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DESCRIPTION

FIELD OF THE INVENTION

[0001] The invention relates to a solar-biomass complementary thermal energy supply system, which belongs to the field of clean energy.

BACKGROUND OF THE INVENTION

[0002] With the dwindling reserves of traditional fossil fuels (coal, oil, natural gas) as well as problems of environmental pollutions caused by the use of fossil energy, which direct threatens human survival and development, to develop a renewable and eco-friendly energy has become a worldwide consensus. Solar energy is characteristic in its wide distribution, unlimited reserves, clean collection and utilization, and zero emission of CO₂.

[0003] As an organic matter produced by the photosynthesis of plants, biomass is characteristics in its wide distribution, large amount of reserves, much cleaner than fossil energy, and zero emission of CO₂. Thus, biomass is a very important renewable energy. Broadly speaking, the biomass energy is also originated from the solar energy, that is, the plant collects the solar energy by photosynthesis of the chlorophyll, which benefits the human beings.

[0004] Solar energy has a wide distribution, limitless reserves, cleanness in collection and utilization, and zero-CO₂ emission. Thus, the solar energy has been concerned by more and more people. However, a large-scale development of the solar power energy has been largely restricted for a long time due to problems such as decentralization of the solar energy, strong dependence on weather, and instability and discontinuity of the thermal concentration.

[0005] Currently, situations of unreasonable energy utilization still happen, which results in great energy waste. For example, electric power plants are constructed to supply electricity for every household. Air conditioners are installed in each household for creating a more comfortable living environment, and the electric power is consumed for the purpose of declining the room temperature and removing the thermal energy into the atmosphere during the summer while raising the room temperature during the winter. Different kinds of hot water heaters (solar energy heating, electric heating, or gas heating) are utilized to provide hot water. And electricity is also consumed for preparing the ice for food preservation. It seems that the electric power is adopted by the existing technical mode, which results in large energy waste.

[0006] Even though hybrid power generation schemes using solar and non-solar energy sources are known, e.g. from US 2005/0279095 A1, the energy waste problem described

before still remains.

[0007] Thus, to find a technical route, the thermal energy of the biomass and the solar energy are combined, and the electric power generation, refrigeration, ice preparation, water heating are integrated and provided to users, so that the respective shortages thereof are offset by one another, and a three-cooperated dynamic center for providing electricity, refrigeration, and heating is established, thereby providing an effective route for solving the problem of energy waste.

SUMMARY OF THE INVENTION

[0008] In view of the above-described problems, it is one objective of the invention to provide a solar-biomass complementary thermal energy supply system that can make full use of the complementarity of biomass energy and solar energy for central cool supply, ice supply and heat supply, so that the clean solar energy and biomass energy can be multi-recycled, thereby maximizing the utilization of energy. The solar-biomass complementary thermal energy supply system can be used in a low carbon industrial park for power generation, cooling and ice generation, and hot water generation.

[0009] To achieve the above objective, in accordance with one embodiment of the invention, there is provided a solar-biomass complementary thermal energy supply system, comprising: a solar concentrating device, a solar storage tank comprising a first heat exchanger and a second heat exchanger, a biomass power station comprising a biomass boiler, a central refrigeration and ice maker, and a central hot water supply tank, wherein the solar concentrating device is connected to the solar storage tank via pipes; an inlet of the first heat exchanger B1 of the solar storage tank is connected to an outlet of a feedwater pump of the biomass boiler; an outlet of the first heat exchanger B1 is connected to an inlet of a water feeding system of the biomass boiler; an inlet pipe of the second heat exchanger B2 of the solar storage tank is connected to an outlet pipe of a water purification plant; an outlet of the second heat exchanger B2 is connected to a thermal energy input pipe of the central refrigeration and ice maker; cooling water in the central refrigeration and ice maker absorbs released thermal energy produced by the central refrigeration and ice maker and converges with hot water from a waste heat collector disposed in a flue of the biomass boiler, and the confluent hot water is transported to the central hot water supply tank.

