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(54) **Stabilised imide graft of ethylene copolymeric additives for lubricants, process for their preparation, process for stabilising additive concentrates for lubricants based on the imide graft ethylene copolymer and lubricating oil compositions comprising the stabilised additive.**

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Stabilised imide graft of ethylene copolymeric additives for lubricants, process for their preparation, process for stabilising additive concentrates for lubricants based on the imide graft ethylene copolymer and lubricating oil compositions comprising the stabilised additive

This invention relates to stable polymeric dispersant additives and viscosity-index improvers for lubricating oils. More particularly, this invention relates to viscosity-stable solutions of substantially saturated polymers comprising ethylene and one or more C_3 to C_{28} alpha-olefins, preferably propylene, which have been grafted in the presence of a free radical initiator with an ethylenically-unsaturated dicarboxylic acid material, preferably at an elevated temperature and in an inert atmosphere, and thereafter reacted first with a polyamine, preferably an alkylene polyamine, having at least two primary amino groups, such as diethylene triamine, and then with an anhydride of an organic acid, to form multifunctional polymeric reaction products characterized by viscosity-stabilising activity in mineral oil solutions.

Ashless dispersants for lubricating oil compositions are known to enhance the sludge dispersing ability of said compositions see for example United States Patent 3374174.

One type of dispersant is generally derived from a hydrocarbon-substituted dicarboxylic acid material such as an alkenyl succinic acid or anhydride reacted with a nitrogen-containing material. United Kingdom Patent Specification 1,018,982 discloses the reaction of said alkenyl succinic anhydride with a 2-imidazoline or pyrimidine (the latter is obtained by the reaction of a carboxylic acid, e.g. acetic acid and an alkylene polyamine, e.g. diethylene triamine) to provide a sludge dispersant for lubricating oils. Similarly, U.S. Patent 3,415,750 discloses polyalkenyl succinicimido imidazolines and bis-imidazolines which can be used as said ashless detergents. The imidazoline is first prepared by the sequential reaction of a polyalkylene polyamine with a carboxylic acid or its anhydride, e.g. acetic, which product is thereafter reacted with a polyalkenyl succinic anhydride as is described in Column 3 lines 9 to 15 and in Examples 4 to 6.

U.S. Patent 3,216,936 teaches that it is advantageous to ensure that the reaction product of a mixture of a hydrocarbon-substituted succinic acid, a monocarboxylic acid and an alkylene polyamine does not come from an intermediate reaction product of said monocarboxylic acid and said amine in order to avoid destroying the sludge dispersant activity of the final reaction product. The reactions of this patent being sequential as is shown at column 5 lines 28 to 33.

It is well known that the introduction of carboxylic acid groups onto ethylene copolymers provides a means for derivatizing said copolymers which have viscosity index (V.I.) improving activity when dissolved in mineral oils. One means of introducing the carboxylic groups is by grafting maleic anhydride onto said polymer as by a free radical mechanism.

Belgian Patent 843,360 teaches the production of soluble, sludge-dispersing additives for hydrocarbon fuels and lubricating oils by the free-radical induced grafting in solution of an ethylenically-unsaturated dicarboxylic acid material, such as maleic anhydride, onto a substantially saturated copolymer comprising ethylene and at least one other alpha-olefin at an elevated temperature to provide, without substantial polymer degradation, a useful precursor copolymer which can be subsequently reacted with a carboxylic acid reacting polyfunctional material, such as a polyamine or a hydroxyamine or mixtures of these, to form multifunctional polymeric imidated derivatives having particular utility as engine sludge and varnish control additives for lubricating oils.

It is often found that during the storage of oil solutions of these various imidated grafted hydrocarbon polymers that the viscosity of the solution is increased. The source of this increase appears to be at least in part the chain extension of the polymer.

It has now been discovered that the reaction of the imidated products/byproducts of the graft reaction with organic acid anhydrides, e.g. acetic anhydride, results in amide derivatization of any primary amino groups of the imidated ethylene copolymer whereby viscosity stabilizing activity is provided to said copolymers.

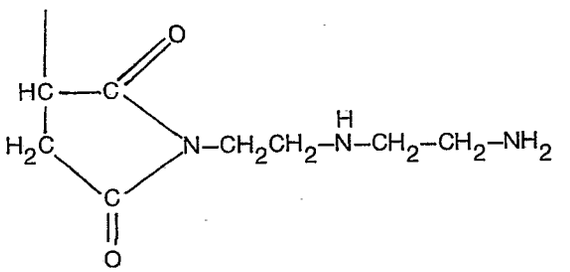
The present invention therefore provides an oil-soluble ethylene polymeric viscosity index improver containing in the range of from 0.001 to 8 wt. % of nitrogen, which improver has been formed by grafting an ethylenically unsaturated dicarboxylic acid or anhydride onto an ethylene copolymer comprising 30 to 80 wt. % ethylene and 20 to 70 wt. % C_3 to C_{28} alpha olefin, reacting said grafted ethylene copolymer with polyamine of 2 to 60 carbons and 2 to 12 nitrogens and having at least two primary amine groups, wherein essentially one of said primary amine groups reacts with an acid moiety of said grafted ethylene copolymer characterised in that said imidization reaction product is then reacted with an anhydride of an organic carboxylic acid having a C_1 to C_{30} hydrocarbyl group to thereby stabilize the resulting ethylene polymeric viscosity index improver and inhibit viscosity increase upon ageing.

The present invention also provides process for improving the viscosity stability of an oil additive concentrate consisting essentially of a hydrocarbon solvent and from .1 to 50 wt. %, based on the total weight of said concentrate, of an imidated grafted ethylene/C_3—C_{28} alpha-olefin copolymeric viscosity index improver containing from 0.001 to 8 wt. % of nitrogen and having a molecular weight ($\overline{M}_n$) of 700 to 500,000 and a $\overline{M}_w/\overline{M}_n$ ratio of less than 7, said viscosity index improver being formed by grafting maleic anhydride onto an ethylene copolymer comprising 30 to 80 wt. % ethylene and 20 to

70 wt. % of said C_3—C_{28} alpha-olefin, followed by reaction of said maleic anhydride moieties with a polyamine of 2 to 60 carbon atoms and 2 to 12 nitrogen atoms and having at least two primary amine groups, wherein at least some of said primary amine groups remain unreacted, said process being characterised by the step of reacting said concentrate with a hydrocarbyl-substituted acid anhydride having from 2 to 30 carbons by adding said acid anhydride in an amount to provide an excess of at least 5% based on the primary amino concentration in said concentrate and maintaining said concentrate at a temperature ranging from 50° to 250°C. and for a period of 0.25 to 8 hours and thereafter removing all unreacted anhydride and byproducts of said reaction while maintaining said concentrate under an inert and water-free environment.

The reaction appears to be an acylation of pendant primary amine groups by their reaction with the organic acid anhydride which can be represented as follows:

Ethylene copolymer chain



Alkylene amino-imide of a grafted ethylene copolymer

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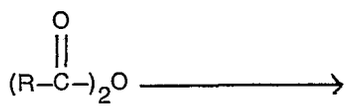
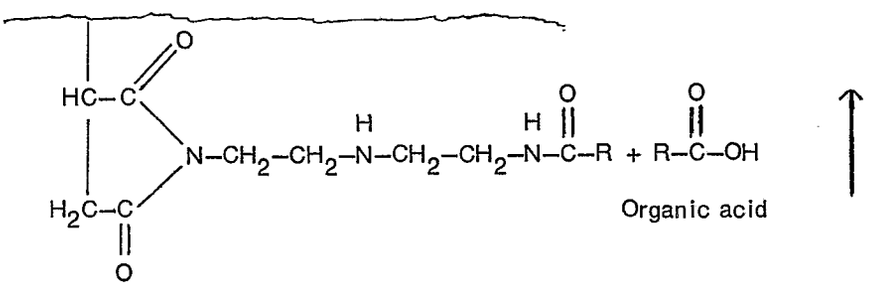


Organic Acid Anhydride



Organic acid

Hydrocarbyl amide of an alkylene imide grafted ethylene copolymer

This acylation of the free primary amino group with the anhydride produces an amide structure which limits the multifunctionalized copolymers property of solution chain extension thereby inhibiting viscosity increase of oil solutions containing the additives of the invention.

