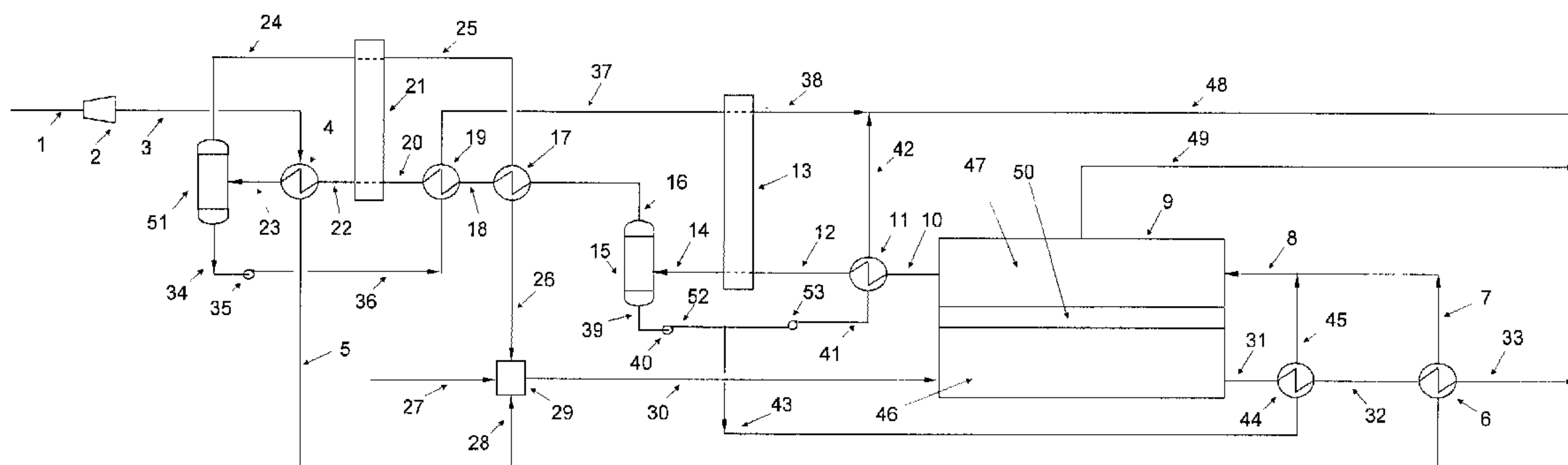




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(54) Titre : METHODE DE PRODUCTION D'HUILE LOURDE AU MOYEN D'UNE PILE A COMBUSTIBLE
 (54) Title: METHOD OF PRODUCING HEAVY OIL USING A FUEL CELL



(57) **Abrégé/Abstract:**

A method to enhance the production of oil from underground oil deposits recovers the anode exhaust stream components and thermal energy from a fuel cell for injection in a well pipeline to heat, displace and flow oil into a production well pipeline at optimal reservoir pressure and operating conditions. The process recovers and injects the GHG emission stream from a fuel cell anode exhaust stream into an oil reservoir to increase oil production.

ABSTRACT OF THE DISCLOSURE

A method to enhance the production of oil from underground oil deposits recovers the anode exhaust stream components and thermal energy from a fuel cell for injection in a well pipeline to heat, displace and flow oil into a production well pipeline at optimal reservoir pressure and operating conditions. The process recovers and injects the GHG emission stream from a fuel cell anode exhaust stream into an oil reservoir to increase oil production.

METHOD OF PRODUCING HEAVY OIL USING A FUEL CELL

FIELD

[0001] This relates to a method that enhances the production of heavy oil from underground oil deposits by reducing in situ the viscosity of heavy oil to flow from an oil reservoir to a production well pipeline. The process recovers the anode exhaust stream components and thermal energy of a fuel cell for injection in a well pipeline to heat, displace and flow heavy oil into a production well pipeline at optimal reservoir pressure and operating conditions.

10 BACKGROUND

[0002] A variety of processes are currently used to recover viscous hydrocarbons such as heavy oil or bitumen from underground oil deposits. Typically, in situ methods are used in heavy oil or bitumen at depths greater than 50 meters where it is no longer economic to recover the hydrocarbon by current surface mining technologies. Depending on the operating conditions of the in situ process and the geology of the reservoir, in situ processes can recover between 25 and 75% of the oil.

[0003] The primary focus associated with producing hydrocarbons from such deposits is to reduce the in situ viscosity of the heavy oil so it can flow from the reservoir to the production well pipeline. The present industry practice to reduce in situ heavy oil viscosity is, raising the reservoir temperature with steam and/or by dilution with solvents.

[0004] Steam Assisted Gravity Drainage (SAGD) is a popular in situ oil recovery method. SAGD uses two horizontal well pipelines (a well pair) positioned in a reservoir to recover hydrocarbons. This method is more environmentally benign than oil sands mining. In the SAGD process, two well pipelines are drilled paralleled to each other by directional drilling. The bottom well pipeline is the production well pipeline and is typically located just above the base of the

reservoir. The top well pipeline is the injection well pipeline and is typically located between 15 and 30 feet above the production well pipeline. The top well pipeline injects steam into the reservoir from the surface. In the reservoir, the injected steam flows from the injection well pipeline and loses its latent heat to the heavy oil or bitumen, as a result the viscosity of the heated heavy oil or bitumen decreases and flows under gravity towards the production well pipeline located below the injection well pipeline. Anywhere between 4 and 20 well-pairs are drilled on a particular section of land or pad. All the well-pairs are drilled parallel to one another, about 300 feet apart, with half of the well-pairs oriented in one direction, and the other half of the well-pairs typically oriented 180° in the opposite direction to maximize reservoir coverage. A 15 ft separation between injection and production well pipelines has been proven to be the optimal gap which allows for the maximum reservoir production due to the most effective impact of the injected steam. Although the separation between injector and production wells pipelines are planned for 15 ft, some wells have as high as 30 ft gaps, reducing production capability from that particular zone. Typically, a SAGD process is considered thermally efficient if its Steam to Oil Ratio (SOR) is 3 or lower. The SAGD process requires about 1,200 cubic feet of natural gas to generate steam per 1 barrel of bitumen produced. Canada National Energy Board (NEB) estimates capital cost of \$18 - \$22 to produce a barrel of bitumen by the SAGD method. The high ratio of water requirement for steam generation in the SAGD process is forcing the industry to look at alternative processes to reduce water consumption.

20 [0005] An alternative process to reduce steam usage is an extension of the SAGD process, the Steam and Gas Push (SAGP) where steam and a non-condensable gas are co-injected into the reservoir. The non-condensable gas provides an insulating layer and improves the thermal efficiency of the process, resulting in a reduction of steam requirements.

25 [0006] Another alternative process, to replace steam usage is the Vapour Extraction Process (VAPEX) where a solvent is injected into the reservoir. Similar to SAGD, it consists of two horizontal well pipelines positioned in the reservoir, whereas the top well is the injection well pipeline and the bottom well is the production well pipeline. In VAPEX, a gaseous solvent such as propane is injected into the reservoir instead of steam. The injected solvent condenses and mixes

with the heavy oil or bitumen to dilute and reduce its viscosity. Under the action of gravity, the mixture of solvent and bitumen flow towards the production well pipeline and is pumped to the surface. A major concern with the VAPEX process is how to control the significant solvent losses to the reservoir, which has a large impact on its economics.

