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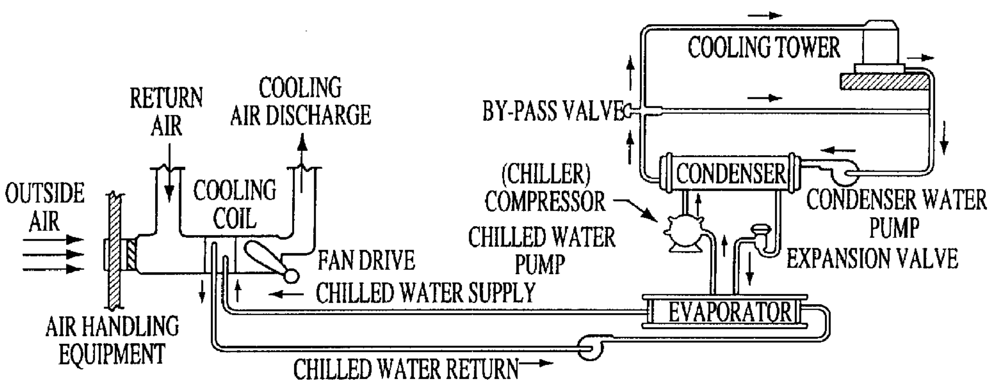
(54) **COMMANDE NUMERIQUE POUR UNE INSTALLATION DE REFROIDISSEMENT ET DE CHAUFFAGE AYANT UNE STRATEGIE DE COMMANDE DE VALEURS DE REGLAGE GLOBAL QUASI OPTIMALES**

(54) **A DIGITAL CONTROLLER FOR A COOLING AND HEATING PLANT HAVING NEAR-OPTIMAL GLOBAL SET POINT CONTROL STRATEGY**



(57) L'invention a trait à une commande numérique directe (DDC) mettant en oeuvre une stratégie de commande qui fournit des valeurs de réglage global quasi optimales, ce qui permet de minimiser la consommation d'énergie et par conséquent les coûts d'énergie reliés à l'exploitation des installations de chauffage et (ou) de refroidissement. La commande peut mettre en oeuvre deux modèles de composants d'installations de refroidissement qui expriment l'alimentation en énergie du refroidisseur, de la pompe à eau froide et du ventilateur de circulation d'air en tant que fonction de la variation de température de l'eau froide à l'arrivée et au retour. Les modèles sont dérivés d'analyses mathématiques basées sur les relations de la mécanique des fluides et de l'échange thermique en prenant pour acquis un état de charge stationnaire. L'analyse s'applique aux refroidisseurs, aux pompes à

(57) A DDC controller is disclosed which implements a control strategy that provides for near-optimal global set points, so that power consumption and therefore energy costs for operating a heating and/or cooling plant can be minimized. The controller can implement two chiller plant component models expressing chiller, chilled water pump, and air handler fan power as a function of chilled water supply/return differential temperature. The models are derived from a mathematical analysis using relations from fluid mechanics and heat transfer under the assumption of a steady-state load condition. The analysis applies to both constant speed and variable speed chillers, chilled water pumps, and air handler fans. Similar models are presented for a heating plant consisting of a hot water boiler, hot water pump, and air handler fan which relates power as a function of the hot water supply/return differential temperature. A relatively

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eau froide et aux ventilateur de circulation d'air à vitesse constante et à vitesse variable. On présente des modèles semblables pour une installation de chauffage comprenant une chaudière à eau chaude, une pompe à eau chaude et un ventilateur de circulation d'air qui expriment l'alimentation en énergie en tant que fonction de la variation de température de l'eau chaude à l'arrivée et au retour. On présente une technique relativement simple pour calculer les températures des valeurs de réglage quasi optimales pour l'eau froide et l'eau chaude à chaque fois qu'un nouvel état de charge stationnaire s'établit, de manière à minimiser la consommation totale d'énergie. À partir des valeurs quasi optimales calculées pour les températures d'arrivée de l'eau froide et de l'eau chaude on peut calculer une température d'air de sortie quasi optimale à partir d'un dispositif de circulation d'air central pour chaque variation de charge. Même si les valeurs de réglage sont quasi optimales, la technique de calcul est suffisamment simple pour être mise en oeuvre dans une commande numérique directe.

simple technique is presented to calculate near-optimal chilled water and hot water set point temperatures whenever a new steady-state load occurs, in order to minimize total power consumption. From the calculated values of near-optimal chilled water and hot water supply temperatures, a near-optimal discharge air temperature from a central air handler can be calculated for each step in load. Although the set points are near-optimal, the technique of calculation is simple enough to implement in a DDC controller.

Abstract of the Disclosure

A DDC controller is disclosed which implements a control strategy that provides for near-optimal global set points, so that power consumption and therefore energy costs for operating a heating and/or cooling plant can be minimized. The controller can implement two chiller plant component models expressing chiller, chilled water pump, and air handler fan power as a function of chilled water supply/return differential temperature. The models are derived from a mathematical analysis using relations from fluid mechanics and heat transfer under the assumption of a steady-state load condition. The analysis applies to both constant speed and variable speed chillers, chilled water pumps, and air handler fans. Similar models are presented for a heating plant consisting of a hot water boiler, hot water pump, and air handler fan which relates power as a function of the hot water supply/return differential temperature. A relatively simple technique is presented to calculate near-optimal chilled water and hot water set point temperatures whenever a new steady-state load occurs, in order to minimize total power consumption. From the calculated values of near-optimal chilled water and hot water supply temperatures, a near-optimal discharge air temperature from a central air handler can be calculated for each step in load. Although the set points are near-optimal, the technique of calculation is simple enough to implement in a DDC controller.

A DIGITAL CONTROLLER FOR A COOLING AND HEATING PLANT HAVING NEAR-OPTIMAL GLOBAL SET POINT CONTROL STRATEGY

The present invention is generally related to a digital controller for use in controlling a cooling and heating plant of a facility, and more particularly related to such a controller which has a near-optimal global set point control strategy for minimizing energy costs during operation.

Background of the Invention

Cooling plants for large buildings and other facilities provide air conditioning of the interior space and include chillers, chilled water pumps, condensers, condenser water pumps, cooling towers with cooling tower fans, and air handling fans for distributing the cool air to the interior space. The drives for the pumps and fans may be variable or constant speed drives. Heating plants for such facilities include hot water boilers, hot water pumps, and air handling fans. The drives for these pumps and fans may also be variable or constant speed drives.

Global set point optimization is defined as the selection of the proper set points for chilled water supply, hot water supply, condenser water flow rate, tower fan air flow rate, and air handler discharge temperature that result in minimal total energy consumption of the chillers, boilers, chilled water pumps, condenser water pumps, hot water pumps, and air handling fans. Determining these optimal set points holds the key to substantial energy savings in a facility since the chillers, towers, boilers, pumps, and air handler fans together can comprise anywhere from 40% to 70% of the total energy consumption in a facility.

There has been study of the matter of determining optimal set points in the past. For example, in the article by Braun et al. 1989b. "Methodologies for optimal control of chilled water systems without storage", *ASHRAE Transactions*, Vol. 95, Part 1, pp. 652-62, they have shown that there is a strong coupling between optimal values of the chilled water and supply air temperatures; however, the coupling between optimal values of the chilled water loop and condenser water loop is not as strong. (This justifies the approach taken in the present invention of considering the chilled water loop and condenser water/cooling tower loops as separate loops and treating only the chiller, the chilled water pump, and air handler fan components to determine optimal ΔT of the chilled water and air temperature across the cooling coil.)