To enhance the freedom from haze of the mineral oil solutions, the mineral oil compositions of the invention can be further reacted with an oil-soluble hydrocarbyl substituted acid having from about 10 to 70 carbon atoms having a pK of less than about 2.5, preferably a polymethylene substituted benzene sulfonic acid, said polymethylene substituent having from 18—40, optimally 24 to 32 carbons, in an amount of from about 0.01 wt. % to 8 wt. % at a temperature within the range of about 150°C. to about 200°C. and for a period from about 0.1 hour to about 20 hours, e.g. for 1 hour at 190°C. This further step results in an additive oil composition of improved viscosity stability which has no visually perceptible haze.

The Ethylene Copolymer

The ethylene copolymers to be grafted contain from about 30 to 80 wt. % preferably 38 to 70 wt. % of ethylene, and 20 to 70 wt. % of one or more C_3 to C_{28}, preferably C_3 to C_{18}, more preferably C_3 to C_8, alpha-olefins, e.g. propylene. Such copolymers preferably have a degree of crystallinity of less than 25 wt. %, as determined by X-ray and differential scanning calorimetry, and a number average molecular weight ($\overline{M}_n$) in the range of about 700 to about 500,000, preferably 10,000 to 250,000, as determined by vapor phase osmometry (VPO) or membrane osmometry. Copolymers of ethylene and

propylene are most preferred. Other alpha-olefins suitable in place of propylene to form the copolymer or to be used in combination with ethylene and propylene to form a terpolymer include 1-butene, 1-pentene, 1-hexene, 1-octene; also branched-chain alpha-olefins, such as 5-methylpentene-1 and 6-methylheptene-1 and mixtures thereof.

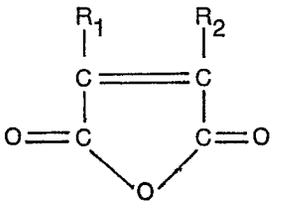
Terpolymers of ethylene, said alpha-olefin and a non-conjugated diolefin or mixtures of such diolefins may also be used. The amount of the non-conjugated diolefin ranges from about 0.5 to 20 mole percent, preferably about 1 to about 7 mole percent, based on the total amount of ethylene and alpha-olefin present. Representative diolefins include cyclopentadiene, 2-methylene-5-norbornene, non-conjugated hexadiene, or any other alicyclic or aliphatic non-conjugated diolefin having from 6 to 15 carbon atoms per molecule, such as 2-methyl or ethyl norbornadiene, 2,4-dimethyl-2-octadiene, 3-(2-methyl-1-propene) cyclopentene, ethylidene norbornene, etc.

These ethylene copolymers, this term including terpolymers, may be prepared using the well-known Ziegler-Natta catalyst compositions as described in U.K. Patent 1,397,994.

Such polymerization may be effected to produce the ethylene copolymers by passing 0.1 to 15, for example, 5 parts of ethylene; 0.05 to 10, for example, 2.5 parts of said higher alpha-olefin, typically propylene; and from 10 to 10,000 parts of hydrogen per million parts of ethylene; into 100 parts of an inert liquid solvent containing (a) from about 0.0017 to 0.017, for example, 0.0086 parts of a transition metal principal catalyst, for example, $VOCl_3$; and (b) from about 0.0084 to 0.084, for example, 0.042 parts of cocatalyst, e.g. $(C_2H_5)_3Al_2Cl_3$; at a temperature of about 25°C. and a pressure of 60 psig for a period of time sufficient to effect optimum conversion, for example, 15 minutes to one-half hour; all parts being parts by weight.

Ethylenically Unsaturated Carboxylic Acid Materials

These materials which are grafted (attached) onto the copolymer contain at least one ethylenic bond and two, carboxylic acid groups or the anhydride or a polar group which is convertible into said carboxyl groups by oxidation or hydrolysis. Maleic anhydride or a derivative thereof is preferred as it does not appear to homopolymerize appreciably but grafts onto the ethylene copolymer or terpolymer to give two carboxylic acid functionalities. Such preferred materials have the generic formula



wherein R_1 and R_2 are hydrogen or a halogen. Suitable examples additionally include chloromaleic anhydride, itaconic anhydride, or the corresponding dicarboxylic acids, such as maleic acid or fumaric acid or their monoesters.

Grafting of the Polymer

The free-radical induced grafting of ethylenically unsaturated carboxylic acid materials in solvents, such as benzene, is known in the art (see U.S. Patent 3,236,917). The grafting according to the process of this invention is carried out at an elevated temperature in the range of 100°C. to 250°C., preferably 120 to 190°C., and more preferably 150 to 180°C., e.g. above 160°C., in a solvent, preferably a mineral lubricating oil solution containing, e.g. 1 to 50, preferably 5 to 30 wt. %, based on the initial total oil solution, of the ethylene polymer and under an inert environment. The grafting is carried out in the presence of a high-temperature decomposable compound capable of supplying free radicals at said elevated temperature.

The free-radical initiators which may be used are peroxides, hydroperoxides, and azo compounds which have a boiling point greater than about 100°C. and decompose thermally within the grafting temperature range to provide said free radicals. Representative of these free-radical initiators are azo-butyronitrile and 2,5-dimethyl-hex-3-yne-2,5 bis-tertiary-butyl peroxide, commercially sold as Lupersol (Registered Trade Mark) 130 or its hexane analogue. The initiator is preferably used at a level of between about 0.005% and about 1%, based on the total weight of the polymer solution.

The ethylenically unsaturated carboxylic acid material, e.g. maleic anhydride, is used in an amount ranging from about 0.01% to about 10%, preferably 0.1 to 2.0%, based on the weight of the initial total oil solution. The aforesaid carboxylic acid material and free radical initiator are used in a weight percent ratio range of 1.0:1 to 30:1, preferably 2.0:1 to 7:1, more preferably 3.0:1 to 6:1.

The grafting is carried out in an inert atmosphere, such as by nitrogen blanketing. While the grafting can be carried out in the presence of air, the yield of the desired graft polymer is decreased as compared to grafting under an inert atmosphere. The inert environment should be substantially free of oxygen. The grafting time is generally from about 0.1 to 12 hours, preferably from about 0.5 to 6 hours,

more preferably 0.5 to 3 hours. The graft reaction is carried out to at least approximately 4 times, preferably at least about 6 times the half-life of the free-radical initiator at the reaction temperature employed, e.g. with 2,5-dimethyl hex-3-yne-2,5-bis(t-butyl peroxide) 2 hours at 160°C. and one hour at 170°C.

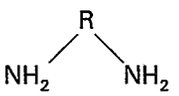
In the grafting process, the copolymer solution is first heated to grafting temperature and thereafter said carboxylic acid material and initiator are added with agitation although they could have been added prior to heating. When the reaction is complete, any excess acid material may be eliminated by an inert gas purge, e.g. nitrogen sparging.

In the grafting step, the maleic anhydride or other carboxylic acid material used is grafted onto both the polymer and the solvent for the reaction. The wt. % grafted onto the polymer is normally greater than the amount grafted onto the oil due to greater reactivity of the polymer to grafting. However, the exact split between the two materials depends upon the polymer and its reactivity, the reactivity and type of oil, and also the concentration of the polymer in the oil. The split can be measured empirically from the infrared analyses of product dialyzed into oil and polymer fractions and measuring the anhydride peak absorbance in each.

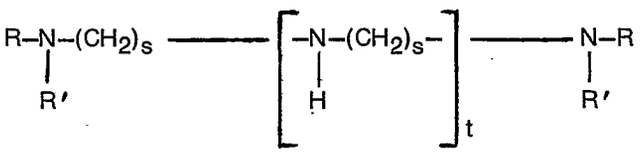
The grafting is preferably carried out in a mineral lubricating oil which need not be removed after the grafting step but can be used as the solvent in the subsequent reaction of the graft polymer with the polyfunctional material and as a solvent for the end product to form the concentrate.

