

- [54] **EXPANDED OLEFIN POLYMER**
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- [58] **Field of Search 521/79, 143, 88, 94, 521/95, 97, 149, 144, 145; 524/224, 317**

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Primary Examiner—Morton Foelak

[57] ABSTRACT

A thermoplastic synthetic resin such as polyethylene or ethylene-vinyl acetate copolymer resin containing 0.1 to 10 wt. % of a specific additive selected from specific classes of compounds, namely saturated higher fatty acid amides, saturated higher aliphatic amines and complete esters of saturated higher fatty acids is found to be very suitable for production of expanded articles and can be easily formed into expanded articles with little shrinkage after expansion, free from creases on the surface or cracks on the cell walls, and having excellent characteristics such as good closed cellular characteristic, high compressive strength, low density, etc.

6 Claims, 5 Drawing Figures

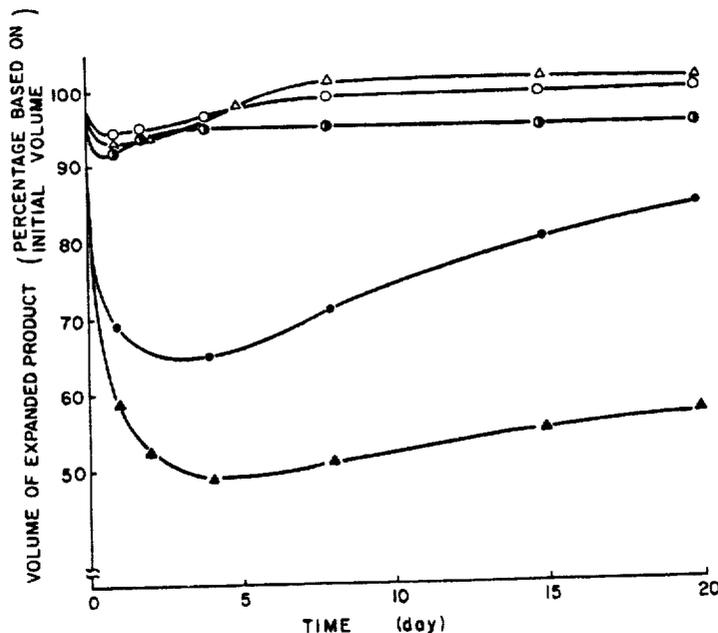


FIG. 1

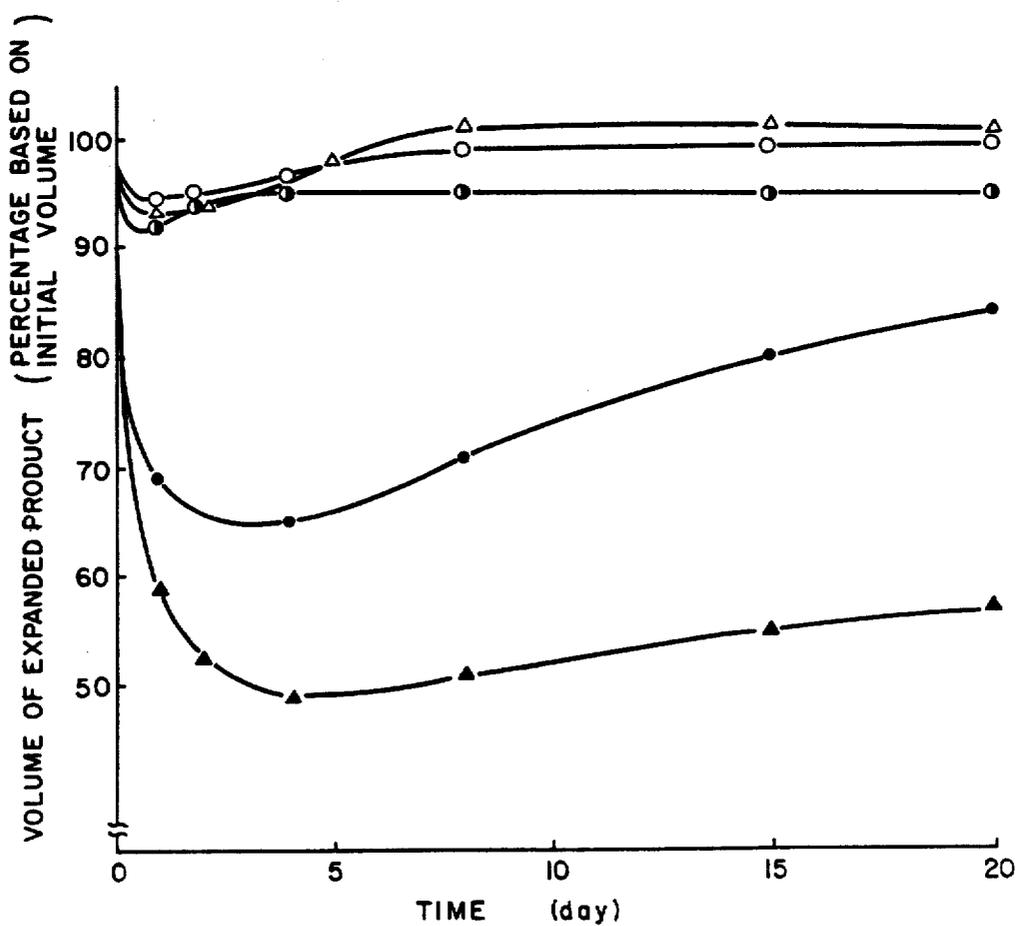


FIG. 2

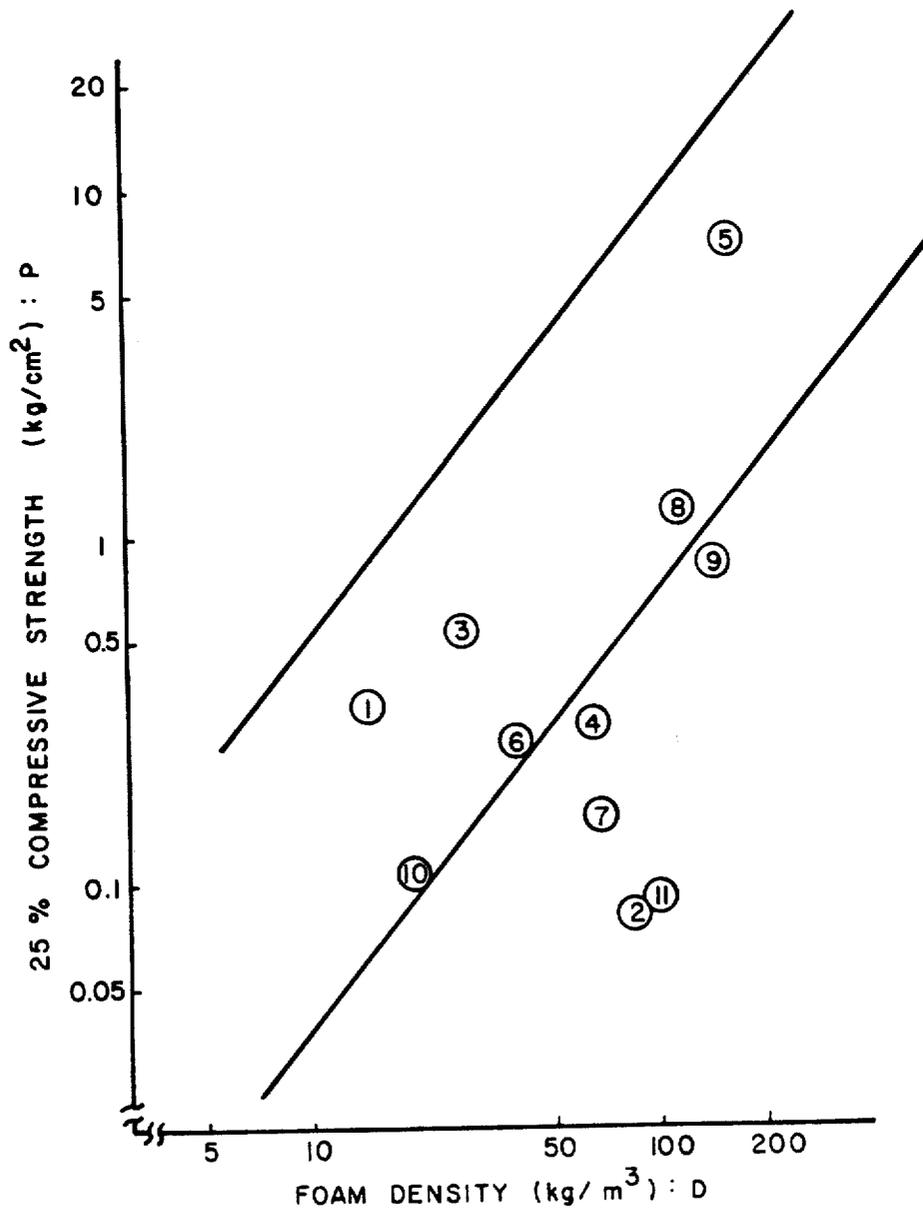


FIG. 3

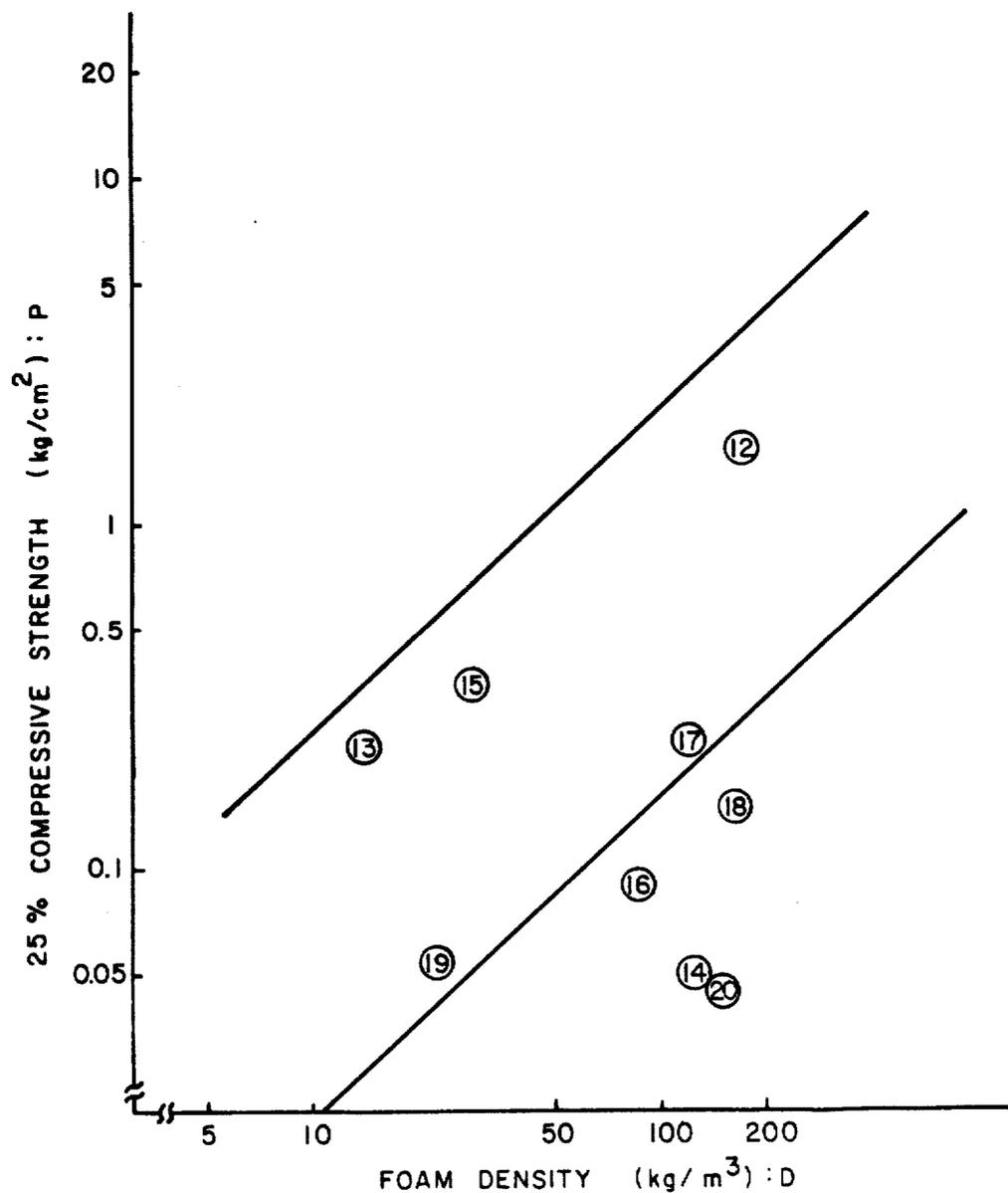


FIG. 4

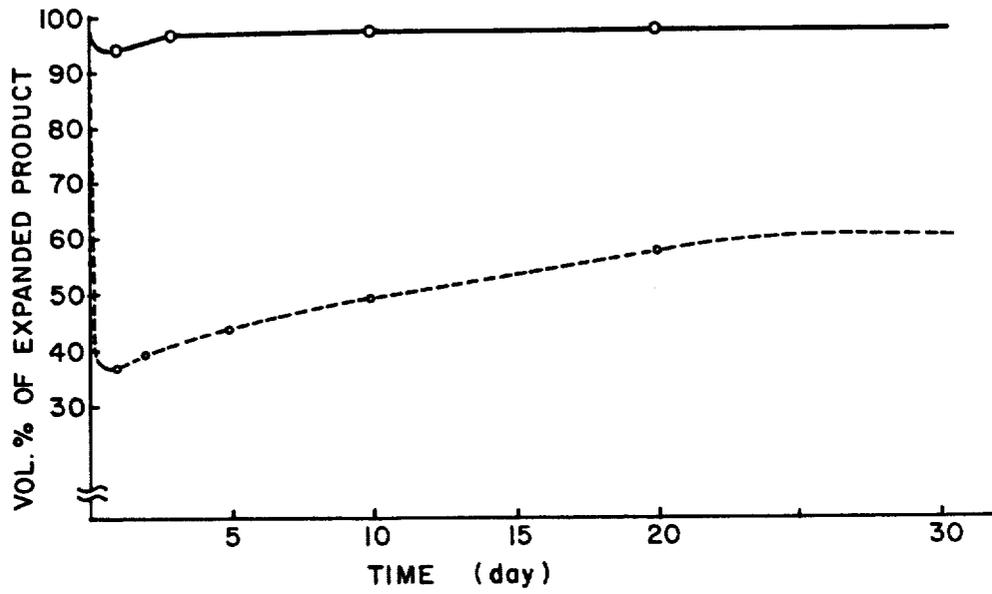
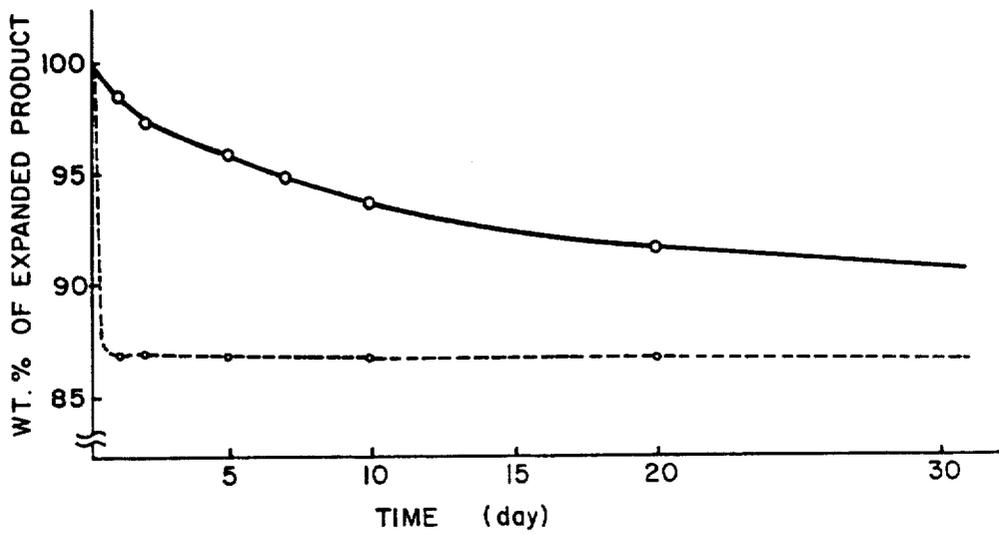


FIG. 5



EXPANDED OLEFIN POLYMER

Matter enclosed in heavy brackets [] appears in the original patent but forms no part of this reissue specification; matter printed in italics indicates the additions made by reissue.

This invention relates to a novel thermoplastic synthetic resin composition suitable for manufacturing expanded products of various kinds, which contains at least one compound selected from specific classes of compounds. This invention relates also to a process for expanding such a novel thermoplastic synthetic resin composition and to expanded products of a polyolefin resin obtained by such a process having excellent characteristics.

A thermoplastic synthetic resin of which expansion molding is difficult, for example, a polyolefin resin is known to be inferior in retentivity of gases such as of blowing agents as compared with such a resin as polystyrene resin.

Typical well-known methods of prior art for improvement of expandability of polyolefin resins may be classified broadly into four methods as follows:

(1) A method as disclosed by Japanese published examined patent applications No. 8840/1965 and No. 6278/1966, wherein the starting resin is subjected to crosslinking;