[0010] In a class of this embodiment, the solar storage tank comprises two media for heat exchange and two cycles; the two media are a heat storage medium and circulating water; the heat storage medium is heat conduction oil or molten salt and is disposed in the solar storage tank; the heat conduction oil or molten salt is driven by a high temperature pump to the solar concentrating device where the heat conduction oil or molten salt is heated by solar energy; the heated heat conduction oil or molten salt returns to the solar storage tank and releases heat energy; part of the heat energy heats the circulating water from the feedwater pump of the biomass boiler via the first heat exchanger B1, and the heated circulating water is

introduced to the biomass boiler; another part of the heat energy heats the circulating water from the water purification plant via the second heat exchanger B2, and the heated circulating water is introduced to the central refrigeration and ice maker.

[0011] In a class of this embodiment, the solar storage tank comprises three media for heat exchange and two cycles; the three media are a heat storage medium, a heat transfer medium, and circulating water; the heat storage medium is molten salt disposed in the solar storage tank; the heat transfer medium is heat conduction oil disposed in a solar heat exchanger A; the heat conduction oil is driven to the solar concentrating device where the heat conduction oil is heated by solar energy; the heated heat conduction oil returns to the solar storage tank and exchanges heat energy with the molten salt via the solar heat exchanger A; part of the heated molten salt heats the circulating water from the feedwater pump of the biomass boiler via the first heat exchanger B1, and the heated circulating water is introduced to the biomass boiler; another part of the heated molten salt heats the circulating water from the water purification plant via the second heat exchanger B2, and the heated circulating water is introduced to the central refrigeration and ice maker.

[0012] In a class of this embodiment, the waste heat collector is disposed in the flue of the biomass boiler, and a hot water output pipe of the waste heat collector is connected to the central hot water supply tank.

[0013] In a class of this embodiment, the central hot water supply tank is connected to the solar storage tank via pipes, valves, and back water pumps.

[0014] In a class of this embodiment, the central refrigeration and ice maker is a lithium-bromide absorption-type refrigerator or an evaporation refrigerator.

[0015] In a class of this embodiment, the heat conduction medium in the solar concentrating device is heat conduction oil or molten salt.

[0016] In a class of this embodiment, the molten salt is a binary nitrate system comprising NaNO_3 and KNO_3 , for example, between 40% and 90 wt. % of NaNO_3 and between 10% and 60 wt. % of KNO_3 .

[0017] In a class of this embodiment, the molten salt is a ternary nitrate system comprising NaNO_2 , NaNO_3 , KNO_3 , for example, between 5% and 10 wt. % of NaNO_2 , between 30% and 70 wt. % of NaNO_3 and between 20% and 65 wt. % of KNO_3 .

[0018] In a class of this embodiment, the binary nitrate system comprises between 40% and 60 wt. % of NaNO_3 and between 40% and 60 wt. % of KNO_3 .

[0019] In a class of this embodiment, the ternary nitrate system comprises 7 wt. % of NaNO_2 , 40 wt. % of NaNO_3 and 53 wt. % of KNO_3 .

[0020] Advantages of the invention are summarized as follows. The thermal energy supply system of the invention makes full use of the complementarity of the biomass energy and solar energy for power generation, central cool supply (air conditioner), ice supply (fresh keeping) and heat supply, so that the clean solar energy and biomass energy can be recycled for three consecutive times. Compared with conventional energy utilization technology, the system of the invention is much more energy-efficient.

[0021] The heat storage medium in the solar storage tank is driven by the high temperature pump and flows through the solar concentrating device where the heat storage medium absorbs heat energy and raises the temperature and then returns to the heat insulation layer of the solar storage tank. The feedwater of the biomass boiler is driven by the feedwater pump and flows through the heat exchanger of the solar storage tank where the feedwater is heated and then introduced to the boiler for vapor generation. The produced vapor is transported to a turbine for power generation. The system of the invention employs practicable heat storage medium and heat energy collection equipment, solves the problem of unstable solar energy and saves the fuel consumption, and ensures the smooth operation of the turbine generator. In addition, the system employs the clean solar energy as a main power energy for cold and ice supply, and the produced waste heat from the power generation and cold and ice making can be used for hot water generation for bath or industrial applications such as food processing, textile, and printing and dyeing, thereby achieving the energy utilization recycling.

