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(71) Applicant: EMPIRE TECHNOLOGY DEVELOPMENT LLC [US/US]; 2711 Centerville Road, Suite 400, Wilmington, DE 19808 (US).

(72) Inventors: GRAF, Edwin, X.; 910 Gunnlaugsson Drive, Washington Island, WI 54246 (US). KERY, Robert, Thomas; 107 Neerim Road, Castle Cove, New South Wales 2069 (AU).

(74) Agent: LAGERWALL, Nicholas, M.; Foley & Lardner LLP, 150 E Gilman Street, Suite 5000, Madison, WI 53703-1482 (US).

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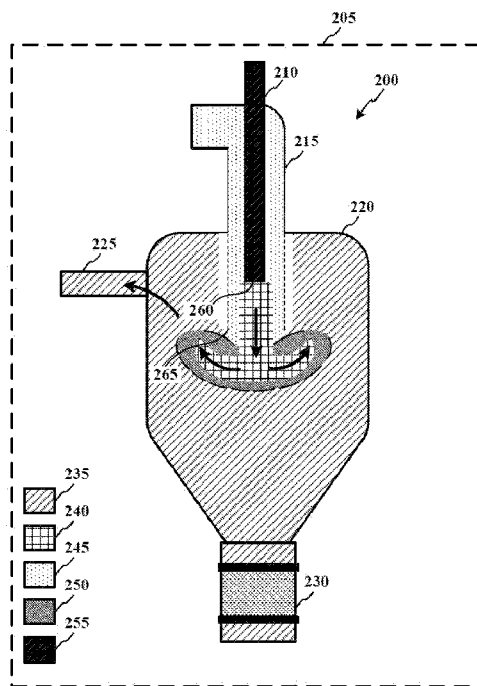


FIG. 2C

(57) Abstract: Systems and methods for reducing or eliminating corrosion of components of a reactor system, including a supercritical water gasification system, are described. The reactor system may include a reactor vessel configured to receive a reactor fluid through a reactor fluid inlet and a product source fluid corrosive to portions of the reactor system through a product source fluid inlet. The product source fluid may react with the reactor fluid to produce one or more reaction products, such as a fuel gas. The product source fluid inlet may be arranged within the reactor fluid inlet such that the product source fluid entering the reactor vessel is encased by a fluid conduit formed by the flow of reactor fluid entering the reactor vessel. The layer may operate to reduce corrosion by forming a barrier between the product source fluid and the surface of the reactor fluid inlet and/or the reactor vessel.

REDUCING CORROSION IN A REACTOR SYSTEM USING FLUID ENCASEMENT

BACKGROUND

[0001] Reactor systems are capable of generating fuel from materials that are typically considered waste, such as liquid biomass, or unclean fuel sources, including coal and other fossil fuels. For example, a supercritical water gasification system may produce hydrogen-rich synthesis gas by reacting a coal slurry with supercritical water, which is water that is heated to very high temperatures (for instance, above about 400 °C) under high pressure (for instance, about 22 megapascals). Supercritical water is very reactive and is able to break down the slurry to generate the hydrogen-rich fuel. The fuel may be used for various purposes, such as powering an engine, producing electricity and generating heat.

[0002] Due to the harsh conditions that occur during the reaction process, system components are susceptible to corrosion and breaking down. Accordingly, the efficiency and cost-effectiveness of a reactor system is subject to the rate of corrosion of system components, such as heaters and reactor vessels that come into contact with reactor materials. Management of corrosion typically involves the constant replacement of corroded parts or constructing components from corrosion-resistant materials, which can be expensive and largely ineffective. It will therefore be desirable to reduce corrosion in reactor systems through the use of components configured to eliminate contact between system components and damaging reactor process elements.

SUMMARY

[0003] This disclosure is not limited to the particular systems, devices and methods described, as these may vary. The terminology used in the description is for the purpose of describing the particular versions or embodiments only, and is not intended to limit the scope.

[0004] As used in this document, the singular forms “a,” “an,” and “the” include plural references unless the context clearly dictates otherwise. Unless defined otherwise, all technical and scientific terms used herein have the same meanings as commonly understood by one of ordinary skill in the art. Nothing in this disclosure is to be construed as an admission that the embodiments described in this disclosure are not entitled to antedate such disclosure by virtue of prior invention. As used in this document, the term “comprising” means “including, but not limited to.”

[0005] In an embodiment, a reactor system configured to reduce corrosion of portions thereof may comprise at least one reactor vessel, at least one reactor fluid inlet, at least one product source fluid inlet, and at least one product outlet. The reactor vessel may comprise an inner surface and may be configured to receive a reactor fluid through the at least one reactor fluid inlet and to receive a product source fluid corrosive to at least a portion of the inner surface through the at least one product source fluid inlet. The at least one product outlet may be configured to provide a discharge path for the reactor fluid and reaction product substances generated by a reaction of the product source fluid with the reactor fluid within the at least one reactor vessel. The at least one product source fluid inlet may be arranged within at least a portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by a flow of the reactor fluid, the reactor fluid thereby operating to reduce corrosion by forming a barrier between the product source fluid and the at least a portion of the inner surface.

[0006] In an embodiment, a method of reducing corrosion in a reactor system may comprise providing at least one reactor vessel comprising an inner surface and configured to receive a reactor fluid through at least one reactor fluid inlet and to receive a product source fluid corrosive to at least a portion of the inner surface through at least one product source fluid inlet. At least a portion of the at least one product source fluid inlet may be arranged

within at least a portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by the reactor fluid. The reactor vessel may receive the reactor fluid through the at least one reactor fluid inlet and may receive the product source fluid through the at least one product source fluid inlet such that the product source fluid reacts with the reactor fluid to generate reaction product substances. Corrosion may be reduced by the reactor fluid forming a barrier between the product source fluid and the at least a portion of the inner surface. The reactor fluid and the reaction product substances may be discharged through at least one product outlet in fluid communication with the reactor vessel.

[0007] In an embodiment, a method of manufacturing a reactor system configured to reduce corrosion thereof may comprise providing at least one reactor vessel comprising an inner surface. The at least one reactor vessel may be configured to receive a reactor fluid through at least one reactor fluid inlet and to receive a product source fluid corrosive to at least a portion of the inner surface through at least one product source fluid inlet. The at least one product source fluid inlet may be within at least a portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by a flow of the reactor fluid, the reactor fluid thereby operating to reduce corrosion by forming a barrier between the product source fluid and the at least a portion of the inner surface. At least one product outlet may be configured to discharge the reactor fluid and reaction product substances generated by a reaction of the product source fluid with the reactor fluid within the at least one reactor vessel.

BRIEF DESCRIPTION OF THE DRAWINGS

[0008] FIG. 1 depicts an illustrative reactor system according to some embodiments.

[0009] FIG. 2A depicts an illustrative reactor vessel according to some embodiments.

[0010] FIG. 2B depicts a bottom-up view of the product source fluid inlet arranged within the reactor fluid inlet.

[0011] FIG. 2C depicts an illustrative product source fluid conversion process within a reactor vessel configured according to some embodiments.

[0012] FIG. 3 depicts a flow diagram for an illustrative corrosion reduction method for a reactor system according to some embodiments.

DETAILED DESCRIPTION

[0013] The terminology used in the description is for the purpose of describing the particular versions or embodiments only, and is not intended to limit the scope.

[0014] The described technology relates generally to systems and methods for reducing or eliminating corrosion in reactor systems. The reactor systems may include supercritical water reactor systems, such as a supercritical water gasification system. In particular, embodiments provide systems and methods for reducing contact between corrosive reactor system fluids, such as product source fluids and/or reactor fluids, and the surfaces of reactor system components. Some embodiments include a reactor vessel configured to receive a product source fluid encased in a reactor fluid. For example, the product source fluid may enter the reactor vessel through a product source fluid inlet arranged at least partially within a reactor fluid inlet. The pressure of the reactor fluid entering the reactor vessel may be sufficient to enclose the product source fluid flowing therein. The reactor fluid may form a barrier preventing or substantially preventing the product source fluid from contacting surfaces of the reactor vessel, thereby reducing or eliminating corrosion of the reactor vessel.

[0015] Non-limiting examples of product source fluids include coal slurry, coal dust, liquid biomass, pulverized toxic waste, pulverized electronic waste (“e-waste”), or the like. A non-limiting example of a reactor fluid includes water, such as supercritical water and/or subcritical water. Supercritical water may include water at a pressure of about 22 megapascals to about 35 megapascals and at a temperature of about 375 °C to about 900 °C. Subcritical water generally includes water at an elevated pressure having a temperature below the temperature of supercritical water. For example, subcritical water may include water at a pressure of about 22 megapascals to about 30 megapascals at a temperature of about 275 °C to about 375 °C. Supercritical water without or substantially without corrosive ions (for example, heteroatoms) may be non-corrosive to reactor system components formed from materials known to those having ordinary skill in the art.

[0016] According to some embodiments, the product source fluid and the reactor fluid may enter the reactor vessel at temperatures and pressures that are non-corrosive or substantially non-corrosive to surfaces of the reactor vessel and components thereof. For example, the reactor fluid may include supercritical water devoid of corrosive ions, and the product source fluid may include a slurry at a temperature and pressure that are outside of a high-corrosion level of the slurry.

