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(54) Title: A METHOD FOR THE CRYSTALLIZATION OF HUMAN SERUM ALBUMIN

(57) Abstract: The present invention relates to the purification and production of human albumin from various sources through crystallization and repeated crystallization. Basic features of the invented process include providing specific reaction conditions and precipitating reagents to maximize albumin crystallization. Solubility diagrams are utilized as the basis for process control of the invented method. The current invention specifically controls phosphate concentration, pH and temperature to precisely guide crystallization kinetics and crystal yield.



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A METHOD FOR THE CRYSTALLIZATION OF HUMAN SERUM ALBUMIN

FIELD OF THE INVENTION

5 [001] The present invention relates to methods for provide a highly reliable method and commercially viable method of crystallizing human albumin. More specifically, the current invention provides a method to produce crystalline human albumin purified from various albumin sources, specifically including from transgenic animals or other recombinant sources.

BACKGROUND OF THE INVENTION

10 [002] The present invention is directed to an improved method of crystallizing human serum albumin ("hSA")(herein, hSA will be used interchangeably with the term human serum albumin). This process is preferably done to enhance purification
15 procedures for recombinant hSA that can then be utilized in therapeutic applications or as an excipient in pharmaceutical preparations. With regard to pharmaceutical preparations human albumin as purified herein can be used as a therapeutic agent or as an excipient. In either case suitable formulations can be found in REMINGTON'S PHARMACEUTICAL SCIENCES (16th and 18th Eds., Mack Publishing, Easton, Pa. (1980
20 and 1990)), and in INTRODUCTION TO PHARMACEUTICAL DOSAGE FORMS (4th Edition, Lea & Febiger, Philadelphia (1985)), each of which is incorporated herein by reference.

[003] For therapeutic applications of hSA the objective of albumin administration is primarily to maintain circulating plasma volume by maintaining the plasma colloid oncotic pressure, and to treat otherwise resistant severe edema by
25 making intracavital and interstitial fluids move into the blood vessels.

[004] Albumin products are used to achieve transient improvement of the condition by replenishing albumin in pathological conditions attributable to acute hypoproteinemia, and pathological conditions resulting from chronic hypoproteinemia which is resistant to other methods of treatment.

30 [005] Albumin was the first natural colloid composition for clinical use as a blood volume expander, and it is the standard colloidal agent for comparison with other colloid products. Some of the specific medical indications in which albumin may be used to increase intravascular oncotic pressure and thereby expand intravascular

volume in patients include: hypovolemic shock; severe burn injury; adult respiratory distress syndrome (ARDS); ascites; liver failure; pancreatitis and in patients undergoing cardiopulmonary bypass. (Cochrane et al., 1998). Albumin may also be used to treat neonatal hyperbilirubinemia, hypoproteinemia, and nephrotic syndrome. (Vermeulen et al., 1995).

[006] The albumin portion of human blood serves three primary physiologic roles: (1) maintenance of plasma colloid osmotic pressure, (2) transport and sequestration of bilirubin, and (3) transport of fatty acids and other intermediate metabolites such as hormones and enzymes. (Peters, T et. al.,). Because albumin accounts for approximately 80% of the oncotic pressure of plasma, a 50% reduction in serum albumin concentration consequently produces a 66% decrease in colloid oncotic pressure. (Rainey T.G., et al., 1994). In critically ill patients, risk of death is inversely related to serum albumin concentration. (Cochrane et al., 1998). Goldwaser and Feldman estimate that for each 2.5 g/dL decrease in serum albumin concentration, there is a 24%–56% increase in the risk of death. (Goldwaser et al., 1997). This estimate was made after adjusting for other co-variants (e.g., renal function, serum trans-aminase, lactic acidosis), and it strongly indicates that albumin infusion may have a direct cytoprotective effect. (Cochrane et al., 1998).

[007] Given the above, it is clear that hSA is perhaps the best known of all the plasma proteins judging both by the amount of scientific literature available describing it as well as through the number of industrial uses it enjoys. However, this abundant amount of knowledge is focused primarily on its physiology and the clinical use of albumin, not the methodology used to purify it or sourcing the molecule from anything other than plasma fractionation. The best-known and still widely used purification methods were developed by Cohn and co-workers 60 years ago (Cohn E.J. et al., 1947). The Cohn plasma fractionation method is primarily used to produce purified plasma products for a wide variety of clinical uses. Cohn also developed a widely used crystallization process which utilizes principles similar to those well-known from plasma fractionation processes for use with human serum albumin. However, the process has significant inefficiencies and often does not provide an adequate supply of highly purified hSA.

Effect of pH

[008] The effect of pH is one of the major factors in protein crystallization. Usually protein crystals have a well-defined minimum point of solubility at a specific pH. In the general literature of protein crystallization, it is most often the case that this
5 minimum solubility is at the isoelectric point of the target protein. However, hSA is highly soluble at its isoelectric point, across a wide range of ionic strengths. Thus, the crystallization properties of albumin are much more complex than those of many other proteins making reliable crystallization and/or purification problematic.

[009] Albumin has a varying isoelectric point depending on the chemical
10 treatment that it has received. With a full complement of six bound fatty acids hSA's pI is normally 4.6, however, when fully de-fatted its pI may be as high as 5.6. Therefore, the crystallization properties of hSA vary as between its "native" and de-fatted states and the reported optimum pH for the crystallization of hSA itself varies substantially in the literature from a low of pH 4.6 to a high of pH 8.0 and may be
15 highly dependent upon the molecular state of hSA in a batch-by-batch basis. Thus, the wide range of pH that is considered to be optimal for the crystallization of hSA present in the literature is confusing and apparently relies on various precipitating reagents, each of which is utilized having a variable concentration and which may be optimal for only one of the possible molecular states of hSA.

[0010] For example, with hSA at low ionic strength, like that expected in the
20 Cohn alcohol process, crystallization proceeds optimally at pH 4.9 – 5.3 which is close to the isoelectric point of native albumin. In conditions with a higher ionic strength and when strongly buffered the optimal pH for crystallization by PEG solutions is 7.4. In sum, the reported pH effects for optimal crystallization of hSA are dependent on the
25 reagent composition in such a seemingly irregular way that solid conclusions cannot be made by reference to the prior art and prior art methodology. In fact, given the status of the teachings of the prior art, every new reagent and technique must be laboriously optimized according to a specific pH or other single variable to be kept constant while crystallization conditions are worked out.

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Effect of Precipitating Reagents

[0011] It should be noted that hSA has a very high solubility in varying salt concentrations. It can be precipitated or crystallized at low ionic strength with added ethanol (Cohn process; Cohn E.J. et al., 1947) or other solvents. Alternatively, salting

out with very high salt concentration is possible, and the early literature mostly used ammonium sulfate or ethanol is described. In the more recent literature PEG solutions of various molecular weights have been utilized widely. However, the reagents present in the literature are unacceptable for the clinical use of the resulting hSA because of the remaining contaminants. Of the prior art precipitating reagents only ethanol and ammonium sulfate are useful in the production of hSA. However, they both have significant practical problems. Crystallization with ethanol requires the addition of toxic organic modifiers such as benzene or heavy metals. Ammonium sulfate is not a suitable salt for final albumin formulation, and would thus need to be removed.

Effect of Specific Reagents

[0012] In addition to its other characteristics albumin has an extraordinary capacity to combine and attach to a wide variety of smaller molecules and ions. The association of various long chain alcohols and fatty acids with hSA strongly affect the crystallization profile of molecular hSA and again act to make the production of clinical grade human serum albumin highly variable and unpredictable. Examples of reagents capable of significantly effecting the crystallization profile of hSA include: decanol, palmitic acid and caprylic acid.