5 [0007] More recently, new processes such as Combustion Assisted Gravity Drainage and Toe to Heel Air Injection (THAI) are promoted as being more environmentally responsible since no emissions are released into the atmosphere. These processes employ in situ combustion to heat the reservoir by compressing combustion air into the reservoir to support in-situ combustion. In all of the described processes, the objective is to reduce viscosity and increase oil flow to the production
10 well pipeline.

[0008] Another process involves an injection well and a production well, both of which are vertical. Water, carbon dioxide, or a combination of both may be used to pressurize the injection well and flush oil from a subsurface oil-bearing formation into the production well. This is sometimes referred to as a “huff and puff” process.

15

SUMMARY

[0009] According to an aspect, the method disclosed herein may be used to enhance the production of heavy oil or bitumen from underground oil deposits into a production well pipeline. The method reduces a reservoir heavy oil viscosity by injecting exhaust gases typically released into
20 the atmosphere from consumption of natural gas. These exhaust gases and its thermal energy is preferentially recovered from an anode exhaust stream of a fuel cell. The natural gas fuel cell anode exhaust stream composition unlike a natural gas combustion exhaust stream is primarily carbon dioxide and water. The total mass flowrate of a fuel cell anode exhaust stream is typically less than
25 and re-use. In the disclosed process, a fuel cell anode exhaust stream is cooled, condensed, recovered, pumped, re-heated and routed to an injection well pipeline at the optimal reservoir operating pressure and temperature. This is another feature of the process, capable of meeting a

wide range of reservoir pressure and temperature operation parameters compared to existing gravity drainage processes.

[0010] According to an aspect, the method may be used to enhance the production of heavy oil or bitumen from underground oil deposits. The process recovers the anode exhaust stream and its thermal energy from a power generation natural gas fuel cell to heat, displace and flow heavy oil in a reservoir to a production well pipeline at optimal reservoir pressure and temperature conditions. The process of generating power with a natural gas fuel cell differs from standard power generation plants that use natural gas. In a fuel cell, natural gas is consumed at the anode by an electrochemical reaction that produces electricity and a hot exhaust stream of gases, mainly water vapor and carbon dioxide. The other power generation plants combust natural gas to produce electricity and a large hot exhaust gas stream, mainly nitrogen oxide.

[0011] The method discussed herein benefits from recovering the fuel cell anode exhaust stream and its thermal energy to enhance the production of heavy oil. It is well documented that CO₂ injection into oil fields resulted into an increase in heavy oil production. Today, operators inject more than 1.6 billion cubic feet per day into Permian Basin fields in the U.S., to produce 170,000 barrels of incremental oil per day as reported by the National Energy Technology Laboratory of the U.S. Department of Energy. Unlike current CO₂ injection methods where it is first processed, compressed and pipeline transported to well sites, the inventive process generates and pumps the CO₂ at point of use. The use of steam to heat underground oil deposits is well documented and proven as per the SAGD process. Unlike the above processes, the present method may be used to meet optimal reservoir pressure and temperature conditions at substantial less energy consumption.

[0012] Some aspects of the method may include: power generation by chemical reaction of methane in a fuel cell at an oil production field; elimination or reduction in GHG emissions, as the fuel cell anode exhaust stream may be fully recovered and injected into the oil reservoir, 5 Kg of water and carbon dioxide per Kg of methane reacted in a fuel cell; elimination or reduction in external water requirements as a fuel cell power plant is a net water producer, where the anode chemical reaction of hydrogen with oxygen by stoichiometry produces 2.25 Kg of water per Kg of

methane; production of carbon dioxide in-situ, the anode chemical reaction of carbon with oxygen by stoichiometry produces 2.75 Kg of carbon dioxide per Kg of methane; recovery of a fuel cell anode exhaust stream and its thermal energy to enhance oil production; ability to deliver the recovered anode exhaust stream at optimal reservoir pressure and temperature; substantial reduction
5 in energy consumption versus current practices of oil production processes.

[0013] In one embodiment, the process may produce electricity for export from a carbonate fuel cell and recovers its anode exhaust stream of carbon dioxide and water to inject into an oil reservoir at optimal pressure and temperature operation conditions to enhance oil production. The process for the enhancement of oil production at an oil field may comprise: reducing the
10 natural gas pressure supply to the fuel cell anode through an expander generator, producing electricity and a refrigerant natural gas stream; causing the refrigerant natural gas fuel cell anode supply stream to enter a heat exchanger in a counter-current flow with the gaseous anode exhaust stream to cool and condense carbon dioxide; causing the fuel cell anode natural gas supply stream to exit the counter-current heat exchanger and be further heated in another counter-current heat
15 exchanger by the cathode exhaust gaseous stream; causing the heated natural gas supply stream to enter the fuel cell anode where it is converted by steam reforming and electrochemical reactions into electricity and a high temperature anode exhaust gas stream of mainly carbon dioxide and water; pre-cooling the high temperature anode exhaust gas stream in a counter-current flow heat exchanger with the recovered water; further cooling the anode exhaust gas stream in a counter-
20 current flow heat exchanger with the recovered carbon dioxide to condense the water fraction of the anode exhaust gas stream; recovering the condensed water fraction of the anode exhaust gas stream in a gas/liquid separator and route the separated anode exhaust gaseous carbon dioxide stream for further cooling in a counter-current heat exchanger with the recovered liquid carbon dioxide stream; further cooling the anode exhaust gaseous carbon dioxide stream in a counter-
25 current heat exchanger with a cold carbon dioxide gaseous stream; further cooling the anode exhaust gaseous carbon dioxide stream in a counter-current heat exchanger with the fuel cell anode refrigerant natural gas supply stream to condense the carbon dioxide; pumping the recovered liquid carbon dioxide stream to optimal oil reservoir pressure and heating the recovered liquid carbon dioxide stream in a heat exchange in a counter-current flow with the

anode exhaust stream to optimal oil reservoir temperature and route it to injection well pipeline; pumping to optimal oil reservoir pressure the recovered water stream and heat exchange in a counter-current flow with the anode exhaust stream to optimal oil reservoir temperature and route it to injection well pipeline; mixing the gaseous carbon dioxide stream from the carbon dioxide separator with fresh air and catalysing the mixture in a catalytic oxidizer to heat this oxidant stream up to fuel cell cathode temperature, where the cathode consumes oxygen from the air and the carbon dioxide to produce a carbonate ion that is transferred through the fuel cell electrolyte layer to the anode to react with the anode hydrogen producing; water, carbon dioxide and electricity; and routing a portion of the recovered water to produce steam in a counter-current flow heat exchanger with the cathode exhaust gas stream to supply steam reformer at the anode.

[0014] The process described herein may enhance oil field production by first recovering the water and carbon dioxide from a fuel cell anode exhaust stream, and second, by pumping and heating them in a counter-current heat exchangers to optimal oil reservoir operating conditions before entering the injection well pipeline to heat and reduce the viscosity of oil in a reservoir. The process may allow the elimination of the current industry practices of steam generation for SAGD operations and substantially reduces its associated environmental challenges. Moreover, it recovers and provides carbon dioxide, a solvent for oil production enhancement at point of use.