It has also been shown that the optimization of the cooling tower loop can be handled by use of an open-loop control algorithm (Braun and Diderrich, 1990, "Performance and control characteristics of a large cooling system." *ASHRAE Transactions*, Vol. 93, Part 1, pp. 1830-52). They have also shown that a change in wet bulb temperature has an insignificant influence on chiller plant power consumption and that near-optimal control of cooling towers for chilled water systems can be obtained from an algorithm based upon a combination of heuristic rules for tower sequencing and an open-loop control equation. This equation is a linear equation in only one variable, i.e., load, and correlates a near-optimal tower air flow in terms of load (part-load ratio).

$$G_{twr} = 1 - \beta_{twr}(PLR_{twr,\,cap} - PLR) \qquad 0.25 < PLR < 1.0 \qquad (1)$$

where

G_{twr} = the tower air flow divided by the maximum air flow with all cells operating at high speed

PLR = the chilled water load divided by the total chiller cooling capacity (part-load ratio)

$PLR_{twr,cap}$ = value of PLR at which the tower operates at its capacity ($G_{twr} = 1$)

β_{twr} = the slope of the relative tower air flow (G_{twr}) versus the PLR function.

Estimates of these parameters may be obtained using design data and relationships presented in Table 1 below:

TABLE 1.
Parameter Estimates for Eqn. 1

Parameter	Single-Speed Fans	Two-Speed Fans	Variable-Speed Fans
$PLR_{twr,cap}$	PLR_0	$\sqrt{2}\cdot PLR_0$	$\sqrt{3}\cdot PLR_0$
β_{twr}	$\frac{1}{PLR_{twr,cap}}$	$\frac{2}{3\cdot PLR_{twr,cap}}$	$\frac{1}{2\cdot PLR_{twr,cap}}$

$$PLR_0 = \frac{1}{\sqrt{\left(\frac{P_{ch,des}}{P_{twr,des}}\right)\cdot S\cdot\left(a_{twr,des}+r_{twr,des}\right)}}$$

where:

$\left(\frac{P_{ch,des}}{P_{twr,des}}\right)$ = the ratio of the chiller power to cooling tower fan power at design conditions

$$S = Sensitivity = \frac{(change\ in\ chiller\ power)}{(change\ in\ condenser\ water\ temperature)\times(chiller\ power)}$$

$\left(a_{twr,des}+r_{twr,des}\right)$ = the sum of the tower approach and range at design conditions

Once a near-optimal tower air flow is determined, Braun et al., 1987, "Performance and control characteristics of a large cooling system." *ASHRAE Transactions*, Vol. 93, Part 1, pp. 1830-52 have shown that for a tower with an effectiveness near unity, the optimal condenser flow is determined when the thermal capacities of the air and water are equal.

Cooling tower effectiveness is defined as:

$$\varepsilon = \frac{Q_{tower}}{Min(Q_{a,\max}, Q_{w,\max})}$$

$$where$$

$$\varepsilon = effectiveness\ of\ cooling\ tower$$

$$Q_{a,\max} = m_{a,twr}(h_{s,cwr} - h_{s,i}) \quad , sigma\ energy, h_{s,\_} = h_{air,\_} - \omega\_c_{pw}T_{wb}$$

$$Q_{w,\max} = m_{cw}c_{pw}(T_{cwr} - T_{wb}) \qquad (2)$$

$$m_{a,twr} = tower\ air\ flow\ rate$$

$$m_{cw} = condenser\ water\ flow\ rate$$

$$T_{cwr} = condenser\ water\ return\ temperature$$

$$T_{wb} = ambient\ air\ wet\ bulb\ temperature$$

A DDC controller can calculate the effectiveness, ε, of the cooling tower, and if it is between 0.9 and 1.0 (Braun et al. 1987), m_{cw} can be calculated from equating $Q_{a,\max}$ and $Q_{w,\max}$ once $m_{a,twr}$ is determined from Eqn. 1. Near-optimal operation of the condenser water flow and the cooling tower air flow can be obtained when variable speed drives are used for both the condenser water pumps and cooling tower fans.

Braun et al. (1989a. "Applications of optimal control to chilled water systems without storage." *ASHRAE Transactions*, Vol. 95, Part 1, pp. 663-75; 1989b. "Methodologies for optimal control of chilled water systems without storage", *ASHRAE Transactions*, Vol. 95, Part 1, pp. 652-62; 1987, "Performance and control characteristics of a large cooling system." *ASHRAE Transactions*, Vol. 93, Part 1, pp. 1830-52.) have done a number of pioneering studies on optimal and near-optimal control of chilled water systems. These studies involve application of two basic methodologies for determining optimal values of the independent control variables that minimize the instantaneous cost of chiller plant operation. These independent control variables are: 1) supply air set point temperature, 2) chilled water set point temperature, 3) relative tower air flow (ratio of the actual tower air flow to the design air flow), 4) relative condenser water flow (ratio of the actual condenser water flow to the design condenser water flow), and 5) the number of operating chillers.

One methodology uses component-based models of the power consumption of the chiller, cooling tower, condenser and chilled water pumps, and air handler fans. However, applying this method in its full generality is mathematically complex because it requires simultaneous solution of differential equations. In addition, this method requires measurements of power and input variables, such as load and ambient dry bulb and wet bulb temperatures, at each step in time. The capability of solving simultaneous differential equations is lacking in today's DDC controllers. Therefore, implementing this methodology in an energy management system is not practical.

Braun et al. (1987, 1989a, 1989b) also present an alternative, and somewhat simpler methodology for near-optimal control that involves correlating the overall system power consumption with a single function. This method allows a rapid determination of optimal control variables and requires measurements of only total power over a range of conditions. However, this methodology still requires the simultaneous solution of differential equations and therefore cannot practically be implemented in a DDC controller.

Optimal air-side and water-side control set points were identified by Hackner et al. (1985, "System Dynamics and Energy Use." *ASHRAE Journal*, June.) for a specific plant through the use of performance maps. These maps were generated by many simulations of the plant over the range of expected operating conditions. However, this procedure lacks generality and is not easily implemented in a DDC controller.

Braun et al. (1987) has suggested the use of a bi-quadratic equation to model chiller performance of the form:

$$\frac{P_{ch}}{P_{des}} = a + bx + cx^2 + dy + ey^2 + fxy \qquad (3)$$

where "x" is the ratio of the load to a design load, "y" is the leaving condenser water temperature minus the leaving chilled water temperature, divided by a design value, P_{ch} is the actual chiller power consumption, and P_{des} is the chiller power associated with the design conditions. The empirical coefficients of the above equation (a, b, c, d, e, f) are determined with linear least-squares curve-fitting applied to measured or modeled performance data. This model can be applied to both variable speed and constant speed chillers.

Kaya et al. (1983, "Chiller optimization by distributed control to save energy", *Proceedings of the Instrument Society of America Conference*, Houston, TX.) has used a component-based approach for modeling the power consumption of the chiller and chilled water pump under steady-state load conditions. In his paper, the chiller component power is approximated to be a linear function of the chilled water differential temperature, and chilled water pump component power to be proportional to the cube of the reciprocal of the chilled water differential temperature for each steady-state load condition.

$$\begin{aligned} P_{Tot}(\Delta T_{chw}) &= P_{comp}(\Delta T_{chw}) + P_{pump}(\Delta T_{chw}) \\ &= K_{comp} \cdot \Delta T_{chw} + K_{pump} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 \end{aligned} \qquad (4)$$

where

P_{Tot} = the total power consumption

P_{comp} = the power consumption of the chiller's compressor

P_{pump} = the power consumption of the chilled water pump

ΔT_{chw} = the supply/return chilled water temperature

K_{comp} , K_{pump} = constants, dependent on load

While the above described work allows the calculation of the optimal ΔT_{chw}, it lacks generality since the power consumption of the air handler fans is not considerein in the analysis.

Accordingly, it is a primary object of the present invention to provide an improved digital controller for a cooling and heating plant that easily and effectively implements a near-optimal global set point control strategy.

A related object is to provide such an improved controller which enables a heating and/or cooling plant to be efficiently operated and thereby minimizes the energy costs involved in such operation.

Yet another object of the present invention is to provide such a controller that is adapted to provide approximate instantaneous cost savings information for a cooling or heating plant compared to a baseline operation.

A related object is to provide such a controller which provides accumulated cost savings information.

These and other objects of the present invention will become apparent upon reading the following detailed description while referring to the attached drawings.

Description of the Drawings

FIGURE 1 is a schematic diagram of a generic cooling plant consisting of equipment that includes a chiller, a chilled water pump, a condenser water pump, a cooling tower, a cooling tower fan and an air handling fan.

