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(54) **PROCESS FOR PREPARING COLD WATER SWELLING PHOSPHATE-CROSS-LINKED GELATINISED STARCH**

VERFAHREN ZUR HERSTELLUNG VON IN KALTEM WASSER QUELLBARER, MIT PHOSPHAT VERNETZTER, GELATINISIERTER STÄRKE

PROCÉDÉ DE PRÉPARATION D'AMIDON GÉLATINISÉ RÉTICULÉ PAR DES LIAISONS PHOSPHATÉES ET GONFLANT À L'EAU FROIDE

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Description

[0001] The invention relates to a continuous process for preparing cold water swelling phosphate-cross-linked (pre-)gelatinised starch derivatives.

[0002] Currently, phosphate-cross-linked starches have been prepared by reacting starch with a polyphosphate or a phosphorus oxychloride reagent, for instance POCl_3 .

[0003] In US 2,852,393 and US 2,801,242, procedures are disclosed using sodium trimetaphosphate (STMP) as the cross-linking agent. Thereby, granular cross-linked starches are disclosed which may swell but which do not disintegrate.

[0004] In US 2,328,537 and US 2,754,232, the use of POCl_3 as cross-linking agent is disclosed as an alternative to STMP. The purpose of this cross-linking process is to provide a starch derivative which is more resistant to gelatinisation while pastes thereof have increased stability with regard to breakdown by heating, compared to untreated starches.

[0005] In a later stage, such phosphate-cross-linked starches have been further processed in order to obtain pre-gelatinised cold water swelling derivatives. Such instant derivatives are described in US 5,187,272 and US 4,219,646. These starches are used in convenience food applications such as sauces or microwaveable products or as thickeners for instant pudding formulations. These pre-gelatinised cross-linked starches are obtained by spray cooking or drum drying, but also extrusion processes have been used such as disclosed in WO 97/00620 or EP 0 358 444. In these patent documents, the role of the extrusion process is to gelatinise the starch and at the same time to cause some variable molecular degradation.

[0006] Thus, the prior art industrial processes as described above have a number of drawbacks:

- when using an aqueous reaction medium, a lot of polluted water is generated and this water has to be treated by a waste water treatment unit whereby part of the starch is lost;
- these processes are two-step processes which consume a lot of energy and demands for a high investment cost for the process equipment;
- it is also known that the cross-linking reaction is less efficient when performed in wet conditions wherein a water content of above 50 % water is present, this in comparison with reactions performed in (semi) dry conditions, wherein a water content of between 20 - 50 % is present, because water degrades and reacts with the cross-linking agent;
- it is proven that the chemical modification of starch is less homogeneous when the reaction is performed on granular starch. A less homogeneous reaction means that some amylase and/or amylopectin chains are not cross-linked, what means that these chains, when they are realised during cooking, are less resistant against more severe pH, temperature and shear conditions.

[0007] Reactive extrusion (wherein the reaction is performed in the extruder) using phosphate-containing reagent has been disclosed in EP 0 396 226 and WO 2004/108813. In EP 0 396 226, a glass-like cross-linked starch is prepared to be used as a paint stripping agent. These modified starches therein do not have cold swelling properties. In WO 2004/108813, rye flour is modified with SMTP, thereby providing a modified flour showing improved suspension properties. This modified flour is used in paper sizing applications.

[0008] Reactive extrusion has also been described in the scientific and technical literature. In the "Journal of Food Process Engineering (2003)" and in "Carbohydrate Polymers (2005, M. Seker and M.A. Hanna) discuss the cross-linking reaction of starch in a single screw extruder. In both cases, cross-linking is performed using STMP as the reagent. Quite high concentrations of STMP are needed to provide products showing instant thickening properties. When food applications are considered, excess phosphate salts need to be removed, thereby requiring an additional purification step.

[0009] A purpose of this invention is therefore to provide an improved and simpler continuous process for preparing cold water swelling phosphate-cross-linked gelatinised starch derivatives which can be used as thickeners in food or non-food applications or as adhesives thereby overcoming the abovementioned shortcomings, including a limited number of steps, a lower consumption of energy, a reduced quantity of waste water production and a reduced chemical consumption.

[0010] The purpose of the invention is solved by providing a continuous extrusion process for preparing cold water swelling phosphate-cross-linked gelatinised starch derivatives, wherein the process consists of the subsequent steps of

- gelatinising an alkaline starch in a first zone in the extruder;
- adding POCl_3 as cross-linking reagent in a second zone in the extruder;
- cross-linking the obtained gelatinised starch by means of POCl_3 in the second and third zone in the extruder, and
- neutralising the obtained cross-linked gelatinised starch that is present in a fourth zone in the extruder;
- recovering the obtained cross-linked, gelatinised starch in a fifth zone in the extruder.

[0011] With this process, first of all the number of steps is reduced to one step, and a lower consumption of energy, a reduced quantity of waste water production and a reduced chemical consumption is obtained.

[0012] Further advantages of this process is that cross-linked starches are obtained which

- can be used in both food and non-food applications,
- are gelatinised, cross-linked and neutralised at the same time;
- have different properties than starches that are first cross-linked and afterwards are gelatinized via drum drying, spray-cooking or extrusion.