[0015] As will hereinafter be described, the above method can operate at any oil field production sites where heat, water and solvents are required to enhance oil production.

[0016] The method described herein was developed with a view to supply thermal energy, water and carbon dioxide to oil production fields from a fuel cell anode exhaust stream, thereby eliminating the need for an external water source and its processing for steam generation as well as the energy required to produce it. The process added benefit is the recovery and supply in-situ of a GHG emission gas, carbon dioxide, an oil miscible solvent that reduces oil viscosity and enhances oil production at a reservoir.

[0017] As will hereinafter be further described, there is provided, in one aspect, an oil production enhancement process, which includes a natural gas supply stream to a fuel cell, first reducing the natural gas pressure through a gas expander/generator producing a refrigerant natural gas stream and electricity. The refrigerant natural gas stream is pre-heated in a counter-current heat exchanger with a separated anode exhaust gaseous stream to condense and produce liquid carbon dioxide. The heated fuel cell natural gas stream is further heated and fed to the fuel cell anode where first it is steam reformed to produce hydrogen and carbon dioxide, the hydrogen is further reacted with a carbonate ion to produce water, carbon dioxide and electricity. The anode hot exhaust gas stream, is cooled, condensed, separated, recovered, pumped and re-heated to optimal oil reservoir pressure and temperature operation conditions before injection into an oil reservoir to heat and reduce oil viscosity for the enhancement of oil production. The current industry practices of oil production use steam generated from natural bodies of water and or imported solvents. The objective of the process is to provide the steam and solvent required for enhancing oil production from a by-product of a power plant, the fuel cell anode exhaust stream.

[0018] According to an aspect, there is provided a method of injecting fluids into an underground formation using exhaust streams from a fuel cell, such as to produce heavy oil from an oil bearing formation, the fuel cell comprising an anode and a cathode, the fuel cell having an anode input stream comprising at least a fuel and water, a cathode input stream comprising at least oxygen and carbon dioxide, an anode exhaust stream comprising at least carbon dioxide and steam, and a cathode exhaust stream. The method comprises the steps of: condensing and separating water from the anode exhaust stream to produce a stream of water and a stream of carbon dioxide; heating a first portion of the stream of water to produce a stream of steam; combining the stream of steam and the fuel to form the anode input stream; producing an injection stream of steam by heating and pumping a second portion of the stream of water to a desired temperature and pressure; obtaining a stream of condensed carbon dioxide by condensing at least a portion of the carbon dioxide in the stream of carbon dioxide; heating and pumping the stream of condensed carbon dioxide to a desired temperature and pressure to produce an injection stream of carbon dioxide gas; and injecting at least one of the injection stream of

carbon dioxide gas and the injection stream of steam into the underground formation, and preferably both if injected for the purpose of producing oil from an oil bearing formation.

[0019] The method may comprise one or more of the following aspects: the fuel of the anode input stream may comprises a stream of hydrocarbons such as natural gas; the natural gas
5 may be obtained from a supply of natural gas, with the supply of natural gas being used as a refrigerant to condense the portion of the carbon dioxide to form the stream of condensed carbon dioxide; the supply of natural gas may be a liquid natural gas (LNG) tank; the supply of natural gas may be a pressurized stream of natural gas, and wherein the pressurized stream of natural gas may be expanded and cooled to produce cold temperatures; the supply of natural gas may be
10 passed through at least one of a refrigeration plant and a condenser and air cooler; the stream of carbon dioxide may be compressed to meet desired operations properties using a pressure enthalpy diagram of the stream; the method may further comprise the step of injecting at least one of water and a solvent into the oil bearing formation with the injection stream of carbon dioxide and the injection stream of steam; after condensing, the stream of carbon dioxide may be
15 separated into the stream of condensed carbon dioxide and a cathode stream of carbon dioxide; the method may further comprise the step of combining oxygen and the cathode stream of carbon dioxide to form the cathode input stream; forming the cathode input stream may comprise combining the first stream of carbon dioxide and atmospheric air; the anode exhaust stream may further comprise residual hydrogen, and wherein the cathode stream of carbon dioxide may
20 further comprise the residual hydrogen; forming the cathode input stream may further comprise preheating the first stream of carbon dioxide and oxygen in a combustion heater that is fuelled by a hydrocarbon and the residual hydrogen; and the method may further comprise the step of supplying carbon dioxide for the cathode input stream from a source of captured carbon dioxide.

25 BRIEF DESCRIPTION OF THE DRAWINGS

[0020] These and other features of the invention will become more apparent from the following description in which reference is made to the appended drawings, the drawings are for the purpose

of illustration only and are not intended to in any way limit the scope of the invention to the particular embodiment or embodiments shown, wherein:

FIG. 1 is a schematic diagram of a fuel cell with the water, carbon dioxide and thermal energy of the anode exhaust stream being recovered for injection into an oil production reservoir.

5 FIG. 2 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that employs a compression step in the separated anode exhaust stream.

FIG. 3 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that employs a pressure reducing valve in the fuel cell natural gas supply in lieu of an expander/generator.

10 FIG. 4 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that compressing the fuel cell natural gas supply, and uses an ambient air heat exchanger before a pressure reducing valve, to produce a refrigerant natural gas supply.

FIG. 5 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that provides additional refrigeration to the fuel cell natural gas supply after a pressure reducing valve.

FIG. 6 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that uses liquid natural gas (LNG) as the fuel cell's natural gas supply

FIG. 7 is a schematic diagram of an alternative method of recovering the fuel cell anode exhaust stream that permits water or solvents to be added to the recovered injection stream to the reservoir.

FIG. 8 is a schematic diagram of a fuel cell that is fuelled by alternative sources of fuel, such as biogas, and carbon dioxide.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENT

25 [0021] The method described below was developed primarily with a view to supply thermal energy, water and carbon dioxide to oil production fields from a fuel cell anode exhaust stream. The method uses a different approach to provide steam and/or solvents for the enhancement of oil production. The system here described takes advantage of a concentrated hot exhaust gas stream

from a fuel cell anode to deliver the steam and carbon dioxide required at optimal temperature and pressure operating conditions to reduce oil viscosity and enhance oil production in an oil reservoir.

[0022] United States patent no. 8,088,528 (Lourenco) entitled "Method to condense and recover carbon dioxide from fuel cells" relates to the recovery of a fuel cell exhaust stream at gas pressure reduction stations in a natural gas distribution system. The presently described system allows for an improved method of recovering a fuel cell anode exhaust stream where both the components and its thermal energy are recovered for immediate use in-situ to replace the current practices of importing carbon dioxide and generating steam for injection into an oil reservoir to heat and reduce oil viscosities to enhance oil production. This new method recovers an exhaust gas stream of water and carbon dioxide that is typically discharged into the atmosphere as a by-product of a power generation plant to substantially improve the thermal requirements of an oil producing reservoir. The description of application of the method should, therefore, be considered as an example.

