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(54) Title: METHOD FOR IMPROVING THE CONSOLIDATION AND DEWATERING OF SUSPENDED PARTICULATE MATTER

(57) Abstract: Methods are provided for treating suspensions of particles to improve the drainage rate and/or the solids content of flocs of the particles. The method includes the steps of (i) providing a suspension which comprises particles in a fluid; (ii) adding a cyclodextrin compound to the suspension; and (iii) dewatering the suspension by removing at least a portion of the fluid to form a cake comprising the particles. The cyclodextrin compound desirably is added in an amount effective to increase the dewatering rate of the flocs, to increase the solids content, or both, over that rate, solids content, or both, that would be obtained without the addition of the cyclodextrin compound. The suspension may be, for example, a biological or non-biological sludge, or a suspension of pulp fibers, such as in a pulping or papermaking process.



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METHOD FOR IMPROVING THE CONSOLIDATION AND DEWATERING OF SUSPENDED PARTICULATE MATTER

Cross Reference to Related Applications

This application claims the benefit of U.S. Provisional Application No. 60/653,052, filed February 15, 2005, which is incorporated herein by reference in its entirety.

Background of the Invention

This invention is generally in the field of dewatering wet particulate matter, and more particularly to methods for increasing the rate of dewatering sludge, pulp fibers, or other solid particulate materials and for increasing the solids content of a dewatered cake.

Industrial processes can produce wet solids that require treatment before disposal, use, or reuse. Examples of such processes include the biological treatment of wastewater and the manufacture of pulp and paper. The wet solids are commonly referred to as sludge, and generally comprise a suspension of particles in a liquid. An example of treating sewage sludge is described in U.S. Patent No. 6,808,636 to Ward et al., which is incorporated herein by reference.

Conventional techniques for treating wet solids include the steps of promoting flocculation of particles and then dewatering of the flocculated particles. Chemical thickeners, such as polymers and lime, are generally used to promote flocculation of the particles to form flocs. Dewatering techniques, which are well known in the art, are used to produce a cake for disposal. Non-limiting examples of such techniques include pressing and centrifugation of the flocculated particles. The resulting cake typically comprises between approximately 15 and 50% solids (i.e., about 85 to 50% water content).

Disposal methods for the cake typically include means such as landfilling, burning, or landspreading. The water content of the cake is merely a deadload. Accordingly, it would be highly advantageous to reduce the water content of the final cake as much as possible, which can be achieved by increasing the solids content of the cake. Thus, there is a need for a method to increase the solids content of a cake derived from dewatered wet solids.

Dewatering is also critical in other applications. For instance, dewatering is particularly important in the processing of fibers, such as pulp. See, for example, U.S. Patent No. 6,103,064 to Asplund et al., which is incorporated herein by reference. In a conventional process, the pulp is thickened through drainage or pressing during various process operations, for example in a papermaking process. Improving the drainage rate or the solids content of the drained pulp

would improve throughput and increase production. Accordingly, a need exists for a method to increase the rate of dewatering, in order to maximize the throughput of the dewatering device.

Summary of the Invention

5 Methods are provided for treating suspensions of particles to improve the drainage rate or the solids content of flocs of the particles, to thereby provide better dewatering process throughput and, in the case of sludge, less deadload for disposal. Generally, the method includes the steps of (i) providing a suspension which comprises particles in a fluid; (ii) adding a cyclodextrin compound to the suspension—typically in addition to at least one conventionally
10 used thickening additive; and (iii) dewatering the suspension by removing at least a portion of the fluid to form a cake comprising the particles. The cyclodextrin compound desirably is added in an amount effective to increase the dewatering rate of the flocs, to increase the solids content, or both, over that rate, solids content, or both, that would be obtained without the addition of the cyclodextrin compound. The fluid may be aqueous. In a preferred embodiment, the suspension
15 comprises a biological sludge, a non-biological sludge (e.g., an industrial sludge), or a combination thereof. In another embodiment, the suspension comprises pulp fibers, such as in a pulping or papermaking process.