Polyamines

Useful polyamines for reaction with the grafted ethylene-containing polymers are those which have at least two primary amino groups, hereafter designated poly(primary amines), i.e. one group to react with the dicarboxylic acid moiety to form the imido linkage and one more group to react with the organic acid anhydride whereby an amide is formed. Such poly(primary amines) can be represented by the formula



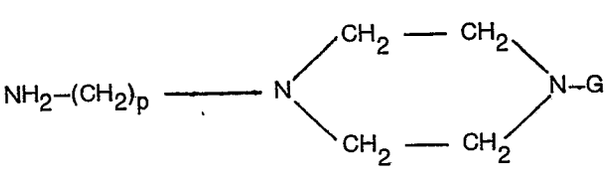
wherein R represents an alkylene group, an alkylene imino group, a hydrocarbyl group, a saturated ring structure, an unsaturated ring structure or a nitrogen containing heterocyclic ring structure. The useful poly(primary amines) include poly(primary amines) of about 2 to 60, e.g. 3 to 20, total carbon atoms and about 2 to 12, e.g. 2 to 6 nitrogen atoms in the molecule, which amines may be hydrocarbyl poly(primary amines) or may be hydrocarbyl poly(primary amines) including other groups, e.g., cyano groups, amide groups, imidazoline groups, and the like. Preferred amines are aliphatic saturated poly(primary amines), including those of the general formula:



wherein R and R′ are independently selected from hydrogen, amino alkylene radicals, and C_1 to C_{12} alkylamino C_2 to C_6 alkylene radicals, s is a number of from 2 to 6, preferably 2 to 4, and t is a number of from 0 to 10, preferably 2 to 6.

Examples of suitable amine compounds include ethylene diamine, diaminomethane, 1,3-diaminopropane, 1,4-diaminobutane, 1,6-diaminohexane, diethylene triamine, triethylene tetraamine, tetraethylene pentamine, 1,2-propylene diamine, di-(1,2-propylene) triamine, di-(1,3-propylene) triamine, di-(1,4-butylene) triamine and N,N-di-(2-aminoethyl) ethylene diamine.

Other useful amine compounds include alicyclic diamines such as 1,4-di-(aminoethyl) cyclohexane and heterocyclic nitrogen compounds, such as N-amino-alkyl piperazines of the general formula:



wherein G is an omega-aminoalkylene radical of from 1 to 3 carbon atoms and p is an integer of from 1 to 4. An example of such an amine is N,N′-di-(2-aminomethyl) piperazine.

Commercial mixtures of amine compounds may advantageously be used. For example, one process for preparing alkylene amines involves the reaction of an alkylene dihalide (such as ethylene dichloride or propylene dichloride) with ammonia, which results in a complex mixture of alkylene groups, forming such compounds as diethylene triamine, triethylenetetramine, tetraethylene pentamine and isomeric piperazines. Low cost poly(ethylene amines) compounds having a composition approximating tetraethylene pentamine are available commercially under the trade name Polyamine 400. Still other polyamines separated by hetero atom chains such as polyethers or sulfides can be used.

Multifunctionalization (Imidization) Process

The grafted polymer, preferably in solution, can be readily reacted with said poly(primary amine) and mixtures thereof by admixture together and heating at a temperature of from about 100°C. to 250°C. for from 10 minutes to 30 hours, preferably 10 minutes to 10 hours, usually about 15 minutes to about 3 hours. It is preferred to use 0.01 to 2.5 mole, more preferably 0.5 to 1.0 mole, of the poly-(primary amine) per mole of grafted carboxylic material, such as maleic anhydride. The reaction of diethylene triamine with the grafted ethylene-containing polymer occurs in 15 minutes or less at 170°C. with a nitrogen blanket.

The solution grafting step is carried out in the presence of a high temperature decomposable peroxide and is accomplished without significant degradation of the chain length (molecular weight) of the ethylene-containing polymer. Measurement of molecular weights and degradation can be evaluated by determination of the thickening efficiency of the polymer.

Thickening efficiency (T.E.) is defined as the ratio of the weight percent of a polyisobutylene (sold as an oil solution by Exxon Chemical Co. as Paratone (Registered Trade Mark) N), having a Staudinger Molecular Weight of 20,000, required to thicken a solvent-extracted neutral mineral lubricating oil, having a viscosity of 150 SUS at 37.8°C., a viscosity index of 105 and an ASTM pour point of 0°F., (Solvent 150 Neutral) a viscosity of 12.4 centistokes at 98.9°C., to the weight percent of a test copolymer required to thicken the same oil to the same viscosity at the same temperature. T.E. is related to ($\bar{M}_n$) and is a convenient, useful measurement for the formulation of lubricating oils of various grades.

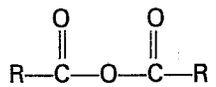
The oil having attached grafted carboxyl, e.g. maleic anhydride, groups when reacted with the polyfunctional derivatives, e.g. polyamine, is also converted to the corresponding derivatives.

The imidization reaction product contains in the range of 0.001 to 8, preferably 0.01 to 2, wt. % nitrogen and preferably has a $\bar{M}_n$ in the range of 700 to 500,000, preferably 700 to 250,000.

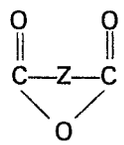
Amide Reaction

The imidization reaction product is readily reacted with the organic acid anhydride to achieve imidation of the imidized grafted ethylene copolymer.

Suitable organic acid anhydrides include anhydrides of monocarboxylic and dicarboxylic acids represented by the structure



and



wherein Z is selected from alkylene, arylene and alkenylene and contains from 2 to 10 carbon atoms.

For the anhydrides of the monocarboxylic acids, the anhydrides of the following aliphatic mono-carboxylic acids are representative.

(i) Where R is an alkyl or substituted alkyl radical, i.e. acetic acid, fluoroacetic acid, propionic acid, beta-chloropropionic acid, butyric acid, isobutyric acid, nitroisobutyric acid, valeric acid, isovaleric acid, hexanoic acid, heptanoic acid, 2 ethylhexanoic acid, nonanoic acid, decanoic acid, dodecanoic acid, undecanoic acid, tetradecanoic acid, hexadecanoic acid, heptadecanoic acid, octadecanoic acid, eicosanoic acid, docosanic acid and triacontanoic acid.

(ii) Where R is an alkenyl or substituted alkenyl radical, i.e. butenic acid, pentenic acid, hexenic acid, teracrylic acid, hypogeic acid, oleic acid, elaidic acid, linoleic acid, alpha-eleosteraric acid, beta-eleostearic acid, alpha-linoleic acid, acrylic acid, beta-chloroacrylic acid, methacrylic acid, crotonic acid, isocrotonic acid, 3-butenoic acid, angelic acid, senecioic acid, hydrosorbic acid, sorbic acid and 4-tetradecenoic acid.

For the anhydrides of the dicarboxylic acids the anhydrides of the following acids are representative.

(a) Aliphatic dicarboxylic acids.

(i) Where Z is an alkylene radical, e.g. succinic acid and glutaric acid.

(ii) Where Z is an alkenylene radical, i.e. maleic acid, fumaric acid, glutaconic acid, citraconic acid and itaconic acid.

The amidation of the imide grafted ethylene copolymer, which imidization reaction was preferentially carried out in a mineral oil solution, can be preferentially conducted as a continuation of the imidization reaction by subsequently injecting the organic acid anhydride directly into the system. If desired, amidation can be a separate non-integrated reaction step. When the reaction is in an oil solution a sufficient amount of the organic acid anhydride is introduced into the heated solution containing the imidized grafted ethylene copolymer and the reaction carried on for a period of 0.25 to 8 hours at a temperature ranging from 50 to 250°C., a temperature of about 100 to 200°C. being preferred. In order to fully complete the reaction, it is useful to utilize a slight excess, i.e. 1 to 30, more usually about 1 to 10, percent by weight of the injected anhydride. The entire reaction is carried out under an inert atmosphere, for example, a nitrogen blanket and the organic acid byproduct removed from the system by sparging or other means in order to complete the reaction. With a low boiling acid, e.g. acetic acid, this is accomplished by nitrogen sparging.