[0023] FIG. 1 depicts a preferred method of recovering a fuel cell anode exhaust stream that includes water and carbon dioxide for injection into an oil reservoir. Fuel cells such as the Direct Fuel Cell (DFC) manufactured by Fuel Cell Energy in the USA have been available since 2003. The largest DFC power generation plant is a 59 MW. A major advantage of a DFC power generation plant versus standard power generation plants is the smaller mass flow rate of the anode exhaust gas stream with a high concentration of carbon dioxide and water, allowing for ease of recovery and use.

[0024] In the depicted example, natural gas is delivered from a main transmission pipeline through stream 1 and enters an expander/generator 2 to reduce the main transmission pipeline pressure to meet fuel cell inlet pressure stream 3. The temperature of stream 3 is decreased by about 1.5 to 2 degrees Celsius for every 15 psi pressure drop. The cooler natural gas stream 3 enters heat exchanger 4 to give up its coolth to stream 22. A portion of natural gas stream 5 is routed through stream 28 to provide gas to air pre-heater 29. The balance of stream 5 is further heated in heat exchanger 6 by fuel cell cathode exhaust stream 32. The heated fuel cell gas stream 7 is mixed with steam stream 45, and enters the fuel cell 9 at anode section 47, through stream 8. At fuel cell anode 47, the natural gas/steam stream 8 is first reformed to produce hydrogen and carbon dioxide, the

hydrogen through an electrochemical reaction with a carbonate ion produced in cathode 46, and transferred through an electrolyte layer 50 to the anode 47. The fuel cell reaction produces electricity stream 49, and a hot anode exhaust stream 10. The carbonate ion produced in cathode 46 and transferred through electrolyte layer 50 into anode 47 is converted back to carbon dioxide in the electrochemical reaction. The hot anode exhaust stream 10 main components are steam and carbon dioxide with some residual hydrogen. The hot anode exhaust stream 10 enters heat exchanger 11 to give up some of its heat to water stream 41. The cooler anode exhaust stream 12 is further cooled in heat exchanger 13 to give up more of its heat to carbon dioxide stream 37. The cooler anode exhaust stream 14 enters separator 15 to separate and collect the condensed water component of the anode exhaust stream 14. The concentrated carbon dioxide anode exhaust stream 16 exits separator 15 and is further cooled in heat exchanger 17 by carbon dioxide stream 25. The colder concentrated carbon dioxide anode exhaust 18 is further cooled in heat exchanger 19 by liquid carbon dioxide stream 36 and further cooled in heat exchanger 21 by carbon dioxide stream 24, followed by yet more cooling in heat exchanger 4 by natural gas stream 3. The cold concentrated carbon dioxide anode exhaust stream 23 enters carbon dioxide separator 51 where the condensed carbon dioxide is separated from the gaseous carbon dioxide and residual hydrogen. The gaseous cold carbon dioxide stream and residual hydrogen stream 24 enters heat exchanger to give up some of its coolth to anode exhaust stream 20. The warmer stream 25 is further heated in heat exchanger 17 by anode exhaust stream 16, the heated gaseous carbon dioxide and residual hydrogen stream 26 is mixed with air stream 27 at air pre-heater 29 where the residual hydrogen is catalytically oxidized and the oxidant stream 30 is heated to a temperature suitable for cathode 46. The fuel cell cathode 46 consumes the oxygen from air stream 27 and the circulated carbon dioxide from stream 26 to produce carbonate ions that are transferred through electrolyte layer 50 to the fuel cell anode 47. The hot cathode exhaust stream exits fuel cell cathode 46 through stream 31. The cathode exhaust stream, which is mainly nitrogen with residuals of carbon dioxide, water vapour and oxygen, enters heat exchanger 44 to heat water stream 43 and produce steam in stream 45, which is mixed with heated natural gas stream 7, the mixed stream 8 is fed to the fuel cell anode 47 reformer to produce hydrogen and carbon dioxide. The cathode exhaust stream 32 is further cooled in heat exchanger 6, heating fuel cell anode natural gas supply stream 5, and is exhausted into the atmosphere through stream 33. The recovered water stream 39 from separator 15 enters pump 40 and is pumped into stream 52. A

circulating water stream 43 is routed to heat exchanger 44 to produce steam for the fuel cell anode 47 reformer as discussed above. The balance of the water enters pump 53 where it is pressurized to reach an optimal operating pressure for the oil reservoir. The pressurized water stream 41 enters heat exchanger 11 to produce steam in stream 42, and is mixed with heated carbon dioxide stream 5 38. The mixed steam and hot carbon dioxide mixture is injected into the oil reservoir through stream 48. The recovered carbon dioxide liquid stream 34 is routed to pump 35 and pressurized to meet optimal reservoir operating pressure. The pressurized liquid carbon dioxide stream 36 is routed through heat exchanger 19 to give up its coolth, and the warmer carbon dioxide stream 37 is further heated in heat exchanger 13 and the hot carbon dioxide stream 38 is mixed with steam 10 stream 42 for injection into the oil reservoir.

[0025] The objectives of the process are first, to recover the concentrated water and carbon dioxide components of a fuel cell anode exhaust stream by condensation in a counter current heat exchange process configuration, and second, to enhance oil production by pressurizing and re-heating the recovered liquids in a counter current heat exchange process configuration for injection 15 into an oil reservoir to enhance oil production. The process meets the industry requirement to provide steam and/or a solvent to enhance oil production. The process allows for an efficient recovery of components and thermal energy from a fuel cell anode exhaust stream at a power generation plant that can be used to replace or supplement the current practice of steam generation and purchased carbon dioxide for stimulation of an oil reservoir to increase oil production.

20 [0026] Those skilled in the art will understand that variations of the above-described process are possible, and that designs other than what is depicted may be used to accomplish similar process steps. Some non-limiting examples are given below. Referring to FIG. 2, the process is similar to that shown in FIG. 1, however the concentrated carbon dioxide anode exhaust stream 16 is compressed by compressing stream 16 with compressor 200 to produce a higher pressure stream 25 201. This may be used to meet desired carbon dioxide properties in stream 16 based on the pressure enthalpy diagram for carbon dioxide recovery as a liquid.

[0027] Referring to FIG. 3, another variation is shown, in which the main transmission natural gas pipeline pressure supply stream 1 is provided with a JT (Joules Thompson) valve 300 in lieu of

an expander/generator to reduce the pressure of the natural gas. The use of a JT valve is not as efficient as an expander/generator but it is an alternative method of operation that may reduce the capital cost requirements.

[0028] Referring to FIG. 4, another variation is shown, in which a compressor 400 is used to increase the main transmission natural gas pipeline pressure supply stream 1, in case the available natural gas pipeline pressure is lower than what is required to generate a refrigerant natural gas stream as in FIG. 1. The higher pressure transmission natural gas supply stream 401 is first cooled by ambient air heat exchanger 402, the ambient air cooled higher pressure natural gas supply stream 403 is depressurized through JT valve 404 to produce a refrigerant natural gas stream 405. It is understood, JT valve 404 can be substituted by an expander/generator to produce a colder refrigerant stream 405 if required.