FIG. 2 is a schematic diagram of another generic cooling plant having primary-secondary chilled water loops, multiple chillers, multiple chilled water pumps and multiple air handling fans.

FIG. 3 is a schematic diagram of a generic heating plant consisting of equipment that includes a hot water boiler, a hot water pump and an air handling fan.

Detailed Description

Broadly stated, the present invention is directed to a DDC controller for controlling such heating and cooling plants that is adapted to quickly and easily determine set points that are near-optimal, rather than optimal, because neither the condenser water pump power nor the cooling tower fan power are integrated into the determination of the set points.

The controller uses a strategy that can be easily implemented in a DDC controller to calculate near-optimal chilled water, hot water, and central air handler discharge air set points in order to minimize cooling and heating plant energy consumption. The component models for the chiller, hot water boiler, chilled water and hot water pumps and air handler fans power consumption have been derived from well known heat transfer and fluid mechanics relations.

The present invention also uses a strategy that is similar to that used by Kaya et al. for determining the power consumed by the air handler fans as well as the chiller and chilled water pumps. First, the simplified linear chiller component model of Kaya et al. is used for the chilled water pump and air handler component models, then a more general bi-quadratic chiller model of Braun (1987) is used for the chilled water pump and air handler component models. In both of these cooling plant models, the total power consumption in the plant can be represented as a function of only one variable, which is the chilled water supply/return differential temperature ΔT_{chw}. This greatly simplifies the mathematics and enables quick computation of optimal chilled water and supply air set points by the DDC controller embodying the present invention. In addition, a similar set of models and computations are used for the components of a typical heating plant--namely, hot water boilers, hot water pumps, and central air handler fans.

Turning to the drawings and particularly FIG. 1, a generic cooling plant is illustrated and is the type of plant that the digital controller of the present invention can operate. The drawing shows a single chiller, but could and often does have multiple chillers. The plant operates by pumping chilled water returning from the building, which would be a cooling coil in the air handler duct, and pumping it through the evaporator of the chiller. The evaporator cools the chilled water down to approximately 40 to 45 degrees F and it then is pumped back up through the cooling coil to further cool the air. The outside air and the return air are mixed in the mixed air duct and that air is then cooled by the cooling coil and discharged by the fan into the building space.

In the condenser water loop, the cooling tower serves to cool the hot water leaving the condenser to a cooler temperature so that it can condense the refrigerant gas that is pumped by the compresser from the evaporator to the condenser in the refrigerant loop. With respect to the refrigeration loop comprising the compressor, evaporator and the condenser, the compressor compresses the refrigerent gas into a high temperature, high pressure state in the condenser, which is nothing more than a shell and tube heat exchanger. On the shell side of the condenser, there is hot refrigerant gas, and on the tube side, there is cool cooling tower water. In operation, when the cool tubes in the condenser are touched by the hot refrigerant gas, it condenses into a liquid which gathers at the bottom of the condenser and is forced through an expansion valve which causes its temperature and pressure to drop and be vaporized into a cold gaseous state. So the tubes are surrounded by cold refrigerant gas in the evaporator, which is also a shell and tube heat exchanger, with cold refrigerant gas on the shell side and returned chilled water on the tube side. So the chilled water coming back from the building is cooled. The approximate temperature drop between supply and returned chilled water is about 10 to 12 degrees at full load conditions.

The present invention is directed to a controller that controls the cooling plant to optimize the supply chilled water going to the coil and the discharge air temperature off the coil, considering the chilled water pump energy, the chiller energy and the fan energy. The controller is trying to determine the discharge air set point and the chilled water set point such that the load is satisfied at the minimum power consumption.

The controller utilizes a classical calculus technique, where the chiller power, chilled water pump power and air handler power are modeled as functions of the ΔT_{chw} and summed in a polynomial function (the total power), then the first derivative of the functional relationship of the total power is set to zero and the equation is solved for ΔT_{chw} which is the optimum ΔT_{chw}.

The schematic diagram of FIG. 2 is another typical chiller plant which includes multiple chillers, multiple chilled water pumps, multiple air handler fans and multiple air handler coils. The present invention is applicable to controlling plants of the type shown in FIGS. 1, 2 or 3.

In accordance with an important aspect of the present invention, the controller utilizes a strategy that applies to both cooling and heating plants, and is implemented in a manner which utilizes several valid assumptions. A first assumption is that load is at a steady-state condition at the time of optimal chilled water, hot water and coil discharge air temperature calculation. Under this assumption, from basic heat transfer equations:

$$BTU / H = 500 \times GPM \times \Delta T_{chw} \equiv constant$$
$$BTU / H = 4.5 \times CFM \times \Delta h_{air} \equiv constant \qquad (4)$$

It is evident that if flow is varied, the ΔT_{chw} or the Δh_{air} must vary proportionately in order to keep the load fixed. This assumption is justified because time constants for chilled water, hot water, and space air temperature change control loops is on the order of 20 minutes or less, and facilities can usually hold at approximate steady-state conditions for 15 or 20 minutes at a time.

A second assumption is that the ΔT_{chw} and the Δh_{air} are assumed to be constant at the time of optimal chilled water, hot water, and coil discharge air temperature calculation due to the local loop controls (the first assumption combined with the sixth assumption). Therefore, this implies that the GPM of the chilled water through the cooling coil and the CFM of the air across the cooling coil must also be constant at the time of optimal set point calculations.

A third assumption is that the specific heats of the water and air at remain essentially constant for any load condition. This assumption is justified because the specific heats of the chilled water, hot water, and the air at the heat exchanger is only a weak function of temperature and the temperature change of either the water or air through the heat exchanger is relatively small (on the order 5 - 15°F for chilled water temperature change and 20 - 40°F for hot water or air temperature change).

A fourth assumption is that convection heat transfer coefficients are constant throughout the heat exchanger. This assumption is more serious than the third assumption because of entrance effects, fluid viscosity, and thermal conductivity changes. However, because water and air flow rates are essentially constant at steady-state load conditions, and fluid viscosity of the air and thermal conductivity and viscosity of the air and water vary only slightly in the temperature range considered, this assumption is also valid.

A fifth assumption is that the chilled water systems for which the following results apply do not have significant thermal storage characteristics. That is, the strategy does not apply for buildings that are thermally massive or contain chilled water or ice storage tanks that would shift loads in time.

A sixth assumption is that in addition to the independent optimization control variables, there are also local loop controls associated with the chillers, air handlers, and chilled water pumps. The chiller is considered to be controlled such that the specified chilled water set point temperature is maintained. The air handler local loop control involves control of both the coil water flow and fan air flow in order to maintain a given supply air set point and fan static pressure set point. Modulation of a variable speed primary chilled water pump is implemented through a local loop control to maintain a constant differential temperature across the evaporator. All local loop controls are assumed ideal, such that their dynamics can be neglected.

In accordance with an important aspect of the present invention, and referring to FIG. 1, the controller strategy involves the modeling of the cooling plant, and involves simple component models of cooling plant power consumption as a function of a single variable. The individual component models for the chiller, the chilled water pump, and the air handler fan are then summed to get the total instantaneous power consumed in the chiller plant.

$$P_{Tot} = P_{comp} + P_{CHW\,pump} + P_{AHU\,fan} \qquad (5)$$

For the analysis which follows, we assume that the chiller, chilled water pump, and the air handler fan are variable speed devices. However, this assumption is not overly restrictive, since it will be shown that the analysis also applies to constant speed chillers, constant speed chilled water pumps with two-way chilled water valves, and constant speed, constant volume air handler fans without air bypass.

There are two distinct chiller models that can be used, one being a linear model and the other a bi-quadratic model. With respect to the linear model, Kaya et al. (1983) have shown that a first approximation for the chiller component of the total power under a steady-state load condition is:

$$P_{comp} = K_1 \cdot \Delta T_{ref} = K_2 \cdot \Delta T_{chw} \qquad (7)$$

The derivation of the first half of Eqn. 7 is shown in the attached Appendix A. The second half of Eqn. 7 holds because as the chilled water supply temperature is increased for a given chilled water return temperature, ΔT_{chw} is decreased in the same proportion as ΔT_{ref}.