The amidation process step is preferentially conducted on an imidized graft ethylene copolymeric mineral oil solution wherein the excess poly(primary amine) e.g. alkylene polyamine is reduced to a level of less than about 0.05, optimally less than about 0.02, weight percent free (unreacted) amine.

The amidation reaction can be monitored by differential infrared analysis of the reaction medium. Differential infrared analysis involves absorption comparison of a sample of the starting material placed in the reference beam with a test sample placed in the sample beam using matched cells. It has been found that amidation results in the development of maximum absorption at an amide band of 1650—1670 cm^{-1} whereas the acid absorption band of between 1720 and 1740 cm^{-1} first increases and then decreases as the reaction is completed since the excess anhydride and acid byproducts responsible for acid absorption are depleted through removal. The best method of monitoring completion of the amidation of the imide grafted ethylene copolymer is to continue the reaction until absorption at the 1650—1670 cm^{-1} band is at a maximum.

Illustrative of such differential I.R. monitoring of the reaction is the following Table I which shows the varying levels of absorption for the amide and acid bands during amidation with acetic acid anhydride.

TABLE I

	Absorbance	
Reaction Time (Min.)	Amide Peak 1650 cm^{-1}	Acid Peak 1720 cm^{-1}
0	0	0
15	.078	.10
30	.143	.162
60	.189	.170
120*	.181	.237
180	.176	0
240	.164	0

*reaction at ~120°C. believed completed and sparging with nitrogen initiated.

Haze-Treating Step

The mineral oil additive composition containing the ethylene copolymer dispersant additives usually contain from about .1 to about 50 wt.% based upon the total weight of the hydrocarbon solution of the amidated-imidated, grafted ethylene copolymer additive. In some instances, these oil additive compositions are found to be hazy because they contain a hazing material derived from homopolymerization of the grafted moieties and/or low molecular weight polar species insoluble in oil. It is therefore useful to treat the composition by adding at least a haze-removing amount of an oil-soluble acid having a pK of less than about 2.5, e.g. a dialkylbenzene sulfonic acid.

It has been found useful to carry out the haze removing process by treating said copolymer containing oil composition with said organic acid in an amount within the range of from about 0.1 to

about 2.5 molar equivalents of oil-soluble organic acid per molar equivalent of haze material. Preferably said acid is added in an amount of 1 equivalent per equivalent of haze material. A molar equivalent of haze material is measured by reference to the total molar amount of polyfunctional material which reacts with said grafted copolymer, e.g. one mole of said material equals one molar equivalent of haze material.

The treatment of the haze-containing oil composition is carried out at a temperature of about room temperature to about 250°C., preferably from about 150 to about 200°C. and for a time period of about 0.1 hour up to about 20 hours, preferably from 0.5 to about 3 hours. The oil-soluble acid preferably has a pK of from about 0.001 to about 2.5, optimally from about 0.1 to about 2. The term pK or the purpose of this disclosure is used herein to express the extent of the dissociation of the acid used to treat the haze causing substance. Thus, pK can be defined as the negative logarithm of the base 10 of the equilibrium constant for the dissociation of the oil-soluble strong acid.

Useful acids which eliminate the hazing property of the hazing substance are represented by oil-soluble derivatives of alkyl carboxylic acids, such as isostearic acid, maleic acid, malonic acid, phosphoric acid, thiophosphoric acids, phosphonic acid, thiophosphonic acids, phosphinic acid, thiophosphinic acids, sulfonic acid, sulfuric acid, sulfinic acid and alpha-substituted halo- or nitro- or nitrilo-carboxylic acids wherein the oil solubilizing group or groups are hydrocarbyl and containing from about 3 to about 70, preferably from about 18 to 40, optimally 25 to 32 carbon atoms.

Particularly preferred for use in this invention for treating the hazing substance are the oil-soluble sulfonic acids which are typically alkarly sulfonic acids. These alkylaryl sulfonic acids generally have from 9 to 76, preferably 24 to 46, total carbons. The alkyl substituent or substituents preferably have 18 to 40, optimally 24 to 32, total carbons.

Especially preferred alkyl mono-aryl sulfonic acids are those acids that are formed by alkylating benzene with oligomers of propylene or C_4—C_{10} 1-alkenes containing 20 to 40 carbon atoms and thereafter sulfonating the resulting alkylate. The class of compounds may thus be identified as the polyalkyl benzene sulfonic acids. An especially preferred compound is the octacosyl benzene sulfonic acid wherein the alkyl radical is derived from a nominal 28 carbon propylene oligomer.

A wide range, e.g. 0.001 to 50 wt. %, preferably 0.005 to 20%, of the oil-soluble nitrogen containing graft polymers treated in accordance with this invention can be incorporated into about a major amount of an oleaginous material, such as a lubricating oil or hydrocarbon fuel. When used in lubricating oil compositions e.g. automotive or diesel crankcase lubricating oil, the treated polymer concentrations are within the range of about 0.01 to 20 wt. % e.g., 0.1 to 15.0 wt. %, preferably 0.25 to 10.0 wt.%, of the total composition. The lubrications oils to which the products of this invention can be added include not only hydrocarbon oil derived from petroleum, but also include synthetic lubricating oils such as esters of dibasic acids and complex esters made by esterification of monobasic acids, polyglycols, dibasic acids and alcohols.

The amidated-imidated graft polymers of the invention may be utilized in a concentrate form, e.g., from about 10 wt. % to about 50 wt. %, preferably 15 to 49 wt. % in oil, e.g., mineral lubrications oil, for ease of handling.

The above concentrates and lubricating oil compositions may contain other conventional additives, such as dyes, pour point depressants, antiwear agents, antioxidants, other viscosity-index improvers, dispersants and the like.

In the following examples, as elsewhere in this specification, all parts are by weight unless specifically indicated otherwise; all nitrogen analyses were determined by the Kjeldahl Method.

Example 1

Preparation of imide graft ethylene copolymers

5314 kilograms of a 20.2 wt. % solution of an ethylene-propylene copolymer concentrate (made by the Zeigler-Natta process using H_2 moderated $VOCl_3$/aluminum sesquichloride catalyst having a crystallinity less than 25%; containing about 45 wt. % ethylene and 55 wt. % propylene; and having a T.E. of 1.4 (Π_n = 27,000) in SI3ON (Solven 130 Neutral Mineral Oil) was heated to 121°C (250°F) under N_2 sparge and stirring, taking 1 hour and 5 min. Under N_2 blanket 31 kilograms of maleic anhydride were added over 10 minutes. The solution was heated to 154°C (310°F) during a period of 2 hours and 15 minutes; 6 kilograms of Lupersol 130 (2,5-dimethyl hex-3-yne-2,5-bis-tertiary butyl peroxide) was added in three equal charges over a 2 hour and 50 min. period. Excess maleic anhydride was stripped out with N_2 over 2 hours and 20 minutes. 20 kg of diethylene triamine (DETA) was charged and allowed to react for 1.5 hrs. Excess DETA was stripped with vacuum and N_2 for 6 hours. The resulting material was diluted with S130N to 14 wt. % polymer and cooled. The final material had about 0.262 wt. % DETA incorporated.

Example 2

Preparation of acylamidate of maleimide graft of ethylene copolymer

2528 grams (0.065 moles of DETA) of the product of Example 1 was heated to 120°C. under a nitrogen sparge. To this heated soution, 16.9 grams (0.699 wt. %, 0.166 moles, an excess) of acetic anhydride was slowly added over a period of 30 minutes with stirring. The mixture is allowed to soak at

a temperature of about 120°C. under the nitrogen blanket for 1.5 hours after which the reaction byproducts including the acetic anhydride were sparged off for two hours at a temperature of 120°C. with nitrogen. The resulting product shows under differential I.R. a substantial absorption peak at 1650 cm^{-1} and a lack of acetic acid, since there is substantially no absorption at 1720 cm^{-1}. The resulting copolymer solution had a color of 5 with a haze reading of 108 nephelos (unchanged from the starting material), as measured on a naphelometer purchased from Kohlmann Industries, Maywood, Ill and identified as Model 9. This material had a viscosity of 1543 centistokes (1543 x 10^{-6} m^2—S^{-1}) at 99°C (210°F), active ingredient of 15.42 wt. % by dialysis, N wt. % of 0.12% (0.49 wt. % N on polymer), flash point of 420°F. and T.E. of 1.43. On blends with a test oil of 6.2 cs, 9.5 wt. % gave a 12.8 cs. 99°C (210°F) viscosity, 13% sonic shear breakdown, a pour point (with 0.4 wt. % of a vinyl acetate/fumerate pour depressant) of less than —35°C., and a —18°C (0°F) viscosity of 2.53 Pa.s. (25.3 poise) in a Cold Cranking Simulator (ASTM) method.

