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(71) Applicant(s)  
**Baxter Healthcare S.A.;Baxter International Inc.**

(72) Inventor(s)  
**Mundt, Wolfgang;Grillberger, Leopold;Reiter, Manfred;Mitterer, Artur**

(74) Agent / Attorney  
**Cullens Patent and Trade Mark Attorneys, Level 32 239 George Street, Brisbane, QLD, 4000**

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(71) Applicants (for all designated States except US): **BAXTER INTERNATIONAL INC.** [US/US]; One Baxter Parkway, Deerfield, IL 60015 (US). **BAXTER HEALTHCARE S.A.** [CH/CH]; Hertistrasse 2, CH-8304 Wallisellen (CH).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **GRILLBERGER, Leopold** [AT/AT]; Postgasse 13/20, A-1010 Vienna (AT). **REITER, Manfred** [AT/AT]; Gebrueder-Lang-Gasse 11/17, A-1150 Vienna (AT). **MUNDT, Wolfgang** [AT/AT]; Florianigasse 57/1/2/6, A-1080 Vienna (AT). **MITTERER, Artur** [AT/AT]; Schwarzeckerweg 10, A-2304 Orth/Donau (AT).

(74) Agent: **PERREY, Ralf**; Müller-Boré & Partner, Grafinger Strasse 2, 81671 Munich (DE).

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(54) Title: OLIGOPEPTIDE-FREE CELL CULTURE MEDIA

(57) Abstract: The present invention relates to oligopeptide-free cell culture media comprising at least 0.5 mg/L of a polyamine and to methods for cultivating cells in said oligopeptide-free cell culture media comprising at least 0.5 mg/L of a polyamine. The invention also relates to methods for expressing at least one protein in a medium comprising at least 0.5 mg/L of a polyamine and to methods for producing at least one virus in a medium comprising at least 0.5 mg/L of a polyamine.



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## **OLIGOPEPTIDE-FREE CELL CULTURE MEDIA**

### **FIELD OF THE INVENTION**

[001] The present invention relates to oligopeptide-free cell culture media comprising at least 0.5 mg/L of a polyamine and to methods for cultivating cells in said oligopeptide-free cell culture media comprising at least 0.5 mg/L of a polyamine. The invention also relates to methods for expressing at least one protein in a medium comprising at least 0.5 mg/L of a polyamine and to methods for producing at least one virus in a medium comprising at least 0.5 mg/L of a polyamine.

### **BACKGROUND OF THE INVENTION**

[002] For cultivation of cells, particularly eukaryotic cells, and more specifically mammalian cells, there is a constant need to use special culture media providing nutrient substances that are required for efficient growth of cells and for the production of biological products, especially biopharmaceuticals, such as, for example, recombinant proteins, antibodies, viruses, viral antigens, and virus-like particles. For the efficient production of said biological products, it is important to achieve an optimal cell density as well as an increase of the protein expression itself in order to obtain maximal product yield.

[003] Cell culture media formulations have been supplemented with a range of additives, including undefined components like fetal calf serum (FCS), several animal derived proteins and/or protein hydrolysates of bovine origin as well as protein hydrolysates derived from plants or yeast.

[004] In general, serum or serum-derived substances, such as e.g. albumin, transferrin or insulin, may comprise unwanted agents that can contaminate the cell cultures and the biological products obtained thereof. Furthermore, human serum derived additives have to be tested for all known viruses, including hepatitis viruses and HIV which can be transmitted via serum. Moreover, bovine serum and products derived thereof bear the risk of BSE contamination. In addition, all serum-derived products can be contaminated by unknown substances. When using serum or protein additives derived from human or animal sources in cell culture, there are numerous problems (e.g. the varying quality in composition of different batches and the risk of contamination with mycoplasma, viruses or BSE), particularly if the cells are used in the manufacture of drugs or vaccines for human administration.

[005] Therefore, many attempts have been made to provide efficient host systems and cultivation conditions, which do not require serum or other animal protein compounds.

[006] Such serum-free media have been developed on the basis of protein extracts derived from plants or yeast. For example, soy hydrolysates are known to be useful for fermentation processes and can enhance the growth of many fastidious organisms, yeasts and fungi. WO 96/26266 describes that papaic digests of soy meal are a source of carbohydrate and nitrogen and many of the components can be used in tissue culture. Franek et al. (Biotechnology Progress (2000) 16, 688 - 692) describe growth and productivity promoting effects of defined soy and wheat hydrolysate peptide fractions.

[007] WO 96/15231 discloses a serum-free medium composed of a synthetic minimal essential medium and a yeast extract for the propagation of vertebrate cells and a virus production process. A medium formulation composed of a basal cell culture medium comprising a rice peptide and an extract of yeast and an enzymatic digest thereof, and/or a plant lipid for growth of animal cells is disclosed in WO 98/15614. A medium comprising purified soy hydrolysate for the cultivation of recombinant cells is disclosed in WO 01/23527. WO 00/03000 discloses a medium that comprises a soy hydrolysate and

a yeast extract, but also requires the presence of recombinant forms of animal proteins, such as growth factors.

[008] EP-A-0 481 791 describes a biochemically defined culture medium for culturing engineered CHO cells, which is free from protein, lipid and carbohydrate isolated from an animal source, further comprising a recombinant insulin or insulin analogue, 1 % to 0.025 % w/v papain digested soy peptone and putrescine. WO 98/08934 describes a serum-free eukaryotic cell culture comprising hydrolyzed soy peptides (1 - 1000 mg/L), 0.01 to 1 mg/L putrescine and a variety of animal-derived components, including albumin, fetuin, various hormones and other proteins. In this context, it should be noted that putrescine is also known to be comprised in standard media like DMEM/Ham's F12 in a concentration of 0.08 mg/L.