Effect of Temperature

[0013] It should also be noted that prior art attempts to crystallize hSA in ethanol solutions have typically been made at low temperatures in the range of 0 - 10°C. High salt and PEG procedures are often made at a wider temperature range of 4 - 20°C. In these prior art efforts it is not clear what the effect of temperature really is on albumin precipitation. In ethanol the crystal solubility is seemingly lower at low temperature. The effect of temperature is not clearly described in the PEG and salt methods found in the prior art. For production efficiency and commercial viable processes temperature is one of the major factors. Overall, the significance of temperature is not explained or disclosed by the prior art.

Kinetics and Seeding

[0014] According to the prior art, the time period needed for the crystallization of albumin in a given reaction to be complete can take up to several days. However, of

the prior art methods those employing ethanol may be the most rapid, requiring only 12 to 24 hours to initiate crystallization. Also according to prior art methods the actual crystallization of albumin may not be possible at all without additives including seeding a reaction mixture with crystals formed from a prior reaction. In addition, the methods
5 of crystallization relying on PEG, may or may not utilize this type of additive. It should be noted that seeding does speed up the crystal growth significantly, though given the confusion in the art generally there are no references that can be utilized which give consistently reliable results or generate a high yield of crystal.

Table 1.**Example List of Crystallizing Reagents and Conditions Found in the Literature.**

Precipitants	Additives	buffers 0.05 – 0.1 M	pH	temp. °C	References
(NH ₄) ₂ SO ₄ 50% Na ₂ SO ₄ 15-20% K-phosphate 2.2M Na-phosphate 3M	Decanol	phosphate acetate	4.6-7.7 5.0- 6.8 5.9 6.8	4-6 20 4-6	Haupt, H. and Heide, K.Klin. Wochenschr. (1967), 45(14), pp.726- 729.
PEG 180-800 40 % PEG 400 40 %		K-phosphate Na-acetate Na-citrate, Tris	4.6- 7.2 6.8 5.5-7.2	4	(1) Carter, D. C. EP 0 357 857 A1 <i>and</i> (2) Carter, D. C.et.al. Science 244 (4909) (1989) p.1195
PEG 3350 17.5%	long chain fatty acids	phosphates Na-acetate Na-citrate, Tris	7.5 4.6-8.0 7.0-7.5	22	(1) Carter, D. C. U.S. 5.585.466 <i>and</i> (2) Carter, D. C.et.al. <i>Eur.J. Biochem.</i> 226(3)(1994) p.1049
PEG 3350 28-30%		K-phosphate	7	4	Bhattacharya et al <i>J.</i> <i>Biol. Chem.</i> 275(49)(2000) p. 38731
PEG 400, 4000 20-38%		K-phosphate	5.0-5.5 7.0-8.0	15-20	Sugio, S. et.al. <i>Prot. Eng.</i> 12(6) (1999) p.439
(NH ₄) ₂ SO ₄ 45% saturated	Decanol	K-phosphate	6	4	Rao, S. et.al. <i>J. Biol.</i> <i>Chem.</i> 251(10) (1976) p.3191
MPD	Decanol 0.1 %		5.2	1	McClure, R.J. et.al. <i>J.</i> <i>Mol. Biol.</i> 83(4) (1974) p.551
Ethanol			5.2	2	Low, B.W. <i>J. Am. Chem.</i> <i>Soc.</i> 74(1952) p. 4830
(NH ₄) ₂ SO ₄ 54% saturated.	Decanol 0.2 %		6.8	1	Low, B.W. and Weichel, E.J. <i>J. Am. Chem. Soc.</i> 73(1951) p. 3911
Methanol Ethanol 5-30% Acetone	Numerou s compoun ds heavy metals	acetate	4.4-6.5 4.9-5.1	-5 --- +5	Lewin, J. <i>J. Am. Chem.</i> <i>Soc.</i> 73 (1951) p. 3906
Ethanol, mole fractions 0.02 – 0.163	CHCl ₃ Decanol, benzene,		4.9 5.3	-5 --- +10	Cohn, E.J. et.al. <i>J. Am.</i> <i>Chem. Soc.</i> 69 (1947) p.1753
Ethanol 15%	Decanol HgCl ₃		5.2	<0	Hughes, W.L. <i>J. Am.</i> <i>Chem. Soc.</i> 69 (1947) p.1836

Prior Art Methodology with Mineral Salts

[0015] The prior art (Haupt and Heide (1967)) provided methods to crystallize human serum albumin with various mineral salts including: 50% saturated $(\text{NH}_4)_2\text{SO}_4$; 15-20% Na_2SO_4 ; 2.2M K-phosphate pH 6.8 and 3M Na-phosphate pH 5.0. Decanol
5 was found to be a necessary crystallization aid in these prior art methods. Other fatty alcohols with more than five carbon atoms in their molecular backbone were found to be useful also. However, the crystallization conditions and procedures were very sparingly described. No material balances were presented. On the basis of the data available from this citation it is not possible to perform crystallization of albumin in a
10 sufficiently controlled or reliable way.

[0016] A review of the prior art literature indicates that while there are several methods of crystallization proposed the relevant citations do not teach a process that is efficient at an industrial or commercial scale, teach a method that is unavailable for use in the production of a therapeutic product or excipient, or provide a process only useful
15 in the production of single crystals useful only in x-ray diffraction studies. Thus, the limitations of the prior art prevent the development of the extensive knowledge of crystallizing conditions necessary in the design of a large-scale crystallization processes for hSA in a therapeutic, pharmaceutical excipient, or medical adjuvant role. Moreover, the prior art does not provide teachings that provide for the use from sources other than
20 human plasma. Therefore, a need exists to understand the physical and chemical conditions which produce crystals of albumin reliably and on an commercial scale from a variety of sources.

SUMMARY OF THE INVENTION

[0017] The present invention provides improved methods for producing
25 crystalline human albumin. The method is suitable for various albumin sources including: human plasma, and from recombinant albumin sources such as cultured mammalian cells, the milk or other bodily fluids of transgenic mammals, transgenic plants, transgenic avians, recombinant bacterial cell cultures, recombinant yeast cell
30 cultures or recombinant insect cell cultures. That is, it is useful for the production of crystallized and pharmaceutically grade hSA regardless of the feedstream from which it comes. The method has a high purification power so that crystalline albumin can be effectively separated from other proteins, bacteria, fatty acids or other molecular species present in a particular starting material or feedstream. In an additional

embodiment of the current invention, albumin can be dissolved and re-crystallized by heating and cooling cycle in the crystallizing medium. This, re-crystallization procedure can be repeated unlimited number of times according the needs of the user of the current invention. Purity of albumin is regularly improved in the re-crystallization
5 procedure.

[0018] The methods of the current invention also provide precise combinations of reagents and conditions that allow the optimization of the production of crystalline human albumin. In these methods important the process parameters such as pH and temperature are precisely manipulated. An additional embodiment of the current
10 invention provides optimal concentrations of precipitating agents of sodium or potassium phosphates and/or caprylic acid or caprylate salts.

[0019] The process of the current invention is based on certain key factors influencing the crystallization of human albumin. Preferably, the process of the current invention optimizes the following variables in a specific manner so as to optimize the
15 crystallization protocol parameters as follows:

1. changing the phosphate salt concentration in planned steps;
2. varying the temperature of the reaction mixture in planned steps
20 wherein heating and cooling procedures are applied successively;
3. controlling the pH or varying the pH of the reaction mixture planned steps manner;
- 25 4. wherein the application of these specific steps allows the purification and crystallization of human albumin from a given feedstream.