With respect to the bi-quadratic model, an improvement of the linear chiller model is given by Braun et al. (1987). However, Braun's chiller model can be further improved when the bi-quadratic model is expressed in its most general form:

$$\frac{P_{ch}}{P_{des}} = (A_0 + A_1 y + A_2 y^2) + (B_0 + B_1 y + B_2 y^2)x + (C_0 + C_1 y + C_2 y^2)x^2 \qquad (8)$$

where the empirical coefficients of the above equation $(A_0, A_1, A_2, B_0, B_1, B_2, C_0, C_1, C_2)$ are determined with linear least-squares curve-fitting applied to measured performance data.

With respect to the chilled water pump model, the relationship of the chilled water pump power as a function of ΔT_{chw} as:

$$P_{pump} = K_5 \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 \qquad (9)$$

where K_5 is a constant. The derivation of this relationship is shown in the attached Appendix B.

With respect to the air handler model, the relationship of the chilled water pump power as a function of ΔT_{air} has been derived in attached Appendix C as:

$$P_{fan} = K_{fan} \cdot \left(\frac{1}{\Delta T_{air}}\right)^3 \text{ for a dry cooling coil, and} \tag{10}$$

$$P_{fan} = K_{fan} \cdot \left(\frac{1}{\Delta T^*_{air}}\right)^3 \text{ for a wet cooling coil, where } \Delta T^*_{air} \text{ is the wet bulb} \tag{11}$$

temperature difference across the coil.

In accordance with an important aspect of the present invention, the optimal chilled water/supply air delta T calculation can be made using a linear chiller model. The above relationships enable the total power to be expressed solely in terms of a function with variables ΔT_{chw} and ΔT^*_{air}, with ΔT_{air} as follows:

$$\begin{aligned} P_{Tot}(\Delta T_{chw}, \Delta T_{air}) &= P_{comp}(\Delta T_{chw}) + P_{pump}(\Delta T_{chw}) + P_{fan}(\Delta T^*_{air}) \\ &= K_{comp} \cdot \Delta T_{chw} + K_{pump} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 + K_{fan} \cdot \left(\frac{1}{\Delta T^*_{air}}\right)^3 \end{aligned} \tag{12}$$

for a wet surface cooling coil

or

$$\begin{aligned} P_{Tot}(\Delta T_{chw}, \Delta T_{air}) &= P_{comp}(\Delta T_{chw}) + P_{pump}(\Delta T_{chw}) + P_{fan}(\Delta T_{air}) \\ &= K_{comp} \cdot \Delta T_{chw} + K_{pump} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 + K_{fan} \cdot \left(\frac{1}{\Delta T_{air}}\right)^3 \end{aligned} \tag{12a}$$

for a dry surface cooling coil

From Eqns. C-3 and C-3a in Appendix C, since we are assuming steady-state load conditions, the air flow rate and chilled water flow rate are at steady-state (constant) values (the second assumption) and we can relate the ΔT^{*}_{air} for the wet coil and the ΔT_{air} for the dry coil as follows:

$$K_3 \cdot CFM \cdot \Delta T^{*}_{air} = c \cdot m_{chw} \cdot \Delta T_{chw}$$
$$\Rightarrow \Delta T^{*}_{air} = K_3^{*} \cdot \Delta T_{chw} \qquad \textit{for the wet coil} \qquad (13)$$

or

$$K_3 \cdot CFM \cdot \Delta T_{air} = c \cdot m_{chw} \cdot \Delta T_{chw}$$
$$\Rightarrow \Delta T_{air} = K_3 \cdot \Delta T_{chw} \qquad \textit{for the dry coil} \qquad (13a)$$

Therefore, both ΔT^{*}_{air} and ΔT_{air} are proportional to ΔT_{chw} and either of Eqns. 12 and 12a can be written:

$$P_{Tot}(\Delta T_{chw}) = K_{comp} \cdot \Delta T_{chw} + K_{pump} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 + K_{fan}{'} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 \qquad (14)$$

for either a wet or dry surface cooling coil

By definition from differential calculus, a maximum or minimum of the total power curve, P_{Tot}, occurs at a $\Delta T_{chw} = \Delta T_{chw\,opt}$ when its first derivative is equal to zero:

$$\frac{d(P_{Tot})}{d(\Delta T_{chw})} = K_{comp} - 3K_{pump}(\Delta T_{chw\,opt})^{-4} - 3K'_{fan}(\Delta T_{chw\,opt})^{-4} = 0$$
$$\textit{or equivalently:} \quad K_{comp}(\Delta T_{chw\,opt})^{4} - 3K_{pump} - 3K'_{fan} = 0 \qquad (15)$$
$$\therefore \Delta T_{chw\,opt} = \sqrt[4]{\frac{3\left(K_{pump} + K'_{fan}\right)}{K_{comp}}}$$

To determine the optimum delta T of the air across the cooling coil, either Eqn. 13 or 13a must be used. If it is assumed to be a wet cooling coil, then:

$$\begin{aligned}
\frac{\Delta T^{*}_{air\ opt}}{\Delta T_{chw}} &= \frac{c \cdot m_{chw}}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \\
\therefore \quad \Delta T^{*}_{air\ opt} &= \Delta T_{chw} \cdot \left\{ \frac{c \cdot m_{chw}}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \right\} \\
&= \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \right\}
\end{aligned} \tag{15a}$$

where c is the specific heat of water, ω is the specific humidity of the incoming air stream, and the mass flow rate m_{chw} of chilled water has been replaced by the equivalent volumetric flow rate in GPM, multiplied by a conversion factor (500). Assuming that the chilled water valves in the cooling plant have been selected as equal percentage (which is the common design practice), we can calculate the GPM in Eqn. 15a directly from the control valve signal if we know the valve's *authority* (the ratio of the pressure drop across the valve when it is controlling to the pressure drop across the valve at full open position). The valve's authority can be determined from the valve manufacturer. The *1996 ASHRAE Systems and Equipment Handbook* provides a functional relationship between percent flow rate of water through the valve versus the percent valve lift, so that the water flow through the valve can be calculated as:

$$\begin{aligned}
GPM &= \left(Max\ flow\right) \times f\left(\%\ valve\ lift\right) \\
&= \left(Max\ flow\right) \times f\left(\%\ full\ span\ of\ control\ signal\right)
\end{aligned} \tag{15b}$$

where f is a nonlinear function defining the valve flow characteristic. Since the CFM and the humidity of the air stream can be either measured directly or calculated by the DDC system, we can calculate $\Delta T^{*}_{air\ opt}$ once $\Delta T_{chw\ opt}$ is known by the following procedure:

1. Calculate the GPM from Eqn. (15b).
2. Measure or calculate the CFM of the air across the cooling coil. CFM can be calculated from measured static pressure across the fan and manufacturer's fan curves.
3. Calculate the actual ΔT_{chw} across each cooling coil from the optimum chilled water supply temperature and known chilled water return temperature:

$$[1.08 + 4.5(0.45\omega)] \cdot CFM = 500 \cdot GPM \cdot (T_{chwr} - T_{chws\,opt})$$
$$\Rightarrow \Delta T_{chw} = \frac{[1.08 + 4.5(0.45\omega)] \cdot CFM}{500 \cdot GPM}, \quad where\,(T_{chwr} - T_{chws\,opt}) = \Delta T_{chw} \qquad (15c)$$

4. Calculate $\Delta T^{*}_{air\,opt}$ once the actual ΔT_{chw} is known:

$$\Delta T^{*}_{air\,opt} = \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{[1.08 + 4.5(0.45\omega)] \times CFM} \right\} \qquad (15d)$$

5. Finally, calculate the actual discharge air set point based on the known (measured) cooling coil inlet temperature:

$$T^{*}_{opt\,cc\,disch} = T^{*}_{cc\,inlet} - \Delta T^{*}_{air\,opt} \qquad (15e)$$

To determine whether the $\Delta T_{chw\,opt}$ calculated in Eqn. 15 corresponds to a maximum or minimum total power, we take the second derivative of P_{Tot} with respect to ΔT_{chw}:

$$\frac{d^2(P_{Tot})}{d(\Delta T_{chw})^2} = (-3) \cdot (-4) \cdot K_{pump} (\Delta T_{chw\,opt})^{-5} + (-3) \cdot (-4) \cdot K'_{fan} (\Delta T_{chw\,opt})^{-5} \qquad (16)$$

Since Eqn. 16 must always be positive, the function $P_{Tot}(\Delta T)$ must be concave upward and we see the calculated $\Delta T_{chw\,opt}$ in Eqn. 15 occurs at the <u>minimum</u> of P_{Tot}.

