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(54) Title: POROUS POLYTETRAFLUOROETHYLENE AND PREPARATION (57) Abstract This invention relates to porous polyfluoroethylene (PTFE), shaped articles prepared therefrom, and to methods of preparing said articles.		

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TITLE

POROUS POLYTETRAFLUOROETHYLENE AND PREPARATION
FIELD OF THE INVENTION

This invention relates to porous polytetrafluoro-
5 ethylene (PTFE) compositions, shaped articles made
therefrom, and their preparation.

TECHNICAL BACKGROUND

U.S. Patents 4,360,488 and 4,385,026 disclose
formation of "non-draining" gels by heating PTFE with a
10 highly fluorinated high-boiling material at a
temperature close to the crystalline melting point of
the polymer (330-350°C). A solution or swollen mass
containing from about 1 to about 50 weight % polymer is
formed on heating, from which is recovered, on cooling,
15 a sponge-like gel, said gel being without defined shape
and retaining no "memory" of the crystallinity of the
original PTFE. The gel, after removal of the
fluorinated material by extraction in refluxing solvent
such as Freon®-113 (bp 45.8°C), is described as porous,
20 and could be formed into porous shapes, e.g. into porous
sheet by pressing between platens. The process appears
to employ granular PTFE only and, because crystalline
memory is lost during processing, the initial gels are
shapeless globs which require post fabrication into
25 shaped articles. The porous products have increased
crystallinity and a partially fibrillar structure. Use
as filter membranes or diaphragms for electrochemical
cells is disclosed.

Microporous PTFE films and sheeting are known. U.S.
30 Patent 3,664,915 discloses uniaxially stretched film
having at least 40% voids and a highly fibrillar
structure. U.S. Patents 3,953,566, 3,962,153 and
4,187,390 disclose porous PTFE films having at least 70%
voids, said films consisting of nodes and fibrils.
35 wherein the nodes are at least 1000 times thicker than

the fibrils. Pore size in the above films is at least 0.2 μm . Unsintered, paste-extruded PTFE film is stretched at rates of over 2000%/sec and as high as 40,000%/sec to achieve porosity, followed by sintering under constraint at 327 to 370°C. Such stretching rates are far higher than those employed in conventional film preparation. U.S. Patent 4,110,392 discloses microporous PTFE films having pore sizes as low as 0.01 μm , achieved by stretching unsintered PTFE as above, followed by sintering without constraint, then stretching a second time at high speed. Porosities of these films are 10 to 50%. Japanese Application 3-221541 discloses microporous PTFE film with pore size of 0.1 to 0.2 μm . The films are prepared by a modification of the above-described art procedures and have different film morphology and improved air permeability. However, ultrahigh stretching rates are again required. The art does not provide the means of improving porous PTFE articles by stretching at conventional rates.

SUMMARY OF THE INVENTION

The present invention provides a novel process (I) for introducing porosity into PTFE, said process comprising (a) contacting PTFE with a fluid which penetrates and swells, but does not significantly dissolve the polymer or eliminate viscoelastic memory therefrom, at a temperature in the range of about 250-400°C; (b) cooling and separating the penetrated, swollen polymer from unabsorbed fluid, said polymer containing up to about 50% by weight of absorbed fluid; and (c) removing the absorbed fluid, to form a porous product having a single DSC melting endotherm, said endotherm being in the range of about 320°C to 333°C with an associated heat of fusion of at least 35 J/g. In step (a), temperatures within the range of about

250°C to 400°C, should be sufficiently high for the selected fluid to extensively penetrate and swell the PTFE under process conditions, but low enough to avoid significant dissolution of the polymer or loss of viscoelastic memory therefrom. Preferably, the temperature is at or near the melting point of the PTFE under process conditions. Usually, this temperature is in the range of about 290°C to 360°C - toward the lower end for sintered or recrystallized PTFE, and toward the higher end for virgin or unsintered PTFE. Some of the porous products have a fibrillar structure.

For certain embodiments, preferred fluids are liquids at 25°C and 1 bar. Halogenated organic liquids containing fluorine and/or chlorine and, optionally, also intra-chain ether oxygen, are most preferred.

The invention also provides a variation of the above process (Process II) wherein a porous, shrink-resistant PTFE shaped article is prepared by subjecting the porous product from step (b) or step (c) to low-rate uniaxial or biaxial stretching, or wherein step (c) and stretching are performed simultaneously. Suitable fluids for use in Process II include halogenated organic fluids which may also contain intra-chain ether oxygen, and non-halogenated aromatic hydrocarbons, optionally also containing one or more substituents that are inert under process conditions. Halogen is preferably fluorine and/or chlorine.

The porous, shrink-resistant PTFE shaped article prepared by process II has a mean pore size of less than about 10 μm , a porosity of at least about 40%, and a DSC melting endotherm in the range of about 320 to 333°C with an associated heat of fusion of at least 35 J/g, and has no DSC melting endotherm at temperatures above 370°C.

Preferably, the mean pore size of the shaped article, prepared by process II, is less than 2 μm , more preferably less than 1 μm . Preferred porosity is at least about 50%, more preferably at least 60%. The heat of fusion associated with the 320°C to 333°C melting endotherm is preferably at least 40 J/g and accounts for at least 80% of the total heat of fusion of the article. Also included in this invention are:

- (1) non-draining compositions consisting essentially of PTFE and, absorbed therein, up to about 50% by weight of a fluid penetrant;
- (2) Unstretched, porous PTFE containing up to about 50% voids;
- (3) shaped articles of (1) and (2);
- (4) extruded articles such as wire, cable, fiber or tubing coated with the compositions (1) or (2), and a process for their preparation;
- (5) composites comprising PTFE and up to about 50% by weight of one or more polymers, and a process for preparing said composites.

DETAILS OF THE INVENTION

In the process (I) of the present invention for introducing porosity into PTFE, as-polymerized PTFE and melt-recrystallized PTFE are equally suitable starting materials. These may be in the form of particules or shaped articles such as film, sheet, fiber, rod or billet. The PTFE is contacted with an excess of a fluid which penetrates and swells but does not dissolve or eliminate viscoelastic memory from the PTFE under process conditions, and heated therein at a temperature in the range of about 250-400°C.

By "excess fluid" is meant substantially more fluid than is required to penetrate and swell the polymer fully under process conditions; i.e. substantially more

than 50% of the volume occupied by the unswollen polymer.

When the fluid is a relatively volatile liquid, vapor or gas, the process may be operated under pressure. Operating pressure for the invention process is from about atmospheric pressure to about 300 MPa or higher. The starting PTFE may be immersed in unheated fluid and then heated to the operating temperature, or immersed in fluid previously heated to the operating temperature. It is preferable, but not essential, to completely envelope the PTFE in fluid. The polymer should preferably remain completely enveloped by the fluid throughout the fluid contacting procedure. Precautions should be taken to insure that fluids causing chemical reactions under process conditions are avoided.

In the invention process (II) for preparing stretched, porous, shrink-resistant PTFE shaped articles, conventionally formed shaped articles, such as film, fiber or billet, of PTFE, are contacted with an excess of an appropriate organic fluid in which the PTFE is insoluble or of limited solubility under process conditions, and heated therein at a temperature at or near the melting point of the PTFE under said process conditions. The starting article may be immersed in unheated fluid and then heated to the operating temperature, or immersed in fluid previously heated to the operating temperature. The polymer should preferably remain completely enveloped by the fluid throughout the fluid contacting procedure.

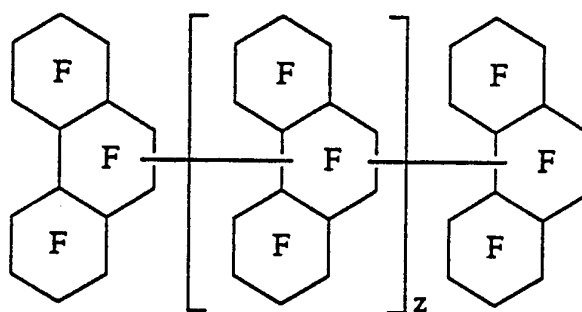
As indicated above, the appropriate temperature in the invention process should be sufficiently high to permit high fluid uptake but must not exceed that required to maintain the shape of the starting PTFE article under process conditions. Suitable process

temperatures are at or near the melting point of the PTFE under process conditions. Factors affecting the appropriate temperature include the swelling power of the selected fluid, the crystalline morphology of the PTFE, the duration of exposure in step (a), and the surface/volume ratio of the PTFE article. Temperatures in the range of 290-360°C are usually suitable.

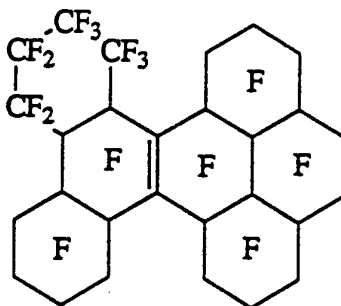
Preferred fluids for use in processes I and II include halogenated organic liquids containing fluorine and/or chlorine and, optionally, also ether oxygen. Non-limiting examples of such liquids include chlorobenzene, fluorobenzene, 1,2-dichlorobenzene, benzo-trifluoride, perfluorodimethylcyclobutane, perchloroethylene, Freon®-113 (1,1,2-trichloro-1,2,2-trifluoroethane), Freon®-114 (1,2-dichloro-1,1,2,2-tetrafluoroethane, 1,1-difluoro-1,2,2,2-tetrachloroethane, 1,2-difluoro-1,1,2,2-tetrachloroethane, perfluoro-n-butyl-tetrahydrofuran, Krytox®-143AZ perfluorinated oil (perfluoropropene oxide oligomers), pentafluoroethane, chloroform, methylene chloride, 1,1,2-trichloroethylene, carbon tetrachloride, and mixtures thereof. Higher boiling perfluorinated alkanes and perfluorinated cycloalkanes, which are strong solvents for PTFE, may be suitable when mixed with one or more fluids which reduce the solvent power of said alkanes or cycloalkanes or, alternatively, the PTFE can be contacted with said alkanes or cycloalkanes for a sufficiently short duration and/or at a sufficiently low temperature that the PTFE is not significantly dissolved and suffers no significant loss of shape. The perfluorinated alkanes and cycloalkanes can be made by fluorination of the corresponding hydrocarbon compound, see for example British Patent 1,281,822.

