

(19) World Intellectual Property Organization  
International Bureau



(43) International Publication Date  
20 June 2002 (20.06.2002)

PCT

(10) International Publication Number  
**WO 02/48063 A2**

- (51) International Patent Classification<sup>7</sup>: **C03C**
- (21) International Application Number: PCT/EP01/13173
- (22) International Filing Date:  
13 November 2001 (13.11.2001)
- (25) Filing Language: English
- (26) Publication Language: English
- (30) Priority Data:  
MI2000A002714  
15 December 2000 (15.12.2000) IT
- (71) Applicants (for all designated States except US): **ENI S.P.A.** [IT/IT]; Piazzale E. Mattei, 1, I-00144 Roma (IT). **ENITECNOLOGIE S.P.A.** [IT/IT]; Via F. Maritano, 26, I-20097 San Donato Milanese (IT).
- (72) Inventors; and
- (75) Inventors/Applicants (for US only): **MARCOTULLIO, Armando** [IT/IT]; Via Trento, 4, San Donato Milanese, I-20097 Milan (IT). **MONGA, Raffaella** [IT/IT]; Via Maestri Campionesi 25, I-20135 Milan (IT). **BELMONTE, Giuseppe** [IT/IT]; Via Conte di Roccavione 105, I-10147 Torino (IT). **CALDERONI, Angelo** [IT/IT]; Via Strasburgo 2/C, I-20097 San Donato Milanese-Milan (IT). **FERRARI, Giovanni** [IT/IT]; Via Tempio 28, I-29100 Piacenza (IT).
- (74) Agents: **DE GREGORI, Antonella** et al.; Ing. Barzanó & Zanardo Milano S.p.A., Via Borgonuovo 10, I-20121 Milan (IT).
- (81) Designated States (*national*): AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW.
- (84) Designated States (*regional*): ARIPO patent (GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).
- Published:**  
— without international search report and to be republished upon receipt of that report
- For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.*



**WO 02/48063 A2**

(54) Title: PROCESS FOR THE SEPARATION OF HOLLOW GLASS MICROSPHERES FROM MUDS CONTAINING THEM

(57) Abstract: Process for recovering at least 70% of hollow glass microspheres having an average diameter, according to the ASTM D1214-1989, ranging from 5 to 200 µm contained in a mixture of drilling mud and cuttings which comprises: a) screening, if necessary, the mixture through one or more 5 to 20 mesh sieves; b) feeding the screened mixture to one or more cyclones and/or hydrocyclones arranged in series, each of which is fed with a volume flow-rate from 1.5 to 10 times higher than the maximum nominal operating value.

5

PROCESS FOR THE SEPARATION OF HOLLOW GLASS MICROSPHERES  
FROM MUDS CONTAINING THEM

The present invention relates to a process for the  
10 separation of hollow glass microspheres from muds contain-  
ing them.

More specifically, the present invention relates to a  
process for the separation of hollow glass microspheres  
contained in muds and cuttings produced during the drilling  
15 of oil wells or wells for the production of natural gas.

As it is well known, during the drilling of wells for  
the production of oil or natural gas, particular fluids are  
used, commonly called drilling fluids or muds, whose pur-  
pose is of primary importance for the correct and safe han-  
20 dling of the well preparation phase. As described, for ex-  
ample, in patent U.S. 3,035,042, drilling fluids have nu-  
merous functions: they are used for cooling and lubricating  
the head of the drilling bit probe; they remove and carry  
to the surface the cuttings produced during drilling; they  
25 help to seal and consolidate the well walls; they keep the

cuttings in suspension when the drilling is momentarily stopped; they contribute to forming a hydrostatic pressure which serves to control and regulate the flow towards the surface of oil/gas under pressure when the bit reaches the  
5 reservoir.

The most traditionally used drilling fluids consist of aqueous or oily dispersions of clay and/or sandy materials such as bentonite, illite, kaolinite, etc. These are fluids with a thixotropic behaviour, so that when the drilling is  
10 stopped, they tend to gelify and prevent sedimentation of the cuttings around the bit. Dispersing agents or fluidifying agents can also be added to these fluids to maintain their viscosity at low values during drilling, to enable them to easily entrain the cuttings produced by the bit.  
15 Examples of dispersing and/or fluidifying agents are lignin sulfonates, lignites, synthetic polymers of (meth)acrylic acid and/or of (meth)acrylamide, etc. Details on the composition of drilling fluids or muds can be found in European patent 565,187.