[0013] In a preferred continuous extrusion process according to the invention, the process consists of the subsequent steps of

- continuously feeding the alkaline starch into a first partial zone of the said first zone in the extruder, the temperature in the first zone being between $20\text{ °C} \pm 3\text{ °C}$;
- continuously feeding an extra amount of water to the alkaline starch in a second partial zone of the said first zone in the extruder in a ratio of dry weight starch versus water of between 70:30 and 50:50, at a temperature of between 55 and 65 °C ;
- kneading the alkaline starch/water mixture in a third partial zone of the said first zone in the extruder at a temperature of about 100 °C through which a gelatinised starch is obtained;
- continuously feeding POCl_3 to the gelatinised starch in the second zone in the extruder wherein the temperature is about $100\text{ °C} \pm 5\text{ °C}$;
- cross-linking the gelatinised starch in the second and in the third zone in the extruder through which a cross-linked, gelatinised starch is obtained;
- neutralising the cross-linked, gelatinised starch in the fourth zone in the extruder;
- recovering the cross-linked, gelatinised starch in the fifth zone in the extruder.

[0014] In a favourable continuous extrusion process according the invention, after the recovered cross-linked, gelatinised starch is cooled to substantially room temperature, it is further reduced in size.

[0015] The needed specific mechanical input of the continuous extrusion process is situated between 350 and 1000 kJ/kg.

[0016] More preferably, the needed specific mechanical input of the continuous extrusion process is situated between 450 and 750 kJ/kg.

[0017] In a preferred embodiment of a continuous extrusion process according the invention, the ratio of dry weight starch versus water in the second partial zone of the first zone in the extruder is between 70:30 and 50:50. With the expression "dry weight starch" is meant 100% dry starch.

[0018] The cross-linking of the obtained gelatinised starch by means of POCl_3 in the second and third zone in the extruder is preferably performed at temperatures measured and monitored between 70 °C and 90 °C .

[0019] In an advantageous continuous extrusion process according to the invention, the cross-linking of the obtained gelatinised starch by means of POCl_3 in the second and third zone in the extruder is performed at temperatures measured and monitored between 75 °C and 85 °C .

[0020] In a preferred embodiment of a continuous extrusion process according to the invention, the further reduction of the recovered and cooled cross-linked gelatinised starch is done by milling.

[0021] Preferably, the continuous feeding of an alkaline starch is performed by means of a dosing system.

[0022] In a favourable continuous extrusion process according to the invention, the extrusion process is performed using a single screw, a twin screw co-rotating or a twin screw counter-rotating configuration in the extruder.

[0023] In a preferred embodiment of the invention extruder screw configuration is provided allowing the performing of the continuous process for preparing cold water swelling phosphate-cross-linked gelatinised starch derivatives according to the invention, wherein

- the first zone consists of
 - a first and second partial zone composed of Z-flight conveying elements;
 - a third partial zone composed of Z-flight conveying elements followed by a kneading block part;
- the second zone is composed of conveying elements in combination with a further kneading block;
- the third zone is composed of Z-flight conveying elements;
- the fourth zone is composed of conveying elements and a mixing block; and
- the fifth zone consists of a screw tip, wherein the mixing block of the fourth zone is just in front of the said screw tip.

[0024] The extruder screw configuration according to the invention is preferably provided for performing a continuous extrusion process according to the invention as described above.

[0025] This invention will now be illustrated by the following graphs and examples which should be considered as being not limiting to the scope of the invention as such and as expressed in the following claims, wherein reference numerals are used to refer to the attached drawings, wherein

- in figure 1 the viscosity development of two known starches and one starch according to the invention at 30 °C over a period for 60 minutes in a RVA-equipment at 160 rpm is shown;
- in figure 2 the viscosity development of two known starches and one starch according to the invention is shown, in a RVA-equipment at 160 rpm, when submitted to a temperature profile: 10 minutes at 30°C, heating from 30°C to 95°C within 10 minutes, holding at 95°C during 6 minutes, cooling from 95°C to 30°C within 10 minutes and holding at 30°C for 10 minutes ;
- in figure 3 a first embodiment of a screw configuration which is provided to perform a continuous extrusion process according to the invention is shown;
- in figure 4 a second embodiment of a screw configuration which is provided to perform a continuous extrusion process according to the invention is shown.

[0026] Rheological properties of the phosphate cross-linked, gelatinised starches of the invention are illustrated in figures 1 and 2.

[0027] In figure 1, a product of the invention (1) is compared with a starch (2) which has been cross-linked in slurry followed by gelatinisation on a drum drier (Merigel 310), and a starch (3) which has been cross-linked in slurry followed by gelatinisation in an extruder (Resistamyl 310 extruded).

[0028] In figure 2, the same three starch derivatives (1, 2 and 3) were evaluated when submitted to a cooking step.

[0029] In figure 1 as well as in figure 2, in curve (4) the temperature in °C and in curve (5), the speed in rpm have been set out.

[0030] Furthermore, it should be emphasized that, compared to prior art methods using STMP in reactive extrusion processes, the process of the invention uses up to 10 times less reagent in order to obtain the same cross-linking degree. As a result thereof, residual phosphate is almost non-existing thereby allowing the use of the starches of the invention in food application, this without additional and costly purification steps.