Note that for a wet surface cooling coil, the ΔT_{air} across the coil is really the wet bulb $\Delta T_{air} = \Delta T^{*}_{air}$. Thus, in the case for a wet surface cooling coil, a dew point sensor as well as a dry bulb temperature sensor would be required to calculate the inlet wet bulb temperature. The cooling coil discharge requires only a dry bulb temperature sensor, however, since we are assuming saturated conditions.

For a given measured ΔT_{chw} and a given load at steady-state conditions, K_{comp}, K_{pump} and K_{fan} can easily be calculated in a DDC controller from a single measurement of the compressor power, chilled water pump power and the air handler fan power, respectively, since we know the functional forms of $P_{comp}(\Delta T_{chw})$, $P_{pump}(\Delta T_{chw})$, and $P_{fan}(\Delta T_{chw})$, respectively. Once the optimum chilled water delta T has been found, the optimum air side delta T across the cooling coil can be calculated from a calculated value of the GPM of the chilled water, the known valve authority, and measured (or calculated) value of the fan CFM.

To implement the strategy in a DDC controller, the following steps are carried out for calculating the optimum chilled water and cooling coil air-side ΔT:

1. For each steady-state load condition:

a) determine K_{pump} from a single measurement of the pump power and the ΔT_{chw}:

$$K_{pump} = P_{pump} \times \left(\Delta T_{chw}\right)^3 \qquad (17)$$

b) determine K_{fan} from a single measurement of the fan power and the ΔT_{chw}:

$$K_{fan} = P_{fan} \times \left(\Delta T_{chw}\right)^3 \qquad (18)$$

c) determine K_{comp} from a single measurement of the chiller power and the ΔT_{chw} at steady-state load conditions:

$$K_{comp} = \frac{P_{comp}}{\Delta T_{chw}} \qquad (19)$$

2. Calculate the optimum ΔT for the chilled water in the PPCL program from the following formula:

$$\Delta T_{chw\ opt} = \sqrt[4]{\frac{3\left(K_{pump} + K_{fan}\right)}{K_{comp}}} \qquad (20)$$

3. Calculate the optimum chilled water supply set point from the following formulas:
For a primary-only chilled water system:

$$\begin{aligned}
&\Delta T_{chw\ opt} = T_{chwr} - T_{chws} \\
&\Rightarrow T_{chws\ opt} = T_{chwr} - \Delta T_{chw\ opt} \\
&and \\
&\Delta T_{air\ opt} = T_{cc\ inlet} - T_{cc\ discharge} \\
&\Rightarrow T_{cc\ discharge} = T_{cc\ inlet} - \Delta T_{air\ opt}
\end{aligned} \qquad (21)$$

For a primary-secondary chilled water system the optimum secondary chilled water temperature from the optimum primary and optimum secondary chilled water differential temperatures can be calculated by making use of the fact that the calculated load in the primary loop must equal the calculated load in the secondary chilled water loop:

$$\begin{aligned}
&\Delta T_{sec\ chw\ opt} \times sflow = \Delta T_{chw,\ opt} \times pflow \\
&\Rightarrow \Delta T_{sec\ chw\ opt} = \Delta T_{chw\ opt} \times \left(\frac{pflow}{sflow}\right) = \left(T_{sec\ chwr} - T_{sec\ chws\ opt}\right) \\
&\therefore T_{sec\ chws\ opt} = T_{sec\ chwr} - \Delta T_{chw\ opt} \times \left(\frac{pflow}{sflow}\right)
\end{aligned} \qquad (21a)$$

$$\begin{aligned}
where{:}\quad & pflow = Primary\ chilled\ water\ loop\ flow \\
& sflow = Secondary\ chilled\ water\ loop\ flow
\end{aligned}$$

4. Calculate the optimum ΔT of the air across the cooling coil in the DDC control program from the following formula:

$$\Delta T^{*}_{air\ opt} = \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \right\}$$

5. Calculate the optimum cooling coil discharge air temperature (dry bulb or wet bulb) from the known (measured) cooling coil inlet temperature (dry bulb or wet bulb).

$$T^{*}_{opt\ cc\ disch} = T^{*}_{cc\ inlet} - \Delta T^{*}_{air\ opt}$$
or
$$T_{opt\ cc\ disch} = T_{cc\ inlet} - \Delta T_{air\ opt}$$

6. After the load has assumed a new steady-state value, repeat steps 1-5.

In accordance with another important aspect of the present invention, the optimal chilled water/supply air delta T calculation can be made using a bi-quadratic chiller model. If the chiller is modeled by the more accurate bi-quadratic model of Eqn. 8, the expression for the total power becomes:

$$\begin{aligned} P_{Tot}(\Delta T_{chw}) &= P_{comp}(\Delta T_{chw}) + P_{pump}(\Delta T_{chw}) + P_{fan}(\Delta T_{chw}) \\ &= P_{des}\left[\left(A_0 + A_1 y + A_2 y^2\right) + \left(B_0 + B_1 y + B_2 y^2\right)x + \left(C_0 + C_1 y + C_2 y^2\right)x^2\right] \\ &\quad + K_{pump} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 + K'_{fan} \cdot \left(\frac{1}{\Delta T_{chw}}\right)^3 \end{aligned} \qquad (22)$$

for a wet surface cooling coil

As in the analysis for the linear chiller model, the expressions for a dry surface cooling coil are completely analogous as those for a wet coil. Therefore, only the expressions for a wet surface cooling coil will be presented here.

When the first derivative of Eqn. 22 is taken and equated to zero, then:

$$\frac{d(P_{Tot})}{d(\Delta T_{chw})} = P_{des}\left[\left(B_0 + B_1 y + B_2 y^2\right) + 2\left(C_0 + C_1 y + C_2 y^2\right)\Delta T_{chw\,opt}\right]\cdot\left[\frac{(sec\ CHW\ flow)}{24\cdot(chiller\ design\ tons)}\right]$$
$$- 3K_{pump}(\Delta T_{chw\,opt})^{-4} - 3K_{fan}(\Delta T_{chw\,opt})^{-4} = 0$$

or equivalently:

$$P_{des}\left[\frac{(sec\ CHW\ flow)}{24\cdot(chiller\ design\ tons)}\right]\cdot\left[2\left(C_0 + C_1 y + C_2 y^2\right)\Delta T_{chw\,opt}{}^5 + \left(B_0 + B_1 y + B_2 y^2\right)\Delta T_{chw\,opt}{}^4\right]$$
$$- 3K_{pump} - 3K_{fan} = 0 \qquad (23)$$

Eqn. 23 is a fifth order polynomial, for which the roots must be found by means of a numerical method. Descartes' polynomial rule states that the number of positive roots is equal to the number of sign changes of the coefficients or is less than this number by an even integer. It can be shown that the coefficients B_2 and C_2 in Eqn. 23 are both negative, all other coefficients are positive, and since K_{pump} and K_{fan} must also be positive, Eqn. 23 has three sign changes. Therefore, there will be either three positive real roots or one positive real root of the equation. The first real root can be found by means of the Newton-Raphson Method and it can be shown that this is the <u>only</u> real root. The Newton-Raphson Method requires a first approximation to the solution of Eqn. 23. This approximation can be calculated from Eqn. 20, the results of using a linear chiller model. The Newton-Raphson Method and Eqn. 20 can easily be programmed into a DDC controller, so a root can be found to Eqn. 23..