[009] The plant and/or yeast hydrolysates, however, are undefined mixtures of oligopeptides and other unknown components and contaminants. Moreover, the quality of commercially available lots of hydrolysates varies extremely. As a result, there are large variations in the production of recombinant proteins or viral products (a variation of up to a factor of 3) as a function of the lots of hydrolysates used ("lot-to-lot variation"). This drawback affects the proliferation of the cells as well as the protein expression of each cell.

[010] In summary, the media known in the state of the art are supplemented with proteins or peptide extracts derived from animals, plants, or yeast; or with recombinant versions of proteins, such as, for example, insulin, insulin like growth factor or other growth factors.

[011] Therefore, there is a need for a cell culture medium which is free of animal, herbal, and fungal proteins and/or oligopeptides in order to overcome the above-mentioned problems. Furthermore, a current need exists to increase the yield of expressed recombinant proteins or any other expression product, and to provide an

optimal cell culture medium for the production of biological products, such as those used as pharmaceuticals or vaccines in humans.

#### SUMMARY OF THE INVENTION

[012] It is an object of the present invention to provide oligopeptide-free cell culture media. A further object of the present invention is to provide methods for cultivating cells in said media as well as methods for efficient expression of recombinant proteins and/or methods for the efficient production of viruses.

[013] It is another object of the present invention to eliminate animal, plant and/or yeast derived hydrolysates and to provide media which do not comprise any added supplementary proteins or oligopeptides.

[014] Surprisingly, the addition of at least 0.5 mg/L of a polyamine to cell culture media provides an advantageous effect not only by promoting cell growth but also by increasing the protein and/or virus expression per cell. Said unexpected advantageous effect can be achieved even in oligopeptide-free media.

[015] Further, the oligopeptide-free medium according to the present invention allows consistent cell growth and increased yield of desired products, particularly of target proteins such as recombinant proteins and/or viruses, independent of the quality or lot variations of any protein hydrolysates. The specific supplementation of cell culture media with a specific concentration of polyamines acts to increase cell growth, cell specific productivity and final cell density.

[016] Therefore, the media according to the present invention are more favorable for recombinant protein expression, virus production and cell growth rate compared to the

media known in the art. Furthermore, the oligopeptide-free medium according to the present invention obviates the addition of protein hydrolysate to the cell culture medium.

A definition of the specific embodiment of the invention claimed herein follows.

In one broad form, the invention provides a method for expressing at least one protein, comprising the steps of:

- (a) providing a culture of cells;
- (b) introducing at least one nucleic acid sequence comprising a sequence coding for at least one protein selected from the group of coagulation factor VII, coagulation factor VIII, coagulation factor IX, vWF, ADAMTS13 and furin into the cells;
- (c) selecting the cells carrying the nucleic acid sequence; and
- (d) expressing the protein in the cells in an oligo-peptide free medium comprising at least 0.5mg/L of a polyamine.

#### BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 shows a graph which describes the effect of the addition of 2.0 mg/L putrescine.2HCl on the volumetric FVIII-CoA productivity, expressed in [Units per Liter per Day], of GD8/6 cells cultivated in BAV-medium over the culture time, expressed in [days]. Arrow = Day 11: Addition of Putrescine.2HCl (2.0 mg/l).

Figure 2 shows a table which compares the effect of the addition of putrescine optionally in combination with the additional supplementation with Fe (II) and Cu (II) on the volumetric and cell specific productivity (QP, expressed in [Units per Liter per Day], qp, expressed in [mU per 10E06 cells per day]) and on the specific growth rate  $\mu$ , expressed as specific growth rate per day in [d<sup>-1</sup>] of GD8/6 cells cultivated in BAV-medium.

Figure 3 shows a table which compares the effect of putrescine and/or ornithine on the specific growth rate ( $\mu$  absolute,  $\mu$  relative) and the cell specific productivity (qp absolute, expressed in [mU per 10E06 cells per day], qp relative, expressed in %) of GD8/6 cells cultivated in BAV-medium.

Figure 4 shows a table which compares the effect of putrescine and spermine on the specific growth rate ( $\mu$  absolute,  $\mu$  relative) and the cell specific productivity (qp absolute, qp relative) of GD8/6 cells cultivated in BAV-medium.

Figure 5 shows a table which compares the effect of putrescine and ethanolamine on the specific growth ( $\mu$  absolute,  $\mu$  relative) and the cell specific productivity (qp absolute, qp relative) of GD8/6 cells cultivated in BAV-medium.

**[ text continues on page 6. ]**



Figure 6 shows a graph which describes the effect of the addition of 3.6 mg/L putrescine.2HCl on the average MVA virus titer, expressed in [TCID<sub>50</sub>/ml x 10<sup>8</sup>].

- : without addition of Putrescine, Putr.: with addition of 3.6 mg/L putrescine.2HCl.

Figure 7 shows a graph which describes the effect of the addition of various concentrations of putrescine.2HCl, expressed in [mg/l], on the average MVA virus titer, expressed in [TCID<sub>50</sub>/ml x 10<sup>8</sup>].

#### DETAILED DESCRIPTION OF THE INVENTION

[017] One aspect of the invention relates to an oligopeptide-free cell culture medium comprising at least 0.5 mg/L of a polyamine.