[0029] Referring to FIG. 5, another variation is shown in which a refrigeration plant is used to increase the refrigeration properties of the natural gas supply stream. The input stream 3 is cooled in a heat exchanger 500 to produce a cooled stream of natural gas 501 that is then passed through heat exchanger 4 as described above. Heat exchanger 500 is cooled by a cooling circuit 502 and 503 that is in turn cooled by a refrigeration unit 504. Refrigeration unit 504 and the fluid circulating through lines 502 and 503 may be selected by those skilled in the art to meet the cooling demands of a particular process.

[0030] Referring to FIG. 6, another variation is shown in which the natural gas is supplied from a liquefied natural gas (LNG) drum 600. This option enhances the available refrigeration that may be used to condense the carbon dioxide stream 22 when a supply of natural gas is not available by pipeline or in pressurized tanks. As depicted, LNG from storage drum 600 is fed by stream 601 into pump 602. The pressurized stream 603 is routed through heat exchanger 4 to condense carbon dioxide stream 22.

[0031] Referring to FIG. 7, an external source of water or solvent 700 is heated in heat exchanger 701 and mixed in stream 48 along with carbon dioxide from stream 38 and steam from stream 42 for injection into an oil reservoir. The benefit of this process configuration is the ability to

add more steam or a solvent to the reservoir since the temperatures generated by a fuel cell anode exhaust are typically twice as high as common industry steam temperature generated for SAGD operations. This difference in temperature allows for the addition of water or solvent to a fuel cell anode exhaust mass injected into an oil reservoir.

5 [0032] As will be apparent, the system is preferably based on natural gas as the fuel for the anode, as this provides a readily available, predictable source of fuel. It will be understood that other types of fuel may also be used, such as biogas. Preferably, the fuel will include a hydrocarbon feedstock, examples of which include methane, methanol, biogas, etc. that produces water and carbon dioxide as an exhaust stream that can be used in the process as described herein. In addition,
10 while the fuel cell described herein produces a carbonate ion that traverses the membrane, other fuel cells that operate using a different reaction may also be used, such as a solid oxide fuel cell. The cathode inputs may be varied according to the requirements of the specific fuel cell being used.

[0033] Referring to FIG. 8, line 800 is used to represent a source of biogas, although other sources of fuel may also be possible. In a typical biogas, the composition may be around 40%
15 carbon dioxide, 60% methane, and up to 5% hydrogen sulphide. As such, the biogas generally must be treated to remove the carbon dioxide and sulphide components. By removing the carbon dioxide component, the heat content of the volume of biogas supplied to fuel cell 9 is increased. In FIG. 8, the removed carbon dioxide may be introduced via line 801 into the cathode input stream. In addition, alternate sources of carbon dioxide may be provided via line 801 to be used for the input
20 stream to the cathode. Depending on the amount of carbon dioxide, stream 801 may supplement or replace carbon dioxide in stream 26. This may be beneficial, for example, to dispose of carbon dioxide produced by a different industrial process. Pre-air heater 29 may or may not be required, depending on the temperature and pressure of the carbon dioxide and air, and the specifications of the fuel cell.

25 [0034] It will be understood that the variations described with respect to FIG. 2 – 8 may be combined in various combinations other than those explicitly depicted and described, except where the design choices are clearly mutually exclusive.

[0035] The method described herein allows for the efficient recovery of components and thermal energy from a fuel cell anode exhaust stream at a power generation plant to replace the current practice of steam generation and purchased carbon dioxide for stimulation of an oil reservoir to increase oil production. The method may also be used for other purposes, such as for carbon dioxide sequestration, in which the carbon dioxide stream is injected downhole. The water stream likely would not be injected downhole in this example, as it could be diverted for other uses.

[0036] When injecting the streams of carbon dioxide and water downhole in a SAGD-type operation, or an operation in which the goal is to improve the viscosity of the oil, benefits may be had beyond merely transferring the heat to the oil. For example in some circumstances, the carbon dioxide may mix with the oil and reduce its viscosity. In other circumstances, the carbon dioxide and water may react to form carbonic acid, which may help open the formation and increase the flow of oil. In other situations, the products of the fuel cell may be used in other production techniques, such as in situ cracking production to produce lighter oil. The high temperatures and electrical energy produced by the fuel cell may be used to generate favourable conditions to promote hydrocracking downhole, or other reactions, that will increase the production rate of the oil, and may increase the value of the oil being produced. Some techniques may require additional reactants, and it will be apparent to those skilled in the art how the presently described system could be adapted to produce, heat, or otherwise condition the necessary components to be injected with the carbon dioxide and/or water downhole to accomplish the desired downhole reaction.

[0037] The current industry practice is first to treat water in preparation for steam generation, this is done at a considerable cost due to the concern of scaling in the boilers. Secondly, the steam temperature generated is limited by its evaporation temperature at operating pressures, to minimize scaling in the boilers, a once through boiler is preferred resulting in wet steam.

[0038] The method described herein generates a stream carbon dioxide and steam by an electrochemical reaction of hydrogen and a carbonate ion, that is condensed, recovered, pumped and re-heated to an oil reservoir optimal operating conditions to enhance the production of oil.

[0039] In this patent document, the word "comprising" is used in its non-limiting sense to mean that items following the word are included, but items not specifically mentioned are not excluded. A reference to an element by the indefinite article "a" does not exclude the possibility that more than one of the element is present, unless the context clearly requires that there be one and only one of the elements.

[0040] The scope of the claims should not be limited by the preferred embodiments set forth in the examples, but should be given a broad purposive interpretation consistent with the description as a whole.

What is Claimed is:

1. A method to condense, recover, pump and re-heat an anode exhaust stream from a natural gas-powered fuel cell prior to injection into an oil reservoir to enhance the production of oil, the fuel cell having an anode, a cathode, and a cathode exhaust stream, the anode exhaust stream comprising water vapour and carbon dioxide, the method comprising the steps of:
 - 5 providing a refrigerated natural gas supply stream;
 - passing the refrigerant natural gas supply stream and a fuel cell anode exhaust stream through a first heat exchanger to condense carbon dioxide from the fuel cell anode exhaust stream and produce a fuel cell natural gas stream;
 - 10 condensing a steam component of the anode exhaust stream and separating the condensed steam from the gaseous carbon dioxide and residual hydrogen;
 - condensing and separating at least a portion of the carbon dioxide from the gaseous carbon dioxide and residual hydrogen that exits the water separator to produce a condensed carbon dioxide stream a carbon dioxide and residual hydrogen stream;
 - 15 combining the carbon dioxide and residual hydrogen stream with an input air stream mixed into a cathode input stream, the cathode input stream being pre-heated in a catalytic oxidizer prior to being input into the cathode of the fuel cell cathode;
 - pressurizing and heating the condensed carbon dioxide to oil reservoir operating conditions to produce an injection stream of carbon dioxide;
 - 20 pressurizing and heating a first portion of the condensed steam to produce an anode input stream of steam;
 - mixing anode input stream of steam with the fuel cell natural gas stream heated supply of natural gas to produce an anode input stream;
 - pressurizing and heating a second portion of the condensed steam to oil reservoir operating conditions to produce an injection stream of steam;
 - 25 injecting the injection stream of carbon dioxide and the injection stream of steam into the oil reservoir.
2. The method of claim 1, wherein the carbon dioxide and residual hydrogen stream is

compressed to meet desired operations properties using a pressure enthalpy diagram of the stream.

