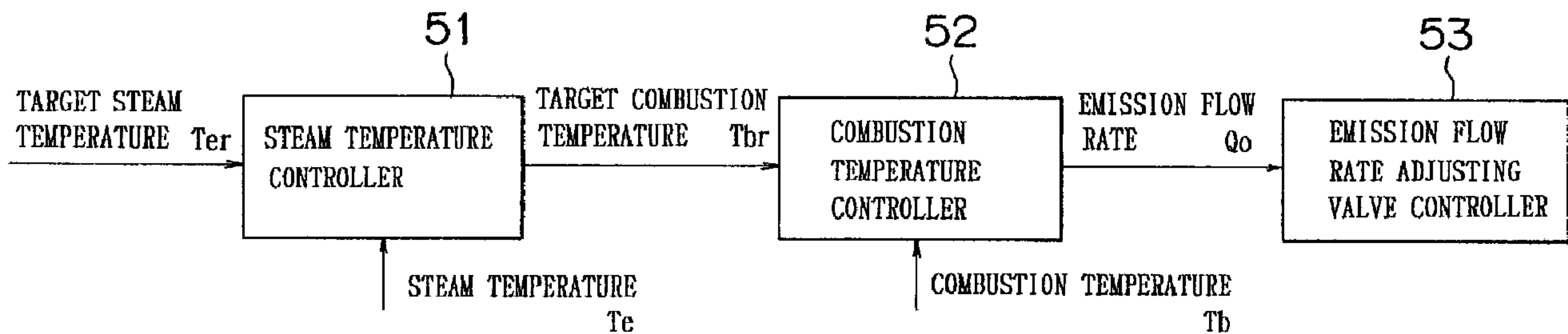




(22) Date de dépôt/Filing Date: 1999/07/14
 (41) Mise à la disp. pub./Open to Public Insp.: 2000/01/16
 (45) Date de délivrance/Issue Date: 2010/06/08
 (62) Demande originale/Original Application: 2 277 676
 (30) Priorités/Priorities: 1998/07/16 (JP HEI 10-201927);
 1998/12/18 (JP HEI 10-361713)

(51) Cl.Int./Int.Cl. *C01B 3/32* (2006.01),
G05D 23/00 (2006.01)
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(54) Titre : DISPOSITIF DE REGULATION POUR REFORMEUR ET METHODE DE REGULATION DU REFORMEUR AU MOYEN DE CE DISPOSITIF
 (54) Title: CONTROL APPARATUS FOR REFORMER AND METHOD OF CONTROLLING REFORMER USING CONTROL APPARATUS



(57) Abrégé/Abstract:

A control apparatus for a reformer and a method of controlling the reformer are provided. The reformer gasifies a reformat fuel by a reforming reaction, supplies the obtained reformat gas to an energy converter to convert the reformat gas into energy of another form, and heats the reformat fuel by burning emission containing unreacted flammable gas produced in the energy converter. The control apparatus comprises a reforming amount assessing device for assessing the amount of the reformat fuel to be gasified, and an emission amount assessing device for assessing the amount of emission to be supplied into the reformer on the basis of the assessed amount of reformat fuel. When using the unreacted hydrogen gas generated in a fuel cell for heating the reformat fuel, the unreacted hydrogen gas and combustion aid gas can be controlled so that the reformat fuel is heated properly.

ABSTRACT OF THE DISCLOSURE

A control apparatus for a reformer and a method of controlling the reformer are provided. The reformer gasifies a reformat fuel by a reforming reaction, supplies the obtained reformat gas to an energy converter to convert the reformat gas into energy of another form, and heats the reformat fuel by burning emission containing unreacted flammable gas produced in the energy converter. The control apparatus comprises a reforming amount assessing device for assessing the amount of the reformat fuel to be gasified, and an emission amount assessing device for assessing the amount of emission to be supplied into the reformer on the basis of the assessed amount of reformat fuel.

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10 When using the unreacted hydrogen gas generated in a fuel cell for heating the reformat fuel, the unreacted hydrogen gas and combustion aid gas can be controlled so that the reformat fuel is heated properly.

CONTROL APPARATUS FOR REFORMER AND METHOD OF CONTROLLING REFORMER USING CONTROL APPARATUS

BACKGROUND OF THE INVENTION

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1. Field of Invention

The present invention relates to a reformer for reforming reformat fuel into a desired fuel such as hydrogen-rich gas, and more particularly to an apparatus for controlling the temperature of such reformat fuel. This invention also relates to a method of controlling a reformer using the apparatus.

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2. Description of Related Art

A reformer for generating gas mainly composed of hydrogen gas by using methyl alcohol (methanol) and water as reformat fuel materials is known. In this reformer, a copper alloy or the like is used as catalyst, and the active temperature of the catalyst is, for example, 280°C, and when the temperature is lower than the activation temperature, the methanol is not reformed sufficiently, and the amount of residual methanol in the reformat gas increases. Moreover, because the reforming reaction of methanol is an endothermic reaction, heat is supplied from an external source in order to promote the reforming reaction as well as to maintain the catalyst temperature.

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The heating method includes, aside from heating by a burner, a method of generating heat by an oxidation reaction and transferring the heat to the reforming portion. The latter method is a so-called partial oxidation reaction method, in which, for example, air is mixed in methanol vapor, and it is oxidized in the presence of catalyst to generate hydrogen, and the heat generated at this time is utilized. Therefore, by utilizing this partial oxidation reaction, the heat accompanying reforming reaction is replenished by the partial oxidation reaction, and the heat absorption and heat generation are balanced, so that heating from an external source is not necessary. In this method, however, only the thermal balance is achieved in the reforming portion so as not to cause temperature changes due to reforming or oxidation, and it is not intended to be applied to setting of the reforming portion to a desired temperature.

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That is, to set the temperature of the reforming portion to an appropriate temperature for the reforming reaction or catalyst activity, heating from an external source is required. Accordingly, in this kind of reformer, by the heat generated in the combustion portion, steam of a specified temperature is obtained from a mixture of methanol and water, and the steam is supplied into the reforming portion.

When this reformer is used, for example, to generate fuel gas in a fuel cell, it is necessary to control the reaction in the reformer depending on variation of load of the fuel cell. That is, along with an increase of load, the production of reformat gas must be increased. When the load drops, the production of reformat gas must be decreased. To increase or decrease the generation of reformat gas, it is required to increase or decrease the material to be supplied to the reforming portion, that is, the mixed steam of methanol and water, but for this purpose it is necessary to increase or decrease the heating calorific value for generating the mixed steam of methanol and water at a desired temperature.

The amount of heat required to generate a mixed steam of methanol and water can be controlled by increasing or decreasing the amount of fuel for heating such as methanol. However, the burner or heat generating device using an oxidation catalyst conventionally used as a heating device for heating the mixture of methanol and water is low in the response of heat generation, and it is hence difficult to control heating promptly coping with load fluctuations in such known reformers. That is, in the event of a sudden load increase, the heat generation is insufficient for the amount of methanol and water to be heated, and the steam temperature or catalyst temperature drops. Consequently, the reforming reaction becomes dull, or the residual methanol amount in the reformat gas increases, and the performance of the fuel cell declines. To the contrary, if the load drops suddenly, due to delay in drop of heating amount, the steam temperature or catalyst temperature may elevate excessively, and the activity of the catalyst is lowered.

To eliminate such disadvantage, the invention disclosed in Japanese Patent Publication No. HEI 7-105240 is intended to control the temperature depending on load fluctuations by controlling the steam ratio. That is, by decreasing the amount of water mixed as reformat fuel, the amount of heat required for heating and evaporation drops, and the temperature of the mixed steam of methanol and water as reformat fuel rises. However, when the amount of water is increased, the amount of heat required for

raising the temperature and evaporating increases, so that the temperature of the mixed steam of methanol and water as reformat fuel declines.

The method of temperature control disclosed in this publication comprises changing the amount of water, changing the amount of heat consumed or absorbed by the water, and thereby controlling the temperature. Therefore, as compared with the method of controlling the heat generation amount by changing the amount of fuel for combustion, the response of temperature control is improved. This published method, however, consumes part of the heat generated for heating and evaporation on the condition that the heat generation by combustion of the fuel is constant. For example, in the case of lowering the reformat gas amount due to small fluctuations in the fuel cell, the amount of heat generation by combustion is maintained higher than the amount of heat determined theoretically. As a result, the combustion is controlled to generate more heat than the heat actually required for reforming the reformat fuel, and the fuel is consumed more than necessary, and thus the fuel economy drops. Also in this published invention, spent fuel containing residual hydrogen is used as a part of the fuel for heating the reformat fuel, and the reformat fuel is heated by burning the residual hydrogen by a burner. Yet, if the reformat fuel is heated by burning the residual hydrogen by a burner, the amount of heat is not controlled. Thus, because the temperature is controlled by the steam ratio, the consumption of the heating fuel containing residual hydrogen that is required is more than the amount needed for heating of reformat fuel. In this respect, also, the residual hydrogen is consumed excessively, and thus this known method has been susceptible to improvement in a more effective use of fuel.

SUMMARY OF THE INVENTION

The invention has been made in the light of the above-described background. It is an object of the present invention to provide a control apparatus that can control combustion fuel for heating reformat fuel, control the reformat fuel temperature to a desired temperature suitable for the reforming reaction, and utilize the reformat fuel effectively.

To achieve this object, the invention uses unreacted flammable gas in the emission resulting from energy conversion of reformat gas for heating of reformat fuel, and controls the amount of unreacted flammable gas for combustion for heating at an appropriate amount depending on the required amount of reformat fuel, as well as on other factors.

In a first aspect of the invention, a control apparatus is provided for controlling a reformer. The reformer can comprise a reformat gas generator that gasifies a reformat fuel by a reforming reaction, the combustion portion that heats the reformat fuel by burning the emission including unreacted flammable gas generated at the time of conversion of the reformat gas obtained from the reformat gas generator into another energy form by an energy converter. The control apparatus comprises a reformed amount assessing device that assesses the amount of reformat fuel to be gasified, and an emission amount assessing device that assesses the amount of emission to be supplied into a combustion portion on the basis of the assessed reformat fuel amount.

Therefore, according to the invention, when the amount of the reformat fuel varies depending on fluctuations of load in the energy converter or the like, the amount of emission including the unreacted flammable gas to be supplied into the reformer accordingly is assessed. By supplying the assessed amount of emission into the reformer, the unreacted flammable gas contained in the emission burns, and the reformat fuel is heated. In this case, because the amount of the reformat fuel and the amount of flammable gas to burn correspond to each other, the reformat fuel is heated to a desired temperature. As a result, the flammable gas is not consumed more than necessary, and the reformat fuel temperature can be controlled to a desired temperature. Moreover, the reforming reaction proceeds desirably, and the reformat gas of high quality is obtained.

Moreover, in other embodiments, the control apparatus can also comprise a heat detector that detects a shortage in the amount of heat for burning the emission including the unreacted flammable gas in the combustion portion necessary for heating the reformat fuel, and a fuel supplying device that supplies the heating fuel into the combustion portion if a shortage of heat is detected.

According to such embodiments, if the necessary amount of heat to be generated in the combustion portion exceeds the amount of heat obtained by combustion of unreacted flammable gas, the heating fuel is supplied into the combustion portion. Therefore, the heating fuel is used only when the amount of heat generated is insufficient by the use of unreacted flammable gas only, and the unreacted flammable gas is used to the maximum extent for heating of the reformat fuel, so that the consumption of heating fuel is decreased, and the energy efficiency is enhanced on the whole.

Additionally, in embodiments, the control apparatus can also comprise a combustion portion temperature detector that detects the temperature of the combustion portion, and a heating fuel adjuster that adjusts (decreases) the amount of heating fuel consumed in the combustion portion on the basis of the detected temperature of the combustion portion.

According to such embodiments, if the temperature of the reformat fuel is higher than necessary, supply of heating fuel into the combustion portion is stopped. As a result, it is possible to prevent a drop of energy efficiency due to excessive combustion of the heating fuel, or a drop of reforming reaction efficiency due to an excessive elevation of temperature of the reformat fuel.

Preferably, the control apparatus further comprises a reformat fuel temperature detector that detects the temperature of the reformat fuel heated in the combustion portion, and a heating fuel arrester that stops supply of heating fuel to the combustion portion when the detected temperature of the reformat fuel exceeds a predetermined temperature.

In such embodiments, when the temperature of the combustion portion becomes higher than the predetermined temperature, the amount of material consumed in the combustion portion decreases, and the heating amount in the combustion portion decreases. Accordingly, abnormal temperature rise of the combustion portion and related damage can be prevented.

In addition to the constitution of the first aspect, the control apparatus can also comprise a flammable gas amount estimator that estimates the amount of unreacted flammable gas in the emission, on the basis of the reformat fuel amount reformed to supply into the energy converter and the load of the energy converter.

In such embodiments, the amount of the unreacted flammable gas used in heating of reformat fuel is more accurate, control of the heating temperature of the reformat fuel is precise, and the unreacted flammable gas can be utilized effectively.

Preferably, the control apparatus further comprises a reformat fuel temperature detector that detects the temperature of the reformat fuel supplied for the reforming reaction, and a temperature adjuster that adjusts the emission amount to be supplied into the reformer on the basis of the detected temperature of the reformat fuel.

According to such embodiments, when the temperature of the reformat fuel is low, or high, the emission amount, that is, the unreacted flammable gas amount,

consumed can be increased or decreased. As a result, the temperature of the reformat fuel is adjusted, and a suitable temperature is obtained.

In addition to the constitution of the first aspect, it may also comprise a delay adjustor that adjusts the emission amount to be supplied to the reformer, on the basis of
5 the time delay until the reformat fuel supplied in the reformer is gasified.

According to such embodiments, prior to sufficient supply of reformat fuel, if the unreacted flammable gas is burned relatively much, or to the contrary if the reformat fuel decreases, it is possible to avoid a decrease of the combustion amount of unreacted flammable gas in advance, so that the heating temperature of the reformat
10 fuel is optimized.

In addition to the constitution of the first aspect, the control apparatus can also comprise a combustion aid gas amount determiner that determines the amount of a combustion aid gas for burning the flammable gas in the emission supplied into the reformer, on the basis of the amount of the unreacted flammable gas supplied into the
15 reformer.

According to such embodiments, the combustion aid gas is supplied into the reformer depending on the amount of the flammable gas supplied for heating the reformat fuel. As a result, the rate of two gas amounts is appropriate, and a desired heating calorific value is obtained, so that the heating temperature of the reformat fuel
20 is optimized.

The control apparatus can further comprise a heating temperature detector that detects the temperature for heating the reformat fuel to be supplied for the reforming reaction, and a temperature adjuster that adjusts the amount of combustion aid gas to be supplied into the reformer on the basis of the detected heating temperature.

According to such embodiments, when the heating temperature is low, for example, the combustion aid gas amount is decreased and the heat taken away by the combustion aid gas is decreased, so that the temperature of the reformat fuel is raised. When the heating temperature is high, for example, the combustion aid gas amount is increased and the heat taken away by the combustion aid gas is increased, so that the
25 temperature of the reformat fuel is lowered. As a result, the heating temperature of the reformat fuel is optimized.
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The control apparatus can further comprise a delay adjustor that adjusts the combustion aid gas amount to be supplied into the reformer on the basis of the delay until the reformat fuel supplied into the reformer is gasified.

According to such embodiments, the heat value given to the reformat fuel by combustion of unreacted flammable gas is changed by the amount of combustion aid gas, and this change occurs depending on the delay of supply of reformat fuel, or on the delay of decrease of supply amount. As a result, the reformat fuel can be heated to an appropriate temperature.

Preferably, the control apparatus can also comprise an A/F detector that detects the ratio of the flammable gas amount to be consumed for heating the reformat fuel and the amount of combustion aid gas for burning the flammable gas, and an A/F adjuster that adjusts the emission amount to be supplied into the reformer.

According to such embodiments, therefore, a surplus or shortage of combustion aid gas amount is adjusted, and the unreacted flammable gas is burned as desired, so that the heating temperature of the reformat fuel is optimized.

Preferably, the control apparatus can comprise a first temperature detector that detects the temperature at the supply side of combustion aid gas of the combustion portion, a second temperature detector that detects the temperature at the exhaust side of the combustion portion, and a combustion aid gas amount controller that increases the supply amount of the combustion aid gas when the temperature at the supply side of combustion aid gas detected by the first temperature detector is higher than the temperature at the exhaust side detected by the second temperature detector, and that decreases the supply amount of the combustion aid gas when the temperature at the supply side of combustion aid gas detected by the first temperature detector is lower than the temperature at the exhaust side detected by the second temperature detector.

According to such embodiments, when the temperature at the inflow side of the combustion portion is high, the supply amount of combustion aid gas increases, and the amount of heat taken away by the combustion aid gas increases and the combustion temperature is lowered. To the contrary, when the temperature at the exhaust side is high, the supply amount of combustion aid gas is decreased, and the amount of heat taken away from the inflow side of the combustion aid gas is decreased, such that the heat value sent to the exhaust side declines, the temperature at the inflow side of the combustion aid gas elevates, and the temperature at the exhaust side drops. Ultimately, the temperature in the inflow side and exhaust side of the combustion aid gas is balanced, and local overheating is prevented.

A second aspect of the invention provides a control apparatus for a reformer. The reformer can comprise a reformat gas generator that gasifies a reformat fuel by a

reforming reaction, and a combustion portion that heats the reformat fuel and supplies into the reformat gas generator by burning the emission including the unreacted flammable gas generated at the time of conversion of the reformat gas by the reformat gas generator into energy of other form by an energy converter. The control apparatus
5 comprises a reformed amount assessing device for assessing the amount of reformat fuel to be gasified; a flammable gas amount assessing device that assesses a necessary amount of flammable gas supplied into the combustion portion on the basis of the assessed amount of reformat fuel; and an emission amount assessing device that assesses the emission amount to be supplied into the combustion portion on the basis of
10 the assessed necessary amount of flammable gas.

According to the second aspect, the amount of the reformat fuel to be gasified is assessed depending on the load at the energy converter or the like, and the amount of flammable gas necessary for heating the reformat fuel is assessed on the basis of the assessed reformat fuel amount. The emission amount including the necessary amount
15 of flammable gas is assessed. Therefore, the unreacted flammable gas for heating the reformat fuel can be used, and the reformat fuel is heated appropriately by the unreacted flammable gas, so that a favorable reforming reaction takes place, thereby obtaining a reformat gas of high quality. At the same time, the fuel can be utilized effectively.

20 In addition to above-described embodiment of the second aspect, the control apparatus can further comprise a combustion aid gas amount assessing device that assesses the amount of combustion aid gas to be supplied together with the unreacted flammable gas into the reformer, on the basis of the amount of flammable gas assessed by the flammable gas assessing device.

25 According to such embodiments, the unreacted flammable gas supplied together with emission can be effectively burned so that the heating temperature of the reformat fuel can have a desired temperature, the temperature of the reformat fuel and the accompanying reforming reaction are favorable, and a reformat gas of high quality is obtained.

30 A third aspect of the invention relates to a control apparatus for a reformer. The reformer can comprise a reformat gas generator that gasifies a reformat fuel by a reforming reaction, and a combustion portion that burns a combustion material, heats the reformat fuel and supplies it into the reformat gas generator. The control apparatus comprises a target combustion temperature setting device that sets the target

combustion temperature in the combustion portion on the basis of the target temperature of the reformat fuel, and a combustion material amount setting device that sets the amount of combustion material to be consumed in the combustion portion on the basis of the target combustion temperature determined in the target combustion temperature setting device.

According to the third aspect, because the amount of combustion material supplied into the combustion portion is set on the basis of the target combustion temperature, an abnormally high temperature in the combustion portion is prevented, and damage of the combustion portion is avoided. Moreover, because the target combustion temperature is determined on the basis of the target temperature of the reformat fuel, the reforming combustion temperature is optimized, and the reforming reaction takes place efficiently.

BRIEF DESCRIPTION OF THE DRAWINGS

Fig. 1 is a flowchart showing an exemplary embodiment of control executed in a control apparatus of the invention;

Fig. 2 is a flowchart showing another exemplary embodiment of control executed in a control apparatus of the invention;

Fig. 3 is a flowchart showing another exemplary embodiment of control executed in a control apparatus of the invention;

Fig. 4 is a diagram showing an example of a map for determining the A/F ratio on the basis of the detected temperature of the combustion portion of the reformer;

Fig. 5 is a flowchart showing another exemplary embodiment of control executed in a control apparatus of the invention;

Fig. 6 is a time chart showing changes of control values when the control shown in Fig. 5 is executed;

Fig. 7 is a flowchart showing another exemplary embodiment of control executed in a control apparatus of the invention;

Fig. 8A is a map showing an emission adjustment coefficient versus combustion portion representative temperature;

Fig. 8B is a map showing a combustion methanol adjustment coefficient versus combustion portion representative temperature;

Fig. 9A is a diagram showing changes of reformat fuel steam temperature when the control shown in Fig. 7 is not executed;

Fig. 9B is a diagram showing changes of representative temperature of the combustion portion when the control shown in Fig. 7 is not executed;

Fig. 9C is a diagram showing changes of the emission amount when the control shown in Fig. 7 is not executed;

5 Fig. 9D is a diagram showing changes of reformat fuel steam temperature of the combustion portion when the control shown in Fig. 7 is executed;

Fig. 9E is a diagram showing changes of representative temperature of the combustion portion when the control shown in Fig. 7 is executed;

10 Fig. 9F is a diagram showing changes of the emission amount when the control shown in Fig. 7 is executed;

Fig. 10 is a block diagram showing an exemplary embodiment of a controller in a flow rate control system of emission;

Fig. 11 is a block diagram showing an exemplary embodiment of a controller in a flow rate control system of combustion methanol;

15 Fig. 12 is a flowchart showing an exemplary embodiment of control to be executed by a steam temperature controller;

Fig. 13 is a diagram showing an example of a map for determining a combustion temperature target value;

20 Fig. 14 is a flowchart showing an exemplary embodiment of control to be executed by a combustion temperature controller;

Fig. 15 is a diagram showing an example of a map for determining a fuel material flow rate;

Fig. 16 is a diagram showing an example of a map for determining a command value for obtaining an assessed combustion material amount;

25 Fig. 17 is a flowchart showing another exemplary embodiment of control to be executed by a control apparatus of the invention;

Fig. 18 is a flowchart showing an exemplary embodiment of a sub-routine for adjusting the air flow rate;

30 Fig. 19 is a diagram showing an example of a map for a target temperature gradient at the combustion portion;

Fig. 20 is a diagram schematically showing a system connecting a reformer to a fuel cell; and

Fig. 21 is a diagram schematically showing an exemplary embodiment of the structure of the heating portion and the control system of the system of Fig. 20.