[018] Unless stated differently, concentration values indicated throughout this document refer to the free base form of the component(s).

[019] The term "polyamine" refers to any of the group of biogenic polyamines, which are organic polycations derived from aromatic or cationic amino acids. Polyamines are composed of carbon, nitrogen, and hydrogen and comprise two or more amino groups. Polyamines have one or more positive charges and a hydrophobic skeleton. The term encompasses, for example, molecules selected from the group consisting of cadaverine, putrescine, spermidine, spermine, agmatine, ornithine, and combinations thereof. In one embodiment of the invention, the oligopeptide-free culture medium comprises ornithine, or putrescine, or spermine, or combinations thereof.

[020] In another embodiment of the oligopeptide-free cell culture medium according to the invention the polyamine originates from a source other than a protein hydrolysate. In one embodiment, the polyamine is synthetically produced.

[021] In one embodiment of the invention, the polyamine concentration is at least about 0.5 mg/L, in another embodiment at least about 1 mg/L, in a further embodiment at least about 2 mg/L, in still another embodiment at least 5 mg/L, in yet another embodiment at least 8 mg/L, and in a further embodiment at least 10 mg/L.

[022] In one embodiment of the invention, the polyamine concentration ranges from about 0.5 mg/L to about 30 mg/L, in another embodiment from about 0.5 mg/L to about 20 mg/L, in a further embodiment from about 1.0 mg/L to about 20 mg/L, in a further embodiment from about 2.0 mg/L to about 20 mg/L, in a further embodiment from about 2 mg/L to about 10 mg/L, in an alternative embodiment from about 2 mg/L to about 8 mg/L, and in a further embodiment from about 2 mg/L to about 5 mg/L in the medium.

[023] The concentrations indicated above are the respective concentrations of pure polyamine. If a polyamine derivative or a polyamine comprising compound is used, the concentration of the polyamine-group is in the above specified ranges. For example, 2 mg/L Putrescine.2HCl is equivalent to a Putrescine concentration of about 1.095 mg/L (without .2HCl).

[024] The term "oligopeptide-free cell culture medium" according to the invention refers to a protein-free medium that does not comprise oligopeptides, such as e.g. oligopeptides derived from a protein hydrolysate. In one embodiment, the medium does not comprise oligopeptides having twenty or more amino acids. In one embodiment of the present invention, the medium does not comprise oligopeptides having fifteen or more amino acids. In another embodiment of the invention, the medium does not comprise oligopeptides having ten or more amino acids. In one embodiment the medium does not comprise oligopeptides having seven or more amino acids, in another embodiment it does not comprise oligopeptides having five or more amino acids, in still another embodiment it does not comprise oligopeptides having three or more amino acids. According to a further embodiment of the present invention, the medium does not comprise oligopeptides having two or more amino acids.

[025] The medium according to the invention may optionally comprise glutathione and/or at least one stable form of glutamine, such as, e.g., L-alanyl-L-glutamine. The term "glutathione" as used herein describes a tripeptide composed of the amino acids glutamate, cysteine and glycine including the oxidized form of glutathione, i.e. glutathione disulfide, a glutathione dimer formed by a disulfide bond between the cysteine sulfhydryl side chains during the course of being oxidized.

[026] In an embodiment of the present invention, the oligopeptide-free cell culture medium does not comprise oligopeptides having three or more amino acids, but may optionally comprise glutathione.

[027] In another embodiment, the oligopeptide-free cell culture medium does not comprise oligopeptides having two or more amino acids, but may optionally comprise glutathione and/or at least one stable form of glutamine.

[028] Typical proteins and/or oligopeptides that are avoided in the media according to the invention are those found in serum and serum-derived substances, such as e.g. albumin, transferrin, insulin or other growth factors as well as recombinant forms thereof, or oligopeptides from plant or yeast hydrolysates or ultrafiltered forms thereof.

[029] The oligopeptide-free culture medium according to the invention may be based on any basal medium such as DMEM, Ham's F12, Medium 199, McCoy, or RPMI generally known to a person skilled in the art. The basal medium may comprise a number of ingredients, including amino acids, vitamins, organic and inorganic salts, and sources of carbohydrate, each ingredient being present in an amount which supports the cultivation of a cell, said amounts being generally known to a person skilled in the art. The medium may comprise auxiliary substances, such as buffer substances, e.g., sodium bicarbonate, antioxidants, stabilisers to counteract mechanical stress, or protease inhibitors. If required, a non-ionic surfactant such as copolymers and/or mixtures of

polyethylene glycols and polypropylene glycols (e.g. Pluronic F68®, SERVA) can be added.

[030] In an embodiment of the culture medium according to the present invention the polyamine controls DNA- and RNA-synthesis, and/or cell proliferation, and/or cell differentiation, and/or membrane stabilization, and/or antioxidative DNA-protection.

[031] In one embodiment, the addition of at least 0.5 mg/L of a polyamine to an oligopeptide-free cell culture medium increases the protein and/or virus expression in the cultured cells. In another embodiment, the protein expression or virus titer in the cultured cells can be increased by at least 50% by the addition of at least 0.5 mg/L of a polyamine to an oligopeptide-free cell culture medium. In still another embodiment said increase is at least 60%. In yet another embodiment the cell specific productivity is increased at least two-fold by the addition of at least 0.5 mg/L of a polyamine to an oligopeptide-free cell culture medium; in another embodiment the cell specific productivity is increased at least three-fold. In still another embodiment, the addition of at least 0.5 mg/L of a polyamine results in an increase in protein expression and/or virus titer to at least 400%; in a further embodiment to at least 500%; in another embodiment to at least 600%; in a further embodiment to at least 700%.