EXAMPLES

Experimental set-up

[0031] The reaction is performed using the following extruder set-up:

- Co-rotating twin screw extruder (Berstorff ZE40*38D).
- Diameter screw is 40 mm.
- Length of the extruder is 38 times the diameter (L/D = 38).
- Throughput alkaline starch is about 10 kg/h.
- To add the very small quantities of the cross-linking reagent POCl₃ and neutralising agent (for neutralising the cross-linked, gelatinised starch in the fourth zone in the extruder), special HPLC pumps are used.
- A die with two holes of 4 mm is used.
- A screw configuration design as shown in figures 3 and 4 is used, wherein each screw configuration consists of
 - first zone (10) consisting of
 - * a first and second partial zone (10a, 10b) composed of Z-flight conveying elements;
 - * a third partial zone (10c) composed of Z-flight conveying elements followed by a kneading block part;
 - a second zone (11) composed of conveying elements in combination with a further kneading block;
 - a third zone (12) composed of Z-flight conveying elements;
 - a fourth zone (13) composed of conveying elements and a mixing block; and
 - a fifth zone (14) consisting of a screw tip, wherein the mixing block of the fourth zone is just in front of the said screw tip.
- Screw speed is 200 rpm.

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- Minimum water content of the starch during extrusion is 35 % (more preferable about 40 %).
- Temperature set-point of the reaction zone is 80-90 °C.
- Reaction time is 30 seconds - 1 minute.
- With this set up the Specific Mechanical Energy to produce the product is between 0.10 and 0.3 kWh/kg

Alkaline starch

[0032] Alkaline waxy corn starch is prepared by spraying a 25 w/w% NaOH solution onto commercial waxy corn starch (11-13% moisture) in a Lödige continuous mixer (CP20 PI). The amount of NaOH sprayed onto the starch is between 0.2 - 2.2 % on dry starch. The alkaline starch is used as is.

Extrusion

[0033]

1. Load the alkaline starch into the extruder with the aid of a double screw dosing system (K-Tron) at a rate of 172 g/min commercial product (e.g. 150 g/min dry substance). The alkaline starch is entering the extruder in the first partial zone (10a) of the first zone (10). The temperature in zone 1 is 20 °C +/- 3%.
2. An extra amount of water (75 g/min) is added to the alkaline starch in the second partial zone (10b) of the first zone (10). This extra amount of water allows the starch to swell out completely or almost completely (at least 90 % of the granules are gelatinized). The total amount of water entering the extruder is 97 g/min (sum of pure water + water fixed onto the starch) resulting in an alkaline starch dry substance concentration of 60.7%. The temperature in this second partial zone (10b) is 61 °C +/- 3%.
3. The alkaline starch/water mixture is well kneaded in the third partial zone (10c) of the first zone (10) (99 °C +/- 3%). The starch swells out in this zone.
4. Mix 0.23 g/min of POCl₃ (0.16% POCl₃ w/w on dry starch) into the gelatinized alkaline starch. The introduction of POCl₃ into the extruder is done with the aid of a HPLC pump which is able to overcome the pressure present in the extruder. The addition of POCl₃ is done in the second zone (11) in the extruder. The temperature in this zone is set at 100 °C +/- 3%. The cross-linking reaction is taking place in the second and third zone (11, 12) in the extruder.
5. The cross-linking reaction is stopped by neutralizing the reaction mixture. This is done in the fourth zone (13) in the extruder where 9.0 g/min HCl (9.25 % w/w) is introduced into the reaction mixture. This is done with a pump which is able to overcome the internal pressure in the extruder. The screw design in the fourth zone (13) is chosen that a pressure drop in the extruder at the position where the HCl-solution is added is created. The final pH of the cross-linked pre-gelatinized starch is measured after reaction in the fifth zone (14) in the extruder.

Examples 1 - 4

[0034] Reaction is performed according to the procedures disclosed above using a screw configuration as shown in figure 3 and the conditions of table 1, hereunder.

[0035] As the substrate waxy maize starch is used and the alkali concentration selected is 1,2% NaOH on dry starch.

Table 1: Extruder parameters during extrusion with waxy com with 1.2% NaOH

Sample	Ref.	Ex. 1	Ex. 2	Ex. 3	Ex. 4
N° Screw design	11	11	11	11	11
T1 (°C) *1	20	21	21	21	21
T2 (°C) *1	59	58	63	61	61
T3 (°C) *1	102	101	104	100	100
T4 (°C) *1	88	89	86	89	89
T5 (°C) *1	83	82	78	80	80
T6 (°C) *1	81	80	80	81	79
T7 (°C) *1	80	81	81	80	80
T8 (°C) *1	80	80	79	80	73
T9 (°C) *1	65	69	66	68	67
Tmelt (°C) *2	70	74	73	75	75

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(continued)

Sample	Ref.	Ex. 1	Ex. 2	Ex. 3	Ex. 4
SME (kWh/kg) *3	0.14	0.17	0.18	0.16	0.16
Speed (rpm)	200	201	201	201	201
Starch throughput (g/min)	172	172	173	171	171
H ₂ O throughput (g/min)	75	75	75	75	75
%H ₂ O calc.*4	39.3	39.3	39.2	39.4	39.4
POCl ₃ throughput (g/min)	0	0.17	0.17	0.08	0.08
%POCl ₃ calc.*5	0	0.11	0.11	0.06	0.06
HCl (10% w/w) throughput (g/min)	18	18	18	18	18
Gelatinised X-ray yes/no*6	yes	Yes	Yes	yes	yes

*1: The extruder exists out of reaction zones (see fig.3 and 4). Every element does have its own temperature

*2: T_{melt} is the melt temperature of the extrusion sample at the end of the extruder

*3: Specific Mechanical Energy (SME)

*4: %H₂O calculated is on dry matter basis

*5: %POCl₃ is calculated on dry matter basis

*6: Gelatinised X-ray: the gelatinisation is checked by X-ray measurement

[0036] The effect of the cross-linking agent on the gelatinised starch was determined by measuring the viscosity of a 6,3% w/w starch dispersion using a Brabender viscograph. All samples were neutralised providing dispersions having a pH of about 5,5.