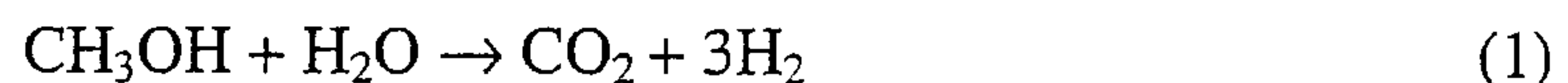
DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS

The invention is further described below while referring to illustrated preferred embodiments thereof. First, as a reformer, using methanol and water as reformat fuel, a system of employing an energy converter for converting the reformat gas generated from the reformer into another form as a fuel cell is described. Fig. 20 schematically shows an exemplary system, in which a reformer 2 is connected to the anode side of a fuel cell 1. The reformer 2 includes a heating portion 3 for heating the reformat fuel, a reforming portion 4, and a carbon monoxide (CO) oxidizing portion 5. The reformer 2 reforms the mixture of methanol and water into hydrogen and carbon dioxide.

The heating portion 3 heats the reformat fuel, and produces a mixed steam of methanol and water. The heating portion 3 comprises a combustion portion 6 for generating heat for heating, and a vaporizing portion 7 for evaporating the reformat fuel by its heat. The combustion portion 6 can comprise a device for burning the heating fuel by a burner, or a catalyst for oxidizing the heating fuel. Therefore, to this combustion portion 6, a pump 8 for supplying methanol, an example of the heating fuel, is connected through an injector 9. An air feed portion 10 for supplying air, as an example of combustion aid gas, to the combustion portion 6 is provided. The air feed portion 10 typically comprises an air pump.

The vaporizing portion 7 is provided with a pump 11 as a reformat fuel feed portion for supplying a mixture of methanol and water. The vaporizing portion 7 and the combustion portion 6 are connected to each other through a heat exchanger 12 so as to transfer heat. A more specific embodiment of the heating portion 3 is described below.

The reforming portion 4 generates a hydrogen-rich gas by a reforming reaction substantially between methanol and water. More specifically, using a copper compound catalyst at an active temperature of about 280°C, a reformat gas substantially comprising hydrogen gas is generated by a reforming reaction expressed in the following equation (1):



The reforming portion 4 generates hydrogen gas and heat by a partial oxidation reaction of methanol, and air is supplied from an air feed portion 13 for this purpose. That is, the reforming reaction shown in the equation (1) is an endothermic reaction. In contrast, the reaction in equation (2) below, which is a partial oxidation reaction of methanol, is

an exothermic reaction. Therefore, by balancing the endothermic amount and the exothermic amount, the temperature of the reforming portion 4 is maintained substantially constant.



5 The reforming reaction shown in equation (1) and the partial oxidation reaction shown in equation (2) are reactions that occur in an ideal state. Moreover, as carbon dioxide is reversibly changed into carbon monoxide, carbon monoxide is inevitably mixed into the reformat gas. This carbon monoxide can poison the catalyst of the anode 15 in the fuel cell 1, and the CO oxidation portion 5 is provided for removing the
10 carbon monoxide. The CO oxidation portion 5 include a CO oxidizing catalyst (not shown), and also includes an air feed portion 14. By passing the reformat gas generated in the reforming portion 4, the carbon monoxide contained in the reformat gas is oxidized by the oxygen in the air and converted to carbon dioxide.

On the other hand, the fuel cell 1 comprises, for example, a proton-transmitting
15 high polymer film as an electrolyte, and an anode 15 and a cathode 16 provided at opposed sides of the electrolyte film. Multiple single cells each having such structure are connected in series and parallel. The anode 15 and the cathode 16 comprise a diffusion layer and reaction layer individually, and the reaction layer in the anode 15 comprises a porous structure carrying, for example, platinum, a platinum alloy,
20 ruthenium or other catalyst, on a carbon support. The reformer 2 is connected to the anode 15, and an air feed portion 17 such as a pump is connected to the cathode 16, and oxygen for reacting with the hydrogen in the reformat gas is supplied.

To the anode 15 and the cathode 16, moreover, a battery 18 and an inverter 19
25 are connected as external loads for forming a closed circuit. A current sensor 20 is included in the closed circuit. A motor 21 is connected to the inverter 19. The motor 21 can be a drive source for driving a vehicle or the like.

Ionization of hydrogen occurring in the anode 15 and oxidation reaction through
the electrolyte film do not take place in all of the hydrogen gas supplied into the fuel cell 1. However, the reaction efficiency is typically several tens percent, and unreacted
30 flammable gas, that is, hydrogen gas is contained in the emission from the anode 15 side. To use the hydrogen gas effectively, a return pipe 22 communicates with the fuel cell 1 and the combustion portion 6 so as to return the anode 15 side gas into the combustion portion 6. In an intermediate portion of the return pipe 22, a flow rate

adjusting valve 23 is provided to control the flow rate of the gas flowing in the return pipe 22. The flow rate adjusting valve 23 controls its opening degree electrically. The return pipe 22 discharges the gas flowing inside properly to the outside without feeding into the combustion portion 6.

5 Fig. 21 shows a further specific constitution of the heating portion 3, together with a control system. The combustion portion 6 includes a combustion chamber 24 for oxidizing the heating fuel while passing methanol as a heating fuel (hereafter referred to as "combustion methanol") and/or unreacted flammable gas and air in a specific direction. The injector 9 is disposed at the inflow side of this combustion chamber 24, so that the combustion methanol is sprayed into the combustion chamber 24 from the injector 9. Moreover, at the inflow side of the combustion chamber 24, an air feed port 25 is formed to open near the spray position of the combustion methanol by the injector 9, and the air pump 10 is connected to this air feed port 25.

10 Further, near the injector 9 of the combustion chamber 24, the return pipe 22 is opened and connected. At both sides of the flow rate adjusting valve 23 inserted in the return pipe 22, pressure sensors 26, 27 are disposed. The upstream side pressure and downstream side pressure of the flow rate adjusting valve 23 are detected by the pressure sensors 26 and 27, respectively.

15 The heat exchanger 12 (Fig. 20) is disposed inside of the combustion chamber 24. The heat exchanger 12 includes plural evaporation pipes 28 extending in an airtight state across the combustion chamber 24, and one end of each evaporation pipe 28 communicates with a liquid feed pipe 29, and the other end communicates with a steam pipe 30. At the outer periphery of each evaporation pipe 28, in the area positioned inside of the combustion chamber 24, an oxidizing catalyst 31 is provided. Therefore, the unreacted flammable gas in the emission gas or combustion methanol supplied inside the combustion chamber 24 is oxidized by the oxygen in the air in the catalyst 31, and heat is generated. To detect the temperature by such combustion, temperature sensors 32 are provided in the catalyst 31 or evaporation pipes 28. These temperature sensors 32 are disposed from the inflow side of the air as combustion aid gas toward the exhaust side.

20 25 30 At the downstream side of the combustion chamber 24, an exhaust pipe 33 is connected, and an air/fuel ratio sensor (A/F sensor) 34 is disposed at the end of the combustion chamber 24 side of this exhaust pipe 33. This A/F sensor 34 issues an electric signal depending on the oxygen concentration in the emission. The A/F sensor

34 detects the ratio (A/F) of the combustion methanol or unreacted flammable gas supplied in the heating portion 3 and the oxygen.

5 The liquid feed pipe 29 is for supplying the mixture of methanol and water as reformat fuel into the evaporation pipes 28, and is connected to the liquid feed pump 11, forming the reformat fuel feed portion. The steam pipe 30 comprises a duct for feeding the mixed steam of methanol and water produced in the evaporation pipes 28 into the reforming portion 4, and a steam temperature sensor 35 that detects the steam temperature is disposed inside the steam pipe 30.

10 The pumps 8, 10, 11 are electrically controlled, and are designed to adjust the displacement properly. A controller such as an electronic control unit (ECU) 36 is provided for control purposes. The ECU 36 is typically a microcomputer comprising a central processing unit (CPU), memory devices (RAM, ROM), and input and output interfaces. Detection signals from the sensors 26, 27, 32, 34, 35 are entered as control data. Moreover, to detect the load of the fuel cell 1, a detection signal of the current
15 sensor 20 is entered in the ECU 36. The opening degree of the flow rate adjusting valve 23 is controlled by this electronic control unit 36.

Regarding the basic operation of the reformer 2, a mixture of methanol and water as reformat fuel is supplied into the evaporation pipes 28 through the liquid feed pipe 29 by the liquid feed pump 11. In the combustion chamber 24, combustion
20 methanol is sprayed by the injector 9, and simultaneously or alternatively, emission containing unreacted hydrogen gas is supplied from the return pipe 22. As the combustion support gas, air is supplied by the air pump 10. The heating fuel and air comprising this combustion methanol and/or unreacted hydrogen gas are oxidized in the oxidation catalyst 31, that is, burned to generate heat. By this heat, the evaporation
25 pipes 28 are heated, and the contained mixed liquid is evaporated, such that a mixed steam of methanol and water is generated. The emission caused by combustion is sent out through the exhaust pipe 33.

The mixed steam generated in the evaporation pipes 28 is supplied into the reforming portion 4 through the steam pipe 30. By the catalyst provided in the
30 reforming portion 4, a reforming reaction between methanol and water occurs, and a reformat gas substantially comprising hydrogen gas and carbon dioxide is produced. At the same time, a partial oxidation reaction between the air and methanol supplied into the reforming portion 4 from the air feed portion 13 occurs. This partial oxidation reaction is expressed in the above equation (2), and, as shown, hydrogen gas and carbon

dioxide are produced. The reforming reaction of methanol is an endothermic reaction and the partial oxidation reaction of methanol is an exothermic reaction. Therefore, by controlling the reaction so that the endothermic amount and exothermic amount by these two reactions are at least substantially equal to each other, the thermal balance of the reforming portion 4 is achieved, and the temperature of the reforming portion 4 is maintained substantially constant. Therefore, there is substantially no input or output of heat in the reforming portion 4, and the heat generated in the combustion portion 6 is at least substantially used for heating and evaporation of the reformat fuel.

The gas produced in the reforming portion 4 is, in principle, only hydrogen gas and carbon dioxide. Actually, however, some carbon monoxide (typically about 1%) is generated. The majority of the carbon dioxide reacts with the oxygen in the air supplied from the air feed portion 14 when the reformat gas passes through the CO oxidation portion 5, and becomes carbon dioxide. Thus, the reformat gas enriched in hydrogen is supplied to the anode 15 in the fuel cell 1, which produces hydrogen ions and electrons in its reaction layer, and hydrogen ions pass through the electrolyte film to react with oxygen at the cathode 16 side to produce water. Electrons pass through an external load to produce power.

In this way, the amount of reformat gas produced in the reformer 2 is controlled to the amount corresponding to the load in the fuel cell 1, and therefore the amount of the mixed steam of methanol and water produced in the heating portion 3 is also controlled to the amount corresponding to the load in the fuel cell 1. The control apparatus of the invention controls the combustion in the combustion portion 6 as described below in order to heat and evaporate the reformat fuel depending on the load in the fuel cell 1.

Fig. 1 is a flowchart for explaining an exemplary embodiment of this control, in which, first, the amount F_k (mol/s) of reformat fuel (mixed liquid of methanol and water) is calculated (step 1). That is, on the basis of the detected value of the current sensor 20 showing the load of the fuel cell 1, the amount of reformat fuel corresponding to the hydrogen amount required in the fuel cell 1 for this load is determined. In this case, the S/C (steam/carbon) ratio is set, for example, typically at about two.

Next, the heating fuel is selected for heating and evaporating the determined amount of reformat fuel to be reformed. That is, the amount of reformat fuel is the amount to be gasified (step 2). As mentioned above, in the combustion portion 6,

combustion methanol and/or unreacted hydrogen gas are supplied to be burned, and therefore either one or both can be used for heating of the reformat fuel. In this case, when the reformat fuel can be heated and evaporated sufficiently by the unreacted hydrogen gas in the emission, only the unreacted hydrogen gas is supplied into the combustion chamber 21 to be used as the fuel for heating the reformat fuel. Therefore, the fuel can be utilized effectively, and the fuel economy may be enhanced.

When the unreacted hydrogen gas in the emission is used as the heating fuel, the amount of hydrogen to be supplied into the combustion portion 6 is determined. First, the necessary hydrogen amount F_{ho} (mol/s) for the reformat fuel amount F_k (mol/s) is determined (step 3). The operation is executed in the following manner.

By heating 1 (mol/s) of reformat fuel to obtain steam, the heat value H_r (kJ/mol) necessary for heating the steam temperature to the target temperature T_{er} ($^{\circ}\text{C}$) at which the activity of the catalyst in the reforming portion 4 is high (that is, the target temperature for generating reformat gas of high quality and high hydrogen gas concentration, for example, 280°C) is determined as follows:

$$H_r = H_{rm} + H_{rw}$$

where H_{rm} is the heat value necessary for methanol (kJ/mol) and H_{rw} is the heat value necessary for water (kJ/mol).

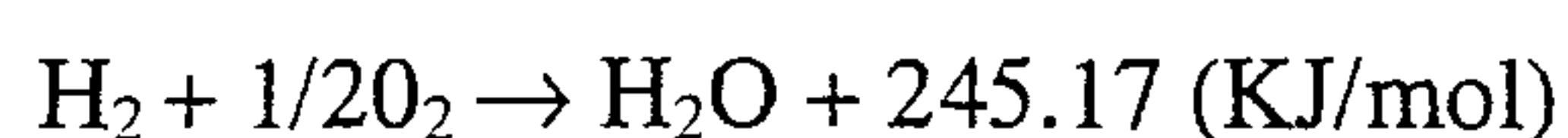
These necessary heat values H_{rm} , H_{rw} are determined by the following equations:

$$H_{rm} = 1 \times (C_{lm} \times (T_{bm} - T_a) + E_{bm} + C_{gm} \times (T_{er} - T_{br}))$$

$$H_{rw} = 2 \times (C_{lw} \times (T_{bw} - T_a) + E_{bw} + C_{gw} \times (T_{er} - T_{br}))$$

where C_{lm} is the mean specific heat capacity of methanol in the liquid phase (kJ/ $^{\circ}\text{C}$ /mol), C_{lw} is the mean specific heat capacity of water in the liquid phase (kJ/ $^{\circ}\text{C}$ /mol), E_{bm} is the evaporation latent heat of methanol (kJ/mol), E_{bw} is the evaporation latent heat of water (kJ/mol), C_{gm} is the mean specific heat capacity of methanol in the gas phase (kJ/ $^{\circ}\text{C}$ /mol), C_{gw} is the mean specific heat capacity of steam (kJ/ $^{\circ}\text{C}$ /mol), T_{bm} is the boiling point of methanol ($^{\circ}\text{C}$), T_{bw} is the boiling point of water ($^{\circ}\text{C}$), and T_a is the ambient temperature ($^{\circ}\text{C}$).

On the other hand, to burn hydrogen by using a catalyst in the combustion portion 6, the oxidation reaction at this time is expressed as:



and considering the necessary heat value H_r to be transmitted to the reformat fuel through the heat exchanger 12, the amount of unreacted hydrogen gas F_{ho} (mol/s) to be supplied as emission is determined by the equation:

$$F_{ho} = F_k \times H_r / 245.17 / \eta$$

5 where η is the heat exchange efficiency (typically about 0.7) of the heat exchanger 12.

As mentioned above, in step 1, a time delay occurs inevitably from the output of the command signal for supplying the determined amount of reformat fuel into the vaporizing portion 7 until this reformat fuel is evaporated. Such time delay is based on the mechanical structure of the pump 11 and vaporizing portion 7 and the chemical
10 reaction, and in step 4, therefore, the unreacted hydrogen gas amount is adjusted according to the delay. That is, supposing the delay time to be t , F_{ho} (mol/s) is adjusted as follows:

$$F_{ho}(t) = F_{ho}(t-\tau)$$

More specifically, according to the equation:

$$15 \quad F_{ho}' = F_{ho}(\text{old}) \times \tau / (DT + \tau) + F_{ho} \times DT / (DT + \tau)$$

where DT is the control period, and $F_{ho}(\text{old})$ is the hysteresis of F_{ho} of one control period before.

Moreover, when heating the reformat fuel by the heat generated by the combustion of unreacted hydrogen gas, it may not be achieved as initially expected due to effects of combustion efficiency or heat exchange efficiency. Accordingly, the
20 amount of unreacted hydrogen gas is adjusted according to the steam temperature at the outlet of the vaporizing portion 7 (step 5). An exemplary embodiment of a method of adjustment is described as follows. Assuming that the steam temperature detected by the steam temperature sensor 35 is T_e ($^{\circ}\text{C}$), the unreacted hydrogen gas amount F_{ho}'' is
25 determined in the equation:

$$F_{ho}'' = F_{ho}' + K_p \times (T_e - T_{er}) + K_i \times \Sigma(T_e - T_{er})$$

where K_p and K_i are control parameters, and $\Sigma(T_e - T_{er})$ is the integrated value of the target temperature and detected steam temperature deviation.

In another exemplary embodiment of adjustment, assuming F_{ho}'' is given by:

$$30 \quad F_{ho}'' = F_{ho}' + F_{hob}$$

the unreacted hydrogen gas amount F_{ho}'' can be adjusted. Herein,

$$\text{If } T_e - T_{er} > \varepsilon, \text{ then } F_{hob} = F_{ho}' + \Delta$$

$$\text{If } T_e - T_{er} < -\varepsilon, \text{ then } F_{hob} = F_{ho}' - \Delta$$

where ε and Δ are control parameters.

The emission amount F_o (mol/s) necessary for feeding the thus calculated amount F_{ho} of unreacted hydrogen gas into the combustion portion 6 and the opening degree V_o of the flow rate adjusting valve 23 are determined (step 6). First, the
 5 hydrogen gas amount F_h (mol/s) sent from the reformer 2 into the fuel cell 1 and the total reformat gas amount F_r (mol/s) are determined according to the respective equations:

$$F_h = K_h \times F_k$$

$$F_r = K_r \times F_r$$

10 where F_k is the reformat fuel amount determined at step 1 (mol/s), K_h is the hydrogen gas generating molar ratio to methanol (constant), and K_r is the reformat gas generating molar ratio to methanol (constant).

Next determined is the ratio R_h of the hydrogen gas in the emission sent from the fuel cell 1 to the return pipe 22. According to the equation:

15
$$R_h = (F_h - I_{fc}/(2 \times K_f))/(F_r - I_{fc}/(2 \times K_f))$$

where I_{fc} is the current value or the load of the fuel cell 1 detected by the current sensor 20, and K_f is the Faraday's constant.

From the determined rate R_h of the unreacted hydrogen gas in the emission and the necessary hydrogen gas amount F_{ho} , the necessary emission amount F_o (mol/s) is
 20 determined using the equation:

$$F_o = F_{ho}/R_h$$

In order to feed this determined emission gas flow rate F_o (mol/s) into the combustion chamber 24, the required opening degree V_o of the flow rate adjusting valve 23 is given by:

25
$$V_o = F_o/(c \times (P_o - P_b)^{1/2})$$

where c is the valve throttle coefficient, P_o is the pressure detected by the pressure sensor 26 at the upstream side of the flow rate adjusting valve 23 (that is, at the anode 15 side), and P_b is the pressure detected by the pressure sensor 27 at the downstream side of the flow rate adjusting valve 23 (that is, at the combustion portion 6 side). When
 30 fluctuations of these pressures P_o , P_b are small, predetermined constants can be used as estimates instead of the pressures actually detected by the sensors. In this case, the pressure sensors 26 and 27 are not necessary. The opening degree V_o of the flow rate adjusting valve 23 is controlled to the above value, and the unreacted hydrogen gas

necessary for heating the reformat fuel to a steam of desired temperature is supplied into the combustion portion 6.

Therefore, according to embodiments of the apparatus of the invention for controlling the feed amount of the unreacted hydrogen gas into the combustion portion 6, the reformat fuel depending on the load of the fuel cell 1 can be heated and evaporated, and a reformat fuel steam of a desired temperature can be obtained. As a result, the activity of the catalyst in the reforming portion 4 is maintained, and reformat gas of high quality can be produced at least substantially without producing carbon monoxide or residual methanol. Accordingly, poisoning of the catalyst and lowering of its durability is prevented. Moreover, the unreacted hydrogen gas inevitably occurring in the anode 15 of the fuel cell 1 (that is, flammable gas) can be utilized effectively, and the fuel economy is enhanced. In particular, by executing this control, the unreacted hydrogen gas is not consumed more than necessary, and hence the enhancing effect of fuel economy is excellent.

The heat generation temperature varies depending on the amount of air supplied into the combustion chamber 24 in relation to the amount of unreacted hydrogen gas, and therefore the air flow is controlled together with the control of the unreacted hydrogen gas amount. An exemplary embodiment of this control is shown in Fig. 2. In the control example shown in Fig. 2, first, the amount of the reformat fuel is determined (step 11). This is the same as the control in step 1 in Fig. 1, and therefore the value calculated in step 1 in Fig. 1 may be utilized in the control of Fig. 2. Next, the type of heating fuel to be supplied into the combustion portion 6 is selected (step 12). That is, as the fuel to be burned in the combustion portion 6, combustion methanol and/or unreacted hydrogen gas is selected. This is the same step as the control in step 2 in Fig. 1, and therefore the control in step 2 in Fig. 1 may be directly utilized in this control. Further heating the required amount of reformat fuel, the hydrogen gas amount necessary for obtaining steam at a desired temperature is determined (step 13). This is the same as the control in step 3 in Fig. 1, and therefore the determined result in step 3 in Fig. 1 may be directly utilized in this control. Because the amount of hydrogen gas supplied into the combustion portion 6 is adjusted, the hydrogen gas amount determined in step 3 and adjusted in steps 4 and 5 may be utilized. In the following explanation, however, an example of utilizing the hydrogen gas amount determined in step 3 is described.