(2) A method as disclosed by U.S. Pat. No. 3,810,964, wherein the starting resin is mixed with a resin other than polyolefin resins;

(3) A method as disclosed by Japanese published examined patent applications No. 4341/1960 and No. 19628/1972, wherein there is employed a blowing agent with a composition and components specifically selected; and

(4) A method as disclosed by Japanese published examined patent applications No. 43997/1971 and No. 43998/1971, wherein there is added in the starting resin a partial ester of a specific polyhydric alcohol.

These methods, however, involve a number of drawbacks and none of them are satisfactory in commercial application. For example, according to the method (1), rheological flow properties of the resin can be improved, whereby it is possible to control resin temperature conditions optimum for melt-flow viscosity suitable for expansion. However, the temperature control range can be improved only to a small extent and besides there is no improvement of retentivity of gases such as blowing agents at all. Thus, this method fails to give substantial improvement in the art. That is, even if expansion may proceed as intended, the resultant expanded product will suffer from immediate shrinkage to be converted directly to expanded products with high density. Alternatively, even if the once shrunk expanded product may have a chance to be expanded again by the air impregnated thereto, the creases, concavo-convex deformations on the surface or cracks on cell walls formed at the time of shrinkage cannot thereby be remedied. In consequence, no excellent expanded product can be obtained. For the same reason as mentioned above in connection with the method (1), the method (2) cannot be free from the same drawback. In addition it further involves the drawback that the desirable characteristics inherent in a polyolefin resin may be impaired. The method (3), especially that as disclosed by Japanese published examined patent application No.

4341/1960, is now accepted as the most excellent method and has been practically used for commercial production of thick expanded articles. But this method cannot also be free from the problem of shrinkage or concavo-convex deformations on the surface of the expanded products. Furthermore, the specific blowing agents to be employed in this method are too expensive to be economical. Lastly, the partial esters used in the method (4) have insufficient effect of preventing shrinkage or cannot sufficiently be kneaded with the resin, whereby expansion moldability is lowered.