[0022] Compared with conventional energy utilization technology, the system of the invention is energy-saving, and only produces a small amount of dust, with SO_2 and CO_2 zero emission.

[0023] The solar storage tank of the system of the invention can be filled with multiple media, preferably, the heat storage medium is molten salt, which is much cheaper.

BRIEF DESCRIPTION OF THE DRAWINGS

[0024]

FIG. 1 is a schematic diagram of a solar-biomass complementary thermal energy supply system in accordance with one embodiment of the invention;

FIG. 2 is a schematic diagram of a solar storage tank comprising two media and two cycles; and

FIG. 3 is a schematic diagram of a solar storage tank comprising three media and two cycles.

DETAILED DESCRIPTION OF THE EMBODIMENTS

[0025] For further illustrating the invention, experiments detailing a solar-biomass complementary thermal energy supply system are described below.

[0026] As shown in FIG. 1, the invention provides a solar-biomass complementary thermal energy supply system, comprising: a solar concentrating device, a solar storage tank comprising a first heat exchanger and a second heat exchanger, a biomass power station comprising a biomass boiler, a central refrigeration and ice maker, and a central hot water supply tank, wherein the solar concentrating device is connected to the solar storage tank via pipes; an inlet of the first heat exchanger **B1** of the solar storage tank is connected to an outlet of a feedwater pump of the biomass boiler; an outlet of the first heat exchanger **B1** is connected to an inlet of a water feeding system of the biomass boiler; an inlet pipe of the second heat exchanger **B2** of the solar storage tank is connected to an outlet pipe of a water purification plant; an outlet of the second heat exchanger **B2** is connected to a thermal energy input pipe of the central refrigeration and ice maker; cooling water in the central refrigeration and ice maker absorbs released thermal energy produced by the central refrigeration and ice maker and converges with hot water from a waste heat collector disposed in a flue of the biomass boiler, and the confluent hot water is transported to the central hot water supply tank.

[0027] FIG. 2 is a schematic diagram of a solar storage tank comprising two media and two cycles.

[0028] The heat storage medium **1a** disposed in the solar storage tank heat **1** is conduction oil or molten salt. The heat conduction oil or molten salt is driven by a high temperature pump **2a** through a high temperature valve **2b** to the solar concentrating device where the heat conduction oil or molten salt is heated by solar energy. The heated heat conduction oil or molten salt returns to the solar storage tank and releases heat energy. Part of the heat energy heats the circulating water from the feedwater pump of the biomass boiler via the first heat exchanger **B1**, and the heated circulating water is introduced to the biomass boiler. **3a** represents the feedwater pump of the biomass boiler, and **3b** represents an outlet valve of the feedwater pump.

[0029] Another part of the heat energy heats the circulating water from the water purification plant via the second heat exchanger **B2**, and the heated circulating water is introduced to the central refrigeration and ice maker. The central refrigeration and ice maker is a lithium-bromide absorption-type refrigerator or an evaporation refrigerator. Preferably, the heat conduction oil is a mixture of 23.5 wt. % of biphenyl and 72.5 wt.% of diphenyl oxide. The molten salt is a mixture of NaNO_3 and KNO_3 , or a mixture of NaNO_2 , NaNO_3 and KNO_3 .

[0030] FIG. 3 is a schematic diagram of a solar storage tank comprising three media and two cycles.

[0031] The three media are a heat storage medium, a heat transfer medium, and circulating water. The heat storage medium **1a** is molten salt disposed in the solar storage tank **1**. The

heat transfer medium is heat conduction oil disposed in a solar heat exchanger **A**. The heat conduction oil is driven by a high temperature pump **2a** through a high temperature valve **2b** to the solar concentrating device where the heat conduction oil is heated by solar energy. The heated heat conduction oil returns to the solar storage tank and exchanges heat energy with the molten salt via the solar heat exchanger **A**. Part of the heated molten salt heats the circulating water from the feedwater pump of the biomass boiler via the first heat exchanger **B1**, and the heated circulating water is introduced to the biomass boiler. **3** represents the feedwater pump of the biomass boiler, and **3a** represents an outlet valve of the feedwater pump.

