	499.2574	550.6337
200	511.0982	564.9974	528.6560	570.1650
220	472.0357	573.1354	497.0194	502.4160
240	460.8459	540.7867	502.4109	503.8401
260	472.7478	522.7814	511.4644	494.2780
280	427.8870	527.3590	483.6934	500.5849
300	450.1648	448.7254	556.1218	485.9365
320	449.4527	520.3400	467.5191	540.1560
340	447.7234	464.7980	495.2901	467.4225
360	438.5681	525.8331	464.7725	480.0364
380	450.5717	453.9134	573.1099	475.2553
400	439.2802	512.1002	508.8196	475.3571
420	431.0404	519.2210	470.8761	519.4041
440	448.0286	454.4220	461.2122	515.7420
460	422.9024	467.9515	492.1366	543.2078
480	431.0404	523.3917	452.6672	455.1137
500	429.2094	438.7563	527.3336	491.8365
520	457.8959	450.8616	463.5518	521.8455
540	426.4628	438.4511	458.2621	469.7622
560	397.8780	433.2631	453.1759	463.0483
580	406.8298	449.3357	446.3603	460.7086
600	438.3647	487.1775	457.9569	471.1863
620	399.5056	423.4975	448.3948	449.1119
640	397.5728	459.7117	439.5447	450.0275
660	392.2831	424.8199	444.2240	495.9056
680	407.2367	493.9931	490.2039	442.0929
700	413.1368	428.3803	486.5417	436.2946
720	421.6817	425.3286	526.2146	480.7485
740	381.5002	457.5755	439.6464	444.2291
760	380.0761	413.1215	501.5971	447.0774
780	399.6073	446.4874	502.0040	449.2137
800	375.0916	468.5618	450.7345	443.4153
820	412.6282	410.3750	426.9307	474.6450
840	438.6698	413.5284	491.4246	518.4886
860	370.6156	446.9961	448.9034	496.6176
880	398.7935	451.3702	426.9307	431.6152
900	374.2778	440.7908	477.7934	426.3255
920	406.1178	409.7646	445.1396	418.5944
940	397.3694	415.3595	457.8552	442.8050
960	373.3622	449.9461	468.7398	508.6212
980	366.4449	457.2703	410.8582	498.6521

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
1000	426.4628	405.4921	415.8427	435.4808
1020	407.4402	401.8300	409.5357	462.6414
1040	379.3640	410.1715	472.9106	463.3535
1060	432.7698	458.0841	445.0378	501.5004
1080	396.9625	435.0942	436.4929	496.3125
1100	374.8881	402.2369	437.7136	410.6598
1120	408.5592	409.7646	436.3912	494.9900
1140	397.1659	446.8943	455.0069	452.4689
1160	376.5157	412.6129	504.1402	442.4998
1180	391.9779	401.6266	470.0623	495.9056
1200	363.08797	404.06799	457.65177	484.30888

The data of Table 9 and Figure 3 demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert faster than w/o latices comprising no inversion agent (control w/o latices) at room temperature in 3.5% SSW and as fast as w/o latices comprising 3 wt% glycerol at room temperature in 3.5% SSW. The data of Table 9 and Figure 3 also demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert to a greater extent than w/o latices comprising no inversion agent (control w/o latices) at room temperature in 3.5% SSW and as completely as w/o latices comprising 3 wt% glycerol at room temperature in 3.5% SSW. The faster or comparable inversion rates and greater or comparable extent of inversion of the w/o latices comprising a nonionic inversion agent provide better or comparable performance of the invertible latices than control w/o latices and w/o latices comprising glycerol under high stress conditions such as high TDS.

Example 7B

Torque data at 4° C for w/o latices comprising 3 wt% of a nonionic inversion agent are presented in Table 10 and Figure 4.

Table 10. Torque data at 4° C of w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent.

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
0	0.2441	0.0559	-0.6612	0.4628
20	17.2323	85.0983	36.1633	23.7579
40	112.0402	263.9313	230.3569	165.9698
60	150.6958	411.0260	406.9519	236.0586
80	193.5221	478.5716	549.6724	280.1056