Example 3

68.1 Kg of 20% by weight of 1.4 T.E. ethylene-propylene rubber in S130N were added to a 200 liter kettle. Under N_2 blanket this was heated to 121°C. It was sparged for 1 hour. 0,413 Kg of maleic anhydride were added and the solution heated to 154°C. under N_2 blanket. Then 0.086 Kg of Lupersol 130 was added over 1-1/2 hours in 3 equal amounts. The reaction continued 30 minutes. The mixture was then N_2 stripped to eliminate free maleic anhydride for 1-1/2 hours. Then 0.27 Kg of DETA were added and reacted for 1 hour. The solution was stripped for 1 hour with N_2 and 84 kilopascals of vacuum. 0.34 Kg of acetic anhydride were charged, reacted for 1 hour and the mixture stripped for 3 hours with N_2 and vacuum. The material was then diluted to 14 wt.% with S130N. The final product had the following characteristics:

99°C. Visc.	1032 cs. (1032 x $10^{-6}m^2S^{-1}$
T.E.	1.49
Haze, nephelos	99
Color, ASTM	5
N, wt. %, concentrate	.125
N wt. %, polymer	.39
6 week at 82°C. Storage Stability increase in 99°C. Visc. in %/Hr.	.004

Example 4

300 grams of Example 1 product was charged into a 4-necked 1 liter flask and heated to 125°C. while stirring and N_2 blanketing. 1 gram of acetic anhydride was added and reacted for 1 hour. The mixture was stripped for 1 hour at 125°C. The temperature was then raised to 170°C. and 3 grams of C_{24} ave. alkylbenzene sulfonic acid were added. Reaction continued for 4 hours. The haze was reduced from 108 (initial) to 16 nephelos.

Example 5

Acetic acid salt of maleimide of graft ethylene copolymer

3000 grams (.077 moles of DETA) of the product of Example 1 were charged to a flask and heated to 118°C. with N_2 sparge. 10 grams (0.167 moles, an excess) of glacial acetic acid were injected. The resulting admixture was reacted at 118°C. with stirring and under a nitrogen blanket and maintained at 118°C. for about 1 hour. The solution was then heated to 155°C. and maintained there for 2 hours with nitrogen blanket. The mixture was then sparged at 155°C. for two hours. The differential IR showed presence of acetic acid during reaction, which was almost completely lost after sparging. Storage stability tests showed no improvement in stability over the starting material. Thus, there is no significant amidation when the acid itself is used rather than the anhydride. Literature information indicates that excessive heat and pressure (if the acid is volatile) is necessary to convert the acid salt to the amide.

Example 6

Acid anhydrides are known not to react with tertiary amines. However, they may react with secondary amines. From the stoichiometry of the reaction of acetic anhydride with an imide made from DETA, as derived from their amide measurements, only the primary amine, not the secondary amine, reacts in this case.

Example 7

The utility of the inventive additives were measured by subjecting the products of Examples 1 and 2 to a standard engine test of blended formulations containing these additives. A 15W50 SAE crankcase oil formulation was made up using 12.5 wt. % of the oil concentrate of Example 2, 2 volume % of the ashless dispersant additive, 1.1 volume % of an overbased magnesium sulfonate, 0.8 volume % of overbased calcium phenate, 0.5 volume % of an antioxidant, and 1.43 volume % of a zinc dialkyldithiophosphate and a mineral lubricating oil blend of base stocks. For comparison purposes, a formulation was made up in the same manner replacing the oil concentrate of Example 2 with the same weight percent of the oil concentrate of Example 1. The above formulations were tested in the Sequence V—C Engine Test, which is described in "Multicylinder Test Sequences for Evaluating Automotive Engine Oils," ASTM Special Technical Publication 315F, page 133ff (1973). The V—C Test evaluates the ability of an oil to keep sludge in suspension and prevent the deposition of varnish deposits on pistons, valves, and other engine parts. The test results given below show that the two blends are not statistically different in performance.

TABLE II

	MS—VC Test Results		
	Sludge	Piston Skirt Varnish	Total Varnish
Oil with product of Ex. 2	9.28	7.86	8.27
Oil with product of Ex. 1	9.31	7.98	7.99
Passing Criteria for Test	8.5	7.9	8.0

In the above tests, the ratings are on a scale of 0 to 10, with 0 being an excessive amount of sludge and varnish while 10 being a completely clean engine.

Example 8

In order to show the surprising viscosity stability provided to the maleimide amide graft products of ethylene copolymeric V.I. improvers provided according to the teachings of this invention, the resulting products Examples 1, 2 and 5 were subjected to a test whereby the change in viscosity of the products were measured over a period of two hours while maintaining the solutions at 99°C. The results are as follows in Table III.

TABLE III

Test*	Product of Example	Initial Viscosity at 99°C	Viscosity After 2 Hrs. at 99°C	Viscosity Increase % Hr.
1	1	($1543 \times 10^{-6} m^2 m^{-1}$) (1543 cs.)	($1547 \times 10^{-6} m^2 s^{-1}$) (1547 cs.)	0.13
2	1	($1224 \times 10^{-6} m^2 s^{-1}$) (1224 cs.)	($1251 \times 10^{-6} m^2 s^{-1}$) (1251 cs.)	1.10
3	5	($1273 \times 10^{-6} m^2 s^{-1}$) (1273 cs.)	($1368 \times 10^{-6} m^2 s^{-1}$) (1368 cs.)	1.07

The above results show that there is a surprising enhancement of the viscosity stabilization activity of solutions of polymer in oil when the products of the invention are used. This two-hour test has been found to correlate with the long-term storage stability results when the solutions containing polymer are stored at temperatures of about 82°C (180°F) for periods of up to two months.

Claims

1. An oil-soluble ethylene polymeric viscosity index improver containing in the range of from 0.001 to 8 wt. % of nitrogen, which improver has been formed by grafting an ethylenically unsaturated dicarboxylic acid or anhydride onto an ethylen copolymer comprising 30 to 80 wt. % ethylene and 20 to 70 wt. % C_3 to C_{28} alpha olefin, reacting said grafted ethylene copolymer with polyamine of 2 to 60 carbons and 2 to 12 nitrogens and having at least two primary amine groups, wherein essentially one of said primary amine groups reacts with an acid moiety of said grafted ethylene copolymer,

characterized in that the imidization reaction product is reacted with an anhydride of an organic carboxylic acid having a C_1 to C_{30} hydrocarbyl group to thereby stabilize the resulting ethylene polymeric viscosity index improver and inhibit viscosity increase upon ageing.

2. A viscosity index improver according to claim 1 wherein the ethylene copolymer is an ethylene-propylene copolymer having a number average molecular weight from 700 to 500,000.

3. A process for preparing a polymeric viscosity index improver which comprises solution grafting an ethylenically unsaturated organic dicarboxylic acid material onto a copolymer comprised of 30 to 80 wt. % ethylene and 20 to 70 wt. % of at least one C_3—C_{28} alpha-olefin at a temperature of from 100°C. to 250°C in a solvent under an oxygen free inert atmosphere, in the presence of a high-temperature decomposable free radical initiator being used in an ethylenically unsaturated organic dicarboxylic acid material: free radical initiator weight per cent ratio of 1.0:1 to 30:1, which grated polymer is then derivatised by reaction with an alkylene polyamine having from 2 to 60 carbons and 2 to 12 nitrogen atoms and having at least 2 primary amine groups characterised in that said imidization product is thereafter reacted with from 0.5 to 2.5 moles of an anhydride of an organic carboxylic acid having a C_1 to C_{30} hydrocarbyl group per primary amino group in said product.