3. The method of claim 1, wherein the pressurized natural gas supply stream is expanded using an expander/generator or a Joules-Thompson valve.
4. The method of claim 1, where the transmission natural gas supply is compressed and then
5 cooled by ambient air heat exchange to increase the refrigeration properties of the natural gas supply stream.
5. The method of claim 1, further comprising the step of cooling the refrigerated natural gas supply streams using a refrigeration plant.
6. The method in claim 1, where the refrigerated natural gas supply stream is derived from a
10 source of liquid natural gas (LNG).
7. The method of claim 1, further comprising the step of adding at least one of a water and a solvent to the stream of carbon dioxide and the injection stream of steam prior to injection into the oil reservoir
8. A method of injecting fluids into an underground formation using exhaust streams from a
15 fuel cell, the fuel cell comprising an anode and a cathode, the fuel cell having an anode input stream comprising at least a fuel and water, a cathode input stream comprising at least oxygen and carbon dioxide, an anode exhaust stream comprising at least carbon dioxide and steam, and a cathode exhaust stream, the method comprising the steps of:
 - condensing and separating water from the anode exhaust stream to produce a stream of
20 water and a stream of carbon dioxide;
 - heating a first portion of the stream of water to produce a stream of steam;
 - combining the stream of steam and the fuel to form the anode input stream;
 - producing an injection stream of steam by heating and compressing a second portion of the stream of water to a desired temperature and pressure;
 - 25 obtaining a stream of condensed carbon dioxide by condensing at least a portion of the carbon dioxide in the stream of carbon dioxide;

heating and compressing the stream of condensed carbon dioxide to a desired temperature and pressure to produce an injection stream of carbon dioxide gas; and

injecting at least the injection stream of carbon dioxide gas into the underground formation.

9. The method of claim 8, wherein the underground formation is an oil bearing formation and
5 further comprises injecting the injection stream of steam into the oil bearing formation.
10. The method of claim 8 or 9, wherein the fuel of the anode input stream comprises a stream of hydrocarbons.
11. The method of claim 10, wherein the stream of hydrocarbons is obtained from a supply of natural gas, the supply of natural gas being used as a refrigerant to condense the portion of the
10 carbon dioxide to form the stream of condensed carbon dioxide.
12. The method of claim 11, wherein the supply of natural gas is a liquid natural gas (LNG) tank.
13. The method of claim 11, wherein the supply of natural gas is a pressurized stream of natural gas, and wherein the pressurized stream of natural gas is expanded and cooled to produce cold
15 temperatures.
14. The method of claim 10, wherein the supply of natural gas is passed through at least one of a refrigeration plant and a condenser and air cooler.
15. The method according to any one of claims 10 through 14, wherein the temperature and pressure of the stream of carbon dioxide are controlled to meet desired operating properties using a
20 pressure enthalpy diagram of the stream.
16. The method according to any one of claims 8 through 15, further comprising the step of injecting at least one of water and a solvent into the oil bearing formation with the injection stream of carbon dioxide and the injection stream of steam.
17. The method according to any one of claim 8 through 16, wherein, after condensing, the

stream of carbon dioxide is separated into the stream of condensed carbon dioxide and a cathode stream of carbon dioxide.

18. The method of claim 17, further comprising the step of combining oxygen and the cathode stream of carbon dioxide to form the cathode input stream.

5 19. The method of claim 18, wherein forming the cathode input stream comprises combining the first stream of carbon dioxide and atmospheric air.

20. The method of claim 17, 18 or 19, wherein the anode exhaust stream further comprises residual hydrogen, and wherein the cathode stream of carbon dioxide further comprises the residual hydrogen.

10 21. The method of claim 20, wherein forming the cathode input stream further comprises preheating the first stream of carbon dioxide and oxygen in a combustion heater that is fuelled by a hydrocarbon and the residual hydrogen.

22. The method according to any one of claims 8 through 21, further comprising the step of supplying carbon dioxide for the cathode input stream from a source of captured carbon dioxide.