[0032] When the solar-biomass complementary thermal energy supply system in FIG. 3 runs smoothly, part of the heated molten salt heats the circulating water from the water purification plant via the second heat exchanger **B2**, and the heated circulating water is introduced to the central refrigeration and ice maker. When the solar storage tank malfunctions for a long time, the molten salt tends to freeze and block the pipes, and thus, superheated steam is introduced to the second heat exchanger **B2** to solve the problem of freezing and blocking.

[0033] To maximize the complementarity of the biomass energy and solar thermal power generation and reduce the waste heat discharge of the system, a waste heat collector is disposed in the flue of the biomass boiler, and a hot water output pipe of the waste heat collector is connected to the central hot water supply tank. Cold water absorbs the waste heat of the exhaust gas of the biomass boiler and the discharged heat energy from the central refrigeration and ice maker and transforms into hot water, which is collected by the central hot water supply tank to supply hot water for a low carbon industrial park.

[0034] The solar concentrating device (employing parabolic trough type evacuated collector tubes, Fresnel type evacuated collector tubes, or tower type solar heat boiler) comprises a heat conduction medium, which absorbs the solar energy and then flows into the solar storage tank with high temperature. In the solar storage tank, the heat conduction medium undergoes the heat exchange and then has low temperature. The heat conduction medium is driven by a high temperature pump and functions as a circulating thermal medium between the solar concentrating device and the solar storage tank. The solar storage tank comprises another cycle, that is, water medium-vapor cycle. Specifically, condenser water from a turbine is confluent with softened water from a chemical water workshop in a deaerator for oxygen removal. The mixed water is driven by the feedwater pump and flows into the heat exchanger in the solar storage tank for heat exchange whereby absorbing heat energy and raising the temperature, and is then introduced to the steam drum of the biomass boiler for steam generation.

[0035] The heat conduction medium flowing through the solar concentrating device is heat conduction oil.

[0036] The heat conduction oil is a mixture of 23.5 wt. % of biphenyl and 72.5 wt.% of diphenyl oxide, which presents solid at the temperature of below 12°C, presents liquid but has high

viscosity and poor fluidity at the temperature of between 12 and 50°C, and tends to thermally decompose at the temperature of exceeding 405°C. In general, the temperature of the mixture is controlled at between 50 and 395°C for heat conduction.

[0037] Preferably, the molten salt is a binary nitrate system comprising NaNO_3 and KNO_3 , for example, between 40% and 90 wt. % of NaNO_3 and between 10% and 60 wt. % of KNO_3 .

[0038] The binary nitrate system presents solid at the temperature of below 295°C, presents liquid at the temperature of between 295 and 565°C, and tends to thermally decompose at the temperature of exceeding 565°C. In general, the temperature of the mixture is controlled at between 295 and 550°C for heat conduction.

[0039] When the weight percentage of the components of the binary nitrate system varies, so do the temperature characteristics.

[0040] Preferably, the molten salt is a ternary nitrate system comprising NaNO_2 , NaNO_3 , KNO_3 , for example, between 5% and 10 wt. % of NaNO_2 , between 30% and 70 wt. % of NaNO_3 and between 20% and 65 wt. % of KNO_3 .

[0041] The ternary nitrate system presents solid at the temperature of below 180°C, presents liquid at the temperature of between 180 and 500°C, and tends to thermally decompose at the temperature of exceeding 500°C, and decompose quickly at the temperature of exceeding 550°C. In general, the temperature of the mixture is controlled at between 180 and 500°C for heat conduction.

[0042] When the weight percentage of the components of the ternary nitrate system varies, so do the temperature characteristics.

[0043] In summary, the thermal energy supply system of the invention makes full use of the complementarity of the biomass energy and solar energy for central cool supply, ice supply and heat supply, so that the clean solar energy and biomass energy can be recycled for three consecutive times, thereby maximizing the utilization of energy.