20 For all drillings in which the normal density of the drilling fluid creates a hydrostatic pressure which exceeds the fracturing gradient (resistance of the rock to hydraulic pressure) of the formation or when the existence of natural fractures in the formation annuls the fracturing  
25 gradient, lightened mud is used to reduce the hydrostatic

seal in the well. In this way, absorptions and/or damage due to the invasion of fluids in the formation are limited. Exceeding the fracturing gradient is a problem which arises in particular in deep-water drilling where there is a limited difference between this gradient and the hydrostatic load required by the drilling fluid for controlling the pore pressure of the formation.

In order to lighten drilling mud, hollow glass microspheres with a low density having an average diameter, measured according to ASTM D1214-1989, ranging from 5 to 200  $\mu\text{m}$ , can be fed, in an intermediate position of the well. These microspheres reduce the density of the mud, once the larger drilling cuttings have been eliminated, to values ranging from 0.7 to 1.3  $\text{g}/\text{cm}^3$ , preferably from 0.95 to 1.05  $\text{g}/\text{cm}^3$ . These microspheres, capable of resisting the strong pressures present inside the wells, are available on the market as the commercial product of Minnesota Mining Manufacturing (3M), for example under the trade-name of S38HS, with an average density ranging from 0.35 to 0.41  $\text{g}/\text{cm}^3$  and an apparent density ranging from 0.19 to 0.28  $\text{g}/\text{cm}^3$ . In literature, patent U.S. 2,978,340 describes a process for the preparation of hollow glass microspheres.

If the use of hollow glass microspheres solves, on one hand, the problem of the hydrostatic seal, on the other hand, it creates another problem in that it is extremely

difficult to separate these bubbles from the mud in order to re-use them. As a result, large quantities of these microspheres are lost.

The Applicants have now found a method which allows the recovery of at least 70% of the hollow glass microspheres dispersed in a mixture of muds and cuttings, coming from a drilling well, which is simple as it does not require the use of any particular technological expedients.

The object of the present invention therefore relates to a process for recovering at least 70% of hollow glass microspheres having an average diameter, measured according to ASTM D1214-1989, ranging from 5 to 200  $\mu\text{m}$  contained in a mixture of drilling mud and cuttings which comprises:

- a) screening, if necessary, the mixture through one or more 5 to 20 mesh sieves;
- b) feeding the screened mixture to one or more cyclones and/or hydrocyclones arranged in series, each of which is fed with a volume flow-rate from 1.5 to 10 times higher than the maximum nominal operating value.

At the end of the possible screening, a part of the cuttings produced by the bit during drilling, higher than 50% by weight, is substantially eliminated, leaving a fluid which has a density ranging from 0.7 to 1.3  $\text{g}/\text{cm}^3$ , preferably from 0.95 to 1.05  $\text{g}/\text{cm}^3$ , and a content of microspheres ranging from 1 to 30% by weight, generally from 3 to 25%.

This fluid can be recovered by a high power pump, for example a multistage centrifugal pump, having a specific power equal to at least 1.5 kW/m<sup>3</sup>/h, and fed to the cyclones. There are generally 1 to 3 cyclones in series.

5       The viscosity of the fluid, which depends on the type of well in which it is used, can be regulated to optimum pumping values by diluting the mud or thickening it with clay and/or other viscosizing agents.

10       The cyclones and/or hydrocyclones used in the process object of the present invention are traditional devices described, for example, in "Ullmann's Encyclopedia of Industrial Chemistry", Fifth Edition, 1988, Vol. B2 or in "Hydrocyclones", L. Svarovsky Holt, Rinehart and Winston, 1984, and are capable of treating dispersions and/or sus-  
15       pensions of solids with nominal operating flow-rates ranging from 3 to 30 m<sup>3</sup>/h.