[032] In one embodiment the specific growth rate of the cultured cells can be increased by the addition of at least 0.5 mg/L of a polyamine to an oligopeptide-free cell culture medium. In a further embodiment, said specific growth rate can be increased by 10%. In still another embodiment, said specific growth rate can be increased by 20%. In yet another embodiment, said specific growth rate can be increased by 50%. In a further embodiment, said specific growth rate can be increased by 70%. In another embodiment, said specific growth rate can be increased by 80%. In still another embodiment, said specific growth rate can be increased by 90%. In yet another embodiment, said specific growth rate can be increased by 100%.

[033] In a further embodiment of the present invention, the medium is chemically defined. The term "chemically defined" as used herein shall mean, that the medium does not comprise any undefined supplements, such as, for example, extracts of animal components, organs, glands, plants, or yeast. Accordingly, each component of a chemically defined medium is accurately defined.

[034] The present invention further relates to a method for cultivating cells, comprising the steps of:

- (a) providing an oligopeptide-free cell culture medium according to the invention, and
- (b) propagating the cells in the medium to form a cell culture.

[035] The present invention is not limited to any type of cells. Examples of cell types include mammalian cells, insect cells, avian cells, bacterial cells, and yeast cells. The cells may be for example stem cells or recombinant cells transformed with a vector for recombinant gene expression, or cells transfected with a virus for producing viral products. The cells may also be for example cells producing a protein of interest without recombinant transformation, e.g. a B-cell producing an antibody, which may be transformed into an immortalized status e.g. by viral infection like Epstein Barr Virus infection. The cells may also be for example primary cells, e.g. chicken embryo cells, or primary cell lines. Useful are cells that are used for *in vitro* virus production. Specific examples of useful cells include BSC cells, LLC-MK cells, CV-1 cells, COS cells, VERO cells, MDBK cells, MDCK cells, CRFK cells, RAF cells, RK cells, TCMK-1 cells, LLCPK cells, PK15 cells, LLC-RK cells, MDOK cells, BHK-21 cells, CHO cells, NS-1 cells, MRC-5 cells, WI-38 cells, BHK cells, 293 cells, RK cells, Per.C6 cells and chicken embryo cells.

[036] The cells used according to the present invention may be cultivated e.g. by a method selected from the group of batch-cultivation, feed-batch-cultivation, perfusion cultivation and chemostate-cultivation, all of which are generally known in the field.

[037] The present invention further relates to a method for expressing at least one protein, such as e.g. a heterologous or autologous protein or a recombinant protein, comprising the steps of:

- a) providing a culture of cells;
- b) introducing at least one nucleic acid sequence comprising a sequence coding for at least one protein into the cells;
- c) selecting the cells carrying the nucleic acid sequence; and
- d) expressing the protein in the cells in a medium comprising at least 0.5 mg/L of a polyamine.

[038] In one embodiment of the present invention, the medium of step d) is an oligopeptide-free medium according to the present invention. In a further embodiment of the present invention, the cells of the culture of step a) have been grown in an oligopeptide-free cell culture medium according to the present invention. In another embodiment, steps a) to d) are conducted in an oligopeptide-free cell culture medium according to the invention.

[039] The nucleic acid sequence comprising a sequence coding for at least one protein may be a vector. The vector may be delivered by a virus or may be a plasmid. The nucleic acid sequence coding for the protein may be a specific gene or a biologically functional part thereof. In one embodiment the protein is at least a biologically active part of a blood coagulation factor such as Factor VIII or at least a biologically active part of a protein involved in the production of red blood cells and angiogenesis such as erythropoietin, or a monoclonal antibody.

[040] In an embodiment, the nucleic acid sequence comprises a sequence coding for at least one protein selected from the group of coagulation factor VII, coagulation factor VIII, coagulation factor IX, vWF, ADAMTS13, and furin.

[041] In an embodiment of the present invention, the nucleic acid further comprises other sequences suitable for a controlled expression of a protein such as promotor sequences, enhancers, TATA boxes, transcription initiation sites, polylinkers, restriction sites, poly-A-sequences, protein processing sequences, selection markers, and the like which are generally known to a person skilled in the art.

[042] In one embodiment of the invention, the cells are selected from the group of CHO cells, 293 cells, and BHK cells.

[043] According to another embodiment of the present invention the following cell lines may be transformed with a recombinant vector for the expression of the respective products: CHO cells for the production of recombinant coagulation factors, for example factor VII, and/or factor VIII, and/or monoclonal antibodies, BHK cells for the production of recombinant erythropoietin, Epstein Barr virus transformed, immortalized human B cells for the production of human antibodies. Useful cell/ protein combinations are, for example, CHO cells/coagulation factor VIII, CHO cells/coagulation factor VII, CHO cells/ADAMTS13, CHO cells/furin, and 293 cells/ coagulation factor IX.

[044] In a further embodiment of the present invention, the expression of the at least one protein by cells being cultivated in a medium according to the present invention is increased when compared to the expression of the protein by cells not being cultivated in a medium of the present invention. In another embodiment said expression is increased for at least 10%, according to a further embodiment for at least 50%.