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
100	225.3621	628.4129	570.4244	357.7220
120	215.0879	700.9430	524.5463	363.2151
140	305.3182	589.5538	712.5346	457.0058
160	306.8441	512.1409	545.9086	441.2384
180	334.3099	565.7501	633.0872	479.3854
200	287.2111	553.2379	692.2913	453.4454
220	293.3146	643.6717	630.8492	469.8232
240	317.7287	623.4283	743.1539	494.3390
260	303.3854	702.8758	587.6160	488.0320
280	336.9548	657.9132	555.3691	507.3598
300	341.1255	561.6811	637.7665	480.8095
320	357.5033	678.7669	538.8896	452.6316
340	376.1190	588.4349	551.7069	432.1849
360	352.4170	667.2719	623.9319	426.9969
380	361.4705	609.5937	515.5945	450.4954
400	381.4087	661.2701	519.4600	538.0809
420	384.9691	612.6455	570.4244	534.4187
440	395.7520	557.0017	667.3686	489.6596
460	376.0173	625.4628	616.4042	475.1129
480	376.4242	651.3011	566.6606	448.1557
500	426.9816	604.8126	615.1835	514.9892
520	414.4694	582.0262	496.9788	532.5877
540	378.0518	599.4212	490.7735	531.5704
560	394.7347	561.8846	666.3513	472.0612
580	396.8709	574.0916	561.1674	457.4127
600	396.6675	550.7965	584.8694	456.9041
620	417.0125	573.0743	707.0414	442.0522
640	394.9382	558.7311	648.8546	466.2628
660	393.3105	513.1582	655.8736	464.0249
680	389.3433	484.0647	640.9200	606.5420
700	403.3813	494.4407	515.3910	566.5639
720	398.6003	585.6883	554.9622	550.5931
740	397.0744	553.4414	533.4981	512.0392
760	393.6157	519.1600	484.0597	469.2128
780	403.0762	520.2789	444.0816	458.1248
800	413.5539	487.7268	461.4766	568.1915
820	402.5675	490.0665	465.0370	520.4824
840	393.1071	567.5812	654.7546	449.0712
860	380.1880	509.2926	561.5743	439.9160
880	401.7537	476.9440	476.8372	451.5127
900	395.0399	474.5026	591.0746	443.8833
920	412.6383	455.5817	540.3137	465.9576
940	386.8001	663.4064	489.3494	649.7752
960	403.0762	672.7651	463.5111	561.2742
980	403.1779	460.4645	454.0507	523.2290
1000	395.7520	468.3990	455.5766	465.1438
1020	404.2969	475.9267	491.6890	451.8178
1040	401.6520	492.4062	483.1441	459.6507
1060	396.1589	475.1129	458.1197	680.1910

Time (sec)	Torque (g.cm)			
	Control	Glycerol	PG 1	PG 2
1080	402.7710	481.7251	458.9335	451.0040
1100	390.7674	567.9881	446.7265	449.3764
1120	395.9554	488.5406	632.8837	429.9469
1140	400.5330	505.8339	459.6456	588.1297
1160	398.1934	477.8595	442.7592	528.5187
1180	392.5985	456.0903	449.5748	452.3265
1200	396.8709	623.5301	445.3023	424.7589

The data of Table 10 and Figure 4 demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert faster than w/o latices comprising no inversion agent (control w/o latices) at 4° C in 3.5% SSW. Some of the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert as fast as w/o latices comprising 3 wt% glycerol at 4° C in 3.5% SSW. The data of Table 10 and Figure 4 also demonstrate that the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert to a greater extent than w/o latices comprising no inversion agent (control w/o latices) at 4° C in 3.5% SSW. Some of the w/o latices of Example 2 comprising 3 wt% of a nonionic inversion agent invert as completely as w/o latices comprising 3 wt% glycerol at 4° C in 3.5% SSW. The faster or comparable inversion rates and greater or comparable extent of inversion of some of the w/o latices comprising a nonionic inversion agent provide better performance of the invertible latices than control w/o latices and w/o latices comprising glycerol under high stress conditions such as high TDS.

The results of Examples 6 and 7 demonstrate that w/o latices comprising a nonionic inversion agent provide improved performance of the invertible latices over control w/o latices and w/o latices comprising glycerol under high stress conditions such as high TDS and across a broad range of temperatures.

Example 8

The surface tension of nonionic inversion agents at 0.5 wt% was measured in a Kruss-K12 processor tensiometer at room temperature. The tested samples were prepared in deionized water and were neutralized with NaOH or H₂SO₄. Data is presented in Table 11 as an average +/- standard deviation (SD) of two experiments.

Table 11. Surface tension data of nonionic inversion agents.

Inversion Agent or Comparative	Surface Tension (mN/m)	SD
None (deionized water)	72.13	0.14

Lauric Acid	22.17	0.15
PG1	67.69	0.09
PG2	54.02	0.37
PEO	52.32	0.16
PPO	48.85	0.21
PEG	56.24	0.12

The data of Table 11 demonstrate that nonionic inversion agents do not reduce the surface tension of water or reduce the surface tension of water by about 32% or less. By comparison, a known surfactant, lauric acid, reduces the surface tension of water by about 69%.