On the basis of the hydrogen gas amount calculated in this step 13 and the optimum A/F (air/fuel) value, the air amount F_a as combustion aid gas is calculated (step 14). For complete oxidation of 1 mole of hydrogen, 1/2 mole of oxygen is needed, and the proportion of oxygen in air is about 1/5. Herein, the gas not presented for oxidation of hydrogen takes away the heat generated by combustion to the outside, and therefore an appropriate A/F value ($= \lambda_r$) is experimentally determined in advance on the basis of the steam temperature or the temperature of the combustion portion 6. Therefore, the air amount F_a necessary for combustion of hydrogen gas in the amount F_{ho} calculated in step 13 is determined as follows:

$$F_a = \lambda_r \times F_{ho}$$

In step 15, it is intended to determine the emission amount for feeding the necessary amount of unreacted hydrogen gas for heating the reformat fuel to obtain steam at a desired temperature into the combustion portion 6, and the opening degree of the flow rate adjusting valve 23 for obtaining such an emission amount. The control procedure is the same as for step 6 in the control in Fig. 1, and the calculated result at step 6 can be directly utilized in this control. In order to obtain such opening degree, a command signal is issued to the flow rate adjusting valve 23 (step 16). Also, a command value of the air pump 10 is issued to achieve the air value determined at step 14 (step 17).

Therefore, according to embodiments of the control apparatus of the invention for controlling as shown in Fig. 2, the amount of the air conforming to the required reformat fuel amount can be supplied into the combustion portion 6, and the temperature of the reformat fuel can be set to a temperature suited to the reforming reaction at the reforming portion 4. As a result, as for the control in Fig. 1, the reforming reaction of the reformat fuel can be promoted favorably, and a reformat gas of high quality is obtained. It is also possible to avoid poisoning or deterioration of the anode 15 or lowering of output of the fuel cell 1.

In the example of control shown in Fig. 2, the air amount is determined on the basis of the demanded unreacted hydrogen gas amount or its adjusted value and optimum A/F value, and the determined amount of air is supplied. In actual operation, however, the expected reaction or heat generation may not always occur due to various factors, and the steam temperature may deviate. Therefore, as for the control example

shown in Fig. 1, the air amount may be adjusted. An example of such adjustment is explained in the following exemplary embodiment.

For use in the heating of reformat fuel, in order to enhance the fuel economy, the emission produced at the anode 15 side of the fuel cell 1 is mixed with unreacted hydrogen gas at a specified rate. In this case, on the basis of the reformat fuel amount, the valve opening degree to determine the flow rate of the emission to the combustion portion 6 can be controlled. That is, the opening degree of the flow rate adjusting valve 23 is determined on the basis of the reformat fuel amount corresponding to the load of the fuel cell 1. In this case, the amount of air supplied into the combustion portion 6 is controlled as follows.

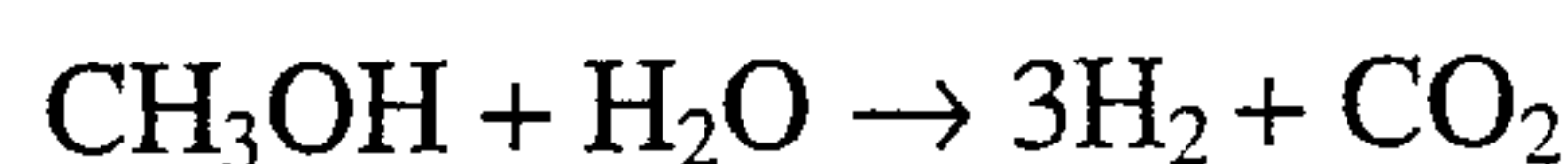
Fig. 3 shows an exemplary embodiment of control. First, the opening degree of the flow rate adjusting valve 23 of the emission is determined (step 21). From the heat value necessary for heating the reformat fuel in the amount calculated depending on the load of the fuel cell 1 to obtain steam at desired temperature, the amount of the unreacted hydrogen gas is determined, and the amount of emission containing it by a specified content is determined. Hence, the opening degree of the flow rate adjusting valve 23 is calculated so as to obtain this emission amount. In this control, the control gain can be determined in advance, and the flow rate adjusting valve can be immediately determined on the basis of the control gain according to the reformat fuel amount.

Next, the amount of air as combustion aid gas is determined. First, the hydrogen gas amount F_h (mol/s) to be sent into the fuel cell 1 and the total amount of reformat gas (mol/s) are estimated as follows:

$$F_h = K_h \times F_k$$

$$F_r = K_r \times F_k$$

This is the same as the determination made at step 6 in Fig. 1. The reforming reaction using methanol is given by:



hence $K_h = 3$ and $K_r = 4$.

Next, the rate R_h of hydrogen gas in the emission sent from the fuel cell 1 into the return pipe 22 is determined by:

$$R_h = (F_h - I_{fc}/(2 \times K_f))/(F_r - I_{fc}/(2 \times k_f))$$

This is same as the determination made in the process of determining the opening degree of the flow rate adjusting valve 23 in the control shown in Fig. 1.

On the other hand, the total amount F_o (volume flow rate) of emission supplied into the combustion portion 6 through the flow rate adjusting valve 23 is determined as follows:

$$F_o = V_o \times c \times (P_o - P_b)^{1/2}$$

where V_o is the opening degree of the flow rate adjusting valve 23, c is the valve throttle coefficient, P_o is the pressure detected by the pressure sensor 26 at the upstream side of the flow rate adjusting valve 23, that is, at the anode 15 side, and P_b is the pressure detected by the pressure sensor 27 at the downstream side of the flow rate adjusting valve 23, that is, at the combustion portion 6 side. When fluctuations of these pressures P_o and P_b are small, predetermined constants can be used as estimated values instead of the pressures actually detected by the sensors. In this case, the pressure sensors 26, 27 are not required.

On the basis of the thus calculated emission amount F_o and hydrogen gas rate R_h , the hydrogen gas amount F_{ho} to be supplied into the combustion portion 6 is determined as follows:

$$F_{ho} = F_o \times R_h$$

For more accurate control, on the basis of the time delay from the supply of reformat fuel until the start of reaction, the unreacted hydrogen gas amount is adjusted. Assuming that the reaction delay is expressed by a primary delay system, the delay characteristic $G_r(s)$ is given by:

$$G_r(s) = 1/(1 + T_r \times s) \times \exp(-L_r \times s)$$

where T_r is the primary delay constant, L_r is the reforming portion gas transport delay time, and s is a Laplacian operator.

The gas transport delay characteristic $G_f(s)$ in the fuel cell 1 is determine by:

$$G_f(s) = \exp(-L_f \times s)$$

where L_f is the gas transport delay time in the fuel cell 1. On the basis of these delay characteristics $G_r(s)$, $G_f(s)$, the hydrogen gas amount F_{ho} is adjusted according to the following equation:

$$F_{ho}' = F_{ho} \times G_r(s) \times G_f(s)$$

In the above description, each delay characteristic is described in the form of a Laplace transform, but the actual determination in the ECU 36 is executed by transforming into a discrete type.

On the basis of the thus determined estimated hydrogen gas amount F_{ho}' , the air amount F_a is determined (step 23). For complete oxidation of 1 mole of hydrogen, 1/2 mole of oxygen is required, and the proportion of oxygen in air is about 1/5. The gas that is not subjected to oxidation of hydrogen can take away the heat generated by combustion to the outside, and therefore an appropriate A/F (air/fuel) value ($= \lambda_r$) can be experimentally determined in advance on the basis of the steam temperature or temperature of the combustion portion 6. Therefore, the air amount F_a required for combustion of hydrogen gas in the amount F_{ho}' estimated in step 22 is determined as follows:

$$F_a = \lambda_r \times F_{ho}'$$

Because the actually supplied air amount may deviate from the target value, the air amount is adjusted on the basis of the oxygen concentration N_o in the emission exhausted from the combustion chamber 24 (step 24). That is, by the A/F sensor 34 disposed in the exhaust pipe 33 provided at the downstream side of the combustion chamber 24, the oxygen concentration N_o in the gas exhausted from the combustion chamber 24 is detected. On the other hand, in the case of complete reaction for the supplied air amount F_a , the target oxygen concentration N_{or} in the emission is determined, and the supplied air amount is adjusted so that the detected oxygen concentration N_o coincides with the target oxygen concentration N_{or} . It is the same meaning as the ratio of the unreacted hydrogen gas supplied in the combustion chamber 24 and the oxygen is detected and the supplied air amount is adjusted accordingly. As an example of adjustment, using the equation:

$$F_a' = F_a + K_{p1} \times (N_o - N_{or}) + K_{i1} \times \Sigma(N_o - N_{or})$$

the adjusted air amount F_a' is determined. Herein, K_{p1} and K_{i1} are control parameters, and $\Sigma(N_o - N_{or})$ is the integrated value of the deviation of the measured oxygen concentration and target oxygen concentration.

In other example of adjustment, according to the equation:

$$F_a' = F_a + F_b$$

the air amount F_a' is adjusted. Herein,

$$\text{If } N_o - N_{or} > \varepsilon_1, \text{ then } F_b = F_b + \Delta_1$$

where ϵ_1 and Δ_1 are control parameters.

This air amount may be further adjusted on the basis of the transport and reaction delay of the reformat fuel. In this case, the air amount adjusted on the basis of the response delay of the reformat fuel may be further adjusted according to the
5 detected value of the A/F sensor 34.

Moreover, the degree of promotion of combustion of unreacted hydrogen gas differs with the temperature at the combustion portion 6, and therefore in order to maintain a suitable temperature at the combustion portion 6, the air amount is adjusted according to the detected temperature (step 25). As mentioned above, the heat
10 generation temperature of each oxidation catalyst 31 in the combustion portion 6 is detected by the temperature sensors 32, and the average temperature or the maximum temperature of the temperatures detected by the temperature sensors 32 is used as a representative temperature T_b of the detected temperatures. Depending on the representative temperature T_b , the target A/F value (λ_r) is varied. The target A/F value
15 λ_r may be determined either by calculation or by using a map. An example of such a map is shown in Fig. 4.

That is, if the detected representative value T_b exceeds a predetermined specified temperature $\alpha^\circ\text{C}$, the target A/F value λ_r value is set to a larger value depending on the temperature. When exceeding other specified temperature b , the
20 target A/F value λ_r is maintained at a specified upper limit value. That is, within a specified temperature range, the higher is the detected temperature of the combustion portion 6, the greater is the air amount to keep the combustion fuel in a so-called lean state, and to the contrary the lower is the detected temperature of the combustion
portion 6, the less is the air amount to set relatively in a so-called rich state. As a result,
25 if the temperature tends to be excessively high, the combustion amount of the unreacted hydrogen gas is suppressed, such that the heat taken away by the exhaust increases, and the temperature rise in the combustion portion 6 is suppressed. On the contrary, when the temperature tends to decline, the combustion amount of the unreacted hydrogen gas increases, such that the heat taken away by the exhaust decreases, and the temperature
30 becomes higher.

Consequently, to adjust to the opening degree of the flow rate adjusting valve 23 determined in step 21, a command signal is issued from the ECU 36 to the flow rate adjusting valve 23 (step 26). To adjust the air amount corresponding to the combustion

portion 6 to the above amount, a command signal is issued from the ECU 36 to the air pump 10 (step 27). These steps 26 and 27 are the same as the control in steps 16 and 17 in Fig. 2.

Therefore, according to the control apparatus of the invention for executing the exemplary embodiment of control shown in Fig. 3, when heating the reformat fuel by supplying unreacted hydrogen gas into the combustion portion 6, the unreacted hydrogen gas amount can be set to an amount suited to the reformat fuel amount. At the same time, depending on the amount of the unreacted hydrogen and adjusted depending on the actual heating temperature or the like, a proper amount of air is supplied into the combustion portion 6. Thus, the unreacted hydrogen gas can be utilized effectively, and the temperature of the reformat fuel can be maintained at a temperature suited to the reforming reaction. As a result, the reforming reaction proceeds favorably, and the reformat gas of high quality is produced, power generation efficiency of the fuel cell 1 is enhanced and poisoning and deterioration of the catalyst can be prevented at the same time.

Fig. 5 is a flowchart showing another exemplary embodiment of control. As shown, first, the amount of the reformat fuel (mixture of methanol and water) is determined (step 31). The hydrogen gas used in the fuel cell 1 is produced by the reaction shown in equations (1) and (2), and therefore it can be determined based on the reforming rate, the utility rate of hydrogen gas in the fuel cell 1, or the Faraday's constant.

The selecting condition of the combustion material to be supplied into the combustion portion 6 is determined (step 32). More specifically, when the logical multiplication (AND) of 3 conditions is established, that is, (A) the opening degree V_o (%) of the flow rate adjusting valve 23 is higher than the predetermined maximum value V_{ou} , (B) the steam temperature T_e ($^{\circ}\text{C}$) of the reformat fuel is lower than the predetermined minimum limit temperature T_{el} , and (C) the control flag F_{ac} is OFF, the combustion methanol as heating fuel is additionally supplied. In other words, when these three conditions are established, although the unreacted flammable gas (hydrogen in the emission) is supplied to the combustion portion 6 to the maximum extent, the reformat fuel temperature is lower than the lower limit value, and the heat generation at the combustion portion 6 is insufficient. Accordingly, in addition to the unreacted flammable gas, combustion methanol is additionally supplied into the combustion portion 6 such that the heat generation capacity is increased. That is, so-called assist

control is executed using the combustion methanol. At the same time, the control flag Fac is turned ON.

Meanwhile, when the logical multiplication (AND) of three conditions is established, that is, (i) the command value τ (%) to the injector 9 for controlling the combustion methanol amount is equal to or lower than 0%, (ii) the reformat fuel steam temperature T_e ($^{\circ}\text{C}$) is higher than the upper limit temperature T_{eu} , and (iii) the control flag Fac is ON, the assist control is terminated. That is, in a state where these three conditions are established, in spite of stopping the supply of combustion methanol, the heat generation in the combustion portion 6 is still higher than the heat required for heating the reformat fuel. Therefore, the assist control of supplying the combustion methanol to the combustion portion in addition to the unreacted flammable gas (hydrogen in the emission) is stopped. At the same time, the control flag Fac is turned OFF.

Fig. 6 shows the time chart in the case where the selecting condition of the combustion material to the combustion portion 6 is determined and the reformat fuel is heated. That is, with the opening degree V_o of the flow rate adjusting valve 23 set at the maximum value V_{ou} , when the steam temperature (reformat fuel temperature) T_e becomes lower than the lower limit value T_{el} (time t_1), because the heat generation in the combustion portion 6 is insufficient, supply of combustion methanol is started. That is, the injector command value τ is set at a specified value, and the control flag Fac is turned ON.

As a result, in the combustion portion 6, combustion of unreacted flammable gas (hydrogen in the emission) and combustion methanol occurs, and as the material fuel is increased, the heat generation capacity in the combustion portion 6 increases. In this case, depending on the steam temperature, the injector command value τ , that is, the combustion methanol amount is controlled.

When the steam temperature gradually increases by an increase of heat generation in the combustion portion 6, or a decrease of the amount of the reformat fuel, the injector command value τ (combustion methanol amount) is lowered accordingly, and at time t_2 when the reformat fuel steam temperature reaches the upper limit temperature T_{eu} , the injector command value τ drops to 0%. In this state, when the reformat fuel steam temperature is higher than the upper limit temperature T_{eu} ,

supply of combustion methanol, that is, assist control, is terminated, and the control flag Fac is turned OFF.

Later, in order to set the reformat fuel steam temperature T_e to the target temperature, the opening degree of the flow rate adjusting valve 23 for emission is decreased depending on the temperature T_e , and the reformat fuel is heated only by the unreacted flammable gas.

Because there is a response delay from the change of heat generation in the combustion portion 6 until the actual change of temperature of the reformat fuel, it is preferable to set a specified temperature difference (for example, 30°C) between the upper limit temperature T_{eu} and the lower limit temperature T_{el} , in order to prevent hunting in control due to a supply or stop of combustion methanol and a change of emission amount.

Thus, basically, the reformat fuel is heated by burning the unreacted flammable gas. Accordingly, the amount of unreacted flammable gas or hydrogen in emissions that can be consumed in the combustion portion 6 is determined (step 33). It is determined, for example, from the amount of hydrogen gas supplied into the fuel cell 1 and the consumption of hydrogen gas assessed on the basis of the electric power supplied to the outside.

In the case of combustion of unreacted flammable gas (hydrogen gas), the heat generation per unit amount is known, and by considering the efficiency when heating the reformat fuel by this heat, the amount of emission necessary for heating the reformat fuel is known. In step 34, hence, the opening degree of the flow rate adjusting valve 23 is determined. When the assist control is executed, that is, when the control flag Fac is turned ON, the opening degree of the flow rate adjusting valve 23 is fixed at the upper limit value V_{ou} . By contrast, when the assist control is not executed, that is, the control flag Fac is turned OFF, the opening degree is determined on the basis of the amount of emission required for heating the reformat fuel. The opening degree is, for example, determined on the basis of the emission amount containing the required amount of unreacted flammable gas, valve throttle coefficient, and the pressure difference between the upstream side and downstream side of the flow rate adjusting valve 23.

On the other hand, if it is impossible to heat the reformat fuel sufficiently by the unreacted flammable gas alone, combustion methanol is additionally supplied into the combustion portion 6 to burn, and the amount of this combustion methanol is

calculated (step 35). Because the heat generation by oxidation of combustion methanol is known, the combustion methanol amount can be determined on the basis of the specific heat or evaporation latent heat of the reformat fuel, amount of reformat fuel, heat transfer rate to the reformat fuel, target temperature of reformat fuel, and
5 adjustment amount due to control delay. This combustion methanol amount is determined by the feedback control on the basis of the reformat fuel steam temperature.

A command signal is sent to the injector 9 so that the thus determined amount of combustion methanol can be supplied into the combustion portion 6 (step 36). In this
10 case, the pump 8 is controlled so that the upstream side temperature of the injector 9 can be a substantially constant pressure (for example, about 2 atm). This is intended to keep a constant relation between the command value to the injector 9 and the displacement, and therefore the amount of combustion methanol supplied by the injector 9 becomes accurate.

15 Such feedback control of the combustion methanol amount is limited only when the control flag Fac is turned ON, that is, the assist control by combustion methanol is executed, and otherwise when the control flag Fac is turned OFF and the assist control is not executed, the command value to the injector 9 is fixed at 0%.

According to embodiment of the control apparatus of the invention for
20 controlling as described above, the reformat fuel is heated by using the unreacted flammable gas produced inevitably from the energy converter for using the reformat fuel such as fuel cell 1 and producing energy in a different form, and only when the heating calorific value is insufficient, heating fuel such as methanol is added to burn. Therefore, the fuel is utilized effectively, enhancing the thermal efficiency. At the same
25 time, because the temperature of the reformat fuel can be maintained at a target temperature, a steam reforming reaction or partial oxidation reforming reaction can be promoted to obtain a reformat gas of high quality, so that poisoning by carbon monoxide in the fuel cell 1 can be decreased.

In this example, an excess or deficiency of heat, and the necessity of additional
30 combustion are judged on the basis of the reformat fuel steam temperature. However, the heat value required for heating the reformat fuel and the heat value obtained by burning the unreacted flammable gas can be both assessed on the basis of the running conditions of the reformer 2, and therefore an excess or deficiency of heating calories and the necessity of additional combustion can be determined from the running

conditions of the reformer 2 without referring to the reformat fuel steam temperature. Therefore, the step 32 can be replaced by the step of selecting the combustion material on the basis of the assessment of such heat values and comparison of the results of assessment.

5 In the case of combustion by supplying unreacted flammable gas or combustion methanol into the combustion portion 6, the combustion reaction, heat transfer to the reformat fuel, or release of heat to the outside is not uniform at all positions, and temperature variations inevitably occur. If a high temperature occurs locally due to such temperature variations, high-heat damage can occur in such location, which can be
10 prevented by the control described below.

Fig. 7 is a flowchart showing an example, in which, first, the emission target flow rate and combustion methanol target flow rate are determined in steps 41 and 42. This is executed according to the control shown in Fig. 5, and when the assist control has been executed, the emission flow rate is fixed at the value of setting the opening
15 degree of the flow rate adjusting valve 23 at the upper limit value V_{ou} , or if the assist control has not been executed, it is determined on the basis of the target temperature of the reformat fuel and its amount. In the case where the assist control has been executed, the flow rate of the combustion methanol is determined on the basis of the temperature of the reformat fuel or the shortage of heat required for heating the
20 reformat fuel to the target temperature.

Consequently, depending on whether the assist control has been executed or not, the emission flow rate and/or combustion methanol flow rate is adjusted (steps 43 and 44). More specifically, if the assist control has not been executed, the emission flow rate is adjusted, and if the assist control has been executed, the flow rate of combustion
25 methanol is adjusted.

These flow rate adjustments are performed on the basis of the temperature of the combustion portion 6. That is, by the temperature sensors 32, the temperatures T_{b1} , T_{b2} , ..., T_{bn} of parts of the combustion portion 6 are detected, and the representative temperature T_{bm} is determined from the detected temperatures T_{b1} , T_{b2} , ..., T_{bn} . This
30 representative temperature T_{bm} can be the temperature at the position most likely to in the combustion portion 6, or the maximum value of the detected temperatures T_{b1} , T_{b2} , ..., T_{bn} . By setting the adjustment coefficients K_o , K_m depending on the representative temperature T_{bm} , each flow rate is adjusted by multiplying the flow rates

Q_o , Q_m assessed in step 41 or 42 by the adjustment coefficient. That is, the emission flow rate is adjusted as:

$$Q_o' = K_o \times Q_o,$$

and the flow rate of combustion methanol is adjusted as:

5 $Q_m' = K_m \times Q_m.$

As the adjustment coefficients K_o , K_m , the values preliminarily set in the form of map can be used, and more specifically the values shown in Fig. 8A and Fig. 8B can be used. That is, when the representative temperature T_{bm} is lower than the first reference temperature T_1 lower by specified temperature than the allowable upper limit temperature of the combustion portion 6, the adjustment coefficients K_o , K_m are "1".
10 And, in a range higher than the first reference temperature T_1 and to the second reference temperature T_2 lower than the allowable upper limit temperature, the adjustment coefficients K_o , K_m decreases from "1" to "0" depending on the increase of the representative temperature T_{bm} . The adjustment coefficients K_o and K_m are set at
15 "0" at temperature higher than the second reference temperature T_2 .