[0017] The product source fluid may react with the reactor fluid to generate reaction product substances, such as fuel products. The reaction of the product source fluid and the reactor fluid may occur within the barrier formed by the flow of reactor fluid within the reactor fluid inlet and/or the reactor vessel. Embodiments provide that the reactor vessel may include a trap configured to receive waste products resulting from the conversion of the product source fluid into fuel products, including, without limitation, salts, char, thorium, and mercury. The supercritical water and the fuel products may be discharged from the reactor vessel through a product outlet.

[0018] Use of the described technology can result in a reduction or elimination of corrosion in reactor system components relative to operation of the same or similar reactor system components without the described methods and materials. The degree of corrosion can generally be reduced by any amount. For example, the degree of corrosion can be reduced by at least about 10%, at least about 20%, at least about 30%, at least about 40%, at least about 50%, at least about 60%, at least about 70%, at least about 80%, at least about 90%, at least about 95%, at least about 96%, at least about 97%, at least about 98%, at least about 99%, and in an ideal situation, about 100% reduction (complete elimination of corrosion).

[0019] FIG. 1 depicts an illustrative reactor system according to some embodiments. As shown in FIG. 1, a reactor system **100** may be configured as a supercritical water gasification system. A product source fluid in the form of a slurry **155** may be introduced into the reactor system **100** through a slurry inlet **130**, which may include, for example, a high pressure slurry feed. The slurry **155** may include any type of material capable of undergoing supercritical water gasification, including, without limitation, biomass fluids (for example, micro algae fluids, bioresidues, biowastes, or the like), slurries of coal and other fossil fuels (for example, pulverized coal and water), solid materials (for example, coal dust), and oxidizable wastes (for example, toxic waste and e-waste). Accordingly, the supercritical water reactor system **100** may be configured to operate as any of various gasification systems, including, without limitation, a coal gasification system, a biomass gasification system, a toxic waste gasification system, an e-waste gasification system, and a waste oxidation system. The slurry **155**, along with air **150** and water **135**, may be fed into a heater **105**, or a pre-heater, such as a gas-fired heater. Although only one heater **105** is depicted in FIG. 1, a reactor system **100** configured according to some embodiments may include multiple heaters, such as one or more heaters for the water **135** and one or more

heaters for the slurry **155**. The water **135** and the slurry **155** may be heated in the heater **105**. Certain gases, such as steam **140** and flue gas **145**, may be exhausted from the heater **105**, for instance, to maintain pressure.

[0020] The slurry **155** and the water **135** may be fed into a reactor vessel **110**. Within the reactor vessel **110**, the slurry **155** may come into contact with the water **135** at a supercritical temperature and pressure (“supercritical water”). Under supercritical conditions, the slurry **155** may include corrosive ions such as the ions of various inorganic salts. The corrosive ions may be highly corrosive to the components of the reactor system **100**, such as the inside surface of the reactor vessel **110**. According to some embodiments, the temperature of the slurry **155** may be below supercritical temperatures such that the slurry **155** does not include or substantially does not include corrosive ions.

[0021] The supercritical water **135** may react with the components of the slurry **155** within the reactor vessel **110** to generate one or more reaction product substances that may be dissolved in the water **135**. In an embodiment, the slurry **155** may include one or more catalysts configured to facilitate the reaction, such as chlorine, sulfate, nitrate, and phosphate. The one or more reaction product substances, within the water **135**, may move through one or more heat exchangers, such as a heat recovery heat exchanger **115** and a cool-down heat exchanger **125**. A gas/liquid separator **120** may be provided to separate the one or more reaction product substances into the desired reaction products **165**, such as fuel gas products, and waste products **170**, such as liquid effluent, ash and char. In an embodiment, all or some of the waste products **170** may be collected in a trap (not shown, see FIGS. 2A and 2B) arranged within the reactor vessel **110**. In such an embodiment, at least a portion of the waste products **170** may exit the reactor vessel through a waste outlet (described in more detail with reference to FIGS. 2A and 2B). The reaction product **165** may include any fuel capable of being generated from the slurry **155** responsive to reacting with the supercritical

water **135**, including gas, solid and/or liquid materials. Illustrative reaction products **165** include, but are not limited to, CO, CO₂ and hydrogen-rich fuels, such as H₂ and/or CH₄.

[0022] During the supercritical water gasification process, the slurry **155** may be heated to various temperatures under different pressures within the reactor system **100**. In addition to supercritical conditions, the slurry **155** may be in a subcritical condition, in which the fluid within the slurry is at an elevated pressure and at a temperature that is below a supercritical temperature. In an embodiment where the fluid within the slurry **155** includes water, a subcritical temperature may be about 275°C to about 375°C. For example, the subcritical temperature may be about 275 °C, about 300 °C, about 325 °C, about 350 °C, about 375 °C, or in a range between any of these values (including endpoints). In an embodiment where the fluid within the slurry **155** includes water, the pressure of the fluid at the subcritical temperature may be about 20 megapascals to about 35 megapascals. For example, the pressure of the fluid at the subcritical temperature may be about 20 megapascals, about 22 megapascals, about 25 megapascals, about 28 megapascals, about 30 megapascals, about 35 megapascals, or in a range between any of these values (including endpoints). The slurry **155** under subcritical conditions typically includes corrosive ions that are highly corrosive to the components of the reactor system **100**. Non-limiting examples of corrosive ions include various ions of chlorine, sulfur (for example, sulphate ions), and/or phosphorous.

[0023] The reactor system **100** depicted in FIG. 1 is provided for illustrative purposes only and may include more or fewer components arranged in one or more configurations, sequences, connections, or the like, such as one or more valves, pre-heaters, reactor vessels, pumps for pumping the slurry **155** through the system, and other components known to those having ordinary skill in the art.

[0024] Supercritical water gasification systems, such as the illustrative reactor system **100** depicted in FIG. 1, may be configured to generate relatively clean energy from various grades of coal or biomass rapidly and with minimal polluting effluents. In addition, supercritical water gasification systems may generate fuel with greater efficiency than conventional gasification systems, such as pulverized coal gasification systems. However the high pressures and high temperatures within a reactor vessel during the gasification process create a harsh, corrosive environment that places severe constraints on reactor design. For instance, conventional system components, such as reactor vessels, suffer from degradation of the reactor components due to corrosion, necessitating frequent, time-consuming and expensive maintenance. The maintenance requirements can greatly affect the reactor cost dynamics, preventing large scale commercial implementation of supercritical water gasification technology.

[0025] Corrosion in supercritical water gasification systems is affected by a number of factors including some that are unique to the supercritical water environment. For example, fuel sources may include corrosive ions, such as ions of chlorine, sulfur, phosphorus and nitrogen, that may become free ions at supercritical temperatures and pressures. In addition, at pressures above about 8 megapascals and temperatures above about 300 °C, the ionic product of water increases rapidly from about $1 \times 10^{-45} \text{ mol}^2/\text{l}^2$ to about $1 \times 10^{-12} \text{ mol}^2/\text{l}^2$. As known to those having ordinary skill in the art, the ionic product, K_i , is generally a measure of the tendency of an amphoteric solvent, XH, to take up or to lose a hydron in the following reaction: $\text{XH} + \text{XH} = \text{XH}_2^+ + \text{X}^-$. In such a reaction, $K_i = a_{\text{XH}_2^+} \times a_{\text{X}^-}$, where $a_{\text{XH}_2^+}$ and a_{X^-} are the activities of XH_2^+ and X^- , respectively. The ionic product of water, K_w , is given by the following: $K_w = a_{\text{H}_3\text{O}^+} \times a_{\text{OH}^-}$; $K_w \approx 1 \times 10^{-14} \text{ mol}^2\text{dm}^{-6}$ at 25 °C. The increased ionic product of water under supercritical conditions causes, among other things, the dissociation of inorganic compounds within the water and/or a fuel product that

includes water. The free inorganic compounds may act to cause the corrosion of component surfaces that come in contact therewith.

[0026] Furthermore, above the critical point of water (for example, above about 374 °C and about 23 megapascals), the solubility of inorganic salts decreases rapidly, causing inorganic salts in reactor fluids and/or product source fluids to precipitate and attach to reactor wall surfaces. The precipitated inorganic salts can clog pipes and/or collect on reactor walls and create sites for corrosion. It is this relatively high ionic product in the supercritical water gasification environment and the availability of free hetero ions that makes the supercritical water gasification environment so corrosive to system components.

[0027] While many materials have been engineered to withstand high temperatures and pressures, much in excess of those required in a supercritical water gasification reactor, the addition of reactive free ions under supercritical conditions causes corrosion of these materials. Illustrative and non-restrictive materials include, without limitation, Inconel® of the Special Metals Corporation (Huntington, WV, USA), Hastelloy® N of Haynes International, Inc. (Kokomo, IN, USA), stainless steel, and various metals and metal alloys, such as nickel, iron and titanium, and any other type of material known to those having ordinary skill in the art, such as those used in conventional supercritical electric power generation boilers. As such, materials known to those having ordinary skill in the art exhibit various forms of corrosion when exposed to reactive ions under supercritical conditions. Accordingly, embodiments may be configured to reduce or eliminate corrosion within a reactor system by preventing or diminishing contact between corrosive reactor system fluids and system components.