The invention illustratively disclosed herein can be suitably practiced in the absence of any element which is not specifically disclosed herein. Additionally each and every embodiment of the invention, as described herein, is intended to be used either alone or in combination with any other embodiment described herein as well as modifications, equivalents, and alternatives thereof. In various embodiments, the invention suitably comprises, consists essentially of, or consists of the elements described herein and claimed according to the claims. It will be recognized that various modifications and changes may be made without following the example embodiments and applications illustrated and described herein, and without departing from the scope of the claims.

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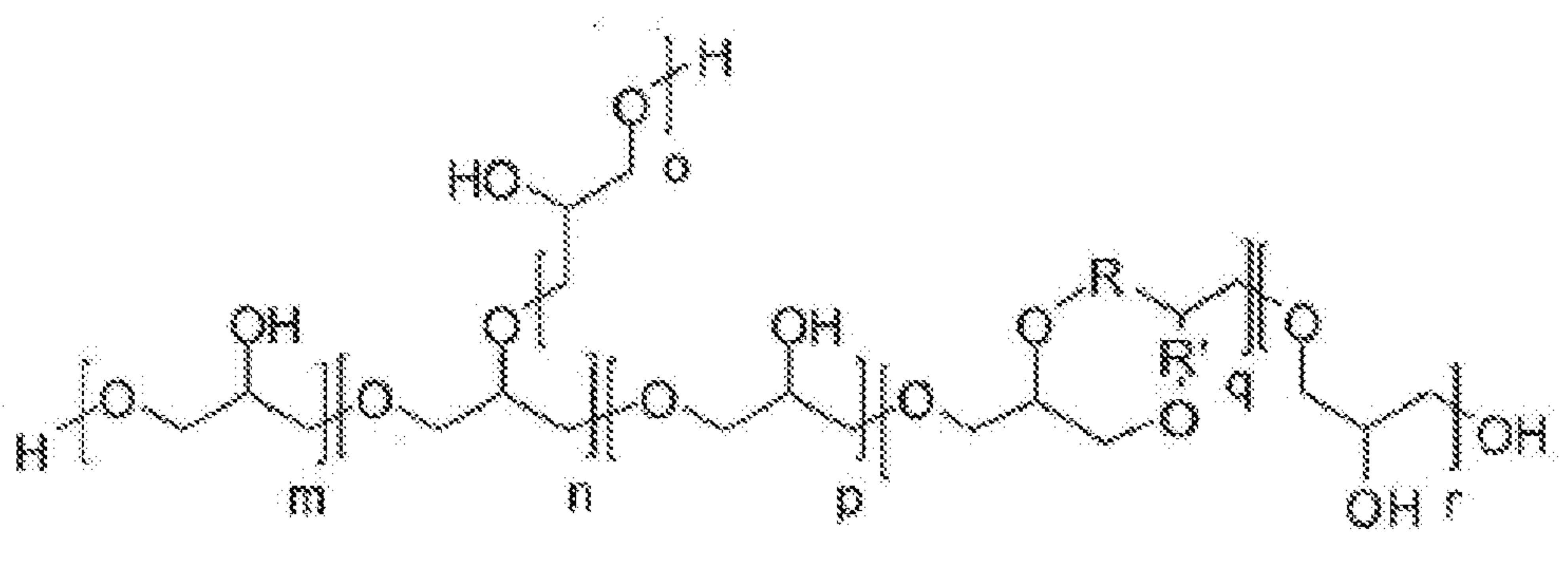
CLAIMS:

1. A water-in-oil latex comprising

about 15 wt% to 70 wt% of a water soluble or dispersible polymer comprising 1 mol % to about 100 mol % acrylamide monomers;

about 0.1 wt% to 20.0 wt% of an inversion surfactant characterized as having a hydrophilic/lipophilic balance of 10 or greater; and

about 0.1 wt% to 20.0 wt% of an inversion agent that is a nonionic inversion agent.
2. The latex of claim 1 comprising about 1.0 wt% to 20.0 wt% of the inversion agent and inversion surfactant combined.
3. The latex of claim 1 or claim 2, wherein the nonionic inversion agent comprises a nonionic compound characterized as a branched alkylene oxide oligomer or polymer.
4. The latex of claim 1 or claim 2, wherein the inversion agent is selected from a structured polyol, branched glycol, and branched, cyclic glycerol-based polyol.
5. The latex of claim 4, wherein the structured polyol is a polyalkoxylate of an organic compound having three or more hydroxyl moieties.
6. The latex of claim 4, wherein the glycerol-based polyol has the following structure:



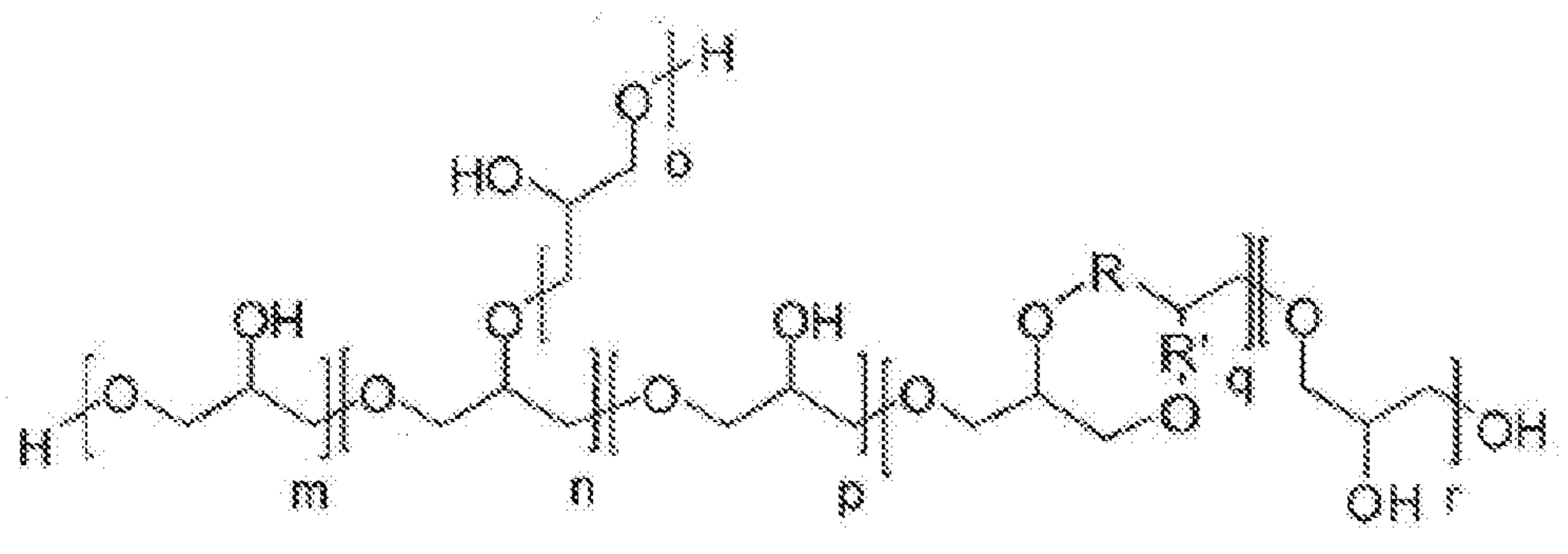
wherein each m, n, o, p, q, and r is independently any integer; and R and R¹ are (CH₂)_n and n in (CH₂)_n is independently 0 or 1.

7. The latex of any one of claims 1 to 6, wherein the inversion agent has a hydrophilic/lipophilic balance of greater than 10.
8. The latex of any one of claims 1 to 7, wherein the inversion agent is not a surfactant.

9. The latex of any one of claims 1 to 8 comprising about 0.1 wt% to 5.0 wt% of the nonionic inversion agent.
10. The latex of any one of claims 1 to 9 comprising
 - about 3 wt% to 50 wt% water;
 - about 10 wt% to 40 wt% of a compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C and is substantially a liquid over the range of 20 °C to 90 °C and comprising linear, branched, or cyclic hydrocarbon moieties;
 - about 20 wt% or less of a latex surfactant characterized as having a hydrophilic/lipophilic balance of between 2 and 10; and
 - about 0.1 wt% to 5.0 wt% of the inversion agent.
11. The latex of any one of claims 1 to 10, wherein the latex is shelf stable.
12. A method of forming an invertible latex, the method comprising
 - (a) forming a water-in-oil latex comprising
 - about 15 wt% to 70 wt% of a water soluble or dispersible polymer;
 - about 3 wt% to 50 wt% water;
 - about 10 wt% to 40 wt% of a compound or blend thereof that is less than 0.1 wt% soluble in water at 25 °C and is substantially a liquid over the range of 20 °C to 90 °C and comprising linear, branched, or cyclic hydrocarbon moieties; and
 - about 20 wt% or less of a latex surfactant characterized as having a hydrophilic/lipophilic balance of between 2 and 10; and
 - (b) adding to the latex about 0.1 wt% to 20.0 wt% of an inversion surfactant characterized as having a hydrophilic/lipophilic balance of 10 or greater and about 0.1 wt% to 5.0 wt% of a nonionic inversion agent to form an invertible latex.
13. The method of claim 12, wherein the invertible latex is shelf stable.
14. The method of claim 12 or claim 13, wherein the nonionic inversion agent comprises a nonionic compound characterized as a branched alkylene oxide oligomer or polymer.
15. The method of claim 12, wherein the inversion agent is selected from structured polyols, branched glycols, and branched, cyclic glycerol-based polyols.