 In a preferred embodiment, the formation of flocs through flocculation of the particles is promoted before the step of adding the cyclodextrin compound. In one embodiment, the step
20 of promoting the formation of flocs is performed by adding a chemical thickener to the suspension. The dewatering step may be carried out by pressing or centrifuging the flocs or a combination thereof. In preferred embodiments, the cyclodextrin compound may be selected from α -cyclodextrin compounds, β -cyclodextrin compounds, and γ -cyclodextrin compounds, or derivatives or and combinations of these. In one embodiment, the amount of the cyclodextrin
25 compound added is between 0.01 and 20 lbs per ton of the particles expressed on a dry solids basis. In another embodiment, the amount of the cyclodextrin compound added is between 0.01 and 2000 mg/liter of the fluid.

 In a preferred aspect, a method is provided for dewatering a suspension of particles that includes the steps of (i) providing a suspension which comprises particles in a fluid; (ii)
30 promoting the formation of flocs through flocculation of the particles by the addition of a chemical thickener to the suspension; (iii) adding a cyclodextrin compound to the suspension; and (iv) dewatering the flocs at a dewatering rate to form a cake comprising the particles. In one embodiment, the chemical thickener comprises a polymer, a mineral, or a combination thereof.

For instance, the chemical thickener may include alum, lime, a cationic polyacrylamide, or a combination thereof.

Brief Description of the Drawings

5 **FIG. 1** is an illustration of the structure of β -cyclodextrin.

FIG. 2 is a process flow diagram showing the general process steps of the methods described herein.

FIG. 3 is a process flow diagram of a particular embodiment of the methods described herein.

10 **FIG. 4** is a series of electron micrographs showing the effect of adding various concentrations of a cyclodextrin compound on the flocculation of a suspension of biological particles.

Detailed Description of the Invention

15 Methods have been developed for treating a suspension of particles in a fluid to improve both the rate of dewatering and the particle content in a cake formed thereby. The methods advantageously improve the drainage rate or the solids content of flocs of the particles, to thereby provide better dewatering process throughput and, in the case of sludge, less deadload for disposal.

20 Conventional dewatering processes include steps for promoting the formation of flocs of particles by the flocculation of the particles and then dewatering of the flocs to form cakes, for subsequent use or disposal. Generally, the step of promoting formation of flocs of particles comprises treating the fluid with chemical thickeners to promote particle agglomeration and formation of flocs of particles, which are more easily dewatered than suspended particles. The
25 step of dewatering typically comprises subjecting the flocs to pressing or centrifugation. The present methods improve upon the prior art methods by treating a fluid comprising a suspension of particles with a cyclodextrin compound, which increases the particle content of the cake and the dewatering rate of the flocs.

 Advantageously, cyclodextrin compounds are generally significantly less expensive
30 than conventional polymer approaches, due for example to the classification of cyclodextrin compounds as a bulk chemical rather than a specialty chemical and the availability of bulk quantities of cyclodextrin compounds from commercial suppliers (such as the Wacker Chemical Company). As used herein, the term "cyclodextrin compound" refers to any compound in the family of oligosaccharides composed of five or more α -D-glycopyranoside units linked 1->4.

Typical cyclodextrin compounds comprise between six and eight glucose monomers in a ring; the α -cyclodextrin compound comprising six glucopyranose units, the β -cyclodextrin compound comprising seven glucopyranose units (illustrated in **FIG. 1**), and the γ -cyclodextrin compound comprising eight glucopyranose units. In preferred embodiments, the cyclodextrin compound
5 may be selected from an α -cyclodextrin compound, a β -cyclodextrin compound, a γ -cyclodextrin compound, derivatives thereof, and combinations thereof

Although the three naturally occurring cyclodextrin compounds are most common, cyclodextrin compounds comprising as few as five glucopyranose units to as many as 150 member cyclic oligosaccharides have also been identified. Typically, the structure of the
10 cyclodextrin compound comprises a relatively hydrophobic core and hydrophilic exterior. The hydrophilic exterior imparts water solubility to the cyclodextrin compounds and their complexes. The functional groups of cyclodextrin compounds can be derivatized to alter the properties of the cyclodextrin compounds.