20       The cyclones and/or hydrocyclones, also commonly called cyclone separators, are generally dimensioned so as to guarantee a flow leaving the base, rich in heavy solids (underflow, UF) and a counter-flow leaving the head, rich in light fraction (overflow, OF). In the process object of the present invention, the overflow leaving the first cyclone can be fed in turn to one or more cyclones in series, operating under analogous conditions to the first, if a  
25       forced separation of the microspheres from the mud is nec-

essary. In any case, operating either with a single cyclone or with several cyclones arranged in series, a recovery of hollow glass microspheres in the overflow equal to at least 70% of the microspheres fed and even over 80%, can be obtained. This stream can be re-used as such and fed to the well to lighten the drilling mud or it can be subjected to further treatment, for example by sedimentation / flotation in water or another liquid, to recover the substantially mud-free microspheres.

Two illustrative and non-limiting examples are provided for a better understanding of the present invention and for its embodiment.

EXAMPLE 1

An amount of mud was prepared in a 10 m<sup>3</sup> tank, having the following composition:

<u>Products</u>	<u>Quantity (kg)</u>	<u>weight %</u>
Water	4000	64.0
KCl	150	2.4
Starch	50	0.8
Xantanes	25	0.4
Antibacterial agent	6	0.1
Cuttings	1439	23.0
S38HS Microspheres (3M)	579	9.3
Total	6250	100.0

The density of the mud was 0.927 g/cm<sup>3</sup> which, by dilu-

tion, was regulated to 0.956 g/cm<sup>3</sup>.

The mud was fed, by means of a pump having a power of 90 kW, to a cyclone with flow-rates of 38 and 60 m<sup>3</sup>/h. The maximum nominal operating flow-rate of the cyclone was 21  
5 m<sup>3</sup>/h.

A stream of fluid (OF) in which the microspheres are concentrated, is recovered from the head of the cyclone, whereas the cuttings are concentrated in the stream at the bottom (UF). The results obtained are indicated in Table 1.

10

TABLE 1

Flow-rate fed (In- let) (m <sup>3</sup> /h)	Flow-rate OF (m <sup>3</sup> /h)	OF/Inlet (%)	Recovery of microspheres (%)
38	10	26	70
	13	34	74
60	16	27	77
	19	32	81

15

20 EXAMPLE 2

Mud prepared and diluted as in example 1, was used for running a test with two cyclones in series with a maximum nominal flow-rate of 11 m<sup>3</sup>/h and 21 m<sup>3</sup>/h respectively, the second cyclone being fed with the OF of the first. The UF  
25 of the first cyclone was regulated so as to form about 13%



of the flow-rate of the flow-rate of the fluid fed. The power of the pump was 90 kW. The results obtained are indicated in Table 2.

TABLE 2

5

Flow-rate fed (Inlet) (m <sup>3</sup> /h)	Flow-rate OF (m <sup>3</sup> /h)	OF/Inlet (%)	Recovery of microspheres (%)
55	14	56	76
	18	33	79

10

15

20

25

CLAIMS

1. A process for recovering at least 70% of hollow glass microspheres having an average diameter, according to ASTM D1214-1989, ranging from 5 to 200  $\mu\text{m}$  contained in  
5 a mixture of drilling mud and cuttings which comprises:
- a) screening, if necessary, the mixture through one or more 5 to 20 mesh sieves;
  - b) feeding the screened mixture to one or more cyclones  
10 and/or hydrocyclones arranged in series, each of which is fed with a volume flow-rate from 1.5 to 10 times higher than the maximum nominal operating value to obtain an underflow rich in heavy solids and an overflow rich in light fraction.
- 15 2. The process according to claim 1, wherein the overall mixture, after screening, has a density ranging from 0.7 to 1.3  $\text{g}/\text{cm}^3$  and a content of microspheres ranging from 1 to 30% by weight.
3. The process according to claim 1 or 2, wherein the  
20 overflow is subjected to sedimentation/flotation in water or another liquid, to recover the substantially mud-free microspheres.
4. The process according to claim 1, 2 or 3, wherein there are from 1 to three cyclones.
- 25 5. The process according to any of the previous claims,

wherein the cyclones have nominal operating flow-rates ranging from 3 to 30 m<sup>3</sup>/h.

5