16. The method of claim 15, wherein the structured polyols are polyalkoxylates of organic compounds having three or more hydroxyl moieties.

17. The method of claim 15, wherein the glycerol-based polyols have the following structure:



wherein each m, n, o, p, q, and r is independently any integer; and R and R¹ are (CH₂)_n and n in (CH₂)_n is independently 0 or 1.

18. A method of recovering hydrocarbon compounds from a subterranean reservoir, the method comprising

- (a) forming an invertible latex according to the method of any one of claims 12 to 17,
- (b) adding a water source to the invertible latex in a single addition to form a polymer flooding solution comprising about 100 ppm to 10,000 ppm of the water soluble or dispersible polymer,
- (c) injecting the polymer flooding solution into the subterranean reservoir, and
- (d) recovering the hydrocarbon compounds.

19. The method of claim 18, wherein the water source is about 30 °C to 100 °C.

20. The method of claim 18 or claim 19, wherein the water source includes about 0.1 to 30 wt% total dissolved solids.

21. Use of the latex of any one of claims 1 to 11 for injection into a subterranean hydrocarbon-containing reservoir.

22. Use of a latex comprising

about 15 wt% to 70 wt% of a water soluble or dispersible polymer comprising 1 mol % to about 100 mol % acrylamide monomers;

about 0.1 wt% to 20.0 wt% of an inversion surfactant characterized as having a hydrophilic/lipophilic balance of 10 or greater; and

about 0.1 wt% to 20.0 wt% of an inversion agent that is a nonionic inversion agent for contacting with a water source to form a polymer flooding solution,

wherein the water source is about 30 °C to 100 °C or includes about 0.1 to 30 wt% total dissolved solids or both.

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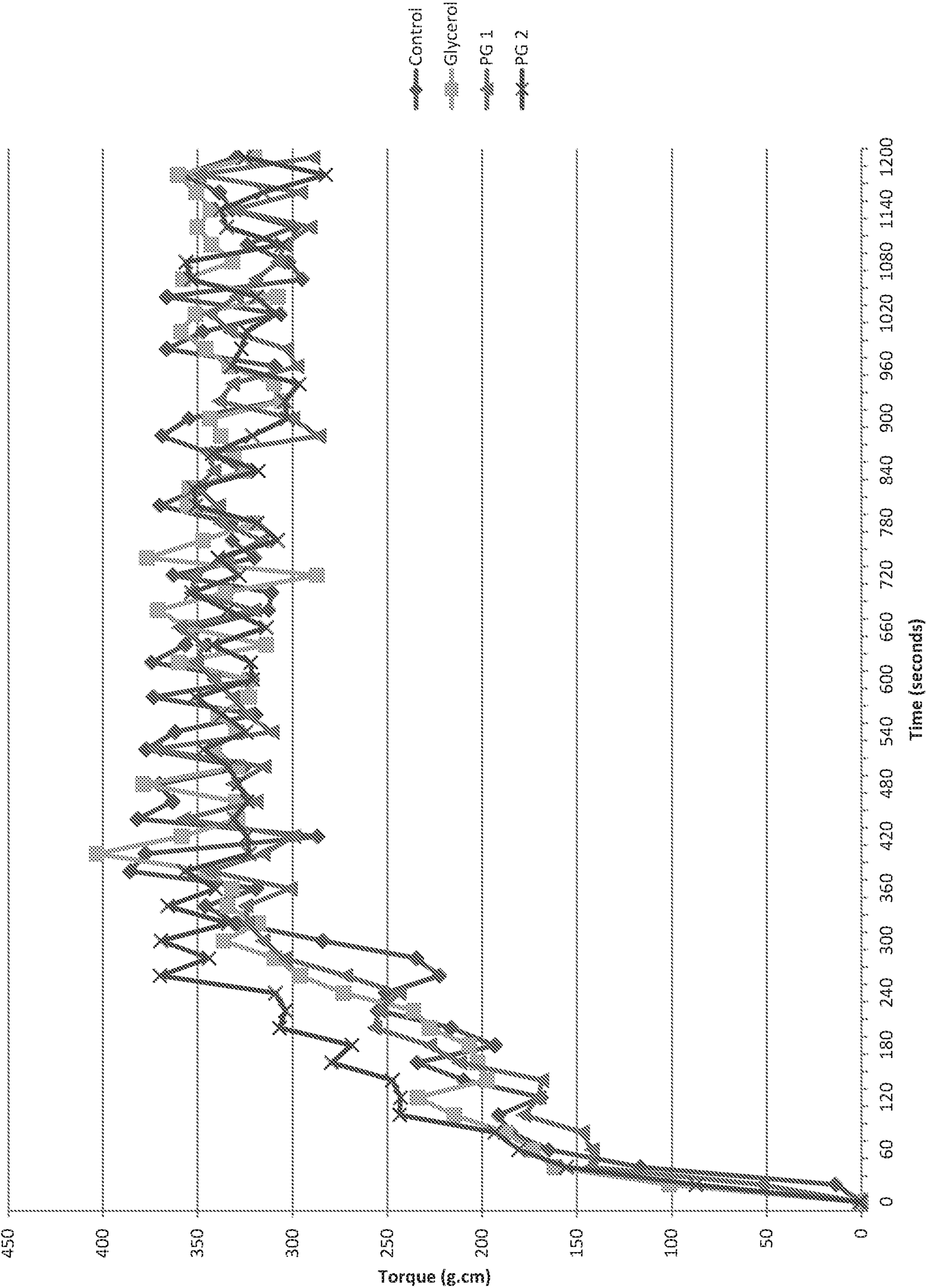