The air amounts corresponding to the emission amount containing the unreacted flammable gas and combustion methanol amount thus determined are assessed (step 45). The oxygen amount required for completely burning the unreacted flammable gas and combustion methanol can be known by the formula of the oxidation reaction.
20 Because the oxygen concentration in the air is known and the temperature in the oxidation reaction can be assumed preliminarily, the required air amount, or the air/fuel ratio (A/F) can be determined from the unreacted flammable gas amount and combustion methanol amount.

In this manner, the emission flow rate, combustion methanol flow rate, and air amount are determined, and corresponding command values can be issued. That is, an opening degree command signal for obtaining the emission flow rate is issued to the flow rate adjusting valve 23 disposed in the return pipe 22 (step 46), a command signal for obtaining the combustion methanol amount is issued to the injector 9 (step 47), and a command signal is issued to the air pump 10, so as to obtain the calculated air amount
25 (step 48).
30

Changes of representative temperature of the combustion portion 6 in the case of the embodiment of control as shown in Fig. 7 are shown in Fig. 9D, Fig. 9E and Fig. 9F together with a comparative example. Fig. 9A, Fig. 9B and Fig. 9C show a comparative example, showing a case without executing flow rate adjustment. Fig. 9A

shows changes of the reformat fuel steam temperature, Fig. 9B shows changes of the representative temperature T_{bm} of the combustion portion 6 and Fig. 9C shows changes of the emission amount Q_o . Fig. 9D, Fig. 9E and Fig. 9F show changes of representative temperature of the combustion portion 6 in the case of executing flow rate adjustment as shown in Fig. 7. Fig. 9D shows changes of the reformat fuel steam temperature, Fig. 9E shows changes of the representative temperature T_{bm} of the combustion portion 6 and Fig. 9F shows changes of the emission amount Q_o . As shown in Fig. 9A, Fig. 9B and Fig. 9C, the comparative example in which along with the decline of the reformat fuel steam temperature, the emission amount Q_o is increased, and the representative temperature T_{bm} of the combustion portion 6 exceeds the allowable upper limit temperature after the specified delay time. By contrast, Fig. 9D, Fig. 9E and Fig. 9F show an example of flow rate adjustment, in which if the emission amount Q_o increases due to a decline of the reformat fuel steam temperature, the flow rate is decreased as soon as the representative temperature T_{bm} becomes higher than the first reference temperature T_1 , and the heat generation in the combustion portion 6 decreases, and therefore the representative temperature T_{bm} of the combustion portion 6 does not exceed the allowable upper limit temperature.

Therefore, according to embodiments of the control apparatus for controlling in this manner, if the reformat fuel amount changes due to fluctuations of the load of the fuel cell 1 and accordingly the heat value required in the combustion portion 6 or the supply amount of combustion material changes, a local overheat state in the combustion portion 6 can be avoided, and high-heat damage or other abnormality in the combustion portion 6 can be prevented.

The control apparatus of the invention controls the flow rate of the emission by adjusting the opening degree of the flow rate adjusting valve 23 disposed in the intermediate portion of the return pipe 22 in the state capable of sufficiently heating the reformat fuel by the unreacted flammable gas, that is, when the assist control is not executed. In this case, the target combustion temperature is set according to the target steam temperature of the reformat fuel, and further depending on the target combustion temperature, the emission flow rate is set. At the same time, as mentioned above, the flow rate is adjusted according to the allowable upper limit temperature in the combustion portion 6. This is the same either when using only the unreacted flammable gas as the combustion material or when using it together with the combustion methanol. In this embodiment, the preferred controller is as follows.

Fig. 10 shows an exemplary embodiment of a controller of the emission flow rate, which comprises a steam temperature controller 51, a combustion temperature controller 52, and an emission flow rate adjusting valve controller 53. Each one of these controllers 51, 52, 53 typically comprises a microcomputer, and the steam
5 temperature controller 51 sets the target combustion temperature T_{br} so that the steam temperature T_e can be the target temperature T_{er} on the basis of the target steam temperature T_{er} and the detected reformat fuel steam temperature T_e . Herein, the target steam temperature T_{er} is the temperature on the basis of the active temperature in the reforming portion 4 (for example, about 330°C).

10 The combustion temperature controller 52 sets the emission flow rate Q_o by calculating on the basis of the input data by receiving the target combustion temperature T_{br} from the steam temperature controller 52 and the detected combustion temperature T_b . The emission flow rate adjusting valve controller 53 controls the opening degree of the flow rate adjusting valve 23 on the basis of the emission flow rate entered from the
15 combustion temperature controller 52.

Fig. 11 shows an exemplary embodiment of a controller for flow rate control of the combustion methanol, which comprises a steam temperature controller 61, a combustion temperature controller 62, and an injector controller 63. Each one of these controllers 61, 62, 63 typically comprises a microcomputer, and the steam temperature
20 controller 61 sets the target combustion temperature T_{br} so that the steam temperature T_e can be the target temperature T_{er} on the basis of the target steam temperature T_{er} and the detected reformat fuel steam temperature T_e . Herein, the target steam temperature T_{er} is the temperature on the basis of the catalyst active temperature in the reforming portion 4 (for example, about 330°C).

25 The combustion temperature controller 62 sets the combustion methanol amount Q_{bm} on the basis of the input data by receiving the target combustion temperature T_{br} from the steam temperature controller 61 and the detected combustion temperature T_b . The injection controller 63 controls the feed amount of the combustion methanol by the injector 9 on the basis of the combustion methanol amount Q_{bm}
30 entered from the combustion temperature controller 62. Herein, meanwhile, the steam temperature controllers 51, 61, and the combustion temperature controllers 52, 62 may each be used commonly.

The process of determining the target combustion temperature T_{br} by the steam temperature controllers 51, 61 is nearly the same, which is shown in Fig. 12. First, the

nominal value T_{brff} of the target combustion temperature is determined (step 71). This is obtained, for example, from the map shown in Fig. 13. The map shown in Fig. 13 specifies the relationship between the amount of the mixed liquid of reformat methanol and water, and the target value of the combustion temperature required for heating to this target steam temperature T_{er} , and it is determined by experiment or by calculation of heat value. Therefore, once the flow rate of the reformat fuel is determined, the nominal value T_{brff} of the target combustion temperature is determined from this map. As this target combustion temperature, the average temperature or representative temperature of the parts in the combustion portion 6 is employed.

Next, the target combustion temperature is adjusted (step 72). That is, if the target combustion temperature T_{br} is set as the nominal value T_{brff} , the steam temperature T_e may not be the target steam temperature T_{er} due to a shortage of heat required for generation of heat depending on the ambient temperature, temperature of the reformat fuel, or fluctuations of the device such as flow rate adjusting valve 23 or injector 9. In step S22, the steam temperature T_e is adjusted to avoid this. For example, the adjustment value T_{brfb} is determined as:

$$T_{brfb} = K_{pe}(T_e - T_{er}) + K_{ie} \Sigma(T_e - T_{er})$$

where K_{pe} and K_{ie} are predetermined control parameters, $\Sigma(T_e - T_{er})$ is the integrated value of the deviation of the target value and detected value of reformat fuel steam. In another adjustment example, adjustment values are determined as follows:

$$\text{If } T_e - T_{er} < -\epsilon_e, \text{ then } T_{brfb} = T_{brfb} + \Delta_e$$

$$\text{If } T_e - T_{er} > \epsilon_e, \text{ then } T_{brfb} = T_{brfb} - \Delta_e$$

where ϵ_e and Δ_e are predetermined control parameters.

Next, adding the adjustment value T_{brfb} to the nominal value T_{brff} , the target combustion temperature T_{br} is determined (step 73) by:

$$T_{br} = T_{brff} + T_{brfb}$$

Further, to prevent high-heat damage of the combustion portion 6, the upper limit guard is set (step 74). That is, from the T_{br} determined as:

$$T_{br} = \min(T_{br}, T_{brMAX})$$

and the predetermined upper limit value T_{brMAX} , the smaller value is employed. In the temperature controllers 51, 61, by executing the control in steps 71 to 74, the target combustion temperature T_{br} is set.

Meanwhile, the calculation process of the emission flow rate and combustion methanol amount in the combustion temperature controllers 52, 62 is similar as shown in Fig. 14. First, the target amount of the emission containing the unreacted flammable gas or the combustion methanol (hereinafter, these are referred to as the "combustion material target") is determined (step 81). It can be obtained from the map, for example, shown in Fig. 15. The map shown in Fig. 15 is a three-dimensional map determining the combustion material flow rate from the target combustion temperature and the amount of mixed liquid of reformat methanol and water. This map is determined either by experiment or by calorific calculation. Therefore, the target combustion temperature is determined according to the routine shown in Fig. 12, and the reformat fuel amount is determined according to the load of the fuel cell 1, and therefore the nominal value Q_{bmff} (Q_{off}) of the combustion material flow rate is determined from the map shown in Fig. 15.

Corresponding to this nominal value Q_{bmff} (Q_{off}), the adjustment value Q_{bmf} (Q_{of}) is determined (step 82), and it is adjusted by the adjustment value Q_{bmf} (Q_{of}) (step 83). These steps 82 and 83 correspond to the steps 72 and 73 shown in Fig. 12, and the adjustment value can be determined and adjusted the same as explained in the steps 72 and 73. That is, the control value, for example, is calculated as

$$Q_{bmf} (Q_{of}) = K_{pb}(T_b - T_{br}) + K_{ib} \Sigma(T_b - T_{br})$$

where K_{pb} and K_{ib} are predetermined control parameters, $\Sigma(T_b - T_{br})$ is the integrated value of the deviation of the target value and detected value of the combustion temperature. In another adjustment example, adjustment values are determined as follows:

$$\text{If } T_b - T_{br} < -\varepsilon_b, \text{ then } Q_{bmf} (Q_{of}) = Q_{bmf} (Q_{of}) + \Delta_b$$

$$\text{If } T_b - T_{br} > \varepsilon_b, \text{ then } Q_{bmf} (Q_{of}) = Q_{bmf} (Q_{of}) - \Delta_b$$

where ε_b and Δ_b are predetermined control parameters.

Next, adding the adjustment value Q_{bmf} (Q_{of}) to the nominal value Q_{bmff} (Q_{off}), the target combustion material amounts Q_{bm} , Q_o are determined (step 83) as follows:

$$Q_{bm}(Q_o) = Q_{bmff}(Q_{off}) + Q_{bmf}(Q_{of})$$

In order to achieve the thus obtained combustion material flow rate, the opening degree of the flow rate adjusting valve 23 or the injection amount of the injector 9 is controlled (step 84). It can be determined from the map, for example, by determining

the relation between the flow rate and command value of the combustion material experimentally with respect to the flow rate adjusting valve 23 and injector 9 and forming a map as shown in Fig. 15.

Therefore, as shown above, the combustion controllers 52, 62 are provided independently, and the flow rate control of the combustion material is executed in consideration of the upper limit temperature in the combustion portion 6 by the combustion temperature-controllers 52, 62, thereby preventing an excessively high combustion temperature or high-heat damage of the combustion portion 6. Moreover, because the flow rate control of the combustion material by the combustion temperature controllers 52, 62 is based on the target combustion temperature by the steam temperature controllers 51, 61, the steam temperature of the reformat fuel is adequately controlled, and the reforming efficiency is enhanced, and deterioration of catalyst in the reforming portion 4 can be prevented.

The air supplied into the combustion portion 6 is not particularly preheated, and it functions as a coolant for the combustion portion 6. The air introduced into the combustion portion 6 is raised in temperature by combustion, and flows into the exhaust side in this state, so that the heat is carried into the exhaust side. As a result, depending on the manner of feed of air, the temperature distribution in the combustion portion 6 varies, and hence the air can be used in control of temperature distribution in the combustion portion 6. Such example is explained below.

When heating the reformat fuel by the heat generated in the combustion portion 6, as mentioned above, a specified command value is issued to the flow rate adjusting valve 23, injector 9 or air pump 10 in order to realize the flow rates by determining the flow rate of the emission including the unreacted flammable gas, amount of combustion methanol, and the amount of air required for combustion, on the basis of the reformat fuel amount or its target steam temperature. The control example shown in Fig. 17 also adjusts the flow rate on the basis of the detected temperature of the combustion portion.

More specifically, determination of the target flow rate of the emission (step 91), determination of the target flow rate of the combustion methanol (step 92), and determination of the air flow rate (step 93) are executed in the same way as explained in Fig. 7. Then, the air flow rate is adjusted (step 94).

A sub-routine of this step 94 is shown in Fig. 18. First, the target temperature gradient A_r in the combustion portion 6 is determined (step 94-1). That is, the target

combustion temperature distribution in the longitudinal direction in the combustion portion 6 (the direction from the inflow side to the exhaust side of the air and combustion material) is determined by experiment or by thermal calculation in each flow rate of the reformat fuel. The temperature distribution is approximately linear, and the slope is obtained as the target temperature gradient A_r . An example of a thus set map of temperature distribution is shown in Fig. 19.

On the other hand, by linearly approximating the temperatures T_{b1} , T_{b2} , ..., T_{bn} of the parts of the combustion portion 6 detected by the temperature sensors 32, the gradient A of the temperature distribution is determined (step S94-2). The linear approximation is achieved, for example, by the method of least squares.

On the basis of thus obtained temperature gradient A and target temperature gradient A_r , the adjustment amount of air Q_{afb} is determined (step 94-3). For example,

(i) In the case of $A - A_r > \varepsilon$, $Q_{afb} = \max(Q_{afb} - \Delta, Q_{afbMIN})$

(ii) In the case of $A - A_r < -\varepsilon$, $Q_{afb} = \min(Q_{afb} + \Delta, Q_{afbMAX})$

where ε and Δ are control parameters.

That is, in the case of (i), the temperature of the exhaust side (downstream side) is high, and in this case, the larger value of either the value by subtracting the specified value Δ or the adjustment minimum value Q_{afbMIN} is employed as the adjustment value Q_{afb} . In the case of (ii), the temperature of the exhaust side (downstream side) is low, and in this case, the smaller value of either the value by adding the specified value Δ or the adjustment maximum value Q_{afbMAX} is employed as the adjustment value Q_{afb} . By adding the adjustment value Q_{afb} to the air amount Q_a determined in step 93, the air amount is adjusted (step 94-4).

In succession, command signals are issued to the flow rate adjusting valve 23, injector 9, and air pump 10 (steps 95, 96, 97) such that the emission amount, combustion methanol amount and air amount may be the values determined above.

By controlling in this manner, if the air inflow side temperature is high, the air supply amount is increased, and the inflow side temperature is lowered by its cooling action, and the exhaust side temperature is raised. In the opposite case, the air inflow amount is decreased, and the inflow side temperature is higher, and the exhaust side temperature drops, so that the temperature is adjusted to the target distribution. That is, local temperature elevation in the combustion portion 6 is prevented, and high-heat loss or other inconvenience of the combustion portion 6 can be avoided.

In the foregoing examples, the invention is applied to the control apparatus for the reformer that feeds fuel to the fuel cell 1, but the invention is not limited to the illustrated examples alone, and the device for feeding reformat gas, that is, the energy converter may be selected as required. As the reformat fuel, methanol and water are shown, but embodiments of the reformer of the invention can also be used to reform other hydrocarbon. Further in the illustrated examples, the required amount of the reforming reaction is the amount of the reformat fuel to be supplied into the reforming portion. However, according to the invention, other parameters in corresponding relation to the reformat fuel amount, for example, the current as the load to the fuel cell 1 can be also used as the required amount of the reforming reaction. In the foregoing examples, the heating portion is structured as shown in Fig. 21, but the heating portion in the reformer in the invention is not particularly limited in structure, so long as it can heat the reformat fuel by the heat accompanying the oxidation of heating fuel, and thus it is not limited in structure to the structure shown in Fig. 21. Moreover, the heating fuel usable in the invention is not limited to methanol, and various other fuels can also be used as desired for heating the reformat fuel.

The illustrated examples relate to the reformer for feeding air to the reformer to cause a partial oxidation reaction, and producing the heat suited to the endothermic amount in the reforming reaction by a partial oxidation reaction, and maintaining the temperature of the reforming portion substantially at a constant level. Although the invention is particularly effective when applied to the reformer for this kind of partial oxidation reaction, it can be also applied to the control apparatus for the reformer of the type that does not produce a partial oxidation reaction.

In the above described embodiments, the various controllers that are described are implemented as programmed general purpose computers. It will be appreciated by those skilled in the art, however, that the controller can be implemented using a single special purpose integrated circuit (e.g., ASIC) having a main or central processor section for overall, system-level control, and separate sections dedicated to performing various different specific computations, functions and other processes under control of the central processor section. The controllers also can be a plurality of separate dedicated or programmable integrated or other electronic circuits or devices (e.g., hardwired electronic or logic circuits such as discrete element circuits, or programmable logic devices such as PLDs, PLAs, PALs or the like). The controllers can be implemented using a suitably programmed general purpose computer, e.g., a

microprocessor, microcontroller or other processor device (CPU or MPU), either alone or in conjunction with one or more peripheral (e.g., integrated circuit) data and signal processing devices. In general, any device or assembly of devices on which a finite state machine capable of implementing the programs shown in Figs. 1, 2, 3, 5, 7, 12, 14, 5 17 and 18 can be used as controllers in the control apparatus. A distributed processing architecture can be used for maximum data/signal processing capability and speed.

While the present invention has been described with reference to what is presently considered to be preferred embodiments thereof, it is to be understood that the present invention is not limited to the disclosed embodiments or constructions. On the 10 contrary, the present invention is intended to cover various modifications and equivalent arrangements. In addition, while the various elements of the disclosed invention are shown in various combinations and configurations, which are exemplary, other combinations and configurations, including more, less or only a single embodiment, are also within the spirit and scope of the present invention.

What is claimed is:

1. A control apparatus for a reformer comprising a reformat gas generator that generates reformat gas by reforming reformat fuel and supplies the reformat gas into a fuel cell, and a combustion portion that heats the reformat fuel to be supplied to the reformat gas generator by burning at least a primary fuel, which is one of an unreacted flammable gas produced in the fuel cell and a heating fuel, the control apparatus comprising:

a heat value detector that detects a shortage in an amount of heat sufficient for heating an amount of the reformat fuel when burning the primary fuel in the combustion portion, the amount of the reformat fuel varying depending on a load applied to the fuel cell;

a secondary fuel supply means that supplies a secondary fuel, which is the other one of the unreacted flammable gas and the heating fuel, to the combustion portion additionally when the heat value detector detects the shortage in the amount of heat while burning the primary fuel in the combustion portion; and

a flow control device that adjusts the amount of the secondary fuel supplied to the combustion portion by the secondary fuel supply means, wherein the flow control device adjusts the amount of the secondary fuel based on a magnitude of the shortage in the amount of heat required in the combustion portion detected by the heat value detector so that the amount of the secondary fuel supplied to the combustion portion compensates for the detected shortage in the amount of heat.

2. The control apparatus according to claim 1, further comprising:

a reformat fuel temperature detector that detects the temperature of reformat fuel heated using the heat produced in the combustion portion, and

a heating fuel arrester that stops supply of the heating fuel to the combustion portion when the detected temperature of the reformat fuel exceeds a predetermined temperature.

3. The control apparatus according to claim 1 or 2, wherein the flow control device supplies the heating fuel to the combustion portion when a heat obtained by the flammable gas burned in the combustion portion is insufficient, and adjusts the amount of

the heating fuel supplied to the combustion portion on the magnitude of the shortage in the amount of the heat required in the combustion portion so that the amount of the heating fuel supplied to the combustion portion compensate for the detected shortage in the amount of heat.

4. A reformer unit controlled by the control apparatus according to any one of claims 1 to 3.

5. A method of controlling a reformer comprising a reformat gas generator that generates reformat gas by reforming reformat fuel and supplies the reformat gas into a fuel cell, and a combustion portion that heats the reformat fuel by burning at least a primary fuel which is one of an unreacted flammable gas produced in the fuel cell and a heating fuel, the method comprising the steps of:

detecting a shortage in an amount of heat sufficient for heating an amount of the reformat fuel when burning the primary fuel in the combustion portion, the amount of the reformat fuel varying depending on a load applied to the fuel cell; and

supplying a secondary fuel, which is the other one of the unreacted flammable gas and the heating fuel, into the combustion portion additionally when the shortage in the amount of heat when burning the primary fuel in the combustion portion is detected.

6. The method according to claim 5, further comprising the steps of:
detecting the temperature of reformat fuel heated using the heat produced in the combustion portion, and

stopping supply of the heating fuel to the combustion portion when the detected temperature of the reformat fuel exceeds a predetermined temperature.

7. The method according to claim 5 or 6, wherein the secondary fuel supplying step supplies the heating fuel to the combustion portion when a heat obtained by the flammable gas burned in the combustion portion is insufficient, and adjusts the amount of the heating fuel supplied to the combustion portion on the magnitude of the shortage in the amount of the heat required in the combustion portion so that the amount of the heating fuel supplied to the combustion portion compensate for the detected shortage in the amount of heat.