[045] The present invention further relates to a method for producing at least one virus or at least one part of a virus, comprising the steps of:

- a) providing a culture of cells;
- b) infecting the cells with at least one virus;
- c) selecting the virus-infected cells; and
- d) propagating the at least one virus in the cells in a medium comprising at least

0.5 mg/L of a polyamine.

[046] In one embodiment of the present invention, the medium of step d) is an oligopeptide-free medium according to the present invention. In a further embodiment of the present invention, the cells of the culture of step a) have been grown in an oligopeptide-free cell culture medium according to the present invention. In another embodiment, steps a) to d) are conducted in an oligopeptide-free cell culture medium according to the invention.

[047] The virus used in the method according to the invention may be any virus, such as, for example, poxviruses, for example vaccinia or attenuated vaccinia viruses; coronaviruses, for example SARS virus; orthomyxoviruses, for example influenza A or B virus; paramyxoviruses; retroviruses, for example Lenti virus; togaviruses, for example Ross River virus; flaviviruses, for example West Nile virus, Yellow Fever Virus, or FSME virus (i.e. tick borne encephalitis virus); enteroviruses, for example hepatitis A virus; picornaviruses; arenaviruses; herpesviruses; or adenoviruses. In one embodiment of the present invention, the virus is Modified Vaccinia Virus Ankara (MVA). The virus can be propagated according to the invention for the production of a respective vaccine.

[048] The virus may be a wild-type-virus, an attenuated virus, a reassortant virus, or a recombinant virus or combinations thereof, e.g. attenuated and recombinant. In addition, instead of actual virions being used to infect cells with a virus, an infectious nucleic acid clone may be used. Split virions may also be used.

[049] The method for producing a virus may be used for producing immunogenic compositions comprising a virus, a virus antigen, or a virus-like-particle.

[050] The cells used in the method for producing a virus according to the present invention may be selected from the group consisting of mammalian cells, insect cells, avian cells, bacterial cells, and yeast cells. In one embodiment, the cells used in the



method for producing a virus according to the present invention are selected from the group consisting of Vero cells and chicken embryo cells.

[051] Useful combinations of cells with viruses for producing a virus or part of a virus are, for example, Vero cell/attenuated vaccinia, Vero cell/Vaccinia, Vero cell/Hepatitis A, Vero cell/ Influenza Virus, Vero cell/West Nile Virus, Vero cell/SARS Virus, Vero cell/Yellow Fever Virus, and chicken embryo cells/FSME virus. In one embodiment of the invention, the cell/virus combination is chicken embryo cells/Modified Vaccinia Virus Ankara (MVA).

[052] Useful cultivation methods include batch-cultivation, feed-batch-cultivation, perfusion cultivation and chemostat-cultivation.

[053] The present invention will now be further illustrated in the following examples, without being limited thereto.

## EXAMPLES

### Example 1: Preparation of BAV-medium

Oligopeptide-free medium (BAV-medium) was prepared with basal DMEM/HAM's F12 (1:1) medium comprising inorganic salts, amino acids, vitamins and other components (Life technologies, 32500 Powder). Also added were L-glutamine ( 600 mg/L), ascorbic acid (20µM), ethanol amine (25 µM), Synperonic® (SERVA) (0.25 g/L), sodium selenite (50 nM). Additionally essential amino acids were supplemented to the cell culture medium: L-Asparagine.H<sub>2</sub>O 20 mg/L, L-Cysteine.HCl.H<sub>2</sub>O 15 mg/L, L-Cystine.2 HCl 20 mg/L, L-Proline 35 mg/L, L-Tryptophan 20 mg/L.

### Example 2: Determination of cell counts

Cell counts from suspension cells or immobilized cells were determined either by counting with a CASY® cell counter as described by Schärfe et al., Biotechnologie in

LaborPraxis 10: 1096 - 1103 (1988), or by citric acid extraction and fluorescent staining of the nuclei followed by counting with a NucleoCounter® (Chemometec, DK). The specific growth rate ( $\mu$ ) is calculated from the increase of the cell densities ( $X_t$ ) and/or the dilution rate ( $D$ ) of the steady state of chemostat cultures of suspensions cells over a certain time interval ( $t$ ):

$$\mu = D + \ln (X_t/X_0)/t$$

#### Example 3: Determination of FVIII activity

The activity of Factor VIII (FVIII) (cf. Figures 1 to 5) was measured by a chromogenic assay (Chromogenic, Sweden).

#### Example 4: Calculation of the volumetric (QP) and cell specific productivity (qp)

The volumetric productivity (QP) is calculated from the amount of activity units yielded per liter reactor volume per day (U/L/d) in the production system.

The cell specific productivity (qp) is defined as the specific amount of produced protein (U or  $\mu$ g) per number of cells per day.

#### Example 5: Large scale cell culture conditions

Cell cultures of recombinant mammalian cells (e.g. CHO-cells stably expressing Factor VIII, such as GD8/6 cells) were grown in suspension in a chemostat culture in 10 l bioreactors. The culture conditions of 37 °C, oxygen saturation 20%, and pH 7.0 to 7.1 were kept constant. The cultures were supplied with a constant feed of BAV-medium.

#### Example 6: Effect of the addition of a polyamine on FVIII expression

GD8/6 cells were grown in chemostat culture in a 10 L bioreactor as described in Example 5 with a continuous feed of BAV-medium for 11 days, resulting in a decreased productivity of < 100U/L/d. By addition of putrescine.2HCl (2 mg/L) the volumetric FVIII-expression increased by 800% (cf. Figure 1). Accordingly, putrescine could be clearly identified as the driving factor of cell specific expression for the GD8/6 cell line.