FIG. 1

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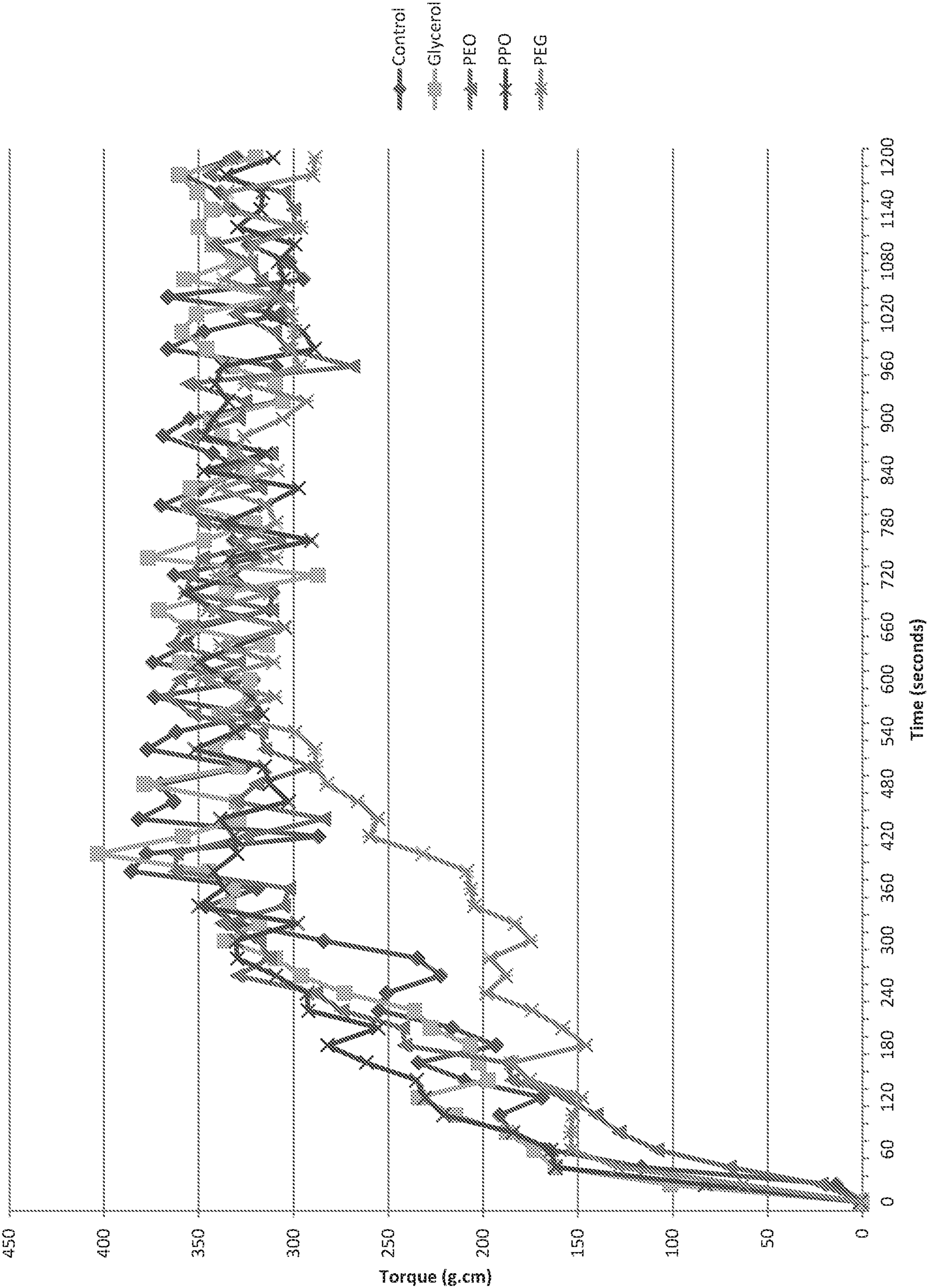