[0037] Viscosity data are provided in table 2.

Table 2: Viscosity of with screw design T&L-11 extruded samples.

Sample	NaOH% waxy corn	%POCl ₃	viscosity 30' at 25°C (Bu)
Ref.	1.2	0	15
Ex. 1	1.2	0.11	1800
Ex. 2	1.2	0.11	1750
Ex. 3	1.2	0.06	725
Ex. 4	1.2	0.06	950

[0038] This table illustrates the effect of the quantity of POCl₃ used, at the same alkali concentration, on the viscosity.

Example 5

[0039] Reaction is performed according to the procedures disclosed above using a screw configuration as shown in figure 4 and the conditions of table 3, hereunder.

[0040] As the substrate waxy maize starch is used and the alkali concentration selected is 0,6% NaOH on dry starch.

Table 3: Extruder parameters of extrusion with waxy corn with 0.6% NaOH

Sample	Reference	Ex. 5
N° Screw design	12	12
T1 (°C)	21	20
T2 (°C)	59	61
T3 (°C)	100	99
T4 (°C)	99	100
T5 (°C)	80	80
T6 (°C)	81	80
T7 (°C)	94	95
T8 (°C)	99	100
T9 (°C)	79	83

(continued)

Sample	Reference	Ex. 5
T _{melt} (°C)	78	84
SME (kWh/kg)	0.16	0.16
Speed (rpm)	200	200
Starch throughput (g/min)	172	172
H ₂ O throughput (g/min)	75	75
%H ₂ O calc,	39.0	39.1
POCl ₃ throughput (g/min)	0	0.23
%POCl ₃ calc	0	0.16
HCl (10% w/w) throughput (g/min)	9.1	9.0
pH directly after extrusion	5 - 5.4	5.1 - 5.4
Gelatinised X-ray yes/no	yes	Yes

[0041] The effect of the cross-linking agent on the gelatinised starch was determined by measuring the viscosity of a 6,3% w/w starch dispersion using a Brabender viscograph. All samples were neutralised providing dispersions having a pH of about 5,5.

[0042] Viscosity data are provided in table 4.

Table 4: Viscosity of with screw design T&L-12 extruded samples.

Sample	NaOH% waxy corn	%POCl ₃	viscosity 30' at 25°C (Bu)
Ref.	0.6	0	19
Ex. 5	0.6	0.16	1690

Claims

1. Continuous extrusion process for preparing cold water swelling phosphate-cross-linked starch derivatives, **characterised in that** the process consists of the subsequent steps of

- gelatinising an alkaline starch in a first zone (10) in the extruder;
- adding of POCl₃ as cross-linking reagent in a second zone (11) in the extruder;
- cross-linking the obtained gelatinised starch by means of the POCl₃ in the second and third zone (11, 12) in the extruder, and
- neutralising the obtained cross-linked gelatinised starch that is present in a fourth zone (13) in the extruder;
- recovering the obtained cross-linked, gelatinised starch in a fifth zone (14) in the extruder.

2. Continuous extrusion process according to claim 1, wherein the process consists of the subsequent steps of

- continuously feeding the alkaline starch into a first partial zone (10a) of the said first zone (10) in the extruder, the temperature in this first partial zone (11) being between 20 °C ± 3°C;
- continuously feeding an extra amount of water to the alkaline starch in a second partial zone (10b) of the said first zone (10) in the extruder in a ratio of dry weight starch versus water of between 70:30 and 50:50, at a temperature of between 55 and 65 °C;
- kneading the alkaline starch/water mixture in a third partial zone (10c) of the said first zone (10) in the extruder at a temperature of about 100 °C through which a gelatinised starch is obtained;
- continuously feeding POCl₃ to the gelatinised starch in the second zone (11) in the extruder wherein the temperature is about 100 °C ± 5°C;
- cross-linking the gelatinised starch in the second and in the third zone (11, 12) in the extruder through which a cross-linked, gelatinised starch is obtained;
- neutralising the cross-linked, gelatinised starch in the fourth zone (13) in the extruder;
- recovering the cross-linked, gelatinised starch in the fifth zone (14) in the extruder.

3. Continuous extrusion process according to claim 1 or 2, **wherein** after the recovered cross-linked, gelatinised starch

is cooled to substantially room temperature, it is further reduced in size.

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4. Continuous extrusion process according to any one claims 1 to 3, wherein the needed specific mechanical input of the continuous extrusion process is situated between 350 and 1000 kJ/kg.
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5. Continuous extrusion process according to claims 4, **wherein** the needed specific mechanical input of the continuous extrusion process is situated between 450 and 750 kJ/kg.
- 15
6. Continuous extrusion process according to any one of claims 1 to 5, wherein the ratio of dry weight starch versus water the second partial zone (10b) of the said first zone in the extruder is in a ratio of between 70:30 and 50:50.
7. Continuous extrusion process according to any one of claims 1 to 6, wherein the cross-linking of the obtained gelatinised starch by means of the POCl_3 in the second and third zone (11, 12) in the extruder is performed at temperatures measured and monitored between 70 °C and 90 °C.
- 20
8. Continuous extrusion process according to claim 7, wherein the cross-linking of the obtained gelatinised starch by means of the POCl_3 in the second and third zone (11, 12) in the extruder is performed at temperatures measured and monitored between 75 °C and 85 °C.
- 25
9. Continuous extrusion process according to any one of claims 1 to 8, wherein the further reduction of the recovered and cooled cross-linked gelatinised starch is done by milling.
10. Continuous extrusion process according to any one of claims 1 to 9, wherein the continuous feeding of an alkaline starch is performed by means of a dosing system.
- 30
11. Continuous extrusion process according to any one of claims 1 to 11, **wherein** the extrusion process is performed using a single screw, a twin screw co-rotating or a twin screw counter-rotating configuration in the extruder.
- 35
12. Continuous extrusion process according to claim 11 wherein said screw is provided with zones wherein:
- the first zone (10) consists of
 - a first and second partial zone (10a, 10b) composed of Z-flight conveying elements;
 - a third partial zone (10c) composed of Z-flight conveying elements followed by a kneading block part;
 - the second zone (11) is composed of conveying elements in combination with a further kneading block;
 - the third zone (12) is composed of Z-flight conveying elements;
 - the fourth zone (13) is composed of conveying elements and a mixing block; and
 - the fifth zone (14) consists of a screw tip, wherein the mixing block of the fourth zone is just in front of the said screw tip.
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Patentansprüche