4. A process according to claim 3 wherein said copolymer is of ethylene and propylene having from 38 to 70 wt. % of ethylene, said dicarboxylic acid material is maleic acid anhydride, said solution grafting is carried out using a mineral lubricating oil as solvent, said polyamine is diethylene triamine and said 0.5 to 2.5 moles of anhydride is of acetic anhydride.

5. The process according to claims 3 or 4 wherein the resulting solution from said reaction with said 0.5 to 2.5 moles of anhydride is treated with an oil-soluble alkyl aryl sulfonic acid containing from 9 to 76 carbon atoms at a temperature ranging from room temperature to 250°C.

6. The process according to claim 5 wherein said sulfonic acid is C_{24} (average) alkylbenzene sulfonic acid.

7. A lubricating oil composition comprising a major amount of a lubricating oil having dissolved therein at least a viscosity index-improving amount of an oil-soluble ethylene polymeric viscosity index improver according to claim 1.

8. A composition according to claim 7 wherein said viscosity index improver is present in an amount of from 0.5 to 50 wt. %, based upon the total weight of said composition.

9. A composition according to claims 7 or 8 wherein said viscosity index improver is prepared by solution grafting an ethylenically unsaturated dicarboxylic acid material onto a copolymer comprised of 30 to 80 wt. % ethylene and 20 to 70 wt. % of at least one C_3—C_{28} alpha-olefin at a temperature of from 100°C to 250°C., in the presence of a high-temperature decomposable free-radical initiator having a boiling point in excess of 100°C., which grafted polymer is then derivatized by reaction with an alkylene polyamine having from 3 to 20 total carbons and 2 to 6 nitrogen atoms to provide a product having sludge dispersant activity and thereafter reacted with from 0.5 to 2.5 moles of said anhydride per primary amino group in said product.

10. A composition according to claim 9 wherein said copolymer is of ethylene and propylene having from 38 to 70 wt. % of ethylene and is present in said composition in an amount ranging from 0.1 to 15 wt.%, said dicarboxylic acid material is maleic acid anhydride, said solution grafting is carried out using a mineral lubricating oil as solvent, said polyamine is diethylene triamine and said 0.5 to 2.5 moles of anhydride is of acetic anhydride.

11. A composition according to claim 7—10 wherein the resulting solution from said reaction with said 0.5 to 2.5 moles of anhydride is treated with an oil-soluble alkyl aryl sulfonic acid containing from 9 to 76 carbons at a temperature ranging from room temperature to 250°C. to inhibit haze.

12. A composition according to claim 11 wherein said sulfonic acid is C_{24} (average) alkylbenzene sulfonic acid.

13. A process for improving the viscosity stability of an oil additive concentrate consisting essentially of a hydrocarbon solvent and from .1 to 50 wt. %, based on the total weight of said concentrate, of an imidated grafted ethylene/C_3—C_{28} alpha-olefin copolymeric viscosity index improver containing from 0.001 to 8 wt. % of nitrogen and having a molecular weight (M_n) of 700 to 500,000 and a $\overline{M}_w/\overline{M}_n$ ratio of less than 7, said viscosity improver being formed by grafting maleic anhydride onto an ethylene copolymer comprising 30 to 80 wt %. of ethylene and 20 to 70 wt. % of said C_3—C_{28} alpha-olefin, followed by reaction of said maleic anhydride moieties with a polyamine of 2 to 60 carbon atoms and 2 to 12 nitrogen atoms and having at least two primary amine groups, wherein at least some of said primary amine groups remain unreacted, said process being characterised by the step of reacting said concentrate with a hydrocarbyl-substituted organic carboxylic acid anhydride having from 2 to 30 carbons by adding said acid anhydride in an amount to provide an excess of at least 5% based on the primary amino concentration in said concentrate and maintaining said concentrate at a temperature ranging from 50°C to 250°C. and for a period of 0.25 to 8 hours and there-after removing all unreacted anhydride and byproducts of said reaction while maintaining said concentrate under an inert and water-free environment.

14. A process according to claim 13 wherein said concentrate contains less than 0.2 wt. % unreacted alkylene polyamine, said hydrocarbyl-substituted acid anhydride is acetic anhydride and said temperature is maintained until maximum absorption at 1650—1670 cm^{-1} is found by differential

infrared testing to be a maximum and said removing is by nitrogen sparging until said absorption is at a minimum at 1720 cm^{-1}.

15. A process according to claims 13 or 14 wherein there is a further process step of treating said concentrate with an oil-soluble hydrocarbyl substituted strong acid containing a hydrogen dissociating moiety which has a pK of less than 2.5 and containing 3 to 70 carbon atoms at a temperature of from room temperature to 250°C.

16. A process according to claim 15 whereins aid strong acid is a dialkyl substituted benzene sulfonic acid present in an amount ranging from 0.1 to 2.5 molar equivalents per molar equivalent to nitrogen material introduced onto said graft copolymeric viscosity index improver and said treating is at a temperature ranging from 20°C. to 250°C. for a period ranging from 0.1 to 20 hours.

1. Agent polymérique éthylénique soluble dans l'huile, améliorant l'indice de viscosité, contenant une proportion de 0,001 à 8% en poids d'azote, cet agent ayant été formé par greffage d'un acide ou anhydride dicarboxylique à non-saturation éthylénique sur un copolymère d'éthylène comprenant 30 à 80 % en poids d'éthylène et 20 à 70% en poids d'une alpha-oléfine en C_3 à C_{28}, réaction dudit copolymère d'éthylène greffé avec une polyamine de 2 à 60 atomes de carbone et de 2 à 12 atomes d'azote et portant au moins deux groupes amino primaires, dont essentiellement l'un desdits groupes amino primaires réagit avec une portion acide dudit copolymère éthylénique greffé, caractérisé en ce que le produit de la réaction d'imidation est amené à réagir avec un anhydride d'un acide carboxylique organique portant un groupe hydrocarbyle en C_1 à C_{30} pour stabiliser ainsi l'agent polymérique éthylénique résultant améliorant l'indice de viscosité et pour inhiber l'élévation de viscosité lors du vieillissement.

2. Agent améliorant l'indice de viscosité suivant la revendication 1, dans lequel le copolymère éthylénique est un copolymère éthlène-propylène ayant une moyenne en nombre du poids moléculaire de 700 à 500 000.

3. Procédé de production d'un agent polymérique améliorant l'indice de viscosité, qui consiste à greffer en solution une matière acide dicarboxylique organique à non-saturation éthylénique sur un copolymère formé de 30 à 80% en poids d'éthylène et de 20 à 70% en poids d'au moins une alpha-oléfine en C_3 à C_{28} à une température de 100 à 250°C dans un solvant sous une atmosphère inerte dépourvue d'oxygène, en présence d'un initiateur de radicaux libres pouvant se décomposer à haute température et étant utilisé dans un rapport de pourcentages en poids de la matière acide dicarboxylique organique à non-saturation éthylénique à l'initiateur de radicaux libres de 1,0:1 à 30:1, ce polymère greffé étant ensuite transformé par réaction avec une alkylènepolyamine ayant 2 à 60 atomes de carbone et 2 à 12 atomes d'azote et ayant au moins deux groupes amino primaires, caractérisé en ce que ledit produit d'imidation est ensuite amené à réagir avec 0,5 à 2,5 moles d'un anhydride d'un acide carboxylique organique ayant un groupe hydrocarbyle en C_1 à C_{30} par groupe amino primaire dans ledit produit.

4. Procédé suivant la revendication 3, dans lequel ledit copolymère est un copolymère d'éthylène et de propylène ayant 38 à 70% en poids d'éthylène, la matière acide dicarboxylique est l'anhydride d'acide maléique, le greffage de la solution est conduit en utilisant comme solvant une huile lubrifiante minérale, la polyamine est la diéthylènetriamine et l'anhydride en proportion de 0,5 à 2,5 moles consiste en anhydride acétique.