[0028] FIG. 2A depicts an illustrative reactor vessel according to some embodiments. A reactor vessel **200** may be arranged within a reactor system **205**, such as the supercritical water gasification reactor system **100** depicted in FIG. 1. The reactor vessel **200**

may include a pressure vessel **220** configured as an outer shell for housing the reaction for converting a product source fluid into one or more reaction product substances, such as a fuel product, according to embodiments described herein. In an embodiment, the pressure vessel and/or components thereof may be insulated, for example, to minimize heat loss. A reactor fluid may enter the pressure vessel **220** through a reactor fluid inlet **215**. In an embodiment, the reactor fluid may include supercritical water, for instance, water at a pressure of about 22 megapascals to about 35 megapascals and at a temperature of about 450 °C to about 900 °C. In an embodiment, the temperature of the supercritical water may be about 600 °C to about 900 °C. In an embodiment, the temperature of the supercritical water may be about 650 °C +/- 50 °C.

[0029] A product source fluid may enter the pressure vessel **220** through a product source fluid inlet **210**. The product source fluid inlet **210** may be arranged within the reactor fluid inlet **215**. In an embodiment, the product source fluid inlet **210** and the reactor fluid inlet **215** may be arranged in various configurations. For example, the product source fluid inlet **210** and the reactor fluid inlet **215** may be arranged as a radius elbow (as shown in FIG. 2A), as an acceleration or venturi elbow arrangement, or combinations thereof. For embodiments including an acceleration elbow, the ratio change in cross-sectional area may be about 1.3:1 to about 3:1. For example, the ratio change in the cross-sectional area may be about 1.3:1, about 1.5:1, about 2:1, about 3:1, and ranges between any two of these values (including endpoints).

[0030] The reactor fluid inlet **210** may extend beyond the product source fluid inlet **215** into the at least one reactor vessel **200** for a certain distance. In an embodiment, the distance may be about 0.1 meters to about 5 meters. For example, the distance may be about 0.1 meters, about 0.25 meters, about 0.5 meters, about 1 meter, about 2 meters, about 3 meters, about 4 meters, about 5 meters, and ranges between any two of these values

(including endpoints). In an embodiment, the distance may be about 0.25 meters to about 2 meters. An opening **260** in the product source fluid inlet **210** where the product source fluid is released into the pressure vessel **220** may be located within the reactor fluid inlet **215**, above an opening **265** in the reactor fluid inlet. As such, the product source fluid may contact the reactor fluid and react therewith at least partially within the reactor fluid inlet **215**, for example, within the shaded area **270**. The size of the area **270** within the reactor fluid inlet **215** may be based on various factors, including the flow rate of the reactor fluid and/or product source fluid, the time required for conversion, or combinations thereof.

[0031] The pressure vessel **220** may have dimensions (for example, height, width, diameter, or the like) and a shape (for example, cylindrical, venturi-based shape, or the like) based on various factors. For example, the dimensions and shape of the pressure vessel **220** may depend on the throughput of the product source fluid and/or reactor fluid in which greater throughput may require a greater reaction time and, therefore, a larger pressure vessel. According to some embodiments, a pressure vessel **220** may be configured to receive a coal-based reactor fluid, such as a pulverized coal slurry, with a throughput of about 2000 tons per about 24 hours. In another example, the dimensions and shape of the pressure vessel **220** may be configured such that the reactor fluid and/or any reaction zone associated therewith does not contact the sides of the pressure vessel.

[0032] FIG. 2B depicts a bottom-up view of the product source fluid inlet **210** arranged within the reactor fluid inlet **215**. As shown in FIG. 2B, the reactor fluid inlet **215** may be configured to surround the product source fluid inlet **210**. As such, the reactor fluid flowing into the reactor vessel **200** may encase the product source fluid flowing into the reactor vessel.

[0033] Referring back to FIG. 2A, the product source fluid may enter the reactor vessel **200** encased by the reactor fluid entering the reactor vessel through the reactor fluid

inlet **215**. For example, the flow of the reactor fluid exiting the reactor fluid inlet **215** may form a fluid conduit through which the product source fluid may flow into the pressure vessel **220**. As such, the reactor fluid provides a physical barrier between the product source fluid and the inner surface of the reactor fluid inlet **215** and the pressure vessel **220**. In this manner, contact between the product source fluid and the surfaces of the reactor fluid inlet **215** and the reactor vessel **220** are reduced or eliminated, diminishing the corrosive effects of the product source fluid. The thickness of the barrier may depend on various factors, such as the type of reactor fluid and/or product source fluid, fluid velocities, reaction temperature, or the like. In an embodiment, the thickness of the barrier may be about 0.5 centimeters to about 15 centimeters. For example, the thickness of the barrier may be about 0.5 centimeters, about 1 centimeter, about 5 centimeters, about 10 centimeters, about 15 centimeters, and ranges between any two of these values (including endpoints). In an embodiment, the thickness of the barrier may be about 1 centimeter to about 5 centimeters.

[0034] According to some embodiments, the product source fluid flowing within the product source fluid inlet **210** may be heated by the reactor fluid flowing within the reactor fluid inlet **215** in contact with the product source fluid inlet. As the product source fluid contacts the reactor fluid within the reactor vessel **220**, the product source fluid may be heated by the higher temperature reactor fluid, reacting with the reactor fluid to generate one or more reactor products. Conversion of the product source fluid into the one or more reactor products may generate waste, such as mercury, effluent, salts, and char. The reactor vessel **200** may include a trap **230** configured to collect waste to allow, among other things, the reactor fluid to be re-used within the reactor system **205** and/or an external system (for instance, a steam turbine). The reactor products and the reactor fluid may exit from the pressure vessel **220** through an outlet **225** and into the reactor system **205** for further use and/or processing according to some embodiments described herein.

[0035] In an embodiment, the product source fluid may include any type of fluid capable of generating a product within a reactor system configured according to some embodiments described herein. For instance, the product source fluid may include biomass, toxic waste, e-waste, or fossil fuel slurries. In an embodiment, the product source fluid may include a coal slurry. In an embodiment, the coal slurry may include a slurry of pulverized coal having a concentration by weight of coal of about 2% to about 25%. For example, the concentration by weight of coal in the slurry may be about 2%, about 5%, about 10%, about 15%, about 20%, about 25%, and ranges between any two of these values (including endpoints). The concentration of coal may depend on various factors, such as the surface area to volume ratio within the reactor vessel, for example, to maximize the reaction kinetics therein.

[0036] The product source fluid may enter the pressure vessel **220** at various pressures, such as at various supercritical pressures. For example, the product source fluid may enter the pressure vessel **220** at a pressure of about 20 megapascals to about 35 megapascals. In further examples, the pressure may be about 20 megapascals, about 22 megapascals, about 25 megapascals, about 28 megapascals, about 30 megapascals, about 35 megapascals, about 40 megapascals, or ranges between any two of these values (including endpoints). In an embodiment, the product source fluid may enter the pressure vessel **220** at a pressure of about 22 megapascals to about 35 megapascals.

[0037] The product source fluid may enter the pressure vessel **220** at various temperatures, such as at various subcritical temperatures. For instance, the product source fluid may enter the pressure vessel **220** at a temperature of equal to or below about 300 °C. In an embodiment, the temperature may be about 200 °C to about 300 °C. In further examples, the temperature may be about 200 °C, about 250 °C, about 300 °C, or ranges between any two of these values (including endpoints). The product source fluid may enter

the pressure vessel **220** in a low-corrosive state, for instance, at a supercritical pressure and at a subcritical temperature.

[0038] The product source fluid may enter the pressure vessel **220** at various velocities or flow rates, for example, relative to the flow rate of the reactor fluid. According to some embodiments, the reactor fluid may enter the pressure vessel **220** at a flow rate of about 0.05 meters/second to about 10 meters/second. For example, the flow rate may be about 0.05 meters/second, about 0.5 meters/second, about 1 meter/second, about 2.5 meters/second, about 5 meters/second, about 10 meters/second, and ranges between any two of these values (including endpoints). In an embodiment, the flow rate of the reactor fluid may be about 0.5 meters/second to about 5 meters/second. According to some embodiments, the product source fluid may have a flow rate that is lower than the flow rate of the reactor fluid by about 5% to about 25%. For example, the flow rate of the product source fluid may be lower than the flow rate of the reactor fluid by about 5%, about 10%, about 15%, about 20%, about 25%, and ranges between any two of these values (including endpoints).

[0039] In an embodiment, the product source fluid may have a flow rate that is about 5% to about 25% greater than the flow rate of the surrounding reactor fluid, for instance, to maximize radial mixing and therefore, to achieve more efficient conversion of the product source fluid into product gases. In such an embodiment, the flow rate of the product source fluid may be greater than the flow rate of the reactor fluid by about 5%, about 10%, about 15%, about 20%, about 25%, and ranges between any two of these values (including endpoints). In an embodiment, the flow rate of the product source fluid may be about 20% greater than the flow rate of the surrounding reactor fluid.

[0040] In an embodiment, the reactor system may include one or more pumps, one or more heaters, and/or one or more heat exchangers in fluid communication with the

reactor vessel **200** to control the temperature, pressure, and/or flow rate of the product source fluid and/or the reactor fluid entering the reactor vessel.

[0041] The pressure vessel **220** and other components of the reactor vessel **200**, such as the product fluid inlet **210**, the reactor fluid inlet **215** and the outlet **225** may be fabricated from various materials. Illustrative and non-restrictive examples of such materials include common corrosion resistant metals and alloys thereof including, without limitation, nickel, chrome-molybdenum, non-magnetic iron, various ceramic materials, Inconel®, Hastelloy® N, stainless steel, titanium, and combinations thereof.