- 45
1. Kontinuierliches Extrusionsverfahren zur Herstellung von in kaltem Wasser quellfähigen phosphatvernetzten Stärkederivaten, **dadurch gekennzeichnet, dass** das Verfahren aus den aufeinanderfolgenden Schritten besteht:
- Gelatinieren einer alkalischen Stärke in einer ersten Zone (10) in dem Extruder;
 - Zugeben von POCl_3 als Vernetzungsreagens in einer zweiten Zone (11) in dem Extruder;
 - 50 - Vernetzen der erhaltenen gelatinierten Stärke durch das POCl_3 in der zweiten und der dritten Zone (11, 12) in dem Extruder; und
 - Neutralisieren der erhaltenen vernetzten gelatinierten Stärke, die in einer vierten Zone (13) in dem Extruder vorhanden ist;
 - Gewinnen der erhaltenen vernetzten gelatinierten Stärke in einer fünften Zone (14) in dem Extruder.
- 55
2. Kontinuierliches Extrusionsverfahren gemäß Anspruch 1, **wobei** das Verfahren aus den aufeinanderfolgenden Schritten besteht:

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- kontinuierliches Zuführen der alkalischen Stärke in eine erste Teilzone (10a) der ersten Zone (10) in dem Extruder, wobei die Temperatur in dieser ersten Teilzone (11) zwischen $20\text{ °C} \pm 3\text{ °C}$ beträgt;
 - kontinuierliches Zuführen einer zusätzlichen Menge Wasser zu der alkalischen Stärke in einer zweiten Teilzone (10b) der ersten Zone (10) in dem Extruder in einem Verhältnis von Trockengewicht an Stärke zu Wasser von zwischen 70:30 und 50:50 bei einer Temperatur von zwischen 55 und 65 °C;
 - Kneten des alkalische-Stärke/Wasser-Gemischs in einer dritten Teilzone (10c) der ersten Zone (10) in dem Extruder bei einer Temperatur von etwa 100 °C, wodurch eine gelatinierte Stärke erhalten wird;
 - kontinuierliches Zuführen von POCl_3 zu der gelatinieren Stärke in der zweiten Zone (11) in dem Extruder, wobei die Temperatur etwa $100\text{ °C} \pm 5\text{ °C}$ beträgt;
 - Vernetzen der gelatinieren Stärke in der zweiten und in der dritten Zone (11, 12) in dem Extruder, wodurch eine vernetzte gelatinieren Stärke erhalten wird;
 - Neutralisieren der vernetzten gelatinieren Stärke in der vierten Zone (13) in dem Extruder;
 - Gewinnen der vernetzten gelatinieren Stärke in der fünften Zone (14) in dem Extruder.
3. Kontinuierliches Extrusionsverfahren gemäß Anspruch 1 oder 2, **wobei** die gewonnene vernetzte gelatinieren Stärke nach dem Abkühlen auf im Wesentlichen Raumtemperatur weiter in der Größe zerkleinert wird.
4. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 3, **wobei** die benötigte spezifische mechanische Eingangsleistung des kontinuierlichen Extrusionsverfahrens zwischen 350 und 1000 kJ/kg beträgt.
5. Kontinuierliches Extrusionsverfahren gemäß Ansprüche 4, **wobei** die benötigte spezifische mechanische Eingangsleistung des kontinuierlichen Extrusionsverfahrens zwischen 450 und 750 kJ/kg beträgt.
6. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 5, **wobei** das Verhältnis von Trockengewicht an Stärke zu Wasser der zweiten Teilzone (10b) der ersten Zone in dem Extruder ein Verhältnis von zwischen 70:30 und 50:50 ist.
7. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 6, **wobei** das Vernetzen der erhaltenen gelatinieren Stärke durch POCl_3 in der zweiten und der dritten Zone (11, 12) in dem Extruder bei Temperaturen durchgeführt wird, die zwischen 70 °C und 90 °C gemessen und überwacht sind.
8. Kontinuierliches Extrusionsverfahren gemäß Anspruch 7, **wobei** das Vernetzen der erhaltenen gelatinieren Stärke durch POCl_3 in der zweiten und der dritten Zone (11, 12) in dem Extruder bei Temperaturen durchgeführt wird, die zwischen 75 °C und 85 °C gemessen und überwacht sind.
9. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 8, **wobei** das weitere Zerkleinern der gewonnenen und abgekühlten vernetzten gelatinieren Stärke durch Mahlen durchgeführt wird.
10. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 9, **wobei** das kontinuierliche Zuführen einer alkalischen Stärke mithilfe eines Dosierungssystems durchgeführt wird.
11. Kontinuierliches Extrusionsverfahren gemäß einem der Ansprüche 1 bis 11, **wobei** das Extrusionsverfahren unter Verwendung einer Einzelschnecken-, einer gleichlaufenden Doppelschnecken- oder einer gegenlaufenden Doppelschneckenkonfiguration in dem Extruder durchgeführt wird.
12. Kontinuierliches Extrusionsverfahren gemäß Anspruch 11, **wobei** die Schnecke mit Zonen ausgestattet ist, wobei:
- die erste Zone (10) aus
 - einer ersten und einer zweiten Teilzone (10a, 10b), die aus Z-Flight-Fördererelementen gebildet sind;
 - einer dritten Teilzone (10c), die aus Z-Flight-Fördererelementen, gefolgt von einem Knetblockteil, gebildet ist; besteht;
 - die zweite Zone (11) aus Fördererelementen in Kombination mit einem weiteren Knetblock gebildet ist;
 - die dritte Zone (12) aus Z-Flight-Fördererelementen gebildet ist;
 - die vierte Zone (13) aus Fördererelementen und einem Mischblock gebildet ist; und
 - die fünfte Zone (14) aus einer Schneckenspitze besteht, wobei der Mischblock der vierten Zone unmittelbar vor der Schneckenspitze liegt.