By "dimer" herein is meant a byproduct from the fluorination of phenanthrene using a combination of CoF_3

and fluorine, as described in British Patent 1,281,822. When phenanthrene is thus fluorinated to perfluoro-tetradecahydrophenanthrene, a higher boiling fraction is obtained upon fractional distillation of the crude liquid product. This fraction has a boiling point in the range of 280°C to about 400°C at atmospheric pressure, typically about 316-340°C. It has a small amount of olefin and a very small amount of hydrogen in it which can be further reduced by postfluorination. It is believed that most of this mixture consists of the general structure



wherein z is 0, 1 or 2. Also believed to be present in smaller quantities are compounds from ring fusion and/or ring opening of the above compounds or their precursors such as



from the compound where z is 0 (it is not possible to say with assurance that this particular isomer is in the mixture - it is merely illustrative of one possible

structure consistent with the analytical data and the synthetic method). Similar fused structures from the compounds where z is 1 or 2 are also believed to be present. Although traces of hydrogen are present, the location has not been determined.

Other fluids suitable for processes I and II include non-halogenated aromatic organic liquids such as, for example, toluene, benzene, anisole, and mixtures thereof with halogenated fluids. Other non-halogenated fluids suitable for process I include cyclohexane, diethyl ether, ethyl acetate, C₁₋₄ alcohols, tetraethoxysilane, water, and mixtures thereof with halogenated fluids. Inorganic liquids such as the tetrachlorides of titanium, silicon and tin, and the trichlorides of iron and bismuth are also suitable fluids for process I, as are gases such as ammonia, nitrogen, and sulfur dioxide. Fluid swelling power can be increased by operating the process at elevated pressure.

In the present processes, heating and pressure are maintained for a period of time dependent on the temperature, pressure, solvent power and volatility of the penetrating fluid being used, and on the dimensions of the sample. The required time may extend from less than 1 minute to several hours, generally decreasing as the swelling power of the penetrating fluid increases. As previously noted, the contact time between PTFE and fluid penetrant under processing conditions should be sufficiently short to avoid significant dissolution of the polymer, or loss of viscoelastic memory therein. "Viscoelastic memory" is herein defined as the ability of the PTFE starting material to retain or regain its original shape, although its original dimensions may increase under the conditions of the invention process.

It is important in the practice of the invention that viscoelastic memory and hence the shape of the PTFE starting material be retained throughout the process. For example, if the polymer is introduced in the form of film or rod, film or rod are recovered at the end of the procedure without significant change in shape, although the dimensions of said shape may increase. If granular PTFE is used, granularity is retained in the product, although slight coalescence may occur. It should be understood that PTFE is not removed, e.g. by extraction, during the invention process; as demonstrated in the Examples, no loss in weight of polymer is detected. The polymer content of the initial (unextracted) products of the present process is greater than about 50% by weight. These products are not free-draining. Higher boiling fluids retained by these products may not be removed easily, e.g. by pressing or evaporation, and may require hot extraction with a solvent such as Freon®-113. Removal of high boiling liquids is particularly difficult and, for this reason, use of thinner sections of PTFE and more volatile fluids is preferred.

In process II, if the solvent-treated, unstretched, porous intermediate article is not in a form suitable for stretching, it may be converted to such a form by conventional procedures, such as, for example, skiving. Forms suitable for stretching include, but are not limited to, fibers, hollow fibers, film and sheet.

By "porous" products is meant products having a significant void content which are permeable to gases. The unstretched porous products of processes I and II have void contents (porosity) of up to about 50%. Both open and closed voids are thought to be present. Preferred void content of the unstretched porous articles of process II is about 15 to 35%. Stretching of the latter articles in process II increases porosity

up to 50% and higher. The porous products of process I of the invention may be fibrillar (Figures 1-3), have a relatively high surface area, and are crystalline with a heat of fusion of at least 35 J/g. The products are particularly useful as insulation, as gas permeable articles including membranes and diaphragms, and as catalyst supports and filters. As demonstrated in the Examples, porosity of the products is shown by the reduced density of the PTFE products measured on dry, essentially liquid-free samples, by increased surface area, and/or by measurement of gas transmission through membranes of the product.

A major advantage of the present process is the ability to introduce porosity into shaped articles of PTFE without loss of shape. Thus, film, fiber, wire and cable coatings, tubing and the like can be rendered porous without the necessity to refabricate the article. As retention time under processing conditions can be quite short, the process is suitable for continuous operation. For example, PTFE film or fiber, or PTFE coatings on wire or cable, can be rendered porous in a continuous operation wherein the article is drawn through a bath containing an appropriate fluid penetrant (Example 31) heated to an operating temperature of at least about 250°C. The latter method is particular suitable in process II for preparing porous film or fiber for subsequent uniaxial or biaxial stretching to form the final invention products. Alternatively, a billet of PTFE fabricated by compaction of virgin PTFE powder may be subjected to fluid penetration in a sealed pressure vessel. After optional fluid removal, the billet is skived into film and stretched to form the final product. As indicated, porosity of the intermediate invention products is substantially further

improved by subjecting said products to uniaxial or biaxial stretching.

The porous PTFE products of process I of this invention can be used to prepare composites of PTFE with one or more additional polymers, wherein said additional polymers occupy pores or voids in a matrix structure formed by the porous PTFE. The composites may be prepared by infusing one or more liquid and/or gaseous monomers, under pressure if necessary, together with appropriate polymerization initiators, into the porous PTFE previously prepared according to the invention process. Suitable monomers include, but are not limited to, ethylene, halogenated ethylenes, methacrylate and acrylate esters such as methyl, ethyl and butyl methacrylates and methyl, ethyl and butyl acrylates, styrenes, urethanes, polymerizable epoxides, difunctional monomers such as dimethacrylates and diacrylates and diglycidyl methacrylate to induce cross-linking, and the like. The selection of appropriate polymerization initiators will depend on the monomers chosen and will be apparent to those skilled in the art of polymerization. For example, α, α' -azobisisobutyronitrile (VAZ0-64®) is a well known free radical polymerization catalyst suitable for the polymerization of monomers such as methacrylates, acrylates, di(meth)acrylates, styrenes and the like.

The monomers may be polymerized in situ by the application of heat and/or irradiation such as UV or electrons. The PTFE composites prepared as described exhibit low friction similar to PTFE itself but have generally higher modulus and creep resistance. The composites are useful in load bearing applications including gaskets and seals.

A separate utility for the non-draining PTFE/absorbate composition of the invention is as an

improved lubricating surface, e.g. for brake cable.
When the PTFE/absorbate composite is flexed, a small
amount of the absorbate exudes to the surface at the
flex point; it is promptly reabsorbed when the stress is
5 removed.

Any type of fully polymerized, high molecular
weight, crystalline or partly crystalline PTFE is
operable in the invention processes. The PTFE may be in
any form; for example granular, fine powder, or
10 fabricated into shaped articles. By "fine powder" is
meant a coagulated and dried PTFE product of emulsion or
dispersion polymerization. By "granular" is meant a
product of suspension polymerization which may
optionally be milled. By "PTFE" is meant polytetra-
15 fluoroethylene homopolymer and copolymers of polytetra-
fluoroethylene, which may contain minor amounts of
repeat units of other monomers, providing said
copolymers are of high molecular weight, crystalline,
and non melt-fabricable, and their viscoelastic memories
20 are not significantly diminished by the penetrating
fluids under process conditions.

By "crystalline PTFE" is meant PTFE having a heat
of fusion of about 65 J/g in the virgin, as-polymerized
state, or a heat of fusion of less than 35 J/g,
25 preferably less than about 30 J/g, after said virgin
polymer has been heated above about 360°C and
recrystallized. The actual heat of fusion and
crystallinity of a given starting PTFE will depend on
its fabrication history. The starting PTFE employed in
30 the invention process, again depending on its
fabrication history, has at least one crystalline
melting point in the temperature range of about 325° to
about 342°C. However, the unstretched porous products
of process I of the invention have one crystalline

melting point, said melting point lying in the range of about 320 to 333°C.

It has been discovered that pore size in the porous products of process II of the invention can be
5 controlled by controlling the fluid used, fluid pressure and rate of cooling of the liquid-treated porous PTFE precursor articles. Such cooling-step control also affects the degree of crystallinity in said articles. Fluid-treated porous PTFE articles (porous precursors)
10 of process II that are suitable for conversion by stretching into the final porous products of the invention have crystallinities represented by heats of fusion in the range of about 35 to 65 J/g.

It has been found in the practice of the invention
15 process that porous precursors of lower crystallinity, as indicated by a heat of fusion toward the lower end of the above range, are more difficult to stretch. Small defects appear to be more detrimental to the integrity of a less crystalline precursor during stretching,
20 particularly when stretching more than fourfold on an areal basis. However, precursor film of lower crystallinity made from fine powder PTFE of higher molecular weight proved more likely to stretch without breaking than that made from granular PTFE. For this
25 reason, the finest pore size films were made from the fine powder PTFE.

In one embodiment of process II wherein unstretched, porous precursors are prepared and then converted into the final stretched, porous products of
30 the invention, virgin PTFE resin in a mold is first cold compacted into a billet or cylindrical preform by placing the mold between the platens of a hydraulic press and applying pressure. The powder compaction step may be carried out below or above room temperature with
35 appropriate adjustments made in pressure and dwell time

(time held at pressure) ¹⁴ to ensure that the resulting billet has sufficient integrity for further handling. At room temperature (about 20 to 35°C), pressures of about 2000 to 5000 psi (14 to 35 MPa) were suitable, with dwell times of about 1 to 120 minutes. Suitable billets can be formed from either granular or fine powder PTFE resins; the former normally require lower pressure and shorter dwell time. Such billets should have a specific gravity of at least about 1.7, preferably at least 1.9.