An object of the present invention is to provide a resin composition which can readily be formed into an expanded product with good quality from a synthetic resin which itself is difficultly formed into an expanded product with good quality due to excessive shrinkage phenomenon, particularly a polyolefin resin composition suitable for preparation of expanded products having a bulk density of 10 to 200 kg/m³ and smooth surface, and being excellent in closed cellular structure as well as in compressive strength.

Another object of the present invention is to provide a novel expanded product of a polyolefin resin having specific characteristics of an expanded product which cannot be obtained by any of prior art methods.

Still another object of the present invention is to provide a process for expansion of a thermoplastic resin which is capable of supplying economically expanded articles with low density, high closed cell percentage having excellent surface smoothness and compressive strength by preventing shrinkage in volume of the expanded products with lapse of time.

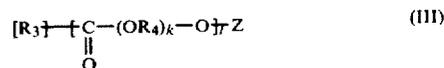
According to the present invention, there is provided a thermoplastic resin composition for manufacturing expanded products, comprising a thermoplastic synthetic resin and at least one compound selected from the group consisting of the compounds represented by the formulas (I), (II) and (III) as set forth below contained in said resin in an amount of 0.1 to 10% by weight based on the weight of said resin:



wherein R₁ is an alkyl group having 10 to 24 carbon atoms, X and X' each hydrogen atom, an alkyl group having 1 to 24 carbon atoms which may be substituted or a substituent containing a group of the formula —(R₄O)_m— wherein R₄ is an alkylene group having 1 to 5 carbon atoms and m an integer of 1 to 10;



wherein R₂ is an alkyl group having 9 to 23 carbon atoms, Y and Y' each hydrogen atom, an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a substituent containing a group of the formula —(R₄O)_m— wherein R₄ is an alkylene group having 1 to 5 carbon atoms and m an integer of 1 to 10;



propylene diamine mono(and di-)palmitate, polyoxyethylene hexadecyl propylene diamine mono(and di-)stearate, polyoxyethylene octadecyl propylene diamine mono(and di-)palmitate, polyoxyethylene octadecyl propylene diamine mono(and di-)stearate, and the like.

The second class of the compounds are saturated fatty acid amides and derivatives thereof as represented by the formula (II) as specified above. The alkyl group R_2 in the formula (II) is required to have 9 to 23 carbon atoms, preferably 11 to 21 atoms, and may be either straight chain, branched or cyclic. For the same practical reason as mentioned above in connection with R_1 , R_2 may preferably a straight chain alkyl having 11 to 21 carbon atoms. Similarly, each of Y and Y' may either be hydrogen atom or a substituent. As substituents, there may be mentioned an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a group of the formula $-(R_4O)_m A_2$ (wherein m is an integer of 1 to 10 and A_2 hydrogen atom, an alkyl having 1 to 24 carbon atoms or an acyl having 10 to 24 carbon atoms).

Typical examples of the compounds (II) are lauric acid amide, myristic acid amide, palmitic acid amide, stearic acid amide, arachic acid amide (eicosyl amide), behenic acid amide (docosyl amide), N-methyl stearic acid amide, N,N'-dimethyl stearic acid amide, di-lauric acid amide, di-palmitic acid amide, di-stearic acid amide, tri-lauric acid amide, tri-palmitic acid amide, tri-stearic acid amide, and so on. The saturated higher fatty acid amide derivatives may include lauric acid mono-(and-di-)ethanolamide, myristic acid mono-(and di-)ethanolamide, palmitic acid mono-(and di-)ethanolamide, stearic acid mono-(and di-)ethanolamide, arachic acid mono-(and di-)ethanolamide, behenic acid mono-(and di-)ethanolamide, lignoceric acid mono-(and di-)ethanolamide, lauric acid mono-isopropanolamide, palmitic acid mono-isopropanolamide, stearic acid mono-isopropanolamide, polyoxyethylene lauric acid amide, polyoxyethylene myristic acid amide, polyoxyethylene palmitic acid amide, polyoxyethylene stearic acid amide, polyoxyethylene arachic acid amide, di-lauric acid mono-ethanolamide, di-myristic acid mono-ethanolamide, di-palmitic acid mono-ethanolamide, di-stearic acid mono-ethanolamide, di-arachic acid mono-ethanolamide, polyoxyethylene di-stearic acid amide, polyoxyethylene lauric acid amide, mono-stearate, polyoxyethylene stearic acid amide, mono-stearate, etc.

The third group of the compounds are complete esters of saturated higher fatty acids as represented by the formula (III) as specified above. They are complete esters of polyhydric alcohols of the formula $Z(OH)_k$ and saturated fatty acids having 10 to 24 carbon atoms. In the above formula, the symbol $[R_3]$ means plural alkyl groups comprehensively, each being attached to each ester linkage which is bonded to polyhydric alcohol residue represented by Z, and each having 9 to 23 carbon atoms. Also in this compound, straight chain alkyl having 11 to 21 carbon atoms is preferred. The complete esters may be modified by addition reaction to include polyoxyalkylene group of the formula $-(OR_4)_k-$ in the molecule. The oxyalkylene group $-OR_4-$ may preferably oxyethylene or oxypropylene.

Typical examples of the compounds (III) are polyoxyethylene di-myristate, polyoxypropylene di-myristate, polyoxyethylene di-palmitate, polyoxypropylene di-palmitate, polyoxyethylene di-stearate, polyoxypropylene di-stearate, polyoxyethylene di-arachate, poly-

oxyethylene di-behenate, ethyleneglycol di-myristate, ethyleneglycol di-palmitate, ethyleneglycol di-stearate, ethyleneglycol di-arachate, ethyleneglycol di-behenate, lauric acid tri-glyceride, myristic acid tri-glyceride, palmitic acid tri-glyceride, stearic acid tri-glyceride, arachic acid tri-glyceride, 1,3-palmito-2-stearic acid glyceride, 1,3-stearo-2-myristic acid glyceride, sorbitane tetra-palmitate, sorbitane tetra-stearate, 12-hydroxy stearic acid tri-glyceride, sorbitane tetra-12-hydroxystearate, mono-stearic acid-di-12-hydroxystearic acid tri-glyceride, polyoxyethylene glycerine tristearate, polyoxyethylene glycerine tri-12-hydroxystearate, polyoxyethylene sorbitane tetra-stearate, polyoxyethylene sorbitane tetra-12-hydroxystearate, mono-stearic acid-di-12-hydroxy stearic acid polyoxyethylene tri-glyceride, and the like.

It is critically required in the present invention that at least one compound selected from the group of the compounds (I), (II) and (III) as described above should be contained in the thermoplastic synthetic resin in a total amount of 0.1 to 10% by weight based on the weight of said resin.

Referring now to Experiments I to IV set forth below, the specific behavior of the compounds within the scope of the present invention when they are contained in an amount within the range as specified above is to be described.

EXPERIMENT I

Using an ethylene-vinyl acetate copolymer (EVA-TATE D-2021, trade mark, produced by Sumitomo Chemical Co., Ltd.; vinyl acetate content: 10 wt. %, density: 0.93, Melt Flow Index: 1.5) as base resin, various samples are prepared by adding the compounds as shown in Table 1 and each sample is fabricated into a non-stretched sheet with thickness of about 0.15 mm.

TABLE 1

Sample No.	Trade name	Principal component	Additives	
			Parts per 100 parts of resin (by weight)	Manufacturer
1	Amine A . B	Octadecyl amine	2	Nippon Oils & Fats Co., Ltd.
2	Fatty acid amide T	Stearic acid amide/ palmitic acid amide	2	Kao Soap Co., Ltd.
3	Hardened oil	Stearic acid tri-glyceride	5	Kao Soap Co., Ltd.
4	Span 85 (reference)	Sorbitane tri-oleate	2	Kao Soap Co., Ltd.
5	— (Control)	—	—	—

The gas permeability characteristics of these sheets are measured according to the following method:

Device: Gas-permeability measuring instrument (LYSSY-L100-3001 model, produced by LYSSY Co.)

Gases to be permeated: Air; Dichlorotetrafluoroethane (blowing agent)

Method: Gas permeability coefficient is determined by measuring the time (seconds) needed until the inner pressure of a vessel initially maintained at 0.2 Torr at about 30° C. is increased to 0.4 Torr by the gas permeated through the sample sheet. The time is measured repeatedly until its value becomes approximately constant, and the average value of

three measured values is divided by the thickness of the sheet to give the gas permeability coefficient. The results of measurement are given in the following Table 2

TABLE 2

Permeated gas	Sample No				
	1	2	3	4	5
	Additive				
	Amine AB	Fatty acid amide T	Hardened oil	Span 85 (reference)	Control
1,2-dichloro-fluoro ethane	244	255	320	121	79
Air	340	350	380	490	320
				units sec/mm	

As apparently seen from Table 2, the compositions according to the present invention (Sample Nos. 1, 2 and 3) suppress noticeably permeability of blowing agent gas as compared with Control (Sample No. 5), while they suppress little permeability of the air. On the contrary, the composition of the reference (Sample No. 4) slightly suppresses permeability of the blowing agent gas, while it greatly suppresses permeability of the air.

Based on the presumption that the well-balanced permeabilities of the air and the blowing agent gas through the resin compositions of the present invention as shown in Table 2 might be reflected in expansion procedure to result in ideal expanded products, the present inventors have made experiments to apply these

90° C. to effect expansion to obtain expanded products. The density of the expanded products obtained is controlled to be 36 to 37 kg/m³.

The volume of the resultant expanded product is thereafter continued to be measured day by day. On the other hand, for the expanded product after 10 days, there are conducted measurements of compressive strength, compression permanent set, compression creep, surface smoothness, maximum shrinkage of the expanded product after expansion, dimensional stability of the expanded product and closed cellular characteristic value (each measurement method is hereinafter described).

FIG. 1 shows the relationship of the volume change with lapse of time and Table 3 the results of the measurement of various characteristics for each expanded product.