Example 7: Effect of the addition of a polyamine and Fe (II) and Cu (II) on FVIII expression

GD8/6 cells were grown in chemostat culture in a 10 L bioreactor as described in Example 5, resulting in an average productivity of 271 U/L/D, with low cell specific productivity and specific growth rates. By addition of Putrescine.2HCl (2mg/L) the FVIII expression increased to 870 U/L/D, mainly due to an increased cell specific productivity. Additional supplementation with Fe (II) and Cu (II) in a concentration as it is otherwise typically comprised in soy hydrolysates was leading to an increased specific growth rate of approximately  $0.60\text{ d}^{-1}$ , and an increase of the cell specific productivity to over 1700 mU/10E06 cells/day could be achieved. Under these conditions a volumetric productivity of over 2685 U/L/D was reached. A further increase of the cell density resulted in a volumetric productivity of over 3000 U/L/D. The maximum volumetric productivity of a soy hydrolysate comprising medium under comparable fermentation conditions was 2000 to 2500 U/L/D, indicating that a chemically defined medium comprising only Putrescine and 2 additional metal ions is superior to any soy hydrolysate comprising medium formulation investigated in this process before (cf. Figure 2).

Example 8: Small scale cell culture conditions

Small scale experiments with GD8/6 cells in suspension culture were carried out in Techne spinner flasks at 200 ml working volume in batch refeed mode at 37°C, without pH and  $pO_2$  control. The cultures were supplied with BAV-medium as defined above additionally supplemented with Putrescine.2HCl, Ornithine.HCl, Spermine.4HCl, or Ethanolamine or combinations thereof in the range of 0-18 mg/L (equivalent to 0-10 mg/L of the biogenic amine without .HCl (cf. Figure 3 to 5).

Example 9: Effect of the addition of several polyamines and combinations of polyamines on FVIII expression

GD8/6 cells from a culture with BAV-medium as described in Example 8 were centrifuged and transferred to Techne Spinner flasks with a working volume of 200 ml

and incubated at a cell density of about  $1-2 \times 10^6$  cell/ml with defined medium, supplemented with ethanolamine, putrescine, ornithine, and/or spermine as indicated in Figures 3, 4, and 5. Ornithine, which is a precursor of putrescine in the pathway of biogenic amines, could partially substitute putrescine in a concentration-dependent manner. The addition of ornithine at different concentrations to the media comprising putrescine.2HCl resulted in an additional increase of specific FVIII productivities and growth rates (cf. Figure 3). However, ethanolamine, which is not a polyamine according to the present invention, could neither replace putrescine in any concentration investigated, nor an increase of the ethanolamine concentration in medium comprising putrescine resulted in a significant increase of volumetric productivities or specific growth rates (cf. Figure 5). A further experiment under similar conditions showed that spermine, another intermediate in the pathway of biogenic amines, could also substitute putrescine in a concentration-dependent manner (cf. Figure 4).

#### Example 10: Effect of the addition of a polyamine on MVA virus production

Primary cell cultures of chicken embryos were cultivated in Techne spinner flasks (working volume 200 ml) using a peptide free medium (FM-Medium) without and with supplementation of 3.6 mg/L Putrescine.2 HCl.

FM medium was prepared with basal M199 medium comprising inorganic salts, amino acids, vitamins and other components (Life technologies, 31150 Powder). Also added were  $\text{NaHCO}_3$  (ad 4.4 g/L), Gentamycin. $\text{SO}_4$  (50  $\mu\text{g/L}$ ) and Neomycin. $\text{SO}_4$  (50 $\mu\text{g/L}$ ).

Cell cultures were infected with MVA virus and supernatants were analysed for virus titer in a TCID<sub>50</sub> assay. By the addition of Putrescine, the average virus titer (n = 16 samples each) could be increased by approximately 50% (cf. Figure 6).

#### Example 11: Effect of the addition of several doses of a polyamine on MVA virus production

Primary cell cultures of chicken embryos were cultivated in Techne spinner flasks (working volume 200 ml) using a peptide free medium (CEM-Medium) without and with supplementation of 3.6 and 9 mg/L Putrescine.2 HCl.

CEM medium was prepared with basal DMEM/HAM's F12 (1:1) medium comprising inorganic salts, amino acids, vitamins and other components (Life technologies, 32500 Powder). Also added were NaHCO<sub>3</sub> (2 g/L) L-glutamine (600 mg/L), ascorbic acid (20µM), ethanol amine (25 µM), Synperonic® (SERVA) (0.25 g/L), sodium selenite (50 nM), FeSO<sub>4</sub>.7H<sub>2</sub>O (600µg/L), Gentamycin.SO<sub>4</sub> (50 µg/L) and Neomycin.SO<sub>4</sub> (50µg/L). Additionally essential amino acids were supplemented to the cell culture medium: L-Asparagine.H<sub>2</sub>O 20 mg/L, L-Cysteine.HCl.H<sub>2</sub>O 15 mg/L, L-Cystine.2 HCl 20 mg/L, L-Proline 35 mg/L, L-Tryptophan 20 mg/L.

Cell cultures were infected with MVA virus and supernatants were analysed for virus titer in a TCID<sub>50</sub> assay. By the addition of Putrescine with 9 mg/L, the average virus titer (n = 4 samples each) could be increased by approximately 60% (cf. Figure 7).