The billet so formed may be conventionally sintered before further handling, but such sintering is unnecessary in the practice of this invention. The billet is placed in a pressure vessel and immersed in an appropriate fluid and heated at a temperature close to the melting point of the polymer in the presence of the fluid under process conditions, for a time (hold period) sufficient for the fluid to uniformly penetrate the billet, but not change the shape of the billet, as discussed above. Temperatures in the range of about 320 to 360°C are suitable for many fluids.

Following the hold period at the selected processing temperature, the billet is subjected to slow, controlled cooling to about 50 to 100°C below the processing temperature. The hold period and cooling rate will depend upon the solvent power of the fluid, process temperature and pressure, and billet thickness.

Following treatment in the pressure vessel, the billet so processed is freed from unabsorbed fluid. Absorbed fluid may optionally be removed at any convenient point in the process, by any convenient means such as, for example, extraction, evaporation or suction.

The billet may be skived into continuous film or sheet of any desired thickness, by conventional methods.

The skived film or sheet is then stretched either biaxially or uniaxially about 300-1000% on an areal basis at rates of about 1 to 1,000%/second, preferably about 10 to 1,000%/second, most preferably about 100 to 500%/second, at temperatures in the range of about 20 to 150°C, preferably 80 to 120°C. Stretching at higher rates within the specified range results in somewhat finer pores.

The rate, extent, and temperature of stretching in process II of the invention are much lower, more easily controlled, less energy-intensive, and less demanding on machinery and on the PTFE itself than stretching methods of the art. Thus, the present process is an improvement over the prior art.

Moreover, the final, oriented shaped articles of this invention resist shrinkage, as exemplified hereinbelow. Shrink resistance is believed to result from lower orientation imposed by the relatively mild conditions of stretching in the present process compared to the prior art, and also to the unusually high degree of crystallinity of said oriented articles.

Stretching may be accomplished by any convenient means including batchwise using e.g., a pantograph, or continuously using a machine direction stretcher and a tenter frame in tandem, or using a continuous biaxial orientation machine.

The porous, shrink-resistant PTFE shaped articles of this invention exhibit a mean pore size of less than about 10 μm , a porosity of about 40% or higher, a melting transition with a peak in the range of 320 to 333°C with an associated heat of fusion of at least 35 J/g and no endotherm above 370°C. The shaped articles of the invention exhibit a morphology comprising interconnecting nodes and fibrils, said nodes being smaller or equal in size to said fibrils.

The porous, shrink-resistant PTFE shaped articles have outstanding chemical inertness and resist undesirable physical changes over a wide temperature range. The porous articles can be provided in many shapes such as, for example, film, sheet, filaments, tubing, rings and rod, and are useful in a wide variety of applications, including, but not limited to: filtration media for separating solids from fluids (gases and liquids); semi-permeable membranes for separating gases or gases and liquids; thermal and electrical insulation; protective clothing (for example, space suits, cleanroom suits, waterproof rainwear, gloves, footwear, socks, undergarments, medical drapings and garments,); sports equipment (for example, tents, sleeping bags); medical materials (for example, vascular, ligament or tendon prostheses, suture needle holders, damming materials, dental floss); seam and sealing tape; gaskets and other load-bearing articles.

In many of the applications where the articles of this invention find utility, advantage is taken of the pore structure which allows the selective transmission of fluids through the article, permitting many types of filtration or separations. An example is transmission of air and water vapor, but not liquid water, through articles of the invention.

It is often advantageous to bond or laminate the invention articles to other materials for, e.g., greater support, comfort or durability; bonding agents are able to significantly penetrate the pore network and, after curing, become locked therein. Certain perfluorinated alkanes and cycloalkanes such as perfluoro(tetradecahydrophenanthrene) and "dimer" described hereinabove, having high solvent power for PTFE, can effectively bond or laminate the invention articles without significantly penetrating the pore network. Any adhesive capable of

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bonding directly to PTFE will be suitable for forming laminates of the invention articles.

Methods of using the present porous, shrink-resistant PTFE shaped articles, including laminated materials, electrical and thermal insulation, protective materials, bearing materials, film, tubes, filaments, rods and the like are essentially those already described by Gore and Associates and in related art for porous PTFE articles prepared by different processes. Such methods, including laminations and bonding, are described in U.S. Patents 5,095,779, 5,128,209, 5,086,914, 4,187,390, 4,194,041, 4,978,813 and 4,208,745 herein incorporated by reference; and in numerous other U.S. Patents assigned to W. L. Gore & Associates, Inc. or related entities.

The invention is further illustrated with reference to the following examples: Examples 1-31 relate to the introduction of porosity into PTFE articles by treatment with fluid penetrants at elevated temperatures. Example 32 relates to the use of a porous product to prepare a polymer composite. Temperatures are expressed in degrees Celsius and percentages are by weight unless otherwise indicated.

EXAMPLE 1

Preparation of Porous Polytetrafluoroethylene by Treatment with Krytox® Vapor

A piece of consolidated polytetrafluoroethylene (PTFE) was suspended in refluxing Krytox®-143AZ fluorinated (perfluoroalkylpolyether) oil vapors at 330 to 335°C for 2 h. The system was protected by a nitrogen atmosphere. The physical changes noted in the sample were as follows:

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	<u>Before</u>	<u>After</u>	<u>Change, %</u>
Thickness, cm	1.35	1.75	+30
Length, cm	4.45	4.50	+1
Width, cm	2.65	2.48	-6
Weight, g	37.32	41.28	10.6

The product contained 3.96 g or 9.6 weight % Krytox® and was more slippery than the initial PTFE sample. About 3.1% of the Krytox® was pressed out when
5 the product was pressed between paper sheets under 15,000 psi pressure.

The above experiment was repeated except that the heat treatment was extended to 28 h. The product was found to contain 23.5 weight % Krytox®. A 2.47 g piece
10 of the sample was extracted for about 24 h with Freon®-113 (F-113, 1,1,2-trichloro-1,2,2-trifluoro-ethane) and dried to constant weight. The sample piece now weighed 1.872 g, indicating a weight loss of 0.60 g or 24.3%. A scanning electron micrograph showed that
15 the interior of the sample was comprised of a mass of interconnecting fibers (Figure 1).

The above experiment was repeated except that the heat treatment was continued for 18 h. The product contained 17.6 wt % Krytox® and had the following
20 physical properties compared with the PTFE starting material:

Physical Properties of PTFE/Krytox® Composites

	<u>Starting PTFE</u>	<u>PTFE/Krytox® Composites</u>
Tensile Properties		
Tensile Str, psi		
Yield	2046	574
Max	3672	2915
Break	3671	2550
Elongation, %		
Yield	86.7	213
Break	230	370
Modulus, Kpsi	89.5	22.5
Izod Impact		
ft lb/in of notch	1.87	1.36
Deformation, %		
(23°, 24 h, 800 psi)	2.5	9.8
Surface Area, m ² /g	0.0019	5.42*
*Measured after removal of Krytox® by extraction with F-113.		

EXAMPLES 2-265 Preparation of Porous PTFE, Various Fluids

In Examples 2-26, sections of PTFE plaques, measuring 1.5 x 0.125 x 5 or 6 in., were placed in a 1 liter monel corrosion-resistant vessel. The plaques were fabricated by either sintering or cold pressing; in the Examples under "Prep", hot compression molded samples are coded "H", cold pressed and sintered samples are coded "S". The liquid or vapor used to prepare the porous PTFE product was poured into the vessel or, if gaseous, introduced into the cold vessel under pressure.

15 The vessel and contents were then heated to the test temperature. After heating for a prescribed time, the vessel was cooled to room temperature and the pressure

was released. The vessel was then opened and the sample was retrieved.

In Examples 2 and 3, perfluorinated liquids were used to prepare porous products according to this invention. In Examples 4-10, partially fluorinated liquids, or mixtures thereof with non-fluorinated liquids, were used. In Examples 11-26, unfluorinated liquids or gases were used to prepare porous PTFE products. Examples 22-26 employed non carbon-containing compounds. The processing conditions and the densities of the porous products obtained in Examples 2-26 are summarized in Table 1. Physical properties of products obtained in Examples are shown in Table 2. Scanning electron micrographs of the products of Examples 23 and 26 are shown in Figures 2 and 3.

TABLE 1

Ex.	Prep.	Fluid.	Conditions			
			Temp. (°C)	Time (h)	Pressure (psi, gage)	Density (g/ml)
2	H	HFP ^a cyclic dimer	340	2	1130	1.80
3	H	iso C ₆ H ₁₄	350	3	1100	*
4	H	FC-20 ^a	350	4	1100	1.81
5	H	F-125 ^a	345	2	3800	1.55
6	H	F-113	335	4	1310	1.77
7	H	F-113	350	2	1450	1.79
8	H	F-113 + Krytox [®]	350	2	1360	1.67
9	H	CFCl ₄ + F-113	350	1	1100	1.71
10	H	Cyclohexane + isoC ₆ F ₁₄	250	1	1360	1.73
11	H	CCl ₄	350	2	1190	1.46**
12	H	CCl ₄	320	3	880	1.94
13	H	TCE ^a	300	3	395	1.65
14	H	CO ₂	350	2	3260	1.96
15	H	Cyclohexane	350	2	1070	1.72
16	H	Methanol	350	2	3800	1.67
17	H	Methanol + Cyclohexane	350	1	2600	1.86
18	H	Ethanol	340	1	2700	1.84
19	S	(C ₂ H ₅) ₂ O	340	1	2300	1.91
20	S	Et Acetate	340	1	1800	1.86
21	S	Toluene	340	2	870	1.60
22	H	SO ₂	350	2	2038	1.95
23	H	Water	350	2	2300	2.08
24	H	Water	325	4	1690	2.15
25	H	NH ₃	340		3200	1.86
26	H	N ₂	340	2	15,400	1.61

* Surface area, 5.4 m²/g; surface area of starting PTFE, 0.084 m²/g.