The compressive strength coefficient is also determined from the formula (2) as hereinafter described and shown in Table 3 in bracket together with 25% compressive strength (according to JIS-K-6767), since the latter varies depending on the density of the expanded product, etc.

As is clear from the above results, the composition of the present invention can be expanded using a blowing agent to give feasibly expanded products with good quality of uncrosslinked polyethylene which has hitherto been deemed to be difficult in the prior art as well as expanded products with good quality of ethylene-vinyl acetate copolymer resin which cannot practically be prepared in the prior art.

TABLE 3

Items Sample No.	Characteristics of expanded products (measured after 10 days after expansion)								
	Evaluation Items								
	Density [kg/m ³]		Compressive strength kg/cm ² (coefficient)	Permanent set at 50% compression (%)	Compressive creep (%)	Surface smoothness (number/cm)	Maximum foam shrinkage after expansion (Vol. %)	Dimensional stability of foam (%)	Closed cellular characteristic value (g/cm ³)
	Immediately after expansion	After 10 days							
1	36	34	1.48 (2.82 × 10 ⁻²)	10	6	0	8.0	3	0.0008
2	36	34	1.46 (2.80 × 10 ⁻²)	11	6	0	5.5	5	0.0012
3	36	34	1.47 (2.81 × 10 ⁻²)	11	6	0	7.5	7	0.0024
4	37	64	0.10 (9.3 × 10 ⁻⁴)	28	24	14	51	8	0.0135
5	37	51	0.11 (1.35 × 10 ⁻³)	24	21	12	35	19	0.0114

compositions for manufacturing expanded products of polyethylene and ethylene-vinyl acetate copolymer resin in spite of the fact that expansion molding of polyethylene resin under uncrosslinked state has been deemed to be difficult and also that expansion molding with high closed cell percentage of ethylene-vinyl acetate copolymer resin has been substantially impossible.

The following Experiments II-IV illustrates the results of these experiments.

EXPERIMENT II

Each of the resin compositions according to Sample Nos. 1 to 5 as described in Experiment I is mixed with 0.1 part by weight of calcium stearate and 0.6 part by weight of calcium stearate and fed to an extruder (30 mmΦ). The mixture is kneaded internally of the extruder together with 28 parts by weight of 1,2-dichlorotetrafluoroethane and the thus mixed resin is extruded into the air while being maintained at about

55

60

65

The concept of compressive strength coefficient is herein introduced to specify the novel expanded articles obtained by use of the composition according to the present invention. This is because apparent compressive strength as shown in Table 3 varies depending on bulk density of the expanded product and therefore it is not desirable to characterize the expanded product in terms of such an apparent compressive strength. As the result of numerous experiments, the present inventors were successful in generalization of the compressive strength relative to bulk, density according to the following formula:

$$P = A \times D^{1.248 \cdot Y} \tag{1}$$

From the formula (1) is obtained:

$$A = P/D^{1.248 \cdot Y} \tag{2}$$

wherein A represents compressive strength coefficient, P 25% compressive strength measured according to JIS-K-6767, D bulk density of expanded product, the value 1.248 is the index experimentally determined from numerous data, Y is parameter $(1-\alpha/100)$, α being percentage (wt.) of the component to be copolymerized in the resin (for example, vinyl acetate in ethylene-vinyl acetate copolymer). This specific compressive strength coefficient is hereinafter referred to as "A value".

EXPERIMENT III

Using a low density polyethylene (Asahi-Dow Polyethylene F-1920, trade mark, produced by Asahi-Dow Limited; density: 0.919, Melt Flow Index 2.0) as base resin, the compositions 1 to 11 containing the additives and blowing agents as shown in Table 4, respectively, per 100 parts by weight of said resin are prepared by kneading similarly in an extruder and subjected to extrusion expansion as in Experiment II. As nucleators, there are employed 0.06 parts by weight of calcium stearate and 0.36 parts by weight of calcium silicate in each composition. After 10 days after formation of expanded product, 25% compressive strength is measured according to JIS-K-6767 for each expanded product from each composition to give the results as shown in FIG. 2, the numbers in FIG. 2 corresponding to those of the compositions.

EXPERIMENT IV

Using an ethylene-vinyl acetate copolymer (EVA-TATE K-2010, trade mark, produced by Sumitomo Chemical Co., Ltd.; vinyl acetate content 25 wt. %, density: 0.95, Melt Flow Index: 3.0) as base resin, 0.1 part of calcium stearate and 0.6 part by weight of calcium silicate as nucleators and the additives and blowing agents as shown in Table 5, under otherwise the same conditions as in Experiment III, the compositions 12 to 20 are formed into expanded products. The results of measurement conducted similarly as in Experiment III are shown in FIG. 3, wherein the numbers correspond to those of the compositions.

TABLE 4

Com-position No.	Blowing agent (wt parts)	Additive (wt parts)
1	Dichlorodifluoromethane (57)	Fatty acid amide T (4.0)
2	Dichlorodifluoromethane (57)	None
3	Dichlorodifluoromethane (22)	Fatty acid amide T (2.0)
4	Dichlorodifluoromethane (22)	None
5	Dichlorodifluoromethane (5)	Amine AB (1.0)
6	Butane(8)	Hardened oil (3.0)
7	Butane(8)	None
8	Butane(6)	Fatty acid amide T (0.5)
9	Butane(6)	None
10	1-chloro-1,1-difluoroethane (60)	Hardened oil (2.0)
11	1-chloro-1,1-difluoroethane (60)	None

TABLE 5

Com-position No.	Blowing agent (wt parts)	Additive (wt parts)
12	1,2-dichloro-tetrafluoroethane (10)	Amine AB (1.0)
13	Dichlorodifluoromethane (57)	Fatty acid amide T (5.0)
14	Dichlorodifluoromethane (57)	None

TABLE 5-continued

Com-position No.	Blowing agent (wt parts)	Additive (wt parts)
15	Dichlorodifluoromethane (22)	Fatty acid amide T (4.0)
16	Dichlorodifluoromethane (22)	None
17	Butane (7)	Hardened oil (2.0)
18	Butane (7)	None
19	1-chloro-1,1-difluoroethane (60)	Hardened oil (3.0)
20	1-chloro-1,1-difluoroethane (60)	None

As apparently seen from FIG. 2 and FIG. 3, the A values of the expanded products obtained by use of the compositions of the present invention are invariably within 2.15×10^{-3} to 2.89×10^{-2} even when the blowing agent employed may be varied. In contrast, the A values of the expanded products using no composition of the present invention are by far smaller than the range as specified above. While being not bound by any theory, this is probably due to the following reason. Blowing agent gases contained in the expanded products are rapidly dissipated therefrom at the stage immediately after expansion in case when no composition of the present invention is employed, while the air penetrates into the expanded product considerably slowly. Consequently, at the stage before complete solidification of the resin while it is hot, the expanded product is brought internally to a state under reduced pressure, whereby it is compressed by atmospheric pressure to be shrunked. Thus, cooling is completed while giving deformations or cracks on cell walls. When the penetration of the air is slower than the cooling speed as mentioned above, the expanded product is cooled as it is to result in an expanded product with high density and having a large number of permanent creases remained on the expanded product. Even when the air may be penetrated more rapidly, simultaneously with reduction in pressure in the expanded product, to effect surface expansion of the expanded product, the deformations or cracks already formed on cell walls will prevent such surface expansion to make restoration to original volume difficult. This speculation is considered to be quite probable because the A values of the expanded products are greatly deteriorated.

Whereas, in the expanded product prepared from the composition of the present invention, the resin can be solidified with very small extent of shrinkage by permitting blowing agent gases to be replaced by the air while maintaining the ratio of both gases permeated suitably. As the result, the expanded product can be free from deformations or cracks on the cell walls to exhibit not only the excellent compressive strength coefficient but also excellent surface smoothness.

If the specific compound of the present invention is used in less than 0.1 wt. % based on the resin, no significant effect can be obtained. On the contrary, an amount in excess of 10 wt. % does not necessarily lead to improvement of the effect but in some cases may cause an adverse effect on the rheological flow properties of the composition itself. Accordingly, the amount of the specific compound added is generally selected from about 0.5 to 7 wt. % from economical standpoint. There is no significant change in the amount of the compound added when it is in the composition or when it is in the expanded product, and it is calculated as a total amount

of the specific compounds employed based on the weight of the resin.

For the purpose of the invention, there may be employed either a single compound or a combination of two or more compounds selected from those as mentioned above. The compound may be incorporated in the resin by any method but it is desirable to contain the compound in the resin so that said compound may be dispersed as homogeneously as possible in the resin when the composition is formed into an expanded product.

In accordance with the present invention, there is also provided a process for expanding a thermoplastic synthetic resin, which comprises incorporating at least one compound selected from the group consisting of the compounds of the formulas (I), (II) and (III) as described above in the thermoplastic synthetic resin in an amount of 0.1 to 10% by weight based on said resin together with a suitable amount of a blowing agent under the condition maintained at a temperature in the range from about 15° to 300° C. to form an expandable resin composition and then allowing said resin composition to expand utilizing the expanding force of the blowing agent contained therein.

In the process as specified above, the compounds may be incorporated in the resin by so called impregnation method wherein a substance to be incorporated is contacted with resin particles and said substance is impregnated into the resin by controlling the pressure and the temperature. Alternatively, there may also be employed so called kneading method wherein the resin and the substance to be incorporated are subjected to mixing and kneading. Furthermore, a combination of both methods may also be applicable. The substances to be incorporated may either be simultaneous or stepwise. These operations may be conducted under well known conditions, namely at a temperature in the range from 15° to 300° C. and a pressure of 0.05 to 300 kg/cm² (gauge).