Revendications

1. Procédé d'extrusion en continu pour la préparation de dérivés d'amidon réticulés par des liaisons phosphate et gonflant à l'eau froide, **caractérisé en ce que** le procédé se compose des étapes suivantes qui consistent à :
 - gélatiniser un amidon alcalin dans une première zone (10) de l'extrudeuse ;
 - ajouter du POCl_3 comme réactif de réticulation dans une deuxième zone (11) de l'extrudeuse ;
 - réticuler l'amidon gélatinisé obtenu au moyen du POCl_3 dans la deuxième zone et dans la troisième zone (11, 12) de l'extrudeuse, et
 - neutraliser l'amidon gélatinisé réticulé obtenu qui est présent dans une quatrième zone (13) de l'extrudeuse ;
 - récupérer l'amidon gélatinisé réticulé obtenu dans une cinquième zone (14) de l'extrudeuse.

2. Procédé d'extrusion en continu selon la revendication 1, le procédé se composant des étapes suivantes qui consistent à :
 - introduire en continu l'amidon alcalin dans une première zone partielle (10a) de ladite première zone (10) de l'extrudeuse, la température dans cette première zone partielle (11) étant de $20\text{ °C} \pm 3\text{ °C}$;
 - introduire en continu une quantité supplémentaire d'eau dans l'amidon alcalin dans une deuxième zone partielle (10b) de ladite première zone (10) de l'extrudeuse selon un rapport du poids sec d'amidon contre l'eau de 70:30 à 50:50, à une température de 55 à 65 °C ;
 - malaxer le mélange amidon alcalin/eau dans une troisième zone partielle (10c) de ladite première zone (10) de l'extrudeuse à une température d'environ 100 °C, un amidon gélatinisé étant ainsi obtenu ;
 - introduire en continu du POCl_3 dans l'amidon gélatinisé dans la deuxième zone (11) de l'extrudeuse, la température étant d'environ $100\text{ °C} \pm 5\text{ °C}$;
 - réticuler l'amidon gélatinisé dans la deuxième zone et dans la troisième zone (11, 12) de l'extrudeuse, un amidon gélatinisé réticulé étant ainsi obtenu ;
 - neutraliser l'amidon gélatinisé réticulé dans la quatrième zone (13) de l'extrudeuse ;
 - récupérer l'amidon gélatinisé réticulé dans la cinquième zone (14) de l'extrudeuse.

3. Procédé d'extrusion en continu selon la revendication 1 ou 2, dans lequel, après un refroidissement de l'amidon gélatinisé réticulé récupéré jusqu'à une température correspondant sensiblement à la température ambiante, sa taille est réduite davantage.

4. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 3, l'apport d'énergie mécanique spécifique nécessaire pour le procédé d'extrusion en continu étant de 350 à 1 000 kJ/kg.

5. Procédé d'extrusion en continu selon les revendications 4, l'apport d'énergie mécanique spécifique nécessaire pour le procédé d'extrusion en continu étant de 450 à 750 kJ/kg.

6. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 5, dans lequel le rapport du poids sec d'amidon contre l'eau la deuxième zone partielle (10b) de ladite première zone de l'extrudeuse est un rapport de 70:30 à 50:50.

7. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 6, dans lequel la réticulation de l'amidon gélatinisé obtenu au moyen du POCl_3 dans la deuxième zone et dans la troisième zone (11, 12) de l'extrudeuse est effectuée à des températures mesurées et surveillées de 70 °C à 90 °C.

8. Procédé d'extrusion en continu selon la revendication 7, dans lequel la réticulation de l'amidon gélatinisé obtenu au moyen du POCl_3 dans la deuxième zone et dans la troisième zone (11, 12) de l'extrudeuse est effectuée à des températures mesurées et surveillées de 75 °C à 85 °C.

9. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 8, dans lequel la réduction supplémentaire de l'amidon gélatinisé réticulé, récupéré et refroidi, est réalisée par broyage.

10. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 9, dans lequel l'introduction en continu d'un amidon alcalin est réalisée au moyen d'un système de dosage.

11. Procédé d'extrusion en continu selon l'une quelconque des revendications 1 à 11, le procédé d'extrusion étant

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exécuté en utilisant une configuration monovis, bivis en co-rotation, ou bivis en rotation inverse dans l'extrudeuse.