** Surface area, 6.0 m²/g.

a HFP = Hexafluoropropene

FC-20 = Perfluoro-n-butyltetrahydrofuran

F-125 = Pentafluoroethane

5 TCE = Tetrachloroethylene

TABLE 2

Properties of porous PTFE after compression

at 150°C and 13,500 psi

<u>Property</u>	<u>Ex. 5</u>	<u>Ex. 6</u>	<u>Ex. 7</u>	<u>Ex. 8</u>	<u>Ex. 12</u>	<u>Ex. 24</u>
<u>DSC</u>						
M.P.°C	332	331	332		331	330
Heat Fusion	54	57	61		43	30
Density g/ml	2.04	1.99	1.79	2.04	2.11	2.17
<u>Tensile Props.</u>						
Tens. Str., psi						
Yield	812	1278	1360	802	1291	1722
Max	827	1837	2209	1641	1896	2333
Break	293	1816	2207	1628	1881	2316
Elongation, %						
Yield	5.0	14.4	5.0	13.3	11.7	43.0
Break	30.5	247	358	146	255	205
T/Mod, kpsi	125	140	158	92.2	131	178
Izod Impact						
ft-lb/in notch	1.7	2.3	2.4	2.0	2.0	2.6

10

EXAMPLE 27

Evidence of Porosity in a Product of the Invention

The 1 liter vessel used in the previous examples was charged with two 31 mil (0.79 mm) thick strips of sintered PTFE separated by monel plates to prevent sticking and loss of shape were immersed in CCl₄ and subjected to the following heating schedule:

310°C for 30 min.

330°C for 30 min.

340°C for 1 h.

15

310°C for 1 h.

After drying the resulting porous sheets were 38 mils thick and were porous to nitrogen gas; flow rates of nitrogen flowing through the sheets at
5 different nitrogen pressures were:

N ₂ Pressure (psi)	N ₂ Flow (ml/h)
6.8	226
6.8 (1 h later)	227
2.1	45
1.2	19.5

Similar qualitative nitrogen permeation tests were run on strips 66-164 mils (1.7-4.2 mm) thick of the
10 porous products from Examples 2, 4-6, 9, 11, 13-16, 19-22, except that the tests were run at room temperature (21°C) and at 6 psi nitrogen pressure. All the strips except that of Example 20 (4.1 mm) were permeable; the strip from the product of Example 20 was
15 permeable at higher nitrogen pressures.

EXAMPLE 28

Preparation of Porous PTFE Films

PTFE films, 3 mils thick and 5 mm wide were slowly passed through refluxing Krytox®. The films were easily
20 drawn while hot to about 5-times their original length, and, while still hot, recovered their original length when tension was released. However, if the 5-fold extension was maintained while the polymer cooled and crystallized, the films did not shrink and measured
25 1.5 mil in thickness. A portion of one film weighing 0.6602 g was extracted for 1 day with FC-113 and then dried to constant weight. Its final weight was 0.4153 g, indicating that the sample before extraction contained 37 weight % Krytox®. The starting film,
30 before processing, could only be drawn 2-fold and was

slightly elastomeric. The porous processed film was not elastomeric.

The rate of Krytox® adsorption by 3 mil PTFE film was measured by soaking film in hot Krytox® 143AZ for various times and measuring the amount (%) of Krytox® in the film:

<u>Soak Time</u>	<u>Krytox® Temp.</u>	<u>Krytox® in Film</u>
(sec)	(°C)	(%)
10	345	6
30	345	16
60	345	16
1800	344	16
300	300	10
300	310	15

A 7 in x 12 in. x 1 in. wide externally heated monel trough containing refluxing Krytox® was used to process larger sheets of PTFE film in continuous mode. Three mil film pulled through the refluxing Krytox® at a rate of 1 ft/min was found to contain 9.3 weight % Krytox®. After removal of the Krytox® from the film by extraction with F-113 and drying, the porous film was opaque relative to the unprocessed film. The porous film lost most of its opaqueness and developed a blue hazy structure when stretched; the unprocessed film became more opaque on stretching.

Films prepared as above were extracted with F-113 and cut into 4.5 mm wide strips labelled A-E which were drawn over hot pins. Krytox® content before extraction and draw conditions are shown relative to unprocessed control film in Table 3; physical properties are shown in Table 4.

25

TABLE 3

<u>Sample</u>	<u>Initial Krytox® Content, %</u>	<u>Draw Ratio</u>	<u>Draw Temp. °C</u>
A	0	4.8	345
B	0	4.8	300
C	13.5	3.2	300
D	13.5	3.3	345
E	11.1	3.3	316

TABLE 4

<u>Sample</u>	<u>Init. Mod. gpd</u>	<u>Tenacity, max. gpd</u>	<u>Elong., %</u>	<u>Toughness gpd</u>
A	4.74	0.70	27.6	0.0991
B	3.91	0.65	33.1	0.1105
C	2.68	0.643	64.2	0.2117
D	2.62	0.717	69.4	0.2524
E	2.95	0.617	67.5	0.2229

It was found possible to draw the films processed with Krytox® in two directions.

5

EXAMPLE 29Preparation of Large Sections of Porous PTFE

In the following experiment, a 1 gallon Hasteloy autoclave was charged with Teflon® TFE resin grade 7A, from DuPont, in the form of a sintered rod weighing
 10 1248.4 g and measuring 5.75 in. x 3 in. diameter with a 0.94 in. core hole through the length. F-113 was added to the autoclave such that the PTFE rod, standing on end, was completely immersed in about 7 in. of the liquid. The autoclave was closed and heated according
 15 to the following schedule:

To 200°C and held for 30 min;

250° for 30 min;

300° for 30 min;

350° for 4 h;

20 330° for 1 h;

26

310° for 2 h;

cool to ambient temperature.

The product weighed 1527 g, indicating a weight gain of 279 g, and measured 6.6 in. long x 3.1 in.

5 diameter. The core diameter was 0.98 in. After drying to remove the F-113 the rod weighed 1248.5 g and had a density of 1.81 g/ml. Film skived from the rod could be both uniaxially and biaxially stretched.

The above experiment was repeated with similar
10 billets of Teflon® 7A which had been either sintered or cold pressed, wherein the F-113 was replaced, respectively, with methanol, water, CCl₄, Krytox®-143 AZ and cyclohexane.

EXAMPLE 30

15 Porous Products from PTFE Powder

Teflon® 7C TFE Granular Resin molding powder (94.3 g) was immersed in refluxing Krytox® for 20 h. On cooling, the recovered product was in the form of a soft lump weighing 178 g and containing 47% Krytox®. Films
20 and other shaped objects could be prepared by hot pressing.

EXAMPLE 31

A mixture of oligomers ("dimer"), which is a by-product of the fluorination of phenanthrene was
25 decolorized by passage over a hot bed of basic alumina (ICN Biochemicals); this mixture is an embodiment of "dimer", as described above. Distillation of the mixture under reduced pressure provided 7 fractions, the lightest of which boiled at 117°C at 0.6 mm (80 Pa), and
30 the heaviest boiled at 255-287°C at 0.2 mm (27 Pa). The fractions were not further characterized.

A test tube 30 cm long of 3.4 cm diameter was half filled with the "dimer" mixture and placed in a Woods' metal bath at 340-360°C. The "dimer" refluxed gently at

27

316-318°C. Silvered copper wire coated with PTFE was plunged into the hot liquid and then into F-113 to cool and extract the "dimer".

TABLE 5

<u>Sample</u>	<u>Coated Wire, mil</u>	<u>Initial Coat, mils</u>	<u>Time, sec.</u>	<u>Final Coat, mils</u>	<u>Coating Dens.g/ml</u>
A	43	18	20	22.5	1.6
B	30	2.5	60	4.0	1.3
C	30	2.5	30	4.0	1.3

- 5 A = Silver coated Cu, Multistran, coated with sintered PTFE
B,C = Silver coated Cu, Multistran, coated with unsintered PTFE.

In similar experiments, where the "dimer" was employed as-received without decolorization,
10 substantially the same results were observed.

EXAMPLE 32

A sheet of PTFE having continuous pores, prepared by treatment in refluxing Krytox®, as described in Example 28, was immersed in liquid methyl methacrylate
15 (MMA) containing 0.2% by weight of VAZO-64® polymerization initiator and centrifuged for about two hours, during which time MMA/initiator was absorbed by the PTFE until no further weight gain was observed. The "composite", together with a small amount of additional
20 MMA/initiator, was then placed between glass plates and the "sandwich" was heated at 60°C for 4 hours, then at 80°C for 5 hours to complete the polymerization of the absorbed MMA. The resulting PTFE/Poly(methyl methacrylate) composite contained 22% by volume of
25 poly(methyl methacrylate) and had the following physical properties, compared with unprocessed commercial PTFE sheet:

	<u>Commercial</u> <u>PTFE Sheet</u>	<u>PTFE/PMMA</u> <u>Composite</u>
Tensile Properties		
Tensile Strength, psi		
At Yield	2046	1760
At Max	3672	1900
At Break	3671	1250
Elongation, %		
At Yield	86.7	6.7
At Break	230	105
Tensile Modulus, kpsi	89.5	168
Izod Impact, ft-lb/in of notch	1.9	1.05

Compressive creep resistance of the composite was tested as follows: A plaque of the composite 0.125 in. thick was cut into 0.5 in. squares. Four of the squares were stacked to give a 0.5 in. high cube. A similar layered cube was prepared from commercial PTFE. A pressure of 1 kpsi was applied to both cubes for 24 h at room temperature and the loss in height was measured continuously. After 24 h the cube of commercial PTFE had compressed 3.36% while the cube of composite had compressed 1.59%. Five minutes after release of pressure the % compression was 2.78 and 1.06%, respectively.

The following Examples 33-68 relate to preparation of porous PTFE precursor articles and their conversion by stretching into the final stretched porous products of the invention.