15

FIG 1

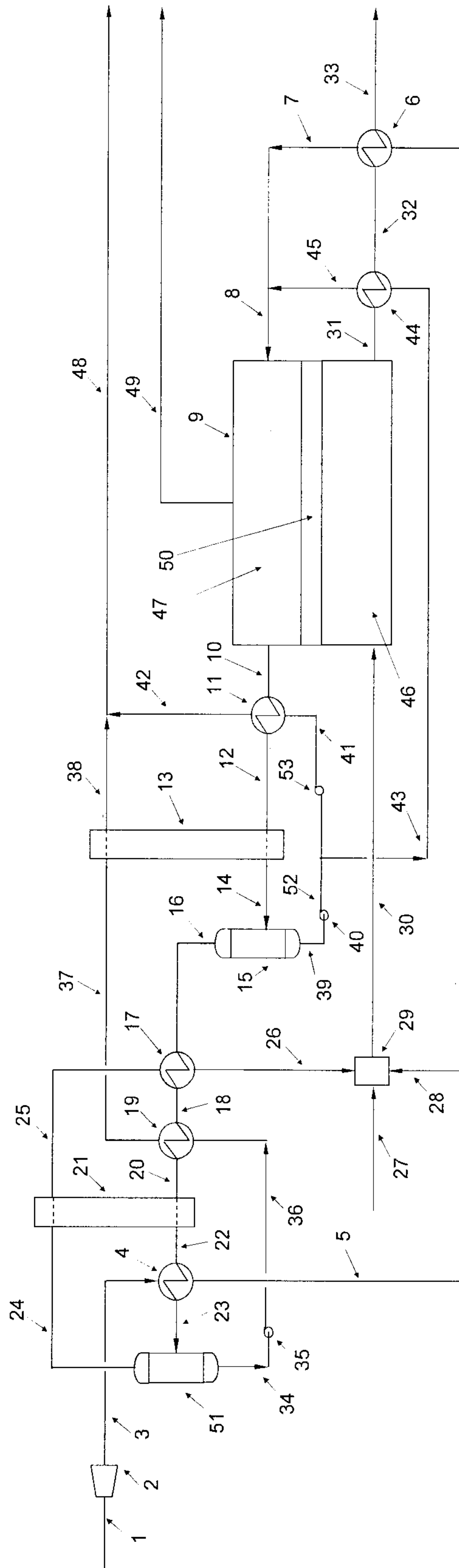


FIG 2

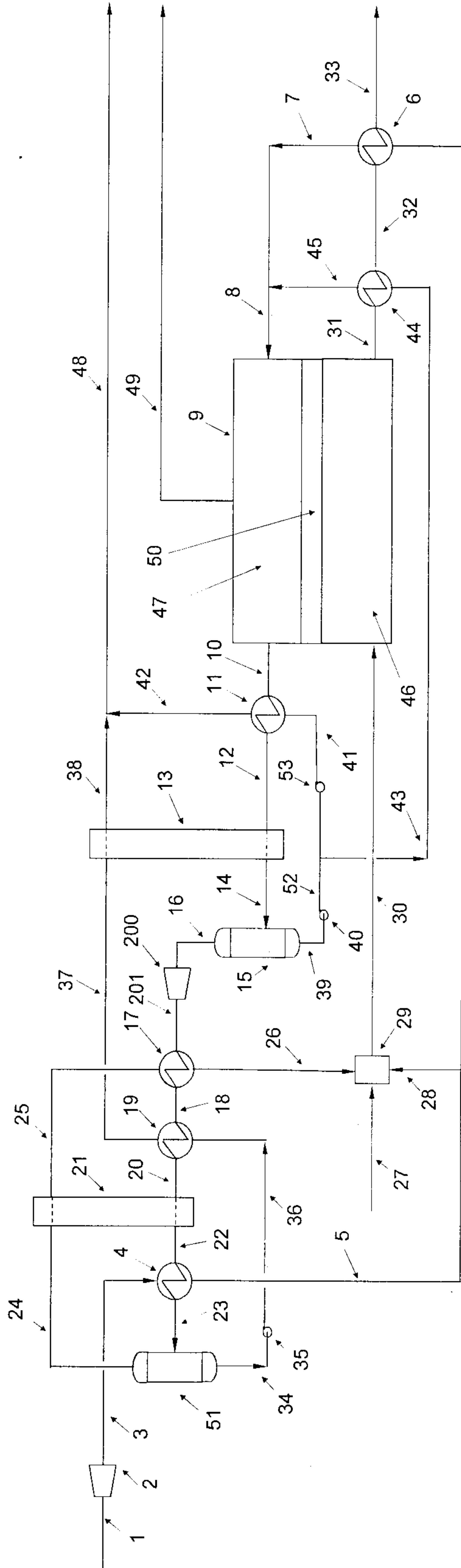


FIG 3

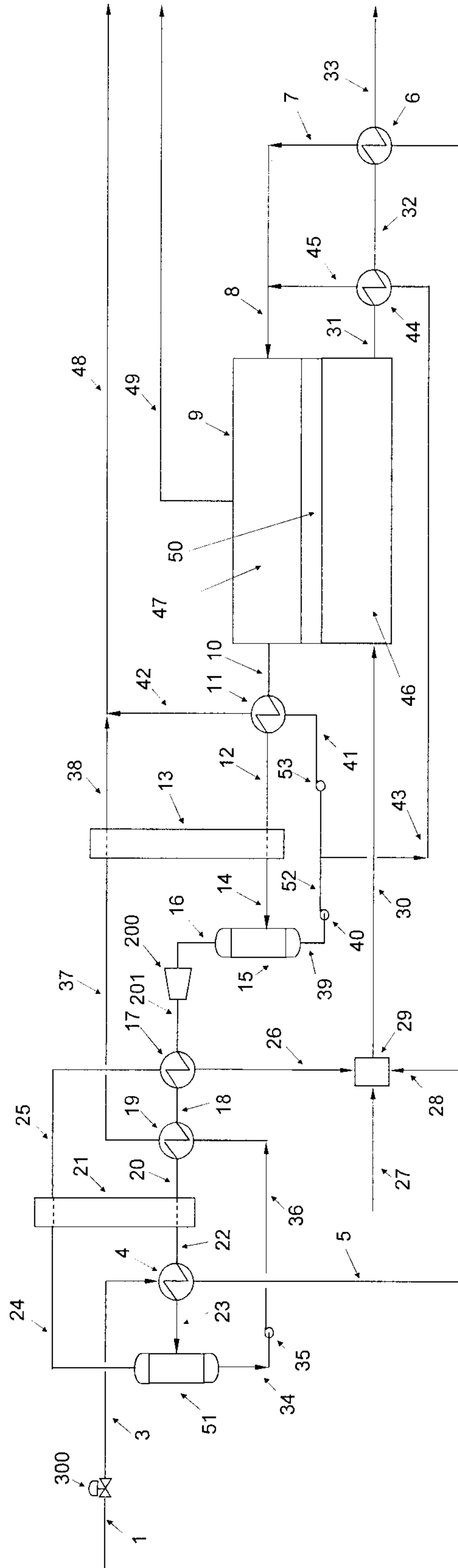


FIG 4