[0042] FIG. 2C depicts an illustrative product source fluid conversion process within a reactor vessel configured according to some embodiments. As shown in FIG. 2C, a product source fluid may enter the pressure vessel **220** through the product source fluid inlet **210**. According to some embodiments, the product source fluid may enter the pressure vessel **220** at a supercritical pressure and at a temperature below a corrosive temperature (for example, below a temperature in which a threshold level of corrosive ions are in solution). For example, the product source fluid may include a slurry of pulverized coal at a supercritical pressure of about 20 megapascals to about 30 megapascals and at a subcritical temperature of equal to or less than about 300 °C. In an embodiment, the product source fluid may include pulverized coal at a supercritical pressure of about 22 megapascals to about 30 megapascals. In an embodiment, the product source fluid may include pulverized coal at a subcritical temperature of about 200 °C to about 300 °C. The reactor fluid may enter the pressure vessel **220** through the reactor fluid inlet **215** at a supercritical pressure and supercritical temperature. For instance, the reactor fluid may include water at a pressure of about 22 megapascals to about 35 megapascals and at a supercritical temperature of about 650 °C. According to some embodiments, the temperature of the reactor fluid **220** within the pressure vessel **220** is above supercritical temperatures, for example, from about 375 °C to

about 900 °C. In an embodiment, the temperature of the reactor fluid may be about 600 °C to about 900 °C.

[0043] During the reactor process, one or more temperature zones **235-255** may be present within the reactor vessel **200** and components thereof. For example, the product source fluid inlet **210** may include a product source fluid temperature zone **255** including a product source fluid at a subcritical temperature. According to some embodiments, the product source fluid within the product source fluid inlet **210** may be heated by the reactor fluid flowing within the reactor fluid inlet **215** in contact with the product source fluid inlet. A supercritical temperature zone **245** may include a reactor fluid at a supercritical temperature, such as supercritical water at a temperature of about 650 °C to about 900 °C.

[0044] The product source fluid may enter the pressure vessel **220** encased by the reactor fluid. The product source fluid may be converted to reaction product substances, such as one or more gas products, by reacting with the reactor fluid within a reaction zone **240**. The temperature within the reaction zone **240** may be the temperature required to allow the product source fluid to react with the reactor fluid, for example, about 650 °C. As such, the temperature of the product source fluid may rise rapidly to the reaction temperature after entering the pressure vessel **220** and contacting the reactor fluid. The product source fluid may remain encased in the reactor fluid throughout all or substantially all of the conversion process. In this manner, the product source fluid at a supercritical temperature may not contact any surfaces of the reactor vessel **200**, such as the product source fluid inlet **210**, the inner surface of the pressure vessel **220** and/or the outlet **225**.

[0045] Gasification of the product source fluid may occur substantially within the portion of the reactor fluid inlet **215** below the opening **260** in the product source fluid inlet **210** (the “reaction zone”). For example, gasification may occur in about 30 seconds (the “gasification reaction time”) after the product source fluid contacts the reactor fluid within

the reactor fluid inlet **215**. The gasification reaction time may be influenced by various factors, such as the granularity and/or concentration of the product source fluid, size and shape of solid particles within the product source fluid, the velocity of the fluid flows, the temperature and/or pressure within the pressure vessel **220**, and/or the geometry of the pressure vessel. According to some embodiments, gasification may occur in about 1 seconds to about 60 seconds. For example, the gasification may occur in about 15 seconds, about 20 seconds, about 25 seconds, about 30 seconds, about 45 seconds, about 60 seconds, and ranges between any two of these values (including endpoints). According to some embodiments, the length of the reactor fluid inlet **215** may be determined based on, among other things, the flow rate of the product source fluid exiting from the opening **260** and the rate of conversion of the product source fluid.

[0046] The one or more reaction products, such as gas products, resulting from the conversion of the product source fluid may be dissolved in the reactor fluid. According to some embodiments, the pressure in the pressure vessel **220** may be about 22 megapascals to about 35 megapascals and the temperature may be about 650 °C +/- 50 °C. In an embodiment, the pressure in the pressure vessel **220** may be maintained at or above supercritical pressures. As such, the reactor fluid may remain in the supercritical state throughout the process depicted in FIG. 2C, and any gas products may remain dissolved in the fluid as it exits through the outlet **225**.

[0047] An outer reaction zone **250** may include fluid that is slightly less than the temperature of the reaction zone **240**. For instance, if the temperature of the reaction zone **240** is about 650 °C, then the temperature of the outer reaction zone **250** may be about 640 °C. The remainder of the pressure vessel **220** may include a sub-reaction zone **235** including fluid (for example, reactor fluid) at supercritical temperatures and supercritical pressures that may be lower than the temperatures and/or pressures with the reaction zones **240**, **250**. For

example, if the temperature of the reactor fluid entering the pressure vessel **220** is about 650 °C, then the temperature of the sub-reaction zone **235** may be less than about 650°C but greater than about 375°C. The reactor fluid and the product may flow from the reaction zone **240** out of the reactor through the outlet **225**.

[0048] The product source fluid may include certain inorganic salts, such as thorium, chloride salts, sulfate salts and phosphate salts. Such inorganic salts may be insoluble at temperatures within the sub-reaction zone **235**, the reaction zone **240** and/or the outer reaction zone **250**. As such, the inorganic salts may come out of solution and remain in a solid state as they fall within the pressure vessel **220** to the trap **230**. The flow of fluids within the pressure vessel **220** may be configured to facilitate the sedimentation of the dissolved inorganic salts, as well as char and other conversion waste products, within the trap **230**. For example, the flow rate of one or more fluids (for example, for the reactor fluid including one or more dissolved product gasses) may be reduced or reversed. In addition, sedimentation of salts and waste may be facilitated by rapid conversion times and the greater density of the salts and waste compared to the reactor fluid.

[0049] FIG. 3 depicts a flow diagram for an illustrative corrosion reduction method for a reactor system according to some embodiments. A reactor vessel may be provided **305** within a reactor system such as a supercritical water reactor system. An illustrative system vessel is the reactor vessel **110** depicted in FIG. 1. According to some embodiments, the reactor vessel may be configured to house a reaction converting a product source fluid into one or more reaction products.

[0050] The reactor vessel may be configured to receive **310** a reactor fluid through a reactor fluid inlet. A non-limiting example of a reactor fluid includes water, such as supercritical water. The reactor vessel may also be configured to receive **315** a product source fluid through a product source fluid inlet. Non-limiting examples of product source

fluids include a coal slurry, pulverized coal, a waste slurry, a toxic waste slurry, an e-waste slurry, a biomass slurry, and fluids including one or more fossil fuels. The product source fluid may, as the temperature increases, become corrosive to an inner surface of the reactor vessel. The product source fluid may be arranged **320** within the reactor fluid inlet such that the flow of the product source fluid into the reactor vessel is substantially surrounded by the reactor fluid. The reactor vessel may receive **325** the reactor fluid and the product source fluid such that the product source fluid reacts with the reactor fluid to generate reaction product substances. A barrier may be provided **330** between the product source fluid and the inner surface through the reactor fluid that substantially surrounds the product source fluid entering the reactor vessel. The reactor fluid and the reaction product substances may be discharged **335** from the reactor vessel through a product outlet. In an embodiment, the discharged reactor fluid may be re-used within the reactor system for another cycle of the reaction process.

EXAMPLES

Example 1: Supercritical Water Biomass Gasification System

[0051] A supercritical water biomass gasification system (“system”) will be configured to generate a synthesis gas including at least about 50% by volume of H₂ from a biomass slurry formed from organic plant waste.

[0052] The reactor vessel will be formed from a nickel alloy material and will have a substantially cylindrical shape with a height of about 3.5 meters and a diameter of about 2 meters. A water inlet pipe will allow supercritical water to enter the reactor vessel at a pressure of about 22 megapascals and a temperature of about 700 °C. The water inlet pipe will be located at a top portion of the reactor. The water inlet pipe will have a diameter of about 0.6 meters and will extend into the reactor vessel for about 1.5 meters. A slurry inlet pipe will be arranged within the water inlet pipe for the biomass slurry to enter the reactor

vessel at a pressure of about 25 megapascals and a temperature of about 250 °C. The slurry inlet pipe will be positioned substantially in the center of the water inlet pipe and will have a diameter of about 0.4 meters and will extend into the reactor vessel for about 0.75 meters. As such, 0.75 meters of the (reactor fluid) water inlet pipe will extend beyond the slurry inlet pipe into the reactor vessel to facilitate proper and managed mixing.

[0053] The supercritical water will flow into the reactor vessel at a flow rate of about 5 meters/second and the slurry will flow into the reactor vessel at a flow rate of about 1 meter/second. The flow of supercritical water into the reactor vessel will form a fluid layer having a thickness of about 2 centimeters that surrounds the biomass slurry and prevents the biomass slurry from contacting the inner surface of the water inlet pipe and the inner surface of the reactor vessel. The slurry will react with the supercritical water to form a gas product containing H₂ within a reaction zone that is located at least partially within the portion of the water inlet pipe extending beyond the slurry inlet pipe.