The expanding force of blowing agent used in this process is obtained through phase transfer (from liquid phase to gas phase), volume expansion of blowing agent and decomposition of blowing agent (from solid to gas), and therefore the conditions are determined depending on the blowing agent employed and expanding operations. For example, when a physical blowing agent is used in extrusion expansion, a resin kneaded for temperature adjustment at a temperature of about 60° to 280° C. under a pressure of 5 to 200 kg/cm² can be extruded into the atmosphere at a temperature of about 20° C. and under pressure of 1 atm. to obtain sufficient expanding force. Alternatively, when a physical blowing agent is used in cavity expansion, a resin containing a blowing agent is filled in a cavity and the cavity is heated under conditions at a temperature of about 115° C. under pressure of 0.23 kg/cm² (gauge).

The specific feature of the process according to the present invention resides in allowing a thermoplastic synthetic resin composition containing 0.1 to 10 wt. % of at least one compound as specified by the formulas (I), (II) and (III) to expand with a blowing agent which is also contained in said resin. This is because, in the absence of the specific compound, the expanded product suffers from shrinkage in the course of preparation and with lapse of time, as explained with reference to FIGS. 1 to 3 and Table 3, thereby giving only expanded products with high density, having much concavo-convex deformations or creases or being very low in closed

cell percentage. In particular, no expanded product with excellent compressive strength can be obtained in the absence of the specific compound.

Similarly as described in connection with the composition of the present invention, an amount of the specific compound less than 0.1 wt. % fails to give the effect of the invention, while an amount exceeding 10 wt. % may cause adverse effect rather than better results. The specific compounds may also be used either singly or in a mixture of two or more compounds. The preferable total amount of the specific compounds falls also within 0.5 to 7 wt. %. They can be contained in the resin in any conventional manner, but it is desirable to disperse the compounds as homogeneously as possible throughout the entire resin.

As blowing agents to be used in the present invention, volatile organic blowing agents and thermally decomposable gas-releasing chemical blowing agents are available. Preferably, there may be employed volatile organic blowing agents having boiling point (at 1 atm.) not higher than melting point of the base resin, such as trichlorofluoromethane, dichlorodifluoromethane, dichlorofluoromethane, chlorodifluoromethane, 1,1',2-trichlorotrifluoroethane, 1,2-dichlorotetrafluoroethane, 1-chlorotrifluoroethane, 1-chloro-1,1'-difluoroethane, 1,1'-difluoroethane, octafluorodichlorobutane, propane, butane, butene, propylene, pentane, etc. When the base resin to be expanded is a non-crosslinked polyolefin resin, it is preferred to select a volatile blowing agent from those as enumerated above having a Kauri-Butanol value in the range of 10 to 25 as determined by the method according to ASTM-D-1133-61.

These blowing agents may be employed generally in an amount in the range from 5 to 70% by weight based on the resin depending on the desired density of expanded products.

The process of the present invention is expected to be most advantageously be applied in the field of so called continuous extrusion expansion. In this case, for example, the base resin, the specific compound and blowing agent are fed into an extruder heated at a temperature higher than melting point of the base resin (generally about 120° to 280° C.), kneaded under a pressure generally of about 50 to 300 kg/cm² therein, then said mixture is adjusted to a temperature suitable for expansion in the range from the melting point of the base resin to the temperature lower by 50° C. than the melting point (generally about 60° to 200° C.) before being extruded through an orifice to the outside at about 25° C. under atmospheric pressure, thereby accomplishing expansion simultaneously with extrusion, followed by cooling to produce expanded articles. This technique is economical in continuous expansion of a large amount of resins. In particular, by use of the specific compound of the present invention, it is rendered possible to select a blowing agent from a large number of less expensive compounds which have hitherto been insufficient in expandability when used alone as blowing agents. To speak one typical example, in place of an expensive blowing agent 1,2-dichlorotetrafluoroethane, there can be employed less expensive blowing agents such as dichlorodifluoromethane, propane or butane to a great economical advantage.

The thermoplastic synthetic resin to be used in the present invention refer to all polymers, copolymers and mixed polymers which can be subjected to melt fabrication. In particular, thermoplastic synthetic resins which can be improved in expandability by addition of the

specific compound of the present invention are those which will undergo shrinkage when expanded due to the greater ratio S'/S exceeding 1 of permeating speed (S') of volatile hydrocarbon or fluorocarbon gas through said resin film to that (S) of the air (at the time of expansion as estimated by FIG. 4 and FIG. 5). More specifically, they may include crosslinked or non-crosslinked polyolefin resins such as ethylene homopolymers (e.g. high density polyethylene, medium density polyethylene or low density polyethylene or a mixture thereof), ethylenic copolymers having ethylene content of 50% or more (e.g. ethylene-vinyl acetate copolymer, ethylene-acrylic acid ester copolymer, ethylene-methacrylic acid ester copolymer, a metallic salt of an ethylene-acrylic acid copolymer, ethylene-propylene copolymer, ethylene-vinyl chloride copolymer), polypropylene and polybutene-1. Among them, polyethylene resin and ethylene-vinyl acetate copolymer are preferably used. The polyolefin resin to be employed in the present invention may have a melt index which is not specifically limited but generally within the range from 0.3 to 45. When it is desired to employ a crosslinked polyolefin resin, it may be prepared by conventional method by effecting crosslinking using a crosslinking agent such as organic peroxides or irradiation of electron beam.

The resin composition of the present invention may further contain, if desired, other inorganic or organic additives such as pigments, fire-retardants, lubricants, anti-oxidants, UV-absorbers, nucleators, anti-static agents or others in an amount of preferably no more than 3% by weight based on the weight of the resin. In particular, it is preferable to use a small amount (not more than 1% by weight) of nucleators such as talc or a fatty acid metal salt in order to control uniformly the cell distribution in the resultant expanded product.

The present invention is further illustrated with reference to the following Examples and Comparison Examples. The measurement of characteristic values and evaluation of these values herein mentioned are conducted by the methods and the criteria, respectively, as set forth below.

1. Compressive strength and compressive strength coefficient

(a) 25% compressive strength (P):

Compressive strength at the time of 25% compression is measured according to JIS-K6767.

(b) compressive strength coefficient (A):

This value is calculated by the formula (2) as mentioned above from the above compressive strength (P) and bulk density (D) of expanded product.

2. 50% compression permanent set:

According to JIS-K-6767 (at the time of 50% compression).

3. Compression creep:

According to JIS-K-6767 (under area load of 0.1 Kg/cm².24 hour)

4. Surface smoothness:

The surface of expanded product is measured over 10 cm length by coarseness measuring instrument to detect creases or concavo-convexes with width of 0.5 mm or more and the number detected is calculated per 1 cm length.

5. Feeding characteristic through extruder:

Change in amount extruded per one minute when performing extrusion by 30 mmΦ extruder is expressed by variance percentage (n=15).

$$\text{Variance percentage} = \frac{\text{Maximum amount} - \text{minimum amount}}{\text{Average amount}} \times 100$$

6. Maximum shrinkage:

Volume of expanded product is measured (by water-sink method) every day for 20 days after expansion and maximum shrinkage is calculated by the following formula:

$$\text{Maximum shrinkage} = 1 - \frac{\text{Volume of expanded product on the day when it is minimum}}{\text{Volume of expanded product immediately after expansion}} \times 100$$

7. Dimensional stability:

From the result of measurement 6. as mentioned above, dimensional stability is calculated by the following formula:

$$\text{Dimensional stability} = \frac{|V_0 - V_{20}|}{V_0} \times 100$$

(wherein V₀ is volume of expanded product immediately after expansion and V₂₀ that after 20 days.)

8. Closed cellular characteristic value:

In water in a vessel having water volume sufficient to sink sample in water and a function to be sealed is sunk an expanded product sample of 15 mm×15 mm×100 mm (volume: V; weight: W₀) to be held therein, followed by sealing of the vessel. Subsequently, the inner pressure in the vessel is reduced to 460 mm Hg and left to stand for 10 minutes. Then, the inner pressure in the vessel is restored to atmospheric and the sample is taken out. The sample is calmly dipped in pure methanol for about 2 seconds, followed by wipe-off of the moisture adhered on the surface, dried in a drier at 60° C. for 5 minutes and thereafter its weight (W₁) is measured. Closed cellular characteristic value is calculated by the following formula:

$$\text{Closed cellular characteristic value (g/cm}^3\text{)} = \frac{W_1 - W_0}{V}$$

9. Criteria for evaluation:

Each evaluation item is rated according to the ranks as shown in the following Table:

Evaluation item	Ranks			
	a (excellent)	b (good)	c (passable)	d (bad)
1. Compressive strength coefficient	8.0 × 10 ⁻³ or more	4.0 × 10 ⁻³ or more, less than 8.0 × 10 ⁻³	2.15 × 10 ⁻³ or more, less than 4.0 × 10 ⁻³	less than 2.15 × 10 ⁻³
2. 50% compression permanent wt (%)	less than 5 to 0	5 or more less than 15	15 or more less than 30	30 or more
3. Compressive creep (%)	less than 5 to 0	5 or more, less than 10	10 or more, less than 20	20 or more
4. Surface smoothness (number/cm)	less than 3 to 0	3 or more, less than 6	6 or more, less than 10	10 or more
5. Feeding characteristic of	less than 5 to 0	5 or more, less than 10	10 or more, less than 15	15 or more

-continued

Evaluation item	Ranks			
	a (excellent)	b (good)	c (passable)	d (bad)
6. Maximum shrinkage (%)	less than 10 to 0	10 or more, less than 15	15 or more, less than 20	20 or more
7. Dimensional stability (%)	less than 5 to 0	5 or more, less than 10	10 or more, less than 15	15 or more
8. Closed cellular characteristic (g/cm ³)	less than 0.010 to 0	0.010 or more, less than 0.025	0.025 or more, less than 0.50	0.50 or more

Overall evaluation is rated from the ranks as set forth above according to the following ranks:

a (excellent)	when there are at least two excellent marks with no bad or passable mark
b (good)	when there is at least one good mark with no bad mark and not more than two passable marks
c (passable)	when there are three or more passable marks with no bad mark
d (bad)	when there is one or more bad mark

The details of the thermoplastic synthetic resins and the specific compounds employed in the following Examples and Comparison Examples are listed below.