12. Procédé d'extrusion en continu selon la revendication 11, dans lequel ladite vis comporte des zones dans lesquelles :

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- la première zone (10) consiste en :
 - une première zone partielle et une deuxième zone partielle (10a, 10b) constituées d'éléments de transport comportant Z pas ;
 - une troisième zone partielle (10c) constituée d'éléments de transport comportant Z pas, suivie d'une partie
- 10
- constituée d'un bloc de malaxage ;
 - la deuxième zone (11) est constituée d'éléments de transport associés à un bloc de pétrissage supplémentaire ;
 - la troisième zone (12) est constituée d'éléments de transport comportant Z pas ;
 - la quatrième zone (13) est constituée d'éléments de transport et d'un bloc de mélange ; et
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- la cinquième zone (14) est constituée d'une extrémité de vis, le bloc de mélange de la quatrième zone se trouvant juste devant ladite extrémité de vis.

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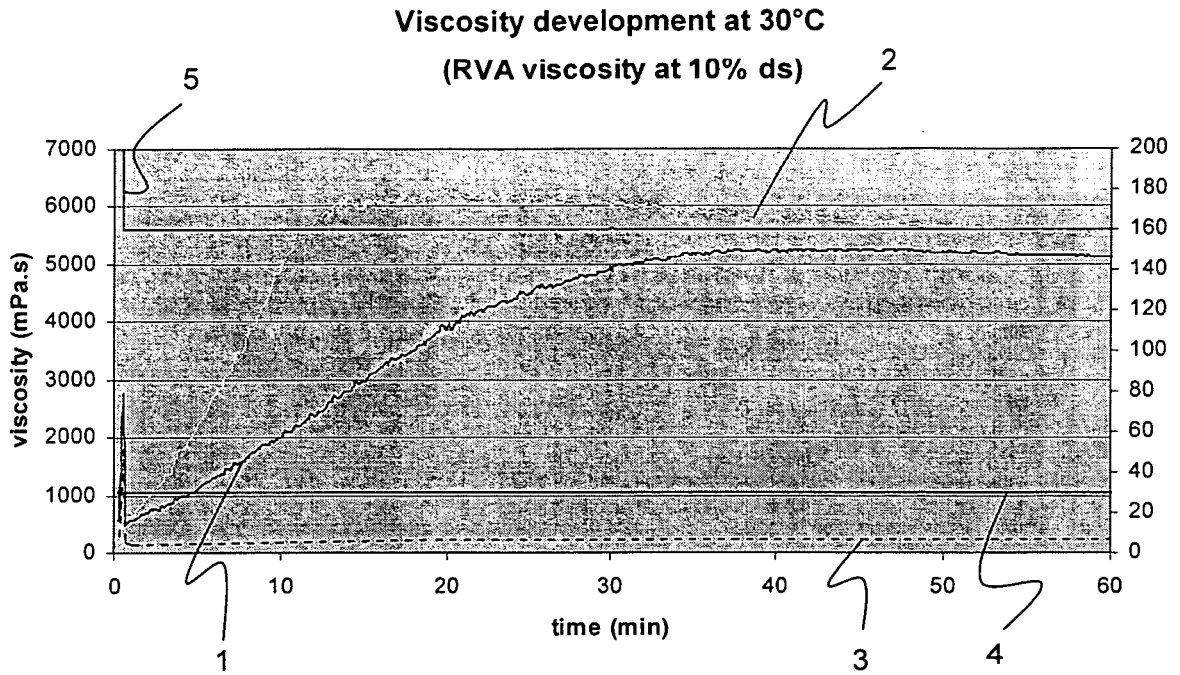