[0020] Other features and advantages of this invention will become apparent in
30 the following detailed description of preferred embodiments of this invention, taken with reference to the accompanying drawings

BRIEF DESCRIPTION OF THE DRAWINGS

- [0021] FIG. 1 shows a process flow diagram for crystallization of recombinant human serum albumin.
- 5 [0022] FIG. 2 shows albumin solubility at different temperatures at pH 6.2, with exponential trendlines.
- [0023] FIG. 3 shows albumin solubility at different temperatures at pH 6.2, with linear trendlines
- 10 [0024] FIG. 4 shows pH Solubility of albumin crystals at 15°C.
- [0025] FIG. 5 provides a solubility study of washed albumin crystals in different phosphate solution at a pH of 6.2.
- 15 [0026] FIG. 6 provides a solubility study of washed albumin crystals in a 2.63M phosphate solution with varying caprylate concentration.
- [0027] FIG. 7 shows a heat precipitation study of hSA crystal slurry in 2.7 M phosphate pH 6.2.
- 20 [0028] FIG. 8 shows a process flow diagram for preparative crystallization of albumin.
- [0029] FIG. 9 shows a process flow diagram for crystallization of recombinant human serum albumin.
- 25 [0030] FIG. 10 shows a process flow diagram for the re-crystallization of recombinant human serum albumin.
- [0031] FIG. 11 shows crystallized human albumin in a solution mixture that is 2.3 Molar Na-K-Phosphate with a pH of 6.2; Caprylate 1.4mg/ml; hSA 80 mg/ml crystallized at 4°C overnight, with two hours at room temperature (RT) in an air tight chamber.
- 30 [0032] FIG. 12 shows crystallized human albumin. shows crystallized human albumin in a solution mixture that is 2.5 Molar Na-K-Phosphate with a pH of 6.2; saturated with Caprylate; hSA 46.5 mg/ml crystallized at 4°C overnight.
- 35 [0033] FIG. 13 shows crystallized human albumin in a solution mixture that is 2.3 Molar Na-K-Phosphate with a pH of 6.2; Caprylate 1.4mg/ml; hSA 80 mg/ml crystallized at 4°C overnight, with 0 hours at room temperature (RT) in an air tight chamber.
- 40 [0034] FIG. 14 shows, albumin crystals of the invention along with more amorphous precipitate. The typical crystal size is approximately 0.1 x 0.4 mm. The precipitate disappears over time becomes crystalline. The crystals were prepared at 4°C in 2.7 Molar ammonium sulfate containing 0.08 % decanol; 0.05 M Na-K phosphate at pH 7.4. Crystallized at 4°C' hSA 58.7 mg/ml.
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DESCRIPTION OF THE PREFERRED EMBODIMENT

[0035] The following abbreviations have designated meanings in the specification:

Abbreviation Key:

5 pH A term used to describe the hydrogen-ion activity of a chemical or compound according to well-known scientific parameters.

PEG An abbreviation for polyethylene glycol

10 **Explanation of Terms:**

Colloids - Refers to large molecules that do not pass readily across capillary walls. These compounds exert an oncotic (i.e., they attract fluid) load and are usually administered to restore intravascular volume and improve tissue perfusion.

15

Diafiltration - An operation incorporating ultrafiltration membranes to efficiently remove salts or other small molecules from a macromolecular solution. The purpose is to remove small molecules from albumin in solution and adjust the buffer for the next procedure.

20

Tissue Perfusion - The amount of blood flow to tissue.

25

Feedstream -The raw material or raw solution provided for a process or method and containing a protein of interest.

[0036] The methods of the current invention for the crystallization of hSA provide a highly desirable method to separate and purify albumin from a feedstream containing a variety of other protein components. Crystals are the most pure form of protein, once precipitated crystals have significantly better mechanical handling properties than amorphous precipitates and can be separated by a variety of methods known in the field. For example, crystals can be separated and washed efficiently on industrial filters. Crystallization is the most used final purification method of fine chemicals and pharmaceuticals.

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[0037] According to a preferred embodiment of the current invention albumin is crystallized with a mixture of sodium and potassium phosphates. Crystallization is optimized by using the invented process conditions and methods in a systematic manner. Albumin may precipitate as amorphous phase, liquid droplets or gel if the conditions are not adjusted optimally. Amorphous precipitate is very difficult to handle, it can not be separated and washed efficiently on filters. Amorphous phase does not

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readily convert to crystals. Crystals production is optimized when the process conditions are adjusted according to this invention. Various embodiments of the current invention are provided below.

5 **1. Phosphate Salts:**

 [0038] Mixtures of sodium and potassium phosphates are preferably used, although crystallization can be made either with sodium phosphate alone or potassium phosphate alone. Phosphate salts NaH_2PO_4 and K_2HPO_4 are preferred since they can be dissolved in concentrates of up to 4 molar aqueous solutions. These 4 M phosphates
10 can be mixed in all proportions to make 4 M crystallization buffers with various desirable pH values.

 [0039] Preferably, albumin is crystallized in relatively high phosphate concentration, typically around 2.7 M or higher. The significance of phosphate concentration is most clearly revealed in the Figures 1 and 2, which describe the
15 solubility of albumin crystals in phosphates with different molarities. The semi-logarithmic plot of Figure 2 shows that crystal solubility is systematically lowered by increasing phosphate molarities. Albumin yield can be adjusted in the process to a desirable level by using increasing molar concentrations of phosphates. Upper limits for usable phosphate concentrations are set by the solubility of phosphate salts. Phosphate
20 solubility is lowered by lowering temperature and increasing albumin concentration. In one embodiment of the current process phosphate solubility is significantly lowered by reducing the temperature of the reagent to below 10°C. By lowering the temperature of the reagent and increasing the albumin concentration the available water concentration is also being lowered.

25 [0040] According to a preferred embodiment of the current invention, most of the impurities precipitate effectively in starting material in the range of phosphate concentration 2.0 – 2.7 M, where albumin does not readily crystallize at room temperature (25 - 30 °C). The impurities are removed by being filtered (after adjusting phosphate concentration 2.0 – 2.7 M). Thereafter the filtrate is refrigerated to 10 °C
30 where albumin is crystallized. Furthermore, phosphate concentration can be increased (utilizing the information of Figures 1 and 2) in order to increase albumin yield in the crystals, see also Table 2 and Figure 4.

2. Significance of pH:

[0041] According to the current invention the pH of the crystallizing batch is fully controlled with the phosphate mixture. Examples of the mixtures with various pH values and the resulting effect on the albumin crystals are presented in the Table 1. The effect of pH on the albumin crystal solubility is presented graphically in the Figure 2, see also Table 2. Albumin crystal solubility is lowered by lowering pH from pH 5.6 to approximately 6.6. The crystal solubility remains at very low level up to at least pH 7.4. Crystals are completely dissolved below pH 5.5.

[0042] The pH has a specific effect on the crystallization kinetics, thus the higher pH range 6.3 – 7.4 can not be used in a simple way. In the higher pH range, albumin precipitates as amorphous (liquid droplet) phase if such pH is adjusted right in the beginning of the process. Thus the crystallization process is preferably made initially with the phosphate pH 6.2 (see table 1 for mixing recipe of phosphates and Figures 2 and 3). Later on when albumin is mostly crystallized, phosphate concentration is increased and pH adjusted to higher value in order to increase the crystal yield. Higher pH is also used advantageously when washing crystals, since the loss of albumin is reduced.

3. Effect of Temperature

[0043] The solubility of albumin crystals at different temperatures and phosphate concentrations is presented graphically in the Figure 3. Albumin crystal solubility is increasing at higher temperatures. Lowest solubility is found around 0°C. However, the preferred crystallizing temperature is around 10°C, since at lower temperature phosphate may crystallize and bring the process out of control. The example procedures around 0°C were possible to be performed, since phosphate crystallization is relatively slow.

[0044] The crystallization kinetics of albumin is very slow at room temperature. Thus the phosphate concentration can be adjusted to 2.6 – 2.7 at room temperature without precipitating or crystallizing albumin. However, impurities are readily precipitated at room temperature. After being filtered, albumin solution is refrigerated to preferably 10°C. The solution is stirred and albumin is crystallized.