FIG. 2

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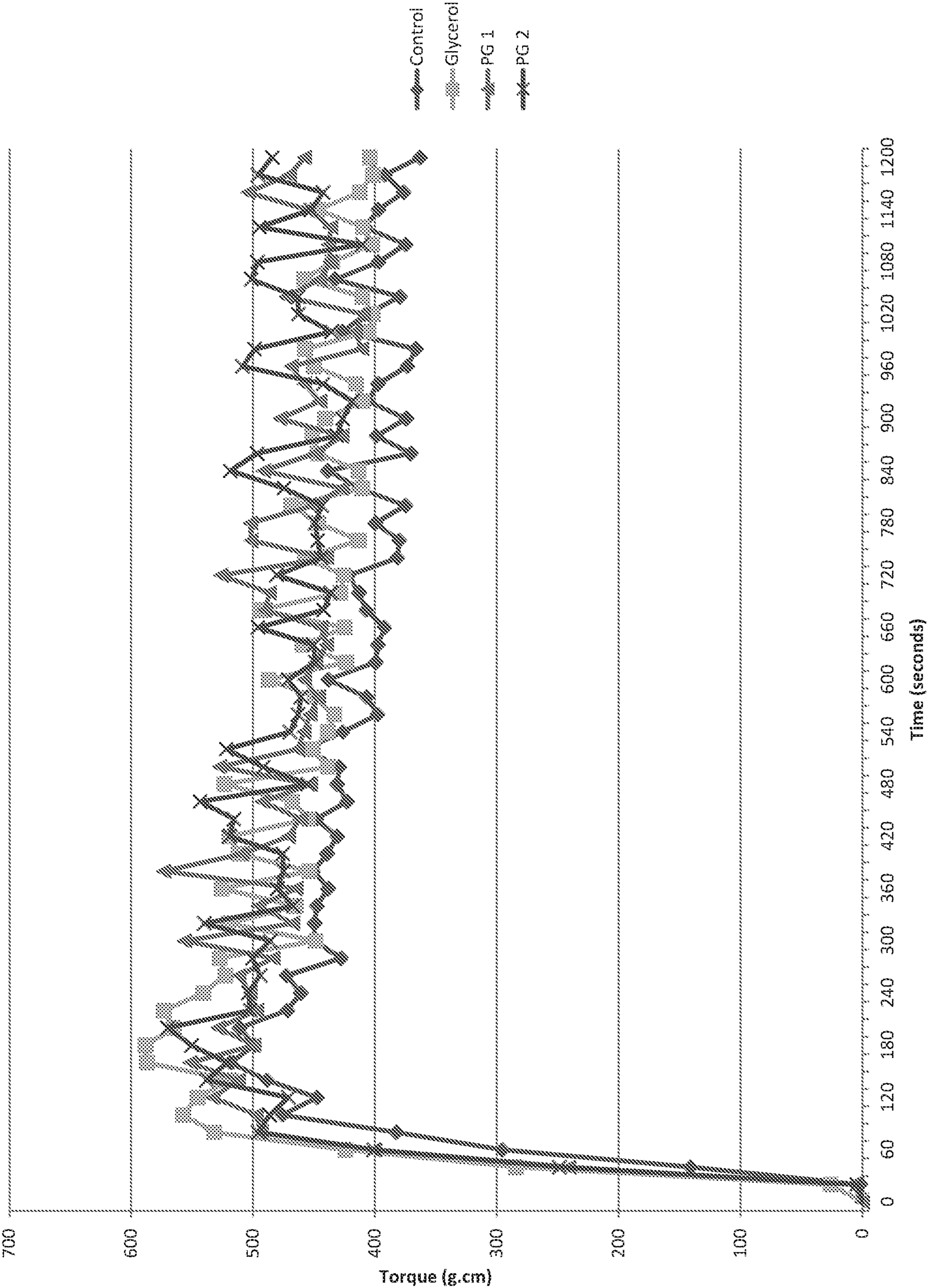