FIG. 1

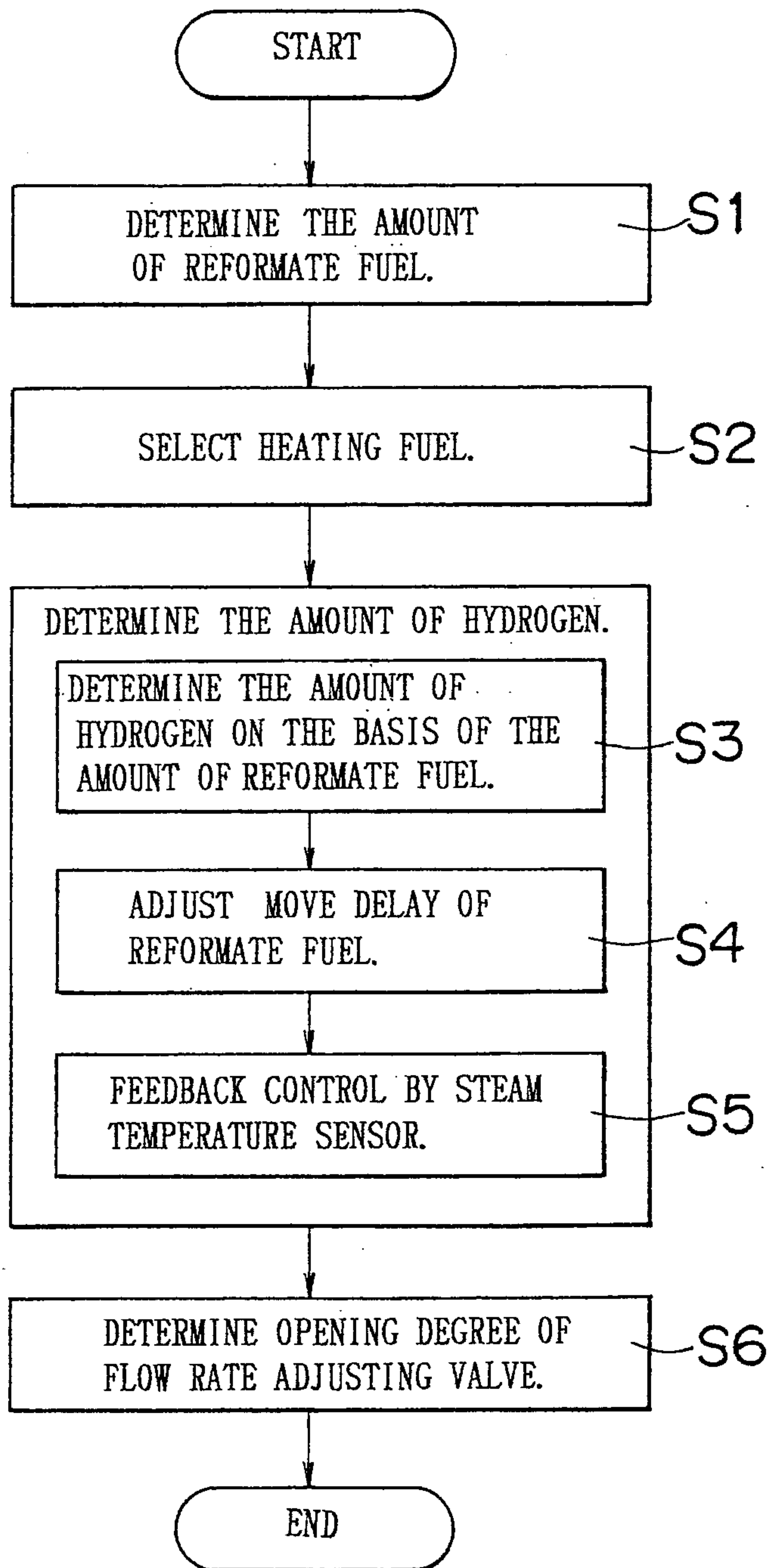


FIG. 2

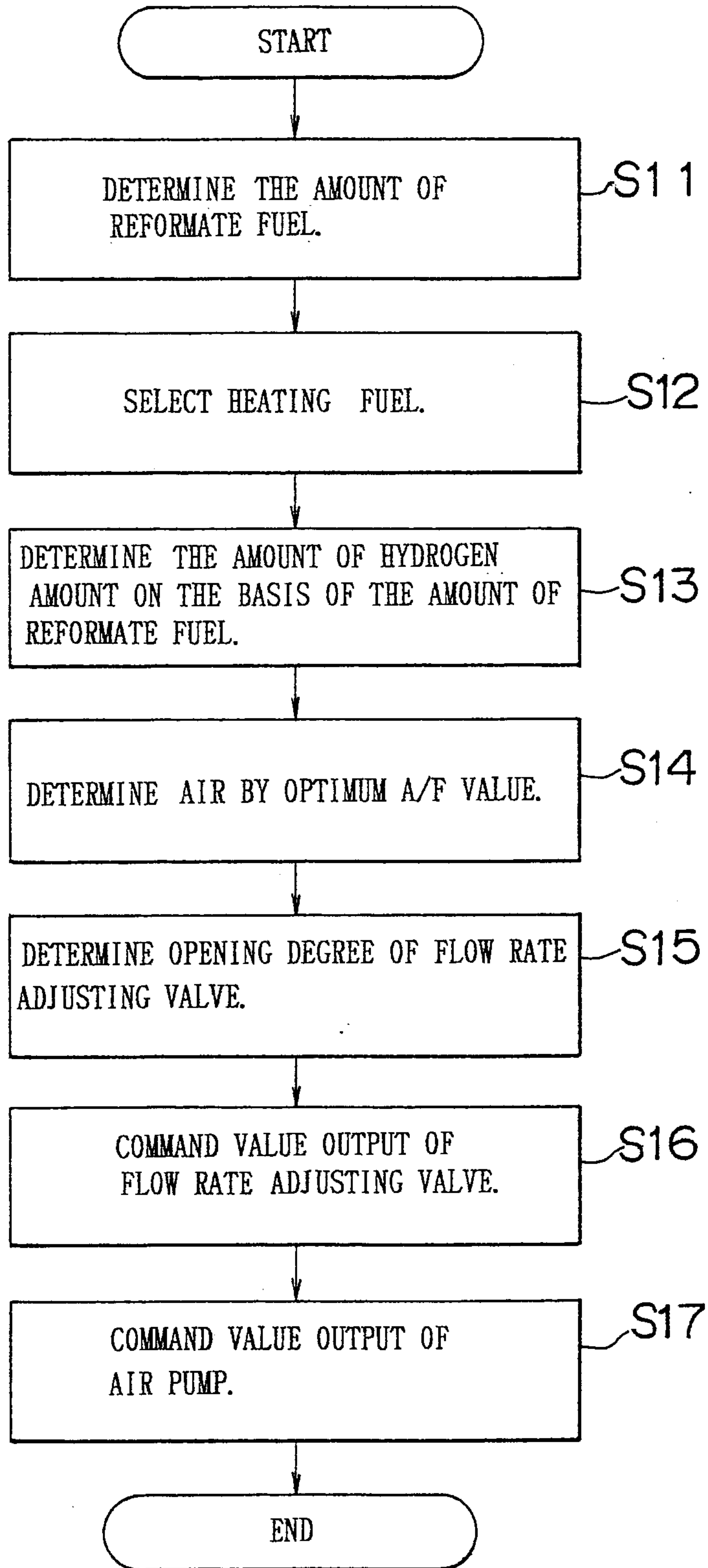


FIG. 3

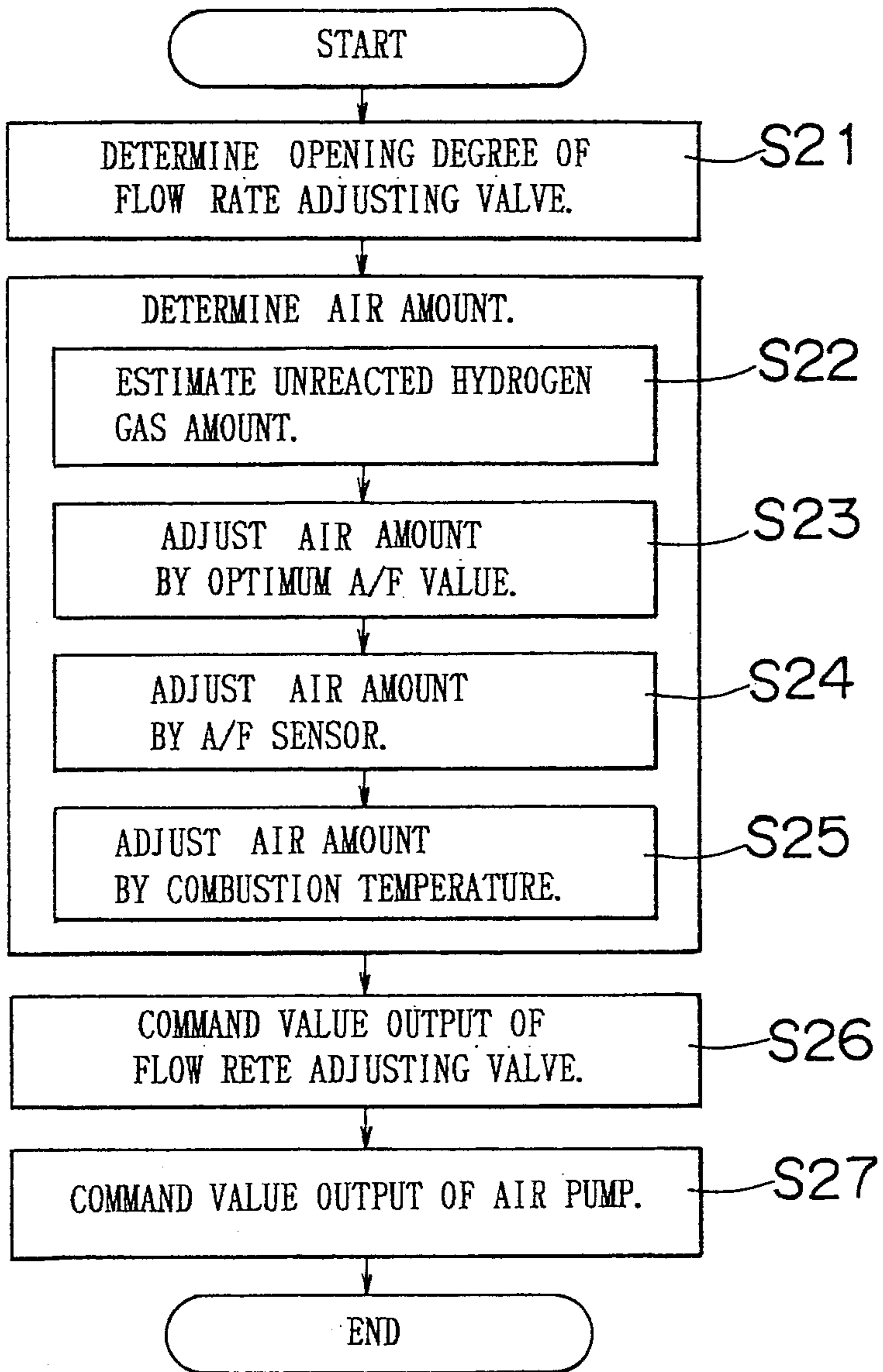


FIG. 4

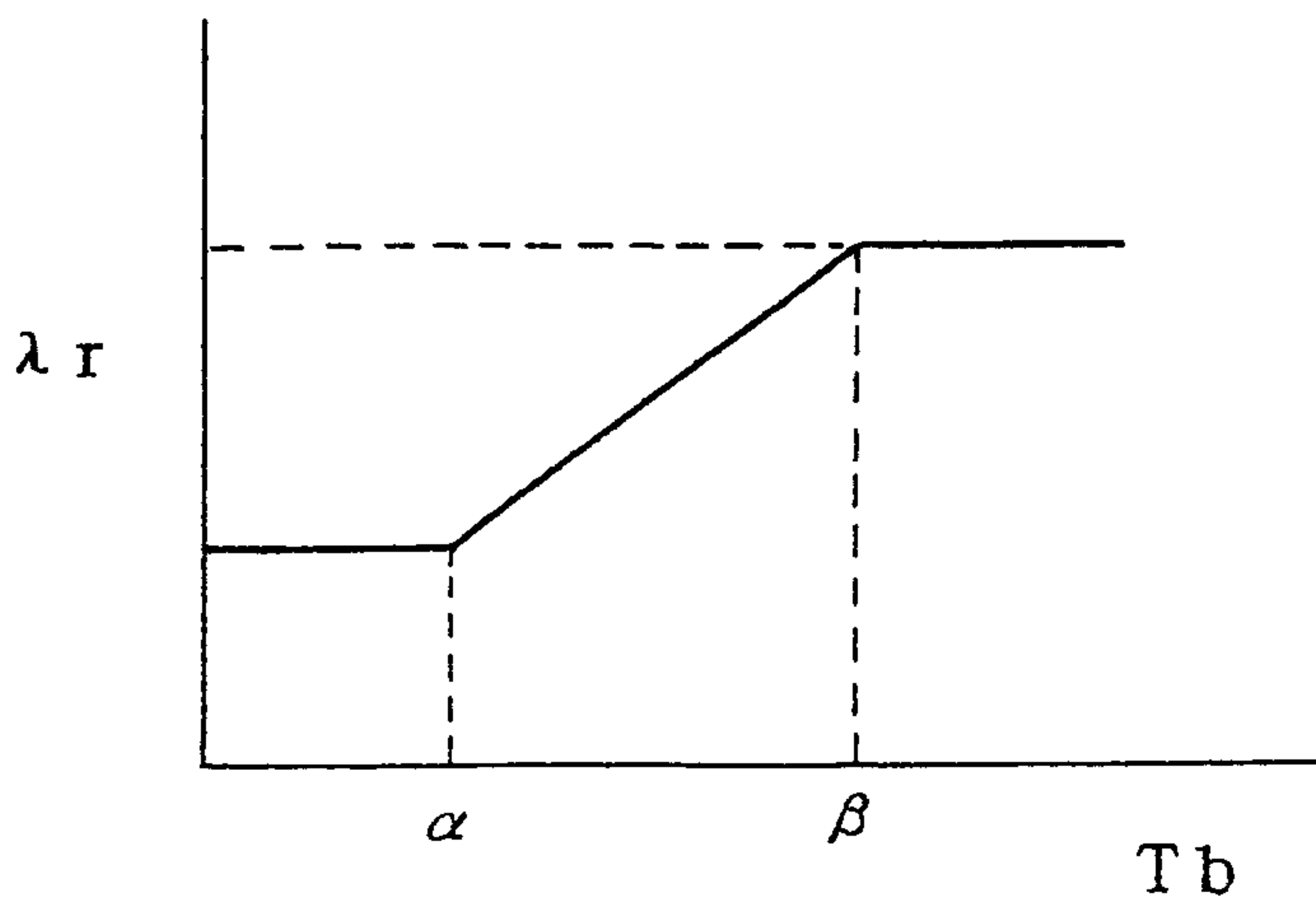


FIG. 5