[0045] Albumin can be re-crystallized by utilizing a heating cycle. The crystals are dissolved by heating to 45 °C. Albumin is crystallized again after refrigeration to 10 °C. Re-crystallization can be used to improve the crystal purity. After each crystallization, the mother liquor can be removed by being filtered. Crystals can be washed on the filter with cold 3 M phosphate. Re-crystallization cycle can be repeated unlimited number of times. Recrystallization can be used to improve albumin purity. For convenience please see Tables 7 and 8 and Figure 7.

[0046] Albumin is relatively heat stable. It can be heated up to 65 – 70 °C for prolonged periods. Most other proteins denature and precipitate at such high temperatures. Thus heating treatment at 65 – 70 °C can be used to purify albumin solution prior to crystallization. The highest tolerable temperature is related to the composition and pH of albumin solution. In high phosphate concentration pH 6.2 the highest temperature is 65 °C. In low salt medium and pH 5.4 heating at 70 °C for 2 – 3 hours is possible. Examples of the effect of heat treatment are presented in the Tables 2 and 3 and Figure 6.

4. Caprylate

[0047] Albumin needs to be saturated with caprylate to be able to crystallize. Caprylate has also a stabilizing effect on the albumin, specially on heat stability. Other long chain fatty acids and long chain alcohols are alternatively useful. Decanol is very effective and well known in prior art. Caprylate has dual effect depending of how it is used. It is beneficial when it is used only to saturate the binding sites of albumin. However, excess of caprylate will dissolve crystals and reduce albumin yield.

[0048] The effect of caprylate is well revealed in the Figure 4. Addition of caprylate to the washed crystals clearly increased crystal solubility. Crystal solubility was rapidly increasing when caprylate was increasing up to 10 mM. The solubility increment was smaller but still significant when caprylate was increasing from 10 mM to 20 mM. At phosphate concentration 2.63 M and temperature 10°C, albumin solubility increased from 9 mg/ml in 0 mM caprylate to 21 mg/ml in 10 mM caprylate. At higher phosphate concentration 2.82 M and temperature 10 °C, albumin solubility increased from 2 mg/ml in 0 mM caprylate to 12 mg/ml in 10 mM caprylate.

[0049] Dissolving effect of caprylate is so significant that concentration of free caprylate should be well controlled and maintained as low as possible in the

crystallizing step. Small level of free caprylate, order of 1-2 mM may be acceptable when conditions are otherwise such that albumin crystal solubility is very low. Please see Figures 2 through 7.

5 5. Albumin: Concentration, Purity

[0050] In experimental solutions albumin concentration in the starting solution is set to a level that is higher than the solubility of crystals in the conditions utilized. According to the current invention, when working with a feedstream sourced from a transgenic animal or cell culture initial clarification steps are typically used to provide a
10 solution in with the concentration of albumin and other chemical parameters are adjusted or manipulated such that it is also higher than the solubility of hSA crystals. In both of these situations albumin recovery can be estimated by using the solubility information in the phase diagrams (Figures 1-4). According to the current invention concentration levels of albumin in feedstream solutions are typically in the range of 15
15 – 300 grams of albumin in one liter of crystallizing batch. In feedstreams from biological sources and usable for the commercial or industrial production of hSA these same ranges are encountered.

[0051] Moreover, albumin need not be pure in the crystallizing process according to the preferred embodiments of the current invention. The processes
20 developed - and provided by the current invention can be utilized to crystallize out albumin in source material wherein the level of purity is approximately 10%, that is, where albumin constitutes only 10% of the total protein of a given solution. For example, with hSA sourced from either transgenic sources or cell cultures most of the impurities remaining after clarification procedures can be removed after precipitation
25 with the first addition of phosphate up to 2.6 M concentration level. It should be noted that transgenic sources, typically milk, but also including other bodily fluids such as blood or urine may contain hSA as a consequence of the insertion of DNA constructs designed to cause the stable expression of hSA (or other protein of interest) in those bodily fluids or tissues. After the precipitation and being filtered, the filtrate is further
30 concentrated by ultrafiltration in order to increase albumin concentration level. Thereafter the concentrated albumin solution is refrigerated and crystallized according to the current invention.

EXAMPLE 1

A PREFERRED CRYSTALLIZATION PROCESS

[0052] This process description is made for the crystallization of a purified
5 albumin solution and for that purposes describes the use of only a phosphate solution
only. However, according to the current invention this method can be used on impure
or only partially purified starting material, as may be found from transgenic or cell
culture feedstreams, with the addition of additional steps provided herein. Variations of
the inventive method, for example utilizing starting solutions with significant impure
10 material, are presented below.

Step 1. Precipitation

[0053] Phosphate stock solution, containing 2.8 moles of NaH_2PO_4 and 1.2
15 moles of K_2HPO_4 dissolved in water and filled to 1.0 liter, was used in crystallization.
This 4 M phosphate solution had pH 6.2 when measured after dilution to 0.5 M.
Thereafter, 200 ml of a purified albumin solution was precipitated by adding 371 ml of
4.0M phosphate stock solution at a pH of 6.2. On the basis of the added volume, the
phosphate concentration was 2.6 M. The solution was allowed to precipitate at room
20 temperature for 4 – 18 hours, for this variation of the current invention the time period
of interest is short relative to prior art methods, in all cases less than 24 hours. The
amount of the produced precipitate is directly related to the amount of impurities in the
albumin solution.

25

Step 2. Filtration

[0054] Thereafter, the precipitated hSA was filtered through glass fiber or
cellulose fiber paper having approximately 1 μm pore size. The filtered solution was
then used in a preferred crystallization procedure according to the invention.

30

Step 3. Crystallization

[0055] Crystallization was performed in 10 °C thermostat incubator. The batch
was stirred slowly (approximately 70 rpm) with a top driven propeller. Phosphate

concentration was increased gradually from 2.6 M to 3 M by adding 229 ml of 4M phosphate which was at a pH of 6.2. The crystallization batch was continued for a period of 4 days before harvesting and washing.

5

Step 4. Harvesting and Washing of Crystals

[0056] According to a preferred embodiment of the current invention hSA crystals were harvested by filtering the batch with glass fiber paper (1 μ m pore size, 142 mm diameter). After being filtered, crystals were then washed with about 80 ml of cold 3 M phosphate pH 6.2. Crystals were then suspended in about 150 ml of cold 3 M phosphate pH 6.2.

[0057] With regard to Table 2 below and the preferred crystallization processes of the current invention, it is preferably if the mixing volume ratios are kept fixed. Preferably, the pH should not be adjusted after making the buffer mixture. For this embodiment of the invention the pH values are approximate, since the value will change with the alteration in phosphate concentration. The buffers of the current invention were used in the study for effect of pH on crystal solubility. As seen below in Table 2, Buffer No: 10 provides conditions that are consistently optimized for crystal development and the conditions provided for this buffer are the preferred conditions for the standard buffer of the current invention. (See also, Figures 11-13).

25

30

Table 2. Mixing Table For 4 M Phosphate Buffers

Buffer No:	Diluted	mixing volumes of 4 M A and B		Behavior of hSA crystals in 2.6 – 2.8 M buffers
	PH	A 4M NaH₂PO₄	B 4M K₂HPO₄	
1	5.3	95	5	hSA dissolved
2	5.4	94	6	hSA dissolved
3	5.5	92	8	hSA dissolved
4	5.6	90	10	hSA Crystallized
5	5.7	87	13	hSA Crystallized
6	5.8	84	16	hSA Crystallized
7	5.9	80	20	hSA Crystallized
8	6.0	77	23	hSA Crystallized
9	6.1	74	26	hSA Crystallized
10	6.2	70	30	hSA Crystallized
11	6.3	65	35	hSA Crystallized
12	6.4	60	40	hSA Crystallized
13	6.5	55	45	hSA crystals are stable
14	6.6	50	50	hSA crystals are stable
15	6.7	43	57	hSA crystals are stable
16	6.8	39	61	hSA crystals are stable
17	6.9	35	65	hSA crystals are stable
18	7.0	30	70	hSA crystals are stable
19	7.1	27	73	hSA crystals are stable
20	7.2	24	76	hSA crystals are stable
21	7.3	21	79	hSA crystals are stable
22	7.4	18	82	hSA crystals are stable

PHOSPHATE BUFFERS

pH values are for diluted buffers in the range of 0.1 – 0.4 M.