While the foregoing has related to a cooling plant, the present invention is also applicable to a heating plant such as is shown in FIG. 3, which shows the equipment being modeled in the heating plant. The model for the hot water pump and the air handler fan blowing across a heating coil is completely analogous to that for the cooling plant. The model for a hot water boiler can easily be derived from the basic definition of its efficiency:

$$\eta_{boiler} = \frac{m_{hw} \cdot c \cdot \Delta T_{hw}}{P_{boiler}} \qquad \textit{where } c = \textit{specific heat of the hot water}$$

$$\therefore P_{boiler} = \frac{m_{hw} \cdot c \cdot \Delta T_{hw}}{\eta_{boiler}} \tag{24}$$

The hot water pump and air handler model derivations are completely analogous to the results derived for the chilled water pump and air handler fan, Eqns. 9 and 10, respectively:

$$P_{hw\ pump} = K_5 \cdot \left(\frac{1}{\Delta T_{hw}}\right)^3 \tag{25}$$

$$P_{fan} = K_{fan} \cdot \left(\frac{1}{\Delta T_{air}}\right)^3$$ where ΔT_{air} is temperature difference across the hot water coil. (26)

The optimum hot water ΔT is completely analogous to the results derived for the linear chiller model, Eqn. 15:

$$\Delta T_{hw\ opt} = \sqrt[4]{\frac{3\left(K_{hw\ pump} + K_{fan}\right)}{K_{boiler}}} \tag{27}$$

Therefore the optimum ΔT_{air} across the heating coil can be calculated once ΔT_{hw} is determined from:

$$\Delta T_{air\ opt} = \Delta T_{hw} \cdot \left\{\frac{500 \cdot GPM}{1.08 \times CFM}\right\} \tag{27-a}$$

The following are observations that can be made about the modeling techniques for the power components in a cooling and heating plant, as implemented in a DDC controller:

1. The "*K*" constants used in the modeling equations can be described as "characterization factors" that must be determined from measured power and ΔT_{chw} of each chiller, boiler, chilled and hot water pump and air handler fan at each steady-state load level. Determining these constants characterizes the power consumption curves of the equipment for each load level. The "*K*" characterization factors for the linear chiller model, the hot water boiler, the chilled and hot water pump, and air handler fan can easily be determined from only a single measurement of power consumed by that component and the ΔT of the chilled or hot water across that component at a given load level.
2. For each power consuming component of the cooling or heating plant, the efficiency of that component varies with the load. This is why it is necessary to recalculate the "*K*" characterization factors of the pumps and AHU fans and the A, B, and C coefficients of the chillers for each load level.
3. The use of constant speed or variable speed chillers, chilled water pumps, or air handler fans does not affect the general formula for $\Delta T_{chw\,opt}$ in Eqn. 15 or the solution of Eqn. 23. For example, if constant speed chilled water pumps with three-way chilled valves are used, the power component of the chilled water pump remains constant at any load level, and $\Delta T_{chw\,opt}$ in Eqn. 15 simplifies to:

$$\Delta T_{chw\,opt} = \sqrt[4]{\frac{3\left(K_{pump} + K_{fan}\right)}{K_{comp}}} = \sqrt[4]{\frac{3K_{fan}}{K_{comp}}} \qquad (28)$$

4. To determine the characterization factors for multiple chillers, chilled water pumps, and air handler fans, Appendices A, B, and C show that it is sufficient to determine the characterization factors for each piece of equipment from measured values of the power and ΔT_{chw} across each piece of equipment, and then sum the characterization factors for each piece of equipment to obtain the total power. For example, for a facility that has *n* chillers, *m* chilled water pumps, and *o* air handler fans currently on-line, the DDC controller must calculate:

$$P_{Tot} = \sum_{n=1}^{n} P_{comp} + \sum_{m=1}^{m} P_{pump} + \sum_{o=1}^{o} P_{fan}$$

$$= \Delta T_{chw} \cdot \sum (K_{comp,1} + K_{comp,2} + \ldots + K_{comp,n}) + \left(\frac{1}{\Delta T_{chw}}\right)^3 \cdot \sum (K_{pump,1} + K_{pump,2} + \ldots + K_{pump,m})$$

$$+ \left(\frac{1}{\Delta T_{chw}}\right)^3 \cdot \sum (K_{fan,1} + K_{fan,2} + \ldots + K_{fan,o})$$

where $\Delta T_{chw} = K \cdot \Delta T_{air}$ *for optimal operation*

(29)

5. To determine when steady-state load conditions exist, cooling and heating load can be measured either in the mechanical room of the cooling or heating plant (from water-side flow and ΔT_{chw} *or* ΔT_{hw}) or out in the space (from CFM of the fan or position of the chilled water or hot water valve). However, it is recommended that load be measured in the space because this will tend to minimize the transient effect due to the "flush time" of the chilled water through the system. Chilled water flush time is typically on the order of 15 - 20 minutes (Hackner et al. 1985). That is, by measuring load in the space, an optimal ΔT can be calculated that is more appropriate for the actual load rather than the load that existed 15 or 20 minutes previously, as would be calculated at the central plant mechanical room.

From the foregoing, it should be understood that an improved DDC controller for heating and/or cooling plants has been shown and described which has many advantages and desirable attributes. The controller is able to implement a control strategy that provides near-optimal global set points for a heating and/or cooling plant. The controller is capable of providing set points that can provide substantial energy savings in the operation of a heating and cooling plant.

While various embodiments of the present invention have been shown and described, it should be understood that other modifications, substitutions and alternatives are apparent to one of ordinary skill in the art. Such modifications, substitutions and alternatives can be made without departing from the spirit and scope of the invention which should be determined from the appended claims.

Various features of the invention are set forth in the appended claims.

WHAT IS CLAIMED IS:

1. A controller for controlling at least a cooling plant of the type which has a primary-only chilled water system, and the plant comprises at least one of each of a cooling tower means, a chilled water pump, an air handling fan, an air cooling coil, a condenser, a condenser water pump, a chiller and an evaporator, said controller being adapted to provide near-optimal global set points for reducing the power consumption of the cooling plant to a level approaching a minimum, said controller comprising:

processing means adapted to receive input data relating to measured power consumption of the chiller, the chilled water pump and the air handler fan, and to generate output signals indicative of set points for controlling the operation of the cooling plant, said processing means including storage means for storing program information and data relating to the operation of the controller;

said program information being adapted to determine the optimum chilled water delta $T_{chw\ opt}$ across the evaporator for a given load and measured delta T_{chw}, utilizing the formula:

$$\Delta T_{chw\ opt} = \sqrt[4]{\frac{3\left(K_{pump} + K_{fan}\right)}{K_{comp}}}$$

where: $$K_{pump} = P_{pump} \times \left(\Delta T_{chw}\right)^3$$

$$K_{fan} = P_{fan} \times \left(\Delta T_{chw}\right)^3 \qquad \text{and}$$

$$K_{comp} = \frac{P_{comp}}{\Delta T_{chw}}$$

said program information being adapted to determine the optimum chilled water supply set point utilizing the formula:

$$T_{chws\ opt} = T_{chwr} - \text{delta } T_{chw\ opt}$$

and to output a control signal to said cooling plant to produce said $T_{chws\ opt}$;

said program information being adapted to determine the optimum air delta $T_{air\ opt}$ across the cooling coil utilizing the formula:

$$\Delta T^{*}_{air\ opt} = \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \right\}$$

said program information being adapted to determine the optimum cooling coil discharge air temperature from the measured cooling coil inlet temperature using the formula:

$$T_{opt\ cc\ disch} = T_{cc\ inlet} - \text{delta } T_{air\ opt}$$

and to output a control signal to said cooling plant to produce said $T_{opt\ cc\ disch}$.