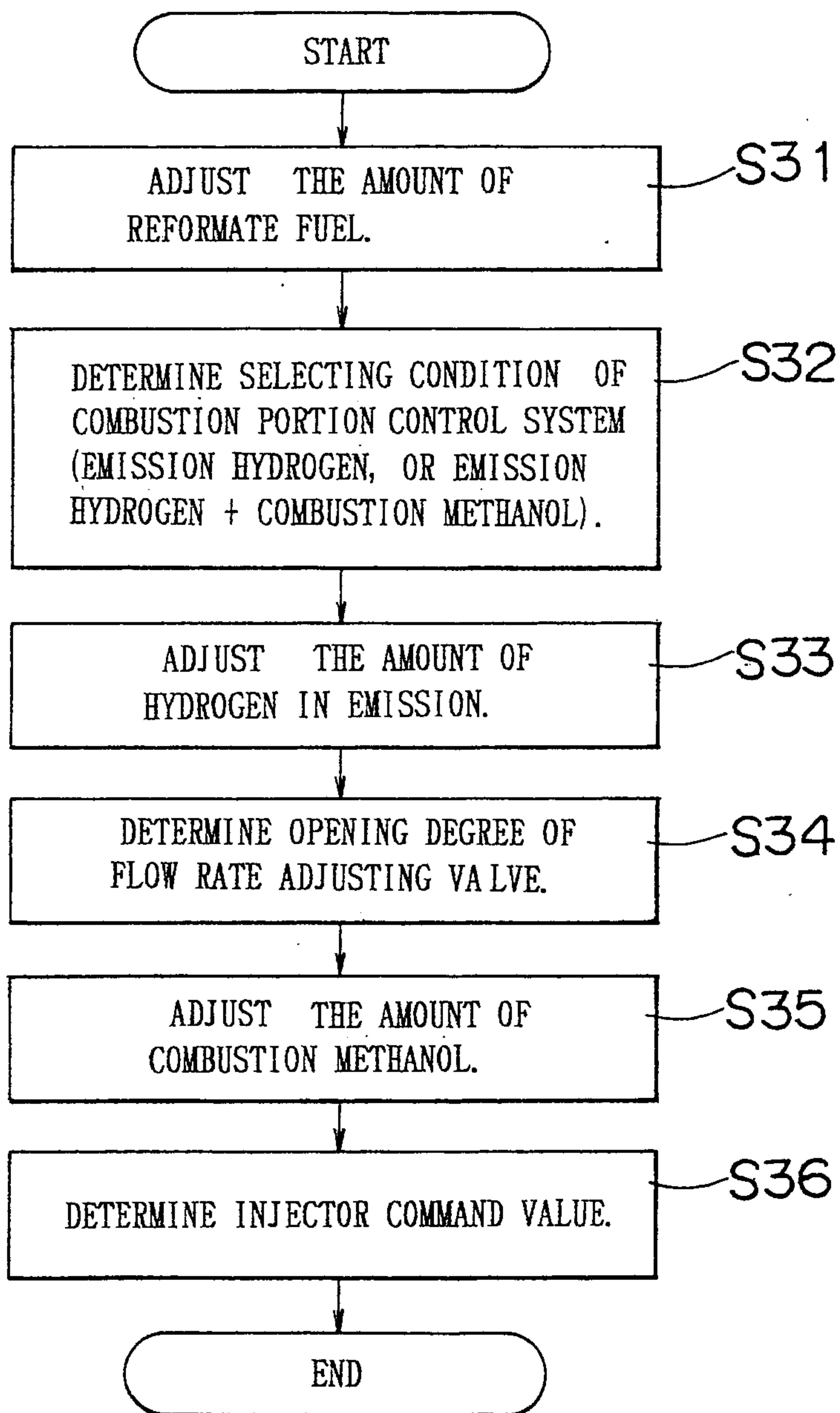


FIG. 6

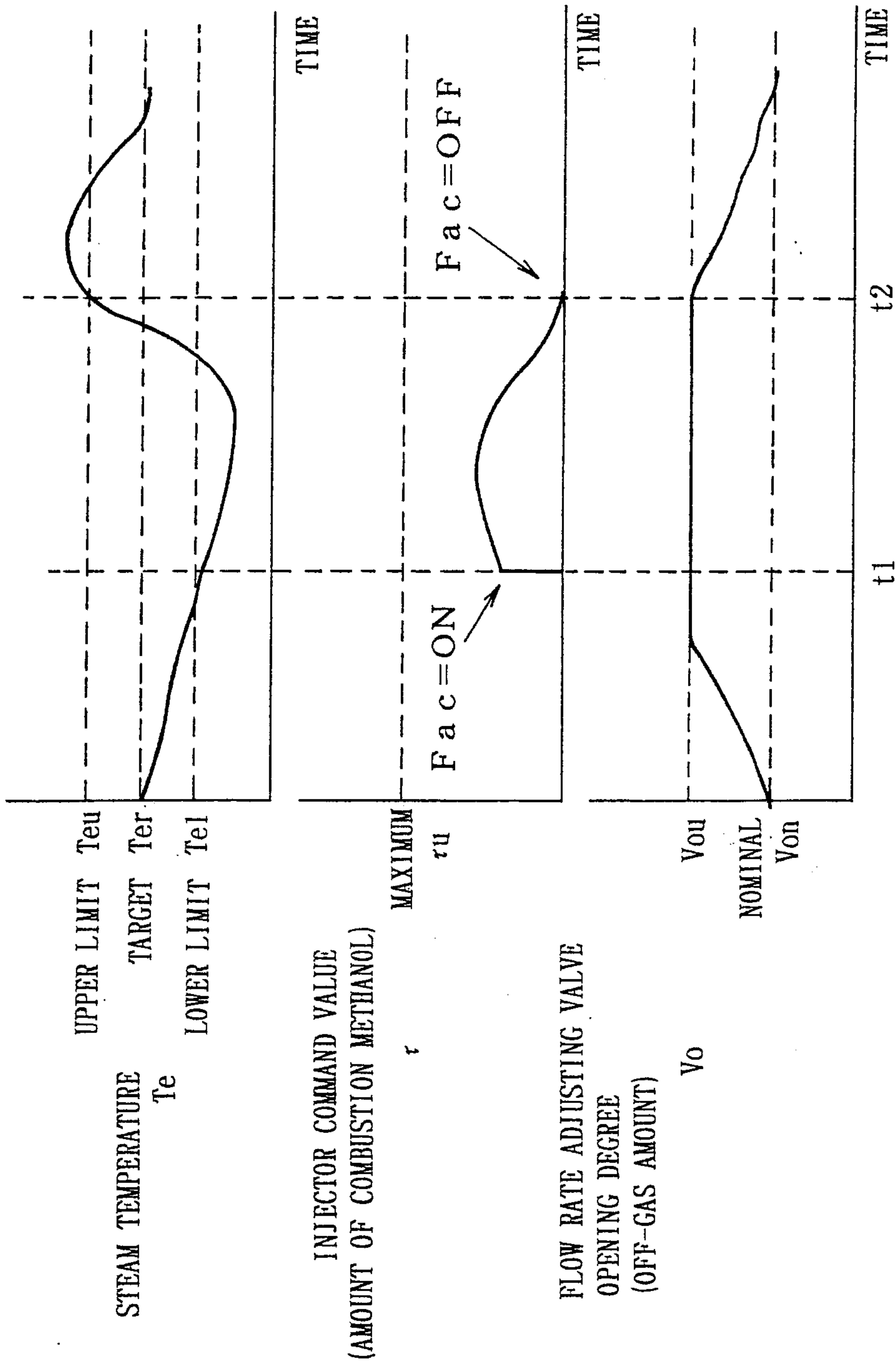


FIG. 7

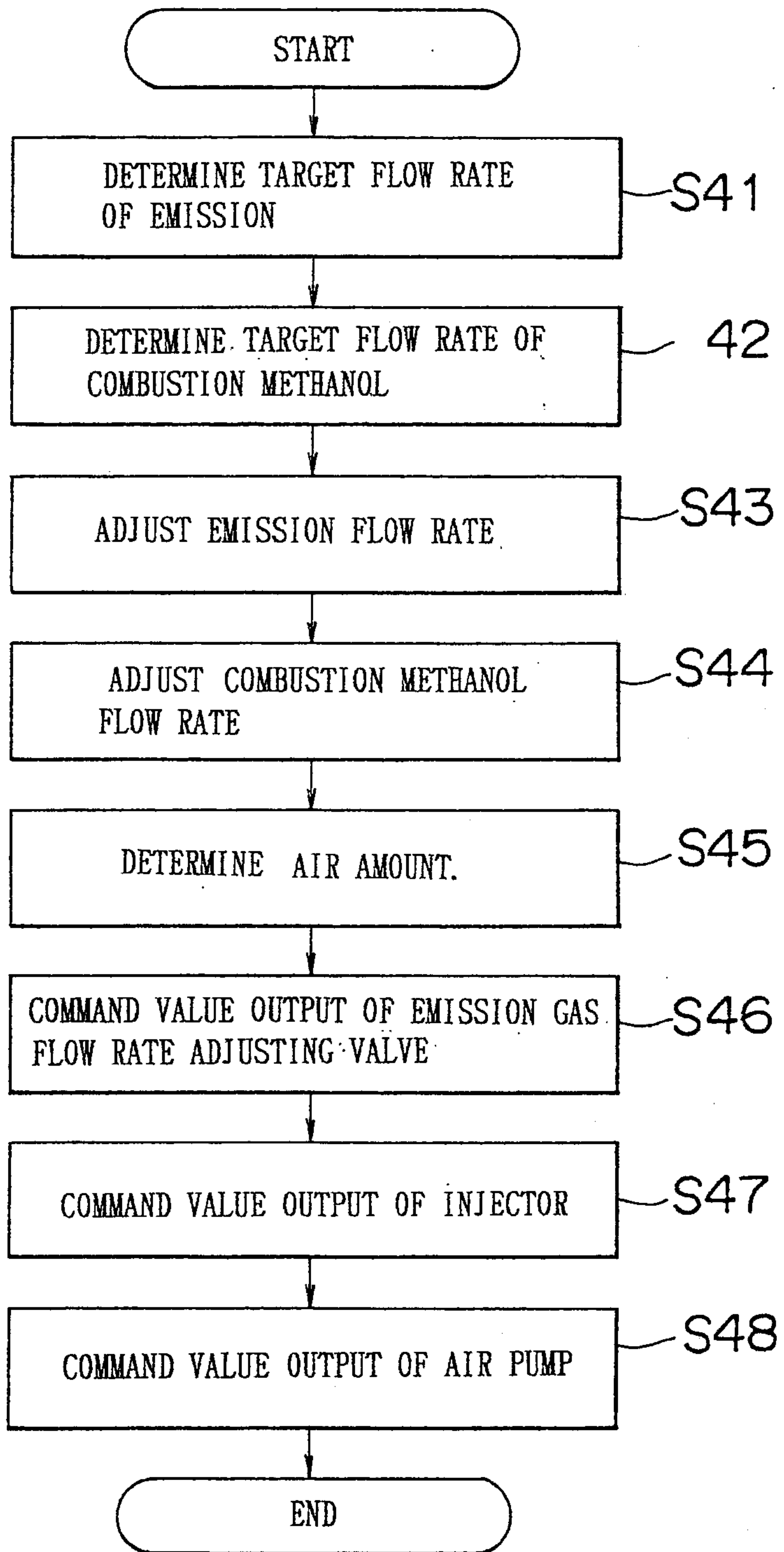


FIG. 8A

FIG. 8B

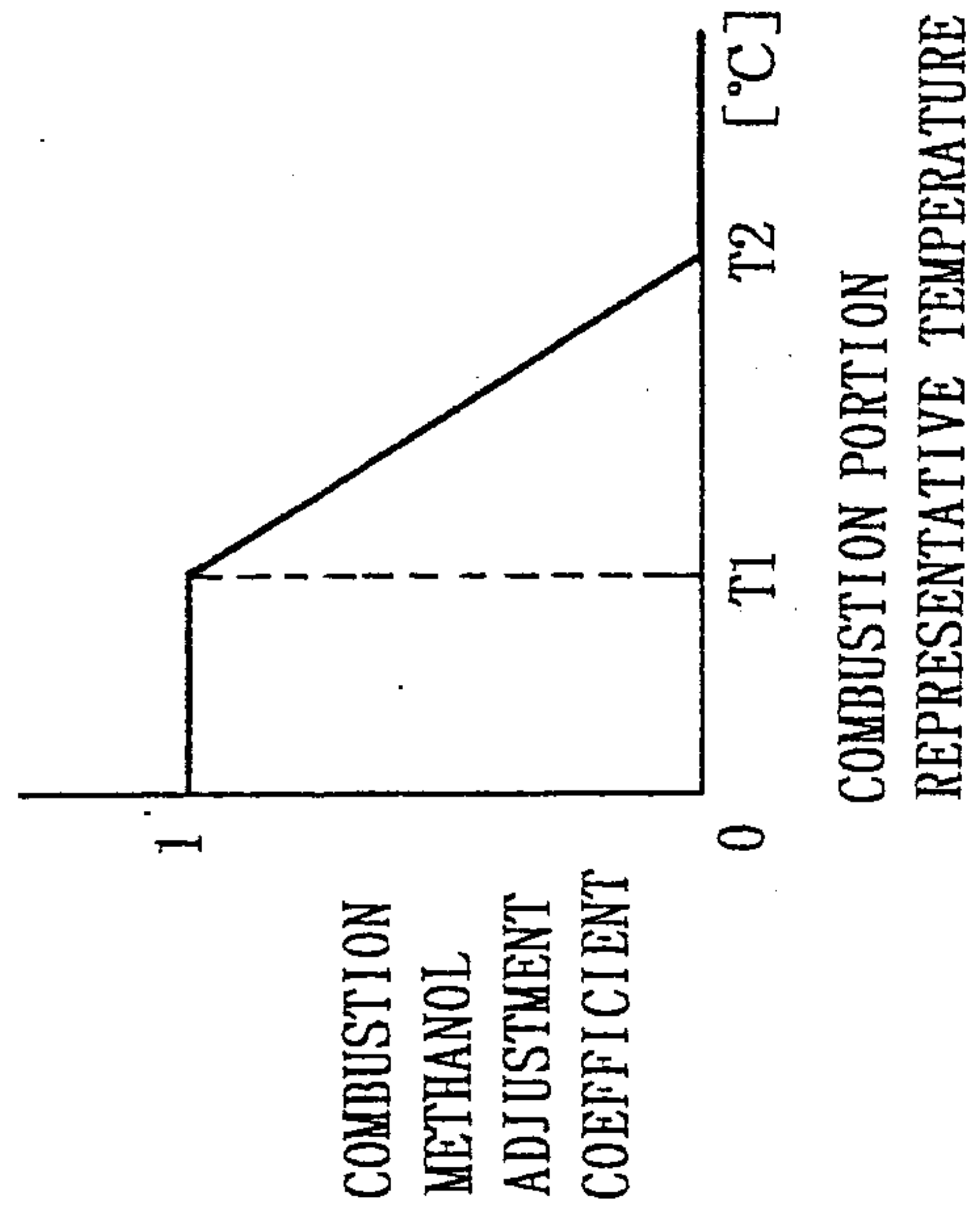
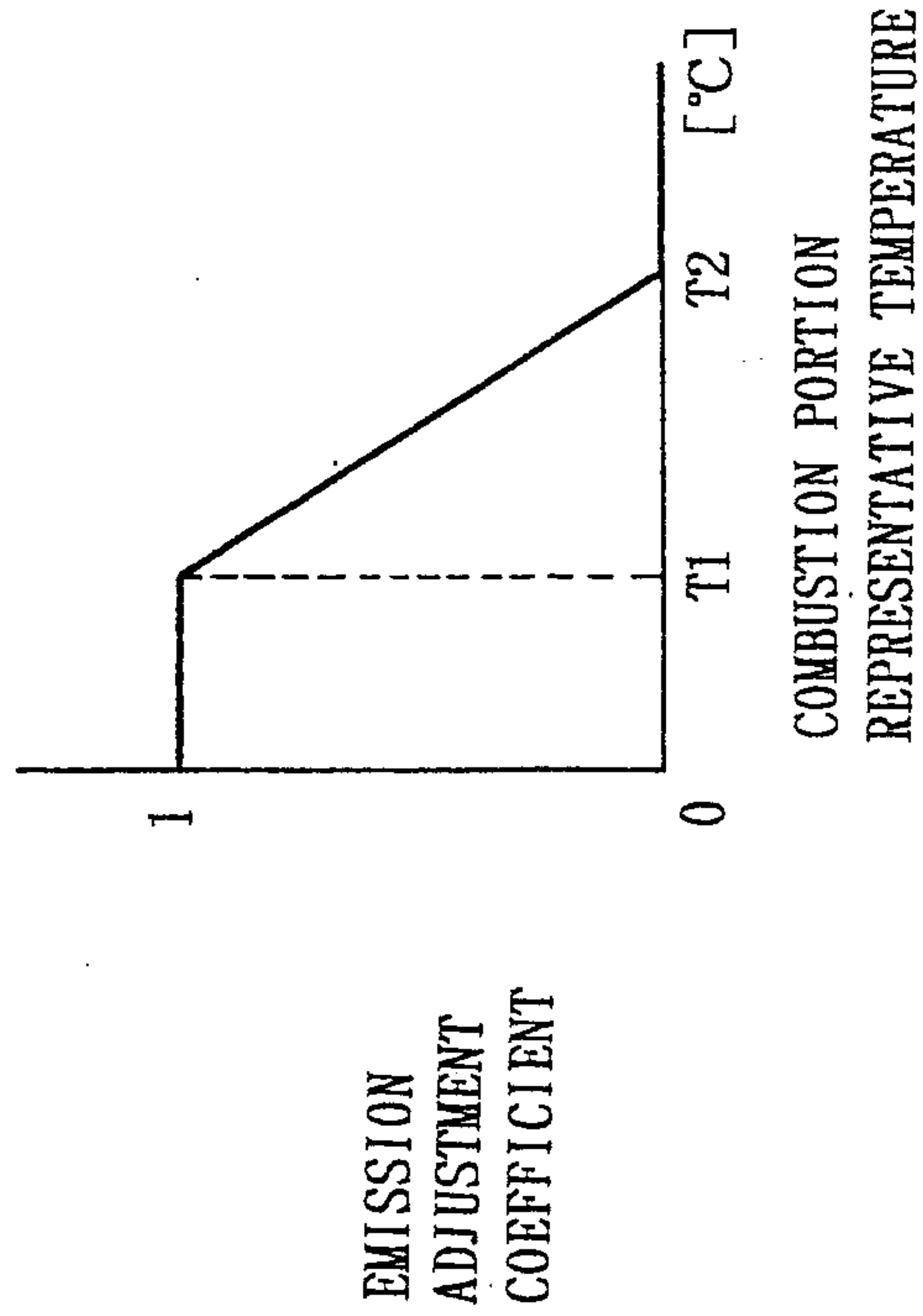