[0054] Waste products including char and precipitated inorganic salts will fall from the reaction zone and will be collected in a trap. The gas product will be dissolved in the supercritical water within the reactor vessel and will flow out of the reactor vessel through an outlet pipe and will be collected by a liquid/gas separator in fluid communication with the reactor vessel. The supercritical water will flow through the system to be used in another gasification cycle.

[0055] The flow of supercritical water surrounding the biomass slurry in the water inlet pipe and the reactor vessel will provide a barrier preventing the biomass slurry from contacting the inner surfaces thereof. Accordingly, the corrosive ions in the biomass slurry will not react with or cause corrosion of the inner surface of the water inlet pipe or the reactor vessel, prolonging the life of these components within the supercritical water biomass gasification system relative to a similar system lacking the dense fluid barrier.

Example 2: Supercritical Water Coal Reactor System

[0056] A manufacturer will use a supercritical water coal gasification system (“system”) to produce gas products including H_2 and CH_4 from a slurry of pulverized coal. The coal slurry will include 15% by weight of coal pulverized by a Babcock & Wilcox (of Charlotte, North Carolina, USA) Roll Wheeler™ coal pulverizer. The gas products will be used to generate electricity to power certain of the manufacturer’s facilities and excess electricity beyond the needs of the manufacturer will be sold on a regional electricity market.

[0057] The system will include a reactor vessel configured to provide a vessel for the reaction of the coal slurry with supercritical water to generate the gas products. A water heater and a water pump will be in fluid communication with the reactor vessel to generate supercritical water by heating water to a temperature of about 650 °C and pressurizing the water to about 28 megapascals before the water enters the reactor vessel. A coal slurry heater and a coal slurry pump will also be in fluid communication with the reactor vessel. The coal slurry heater will be configured to heat the coal slurry to about 300 °C and the coal slurry pump will be configured to pressurize the coal slurry to about 28 megapascals before the coal slurry enters the reactor vessel.

[0058] The reactor vessel will be formed substantially from Hastelloy® N and will have a cylindrical shape with a height of about 5 meters and a diameter of about 3 meters. The reactor vessel will include a water inlet pipe and a slurry inlet pipe formed substantially from titanium arranged at a top portion thereof. The water inlet pipe will extend into the reactor vessel for about 3 meters and will have a diameter of about 1 meter. The slurry inlet pipe will be arranged within the water inlet pipe to form an acceleration elbow having a ratio change in cross-sectional area of about 2:1. The slurry inlet pipe will extend into the reactor vessel within the water inlet pipe for about 1.5 meters.

[0059] The supercritical water contacting the slurry inlet pipe arranged therein will heat the coal slurry to about 300°C before the coal slurry exits the slurry inlet pipe. The coal slurry will exit the slurry inlet pipe and will be encased by the supercritical water within the water inlet pipe. The coal slurry will be heated to about 650 °C and will react with the supercritical water within the 1.5 meters of the water inlet pipe between the end of the slurry inlet pipe and the end of the water pipe to form the gas products. The gas products will be dissolved within the supercritical water within the body of the reactor vessel and will exit the reactor vessel through an outlet pipe.

[0060] The supercritical water will flow from the reactor vessel through a heat exchanger in which heat from the supercritical water will be captured to produce steam for power generation. The gas products will be recovered by passing the supercritical water through a liquid/gas separator and will be pumped through a piping system to a power generation plant to produce electricity.

[0061] The pressure and temperature of the coal slurry as it flows through the slurry inlet will be below a highly corrosive level. The coal slurry will enter the water inlet pipe and the reactor vessel encased in the supercritical water. As such, the higher-temperature, more corrosive coal slurry will not contact the inner surface of the water inlet pipe or the reactor vessel. The supercritical water surrounding the coal slurry in the water inlet pipe and the reactor vessel will provide a barrier preventing the coal slurry from contacting the inner surfaces thereof, prolonging the life of the reactor vessel compared to a similar system lacking the dense fluid barrier.

[0062] In the above detailed description, reference is made to the accompanying drawings, which form a part hereof. In the drawings, similar symbols typically identify similar components, unless context dictates otherwise. The illustrative embodiments

described in the detailed description, drawings, and claims are not meant to be limiting. Other embodiments may be used, and other changes may be made, without departing from the spirit or scope of the subject matter presented herein. It will be readily understood that the aspects of the present disclosure, as generally described herein, and illustrated in the Figures, can be arranged, substituted, combined, separated, and designed in a wide variety of different configurations, all of which are explicitly contemplated herein.

[0063] The present disclosure is not to be limited in terms of the particular embodiments described in this application, which are intended as illustrations of various aspects. Many modifications and variations can be made without departing from its spirit and scope, as will be apparent to those skilled in the art. Functionally equivalent methods and apparatuses within the scope of the disclosure, in addition to those enumerated herein, will be apparent to those skilled in the art from the foregoing descriptions. Such modifications and variations are intended to fall within the scope of the appended claims. The present disclosure is to be limited only by the terms of the appended claims, along with the full scope of equivalents to which such claims are entitled. It is to be understood that this disclosure is not limited to particular methods, reagents, compounds, compositions or biological systems, which can, of course, vary. It is also to be understood that the terminology used herein is for the purpose of describing particular embodiments only, and is not intended to be limiting.

[0064] With respect to the use of substantially any plural and/or singular terms herein, those having skill in the art can translate from the plural to the singular and/or from the singular to the plural as is appropriate to the context and/or application. The various singular/plural permutations may be expressly set forth herein for sake of clarity.

[0065] It will be understood by those within the art that, in general, terms used herein, and especially in the appended claims (for example, bodies of the appended claims) are generally intended as “open” terms (for example, the term “including” should be

interpreted as “including but not limited to,” the term “having” should be interpreted as “having at least,” the term “includes” should be interpreted as “includes but is not limited to”). While various compositions, methods, and devices are described in terms of “comprising” various components or steps (interpreted as meaning “including, but not limited to”), the compositions, methods, and devices can also “consist essentially of” or “consist of” the various components and steps, and such terminology should be interpreted as defining essentially closed-member groups. It will be further understood by those within the art that if a specific number of an introduced claim recitation is intended, such an intent will be explicitly recited in the claim, and in the absence of such recitation no such intent is present. For example, as an aid to understanding, the following appended claims may contain usage of the introductory phrases “at least one” and “one or more” to introduce claim recitations. However, the use of such phrases should not be construed to imply that the introduction of a claim recitation by the indefinite articles “a” or “an” limits any particular claim containing such introduced claim recitation to embodiments containing only one such recitation, even when the same claim includes the introductory phrases “one or more” or “at least one” and indefinite articles such as “a” or “an” (for example, “a” and/or “an” should be interpreted to mean “at least one” or “one or more”); the same holds true for the use of definite articles used to introduce claim recitations. In addition, even if a specific number of an introduced claim recitation is explicitly recited, those skilled in the art will recognize that such recitation should be interpreted to mean at least the recited number (for example, the bare recitation of “two recitations,” without other modifiers, means at least two recitations, or two or more recitations). Furthermore, in those instances where a convention analogous to “at least one of A, B, and C, et cetera” is used, in general such a construction is intended in the sense one having skill in the art would understand the convention (for example, “a system having at least one of A, B, and C” would include but not be limited to systems that have A alone, B

alone, C alone, A and B together, A and C together, B and C together, and/or A, B, and C together, et cetera). In those instances where a convention analogous to “at least one of A, B, or C, et cetera” is used, in general such a construction is intended in the sense one having skill in the art would understand the convention (for example, “a system having at least one of A, B, or C” would include but not be limited to systems that have A alone, B alone, C alone, A and B together, A and C together, B and C together, and/or A, B, and C together, et cetera). It will be further understood by those within the art that virtually any disjunctive word and/or phrase presenting two or more alternative terms, whether in the description, claims, or drawings, should be understood to contemplate the possibilities of including one of the terms, either of the terms, or both terms. For example, the phrase “A or B” will be understood to include the possibilities of “A” or “B” or “A and B.”

[0066] In addition, where features or aspects of the disclosure are described in terms of Markush groups, those skilled in the art will recognize that the disclosure is also thereby described in terms of any individual member or subgroup of members of the Markush group.

[0067] As will be understood by one skilled in the art, for any and all purposes, such as in terms of providing a written description, all ranges disclosed herein also encompass any and all possible subranges and combinations of subranges thereof. Any listed range can be easily recognized as sufficiently describing and enabling the same range being broken down into at least equal halves, thirds, quarters, fifths, tenths, or the like. As a non-limiting example, each range discussed herein can be readily broken down into a lower third, a middle third, and an upper third. As will also be understood by one skilled in the art all language such as “up to,” “at least,” and the like include the number recited and refer to ranges which can be subsequently broken down into subranges as discussed above. Finally, as will be understood by one skilled in the art, a range includes each individual member.

Thus, for example, a group having 1-3 cells refers to groups having 1, 2, or 3 cells. Similarly, a group having 1-5 cells refers to groups having 1, 2, 3, 4, or 5 cells, and so forth.

[0068] Various of the above-disclosed and other features and functions, or alternatives thereof, may be combined into many other different systems or applications. Various presently unforeseen or unanticipated alternatives, modifications, variations or improvements therein may be subsequently made by those skilled in the art, each of which is also intended to be encompassed by the disclosed embodiments.