Unless otherwise indicated, films were formed by skiving billets which had been rendered porous by elevated temperature liquid treatment in a 1 gallon Hastelloy pressure vessel. Billets were formed at room temperature by compacting 1250 g of virgin PTFE resin powder into a cylindrical preform about 15 cm high and

7.7 cm in diameter containing a concentric hole 2.4 cm in diameter. The granular resin employed was Teflon® Type 7A, the fine powder resin was Teflon® TE 3641 resin, both available from DuPont. The granular resin was formed into billets at a pressure of 2200 psi applied for 4 minutes; the fine powder, at a pressure of 4700 psi applied for 30 minutes or more. Billets were skived by mounting the billet on a machinist's lathe and employing a diamond-edged knife. Film so produced was stretched by loading square film specimens, 11.4 cm edge length, into a pantograph stretcher available from the T. M. Long Co., Inc., Somerville, NJ. Unless otherwise indicated: samples were preheated for 2 to 3 minutes before stretching, stretching rate was 75%/second, stretching temperature was 100°C, and samples were stretched biaxially at equal rates and to equal extents. No difference was detected between stretching in the two directions sequentially or simultaneously, and hence both methods have been employed herein without distinction.

Thermal analysis was performed using a System 2000 single cell differential scanning calorimeter available from TA Instruments, Inc. Wilmington, DE. Unless otherwise noted, specimens were heated at a rate of 10°C/min to 400°C, followed by cooling at a rate of 1°C/min to about 250°C, then reheated at 10°C/min to 400°C. Heats of fusion and melting points were determined using the built-in software.

Air permeability and pore-size distribution were determined using a Porometer II instrument available from Coulter Electronics, Ltd., Luton, UK. The Porometer utilized a bubble point technique for determining the pressure at which the initial air flow was detected through a thoroughly wetted test specimen. The pore size distribution, including the mean pore

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size, was determined by measuring the air flow rate as a function of pressure above the bubble point. The pore-size distribution calculation, performed automatically by the Porometer, provides the diametric size distribution of a population of straight cylindrical pores which would exhibit the same pressure/flow rate data as the test membrane. Since the pores in microporous PTFE films are highly irregular in cross-section, the calculated pore sizes are relative rather than absolute. However, the method provides consistent results between samples [to sample] of comparable morphology, and is widely practiced in the art.

The Porometer II is unable to measure the size of pores smaller than about 0.05 μm . As some of the pores of films of the invention were smaller than 0.05 μm , the calculation of the mean flow pore size is believed to overemphasize the larger pore end of the distribution. Mean flow pore sizes given in the ensuing Examples may therefore be somewhat higher than the actual values.

Pressure in the pressure vessel was determined using a model IBH103 pressure transducer manufactured by Magnetek Transducer Products, Simi Valley, CA93065.

Table 6

Ex.	Resin Type	Pressure in Vessel (psi)	Void Content in Skived Film (%)	Heat of Fusion (J/g)	Areal Stretch Ratio	Stretched Film Thickness (μm)	Stretched Film Fusion (J/g)	% of Total Heat from 328 °C Transition	Void Content in Stretched Film (%)	Mean Flow Pore Size (μm)	Max. Pore Size (μm)	Normalized Air Perm. (l-μm/sq.cm-min-bar)
33	Fine Powder	1216	20	40	4.00	48	38	100	48	0.07	0.08	8
34	Fine Powder	1588	21	40	4.00	46	39	100	47	0.07	0.09	8
35	Fine Powder	1588	21	40	4.00	46	47	100	46	0.07	0.08	8
36	Fine Powder	2097	25	43	4.00	44	46	100	49	0.09	0.11	12
37	Granular	1950	22	44	6.25	40	43	100	59	0.10	0.13	24
38	Granular	1950	22	44	4.00	53	44	100	51	0.07	0.13	NA
39	Granular	1950	22	44	3.10	54	44	100	44	0.07	0.14	NA
40	Granular	1950	22	44	6.25	41	41	100	61	0.10	0.14	22
41	Fine Powder	1481	18	45	4.00	46	44	93	50	0.07	0.10	9
42	Granular	1502	12	45	4.00	53	45	100	52	0.10	0.14	18
43	Granular	1450	13	46	4.00	54	44	100	51	0.10	0.14	18
44	Fine Powder	1796	24	47	4.00	46	45	100	55	0.08	0.11	12
45	Granular	1646	12	47	4.00	54	46	100	48	0.11	0.16	20
46	Fine Powder	2050	21	47	6.25	33	44	82	61	0.13	0.16	25
47	Fine Powder	2050	21	47	5.06	38	45	100	59	0.13	0.16	30
48	Fine Powder	2050	21	47	6.25	30	45	100	59	0.13	0.16	29
49	Fine Powder	2050	21	47	6.25	30	44	85	57	0.13	0.16	28
50	Granular	1889	18	48	9.00	34	45	100	65	0.14	0.15	31
51	Granular	1889	18	48	4.00	53	49	100	56	0.09	0.16	24
52	Granular	1935	13	49	4.00	55	49	100	60	0.14	0.21	37
53	Granular	1935	13	49	9.00	34	46	100	72	0.16	0.21	50
54	Fine Powder	2308	13	49	4.00	50	49	86	51	0.10	0.14	17
55	Granular	1800	14	51	9.00	36	49	100	74	0.19	0.25	67
56	Fine Powder	2350	26	53	4.00	54	54	100	61	0.18	0.25	47
57	Granular	2496	20	55	9.00	48	46	100	78	0.34	0.48	166
58	Granular	2536	18	56	9.00	44	46	100	77	0.29	0.39	139
59	Granular	2400	24	56	6.25	55	49	100	75	0.33	0.54	160

EXAMPLES 33-59

In these examples both fine powder and granular resins were employed. Billets were fabricated therefrom and exposed to an excess of trichlorotrifluoroethane at about 350°C for four hours at the pressures shown in Table 6, after which they were cooled to 330°C and held for one hour, then cooled further to 310°C and held for two hours, after which electrical power to the heaters was turned off, and the vessel was allowed to cool to room temperature over a period of about 10 hours.

As shown in Table 6, the void content of films skived from the treated billets ranged from 12 to 26%, and of the stretched films, from 44 to 78%. Mean flow pore size and maximum pore size (related to the bubble point) ranged from 0.07 to 0.42 μm , and 0.08 to 0.64 μm , respectively. Air permeability, normalized for a one micron film thickness and 1 bar applied pressure, ranged from 8 to 166 ($1\text{-}\mu\text{m}/\text{cm}^2\text{-min-bar}$), the higher permeability associated with the larger pore sizes, as expected from theoretical considerations of flow rates through porous substances.

The heats of fusion of the skived films ranged from 40 to 56 J/g, and of the stretched films, from 38 to 54 J/g. In the stretched films, the heat of fusion associated with the 320-333°C DSC endotherm comprised at least 80% and usually 100% of the total heat of fusion of the microporous film. In none of Examples 33-59 was an endotherm above 370°C detected.

These examples show that the maximum pore size in the stretched films of the invention is closely related to the heat of fusion of the associated unstretched, skived film. This is shown in Figure 4 wherein the maximum pore size is plotted on a logarithmic scale vs. the heat of fusion on a linear scale.

A correlation is also seen between the heat of fusion of the skived film and the pressure of the fluid penetrant in the pressure vessel, as shown in Figure 5 wherein the heat of fusion of the skived film is plotted against the maximum pressure.

COMPARATIVE EXAMPLES 1 to 5

Four commercially available microporous PTFE films and one non-porous commercially available PTFE film were evaluated using the same methods as in Examples 33-59.

Results are given in Table 7.

Table 7

Comp. Ex.	Manufacturer	Film Thickness (μm)	Void Content (%)	Max. Pore Size (μm)	Mean Flow Pore Size (μm)	Air Perm. ($1\text{-}\mu\text{m}/\text{cm}^2\text{-min-bar}$)	Film Heat of Fusion (J/g)	% of Total Heat from 328 °C Transition	Endotherm above 370 °C
1	W.L. Gore & Co. Newark DE	83	78	0.49	0.30	204	39	33	1.5 J/g @ 374 °C
2	W.L. Gore & Co. Newark DE	38	79	0.46	0.39	213	32	38	1.9 J/g @ 375 °C
3	Nuclepore	N.A. ^a	N.A.	0.56	0.50	N.A.	35	71	1.4 J/g @ 374 °C
4	Sumitomo Japan	40	66	0.70	0.57	208	28	64	3.1 J/g @ 375 °C
5	DeWal Industries	51	0 ^b	N.A.	N.A.	N.A.	27	100	None

^a Mounted on a Polypropylene backing.^b Commercially available skived PTFE film. Non-porous.

A comparison of the results in Table 7 with those in Table 6 illustrates the inventive features of the present invention. The heats of fusion of the former films were always less than 40 J/g in total, and less than 75% of that total was associated with the 320 to 333°C DSC endotherm. All four of the films exhibited an endotherm of at least 1 J/g at a temperature above 370 °C.

The thermal "signature" of the films of this invention more closely resembles that of non-porous skived PTFE film than that of the microporous films of the prior art. The principal difference in thermal signature between films of the invention and that of non-porous skived PTFE films is that the heat of fusion, and hence the crystallinity, of the former is at least about 50% higher.

EXAMPLES 60-62

These examples demonstrate that the object of this invention may be attained by stretching in one direction only, and also illustrate the effects of different rates of extension.

Films were prepared as in Examples 51 and 52, except that they were stretched 4x in the machine or longitudinal direction only. Stretch rates and results are shown in Table 8.

In Example 61, a stretching rate at the low end of the range suitable for the practice of this invention was employed, producing film well within the scope of the invention. In Example 62, a rate at the high end of the range preferred for the practice of this invention was employed, again producing film well within the scope of the present invention.

A comparison of Examples 61 and 62 shows that increasing stretch rate by about 50x (about 5000%)

resulted in a pore size approximately 35% smaller and a permeability about 40% lower.