FIG. 9A

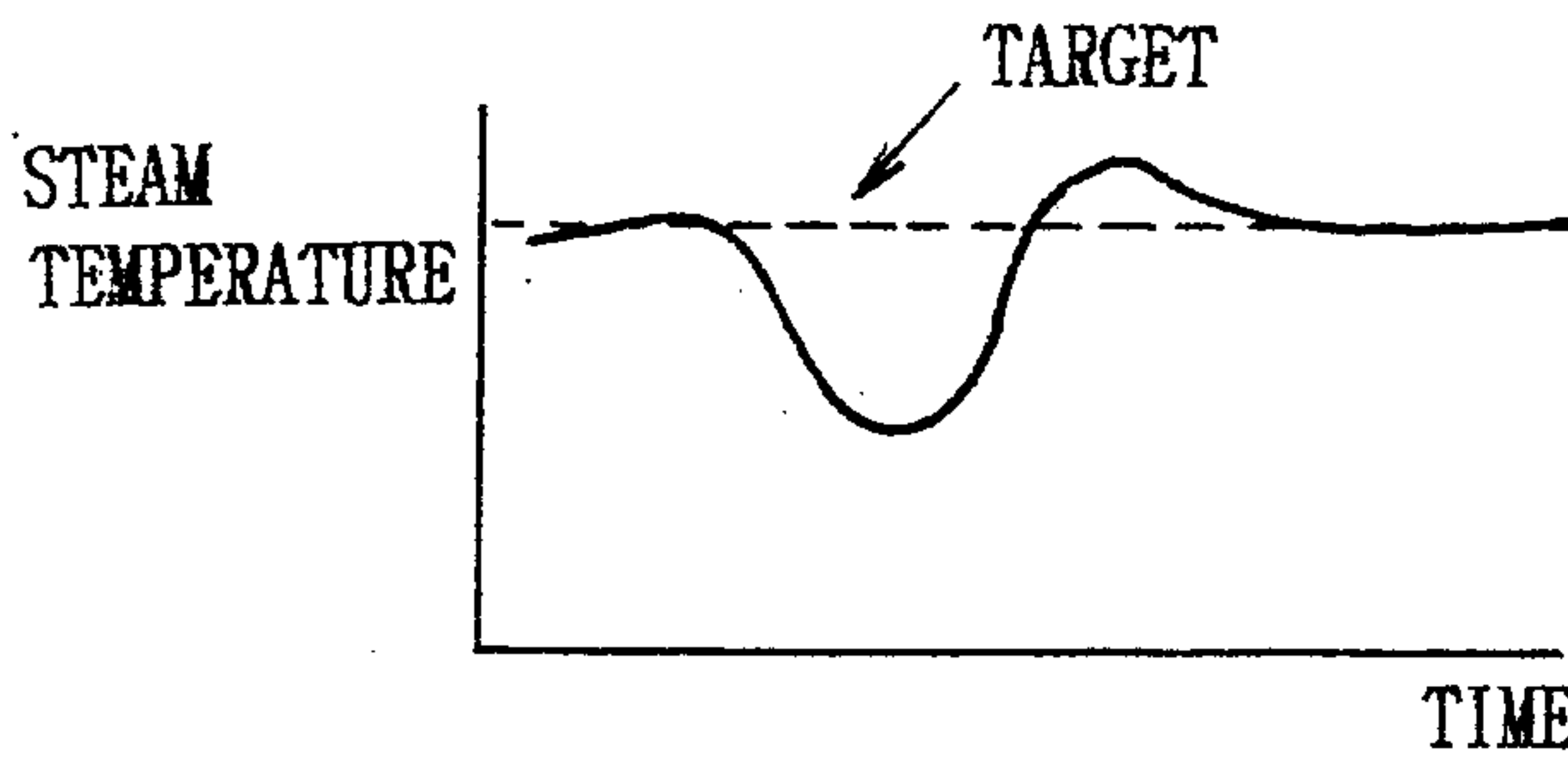


FIG. 9B

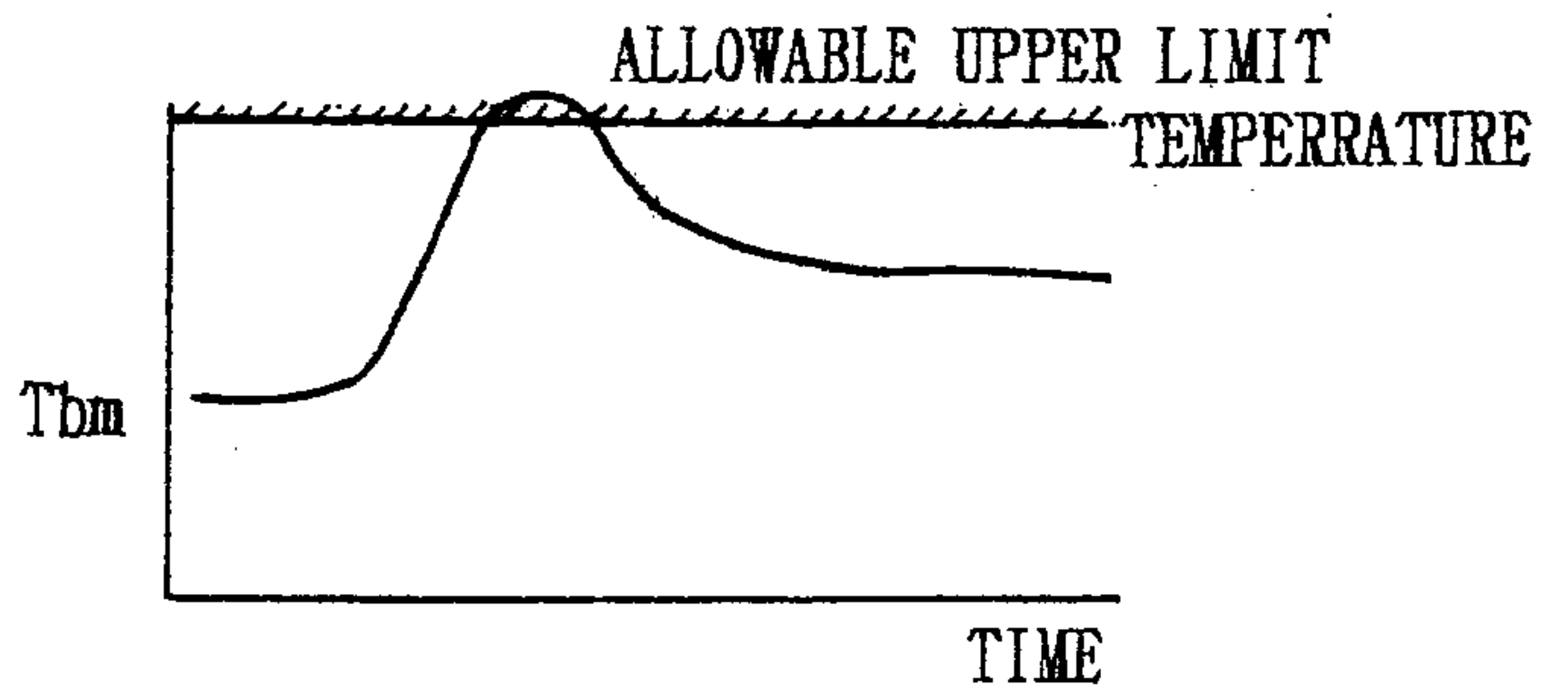


FIG. 9C



FIG. 9D

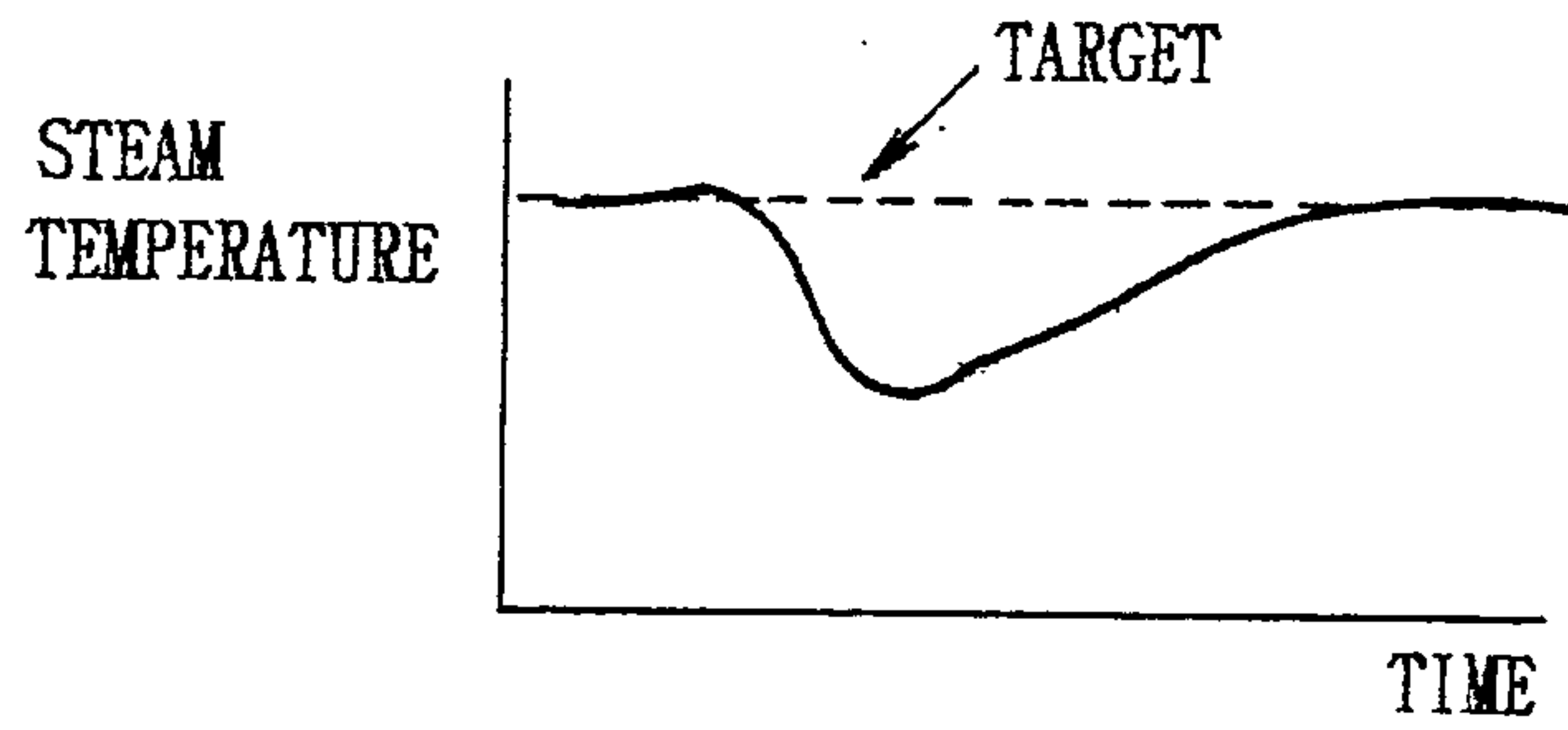


FIG. 9E

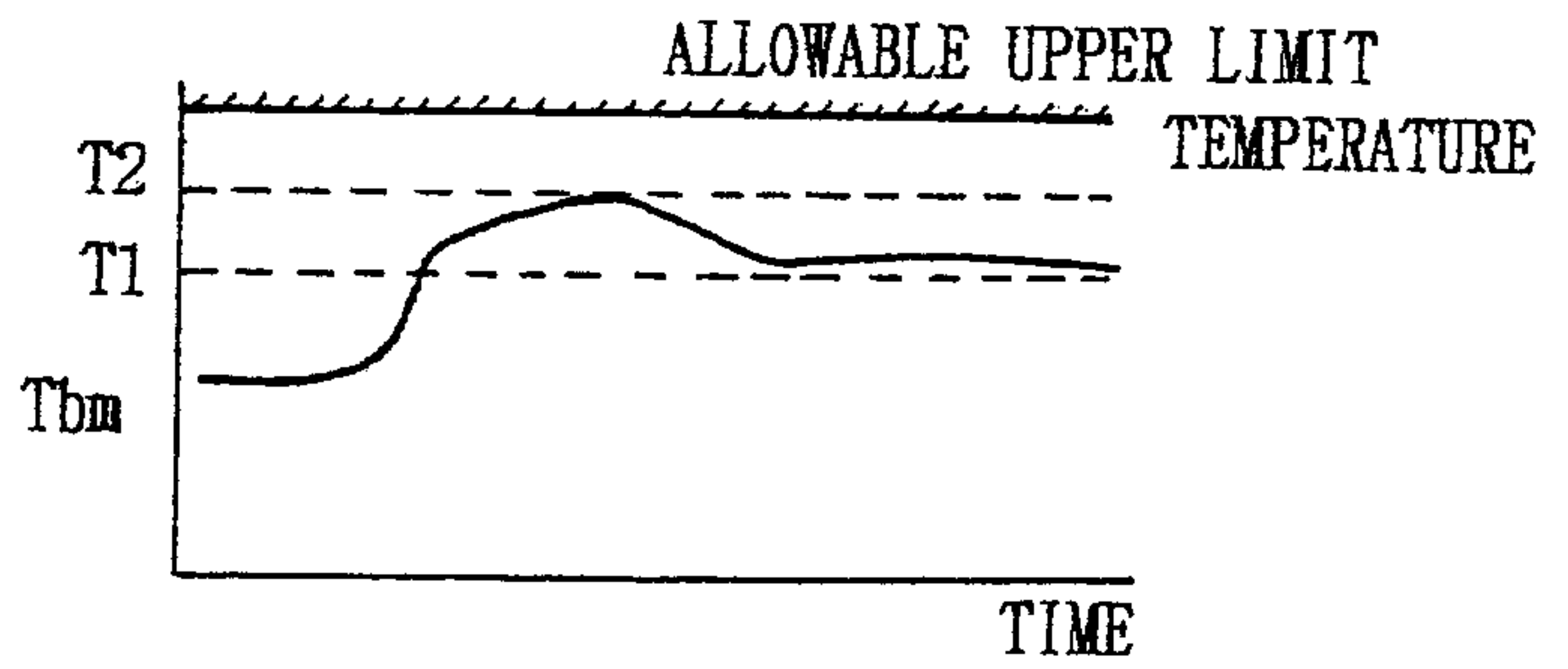


FIG. 9F

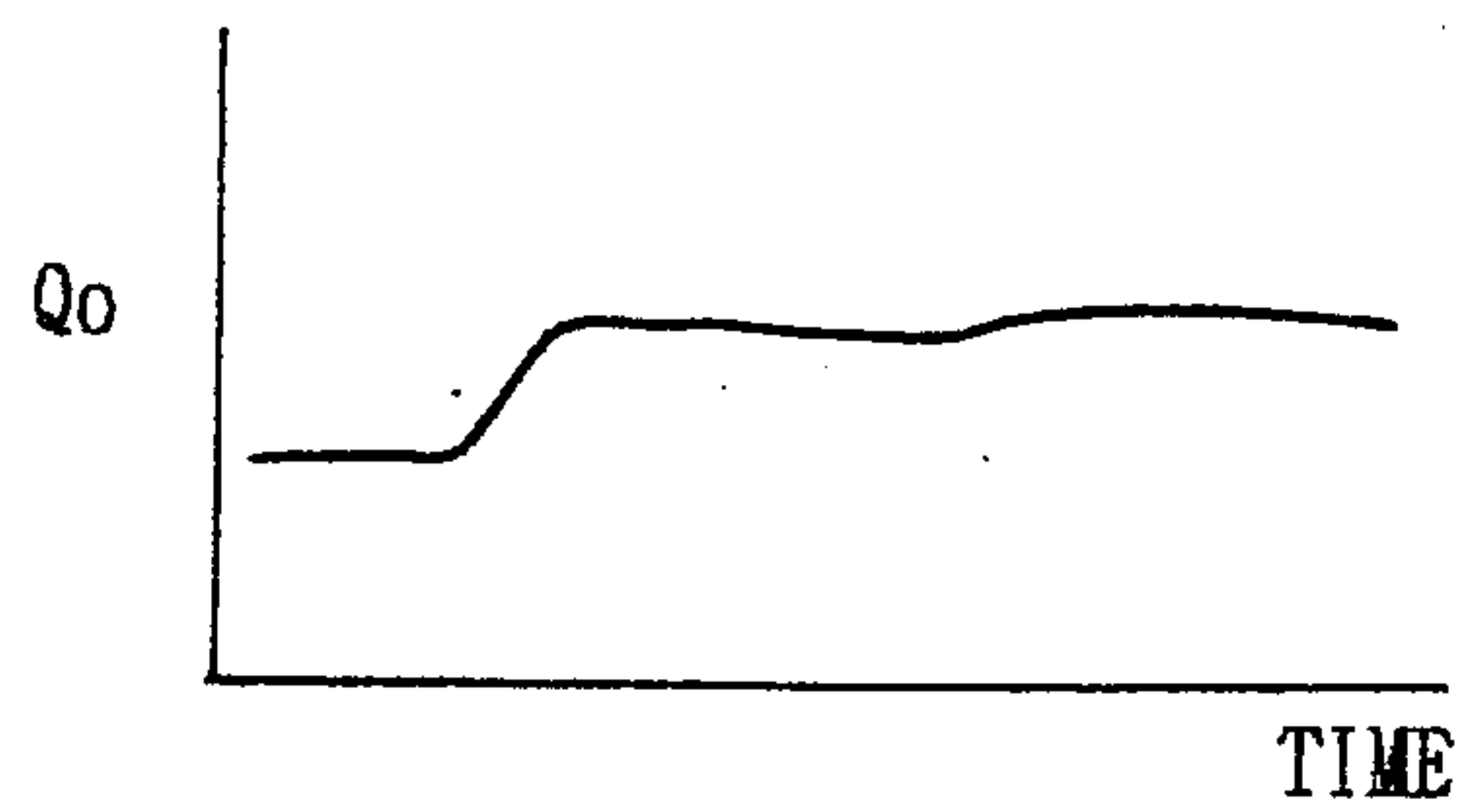


FIG. 10

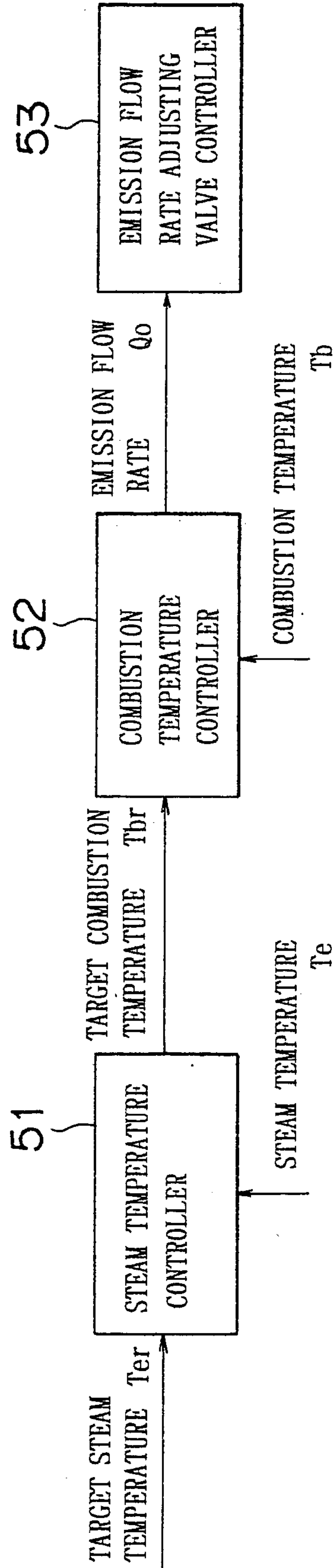


FIG. 11

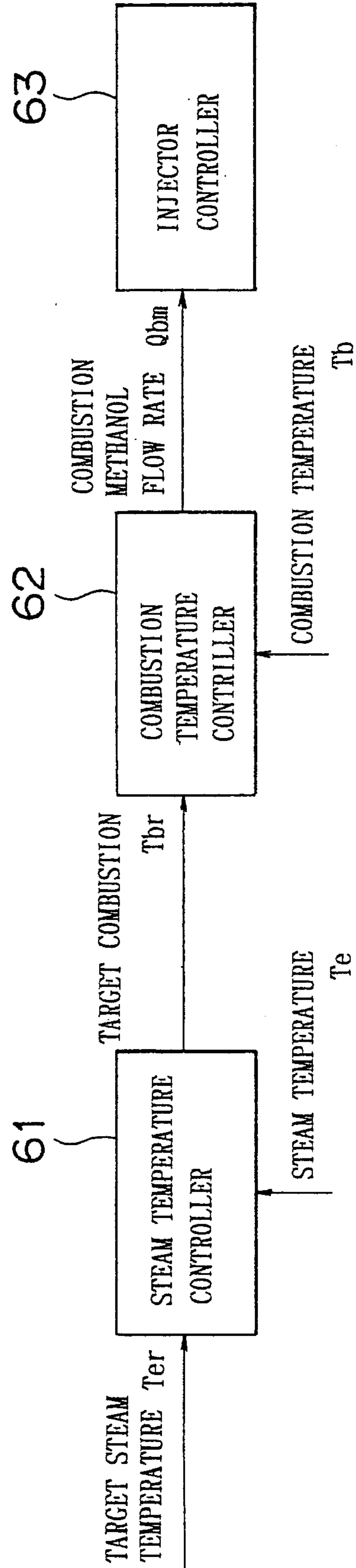


FIG. 12

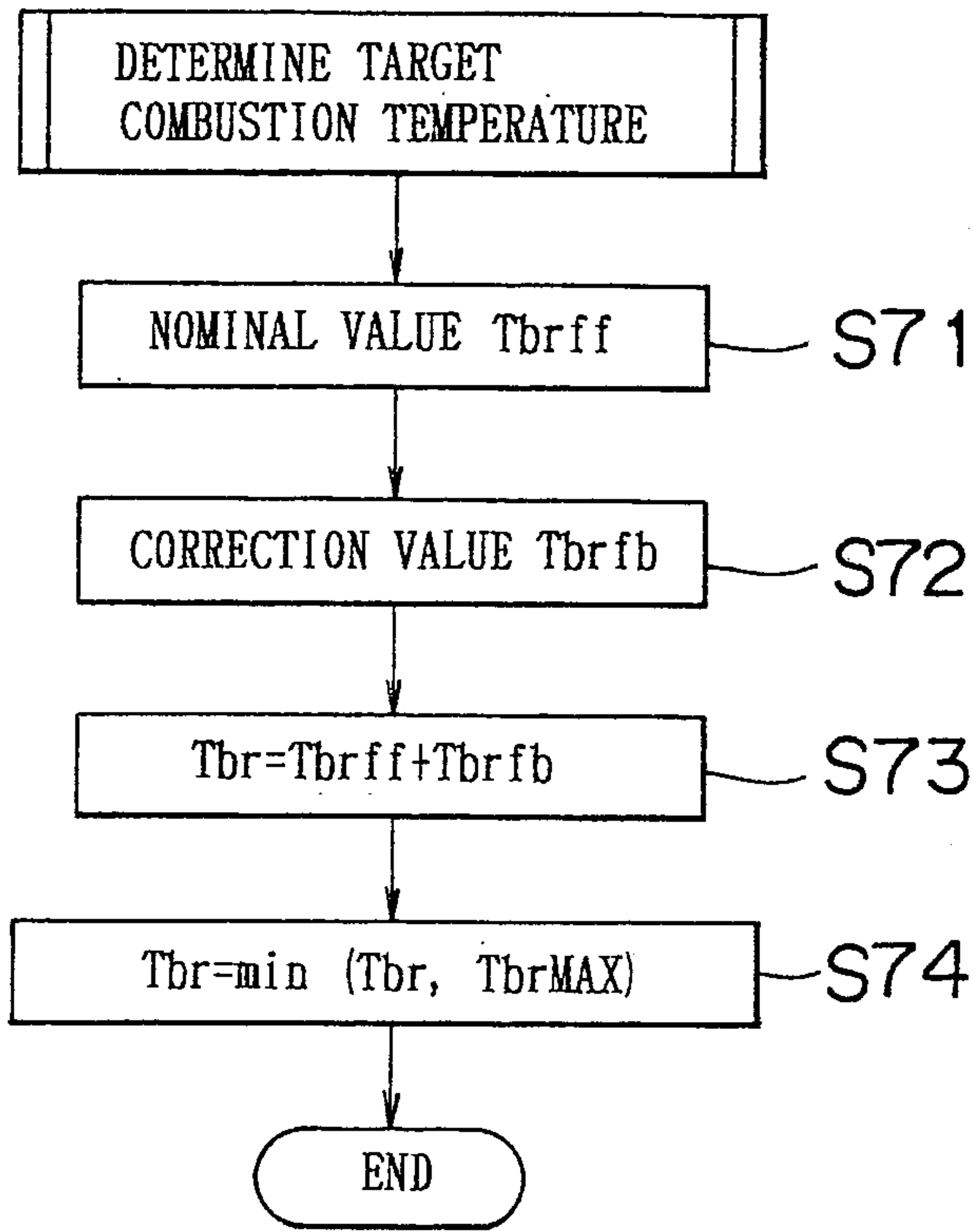