REFERENCES CITED IN THE DESCRIPTION

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Patent documents cited in the description

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P a t e n t k r a v

1. Supplerende termisk sol-biomasse-energiforsyningssystem, omfattende: en solkoncentreringsindretning, en sollagringstank (1) omfattende en første varmeveksler (B1) og en anden varmeveksler (B2), et biomassekraftværk omfattende en biomassekedel, en central køle- og isfremstillingsindretning og en central varmtvandsbeholder, **kendetegnet ved, at** solkoncentreringsindretningen er forbundet med sollagringstanken (1) via rør; et indløb i den første varmeveksler (B1) i sollagringstanken (1) er forbundet med et udløb af en fødevandspumpe (3a) af biomassekedlen; et udløb af den første varmeveksler (B1) er forbundet med et indløb af et vandtilførselssystem til biomassekedlen; et indløbsrør af den anden varmeveksler (B2) i sollagringstanken (1) er forbundet med et udløbsrør af et vandrensingsanlæg; et udløb af den anden varmeveksler (B2) er forbundet med et varmeenergi-indgangsrør af den centrale køle- og isfremstillingsindretning; kølevand i den centrale køle- og isfremstillingsindretning absorberer afgivet varmeenergi produceret af den centrale køle- og isfremstillingsindretning og løber sammen med varmt vand fra en spildvarmeopsamlingsindretning, der er anbragt i et aftræk af biomassekedlen, og det sammenløbende varme vand transporteres til den centrale varmtvandsbeholder.

2. System ifølge krav 1, **kendetegnet ved, at** sollagringstanken (1) omfatter to medier til varmeveksling og to cyklusser; de to medier er et varmelagringsmedium (1a) og cirkulerende vand; varmelagringsmediet (1a) er varmeledningsolie eller saltsmelte og er anbragt i sollagringstanken (1); varmeledningsolie eller saltsmelten drives af en højtemperaturpumpe (2a) til solkoncentreringsindretningen, hvor varmeledningsolie eller saltsmelten opvarmes af solenergi; den opvarmede varmeledningsolie eller saltsmelte kommer tilbage til sollagringstanken (1) og afgiver varmeenergi; en del af varmeenergien opvarmer det cirkulerende vand fra fødevandspumpen (3a) af biomassekedlen via den første varmeveksler (B1), og det opvarmede cirkulerende vand indføres i biomassekedlen; en anden del af varmeenergien opvarmer det cirkulerende vand fra vandrensingsanlægget via den anden varmeveksler (B2), og det opvarmede cirkulerende vand indføres i den centrale køle- og isfremstillingsindretning.

- 5 **3.** System ifølge krav 1, **kendetegnet ved, at** sollagringstanken (1) omfatter tre medier til varmeveksling og to cyklusser; de tre medier er et varmelagringsmedium (1a), et varmeoverføringsmedium og cirkulerende vand; varmelagringsmediet (1a) er saltsmelte anbragt i sollagringstanken (1); varmeoverføringsmediet er varmeledningsolie anbragt i en solvarmeveksler (A); varmeledningsolien drives til solkoncentreringsindretningen, hvor varmeledningsolien opvarmes af solenergi; den opvarmede varmeledningsolie kommer tilbage til sollagringstanken (1) og udveksler varmeenergi med saltsmelten via solvarmeveksleren (A); en del af den opvarmede saltsmelte opvarmer det cirkulerende vand fra fødevandspumpen (3a) af biomassekedlen via den første varmeveksler (B1), og det opvarmede cirkulerende vand indføres i biomassekedlen; en anden del af den opvarmede saltsmelte opvarmer det cirkulerende vand fra vandrensningsanlægget via den anden varmeveksler (B2), og det opvarmede cirkulerende vand indføres i den centrale køle- og isfremstillingsindretning.
- 10
- 15
- 20 **4.** System ifølge krav 1, 2 eller 3, **kendetegnet ved, at** spildvarmeopsamlingsindretningen er anbragt i aftrækket af biomassekedlen, og et varmtvandsudløbsrør af spildvarmeopsamlingsindretningen er forbundet med den centrale varmtvandsbeholder.
- 25 **5.** System ifølge krav 1, 2 eller 3, **kendetegnet ved, at** den centrale køle- og isfremstillingsindretning er en lithium-bromid-absorptionskøleindretning eller en fordampningskøleindretning.
- 30 **6.** System ifølge krav 2 eller 3, **kendetegnet ved, at** saltsmelten er et binært nitratsystem.
- 7.** System ifølge krav 2 eller 3, **kendetegnet ved, at** saltsmelten er et ternært nitratsystem.
- 8.** System ifølge krav 6, **kendetegnet ved, at** det binære nitratsystem omfatter mellem 40 % og 90 vægt-% NaNO_3 og mellem 10 % og 60 vægt-% KNO_3 .