The buffer No: 11. pH 6.3 is not much influenced by dilution.

- 5 The buffers No: 1 – 10 have **lower pH** when M is higher.
 Buffers No: 12- 30 have **higher pH** when molarities are higher.

- 10 [0058] It should also be noted that in Figure 6 of the current disclosure provides a profile of albumin solubility in 2.63 M phosphate as a function of caprylate concentration and temperature: open circles (o) mark samples incubated at 10 °C and black squares (■) mark samples incubated at 5°C.

15 **Example 2**

CRYSTALLIZATION OF ALBUMIN WITH THE MICRODIFFUSION METHOD

[0059] Crystallization examples from 48 samples were prepared according to a hanging drop microdiffusion method known in the art. The sample solution contained

purified 198 mg/ml of albumin and 3.2 mg/ml sodium caprylate. The liquid solution of albumin was prepared by mixing 3 μ l of albumin solution with 3 μ l of 1.8 – 2.3 M phosphate. The drops were allowed to equilibrate in the closed microdiffusion wells and refrigerated at 5 °C. Crystals were produced in less than 24 hours according to this
5 embodiment of the the current invention. According to the current invention, feedstreams from other source material, especially transgenic and cell culture sources, can also be utilized in conjunction with a microdiffusion hanging drop method.

[0060] The crystals were observed with microscope and photographed with digital camera. Information regarding the development of the crystals are provided on
10 tables 19 and 20. These examples show that caprylate saturated albumin is crystallized in 1.8 M through 2.3 M phosphates in a sharply defined pH range, that is, from 5.0 – 6.4. The most preferred pH for crystal formation was at pH 6.2, as seen below in Table 3. The range of experimental conditions provided effectively covers the range of concentrations and solution parameters that have been seen in alternate feedstream
15 sources, see Table 4.

Table 3.

Sample: Mix 90 μ l hSA concentrate 210 mg/ml and 10 μ l caprylate solution (32 mg/ml pH 7.3). Final caprylate concentration is 3.2 mg/ml. Drop: 3 μ l sample + 3 μ l reagent		Microscopy Observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets d = days G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Temperature 5 °C					
Initial protein concentration: 95 mg/ml					
Final protein concentration: 198 mg/ml					
well	Reagents:	Number of days (d), temperature (°C)			
		1 d, 5 °C	3 d, 5 °C	8 d, 5 °C	18d, 5 °C
A1	1.8 M Na-K-phosphate pH 5.0	L	L	C, G	A, G
A2	1.8 M Na-K-phosphate pH 5.6	L	L	C, L, A	C, L, G
A3	1.8 M Na-K-phosphate pH 6.2	L	C	C	C, G
A4	1.8 M Na-K-phosphate pH 7.0	L, G	L, G	L, G	G
A5	1.8 M Na-K-phosphate pH 7.4	G	G	G	G
A6	1.8 M Na-K-phosphate pH 8.2	G	G	G	G
B1	2.0 M Na-K-phosphate pH 5.0	L	L	G	A, G
B2	2.0 M Na-K-phosphate pH 5.6	L, A	L, A	L, G	A, G
B3	2.0 M Na-K-phosphate pH 6.2	L, C	C	C, G	C, G
B4	2.0 M Na-K-phosphate pH 7.0	A, G	A, G	G	G
B5	2.0 M Na-K-phosphate pH 7.4	A, G	A, G	G	G
B6	2.0 M Na-K-phosphate pH 8.2	A, G	A, G	G	G
C1	2.2 M Na-K-phosphate pH 5.0	L, A	L, A	L, A	A, G
C2	2.2 M Na-K-phosphate pH 5.6	L, A	L, A	L, A	A, G
C3	2.2 M Na-K-phosphate pH 6.2	L, C	C	C	C, G
C4	2.2 M Na-K-phosphate pH 7.0	A, G	A, G	G	G
C5	2.2 M Na-K-phosphate pH 7.4	A, G	A, G	G	G
C6	2.2 M Na-K-phosphate pH 8.2	A, G	A, G	G	G
D1	2.3 M Na-K-phosphate pH 5.0	L, A	L, A	L, A	A, G
D2	2.3 M Na-K-phosphate pH 5.6	L	L	L	A, G
D3	2.3 M Na-K-phosphate pH 6.2	L, C	C	C	C, G
D4	2.3 M Na-K-phosphate pH 7.0	A, G	A, G	G	G
D5	2.3 M Na-K-phosphate pH 7.4	A, G	A, G	G	G
D6	2.3 M Na-K-phosphate pH 8.2	A, G	A, G	G	G

Table 4.

Box code: MCSA35		Microscopy observations			
Sample: GTC hSA: 7F 4AC, concentrated using dialysis against PEG 20 k. Mix 45 μ l hSA concentrate, 45 ml water and 10 μ l caprylate solution (32 mg/ml pH 7.3.). Final caprylate concentration is 3.2 mg/ml.		C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets d = days G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Drop: 3 μ l sample + 3 μ l reagent					
Temperature 5 °C					
Initial protein concentration: 49 mg/ml					
Final protein concentration: 98 mg/ml					
well	Reagents:	Number of days (d), temperature (°C)			
		1 d, + 5C	2 d, + 5 C	3 d, + 5C	13 d, + 5 C
A1	1.8 M Na-K-phosphate pH 5.9	L	C, L	C, L	C, G
A2	1.8 M Na-K-phosphate pH 6.0-6.1	L	C, L	C, L	C, G
A3	1.8 M Na-K-phosphate pH 6.2	L	C, L	C, L, G	C, G
A4	1.8 M Na-K-phosphate pH 6.3-6.4	L	C, L	L, C	C, G
A5	1.8 M Na-K-phosphate pH 6.4-6.5	L	L	L	C, G
A6	1.8 M Na-K-phosphate pH 6.6	L	L, A	L	G
B1	2.0 M Na-K-phosphate pH 5.9	L	C, L	C, L	C, G
B2	2.0 M Na-K-phosphate pH 6.0-6.1	L	C, L, A	C, L, G	C, G
B3	2.0 M Na-K-phosphate pH 6.2	L	C, L, G	C, LG	C, G
B4	2.0 M Na-K-phosphate pH 6.3-6.4	L	L, G	L, G	G
B5	2.0 M Na-K-phosphate pH 6.4-6.5	L	L, G	L, G	G
B6	2.0 M Na-K-phosphate pH 6.6	L	L, G	L, G	G
C1	2.2 M Na-K-phosphate pH 5.9	L	C, L, A	C, L, A	C, G
C2	2.2 M Na-K-phosphate pH 6.0-6.1	L	C, L, G	C, L, G	C, G
C3	2.2 M Na-K-phosphate pH 6.2	L, C	C, L, G	C, L, G	C, G
C4	2.2 M Na-K-phosphate pH 6.3-6.4	L	L, G, C	C, L, G,	G
C5	2.2 M Na-K-phosphate pH 6.4-6.5	L	L, G	L, G	G
C6	2.2 M Na-K-phosphate pH 6.6	L	L, G	L, G	G
D1	2.3 M Na-K-phosphate pH 5.9	L	C, L, A	C, L, A	C, G
D2	2.3 M Na-K-phosphate pH 6.0-6.1	L, C	C, LG	C, L, G	C, G
D3	2.3 M Na-K-phosphate pH 6.2	L, C	C, LG	C, L, G	C, G
D4	2.3 M Na-K-phosphate pH 6.3-6.4	L	C, L, G,	C, L, G,	G
D5	2.3 M Na-K-phosphate pH 6.4-6.5	L	L, G	L, G	G
D6	2.3 M Na-K-phosphate pH 6.6	L, G	L, G	L, G	G

Example 3

CRYSTALLIZATION OF ALBUMIN IN IMPURE STARTING MATERIAL

[0061] The following process description is originally made from a recombinant hSA starting material which contains much of impurities which interfere

the crystallization. The first process steps are needed for removal of impurities. If more pure albumin is used, the number of steps is correspondingly reduced.