While not wishing to be bound by any theory, it is believed that this unique structure
15 enables cyclodextrin compounds to bind with particles in a suspension of fluid, thereby promoting the formation of flocs by flocculation of the particles and increasing the content of particles in a cake. It is also believed that this contributes to an increased dewatering rate of flocs. These benefits can provide substantial cost savings by reducing the mass and volume of the wet solids requiring disposal and by increasing the efficiency of the dewatering process.

20 Generally, the present methods include the steps of (i) providing a suspension which comprises particles in a fluid; (ii) adding a cyclodextrin compound to the suspension; and (iii) dewatering the suspension by removing at least a portion of the fluid to form a cake comprising the particles. See **FIG. 2**. The cyclodextrin compound desirably is added in an amount effective to increase the dewatering rate of the flocs, to increase the solids content, or both, over that rate,
25 solids content, or both, that would be obtained without the addition of the cyclodextrin compound. In a preferred embodiment, a method for dewatering a suspension of particles includes the steps of (i) providing a suspension which comprises particles in a fluid; (ii) promoting the formation of flocs through flocculation of the particles by the addition of a chemical thickener to the suspension; (iii) adding a cyclodextrin compound to the suspension;
30 and (iv) dewatering the flocs at a dewatering rate to form a cake comprising the particles. The treatment and dewatering methods described herein may be performed in a continuous, batch, or semi-continuous process, depending upon the particular application needs and processing equipment.

The methods are applicable to a variety of different suspensions of particles. The particles may be in particulate, fiber, or fibril form, or combinations thereof. The particles may be formed of organic matter, inorganic matter, metals, plastics, minerals, biological matter, or combinations thereof. In preferred embodiments, the fluid is aqueous. However, the fluid may also be or include non-aqueous liquids, e.g., organic solvents, etc. In a preferred embodiment, the suspension comprises a biological sludge (e.g., a sewage sludge), a non-biological sludge (e.g., an industrial sludge), or a combination thereof. In another embodiment, the suspension comprises pulp fibers, such as in a pulping or papermaking process.

The step of promoting flocculation can be carried out by essentially any technique known in the art. In a preferred embodiment, the step of promoting the formation of flocs is performed by adding one or more chemical thickeners to the suspension. Suitable chemical thickeners, also called flocculants, are well known in the art and may be selected based, for example, on the particular suspension materials being processed. Representative examples of chemical thickeners include polymers (e.g., a cationic polyacrylamide), minerals (e.g., alum, lime), and combinations thereof. Other examples of useful polymeric flocculants are described in U.S. Patent No. 6,872,779 to Mori et al., which is incorporated herein by reference.

The step of adding the cyclodextrin compound to the suspension can be done before, during, or after the suspension undergoes flocculation. However, the compound preferably is added after pre-treatment of the suspension with a chemical thickener. See FIG. 3. In preferred embodiments, the cyclodextrin compound may be selected from α -cyclodextrin compounds, β -cyclodextrin compounds, and γ -cyclodextrin compounds, or derivatives or combinations of these. In one embodiment, the amount of the cyclodextrin compound added is between 0.01 and 20 lbs per ton of the particles expressed on a dry solids basis. In another embodiment, the amount of the cyclodextrin compound added is between 0.01 and 2000 mg/liter of the fluid.

The cyclodextrin compound can be added to the suspension in any of several different manners and forms. The cyclodextrin compound may be added by itself, or in a dilute or concentrated solution or suspension with a solvent or non-solvent. The one or more cyclodextrin compounds may be in the form of a composition that includes one or more additional components. It may be introduced into the suspension in a single point or in multiple points, in a continuous or non-continuous manner. It may, for example, be introduced into a process stream using a metering pump, or it may be gravity fed.

The dewatering step can be conducted using processes and equipment well known in the art. In preferred embodiments, the dewatering is carried out by pressing in a press or by centrifuging the flocs in a centrifuge. Combinations of such techniques are envisioned.

The present invention may be further understood with reference to the following non-limiting examples.