Table 8

5

Effects of uniaxial stretching and stretching at different rates on the properties of the films of this invention

	Example 60	Example 61	Example 62
Stretch Rate (%/s)	75	7.5	370
Thickness (μm)	46	48	41
Stretched Film Heat of Fusion (J/g)	46	45	49
Mean Pore Size (μm)	0.10	0.13	0.09
Voids (%)	52	55	51
Air Perm. ($1\text{-}\mu\text{m}/\text{cm}^2\text{-min-bar}$)	12	19	8
% From 328° Endotherm	100	89	100
Endotherm above 370°C	NONE	NONE	NONE

10 These examples further show that pore size and permeability of the films of the invention are relatively independent of stretching rate over the wide range of rates suitable for the practice of the invention. This result is a clear departure from the
15 teaching of the art, especially that of Gore and Tamaru, which is inoperable at the stretching rates employed in Examples 60-62.

EXAMPLE 63

20 A billet of granular PTFE was heated in the presence of an excess of 1,1 difluorotetrachloroethane for 4 hours at 335°C and about 725 psi pressure. The billet was cooled to 300°C, held for 30 minutes, then cooled to 270°C, and held for another 30 minutes, after
25 which the heat was shut off and the pressure vessel was permitted to cool naturally to room temperature. Film skived from the billet was stretched 4x under standard

conditions to give a 26 μm thick microporous film with 56% voids, a mean pore size of 0.15 μm , and a heat of fusion associated with the 320 to 333°C DSC endotherm of 49 J/g, which was 97% of the total heat of fusion. No
5 endotherm was detected above 370°C.

EXAMPLE 64

A billet of granular PTFE was heated in the presence of excess carbon tetrachloride for 3 hours at 315°C and about 1050 psi pressure. The billet was then
10 cooled to 300°C, held for 1 hour, then cooled to 275°C, and held for another 1 hour, after which the heat was shut off, and the pressure vessel was permitted to cool naturally to room temperature.

Film skived from the billet was stretched 3.1x
15 under standard conditions to give a 30 μm thick microporous film having 46% voids, a mean pore size of 0.10 μm , and a heat of fusion associated with the 320 to 333°C DSC endotherm of 45 J/g, which was 100% of the total heat of fusion. No endotherm was detected above
20 370°C.

EXAMPLE 65

A billet of granular PTFE was heated in excess perfluorohexane for 3 hours at 400°C and about 2950 psi pressure. The billet was cooled to 330°C, held for 1
25 hour, then cooled to 310°C, and held for another hour, after which the heat was shut off and the pressure vessel was permitted to cool naturally to room temperature.

Film skived from the billet was stretched 4x under
30 standard conditions to give a 71 μm thick microporous film with 78% voids, a mean pore size of 0.18 μm , and a heat of fusion associated with the 320 to 333°C DSC endotherm of 50 J/g, which was 97% of the total heat of fusion. No endotherm was detected above 370°C.

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EXAMPLE 66

In this Example the objects of the invention are provided by a process comprising continuous film treatment. A commercially available (Furon Inc.) skived
5 film of PTFE, about 75 μm in thickness, was fed continuously at a line speed of about 1.2 m/min via a series of rollers into a corrosion-resistant metal bath containing a mixture of oligomers ("dimer") which are a by-product of the fluorination of phenanthrene as
10 described hereinabove, and withdrawn via a similar series of rollers to a constant speed wind-up. The bath was maintained at a temperature of about 290°C. Total residence time in the bath was about 30 seconds.

The film was extracted with trichlorotrifluoro-
15 ethane to remove the absorbed fluid. The film was then stretched 9x at standard rate but at 50°C. Mean pore size was 0.09 μm , porosity was 52%, heat of fusion associated with the 320 to 333°C DSC endotherm was 38 J/g, which was 100% of the total heat of fusion. No
20 endotherm was detected above 370°C.

EXAMPLE 67

Disks 2" in diameter were cut from the films of Examples 33, 55, 65 and Comparative Example 1. The disks were each placed in isopropyl alcohol at room
25 temperature for a period of 88 hours. They were then removed, laid flat, and air-dried. The film of Comparative Example 1 shriveled badly, assuming a highly irregular shape, considerable 3-dimensional bumps, and smaller in overall effective diameter. The films of
30 Examples 33, 55 and 65 were unaffected.

Similar results were obtained in experiments as above wherein isopropyl alcohol was replaced with toluene, commercial cleaning fluid (chlorinated hydrocarbons and petroleum distillates), ethyl alcohol,
35 Krytox® 161-40 or mineral oil.

Figure 6 (a, b, c, d and e) clearly illustrate the difference in shrinkage between the films of this invention and the prior art. In Figure 6 (a, b, c, d and e), the 2 inch disk was a circular piece of cardboard identical in shape to each of the films prior to wetting.

The surface texture of the films of the invention were unchanged by wetting, as was the notch on the periphery of the film of Example 66.

10

EXAMPLE 68

A cold-pressed billet of granular PTFE, 5 15/16 inch high x 3 inch diameter containing a 15/16 inch concentric longitudinal hole, weighing 1247 g, was placed in a 1 gallon hastalloy pressure vessel containing sufficient benzene so that the top of the billet was about 1 inch below the surface of the liquid. the vessel was heated to a mazimum temperature of 346°C, at a pressure of about 950 psi, and held for four hours.

The density of the billet so treated was 1.89 g/cc. The heat of fusion of the skived film was 41.4 J/g. The skived film was stretched 2x x 2x at a rate of 75%/second. The resulting film was 52 µm thick, and contained 51% voids. The mean pore size was 0.10 µm. The heat of fusion of the stretched film was 41 J/g, with 100% of the heat of fusion associated with the 320 to 333°C DSC melting endotherm. No endotherm above 370°C was present.

What is claimed is:

1. Process for preparing porous polytetrafluoroethylene (PTFE) comprising:

(a) contacting PTFE with a fluid which
5 penetrates and swells but does not significantly dissolve the polymer or eliminate viscoelastic memory therefrom, at a temperature in the range of about 250-400°C;

(b) cooling and separating the penetrated
10 polymer from unabsorbed fluid, said polymer containing up to about 50% by weight of absorbed fluid; and

(c) removing the absorbed fluid, to form a porous product having a single DSC melting endotherm, said endotherm being in the range of about 320 to 333°C
15 with an associated heat of fusion of at least 35 J/g.

2. Process for preparing a non-draining polymer composition comprising:

(a) contacting PTFE, in an inert atmosphere, with a fluid which penetrates but does not significantly
20 dissolve the polymer or eliminate viscoelastic memory therefrom, at a temperature in the range of about 250-400°C; and

(b) cooling and separating the penetrated polymer/fluid composition from unabsorbed fluid, said
25 composition containing up to about 50% by weight of absorbed fluid.

3. Process according to Claim 1 wherein, in step (c), absorbed fluid is removed by evaporation or suction, or by extraction into a second, more volatile
30 fluid, wherein said second fluid is removed by evaporation.

4. Process according to Claim 1 wherein the porous PTFE product is a shaped article.

5. Process according to Claim 2 wherein the
35 porous PTFE product is a shaped article.

6. Process according to Claim 1 wherein the fluid is liquid at 25°C.

7. Process according to Claim 2 wherein the fluid is liquid at 25°C.

5 8. Process according to Claim 1 wherein the fluid is a liquid is selected from the group consisting of one or more halogenated hydrocarbons wherein the halogen is fluorine and/or chlorine, non-halogenated aromatic hydrocarbons, and non-halogenated aromatic hydrocarbons
10 containing one or more substituents that are inert under process conditions.

9. Process according to Claim 2 wherein the liquid is selected from the group consisting of one or more halogenated hydrocarbons wherein the halogen is
15 fluorine and/or chlorine, non-halogenated aromatic hydrocarbons, and non-halogenated aromatic hydrocarbons containing one or more substituents that are inert under process conditions.

10 10. Process according to Claim 8 wherein the halogenated hydrocarbon is perfluorinated.

11. Process according to Claim 9 wherein the halogenated hydrocarbon is perfluorinated.

12. Process according to Claim 6 wherein the liquid is a perfluorinated polyether or heterocyclic
25 monoether.

13. Process according to Claim 7 wherein the liquid is a perfluorinated polyether or heterocyclic monoether.

14. Process according to Claim 6 wherein the
30 liquid is a mixture of one or more perfluorinated hydrocarbons and at least one non-perhalogenated liquid.

15. Process according to Claim 7 wherein the liquid is a mixture of one or more perfluorinated hydrocarbons and at least one non-perhalogenated liquid.

16. Process according to Claim 6 wherein the liquid is a mixture of liquids comprising at least one halogenated hydrocarbon wherein the halogen is fluorine and/or chlorine, and at least one non-halogenated organic liquid.

17. Process according to Claim 7 wherein the liquid is a mixture of liquids comprising at least one halogenated hydrocarbon wherein the halogen is fluorine and/or chlorine, and at least one non-halogenated organic liquid.

18. Process according to Claim 6 wherein the liquid is inorganic.

19. Process according to Claim 7 wherein the liquid is inorganic.

20. Process according to Claim 18 wherein the inorganic liquid is a halide melting below 300°C selected from the group consisting of Ti, Si, Sn, Fe and Bi.

21. Process according to Claim 19 wherein the inorganic liquid is a halide melting below 300°C selected from the group consisting of Ti, Si, Sn, Fe and Bi.

22. Process according to Claim 1 wherein in step (a) the PTFE and fluid are subjected to elevated pressure.

23. Process according to Claim 2 wherein in step (a) the PTFE and fluid are subjected to elevated pressure.

24. Process according to Claim 1 wherein the temperature is about 290 to 360°C.

25. Process according to Claim 2 wherein the temperature is about 290 to 360°C.

26. Composition prepared by the process of Claim 1.

27. Composition prepared by the process of Claim 2.

28. Process of preparing a composite comprising:

- (a) contacting PTFE, in an inert atmosphere,
5 with a fluid which penetrates and swells but does not significantly dissolve the polymer or eliminate viscoelastic memory therefrom, at a temperature in the range of about 250-400°C;
- (b) cooling and separating the penetrated,
10 swollen polymer from unabsorbed fluid;
- (c) removing the absorbed fluid to form a porous product;
- (d) infusing one or more polymerizable monomers and appropriate initiators into the porous
15 product from step (c); and
- (e) polymerizing the one or more monomers to form the said composite.