Step 1. Concentration

5 [0062] The starting material should be concentrated by ultrafiltration filtered as much as possible. High protein concentration will reduce the usage of phosphate and increase the yield of crystallizable rhSA. The material should also be filtered with water in the end of concentration procedure in order to reduce the salts originating from the previous process steps. Guideline for protein concentration: $A_{280\text{nm}} = 150 - 200$.

10

Step 2. Initial Precipitation with Phosphate

 [0063] Add 2.5 volumes of 4 M phosphate (pH 6.2) into 1.5 volumes of rhSA concentrate. The final phosphate concentration at this step is 2.5 M which precipitates impurities but not albumin. This procedure is preferably performed at room
15 temperature.

Step 3. Filtration

 [0064] Remove the precipitate that is filtered out with a Buchner funnel or pressure chamber filter. Diatomaceous earth is used as filter aid, since the precipitate is
20 very finely grained amorphous material. Centrifugation is not a convenient option since the precipitate will float on the top of the liquid.

Step 4. Crystallization

 [0065] Crystallization of hSA is started by adding more of 4 M phosphate (pH
25 6.2) in the filtrate until concentration is 2.8 M. Crystallization is performed at refrigerated temperatures preferably around 5.0°C. Crystallization of the hSA, according to this embodiment of the current invention starts spontaneously within 24 hours. In an alternate embodiment the addition of seed crystals will make the process more rapid.

30

Step 5. Washing of Crystals

 [0066] According to the preferred embodiment of the current invention crystals are washed either by centrifugation or preferably by being filtered. In centrifugation the

crystals float on the top of phosphate buffer. Washing is performed with fresh 2.8 M phosphate solution at temperature around +5°C. Crystal washing should be made with low pressure difference, less than 0.1 bar. The washing is repeated 3 - 4 times until the soluble protein of filtrate remains at nearly constant low level, $A_{280\text{nm}} = 1.0$ or less.

5

Step 6. Formulation of Crystal Stock

[0067] The washed crystals are dispersed in a small volume of the 2.8 M phosphate buffer. Crystals can be stored in this until formulated for the next step.

10

Example 4

CRYSTALLIZATION OF IMPURE ALBUMIN AFTER HEAT TREATMENT

Starting Material

15 [0068] The feedstream material used for this example had had a significant amount of proteins as impurities. Albumin was approximately 30% of the protein present. As already stated this is within the typical range of feedstream materials supplied from clarified or partially purified transgenic or cell culture sources. The solutions used included 107 ml of 4 M phosphate pH 6.2 was added into 200 ml of
20 starting material solution (which was in 2 M phosphate before this step) to get 2.70 M solution. According to the current invention this precipitated solution was used as starting solution for crystallization.

Heat Treatment

25 [0069] The precipitated starting solution (in 2.70 M phosphate) was incubated at 55 °C for 90 minutes. A substantial amount of rod-like crystals were formed along with an amorphous precipitate as a result of this heat treatment. Approximately 75% to 80% of total protein was crystallized or precipitated. The crystals and precipitate were removed by filtering the slurry through glass fiber filter when it was still hot.
30 Some diatomaceous earth was used as a filter aid. Only the supernatant filtrate containing albumin was taken for the next step.

Concentration and Filtration

[0070] After being filtered, the solution had too low albumin concentration for crystallization. Thus it was concentrated and diafiltrated at 55°C with a Fresenius Polysulfone UF 6.2 Hemoflow F5HPS dialysis cartridge. The detailed data of process steps is shown in the table 6.

hSA Crystallization

[0071] Phosphate concentration of the concentrate solution was increased and adjusted slowly to 2.8. At the same time the batch was gently agitated in a refrigerator in order to crystallize hSA.

[0072] The hSA crystals were harvested and washed by vacuum being filtered. Washing solution was 2.88 M phosphate pH 6.4. Heat crystallization of impurities is technically easy and rapid method to remove major impurities of the starting material solution as shown in table 5 below and in Figure 7.

Table 5. Purity Analysis of the Starting Material and Washed Crystals. Results of ELISA Assays.

ELISA assay	Impure Starting Material	Washed Crystal Samples 101-98
BSA (ppm)	85000	14300
β -lactoglobulin (ppm)	3488000	4500
α -lactalbumin (ppm)	143000	> 100
IgG (ppm)	69000	> 1700

Starting material: **Genzyme Transgenics hSA**: albumin concentrate lot # X1131FF, protein concentration assays: TP 84 g/l and 79 g/l, ALB 28.58 g/l and 28.75 g/l.

Table 6. Impure Albumin from Starting Material to Crystals.

Batch number and procedure	Composition of the solution, notes	Volume (ml)	Total prot: A 280 x volume	Protein % of starting material
Start with a lot of product Concentrate, diafiltrate	starting material from Sigma	200	14750	100
Add 4 M phosphate pH 6.2	Phosphate 2.7 M	307	14736	43.7
Heat 90 minutes at 55°C	strongly precipitated, mostly crystalline	307	14736	43.7
Add filter aid and filtrate while hot	clear filtrate	260	3276	22
Concentrate with ultrafiltration	clear concentrate, 1.9 M phosphate	111	3024	20
Add 4 M phosphate gradually, concentrate	Phosphate 2.8 M	90.8	3024	20
Protein in the filtrate	0.45µm filtrate of the crystal slurry	90.8	1843	10
Protein in the crystals	crystals calculated by difference of A280nm 33.3-20.3	90.8	1180	8

Material balance of the whole sequence of steps was calculated using the 200 ml aliquot of the sample solution.

5

EXAMPLE 5**RECRYSTALLIZATION OF ALBUMIN BY USING HEATING AND COOLING CYCLES**

[0073] Previously made hSA crystal slurry in 2.7 M phosphate pH 6.2 with a protein concentration of 37.5 g/l was used as starting material for this study conducted according to a preferred embodiment of the current invention. Five samples of the crystal slurry, 0.50 ml each, were incubated alternatively at 40, 45, 55, 65 or 70 °C for 60 minutes. Crystals were dissolved in all the tested temperatures. At the end of heating, the samples were filtered through 0.45 µm filter. Soluble protein of the filtrates was determined by measuring absorbance at 280 nm.

15

[0074] Approximately 10% of total protein was precipitated when the crystal slurry was incubated at 40 – 55 °C for an hour as seen in tables 7 and 8 and in Figure 13. This value was rather constant in this temperature range and it represents impurities

which were removed in the heating being filtered procedure. When the temperature was increased from 65 to 70 °C, the soluble protein of the sample was decreased from 83 % to 37 %. Thus, also albumin starts to precipitate irreversibly at 70°C.

[0075] After being filtered, samples 1 through 5 were heated up to 65°C were all well recrystallized after 18 hours in refrigerator set at 5 °C. When the sample 5 was incubated at 70 °C, no crystals were produced in the filtrate, which indicates that albumin is not stable at that temperature in 2.7 M phosphate, see Table 8. These examples show that albumin can, according to a preferred embodiment of the current invention, be well purified by using heating up to 65°C and thereafter being filtered and going through appropriate re-crystallization cycles.