Thermoplastic resins:

Resin A: low density polyethylene produced by Asahi-Dow Limited, F-1920, trade mark, density: 0.919 g/cc, MI: 2.0 g/10 min.

Resin B: ethylene-vinyl acetate copolymer produced by Sumitomo Chemical Co., Ltd., EVATATE D-2021, trade mark, vinyl acetate content: 10 wt. %, density: 0.93 g/cc, MI: 1.5 g/10 min.

Resin C: ethylene-vinyl acetate copolymer produced by Sumitomo Chemical Co., Ltd., EVATATE K-2010, trade mark, vinyl acetate content: 25 wt. %, density: 0.95 g/cc, MI: 3.0 g/10 min.

Additives (Nos. 1-18: specific compounds of the invention; Nos. 19-31: reference compounds)

No.	Trade name of additives	Manufacturer	Name of the compounds
1	Fatty acid amide T	Kao Soap Co., Ltd.	Stearic acid amide and palmitic acid amide (mixture)
2	Amine BB	Nippon Oils & Fats Co., Ltd.	Dodecyl amine
3	Amine AB	Nippon Oils & Fats Co. Ltd.	Octadecyl amine
4	N-methyl-octadecyl amine	Nippon Oils & Fats Co., Ltd.	N-methyloctadecyl amine
5	Asfazol #20	Nippon Oils & Fats Co., Ltd.	Stearyl propylene diamine
6	Naimine S-202	Kao Soap Co., Ltd.	Polyoxyethylene octadecyl amine (2 moles of oxyethylene added)
7	Naimine S-210	Kao Soap Co., Ltd.	Polyoxyethylene octadecyl amine (10 moles of oxyethylene added)
8	Denon 331 P	Marubishi Petrochemical Co.	Polyoxyethylene stearyl amine mono- and di-stearate (mixture)
9	Esodaamine T-13	Lion Fat & Oil Co., Ltd.	Polyoxyethylene stearyl and palmityl diamine (mixture: 3 moles of oxyethylene added)

-continued

No.	Trade name of additives	Manufacturer	Name of the compounds
5 10	Resicoat 1936	Lion Fat & Oil Co., Ltd.	Oxyethylene stearyl and palmocetyl diamine (mixture: one mole of oxyethylene added)
11	Fatty acid amide C	Kao Soap Co., Ltd.	Lauric acid amide
10 12	Amazol SDE	Kawaken Fine Chemical Co., Ltd.	1:1-type stearic acid dictbanolamide
13	Amazol SME	Kawaken Fine Chemical Co., Ltd.	1:1-type stearic acid mono-ethanolamide
14	Amozol LME	Kawaken Fine Chemical Co., Ltd.	1:1-lauric acid mono-ethanolamide
15	Fatty acid amide P	Kao Soap Co., Ltd.	Palmitic acid amide
16	Hardened oil	Kao Soap Co., Ltd.	Stearic acid triglyceride
20 17	Koa wax 85 powder	Kao Soap Co., Ltd.	12-hydroxy stearic acid triglyceride
18	Unister-E-275	Nippon Oils & Fats Co., Ltd.	Ethylene glycol distearate
19	Syntolex L-100	Nippon Oils & Fats Co., Ltd.	Sodium lauryl sulfate
25 20	A.mos-150	Kao Soap Co., Ltd.	Stearic acid mono- and di-glyceride
21	Cation S ₂ -100	Nippon Oils & Fats Co., Ltd.	Octadecyl dimethyl-benzyl ammonium chloride
22	Noion SN-204.5	Nippon Oils & Fats Co., Ltd.	Polyoxyethylene nonyl phenol ether
23	Caproic acid amide	Kanto Chemical Co., Ltd.	Caproic acid amide
24	Span 85	Kao Soap Co., Ltd.	Sorbitane trioleate
25	Triphenyl carbinol	Kanto Chemical Co., Ltd.	Triphenyl carbinol
30 26	1,2-diphenyl ethylene-diamine	Kanto Chemical Co., Ltd.	1,2-diphenyl ethylene-diamine
27	Phthalamide	Kanto Chemical Co., Ltd.	Phthalamide
28	Lunac S-30	Kao Soap Co., Ltd.	Stearic acid
29	Zinc stearate	Sakai Chemical Co., Ltd.	Zinc stearate
30	Fatty acid amide O	Kao Soap Co., Ltd.	Oleic acid amide
45 31	Alfro P-10	Nippon Oils & Fats Co., Ltd.	Erucic amide

EXAMPLES 1-18 AND COMPARISON EXAMPLES 1-14

To 100 parts by weight of Resin B are added various additives as shown in Table 6, 0.1 part by weight of calcium stearate, 0.6 part by weight of calcium silicate and 22 parts by weight of a volatile blowing agent dichlorodifluormethane. Each mixture is kneaded by means of a 30 mm single screw extruder equipped with a round orifice of 5 mm in diameter and heated at 190° C. By adjusting the resin temperature in the orifice at 90° C., extrusion expansion is carried out for each mixture to prepare an expanded product thereof. These expanded products are subjected to evaluation test as described above to give the results as shown in Table 6. Table 6 clearly shows that the expanded products of Examples 1 to 18 containing the compounds of the formulas (I) to (III) exhibit superior values to those of Comparison example 1 containing no additive and Comparison examples 2 to 14 containing other compounds than those of the formulas (I) to (III).

The volumes and weights of the expanded products obtained in Example 10 and Comparison example 1 are continued to be measured every day for about one month, respectively, and the percentages of volumes and the weights based on those immediately after expansion are plotted versus lapse of time (days) in FIG. 4 and FIG. 5.

As apparently seen from FIG. 4 and FIG. 5, the ex-

panded product of Example 10 is reduced in weight with lapse of time, while its volume is not reduced with small shrinkage and good restorability. In contrast, the expanded product of Comparison example 1 suffers from abrupt and noticeable shrinkage with reduction in weight and its volume restored with lapse of time is at most about 60%.

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TABLE 6-continued

Comparison example	Additive trade name (wt. parts)	Density (10 days after expansion) g/cm ³	Compressive strength coefficient	50% compression permanent set	Compression creep	Surface smoothness	Feeding characteristic through extruder	Maximum shrinkage	Dimensional stability	Closed cellular characteristic value	Overall evaluation
1	None	0.075	d	d	d	d	a	d	d	b	d
2	Atmos 150 (1.5)	"	c	c	c	d	d	c	d	b	d
3	Syntolex L-100 (2.0)	"	d	d	d	d	b	d	d	b	d
4	Cation S ₂ -100 (2.0)	0.073	d	d	d	d	b	d	d	b	d
5	Nonion NS 204.5 (2.0)	0.072	d	d	d	d	d	d	d	b	d
6	Capronamide (2.0)	"	d	d	d	d	a	d	d	b	d
7	Fatty acid amide O (2.0)	0.074	d	d	d	d	b	d	d	b	d
8	Alfro P-10 (2.0)	0.074	d	d	d	d	b	d	d	b	d
9	Span 85 (2.0)	"	d	d	d	d	d	d	d	b	d
10	Triphenyl carbinoyl (2.0)	"	d	d	d	d	b	d	d	b	d
11	1,2-Diphenyl ethylenediamine (2.0)	0.073	d	d	d	d	b	d	d	b	d
12	Phthalamide (2.0)	0.075	d	d	d	d	b	d	d	b	d
13	Lunac 5-30 (2.0)	"	d	d	d	d	b	d	d	b	d
14	Zinc stearate 2.0	"	d	d	d	d	b	d	d	b	d

EXAMPLES 19-27 AND COMPARISON
EXAMPLES 15-17

amples 19 to 27 give better results than Comparison
Examples 15 to 17 when various blowing agents D, E
and F are employed.

TABLE 7

			Base resin: A 100 wt. parts		Nucleators: Calcium stearate 0.06 wt. parts, calcium silicate 0.36 wt. parts		Blowing agents: D: Dichlorodifluoromethane 22 wt. parts		E: 1-chloro-1,1-difluoroethane 20 wt. parts		F: Butane 8 wt. parts	
Example	Additive (wt. parts)		Blowing agent	Density (10 days after expansion g/cm ³)	Evaluation							
	Type of compounds	Trade name			Compressive strength coefficient	50% compression permanent set	Compression creep	Surface smoothness				
19	Saturated higher	Amine AB (1.0)	D	0.030	a	a	a	a	a			
20	aliphatic amines	Amine AB (3.0)	E	0.032	a	b	b	b	b			
21	Saturated higher fatty acid amides	Amine AB (7.0)	F	0.034	a	b	b	b	b			
22	Saturated higher fatty acid amides	Fatty acid amide T (0.3)	D	0.030	a	a	a	a	a			
23	fatty acid amides	Fatty acid amide T (2.0)	E	0.032	a	b	a	a	a			
24	Complete esters of saturated higher fatty acids	Fatty acid amide T (5.0)	F	0.033	a	b	b	b	b			
25	Complete esters of saturated higher fatty acids	Hardened oil (4.0)	D	0.030	a	a	a	a	a			
26	Complete esters of saturated higher fatty acids	Hardened oil (6.0)	E	0.033	a	b	b	b	b			
27	Complete esters of saturated higher fatty acids	Hardened oil (10.0)	F	0.034	a	b	b	b	b			
Comparison example	Additives											
15	None		D	0.063	d	d	d	d	d			
16	None		E	0.062	d	d	d	d	d			
17	None		F	0.069	d	d	d	d	d			
					Evaluation							
Example	Additives (wt. parts)		Feeding characteristic through extruder	Maximum shrinkage	Dimensional stability	Closed cellular characteristic value	Overall evaluation					
	Type of compounds	Trade name										
19	Saturated higher	Amine AB (1.0)	a	a	a	a	a					
20	aliphatic amines	Amine AB (3.0)	a	b	a	a	a					
21	Saturated higher fatty acid amides	Amine AB (2.0)	b	b	a	a	a					
22	Saturated higher fatty acid amides	Fatty acid amide T (0.3)	a	a	a	a	a					
23	fatty acid amides	Fatty acid amide T (2.0)	a	b	a	a	a					
24	Complete esters of saturated higher fatty acids	Fatty acid amide T (5.0)	b	b	a	a	a					
25	Complete esters of saturated higher fatty acids	Hardened oil (4.0)	b	a	a	a	a					
26	Complete esters of saturated higher fatty acids	Hardened oil (6.0)	b	b	a	a	a					
27	Complete esters of saturated higher fatty acids	Hardened oil (10.0)	b	b	a	a	a					
Comparison example	Additives											
15	None		a	d	d	b	d					
16	None		a	d	d	b	d					
17	None		a	d	d	b	d					