29. Composite comprising PTFE and up to about 50% by weight of one or more polymers other than PTFE,
20 prepared according to the process of Claim 28.

30. Composite according to Claim 29 wherein the one or more polymers include poly(methyl methacrylate).

31. An unstretched, porous PTFE containing up to 50% voids, and having a single crystalline melting
25 point, said melting point being in the range of 320 to 333°C with an associated heat of fusion of at least 35 J/g.

32. A shaped article of the unstretched, porous PTFE of Claim 31.

30 33. Process of converting a PTFE coating on an article to the composition of Claim 26.

34. Process of converting a PTFE coating on an article to the composition of Claim 27.

35 35. Process according to Claim 33 wherein the article is wire, cable, fiber or tubing.

36. Process according to Claim 34 wherein the article is wire, cable, fiber or tubing.

37. Process according to Claim 35 wherein the article is electrically conducting metal wire or cable.

5 38. Process according to Claim 36 wherein the article is electrically conducting metal wire or cable.

39. A porous, shrink-resistant polytetrafluoroethylene (PTFE) shaped article having a mean pore size of less than about 10 μm , a porosity of at least 40%, a
10 DSC melting endotherm in the range of 320 to 333°C with an associated heat of fusion of at least 35 J/g, and having no DSC melting endotherm at temperatures above 370°C.

40. The PTFE article according to Claim 39,
15 wherein the shape and dimensions are essentially unchanged by immersion in, and removal of, one or more wetting fluids.

41. The PTFE article according to Claim 39 wherein the heat of fusion associated with the DSC melting
20 endotherm is at least 80% of the total heat of fusion of the article.

42. The PTFE article according to Claim 39 wherein the mean pore size is less than 0.5 μm and the porosity is at least 50%.

25 43. The PTFE article according to Claim 39 wherein the porosity is at least 60%.

44. The PTFE article according to Claim 39 wherein the heat of fusion associated with the 320 to 333°C DSC melting endotherm is at least 40 J/g.

30 45. A porous, shrink-resistant polytetrafluoroethylene (PTFE) shaped article having a mean pore size of less than about 0.1 μm and a porosity of at least 40%.

46. The PTFE article according to Claim 39 in the
35 form of a film, sheet, fiber, tube or rod.

47. The PTFE article according to Claim 45 in the form of a film, sheet, fiber, tube or rod.

48. A load-bearing PTFE article according to Claim 45.

5 49. A load-bearing PTFE article according to Claim 51.

50. Process according to Claim 8 wherein the porous product from step (c) is subjected to low extension by low-rate uniaxial or biaxial stretching.

10 51. Process according to Claim 50 wherein step (c) and stretching are performed simultaneously.

52. Process according to Claim 50 wherein steps (a) and (b) are carried out at elevated pressure.

15 53. Process according to Claim 50 wherein the PTFE is in the form of film or sheet, and said process is operated continuously.

54. The porous, shrink-resistant PTFE shaped article of Claim 39 prepared by the process of Claim 50.

20 55. The porous, shrink-resistant PTFE shaped article according to Claim 39 in the form of a film.

56. The porous, shrink-resistant PTFE shaped article according to Claim 39 in the form of a filament.

57. The porous, shrink-resistant PTFE shaped article according to Claim 39 in the form of a rod.

25 58. The porous, shrink-resistant PTFE shaped article according to Claim 39 in the form of a tube.

59. A laminated structure comprising (i) the shaped article according to Claim 39 and (ii) a second, different shaped article bonded to (i).

30 60. The laminated structure according to Claim 59 wherein a bonding agent bonds article (i) to second article (ii), and said bonding agent is present in the pore network of portions of article (i) that are adjacent to said second shaped article (ii).

61. A filtration medium comprising the article according to Claim 39.

62. A gas/liquid separatory medium comprising the article according to Claim 39.

5 63. The separatory medium according to Claim 62 wherein the gas is air or water vapor and the liquid is water.

64. An article of protective clothing comprising the separatory medium according to Claim 63.

10 65. The article according to Claim 64 wherein the protective clothing is selected from the group consisting of space-suits, cleanroom suits, waterproof rainwear, gloves, footwear, socks, undergarments and medical garments.

15 66. An article of outdoor equipment comprising the separatory medium according to Claim 63.

67. The article according to Claim 66 wherein the outdoor equipment is a tent or sleeping bag.

20 68. Electrical or thermal insulation comprising the article according to Claim 39.

69. A medical material comprising the article according to Claim 39.

25 70. The material according to Claim 69 in the form of a vascular graft, ligament or tendon prosthesis, suture needle holder, damming material or dental floss.

71. A seam or sealing tape comprising the film according to Claim 55.

72. A gasket comprising the article according to Claim 39.

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FIG. 1

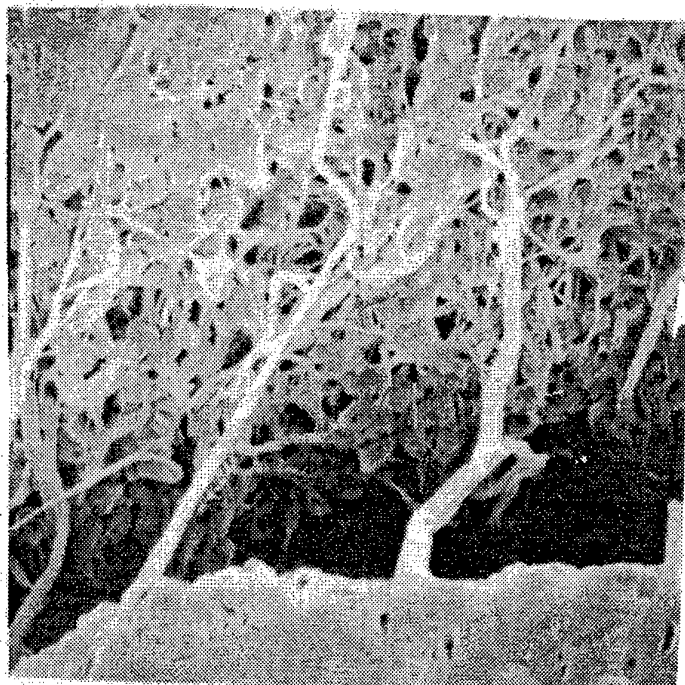


FIG. 2

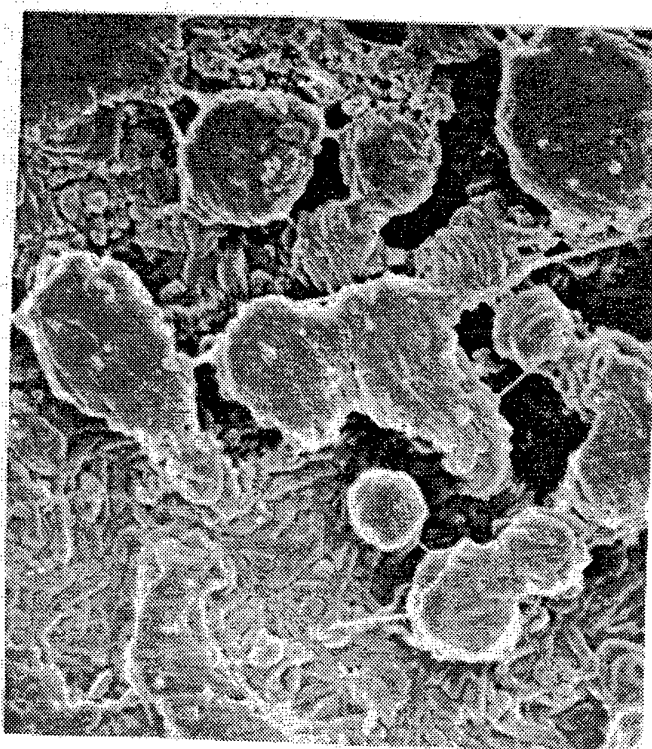
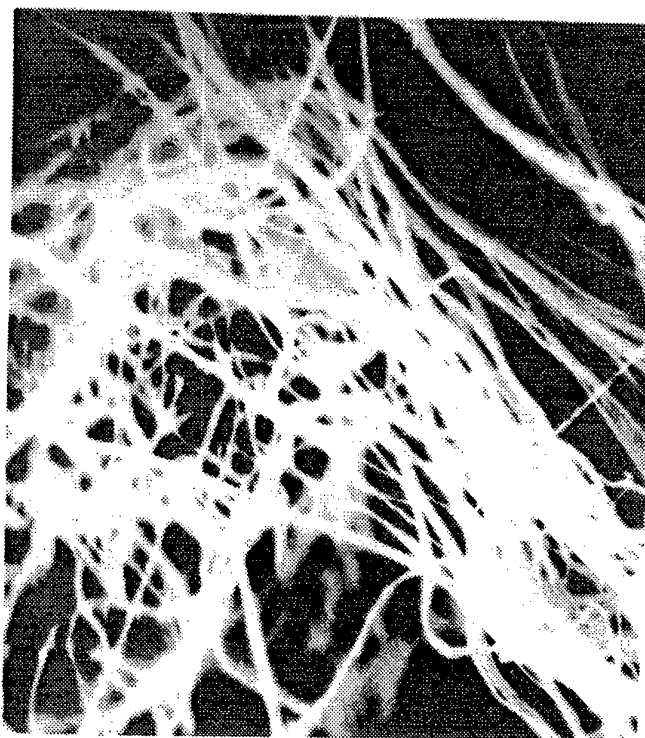