Table 7. Results of the Heat Precipitation Study of hSA Crystal Slurry

Sample No:	Heated at	Observation after heat treatment, before being filtered	A 280 of filtrate 0.45 µm	Soluble protein (%) of total
1	40 °C	Slightly turbid solution. Most of the crystals were dissolved	17.08	86
2	45 °C	Slightly turbid solution, no crystals.	17.90	90
3	55 °C	Slightly turbid solution, no crystals.	17.70	89
4	65 °C	Increasingly turbid solution, no crystals.	16.60	83
5	70 °C	Strongly precipitated slurry, no crystals	7.42	37

Table 8. Observations of the heated and filtered samples, re-crystallized at low temperature.

Filtrate of example No:	Heated at	Microscopy observations after crystallization in refrigerator
1	40 °C	Well formed crystals
2	45 °C	Different sizes, large and very small crystals
3	55 °C	Large crystals and crystal clusters
4	65 °C	Crystals and crystal clusters
5	70 °C	Clear solution, no crystals

Example 6

CRYSTALLIZATION OF ALBUMIN AT HIGHER PH

[0076] The studies done according to the current invention show that albumin crystal solubility and crystallization may be dependent on pH. Another issue is the

separation of caprylate in the presence of phosphate buffer. The solubility of caprylate increases at higher pH. Thus, even slightly higher pH would be desirable for optimal crystallization formation. According to the current invention, trial crystallizations were made at a range of pH 6.2 - 6.6 with three different levels of phosphate molarity.

5 Experimental details are presented in the table 9 below.

Evaluation of Results

[0077] As seen in Table 9 below, albumin was crystallized very effectively when pH was increased to the values 6.4 and 6.5. Albumin solubility was very low above pH 6.4. Unfortunately, at the higher pH levels albumin was crystallized as very small needles (See Figures 10 - 13). It is likely that the crystal size could be developed larger by starting the crystallization at lower pH 6.2 or 6.3. After achieving near equilibrium, pH could be adjusted to higher level by gradually adding 4M K₂HPO₄.

15 **Table 9. Test tube crystallization of albumin concentrate 102-5.**

Sample No#. 3 ml each exp. RhSA 31 mg/ml	Soluble protein 20 h (nd = not determined)	phosphate		Microscopy observation N = no phase separation A = amorphous precipitate C = crystals L = liquid phase separation G = gel particle separation
	A280nm	M	pH	
102-9-1	nd	2.46	6.2	N
102-9-2	nd	2.46	6.3	N
102-9-3	17.6	2.46	6.4	Initially L, finally C
102-9-4	6.2	2.46	6.5	L, C, very thin needles
102-9-5	1.5	2.46	6.6	C, very thin needles, A
102-9-6	nd	2.57	6.2	Initially L, finally C
102-9-7	16.2	2.57	6.3	Initially L, G, finally C
102-9-8	9.0	2.57	6.4	L, G, C needles,
102-9-9	0.3	2.57	6.5	C, short needles or rods
102-9-10	nd	2.57	6.6	C, short needles or rods
102-9-11	nd	2.67	6.2	Initially G, finally C
102-9-12	14.9	2.67	6.3	Initially L, G, finally C
102-9-13	0.3	2.67	6.4	C, many very small needles
102-9-14	nd	2.67	6.5	C, many very small needles
102-9-15	nd	2.67	6.6	C, many very small needles

Example 7**RE-CRYSTALLIZATION AND WASHING OF ALBUMIN CRYSTALS****Re-Crystallization and Washing**

5 [0078] The washed crystals (102-12) were heated 5 minutes at 45 °C. The crystals dissolved rapidly. The solution was filtered with 0.45µm syringe filter while still warm. The filtered solution was agitated at 2 °C until crystallized (3 days). The batch was crystallized well (Figure 2). The crystals were harvested by being filtered and washed with 2.82 M pH 6.2 phosphate on a 0.45 µm (50 mm diameter) Sartorius
10 membrane. The washed crystals were dispersed in 2.82 M phosphate buffer.

Table 10. Recrystallization and Washing of Albumin Crystals

Step	MI	A 280nm	albumin g
Start with 102-12	26.9	36.9	1.877
Step 1. heat 5 minutes at 45 °C	26.9		
Step 2. filtrate 0.45 µm	26		
Step 3. agitated at 2 °C 3 days (see: Figure 2)	26		
Step 4. Harvest and wash, filtrates	37.8	3.6	0.256
Crystal suspension in 2.82 M	22.1	34.8	1.451
Sample 102-13 to Sigma 7	18	34.8	1.182

15

INDICATIONS AND USES**Hypovolemia**

20 [0079] Hypovolemia is a possible indication for albumin purified and made available by the method of the current invention, 25% Solution, Buminate 25%. Its effectiveness in reversing hypovolemia depends largely upon its ability to draw interstitial fluid into the circulation. It is most effective with patients who are well hydrated. When hypovolemia is long standing and hypoalbuminemia exists
25 accompanied by adequate hydration or edema, 25% albumin is preferable to 5% protein solutions. However, in the absence of adequate or excessive hydration, 5% protein solutions should be used or 25% albumin should be diluted with crystalloid. Although crystalloid solutions and colloid-containing plasma substitutes can be used in

emergency treatment of shock, albumin has a prolonged intravascular half-life. When blood volume deficit is the result of hemorrhage, compatible red blood cells or whole blood should be administered as quickly as possible.

5 **Hypoalbuminemia**

[0080] Hypoalbuminemia is another possible indication for use of albumin purified and made available by the method of the current invention, 25% Solution, Buminat 25%. Hypoalbuminemia can result from one or more of the following: Inadequate production (malnutrition, burns, major injury, infections, etc.); Excessive
10 catabolism (burns, major injury, pancreatitis, etc.); Loss from the body (hemorrhage, excessive renal excretion, burn exudates, etc.); and Redistribution within the body (major surgery, various inflammatory conditions, etc.).

[0081] When albumin deficit is the result of excessive protein loss, the effect of administration of albumin will be temporary unless the underlying disorder is
15 reversed. In most cases, increased nutritional replacement of amino acids and/or protein with concurrent treatment of the underlying disorder will restore normal plasma albumin levels more effectively than albumin solutions. Occasionally hypoalbuminemia accompanying severe injuries, infections or pancreatitis cannot be quickly reversed and nutritional supplements may fail to restore serum albumin levels.
20 In these cases, albumin (Human), 25% Solution, Buminat 25% might be a useful therapeutic adjunct.

Burns

[0082] An optimum regimen for the use of albumin, electrolytes and fluid in
25 the early treatment of burns has not been established, however, in conjunction with appropriate crystalloid therapy, Albumin (Human), 25% Solution, Buminat 25% may be indicated for treatment of oncotic deficits after the initial 24 hour period following extensive burns and to replace the protein loss which accompanies any severe burn.

30 **Adult Respiratory Distress Syndrome (ARDS)**

[0083] A characteristic of ARDS is a hypoproteinemic state which may be causally related to the interstitial pulmonary edema. Although uncertainty exists concerning the precise indication of albumin infusion in these patients, if there is a

pulmonary overload accompanied by hypoalbuminemia, 25% albumin solution may have a therapeutic effect when used with a diuretic.

Nephrosis

- 5 [0084] Albumin (Human), 25% Solution may be a useful aid in treating edema in patients with severe nephrosis who are receiving steroids and/or diuretics.

Cardiopulmonary Bypass Surgery

- [0085] Albumin (Human), 25% Solution, Buminate 25% has been recommended prior
10 to or during cardiopulmonary bypass surgery, although no clear data exist indicating its advantage over crystalloid solutions.