CLAIMS*What Is Claimed Is:*

1. A reactor system configured to reduce corrosion of portions thereof, the system comprising:

at least one reactor vessel comprising an inner surface, the at least one reactor vessel configured to receive a reactor fluid through at least one reactor fluid inlet and to receive a product source fluid corrosive to at least a portion of the inner surface through at least one product source fluid inlet; and

at least one product outlet configured to provide a discharge path for the reactor fluid and reaction product substances generated by a reaction of the product source fluid with the reactor fluid within the at least one reactor vessel,

wherein the at least one product source fluid inlet is arranged within at least a portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by a flow of the reactor fluid, the reactor fluid thereby operating to reduce corrosion by forming a barrier between the product source fluid and the at least a portion of the inner surface.

2. The system of claim 1, wherein the reactor system is configured as a supercritical water reactor system.

3. The system of claim 1, wherein the reactor fluid comprises supercritical water.

4. The system of claim 1, wherein the product source fluid comprises a slurry.

5. The system of claim 1, wherein the reactor fluid is disposed within at least a portion of the at least one reactor vessel.

6. The system of claim 1, wherein the product source fluid is disposed within at least a portion of the at least one reactor vessel.

7. The system of claim 1, wherein the reactor system is configured as one of: a coal gasification system, a biomass gasification system, a toxic waste gasification system, an electronic waste oxidation system, and a waste oxidation system.

8. The system of claim 1, wherein the reactor system is configured as a coal gasification system, and the product source fluid comprises a coal slurry.

9. The system of claim 1, wherein the reactor system is configured as a biomass gasification system, and the product source fluid comprises a biomass slurry.

10. The system of claim 1, wherein the at least one reactor vessel is configured to receive the reactor fluid at a temperature of about 600 °C to about 900 °C.

11. The system of claim 1, wherein the at least one reactor vessel is configured to receive the reactor fluid at a pressure of about 22 megapascals to about 35 megapascals.

12. The system of claim 1, wherein the at least one reactor vessel is configured to receive the product source fluid at a temperature equal to or below about 300 °C.

13. The system of claim 1, wherein the at least one reactor vessel is configured to receive the product source fluid at a pressure of about 22 megapascals to about 35 megapascals.

14. The system of claim 1, further comprising at least one pump in fluid communication with the at least one product source fluid inlet and configured to increase a pressure of the product source fluid entering the at least one reactor vessel.

15. The system of claim 1, further comprising at least one heater in fluid communication with the at least one product source fluid inlet and configured to increase a temperature of the product source fluid entering the at least one reactor vessel.

16. The system of claim 1, wherein the barrier has a thickness of about 1 centimeter to about 5 centimeters.

17. The system of claim 1, wherein the at least one reactor vessel is configured such that a flow rate of the product source fluid within the at least one reactor vessel is about 20% greater than a flow rate of the surrounding reactor fluid at least within a reaction zone of the at least one reactor vessel.

18. The system of claim 1, wherein a flow rate of the reactor fluid is about 0.5 meters/second to about 5 meters/second.

19. The system of claim 1, wherein a flow rate of the product source fluid is about 0.5 meters/second to about 5 meters/second.

20. The system of claim 1, wherein at least a portion of the reactor product substances comprises a fuel gas.

21. The system of claim 20, wherein the fuel gas comprises H₂, CH₄, CO, CO₂, or a combination thereof.

22. The system of claim 1, further comprising a trap configured to receive reaction waste substances.

23. The system of claim 22, wherein the reaction waste substances comprise salts, char, or a combination thereof.

24. The system of claim 1, wherein the at least one reactor fluid inlet and the at least one product source fluid inlet are configured as a venturi elbow arrangement.

25. The system of claim 1, wherein the at least one product source fluid inlet is arranged within the at least one reactor fluid inlet and the at least one reactor fluid inlet extends beyond the at least one product source fluid inlet into the at least one reactor vessel by a distance.

26. The system of claim 25, wherein the distance comprises about 0.25 meters to about 2 meters.

27. The system of claim 1, wherein the product source fluid reacts with the reactor fluid within the at least one reactor fluid inlet.

28. The system of claim 1, wherein the at least one reactor fluid inlet extends beyond the at least one product source fluid inlet into the at least one reactor vessel, thereby forming a reaction zone in an area of the at least one reactor fluid inlet where the at least one product source fluid inlet does not extend within the at least one reactor fluid inlet.

29. The system of claim 28, wherein the product source fluid reacts with the reactor fluid within the reaction zone.

30. A method of reducing corrosion in a reactor system, the method comprising:

providing at least one reactor vessel comprising an inner surface, the at least one reactor vessel being configured to receive a reactor fluid through at least one reactor fluid inlet and to receive a product source fluid corrosive to at least a portion of the inner surface through at least one product source fluid inlet, wherein at least a portion of the at least one product source fluid inlet is arranged within at least a

portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by the reactor fluid;

receiving the reactor fluid at the at least one reactor vessel through the at least one reactor fluid inlet;

receiving the product source fluid at the at least one reactor vessel through the at least one product source fluid inlet such that the product source fluid reacts with the reactor fluid to generate reaction product substances, wherein corrosion is reduced by the reactor fluid forming a barrier between the product source fluid and the at least a portion of the inner surface; and

discharging the reactor fluid and the reaction product substances through at least one product outlet.

31. The method of claim 30, wherein the reactor system is configured as a supercritical water reactor system.

32. The method of claim 30, wherein the reactor fluid comprises supercritical water.

33. The method of claim 30, wherein the product source fluid comprises a slurry.

34. The method of claim 30, wherein the reactor system is configured as one of: a coal gasification system, a biomass gasification system, and a waste oxidation system.

35. The method of claim 30, wherein the reactor system is configured as a coal gasification system, and the product source fluid comprises a coal slurry.

36. The method of claim 30, wherein the reactor system is configured as a biomass gasification system, and the product source fluid comprises a biomass slurry.

37. The method of claim 30, wherein the reactor fluid enters the at least one reactor vessel at a temperature of about 600 °C to about 900 °C.

38. The method of claim 30, wherein the reactor fluid enters the at least one reactor vessel at a pressure of about 22 megapascals to about 35 megapascals.

39. The method of claim 30, wherein the product source fluid enters the at least one reactor vessel at a temperature equal to or below about 300 °C.

40. The method of claim 30, wherein the product source fluid enters the at least one reactor vessel at a pressure of about 22 megapascals to about 35 megapascals.

41. The method of claim 30, wherein the flow of the reactor fluid is about 0.5 meters/second to about 5 meters/second.

42. The method of claim 30, wherein the flow of the product source fluid is about 0.5 meters/second to about 5 meters/second.

43. The method of claim 30, wherein a flow rate of the product source fluid within the at least one reactor vessel is about 20% greater than a flow rate of the surrounding reactor fluid at least within a reaction zone of the at least one reactor vessel.

44. The method of claim 30, wherein at least a portion of the reactor product substances comprises a fuel gas.

45. The method of claim 44, wherein the fuel gas comprises H₂, CH₄, CO, CO₂, or a combination thereof.

46. The method of claim 30, further comprising providing at least one trap configured to receive reaction waste substances.

47. The method of claim 46, wherein the reaction waste substances comprise salts, char, or a combination thereof.

48. The method of claim 30, further comprising configuring the at least one reactor fluid inlet and the at least one product source fluid inlet as a venturi elbow arrangement.

49. The method of claim 30, wherein the product source fluid reacts with the reactor fluid within the at least one reactor fluid inlet.

50. A method of manufacturing a reactor system configured to reduce corrosion thereof, the method comprising:

providing at least one reactor vessel comprising an inner surface;

configuring the at least one reactor vessel to receive a reactor fluid through at least one reactor fluid inlet;

configuring the at least one reactor vessel to receive a product source fluid corrosive to at least a portion of the inner surface through at least one product source fluid inlet;

arranging the at least one product source fluid inlet within at least a portion of the at least one reactor fluid inlet such that a flow of the product source fluid within the at least one reactor vessel is substantially surrounded by a flow of the reactor fluid, the reactor fluid thereby operating to reduce corrosion by forming a barrier between the product source fluid and the at least a portion of the inner surface; and

configuring at least one product outlet to discharge the reactor fluid and reaction product substances generated by a reaction of the product source fluid with the reactor fluid within the at least one reactor vessel.

51. The method of claim 50, wherein the reactor system is configured as a supercritical water reactor system.

52. The method of claim 50, wherein the reactor fluid comprises supercritical water.

53. The method of claim 50, wherein the product source fluid comprises a slurry.

54. The method of claim 50, wherein the reactor system is configured as one of: a coal gasification system, a biomass gasification system, and a waste oxidation system.

55. The method of claim 50, wherein the reactor system is configured as a coal gasification system, and the product source fluid comprises a coal slurry.

56. The method of claim 50, wherein the reactor system is configured as a biomass gasification system, and the product source fluid comprises a biomass slurry.

57. The method of claim 50, further comprising configuring the at least one reactor vessel to receive the reactor fluid at a temperature of about 600 °C to about 900 °C.

58. The method of claim 50, further comprising configuring the at least one reactor vessel to receive the reactor fluid at a pressure of about 22 megapascals to about 35 megapascals.

59. The method of claim 50, further comprising configuring the at least one reactor vessel to receive the product source fluid at a temperature below about 300 °C.

60. The method of claim 50, further comprising configuring the at least one reactor vessel to receive the product source fluid at a pressure of about 22 megapascals to about 35 megapascals.