Example 1

β -cyclodextrin, obtained from Wacker Chemical Corporation, was added at up to 2
5 lbs/ton to a biological sludge treated with alum at 10 lbs/ton and cationic polyacrylamide
polymer at 25 lbs/ton. This method of treating biological sludge—without a cyclodextrin—is
well known in the art. The biological sludge comprised material collected from wastewater
treatment systems, and principally, is comprised of microorganisms and debris. The
cyclodextrin-treated mixture was drained on the gravity table of a Crown Press, which is a
10 belt press simulator well known in the art. As shown in Table 1, the drainage (the volume of
filtrate expressed per unit time) increased with the addition of a cyclodextrin compound.

The specific resistance to filtration (SRF), a standard method for measuring sludge
dewaterability, also was obtained by measuring the rate of filtration of sludge through a filter
paper under vacuum, a technique described by Yang & Banerjee in “Sludge Compaction with
15 Ash,” *Appita J.* (2006), which is incorporated herein by reference. As shown in Table 1, the
dewaterability was shown to be improved, that is the SRF decreased, as the cyclodextrin
dosage increased.

Table 1: Effect of β -cyclodextrin on drainage and SRF of biological sludge

Lbs cyclodextrin/ Ton biosludge	Drainage increase on gravity table (10#/t alum added, 25#/t c-PAM)	Decrease in specific resistance to filtration
0.0	-	-
0.1	n/a	12%
0.5	n/a	20%
1.0	15%	34%
2.0	16%	42%

20 Example 2

The flocculation of particles of a biological sludge pre-treated with a concentration of
0.11 lbs/ton of cationic polyacrylamide polymer was observed under a microscope after
addition of various concentrations of β -cyclodextrin. Electron micrographs illustrating the
flocculation of particles are shown in **FIG. 4**. The biological sludge was treated with β -
25 cyclodextrin at amounts as follows in lbs/ton: A=0, B=0.01, C=0.05, D=0.1, E=0.2. As the
amount of β -cyclodextrin increased, the consolidation of particles also increased. A
cyclodextrin dose of 0.1 lb/odt CD is optimal for this application. It is well known that floc
formation improves drainage and dewaterability.

Example 3

A hardwood pulp suspension of 2% by weight was pretreated with cationic polyacrylamide at dosage of 7.5 lbs/ton of pulp. β -cyclodextrin was added at various dosages, and the dewaterability of the pulp was measured using the percent decrease in SRF.

- 5 As shown in Table 2, the dewaterability improves, that is the SRF decreases, in the presence of β -cyclodextrin. The optimum β -cyclodextrin dosage for this application was about 0.18 lbs/ton.

Table 2: Effect of cyclodextrin on the drainage of hardwood pulp

Cyclodextrin concentration (lbs/ton of pulp)	% decrease in SRF
0.76	6.6
0.38	50
0.18	86
0.09	21

10 **Example 4**

- The effect of β -cyclodextrin on dewatering industrial sludge was measured with sludge collected from a newsprint mill in the southeastern United States. The sludge was comprised of ink, fiber debris, and other material. The sludge was first treated with K133L polymer from the Stockhausen Company, a polymer commonly used in sludge dewatering applications, at a dosage of 30 lbs/dry ton of sludge. β -cyclodextrin was added at various dosages, and the mixture pressed in the same Crown Press described in Example 1. As shown in Table 3, the solids content of the cake obtained after pressing clearly illustrates that the cyclodextrin increases the particle content of the cake. Correspondingly, the sludge volume per unit of dry solids is reduced, thereby reducing the volume of sludge requiring disposal in a landfill or otherwise.
- 15
- 20

Table 3: Effect of β -cyclodextrin on cake particle content of industrial sludge

β -cyclodextrin (lbs/ton)	Particle content of cakes (%)
0	28.1
0.2	29.3
0.4	30.5

Example 5

- The effect of β -cyclodextrin on increasing the solids content of biological sludge was measured with sludge collected from an activated sludge plant located at a paper mill. A conventional polymer, Bulab 5196 from Buckman Laboratories, was added at two dosages to the incoming sludge, which comprised a solids content of 1.4% by weight. As shown in
- 25

Table 4, the addition of cyclodextrin increased the solids content of the cake by between 1 and 2.4 percentage points, thereby reducing the volume of the sludge requiring disposal in a landfill or otherwise.