FIG. 13

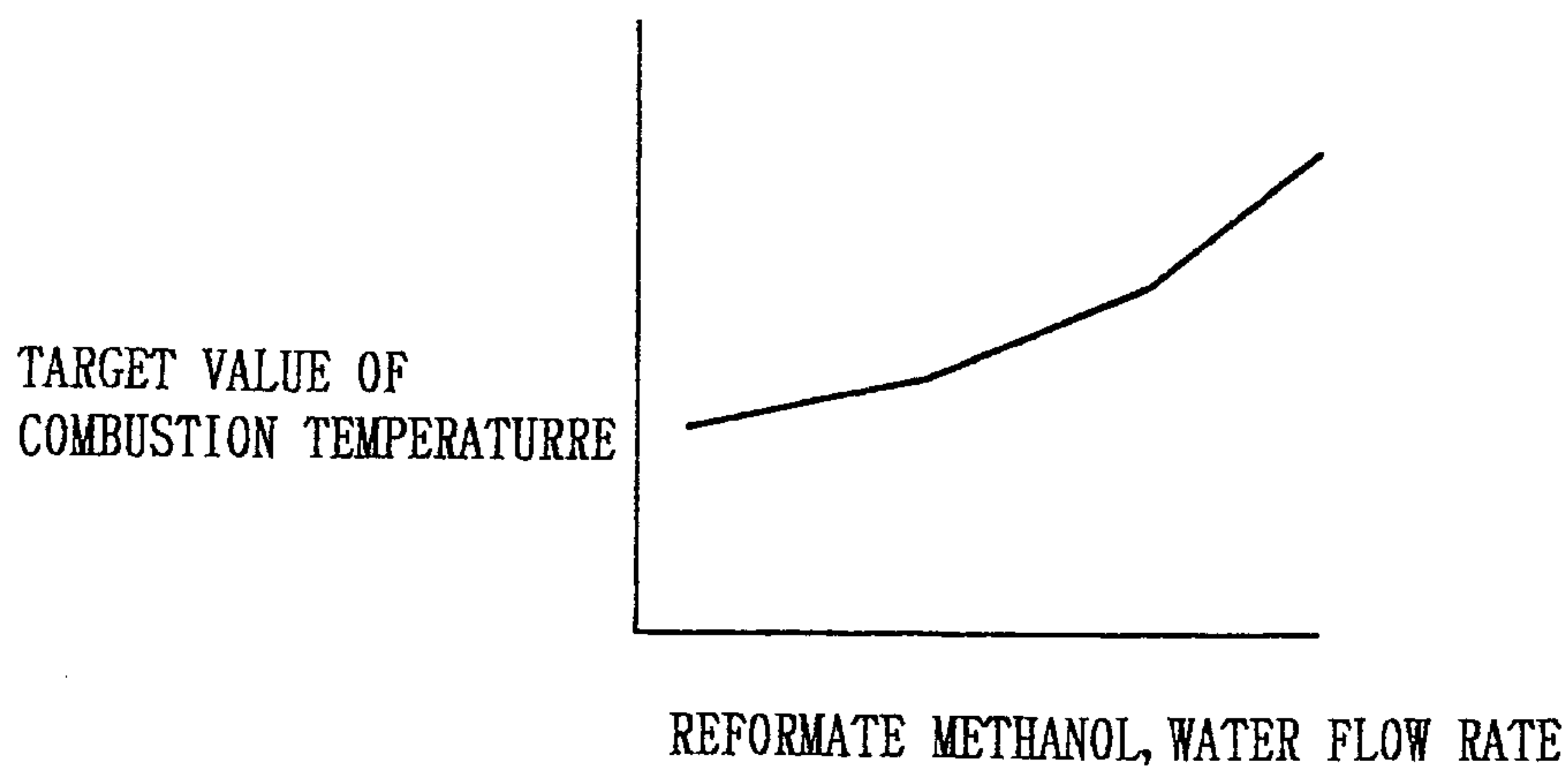


FIG. 14

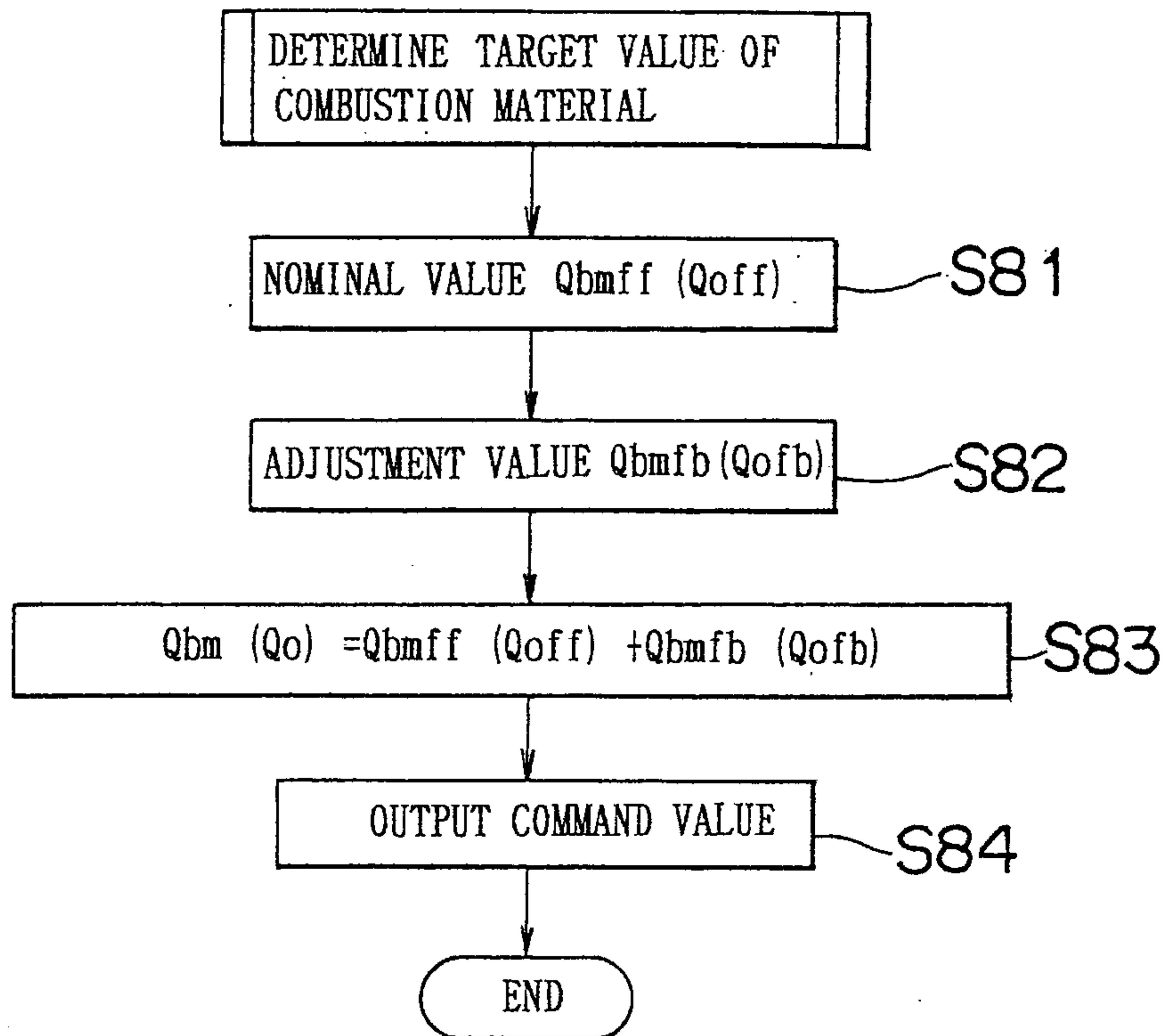


FIG. 15

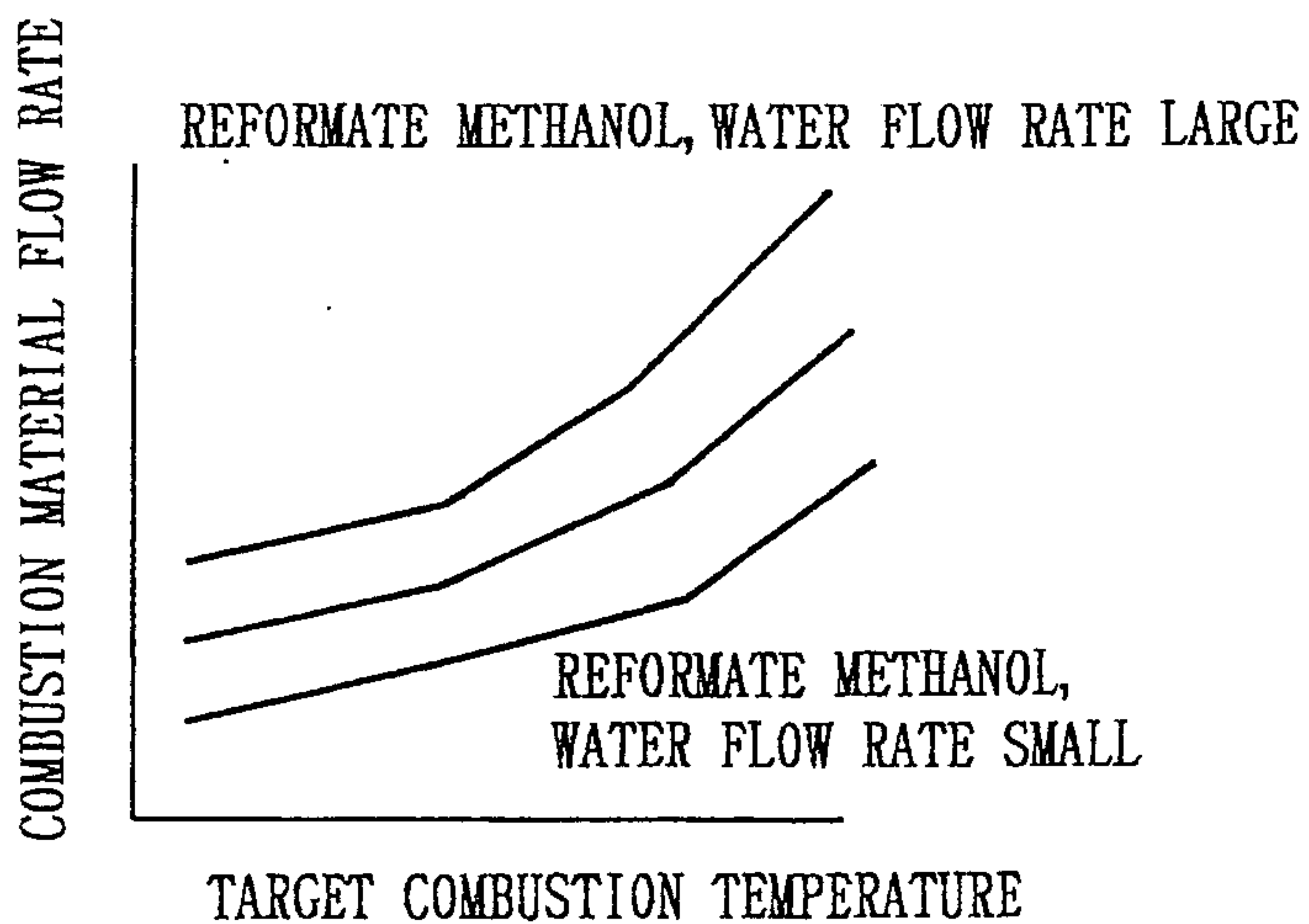


FIG. 16

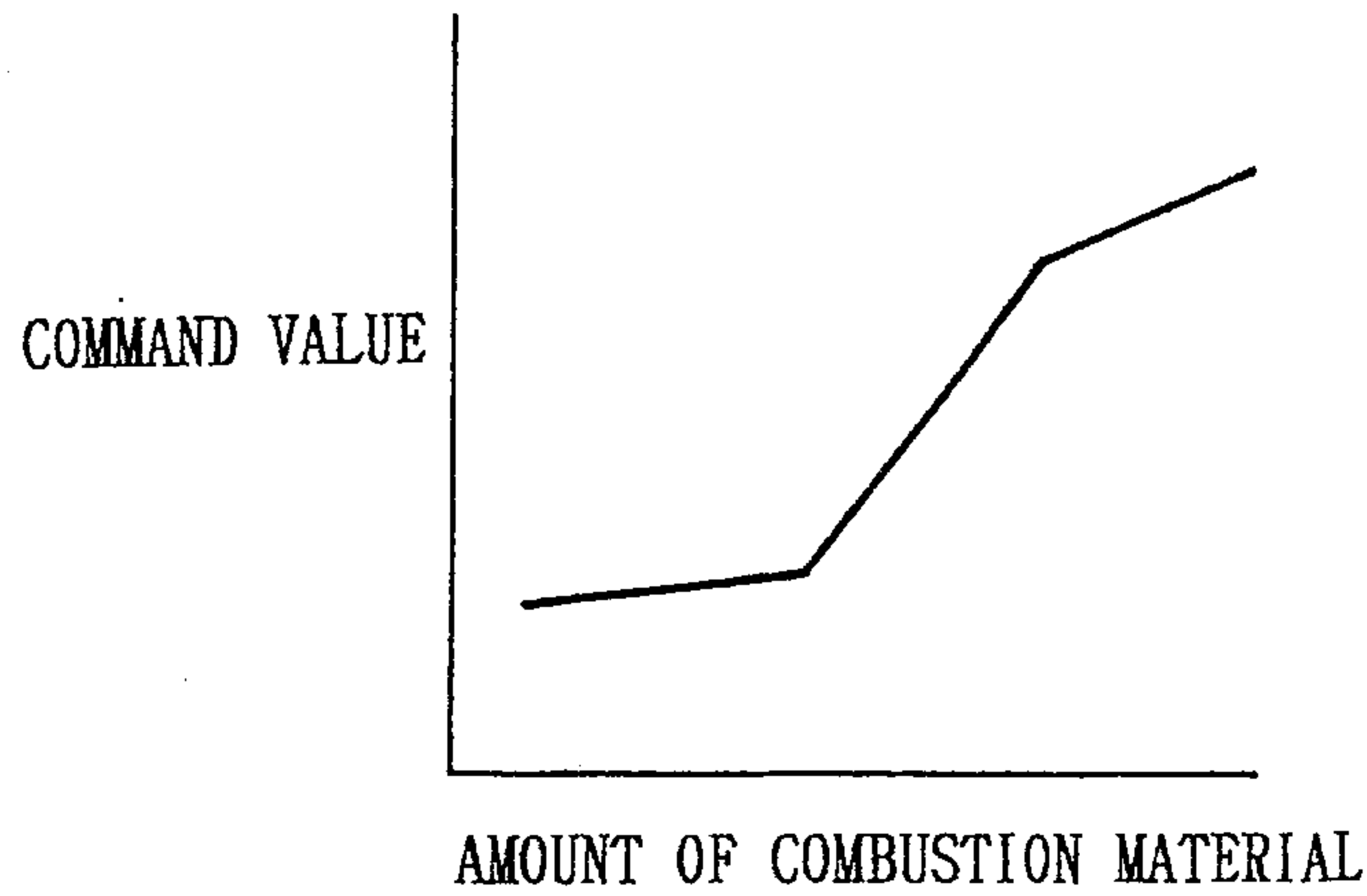


FIG. 17

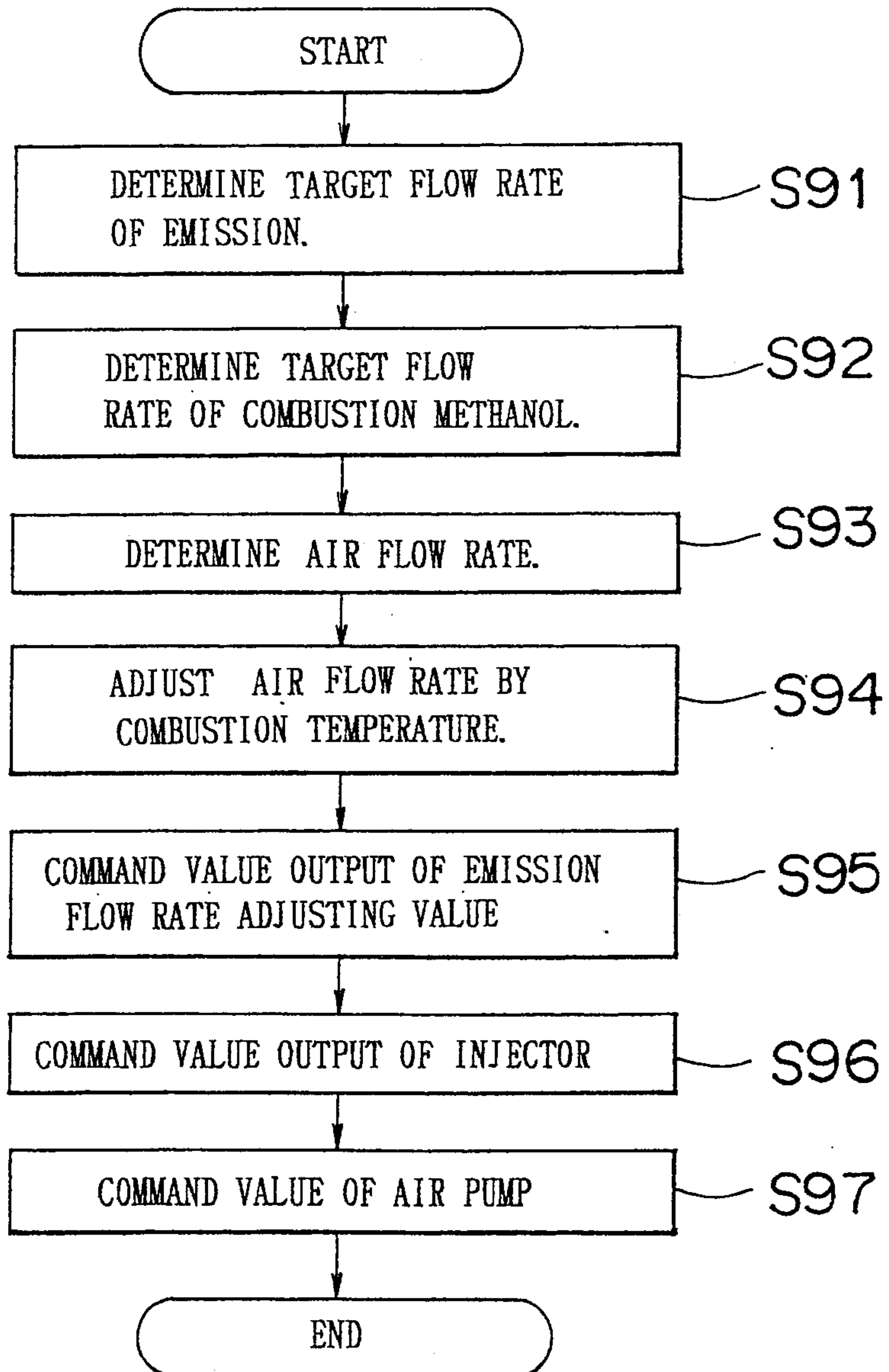


FIG. 18

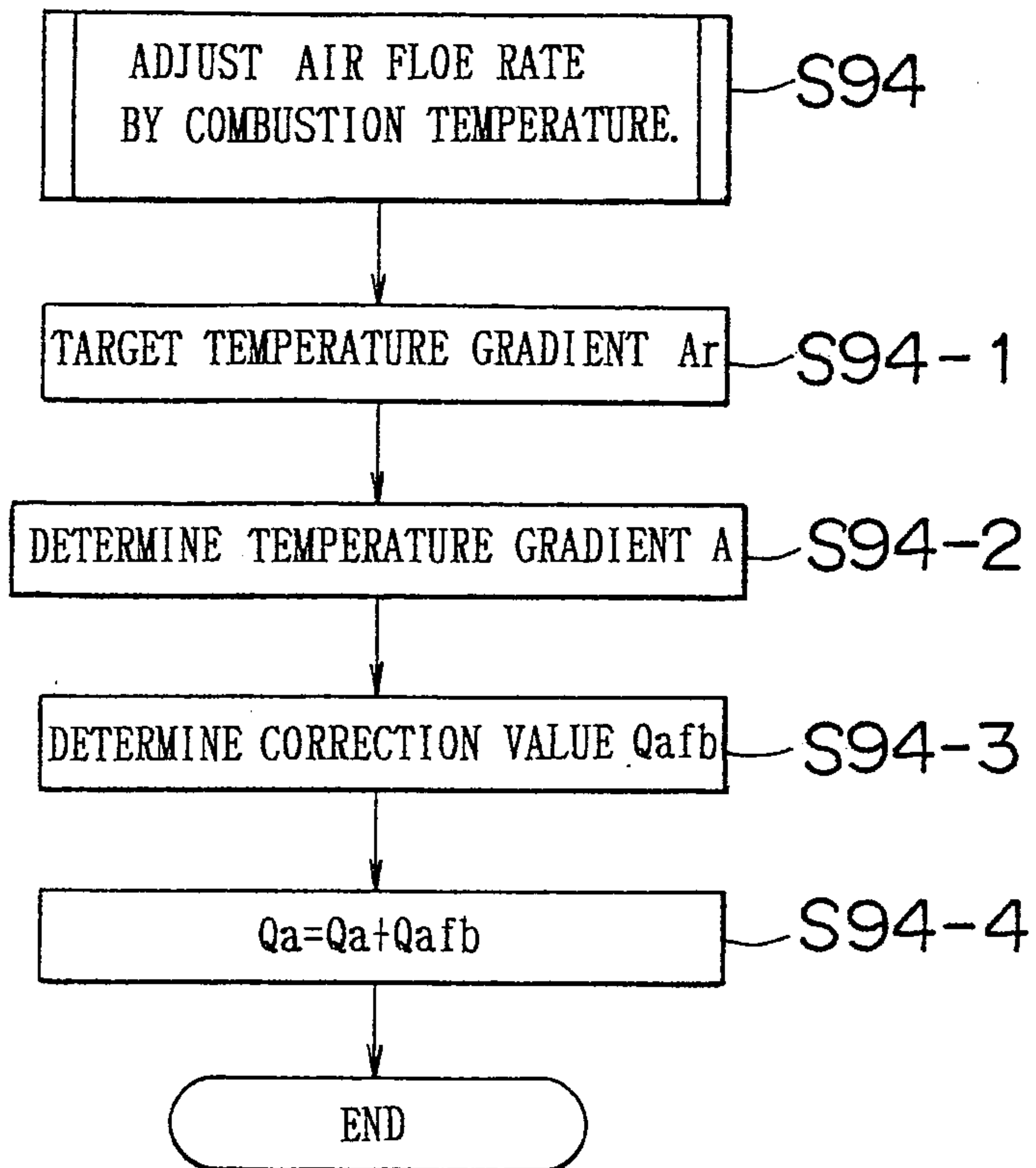


FIG. 19

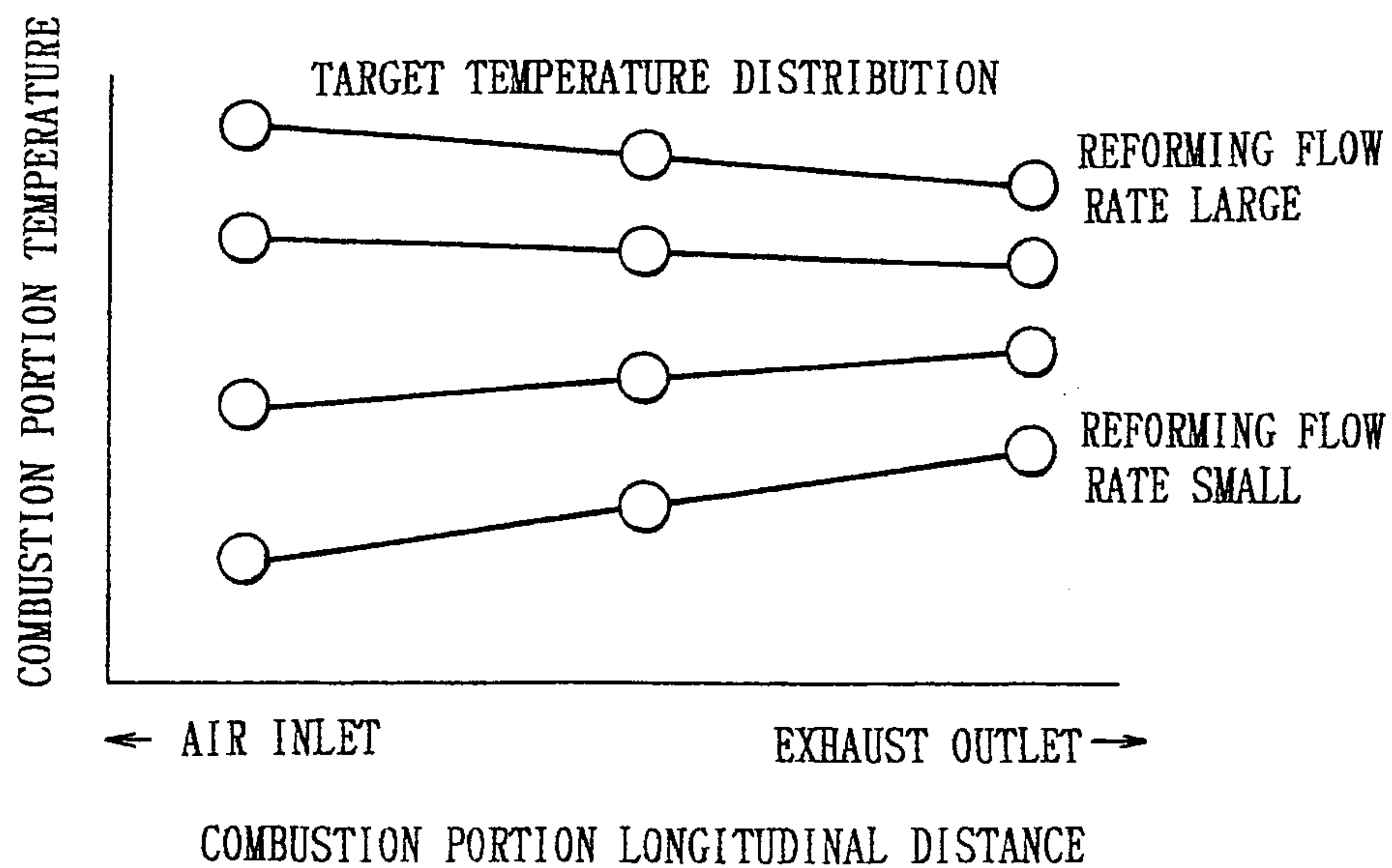


FIG. 20

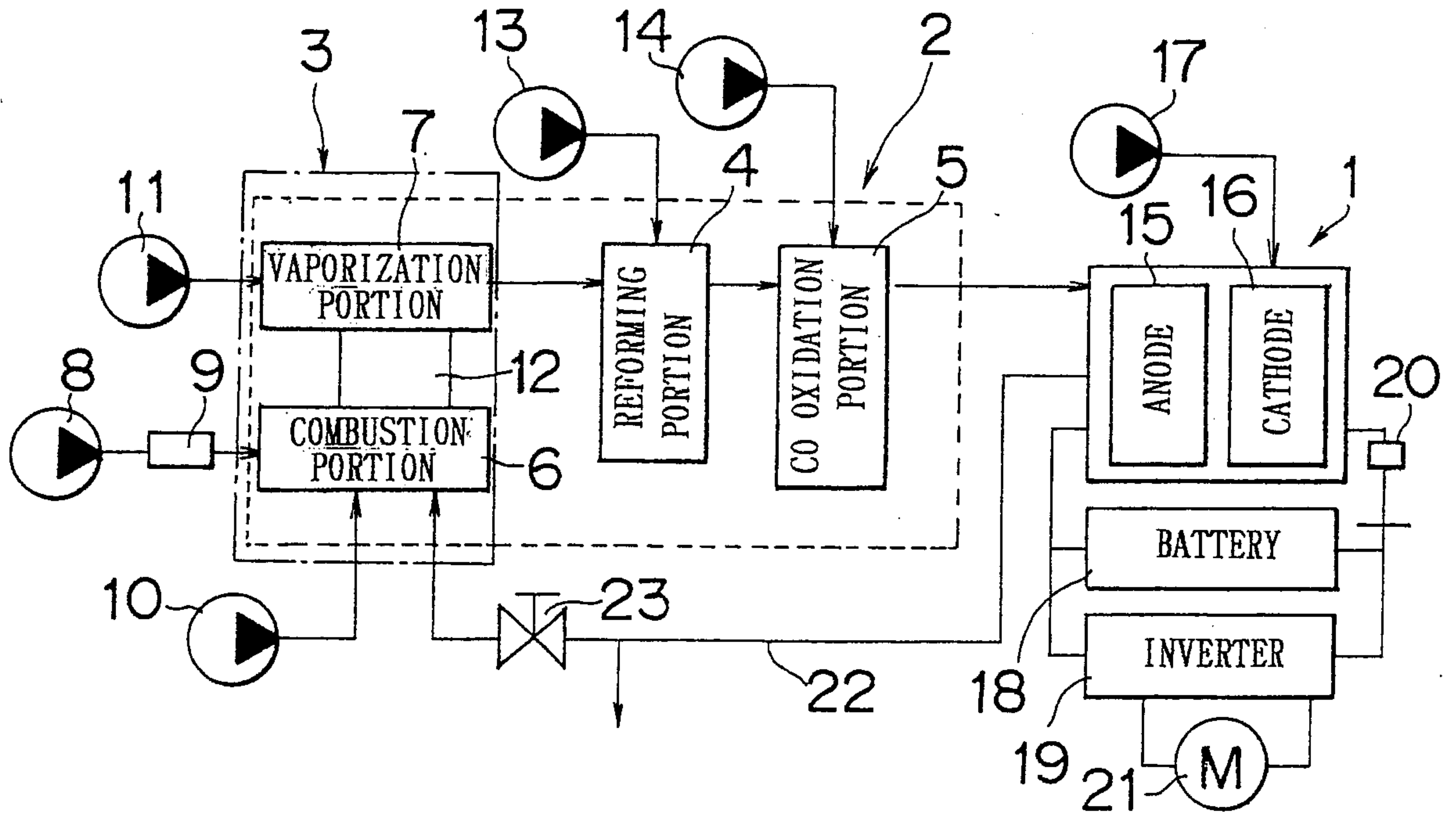


FIG. 21