61. The method of claim 50, further comprising configuring the at least one reactor vessel such that the flow of the reactor fluid is about 0.5 meters/second to about 5 meters/second.

62. The method of claim 50, further comprising configuring the at least one reactor vessel such that the flow of the product source fluid is about 0.5 meters/second to about 5 meters/second.

63. The method of claim 50, further comprising configuring the at least one reactor vessel such that a flow rate of the product source fluid within the at least one reactor vessel is about 20% greater than a flow rate of the surrounding reactor fluid at least within a reaction zone of the at least one reactor vessel.

64. The method of claim 50, wherein at least a portion of the reactor product substances comprises a fuel gas.

65. The method of claim 64, wherein the fuel gas comprises H_2 , CH_4 , CO , CO_2 , or a combination thereof.

66. The method of claim 50, further comprising providing at least one trap configured to receive reaction waste substances.

67. The method of claim 66, wherein the reaction waste substances comprise salts, char, or a combination thereof.

68. The method of claim 50, further comprising configuring the at least one reactor fluid inlet and the at least one product source fluid inlet as a venturi elbow arrangement.

69. The method of claim 50, further comprising configuring the at least one reactor fluid inlet and the at least one product source fluid inlet such that the product source fluid reacts with the reactor fluid within the at least one reactor fluid inlet.

70. The method of claim 50, further comprising configuring the at least one reactor fluid inlet to extend beyond the at least one product source fluid inlet into the at least one reactor vessel, thereby forming a reaction zone in an area of the at least one reactor fluid inlet where the at least one product source fluid inlet does not extend within the at least one reactor fluid inlet.

71. The system of claim 70, wherein the product source fluid reacts with the reactor fluid within the reaction zone.

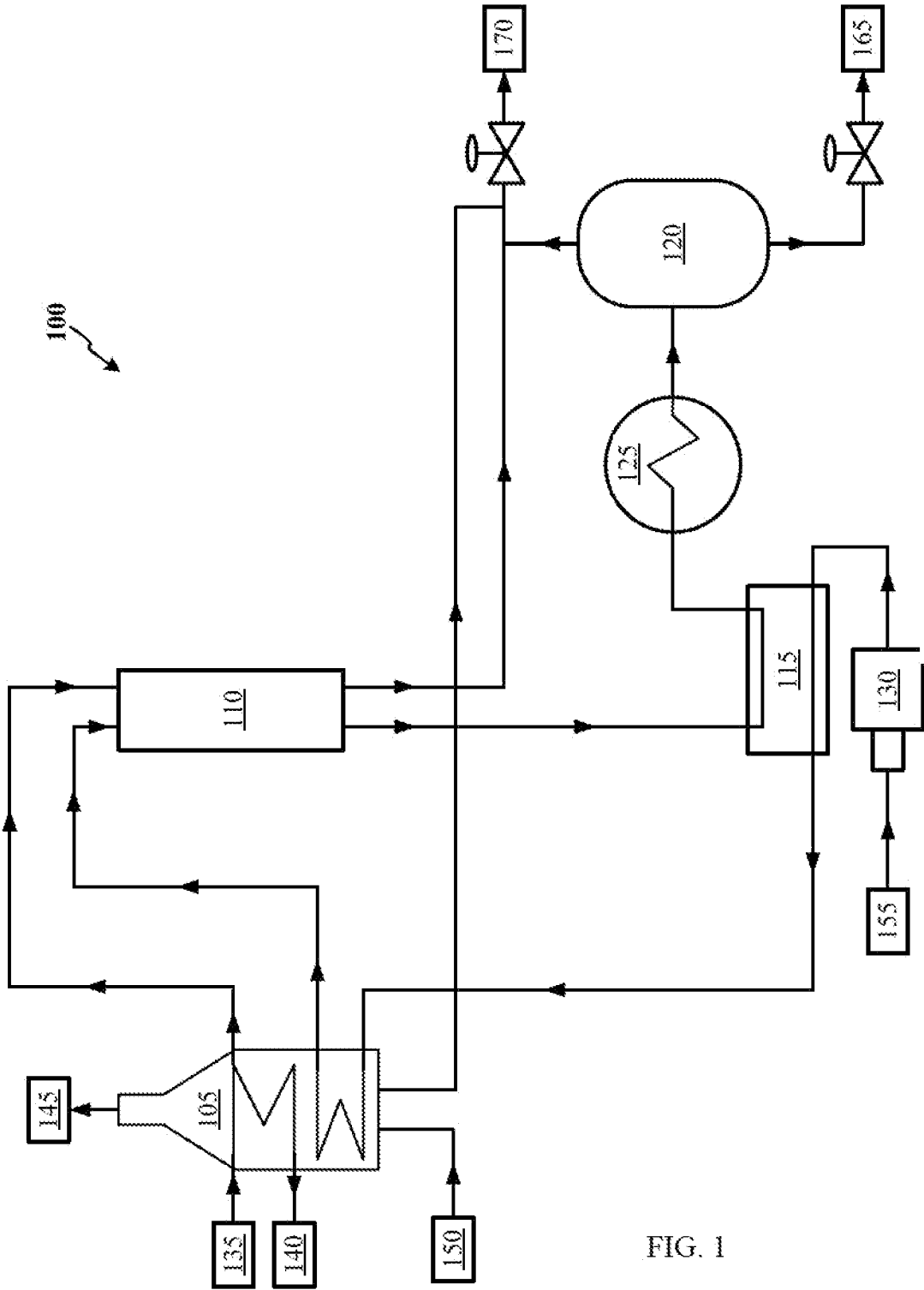


FIG. 1

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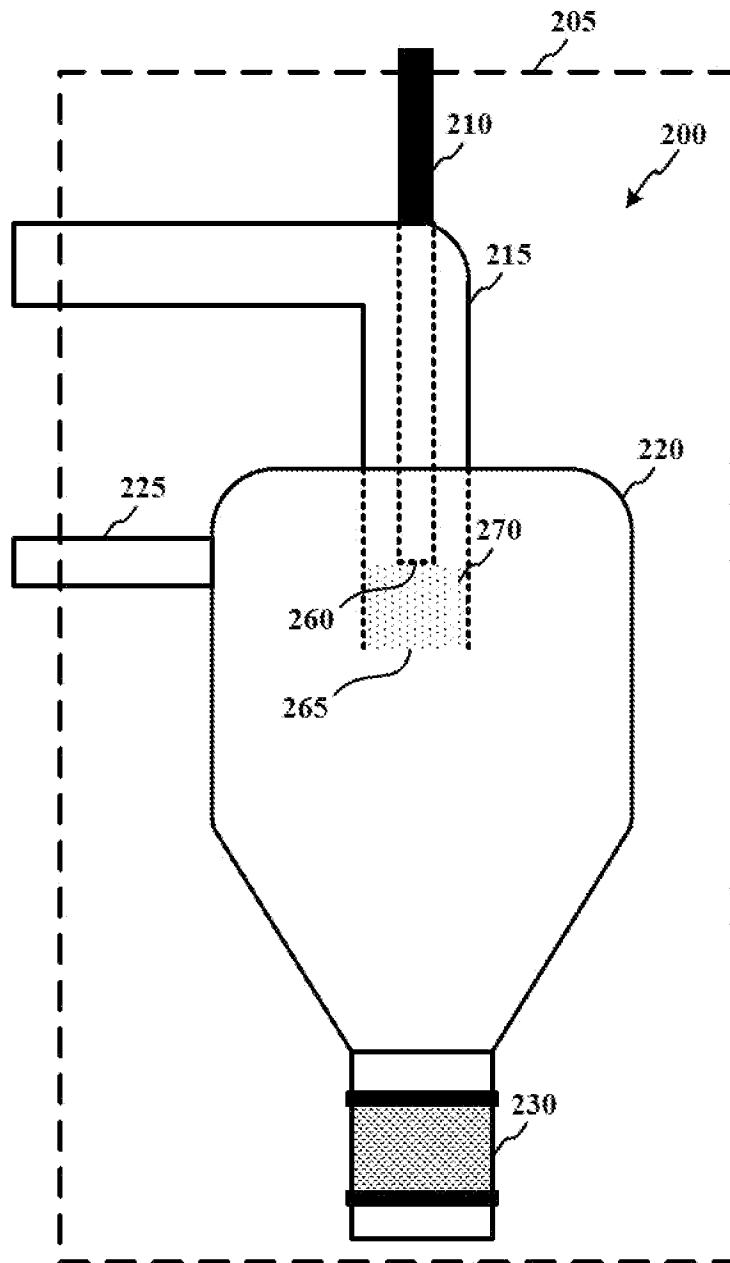