FIG. 3

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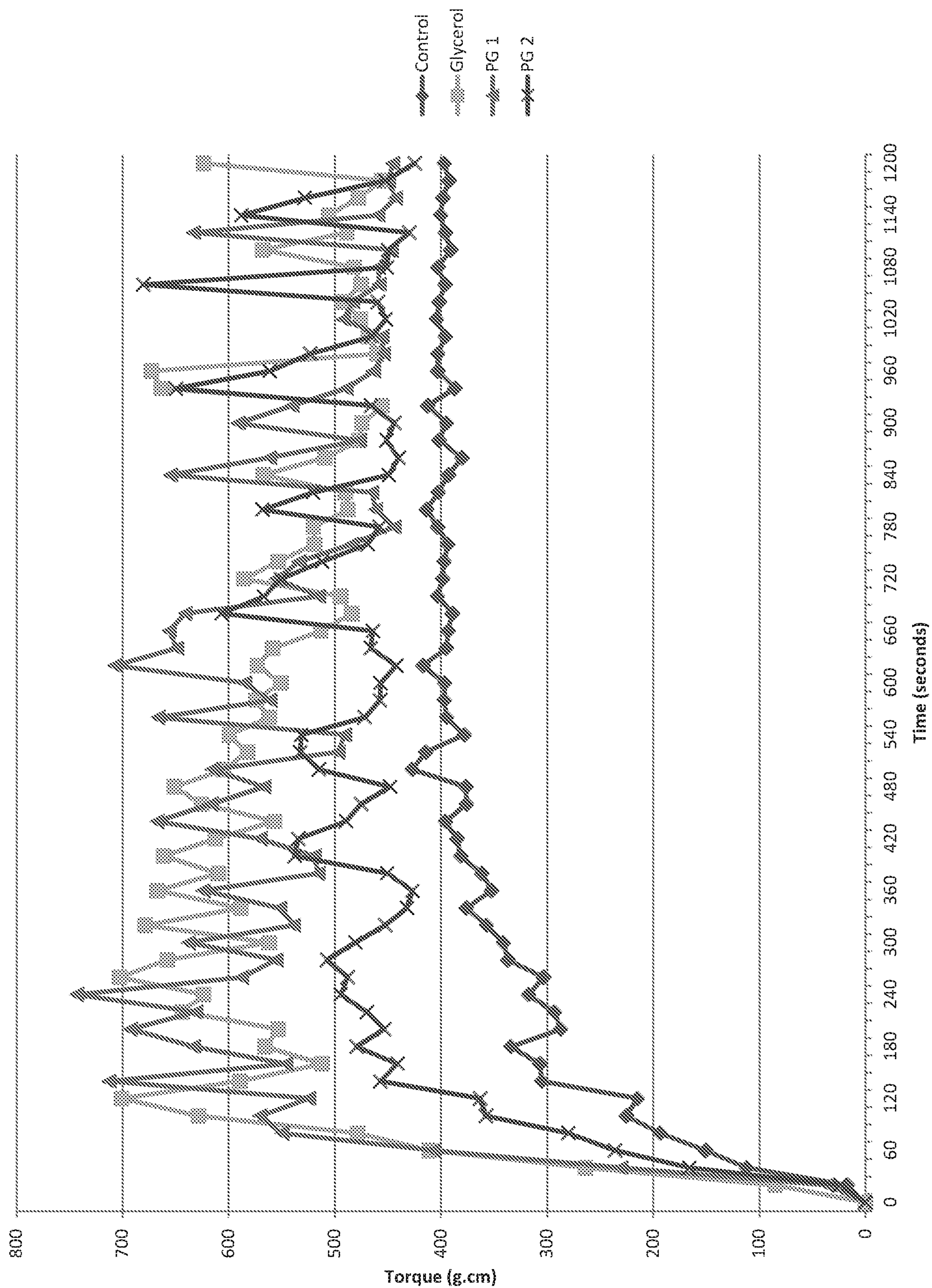


FIG. 4