Table 4: Effect of cyclodextrin on particle content of cakes of biological sludge

β -cyclodextrin (ppm)	Particle content of cakes (%)
Polymer: 5 lbs/ton	
0	23.2
50	24.7
100	24.3
200	25.6
Polymer: 3.75 lbs/ton	
0	24.1
50	25.4
100	24.9
200	25.1

5

Example 6

The effect was studied of various cyclodextrin compounds (abbreviated as "CD" in Table 5 below) in combination with various commercially available cationic polyacrylamide polymers from Eka Chemical Company and from Hercules Chemical Company on the solids content of cakes obtained from pressing pulp obtained from a linerboard mill in the southeastern United States. The polymers were added to the pulp at a concentration of 4 lbs per dry ton of pulp. Various cyclodextrin compounds of known structure, obtained from Wacker Chemical Company of Munich, Germany, were added at a concentration of 0.2 lbs per dry ton of pulp. The sludges were pressed with a Crown Press. As shown in Table 5, the particle content of the cake increased with the addition of cyclodextrin compounds.

10
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Table 5: Effect of CD and polymers on cake particle content (as measured by %)

Polymer	No CD	α -CD	β -CD	γ -CD	Hydroxy- α -CD (CAVSOL W6 HP)	Hydroxy- β -CD (CAVSOL W7 HP)
Eka PL-2620F	16.6	17.3	17.5	17.5	17.7	18.3
Hercules D1373	17.6	18.7	18.7	19.4	19.2	20.2
Hercules PC8715	17.6	17.5	18.9	19.0	20.0	20.7
Hercules PP99	17.1	17.3	17.3	18.7	18.9	17.9

Publications cited herein are incorporated by reference. Modifications and variations of the methods and devices described herein will be obvious to those skilled in the art from the foregoing detailed description. Such modifications and variations are intended to come within the scope of the appended claims.

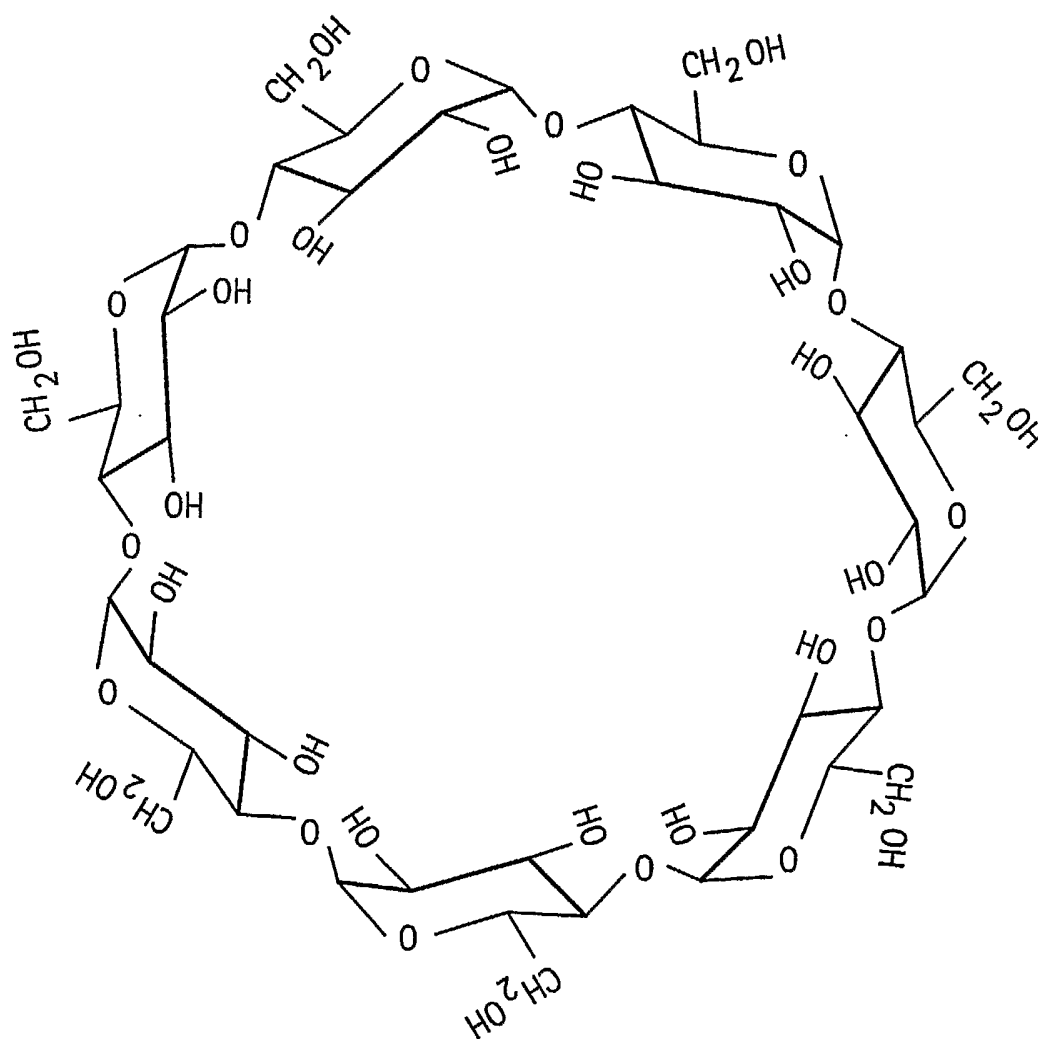
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I claim:

1. A method for treating a suspension of particles, the method comprising the steps of:
providing a suspension which comprises particles in a fluid;
adding at least one cyclodextrin compound to the suspension; and
dewatering the suspension by removing at least a portion of the fluid to form a cake comprising the particles.
2. The method of claim 1, further comprising, before the step of adding the cyclodextrin compound, promoting the formation of flocs through flocculation of the particles.
3. The method of claim 2, wherein the step of promoting the formation of flocs comprises adding a chemical thickener to the suspension.
4. The method of claim 2, wherein the step of dewatering comprises pressing the flocs, centrifuging the flocs, or a combination thereof.
5. The method of claim 1, wherein the cyclodextrin compound is selected from the group consisting of an α -cyclodextrin compound, a β -cyclodextrin compound, a γ -cyclodextrin compound, derivatives thereof, and combinations thereof.
6. The method of claim 1, wherein the fluid is aqueous.
7. The method of claim 1, wherein the suspension comprises a biological sludge, a non-biological sludge, or a mixture thereof.
8. The method of claim 1, wherein the suspension comprises pulp fibers.
9. The method of claim 2, wherein the cyclodextrin compound is added in an amount effective to increase the dewatering rate of the flocs, the solids content, or both, over that rate, solids content, or both, that would be obtained without the addition of the cyclodextrin compound.
10. The method of claim 1, wherein the amount of the cyclodextrin compound added is between 0.01 and 20 lbs per ton of the particles expressed on a dry solids basis.

11. The method of claim 1, wherein the amount of the cyclodextrin compound added is between 0.01 and 2000 mg/liter of the fluid.
12. A method for dewatering a suspension of particles, the method comprising:
 - providing a suspension which comprises particles in a fluid;
 - promoting the formation of flocs through flocculation of the particles by the addition of a chemical thickener to the suspension;
 - adding at least one cyclodextrin compound to the suspension; and
 - dewatering the flocs at a dewatering rate to form a cake comprising the particles.
13. The method of claim 12, wherein the suspension comprises a biological sludge, a non-biological sludge, or a mixture thereof.
14. The method of claim 12, wherein the suspension comprises pulp fibers.
15. The method of claim 12, wherein the chemical thickener comprises a polymer, a mineral, or a combination thereof.
16. The method of claim 15, wherein the chemical thickener comprises alum, lime, a cationic polyacrylamide, or a combination thereof.
17. The method of claim 12, wherein the cyclodextrin compound is added in an amount effective to increase the dewatering rate of the flocs over that rate that would be obtained without the addition of the cyclodextrin compound.
18. The method of claim 12, wherein the cyclodextrin compound is added in an amount effective to increase the solids content of the cake over that solids content that would be obtained without the addition of the cyclodextrin compound.