The term "comprise" and variants of the term such as "comprises" or "comprising" are used herein to denote the inclusion of a stated integer or stated integers but not to exclude any other integer or any other integers, unless in the context or usage an exclusive interpretation of the term is required.

Any reference to publications cited in this specification is not an admission that the disclosures constitute common general knowledge in Australia.

**CLAIMS**

1. A method for expressing at least one protein, comprising the steps of:
  - (a) providing a culture of cells;
  - (b) introducing at least one nucleic acid sequence comprising a sequence coding for at least one protein selected from the group of coagulation factor VII, coagulation factor VIII, coagulation factor IX, vWF, ADAMTS13 and furin into the cells;
  - (c) selecting the cells carrying the nucleic acid sequence; and
  - (d) expressing the protein in the cells in an oligo-peptide free medium comprising at least 0.5mg/L of a polyamine.
2. The method of claim 1, wherein the cells are cultivated by chemostate cultivation.
3. The method of claim 1 or claim 2, wherein the cells are CHO cells, 293 cells or BHK cells.
4. The method of any one of the preceding claims, wherein the cell/protein combination is selected from the group consisting of CHO cells/coagulation factor VIII, CHO cells/coagulation factor VII, CHO cells/ADAMTS13, CHO cells/furin, and 293 cells/coagulation factor IX.
5. The method of any one of the preceding claims, wherein the cell/protein combination is CHO cell/coagulation factor VIII, and wherein the medium comprises added Fe(II) and Cu(II).
6. The method of any one of the preceding claims, wherein the polyamine is selected from the group consisting of cadaverine, putrescine, spermidine, spermine, agmatine, ornithine, and combinations thereof.
7. The method of any one of the preceding claims, wherein the medium comprises ornithine, putrescine or spermine, or combinations thereof.
8. The method of any one of the preceding claims, wherein the polyamine is synthetically produced.
9. The method of any one of the preceding claims, wherein the polyamine is present

in the culture medium in a concentration ranging from 0.5 to 30mg/L.

10. The method of any one of the preceding claims, wherein the medium is chemically defined.

Dated: 5 September 2012

Figure 1

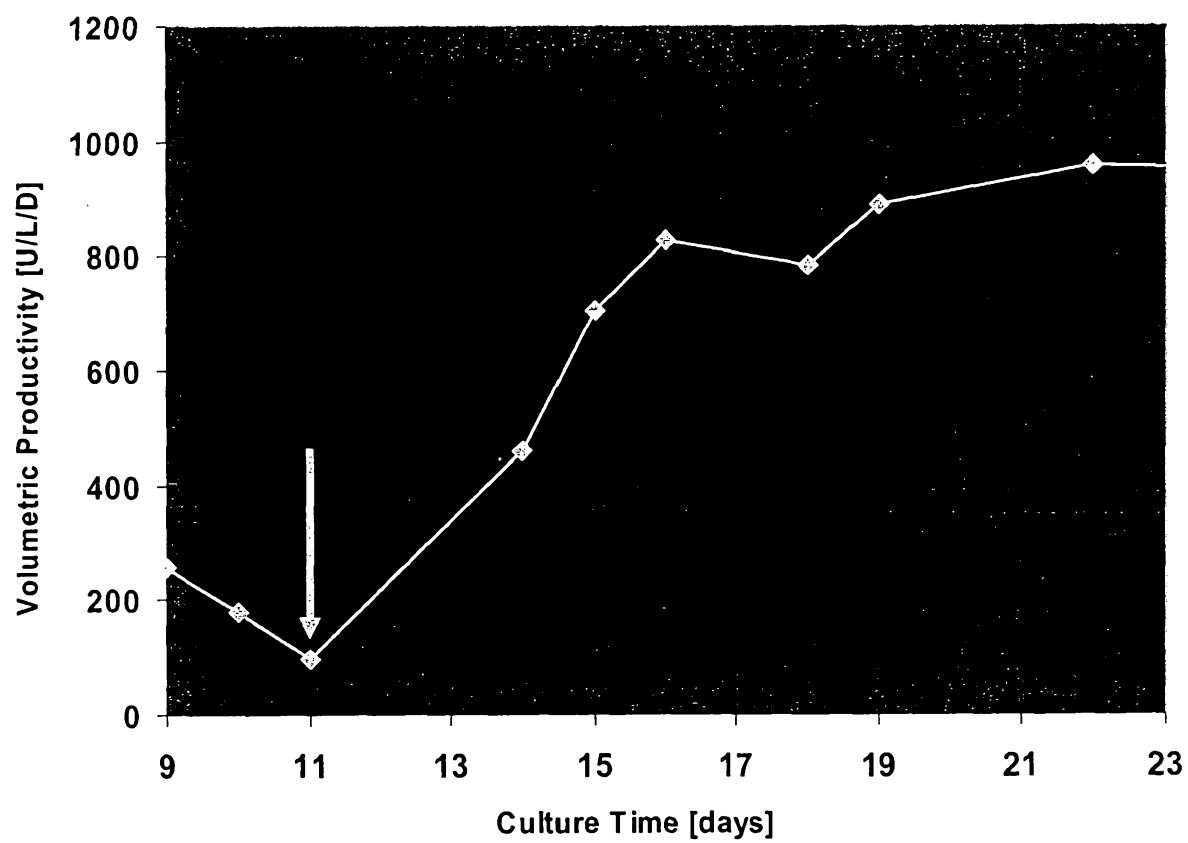




Figure 2

	QP [U/L/D]	qp [mU/10E06 cells/ day]	$\mu$ [d <sup>-1</sup> ]
BAV-Medium without supplement	271	236	0.37
BAV-Medium + Putrescine.2HCl (2 mg/L)	870	671	0.41
BAV-Medium + Putrescine.2HCl (2 mg/L) + Fe(II) ad 2.3 x concentration + Cu (II) ad 2.0 x concentration	1393	958	0.59
BAV-Medium + Putrescine.2HCl (2 mg/L) + Fe(II) ad 2.3 x concentration + Cu (II) ad 12.5 x concentration	2685	1744	0.63
BAV-Medium + Putrescine.2HCl (2 mg/L) + Fe(II) ad 2.3 x concentration + Cu (II) ad 12.5 x concentration With increased cell density	3107	1756	0.63