5. Procédé suivant les revendications 3 ou 4, dans lequel la solution résultant de ladite réaction avec 0,5 à 2,5 moles d'anhydride est traitée avec un acide alkylarylsulfonique soluble dans l'huile contenant 9 à 76 atomes de carbone à une température allant de la température ambiante à 250°C.

6. Procédé suivant la revendication 5, dans lequel l'acide sulfonique est un acide (alkyle en C_{24} en moyenne)-benzènesulfonique.

7. Compositon d'huile lubrifiante, comprenant une quantité dominante d'une huile lubrifiante dans laquelle est dissoute au moins une quantité améliorant l'indice de viscosité d'un agent polymérique éthylénique soluble dans l'huile améliorant l'indice de viscosité suivant la revendication 1.

8. Composition suivant la revendication 7, dans laquelle l'agent améliorant l'indice de viscosité est présent en une quantité de 0,1 à 50% en poids sur la base du poids total de ladite composition.

9. Composition suivant les revendications 7 ou 8, dans laquelle l'agent améliorant l'indice de viscosité est préparé par greffage en solution d'une matière acide dicarboxylique à non-saturation éthylénique sur un copolymère formé de 30 à 80% en poids d'éthylène et de 20 à 70% en poids d'au moins une alpha-oléfine en C_3 à C_{28} à une température de 100 à 250°C, en présence d'un initiateur de radicaux libres décomposable à haute température ayant un point d'ébullition de plus de 100°C, ledit polymère greffé est ensuite transformé par réaction avec une alkylènepolyamine ayant 3 à 20 atomes de carbone et 2 à 6 atomes d'azote et un produit ayant une activité de dispersion de la boue, puis amené à réagir avec 0,5 à 2,5 moles dudit anhydride par groupe amino primaire dudit produit.

10. Composition suivant la revendication 9, dans laquelle ledit copolymère est un copolymère d'éthylène et de propylène ayant 38 à 70% en poids d'éthylène et est présent dans ladite composition en une quantité allant de 0,1 à 15% en poids, ladite matière acide dicarboxylique est l'anhydride d'acide maléique, ledit greffage en solution est conduit en utilisant comme solvant une huile lubrifiante minérale, ladite polyamine est la diéthylène-triamine et ledit anhydride en proportion de 0,5 à 2,5 moles est l'anhydride acétique.

11. Composition suivant les revendications 7 à 10, dans laquelle la solution résultante de ladite réaction avec lesdites 0,5 à 2,5 moles d'anhydride est traitée avec un acide alkylarylsulfonique soluble dans l'huile contenant 9 à 76 atomes de carbone à une température allant de la température ambiante à 250°C pour inhiber le développement d'un trouble.

12. Composition suivant la revendication 11, dans laquelle ledit acide sulfonique est un acide (alkyle en C_{24} en moyenne)-benzènesulfonique.

13. Procédé pour améliorer la stabilité de la viscosité d'un concentré d'additifs pour huile principalement formé d'un solvant hydrocarboné et de 0,1 à 50% en poids, sur la base du poids total dudit concentré, d'un agent améliorant l'indice de viscosité, copolymère d'éthylène et d'une alpha-oléfine en C_3 à C_{28} greffé avec un imide, contenant 0,001 à 8% en poids d'azote et ayant un poids moléculaire ($\overline{M}_n$) de 700 à 500 000 et un rapport $\overline{M}_p/\overline{M}_n$ inférieur à 7, ledit agent améliorant l'indice de viscosité étant formé par greffage d'anhydride maléique sur un copolymère d'éthylène comprenant 30 à 80% en poids d'éthylène et 20 à 70% en poids de ladite alpha-oléfine en C_3 à C_{28}, suivi de la réaction desdites portions d'anhydride maléique avec une polyamine de 2 à 60 atomes de carbone et de 2 à 12 atomes d'azote et portant au moins deux groupes amino primaires, au moins certains des groupes amino primaires restant intacts, ledit procédé étant caractérisé par l'étape de réaction dudit concentré avec un anhydride d'acide carboxylique organique à substituant hydrocarbyle ayant 2 à 30 atomes de carbone par addition dudit anhydride d'acide en une quantité apportant un excès d'au moins 5% sur la base de la concentration en groupes amino primaires dans ledit concentré et maintien dudit concentré à une température allant de 50 à 250°C et pendant une période de 0,25 à 8 heures, puis élimination de la totalité de l'anhydride n'ayant pas réagi et des sous-produits de la réaction tout en maintenant ledit concentré dans un milieu inerte et anhydre.

14. Procédé suivant la revendication 13, dans lequel ledit concentré contient moins de 0,02% en poids d'alkylènepolyamine n'ayant pas réagi, ledit anhydride d'acide à substituant hydrocarbyle est l'anhydride acétique et ladite température est maintenue jusqu'à ce qu'une absorption maximale à 1650—1670 cm^{-1} soit trouvée égale à un maximum par l'analyse infrarouge différentielle, et ladite élimination est effectuée par passage d'un courant d'azote jusqu'à ce que l'absorption soit minimale à 1720 cm^{-1}.

15. Procédé suivant les revendications 13 ou 14 dans lequel il y a en outre une étape de traitement dudit concentré avec un acide fort, à substituant hydrocarbyle, soluble dans l'huile, contenant un groupement se dissociant en hydrogène qui a un pK inférieur à 2,5 et qui contient 3 à 70 atomes de carbone, à une température allant de la température ambiante à 250°C.

16. Procédé suivant la revendication 15, dans lequel ledit acide fort est un acide benzènesulfonique dialkylé présent en une quantité allant de 0,1 à 2,5 équivalents molaires par équivalent molaire de matière azotée introduite sur le copolymère greffé améliorant l'indice de viscosité et ledit traitement est conduit à une température allant de 20 à 250°C pendant une période allant de 0,1 à 20 heures.

Patentansprüche

1. Öllösliches, Ethylen enthaltendes, polymeres Viskositätsindexverbesserungsmittel mit einem Stickstoffgehalt von 0,001 bis 8 Gew.%, das durch Aufpropfen einer ethylenisch ungesättigten Dicarbonsäure oder -anhydrid auf ein 30 bis 80 Gew.% Ethylen und 20 bis 70 Gew.% C_3—C_{28}-α-Olefin enthaltendes Ethylencopolymers und durch Umsetzen des gepropften Ethylencopolymers mit 2 bis 60 Kohlenstoffatome und 2 bis 12 Stickstoffatome enthaltendem Polyamin, das mindestens 2 primäre Amingruppen aufweist, wobei im wesentlichen eine der primären Amingruppen mit einer Säuregruppe des gepropftem Ethylencopolymers reagiert, dadurch gekennzeichnet, daß das Produkt der Imidbildungsreaktion mit einem Anhydrid einer organischen Carbonsäure mit einer C_1—C_{30}-Hydrocarbylgruppe umgesetzt wird, um dadurch das resultierende Ethylen enthaltende polymere Viskositätsindexverbesserungsmittel zu stabilisieren und ein Viskositätszunahme beim Altern zu vermeiden.

2. Viskositätsindexverbesserungsmittel nach Anspruch 1, dadurch gekennzeichnet, daß das Ethylencopolymer ein Ethylenpropylencopolymer mit einem zahlendurchschnittlichen Molekulargewicht von 700 bis 500000 ist.

3. Verfahren zur Herstellung eines polymeren Viskositätsindexverbesserungsmittels, bei dem ein ethylenisch ungesättigtes organisches Dicarbonsäurematerial durch Lösungspfropfpolymerisation in einem Lösungsmittel unter sauerstoffreier, inerter Atmosphäre bei einer Temperatur von 100 bis 250°C in Gegenwart eines bei hoher Temperatur versetzbaren freiradikalischen Initiators auf ein 30 bis 80 Gew.% Ethylen und 20 bis 70 Gew.% mindestens eines C_3—C_{28}-α-Olefins enthaltendes Copolymer aufgepropft wird, wobei das Gewichtsprozentverhältnis von ethylenisch ungesättigtem organischen Dicarbonsäurematerial zu freiradikalischem Initiator 1,0:1 bis 30:1 beträgt und bei dem das gepfropfte Polymer dann durch Umsetzung mit einem Alkylenpolyamin mit 2 bis 60 Kohlenstoffatomen und 2 bis 12 Stockstoffatomen sowie mindestens zwei primären Amingruppen in ein Derivat überführt wird, dadurch gekennzeichnet, daß das Produkt der Imidbildungsreaktion anschließend mit 0,5 bis 2,5 Mol eines Anhydrids einer organischen Carbonsäure mit einer C_1—C_{30}-Hydrocarbylgruppe je primäre Aminogruppe in dem Produkt umgesetz wird.