FIG. 1



2/4

FIG. 2

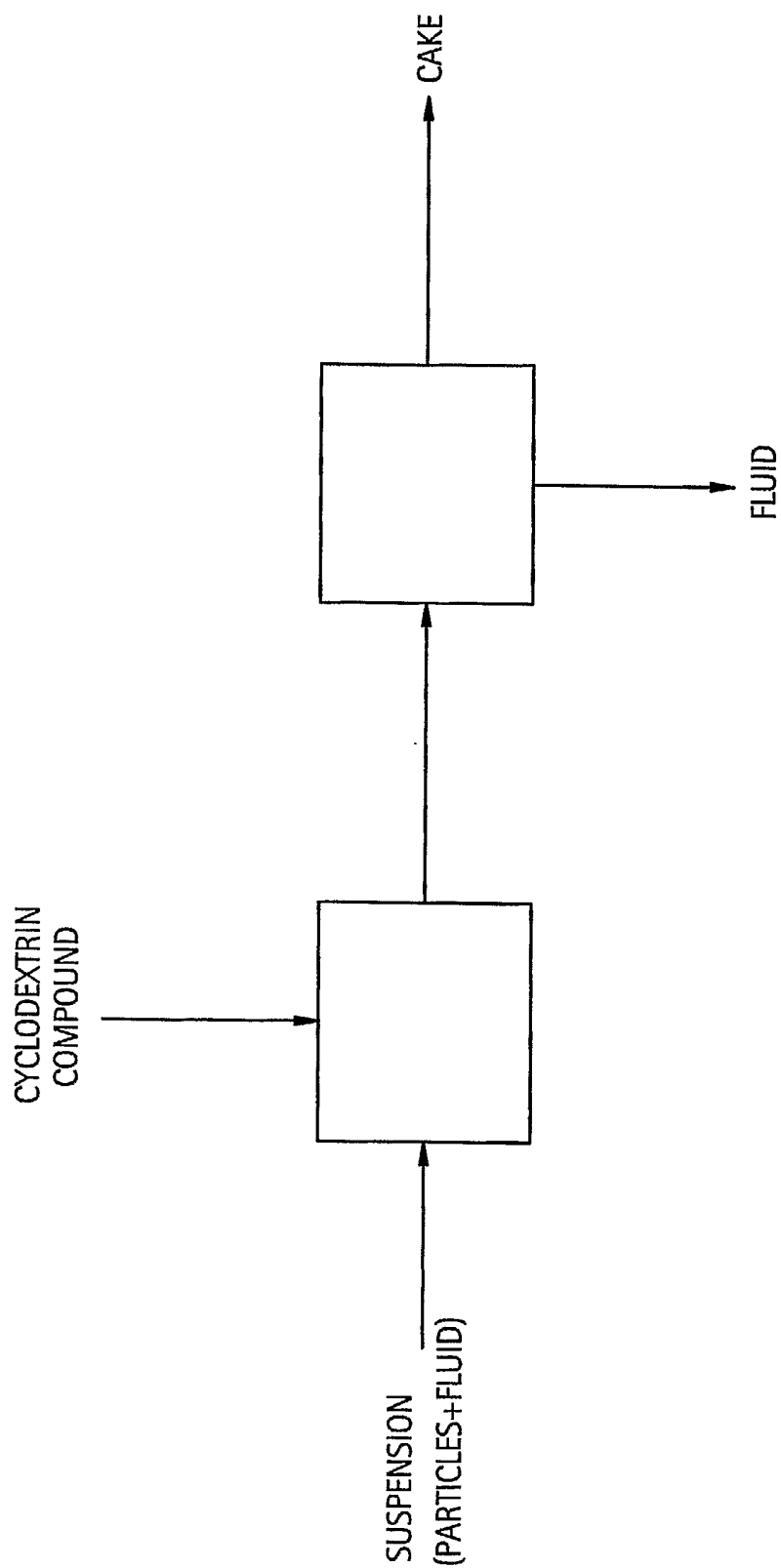


FIG. 3

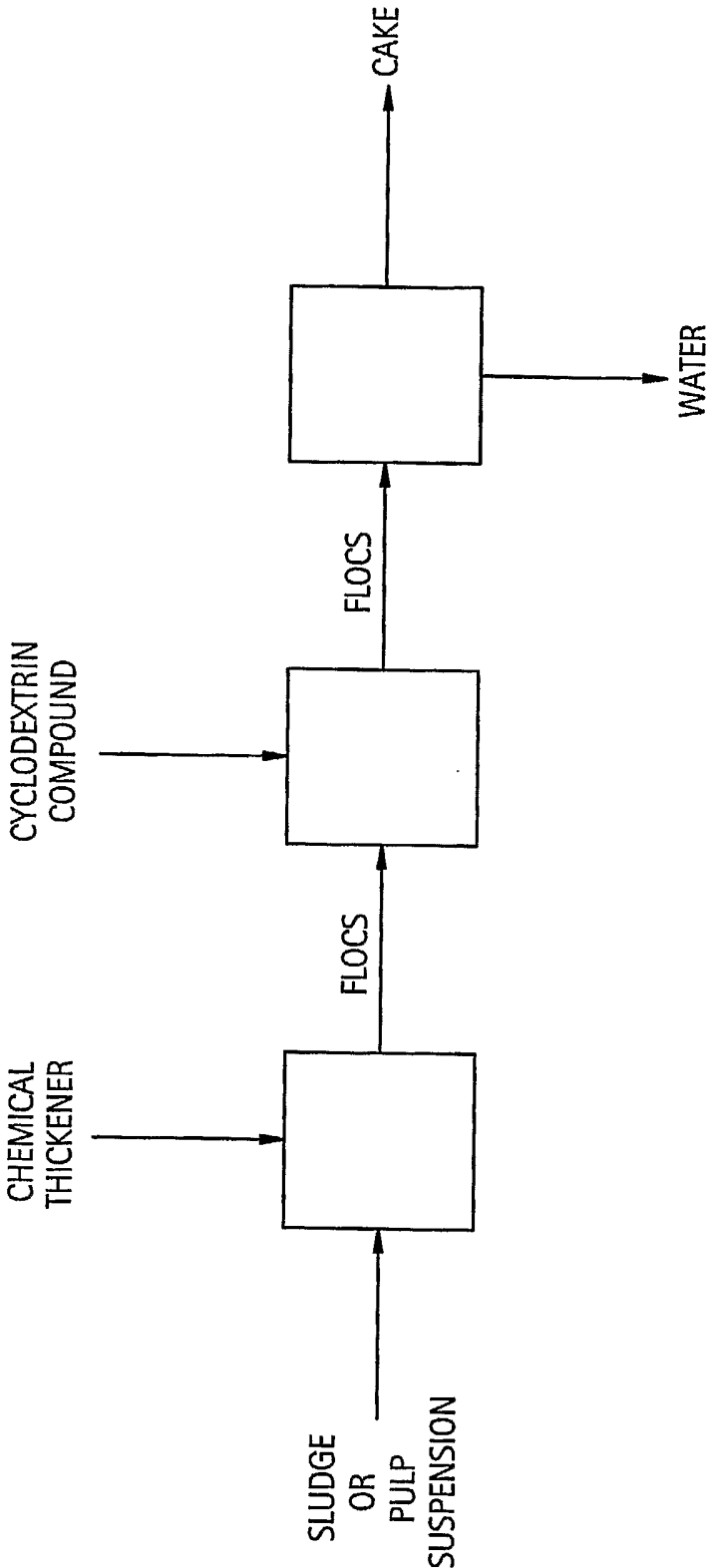


FIG. 4A



FIG. 4B



FIG. 4C



FIG. 4D



FIG. 4E



INTERNATIONAL SEARCH REPORT

International application No.

PCT/US06/05168

A. CLASSIFICATION OF SUBJECT MATTER

IPC: C02F 1/56(2006.01)

USPC: 210/727

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 210/727, 725, 728, 730, 734, 928

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched
None

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)
None

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US 5,846,433 A (SORENSEN et al.) 08 December 1998, col. 2 line 41 through col. 3 line 22, and col. 6 line 37 through col. 8 line 17	1-18
Y	US 3,453,257 A (PARMETER et al.) 01 July 1969, col. 8 lines 31-52	1-18
A	US 4,724,045 A (ACKEL) 09 February 1988	



Further documents are listed in the continuation of Box C.



See patent family annex.

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29 May 2006 (29.05.2006)

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