FIG. 2A

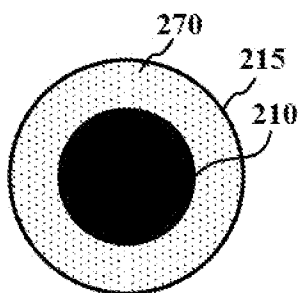


FIG. 2B

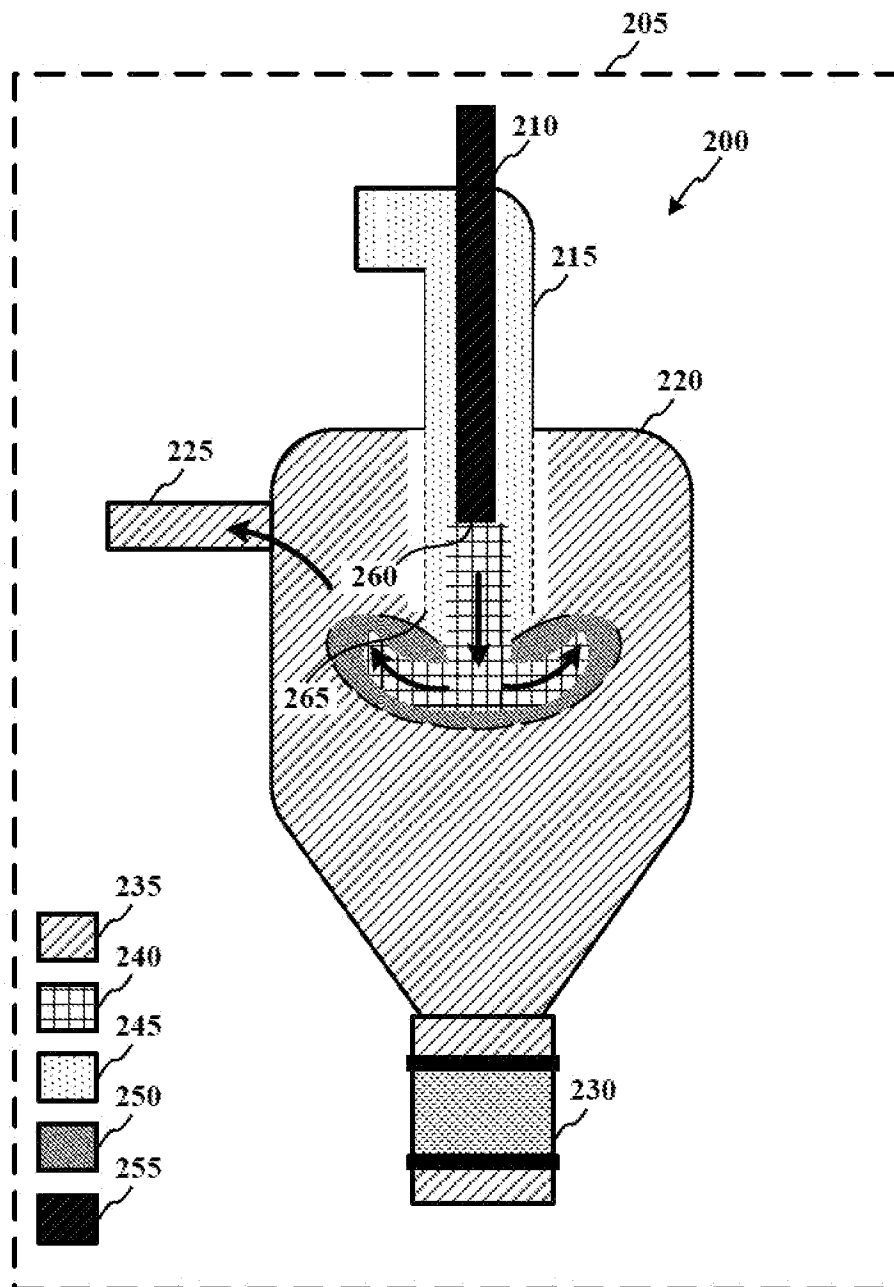


FIG. 2C

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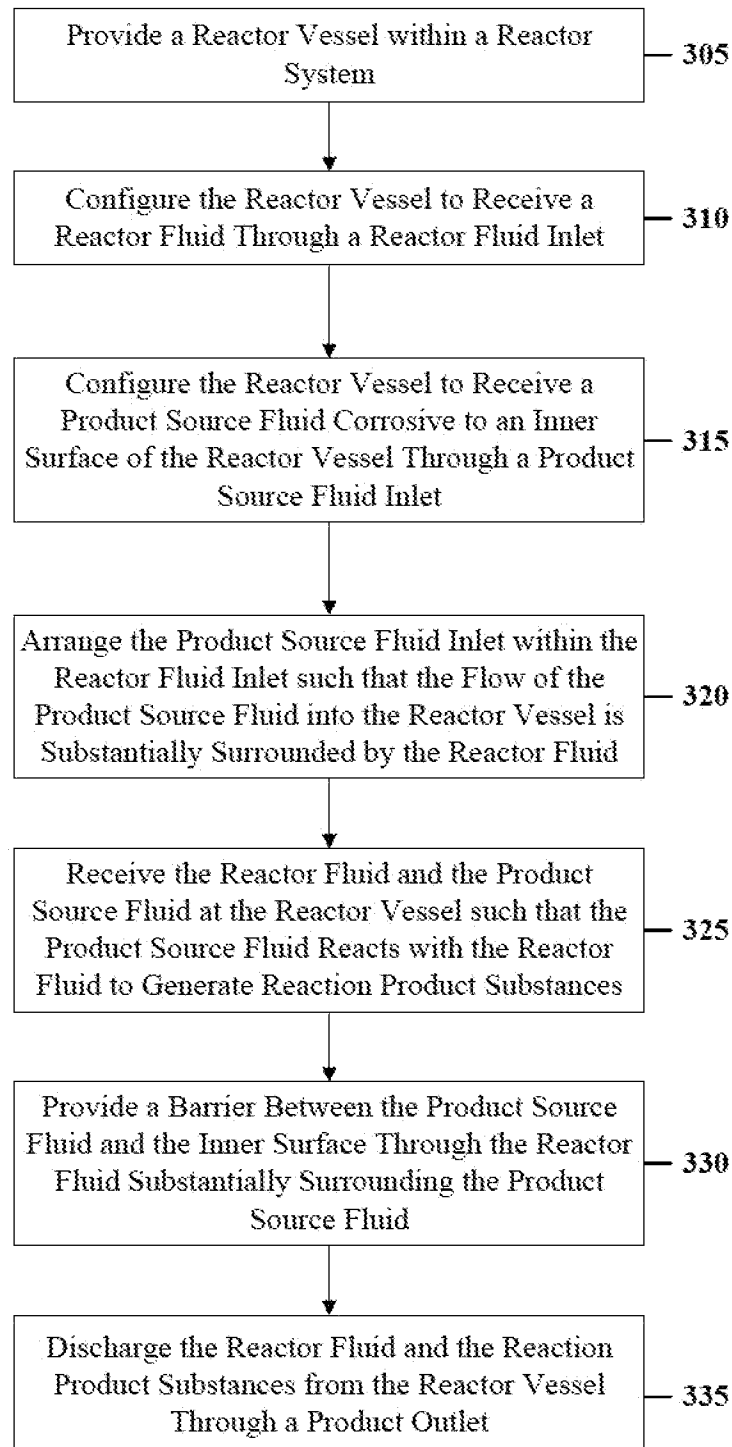


FIG. 3

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US13/51613

A. CLASSIFICATION OF SUBJECT MATTER

IPC(8) - C02F 11/08, 1/02, 1/68 (2013.01)

USPC - 210/761, 765, 766

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC(8): C02F 11/08, 1/02, 1/68, 1/72; B01J 19/24, 19/26, 3/02, 3/04 (2013.01)

USPC: 210/761, 765, 766, 774; 588/320, 405; 422/182, 232; 239/424, 422

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

MicroPatent (US Granted, US Applications, EP-A, EP-B, WO, JP, DE-G, DE-A, DE-T, DE-U, GB-A, FR-A); Google; Google Scholar; ProQuest; Supercritical, water, H₂O, reactor, gasification, waste, system, SCW, inlet, injector, nozzle, feed, jet, annulus, concentric, waste, product, inner, center, central, corrosion, surrounded, shrouded, enveloped, covered, shielded

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X --- Y	US 6709601 B2 (WOFFORD, III, WT et al.) March 23, 2004; figures 1, 3; column 1, lines 60-65; column 4, lines 60-67; column 5, lines 5-10; column 6, lines 35-40; column 7, lines 5-35; column 8, lines 15-35; column 9, lines 30-35; column 11, lines 65-67	1-15, 17-24, 30-48, 50-68 ----- 16, 25-29, 49, 69-71
Y	US 5591415 A (DASSEL, MW et al.) January 7, 1997; figure 4; column 12, lines 40-45; column 16, lines 65-67; column 17, lines 20-35	16, 25-29, 49, 69-71
X	US 5804066 A (MUEGGENBURG, HH et al.) September 8, 1998; entire document	1, 30, 50
A	EP 0135144 A1 (CHOWDHURY, AK) March 27, 1985; entire document	1-71
A	US 5437798 A (LAROCHE, HL et al.) August 1, 1995; entire document	1-71
A	US 2010/0018933 A1 (TITMAS, J) January 28, 2010; entire document	1-71
A	US 5558783 A (MCGUINNESS, TG) September 24, 1996; entire document	1-71

☐ Further documents are listed in the continuation of Box C.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"E" earlier application or patent but published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"&" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

16 December 2013 (16.12.2013)

Date of mailing of the international search report

23 DEC 2013

Name and mailing address of the ISA/US

Mail Stop PCT, Attn: ISA/US, Commissioner for Patents
P.O. Box 1450, Alexandria, Virginia 22313-1450
Facsimile No. 571-273-3201

Authorized officer:

Shane Thomas

PCT Helpdesk: 571-272-4300
PCT OSP: 571-272-7774