FIG. 1

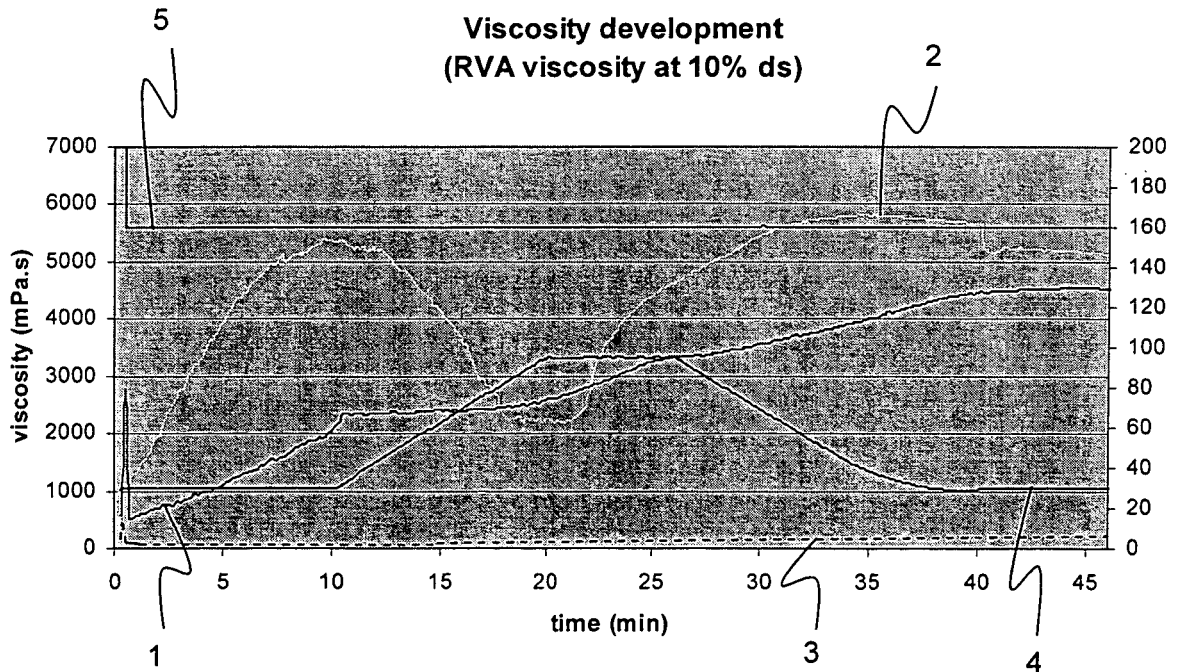


FIG. 2

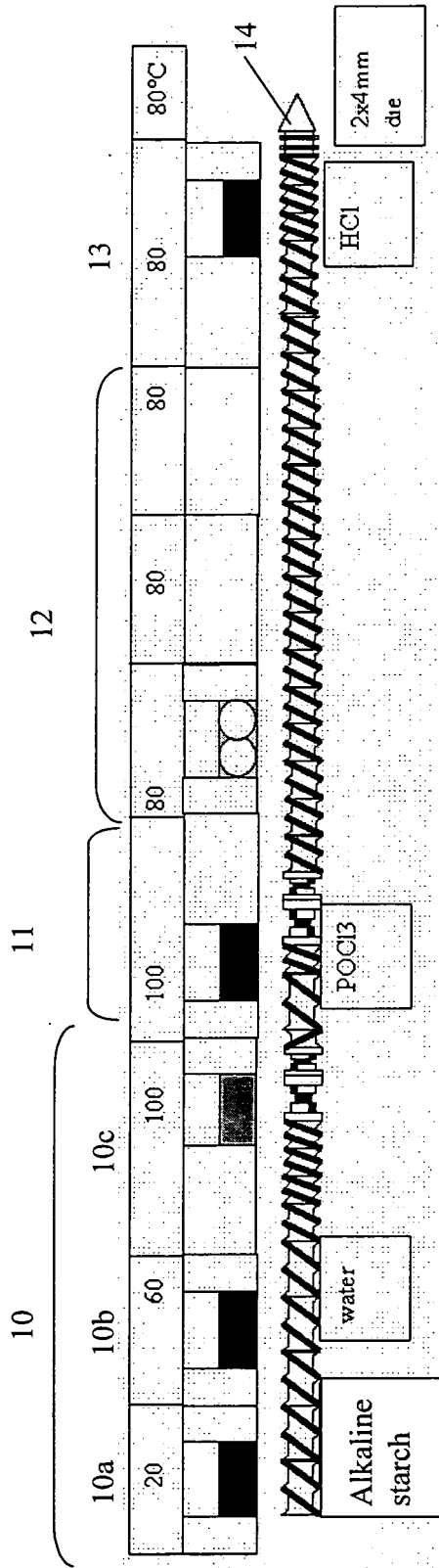


FIG. 3

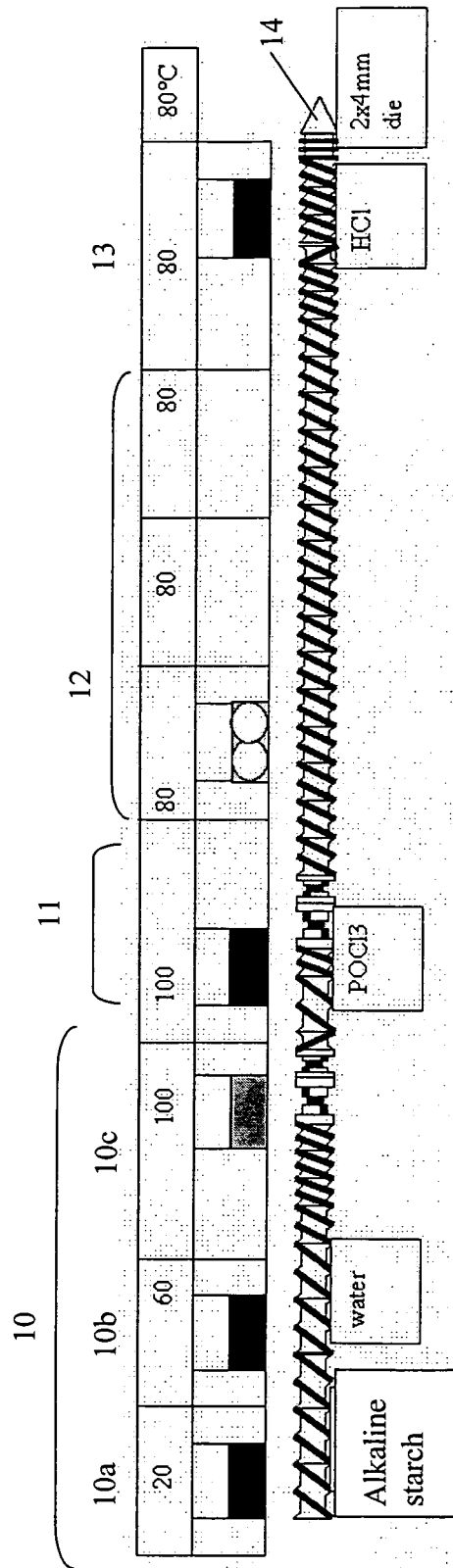


FIG. 4

REFERENCES CITED IN THE DESCRIPTION

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