Expanded products are prepared similarly as described in Examples 1-18 except that 100 parts by weight of Resin A are used as base resin, 0.06 parts by weight of calcium stearate and 0.36 part by weight of calcium silicate powders as nucleators and the blowing agents D, E and F as shown in Table 7 in amounts of 22, 20 and 8 parts by weight, respectively, and that the resin temperature in the orifice is controlled at 104° C. From the results shown in Table 7, it is clearly seen that Ex-

EXAMPLES 28-36 AND COMPARISON
EXAMPLES 18-21

Using 100 parts by weight of Resin C as base resin, blowing agents D, E, G and H as shown in Table 8 in amounts of 22, 20, 28 and 26 parts by weight, respectively, and the additives as shown in Table 8 in amounts

EXAMPLES 37-39 AND COMPARISON
EXAMPLES 22-24

According to the same procedure as in Examples 1-18 except for the specific compounds and their amounts and the amounts of dichlorodifluoromethane as shown in Table 9, various expanded products are prepared. The results as shown in Table 9 indicate that the products of Examples 37-39 are better in expansion moldability and physical properties of the resultant expanded products than those of the Comparative examples even when the amounts of the blowing agent are greatly changed as shown in Table 9.

25 Kg/m³ and have a closed cellular characteristic value of less than 0.01.

COMPARISON EXAMPLE 25

Example 40 is repeated except that no stearic acid amide is added. The resultant primarily expanded particles are found to have a density of 111 Kg/m³, while the secondarily expanded articles a density of 31 Kg/m³. The expanded particles have higher density as compared with those of Example 40 and said particles are found to have relatively large number of creases. When the secondarily expanded particles are molded similarly as in Example 40, the expanded product obtained is

TABLE 9

		Evaluation									
		Density (10 days after expansion) g/cm ³	Compressive strength coefficient	50% compression permanent set	Compression creep	Surface smoothness	Feeding characteristic through extruder	Maximum shrinkage	Dimensional stability	Closed cellular characteristic value	Overall evaluation
Resin:		B 100 wt. parts									
Nucleators:		Calcium stearate 0.1 wt. parts, calcium silicate 0.6 wt. part									
Blowing agent:		Dichlorodifluoromethane									
Example	Additives trade name (wt. parts)	Amount of blowing agent (wt. parts)									
37	Fatty acid amide T (4)	60	0.014	a	b	b	a	b	a	a	a
38	Fatty acid amide T (2)	9	0.077	a	b	b	a	a	a	a	a
39	Fatty acid amide T (1)	5	0.174	a	a	a	a	a	a	a	a
Comparison example											
22		60	0.080	d	d	d	d	a	d	d	b
23		9	0.089	c	c	d	d	a	d	b	b
24		5	0.195	b	c	c	c	a	d	c	d

EXAMPLE 40

In polyethylene resin (F-2130, trade mark, produced by Asahi-Dow Limited, density: 0.921 g/cc, MI: 3.0 g/10 min.), there are added by kneading 0.45% by weight of dicumyl peroxide as crosslinking agent and 1.5% by weight of stearic acid amide (Fatty acid amide T, trade mark, produced by Kao Soap Co., Ltd.) and the mixture is subjected to crosslinking reaction. The resultant crosslinked polyethylene resin particles (spherical with diameter of 1.5 mm) with gel content of 61% are impregnated in an autoclave with dichlorodifluoromethane under pressurization with heating and thereafter cooled. The expandable crosslinked polyethylene resin particles thus obtained are found to contain 14 wt. % of dichlorodifluoromethane. These particles are placed in a pressure-type expanding vessel wherein they are allowed to expand while passing steam of 0.23 Kg/cm²-G for 45 seconds to obtain primarily expanded particles with density of 100 Kg/m³. Subsequently, these primarily expanded particles are placed in an autoclave and, under pressurization with the air at 10 Kg/cm²-G, heat treatment is conducted at 80° C. for 15 hours to increase inner pressure in the cells, followed by passing of steam of 0.32 Kg/cm² to effect expansion to obtain secondarily expanded particles with density of 27 Kg/m³. After increasing the inner pressure in the cells of these secondarily expanded particles, they are filled under compression in a cavity in a molding machine (ECHO-120 model, produced by Toyo Machinery & Metal Co., Ltd.) and subjected to expansion fusion molding by heating with steam of 1.1 Kg/cm²-G. The density of the molded expanded product is found to be

found to have a density of 30 Kg/m³. It is also inferior in closed cell percentage and compressive strength to that of Example 40. The life of beads impregnated with blowing agent for retaining desirable expandability is also shorter by one hour as compared with those of Example 40.

EXAMPLE 41

Using a mixed resin comprising 60 parts by weight of a high density polyethylene (Suntec S-360, trade mark, produced by Asahi Kasei Kogyo Kabushiki Kaisha, density: 0.950 g/cc) and 40 parts by weight of an ionomer (Surlyn A 1706, trade mark, produced by E. I. du Pont de Nemours, Inc.), 1.5 parts by weight of stearic acid amide as specific additive (Fatty acid amide T, trade mark, produced by Kao Soap Co., Ltd.), 0.3 part by weight of calcium silicate powders as nucleators and 27 parts by weight of dichlorodifluoromethane as volatile blowing agent are kneaded with said mixed resin in a 30 mm single screw extruder equipped with an orifice with diameter of 5 mm and heated at 220° C. While adjusting the resin temperature in the orifice at 122° C., extrusion expansion is conducted to obtain expanded product having excellent characteristics such as closed cellular characteristic of 0.005 g/cm³, density of 23 Kg/m³, compressive strength coefficient of 2.01 × 10⁻² and maximum expansion shrinkage of 0.2%.

EXAMPLE 42

Example 41 is repeated except that the base resin of high density polyethylene is replaced by isotactic polypropylene (Chisso Polypro 1011, trade mark, produced by Chisso Corporation) and the resin temperature in the

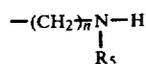
orifice is adjusted at 135° C. The expanded product obtained is found to have excellent characteristics such as closed cellular characteristic. Of 0.008 g/cm³, density of 21 Kg/m³, compressive strength coefficient of 2.10 × 10⁻² and maximum expansion shrinkage of 0.1%.

What we claim is:

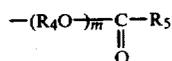
1. An expanded article of an olefin polymer comprising an expanded product of an olefin polymer containing at least one compound, which imports little shrinkage to said expanded article after expansion selected from the group consisting of the compounds represented by the formulas (I), (II) and (III) as set forth below in an amount of 0.1 to 10% by weight based on the weight of said resin and having a closed cellular characteristic value of 0 to 0.5 g/cm³, a bulk density of 10 to 200 kg/m³ and a compressive strength coefficient of 2.15 × 10⁻³ to 2.89 × 10⁻²:



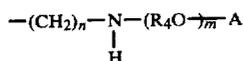
wherein R₁ is an alkyl group having 10 to 24 carbon atoms, X and X' each hydrogen atom, an alkyl group having 1 to 24 carbon atoms which may be substituted or a substituent selected from the group consisting of -(CH₂)_nNH₂ wherein n is an integer of 1 to 22,



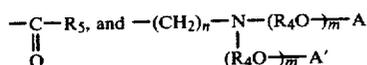
wherein R₅ is an alkyl having 1 to 24 carbon atoms, -(R₄O)_mH wherein R₄ is an alkylene group having 1 to 5 carbon atoms and m an integer of 1 to 10,



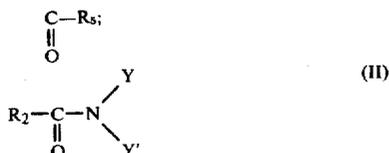
wherein R₅ is an alkyl having 1 to 24 carbon atoms,



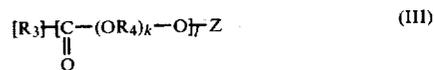
wherein n is an integer of 1 to 22 and A is hydrogen atom or



wherein A' is hydrogen atom or



wherein R₂ is an alkyl group having 9 to 23 carbon atoms, Y and Y' each hydrogen atom, an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a substituent of the formula -(R₄O)_mA₂ wherein A₂ is hydrogen atom, an alkyl having 1 to 24 carbon atoms or acyl having 10 to 24 carbon atoms;



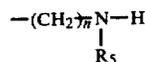
wherein [R₃] means plural alkyl or hydroxyalkyl groups corresponding in number to the integer l, which may be the same or different, each having 9 to 23 carbon atoms, R₄ an alkylene group having 1 to 5 carbon atoms, k an integer of 0 to 7, an integer of 2 to 8 and Z a 1-valent residue of 1-valent polyhydric alcohol from which 1 hydroxyl groups are eliminated.]

2. An expanded article according to claim [7], wherein the olefin polymer is a polyethylene resin oryan ethylenevinyl acetate copolymer resin.