Figure 3

	qp absolute [mU/10E06 cells/ day]	qp relative [ % ]	$\mu$ absolute [ d-1 ]	$\mu$ relative [ % ]
BAV medium without additional biogenic amine	172	100	0.19	100
Putrescine.2HCl (2 mg/L)	697	405	0.34	179
Ornithine.HCl (2 mg/L)	457	266	0.34	179
Ornithine.HCl (10 mg/L)	587	341	0.37	195
Putrescine.2HCl (2 mg/L) +Ornithine.HCl (2 mg/L)	806	467	0.36	189
Putrescine.2HCl (2 mg/L) +Ornithine.HCl (10 mg/L)	1050	610	0.39	205

**Figure 4**

	qp absolute [mU/10E06 cells/ day]	qp relative [ % ]	μ absolute [ d-1 ]	μ relative [ % ]
Putrescine.2HCl (2 mg/L)	2303	100	0.61	100
Spermine.4HCl (0.4 mg/L)	1331	58	0.59	97
Spermine.4HCl (2 mg/L)	2639	115	0.60	98
Spermine.4HCl (10 mg/L)	2651	115	0.59	97

**Figure 5**

	qp absolute [mU/10E06 cells/ day]	qp relative [ % ]	μ absolute [ d-1 ]	μ relative [ % ]
BAV medium standard Ethanolamine (1.53 mg/L) Stand. conc.=neg. control	172	100	0.19	100
Ethanolamine (ad 3.83 mg/L)	188	109	0.23	118
Ethanolamine (ad 15.3 mg/L)	183	106	0.22	118
Ethanolamine (ad 38.3 mg/L)	171	100	0.23	125
Putrescine.2HCl (2 mg/L) +Ethanolamine (ad 3.83 mg/L)	545	317	0.36	193
Putrescine.2HCl (2 mg/L) +Ethanolamine (ad 15.3 mg/L)	609	354	0.32	173
Putrescine.2HCl (2 mg/L) +Ethanolamine (ad 38.3 mg/L)	553	322	0.32	172

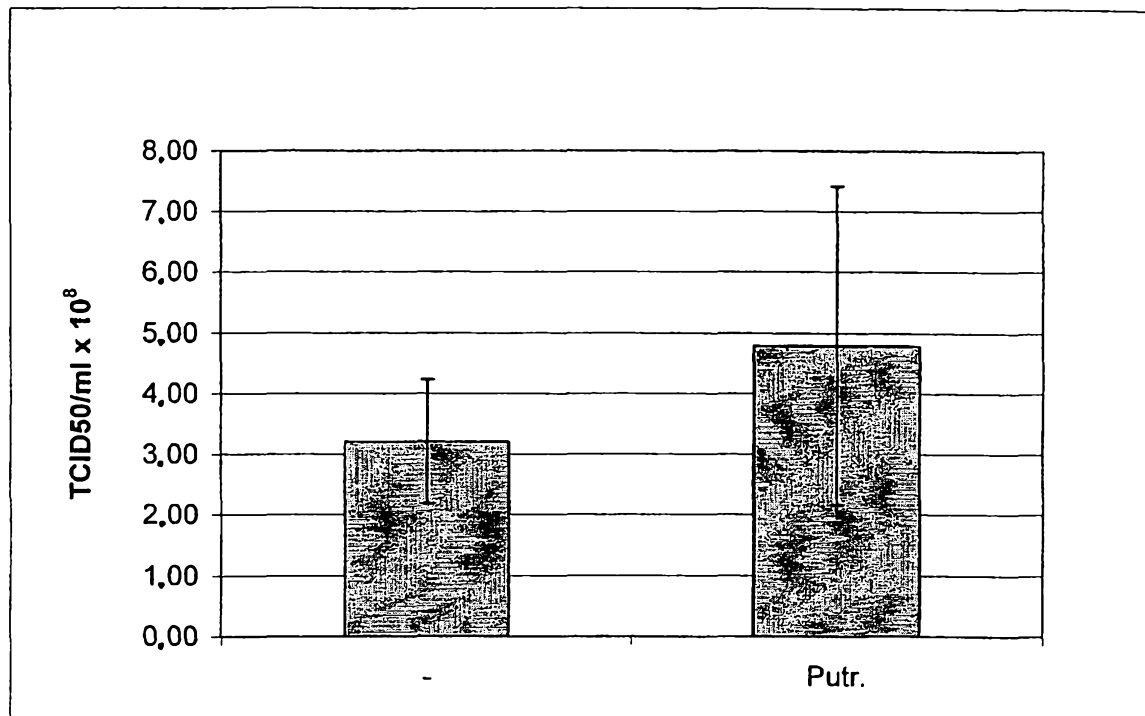
**Figure 6**

Figure 7