9. System ifølge krav 7, **kendetegnet ved, at** det ternære nitratsystem omfatter mellem 5 % og 10 vægt-% NaNO_2 , mellem 30 % og 70 vægt-% NaNO_3 og mellem 20 % og 65 vægt-% KNO_3 .

DRAWINGS

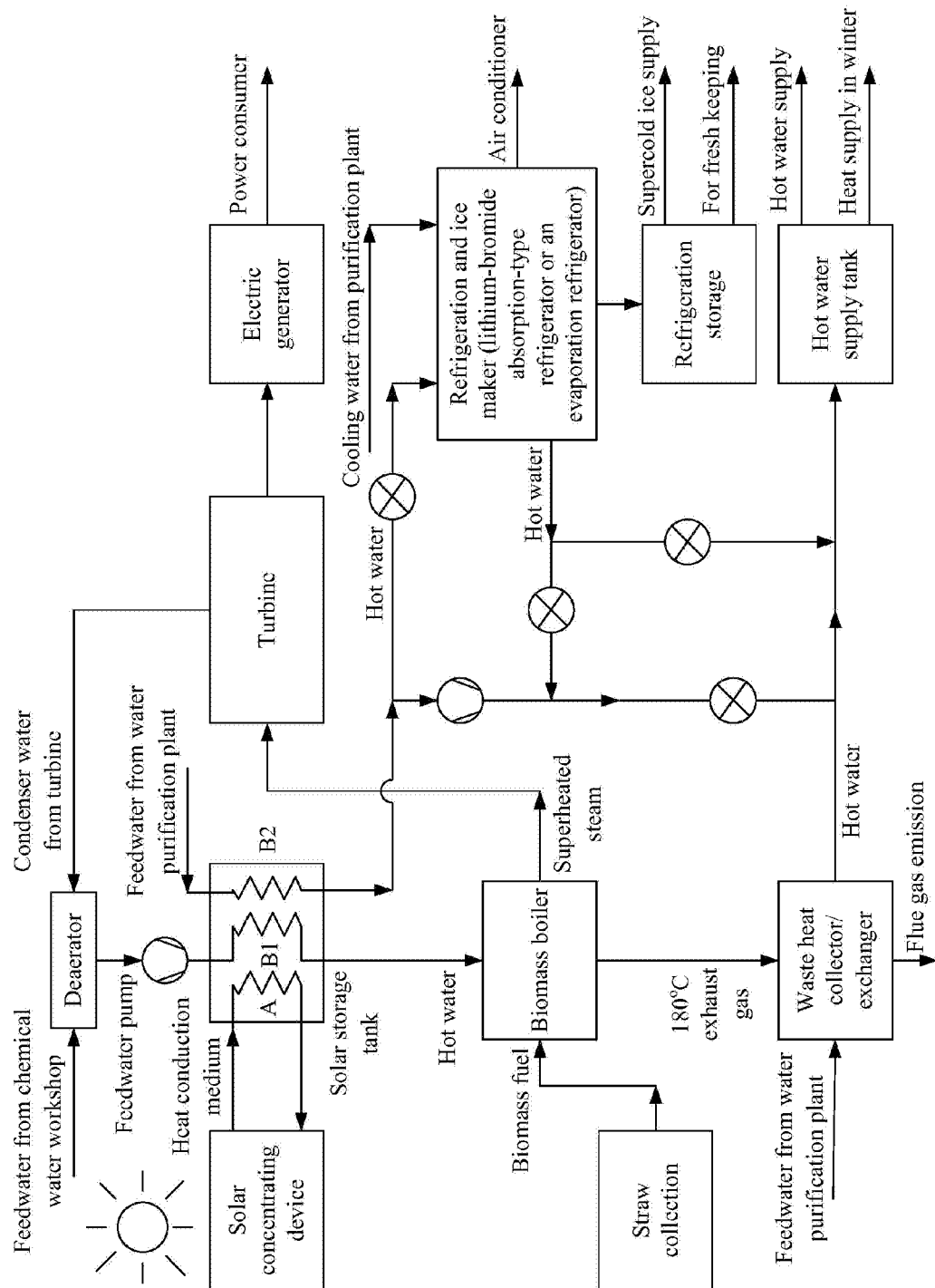
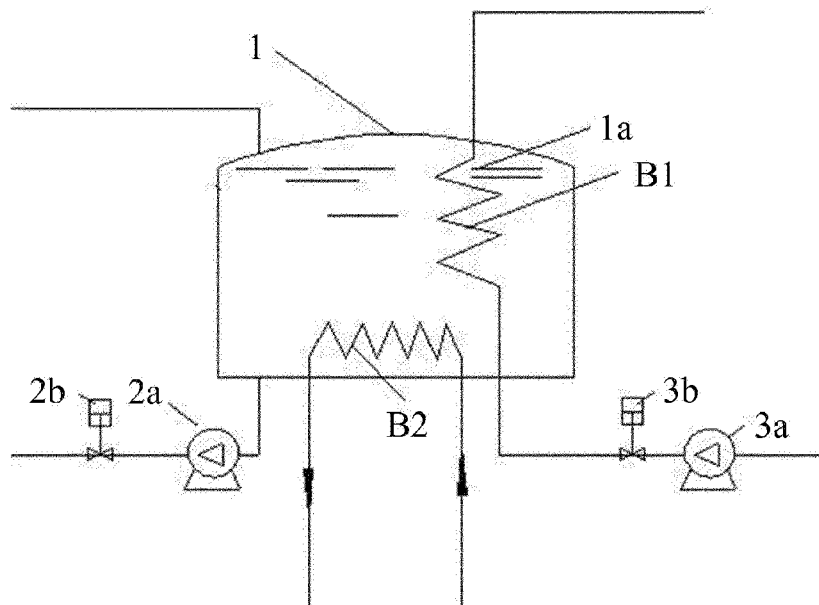
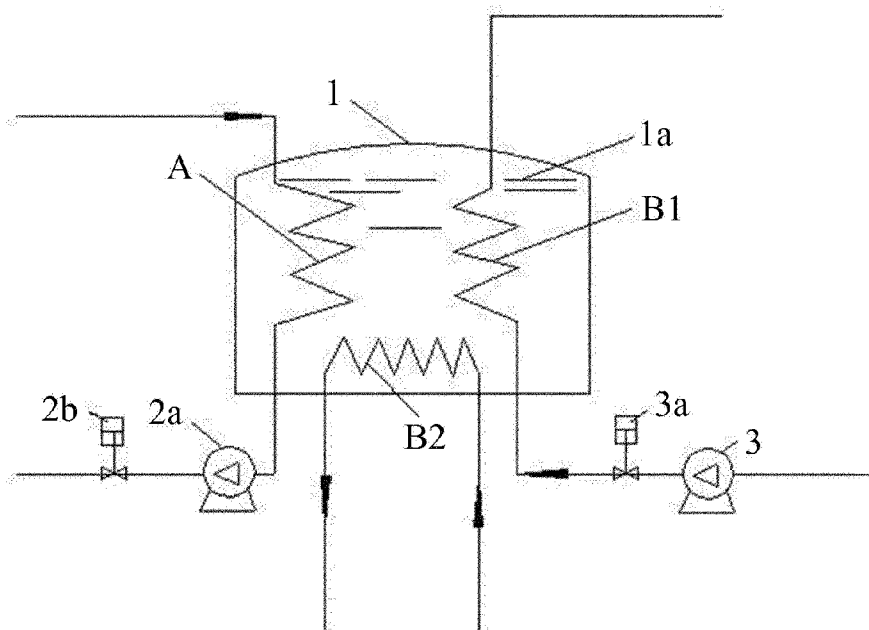


FIG. 1

**FIG. 2****FIG. 3**