2. A controller as defined in claim 1 wherein said program information is adapted to determine the near-optimum cooling tower air flow utilizing the formula:

$$G_{twr} = 1 - \beta_{twr}(PLR_{twr,\,cap} - PLR) \qquad 0.25 < PLR < 1.0$$

where

G_{twr} = the tower air flow divided by the maximum air flow with all cells operating at high speed

PLR = the chilled water load divided by the total chiller cooling capacity (part-load ratio)

$PLR_{twr,\,cap}$ = value of PLR at which the tower operates at its capacity (G_{twr} = 1)

β_{twr} = the slope of the relative tower air flow (G_{twr}) versus the PLR function.

3. A controller as defined in claim 2 wherein said program information is adapted to determine the near-optimum condenser water flow by determining the cooling tower effectiveness by using the equation

$$\varepsilon = \frac{Q_{tower}}{Min(Q_{a,\max}, Q_{w,\max})}$$

where

ε = *effectiveness of cooling tower*

$Q_{a,\max} = m_{a,twr}(h_{s,cwr} - h_{s,i})$, *sigma energy*, $h_{s,\_} = h_{air,\_} - \omega\_c_{pw}T_{wb}$

$Q_{w,\max} = m_{cw}c_{pw}(T_{cwr} - T_{wb})$

$m_{a,twr}$ = *tower air flow rate*

m_{cw} = *condenser water flow rate*

T_{cwr} = *condenser water return temperature*

T_{wb} = *ambient air wet bulb temperature*

and by then equating $Q_{a,\max}$ and $Q_{w,\max}$ to calculate m_{cw} once $m_{a,twr}$ has been determined.

4. A controller as defined in claim 3 wherein said optimum cooling coil discharge air temperature is a dry bulb temperature when said $T_{cc\ inlet}$ and delta $T_{air\ opt}$ values are dry bulb temperatures, and said optimum cooling coil discharge air temperature is a wet bulb temperature when said $T_{cc\ inlet}$ and delta $T_{air\ opt}$ values are wet bulb temperatures.

5. A controller for controlling at least a cooling plant of the type which has a primary-secondary chilled water system, and the cooling plant comprises at least one of each of a cooling tower means, a chilled water pump, an air handling fan, an air cooling coil, a condenser, a condenser water pump, a chiller and an evaporator, said controller being adapted to provide near-optimal global set points for reducing the power

consumption of the cooling plant to a level approaching a minimum, said controller comprising:

processing means adapted to receive input data relating to measured power consumption of the chiller, the chilled water pump and the air handler fan, and to generate output signals indicative of set points for controlling the operation of the cooling plant, said processing means including storage means for storing program information and data relating to the operation of the controller;

said program information being adapted to determine the optimum chilled water delta $T_{chw\ opt}$ across the evaporator for a given load and measured delta T_{chw}, utilizing the formula:

$$\Delta T_{chw\ opt} = \sqrt[4]{\frac{3\left(K_{pump} + K_{fan}\right)}{K_{comp}}}$$

where: $K_{pump} = P_{pump} \times \left(\Delta T_{chw}\right)^3$

$K_{fan} = P_{fan} \times \left(\Delta T_{chw}\right)^3$ and

$$K_{comp} = \frac{P_{comp}}{\Delta T_{chw}}$$

said program information being adapted to determine the optimum chilled water supply set point utilizing the formula:

$$T_{sec\ chws\ opt} = T_{sec\ chwr} - \text{delta } T_{chw\ opt} \times (\text{pflow}/\text{sflow})$$

where pflow = Primary chilled water loop flow, and

sflow = Secondary chilled water loop flow

and to output a control signal to said cooling plant to produce said $T_{chwr\ opt}$;

said program information being adapted to determine the optimum air delta $T_{air\,opt}$ across the cooling coil utilizing the formula:

$$\Delta T^{*}_{air\,opt} = \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{\left[1.08 + 4.5(0.45\omega)\right] \times CFM} \right\}$$

said program information being adapted to determine the optimum cooling coil discharge air temperature from the measured cooling coil inlet temperature using the formula:

$$T_{opt\,cc\,disch} \quad = \quad T_{cc\,inlet} \quad - \quad \text{delta } T_{air\,opt}$$

and to output a control signal to said cooling plant to produce said $T_{opt\,cc\,disch}$.

6. A controller for controlling at least a heating plant of the type which has at least one of each of a hot water boiler, a hot water pump and an air handler fan, said controller being adapted to provide near-optimal global set points for reducing the power consumption of the heating plant to a level approaching a minimum, said controller comprising:

processing means adapted to receive input data relating to measured power consumption of the chiller, the chilled water pump and the air handler fan, and to generate output signals indicative of set points for controlling the operation of the cooling plant, said processing means including storage means for storing program information and data relating to the operation of the controller;

said program information being adapted to determine the optimum hot water delta $T_{hw\,opt}$ across the input and output of the hot water boiler for a given load and measured delta T_{hw}, utilizing the formula:

$$\Delta T^{*}_{hw\,opt} = \sqrt[4]{\frac{3\left(K_{hw\,pump} + K_{fan}\right)}{K_{boiler}}}$$

and to determine the optimum ΔT_{air} across the heating coil can be calculated once ΔT_{hw} is determined from the equation:

$$\Delta T_{air\ opt} = \Delta T_{hw} \cdot \left\{ \frac{500 \cdot GPM}{1.08 \times CFM} \right\} .$$

7. A method of determining near-optimal global set points for reducing the power consumption to a level approaching a minimum for a cooling plant operating in a steady-state condition, said set points including the optimum temperature change across an evaporator in a cooling plant of the type which has at least one of each of a cooling tower means, a chilled water pump, an air handling fan, an air cooling coil, a condenser, a condenser water pump, a chiller and an evaporator, said set points being determined in a direct digital electronic controller adapted to control the cooling plant, the method comprising:

measuring the power being consumed by the chilled water pump, the air handling fan and the chiller and the actual temperature change across the evaporator;

calculating the K constants from the equations

$$K_{pump} = P_{pump} \times (\Delta T_{chw})^3 \ , \ K_{fan} = P_{fan} \times (\Delta T_{chw})^3 \text{ and } K_{comp} = \frac{P_{comp}}{\Delta T_{chw}} ;$$

calculating the optimum ΔT for the chilled water from the following formula:

$$\Delta T_{chw\ opt} = \sqrt[4]{\frac{3(K_{pump} + K_{fan})}{K_{comp}}} .$$

8. A method as defined in claim 7 further including determining a set point for the optimal temperature change across the cooling coil from the formula

$$\Delta T^{*}_{air\ opt} = \Delta T_{chw} \cdot \left\{ \frac{500 \cdot GPM}{[1.08 + 4.5(0.45\omega)] \times CFM} \right\} .$$

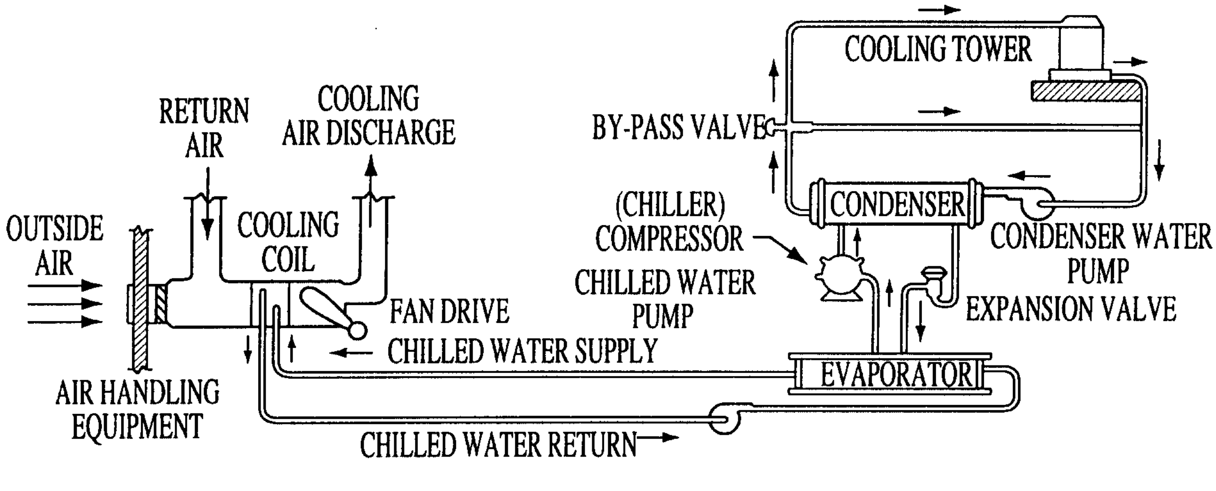

COOLING TOWER
RETURN AIR
COOLING AIR DISCHARGE
BY-PASS VALVE
OUTSIDE AIR
COOLING COIL
CONDENSER
(CHILLER) COMPRESSOR
CONDENSER WATER PUMP
CHILLED WATER PUMP
EXPANSION VALVE
FAN DRIVE
CHILLED WATER SUPPLY
EVAPORATOR
AIR HANDLING EQUIPMENT
CHILLED WATER RETURN