4. Verfahren nach Anspruch 3, dadurch gekennzeichnet, daß das Copolymer ein Ethylen/Propylen-Copolymer mit 38 bis 70 Gew.% Ethylen ist, das Dicarbonsäurematerial Maleinsäureanhydrid ist, die Lösungspfropfpolymerisation unter Verwendung eines Mineralschmieröls als Lösungsmittel durchgeführt wird, das Polyamin Diethylentriamin ist und die 0,5 bis 2 Mol Anhydrid Essigsäureanhydrid sind.

5. Verfahren nach Anspruch 3 oder 4, dadurch gekennzeichnet, daß die aus der Reaktion mit den 0,5 bis 2,5 Mol Anhydrid resultierende Lösung mit einer öllöslichen Alkylarylsulfonsäure mit 9 bis 76 Kohlenstoffatomen bei einer Temperatur von Raumtemperatur bis 250°C behandelt wird.

6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, daß die Sulfonsäure C_{24}(Durchschnitt)-Alkylbenzolsulfonsäure ist.

7. Schmierölzusammensetzung gekennzeichnet durch eine überwiegende Menge eines Schmieröls, in dem mindestens eine den Viskositätsindex verbessernde Menge eines öllöslichen, Ethylen enthaltenden, polymeren Viskositätsindexverbesserungsmittels nach Anspruch 1 gelöst ist.

8. Zusammensetzung nach Anspruch 7, dadurch gekennzeichnet, daß das Viskositätsindexverbesserungsmittel in einer Menge von 0,1 bis 50 Gew.%, bezogen auf das Gesamtgewicht der Zusammensetzung vorliegt.

9. Zusammensetzung nach Anspruch 7 oder 8, dadurch gekennzeichnet, daß das Viskositätsindexverbesserungsmittel hergestellt ist, indem ein ethylenisch ungesättigtes Dicarbonsäurematerial durch Lösungspfropfpolymerisation auf ein 30 bis 80 Gew.% Ethylen und 20 bis 70 Gew.% mindestens eines C_3—C_{28}-α-Olefins enthaltendes Copolymer bei einer Temperatur von 100 bis 250°C in Gegenwart eines bei hoher Temperatur zersetzbaren freiradikalischen Initiators mit einem Siedepunkt über 100°C aufgepfropft wird, das gepfropfte Polymer, um ein Produkt mit Schlamm-dispergieraktivität zu liefern, dann durch Umsetzung mit einem Alkylenpolymin mit 3 bis 20 Kohlenstoffatomen und 2 bis 6 Stickstoffatomen in ein Derivat überführt und anschließend mit 0,5 bis 2,5 Mol des Anhydrids je primäre Aminogruppe in dem Produkt umgesetzt wird.

10. Zusammensetzung nach Anspruch 9, dadurch gekennzeichnet, daß das Copolymer ein Ethylen/Propylen-Copolymer mit 38 bis 70 Gew.% Ethylen ist und in der Zusammensetzung in einer Menge von 0,1 bis 15 Gew.% vorliegt, das Dicarbonsäurematerial Maleinsäureanhydrid ist, die Lösungspfropfpolymerisation unter Verwendung eines Mineralschmieröls als Lösungsmittel durchgeführt wird, das Polyamin Diethylentriamin ist und die 0,5 bis 2,5 Mol Anhydrid Essigsäureanhydrid sind.

11. Zusammensetzung nach den Ansprüche 7 bis 10, dadurch gekennzeichnet, daß die aus der Reaktion mit den 0,5 bis 2,5 Mol Anhydrid resultierende Lösung mit einer öllöslichen Alkylarylsulfonsäure mit 9 bis 76 Kohlenstoffatomen bei einer Temperatur von Raumtemperatur bis 250°C behandelt wird, um Trübungen zu vermeiden.

12. Zusammensetzung nach Anspruch 11, dadurch gekennzeichnet, daß die Sulfonsäure C_{24}(Durchschnitt)-Alkylbenzolsulfonsäure ist.

13. Verfahren zur Verbesserung der Viskositätsstabilität eines Öladditivkonzentrates, das im wesentlichen aus einem Kohlenwasserstofflösungsmittel und 0,1 bis 50 Gew.%, bezogen auf das Gesamtgewicht des Konzentrats, eines imidisierten, gepfropften, copolymeren Ethylen/C_3-C_{28}-α-Olefin-Viskositäsindexvervesserungsmittels mit einem Stickstoffgehalt von 0,001 bis 8 Gew.%, einem Molekulargewicht ($\overline{M}n$) von 700 bis 500 000 und einem $\overline{M}_w/\overline{M}_n$-Verhältnis von weniger als 7 besteht, wobei das Viskositätsindexverbesserungsmittel durch Aufpfropfen von Maleinsäureanhydrid auf ein 30 bis 80 Gew.% Ethylen und 20 bis 70 Gew.% C_3-C_{28}-α-Olefin enthaltendes Ethylencopolymer und anschließende Umsetzung der Maleinsäureanhydridgruppen mit einem 2 bis 60 Kohlenstoffatome und 2 bis 12 Stickstoffatome enthaltendem Polyamin mit mindestens 2 primären Amingruppen gebildet ist, wobei mindenstens einige der primären Amingruppen nicht umgesetzt sind, dadurch gekennzeichnet, daß das Konzentrat mit einem hydrocarbylsubstituierten organischen Carbonsäureanhydrid mit 2 bis 30 Kohlenstoffatomen umgesetzt wird, indem das Säureanhydrid in einer solchen Menge zugesetzt wird, daß bezogen auf die Konzentration der primären Aminogruppen in dem Konzentrat ein Überschuß von mindestens 5% vorhanden ist, das Konzentrat über einen Zeitraum von 0,25 bis 8 Stunden auf einer Temperatur von 50 bis 250°C gehalten wird und anschließend alles nicht umgesetztes Anhydrid und Nebenprodukte der Reaktion entfernt werden, wobei das Konzentrat in einer inerten und wasserfreien Umgebung gehalten wird.

14. Verfahren nach Anspruch 13, dadurch gekennzeichnet, daß das Konzentrat weniger als 0,02 Gew.% nicht umgesetztes Alkylenpolyamin enthält, das hydrocarbylsubstituierte Säureanhydrid Essigsäureanhydrid ist, die Temperatur aufrechterhalten wird, bis durch Differentialinfrarotuntersuchung eine maximale Absorption bei 1650—1670 cm^{-1} gefunden wird, und das Entfernen durch Stickstoffspülung erfolgt, bis die Absorption bei 1720 cm^{-1} ein Minimum erreicht.

15. Verfahren nach Anspruch 13 oder 14, dadurch gekennzeichnet, daß das Konzentrat in einem weiteren Verfahrensschritt mit einer öllöslichen hydrocarbylsubstituierten starken Säure, die eine Wasserstoff abdissoziierende Gruppe mit einem Pk-Wert von weniger als 2,5 und 3 bis 70 Kohlenstoffatome enthält, bei einer Temperatur von Raumtemperatur bis 250°C behandelt.

16. Verfahren nach Anspruch 15, dadurch gekennzeichnet, daß die starke Säure eine dialkylsubstituierte Benzolsulfonsäure ist, die in einer Menge von 0,1 bis 2,5 Moläquivalenten je Moläquivalent in das gepfropfte copolymere Viskositätsindexverbesserungsmittel eingebrachtes Stickstoffmaterial vorliegt, und die Behandlung über einen Zeitraum von 0,1 bis 20 Stunden bei einer Temperatur von 20 bis 250°C erfolgt.