FIG.3



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FIG. 4

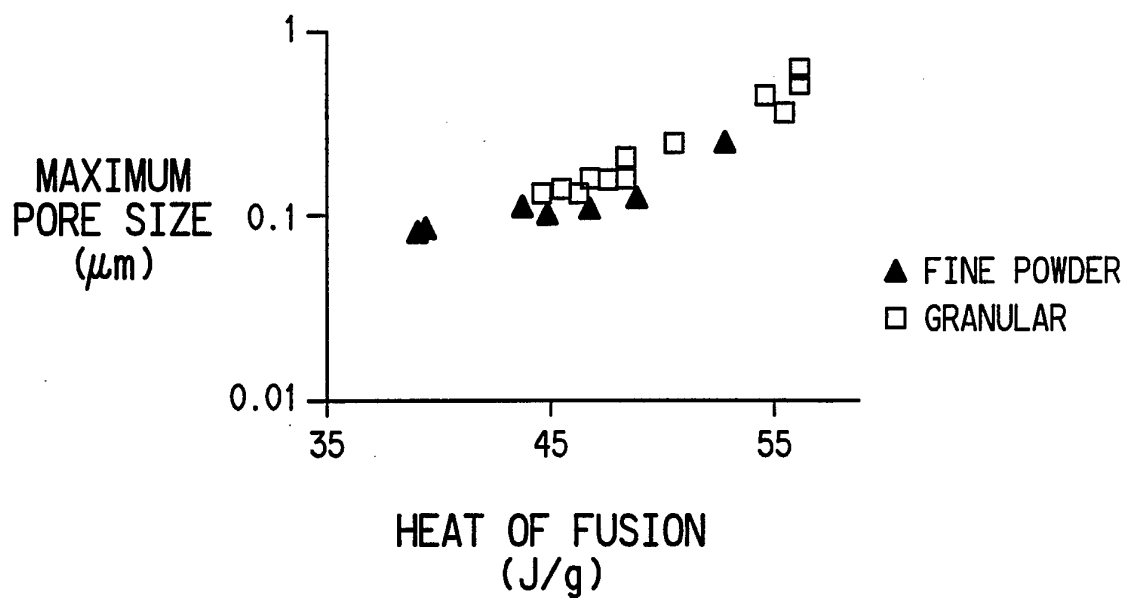


FIG. 5

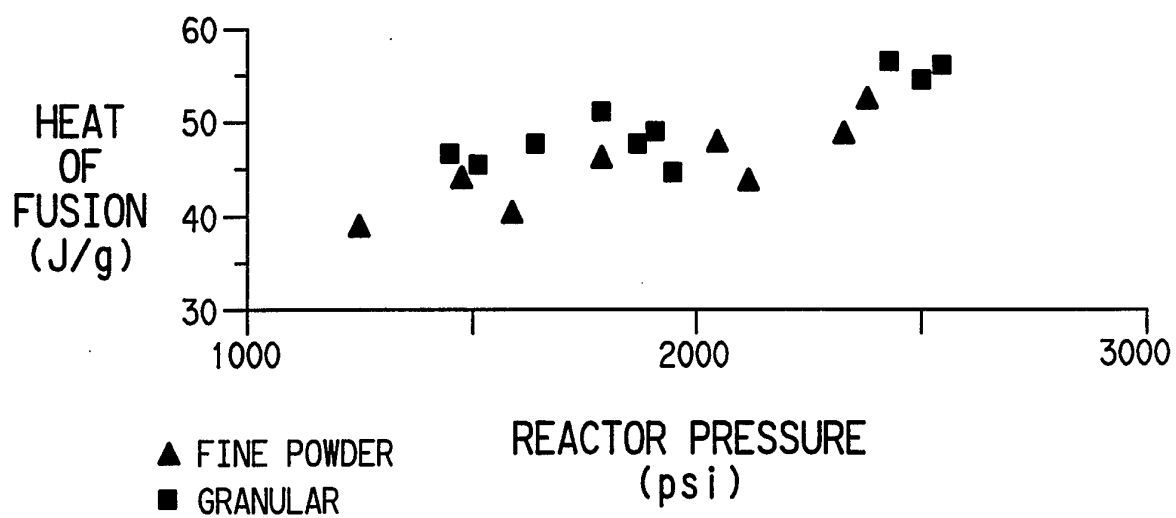
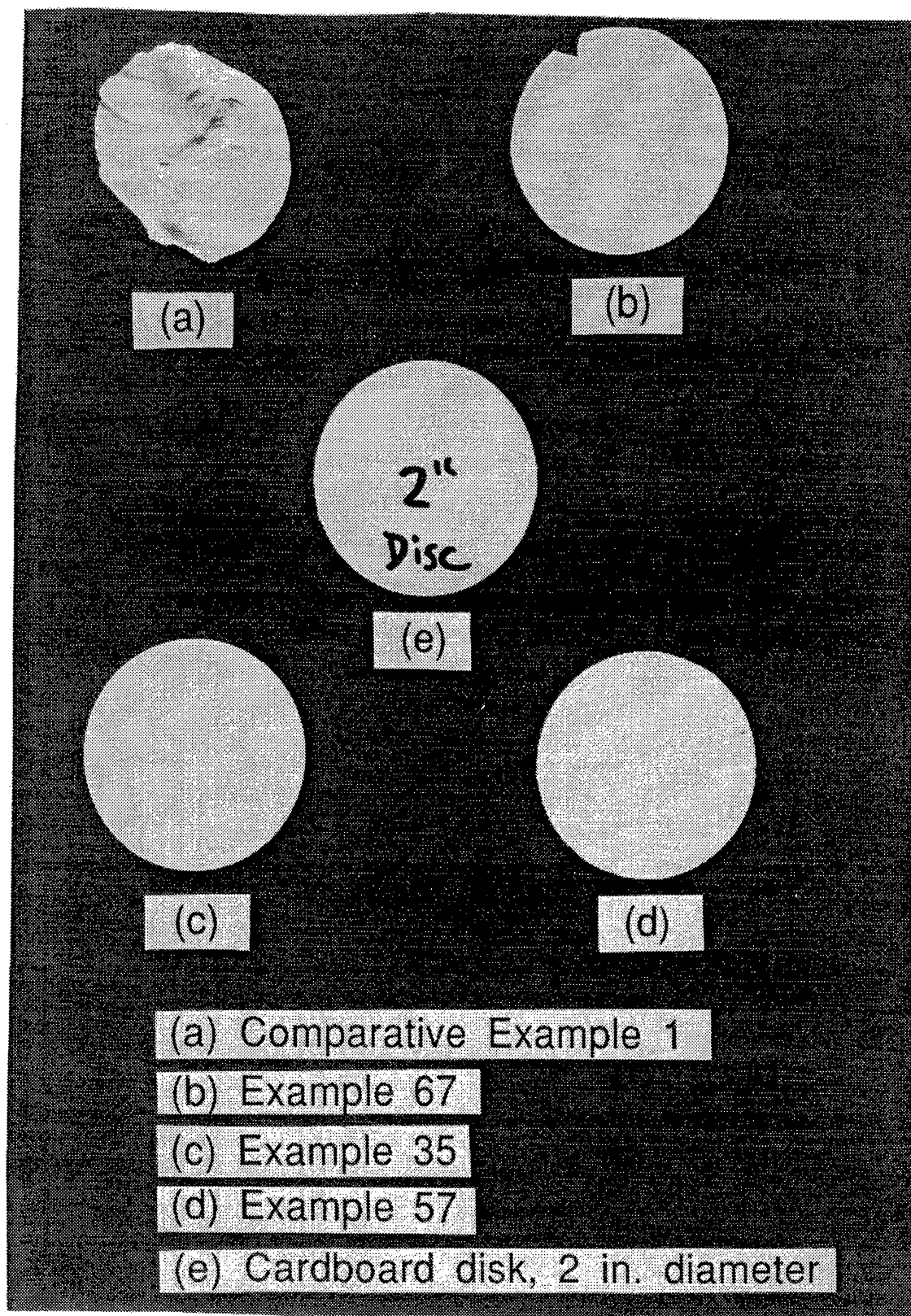


FIG. 6



INTERNATIONAL SEARCH REPORT

PCT/US 93/05884

International Application No

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all) ⁶		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int.Cl. 5 C08J9/18; C08J9/40; C08J9/28; //C08L27/18 D06M14/00A61F02/00		
II. FIELDS SEARCHED		
Minimum Documentation Searched ⁷		
Classification System	Classification Symbols	
Int.Cl. 5	C08J	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched ⁸		
III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹		
Category ^o	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
A	US4 385 026 (ICI) 24 May 1983 cited in the application see claims ---	-
A	DATABASE WPI Week 8605, 4 September 1985 Derwent Publications Ltd., London, GB; AN 030952 & JP,A,60 171 140 (OMIKRON SCI. LTD.) 4 September 1985 see abstract -----	-
^o Special categories of cited documents : ¹⁰ "A" document defining the general state of the art which is not considered to be of particular relevance "E" earlier document but published on or after the international filing date "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "P" document published prior to the international filing date but later than the priority date claimed "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention "X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step "Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art. "&" document member of the same patent family		
IV. CERTIFICATION		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
23 SEPTEMBER 1993	19.10.93	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	OUDOT R.	

INTERNATIONAL SEARCH REPORT

I national application No.

PCT/US 93/ 05884

Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☒ Claims Nos.:
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
Claims searched incompletely: 20-21.
Reason: No iron halide is liquid at 25°C.
see annex.
3. ☐ Claims Nos.:
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☐ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest.
- ☐ No protest accompanied the payment of additional search fees.

FURTHER INFORMATION CONTINUED FROM PCT/ISA/

Claims 20 and 21 are depending on claims 18 and 19 and on claims 6 and 7.
- In claims 20 and 21 are described, among others, iron halides as swelling fluids.

In claims 6 and 7, is precised that the swelling fluids must be liquid at 25°C

The handbook of chemistry and physics teaches us that no one iron halide is liquid below 27°C (see annex).

Claims 20 and 21 are therefore incompletely searched.

**ANNEX TO THE INTERNATIONAL SEARCH REPORT
ON INTERNATIONAL PATENT APPLICATION NO.**

US 9305884
SA 76172

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report.
The members are as contained in the European Patent Office EDP file on
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

23/09/93

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
US-4-385026		None	