FIG. 1

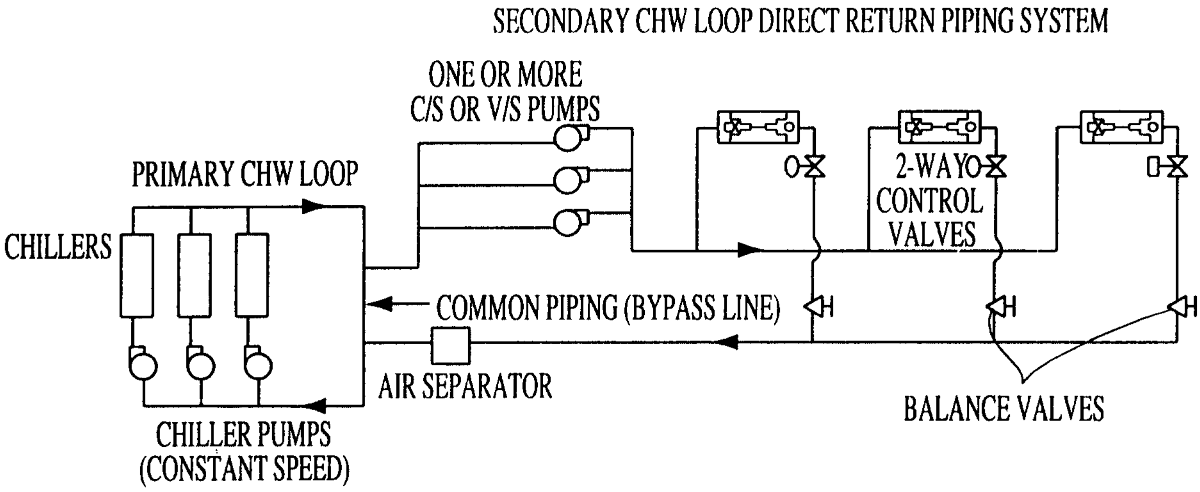

SECONDARY CHW LOOP DIRECT RETURN PIPING SYSTEM
ONE OR MORE C/S OR V/S PUMPS
PRIMARY CHW LOOP
2-WAY CONTROL VALVES
CHILLERS
COMMON PIPING (BYPASS LINE)
AIR SEPARATOR
BALANCE VALVES
CHILLER PUMPS (CONSTANT SPEED)

FIG. 2

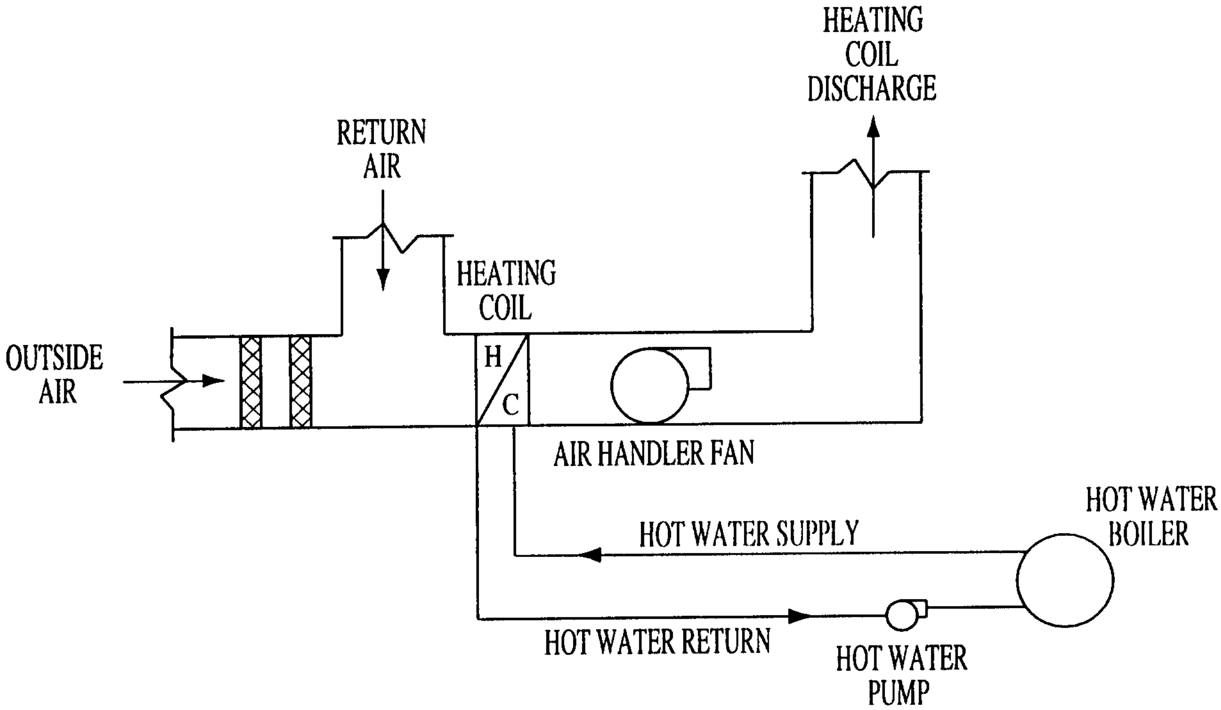
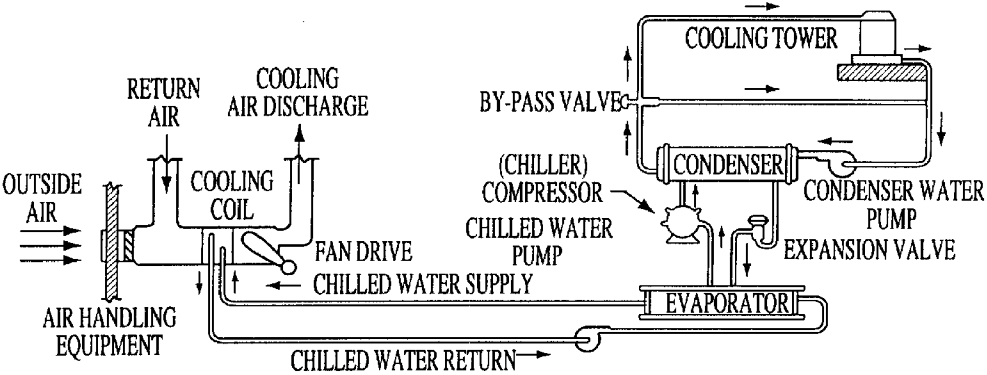

HEATING
COIL
DISCHARGE
RETURN
AIR
HEATING
COIL
OUTSIDE
AIR
H
C
AIR HANDLER FAN
HOT WATER
BOILER
HOT WATER SUPPLY
HOT WATER RETURN
HOT WATER
PUMP

FIG. 3


COOLING TOWER
BY-PASS VALVE
RETURN AIR
COOLING AIR DISCHARGE
OUTSIDE AIR
COOLING COIL
CONDENSER
(CHILLER) COMPRESSOR
CONDENSER WATER PUMP
CHILLED WATER PUMP
EXPANSION VALVE
FAN DRIVE
CHILLED WATER SUPPLY
EVAPORATOR
AIR HANDLING EQUIPMENT
CHILLED WATER RETURN