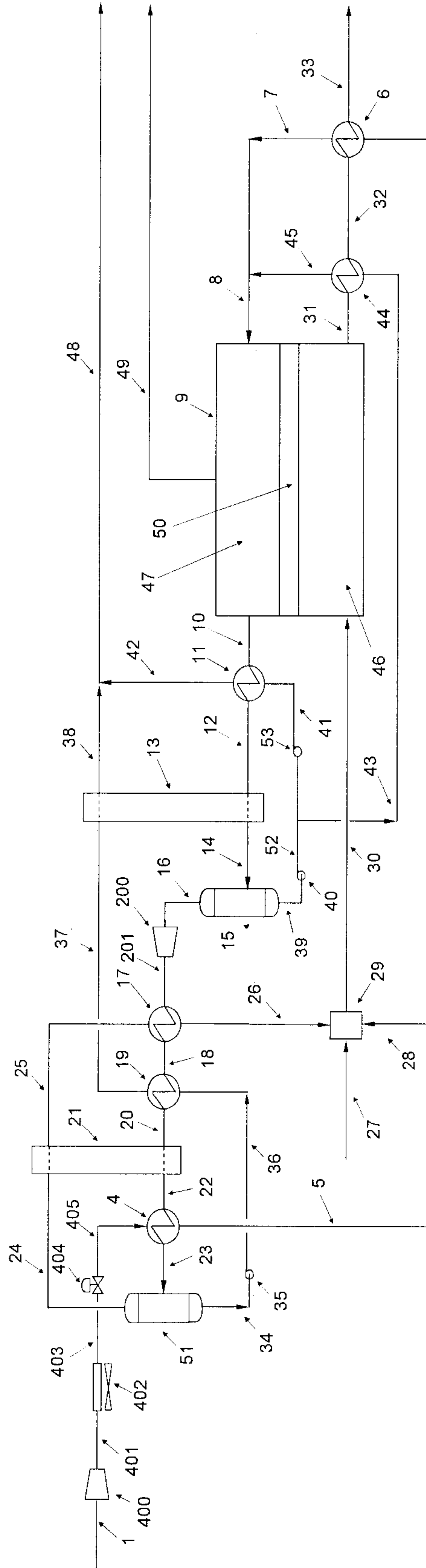


FIG 5

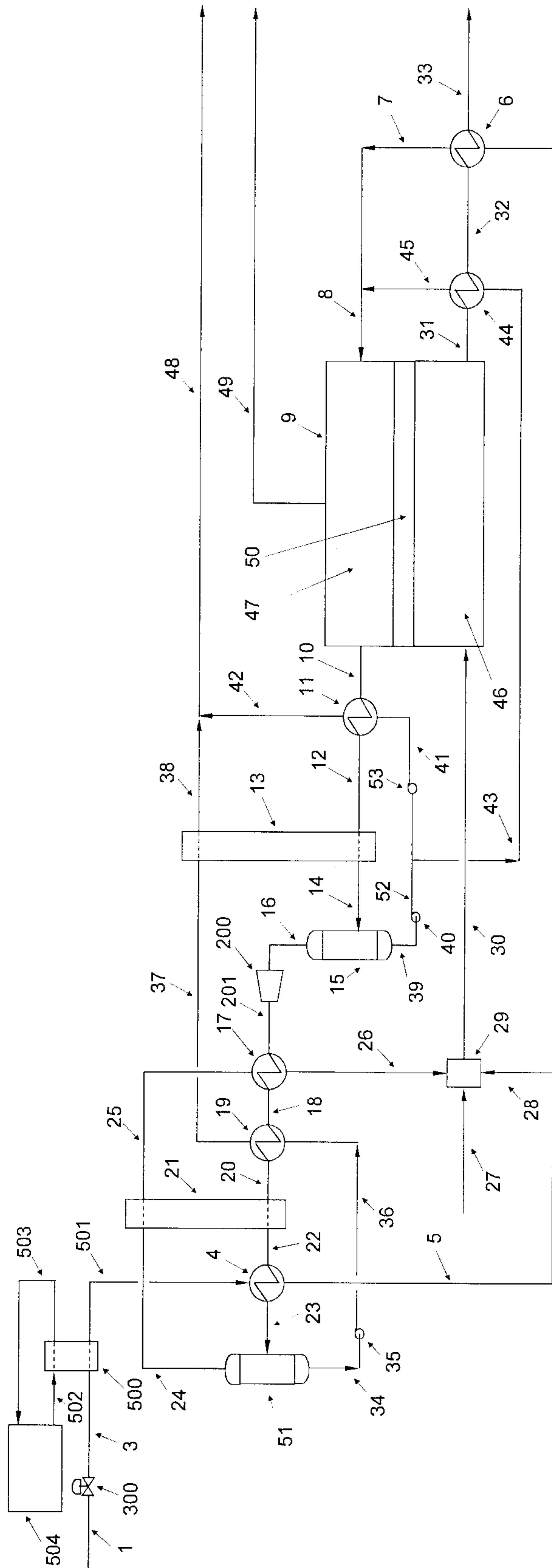


FIG 6

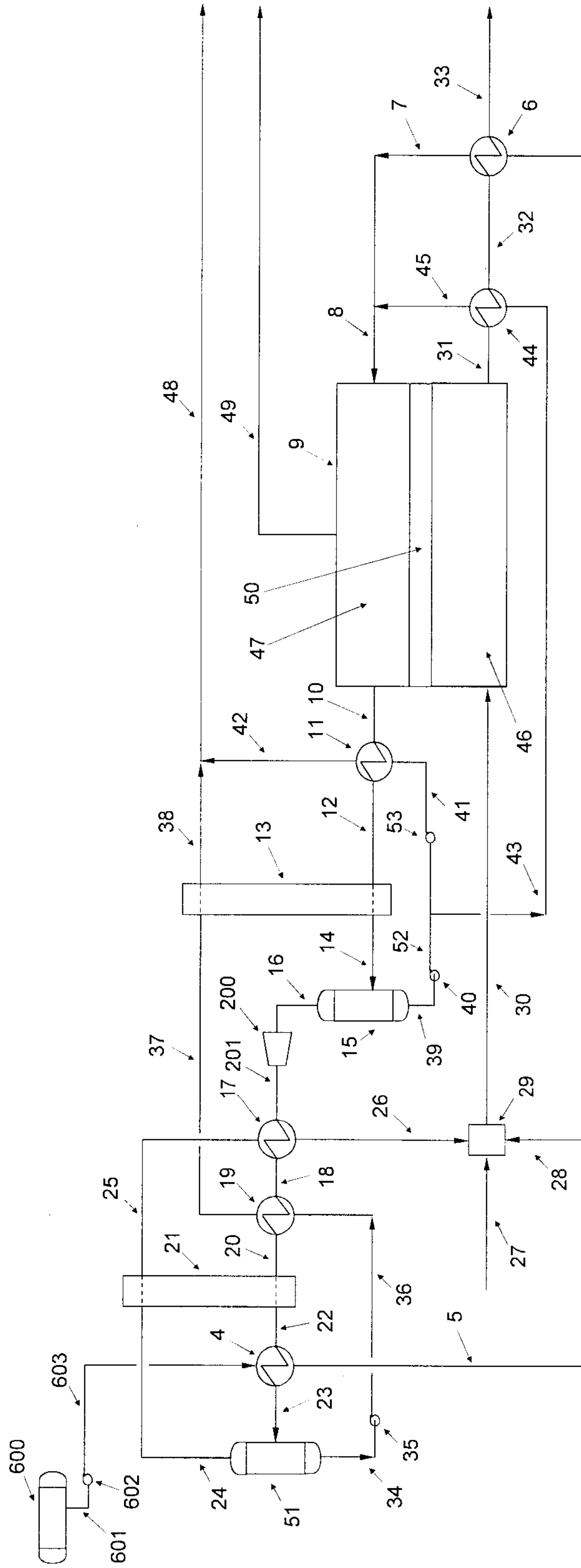


FIG 7

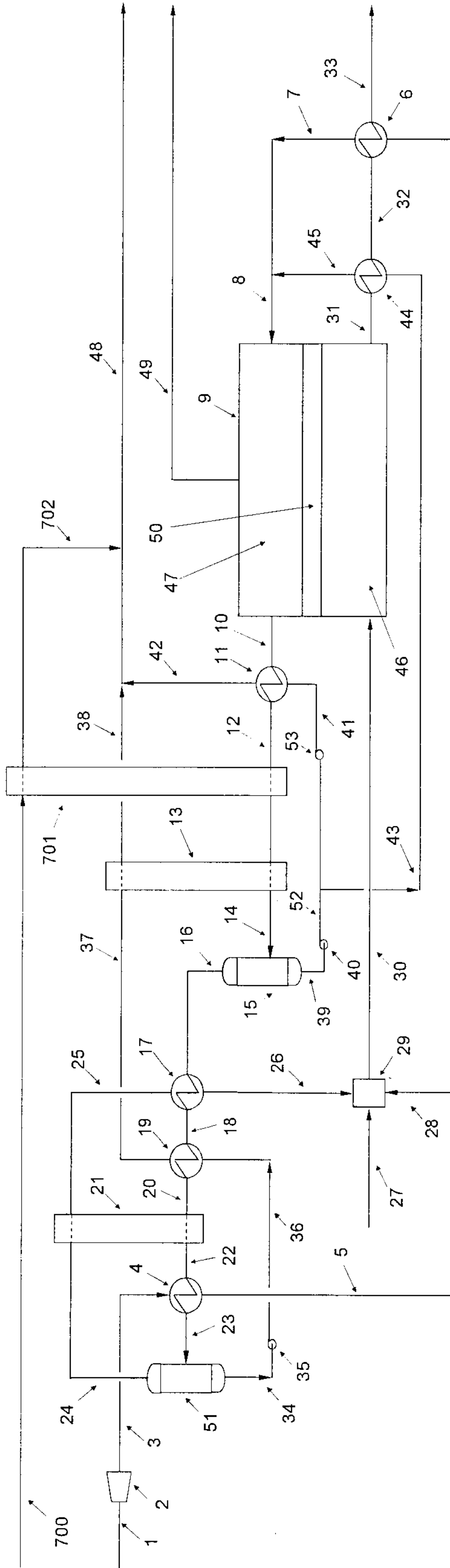


FIG. 8