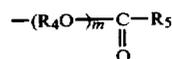
3. A process for expanding an olefin polymer, which comprises incorporating at least one compound, which imparts little shrinkage to said expanded polymer after expansion, selected from the group consisting of the compounds of the formulas (I), (II) and (III) as set forth below in a thermoplastic synthetic resin in an amount of 0.1 to 10% by weight based on the weight of said resin together with a blowing agent under the condition maintained at a temperature in the range from about 15° to 300° C. to form an expandable resin composition and then allowing said resin composition to expand utilizing the expanding force of the blowing agent contained therein:



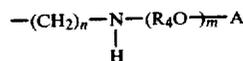
wherein R₁ is an alkyl group having 10 to 24 carbon atoms, X and X' each hydrogen atom, an alkyl group having 1 to 24 carbon atoms which may be substituted or a substituent selected from the group consisting of -(CH₂)_nNH₂ wherein n is an integer of 1 to 22,



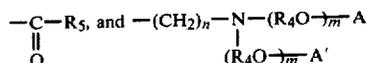
wherein R₅ is an alkyl having 1 to 24 carbon atoms, -(R₄O)_mH wherein R₄ is an alkylene group having 1 to 5 carbon atoms and m is an integer of 1 to 10,



wherein R₅ is an alkyl having 1 to 24 carbon atoms,

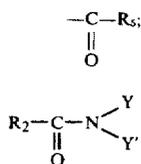


wherein n is an integer of 1 to 22 and A is hydrogen atom or



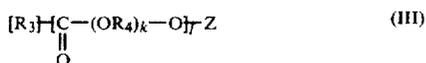
wherein A' is hydrogen atom or

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(II) 5

wherein R₂ is an alkyl group having 9 to 23 carbon atoms, Y and Y' each hydrogen atom, an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a substituent of the formula $-(R_4O)_m A_2$ wherein A₂ is hydrogen atom, an alkyl having 1 to 24 carbon atoms or acyl having 10 to 24 carbon atoms;



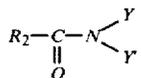
wherein [R₃] means plural alkyl or hydroxyalkyl groups corresponding in number to the integer l, which may be the same or different, each having 9 to 23 carbon atoms, R₄ an alkylene group having 1 to 5 carbon atoms, k an integer of 0 to 7, an integer of 2 to 8 and Z a l-valent residue of l-valent polyhydric alcohol from which l hydroxyl groups are eliminated.]

4. A process according to claim [3,] 8 wherein the olefin polymer is cross-linked.

5. A process according to claim [3,] 8 wherein the olefin polymer is a polyethylene resin, an ethylene-vinyl acetate copolymer resin, or a polypropylene resin.

6. A process according to any of claims [3] 5 to 8, wherein the polymer composition is expanded by extrusion foaming by means of an extruder.

7. An expanded article of an olefin polymer composition comprising an olefin polymer and at least one compound, which reduces shrinkage of said expanded article after expansion, selected from the group consisting of the amide or complete ester compounds represented by the formula (II) or (III), respectively, as set forth below in an amount of 0.1 to 10 percent by weight based on the weight of said olefin polymer and having a closed cellular characteristic value of 0 to 0.5 g/cm³, a bulk density of 10 to 200 kg/m³ and a compressive strength coefficient of 2.15×10^{-3} to 2.89×10^{-2} ;

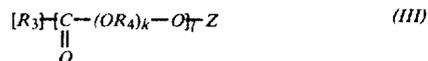


(II)

wherein R₂ is an alkyl group having 9 to 23 carbon atoms, Y and Y' each is a hydrogen atom, an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a substituent of the formula $-(R_4O)_m A_2$ wherein R₄ is an alkylene group having 1 to 5 carbon atoms, m is an integer

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of 1 to 10, and A₂ is hydrogen atom, an alkyl having 1 to 24 carbon atoms or acyl having 10 to 24 carbon atoms;



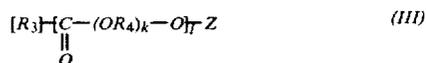
wherein [R₃] means plural alkyl or hydroxyalkyl groups corresponding in number to the integer l, which may be the same or different, each having 9 to 23 carbon atoms, R₄ is an alkylene group having 1 to 5 carbon atoms, k is an integer of 0 to 7, l is an integer of 2 to 8 and Z is an l-valent residue of an l-valent polyhydric alcohol of the formula Z(OH)_l from which l hydroxyl groups are eliminated; said expanded article having been prepared by the use of a volatile organic blowing agent.

8. A process for expanding an olefin polymer, which comprises incorporating at least one compound, which reduces shrinkage of the resulting expanded polymer after expansion, selected from the group consisting of the amide or complete ester compounds of the formula (II) or (III), respectively, as set forth below into the olefin polymer to be expanded in an amount of 0.1 to 10 percent by weight based on the weight of said olefin polymer together with a volatile organic blowing agent under the condition maintained at a temperature in the range of from about 15° to 300° C. to form an expandable resin composition and then allowing said expandable resin composition to expand utilizing the expanding force of the blowing agent contained therein:



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wherein R₂ is an alkyl group having 9 to 23 carbon atoms, Y and Y' each is a hydrogen atom, an alkyl having 1 to 24 carbon atoms, an acyl having 10 to 24 carbon atoms or a substituent of the formula $-(R_4O)_m A_2$ wherein R₄ is an alkylene group having 1 to 5 carbon atoms, m is an integer of 1 to 10, and A₂ is hydrogen atom, an alkyl having 1 to 24 carbon atoms or acyl having 10 to 24 carbon atoms;



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wherein [R₃] means plural alkyl or hydroxyalkyl groups corresponding in number to the integer l, which may be the same or different, each having 9 to 23 carbon atoms, R₄ is an alkylene group having 1 to 5 carbon atoms, k is an integer of 0 to 7, l is an integer of 2 to 8 and Z is an l-valent residue of an l-valent polyhydric alcohol of the formula Z(OH)_l from which l hydroxyl groups are eliminated.

* * * * *

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UNITED STATES PATENT OFFICE
CERTIFICATE OF CORRECTION

PATENT NO. : RE. 31,744 Page 1 of 4
DATED : November 20, 1984
INVENTOR(S) : Seizaburu Watanabe, Yutaka Matsuki

It is certified that error appears in the above-identified patent and that said Letters Patent are hereby corrected as shown below:

Column 3, line 2, the number "1" should be changed to the letter -- 1 -- .

Column 7, Table 2, "fluoro ethane" should be changed to -- tetrafluoro ethane -- .

Column 8, line 62, delete the comma after the word "bulk".

Column 10, line 40, the word "rapdily" should be changed to -- rapidly -- .

Column 14, line 3, the word "percentange" should be changed to -- percentage -- ; line 7, the word "masured" should be changed to -- measured -- .

Column 15, Item 8 under the heading for a(excellent), "0010" should be changed to -- 0.010 -- ; line 65, Item 9 under the heading for Trade name of additives, "Esodao-mine" should be changed to -- Esoduomine -- .

UNITED STATES PATENT OFFICE
CERTIFICATE OF CORRECTION

PATENT NO. : RE. 31,744 Page 2 of 4
DATED : November 20, 1984
INVENTOR(S) : Seizaburu Watanabe, Yutaka Matsuki

It is certified that error appears in the above-identified patent and that said Letters Patent are hereby corrected as shown below:

Column 16 under Trade name of additives, Item No. 14, "Amozol" should read -- Amazol --; Item No. 17, "Koa" should read -- Kao --; Item No. 20, "A mos" should read -- A.mos --.

Column 16 under Manufacturer, Item No. 17, "Koa" should read -- Kao --.

Column 16 under Name of the compounds, Item No. 10, "palmoctyl" should read -- palmityl --; Item No. 12, "dictbanolamide" should read "diethanolamide --; Item No. 14, "1:1-lauric" should read -- 1:1-type lauric --.

Column 21, Table 6-continued, under the heading for Additive trade name(wt.parts), Item No. 10, "carbinoyl" should read -- carbinol --; Item No. 13, "5-30" should read -- S-30 --.

Column 23, TABLE 7, second heading, "Density (10 days after expansion)" should read -- Density (10 days after expansion) --.

UNITED STATES PATENT OFFICE
CERTIFICATE OF CORRECTION

PATENT NO. : RE. 31,744 Page 3 of 4
DATED : November 20, 1984
INVENTOR(S) : Seizaburu Watanabe, Yutaka Matsuki

It is certified that error appears in the above-identified patent and that said Letters Patent are hereby corrected as shown below:

Column 23, TABLE 7, lower half, Item 21 under the heading Trade name, "Amine AB(2.0)" should read -- Amine AB(7.0) --.

Column 25, TABLE 8, fourth heading, "g/cm/hu3" should read -- g/cm³ --; Items 35 and 36 under the heading Surface smoothness, "b" should read -- a -- in both instances.

Column 27, TABLE 9, heading for Nucleators: "0.1 wt. parts" should read -- 0.1 wt. part --; Example 37 under the heading for Closed cellular characteristic value, insert -- b --.

Column 30, lines 14-16, Claim 2 should read as follows:
-- 2. An expanded article according to claim [7] 1, wherein the olefin polymer is a polyethylene resin, or [y] an ethylenevinyl acetate copolymer resin.

UNITED STATES PATENT AND TRADEMARK OFFICE
CERTIFICATE OF CORRECTION

PATENT NO. : RE 31,744

Page 4 of 4

DATED : November 20, 1984

INVENTOR(S) : Seizaburu Watanabe, Yutaka Matsuki

It is certified that error appears in the above-identified patent and that said Letters Patent is hereby corrected as shown below:

Column 32, line 24 of Claim 8, "olfein" should read
--olefin--.

Signed and Sealed this

Third Day of December 1985

[SEAL]

Attest:

DONALD J. QUIGG

Attesting Officer

Commissioner of Patents and Trademarks