Hemolytic Disease of the Newborn (HDN)

- [0086] Albumin (Human), 25% Solution, Buminate 25% may be administered in an
15 attempt to bind and detoxify unconjugated bilirubin in infants with severe HDN.
[0087] It is also possible to use the albumin purified by means of the current invention as an excipient for the delivery of pharmaceuticals.

20 CRYSTAL SCREENING EXPERIMENTS

- [0088] The hanging drop screens are made in boxes with 24 wells divided in 4 rows (A, B, C, D) and 6 columns. The screens are presented in the preliminary report only as lists of the reagents as follows. A brief comment to the results is provided. In
25 the final report the results are provided in tables with complete details similar to the following example tables.

Microscopy and Tables

- [0089] The sample evaluations by microscopy are made in the beginning of
30 experiments with 2-3 days frequency and later on once a week. The microscopy observations in the tables are in abbreviated form using the following letters:

N = no precipitation or other phase separation

C = Some crystals present

CC = A significant amount of crystals present

A = amorphous precipitate, cloud of non-transparent particles looking like cloud or brownish smoke, size of the particles is near the lowest limit of separation power of light microscope

AA = A significant amount of amorphous precipitate

5 L = liquid phase separation, spherical transparent droplets, looking like oil in water

LL = A significant liquid separation

G = gel lumps, irregular glassy transparent particles of several micrometers in diameter

10 GG = A significant amount of gel

X = contaminated or dried drop, discontinued experiment

Table 11.

Reverse temperature effect with amorphous precipitate. Precipitates increases at higher temperature under microscopy. Crystals were very temperature sensitive, they dissolve at higher temperature.

Start date (d,m,y): 17.8.2001 Sample: GTC hSA: labeled 7F-5AC Drop: 8 µl sample + 2 µl reagent Temperatures: + 25 °C or + 4 °C Initial protein concentration: 11.7 mg/ml Final protein concentration: 58 mg/ml Buffer: 0.05 M K-Na-phosphate pH 7.4		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents	3 d +25°C	3d +4 °C	8d, +4 °C	27d, +4 °C
A1	17% PEG 3350 0.08% decanol	N	N	L, G	N
A2	18% PEG 3350 0.08% decanol	N	N	L	N
A3	19% PEG 3350 0.08% decanol	N	N	C	CC
A4	22% PEG 3350 0.08% decanol	N	N	L, G	N
A5	25% PEG 3350 0.08% decanol	N	N	G	N
A6	30% PEG 3350 0.08% decanol	AA	A, GG	G	GG
B1	17% PEG 3350 0.36% decanol	N	N	N	N
B2	18% PEG 3350 0.36% decanol	N	N	N	N
B3	19% PEG 3350 0.36% decanol	N	N	N	N
B4	22% PEG 3350 0.36% decanol	N	N	A	N
B5	25% PEG 3350 0.36% decanol	N	L, GG	G	N
B6	30% PEG 3350 0.36% decanol	AA	A	L, G	GG, LL
C1	1.5 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C2	1.65M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C3	1.8 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C4	2.1 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C5	2.4 M (NH₄)₂SO₄ 0.08% decanol	G	A, GG	C, A	C, L
C6	2.7 M (NH₄)₂SO₄ 0.08% decanol	GG	CC, G Figure 14	CC, G	CC, G
D1	1.5 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	N	N	N
D2	1.65M (NH ₄) ₂ SO ₄ 0.36% decanol	N	N	N	N
D3	1.8 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	N	N	N
D4	2.1 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	A	N	N
D5	2.4 M (NH₄)₂SO₄ 0.36% decanol	AA	C, G	L	LL
D6	2.7 M (NH₄)₂SO₄ 0.36% decanol	L, A, GG	CC, G	C, G	CC, G

- 5 **MCS 23 AAT , Sample: GTC hSA: labeled 7F-5AC; PEG 3350 or (NH₄)₂SO₄ buffered with 0.05 M K-Na-phosphate pH 7.4 effect of decanol additive.** Row A: 500 µl of PEG 3350 17, 18, 19, 22, 25 or 30% in 0.05 M K-Na-phosphate pH 7.4; add 10 µl 4% decanol to each 500 µl of A reagents to get final 0.08% decanol. Row B: like row A, but add 50 µl 4% decanol to each 500 µl of A reagents to get final 0.36 %
- 10 decanol. Row C: 500 µl of (NH₄)₂SO₄ 1.5, 1.65, 1.8, 2.1, 2.4 or 2.7 M in 0.05 M K-Na-phosphate pH 7.4; add 10 µl 4% decanol to each 500 µl of A reagents to get final

0.08% decanol. Row D: like row C, but add 50 μ l 4% decanol to each 500 μ l of A reagents to get final 0.36 % decanol.

- Results:** Crystals of high quality (Figure 14) were produced with 2.4M and 2.7M ammonium sulfate-decanol combinations. Crystals of a different habit were produced with 19% PEG, 0.08% decanol. Amorphous or gel precipitates were also produced with both reagents. Crystallization is very critically related to the reagent concentration and temperature.

Table 12.

Start date (d,m,y): 17.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: Sigma A-9511					
Drop: 2 µl sample + 2 µl reagent					
Temperatures: + 25 °C or + 7 °C					
Initial protein concentration: 55 mg/ml Final protein concentration: 110 mg/ml Buffer: 0.05 M K-Na-phosphate pH 7					
well	Reagents	3 d +25°C	3d + 7°C	8d, +7°C	27d, +7 °C
A1	17% PEG 3350 0.08% decanol	N	N	G	N
A2	18% PEG 3350 0.08% decanol	N	N	L	A
A3	19% PEG 3350 0.08% decanol	N	N	A	N
A4	22% PEG 3350 0.08% decanol	N	N	A	N
A5	25% PEG 3350 0.08% decanol	N	N	A	N
A6	30% PEG 3350 0.08% decanol	AA	AA	A	AA
B1	17% PEG 3350 0.36% decanol	N	N	N	N
B2	18% PEG 3350 0.36% decanol	N	N	N	N
B3	19% PEG 3350 0.36% decanol	N	N	N	N
B4	22% PEG 3350 0.36% decanol	N	N	A	N
B5	25% PEG 3350 0.36% decanol	N	N	N	N
B6	30% PEG 3350 0.36% decanol	N	N	L, G	GG
C1	1.5 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C2	1.65M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C3	1.8 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	N	N	N
C4	2.1 M (NH ₄) ₂ SO ₄ 0.08% decanol	N	A	A	N
C5	2.4 M (NH ₄) ₂ SO ₄ 0.08% decanol	GG	GG	GG	LL, AA
C6	2.7 M (NH ₄) ₂ SO ₄ 0.08% decanol	GG	GG	GG	GG
D1	1.5 M (NH ₄) ₂ SO ₄ 0.36% decanol	GG	GG	C	C
D2	1.65M (NH ₄) ₂ SO ₄ 0.36% decanol	N	N	N	N
D3	1.8 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	N	N	N
D4	2.1 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	A	N	N
D5	2.4 M (NH ₄) ₂ SO ₄ 0.36% decanol	N	A	L	L,A,G
D6	2.7 M (NH ₄) ₂ SO ₄ 0.36% decanol	LL, G	LL,GG	GG	GG

- 10 **Table 12 above, MCS 22 AAS , Sample: Sigma hSA, A-9511**
PEG 3350 or (NH₄)₂SO₄ buffered with 0.05 M K-Na-phosphate pH 7.4
effect of decanol additive Similar screen to table 11.

Results: Sigma hSA did not crystallize as well as GTC hSA 7F-5AC. Only one sample in 1.5 M (NH₄)₂SO₄, 0.36 % decanol produced high quality crystals.

Table 13. Reverse temperature effect with amorphous precipitate. precipitates increase at higher temperature under microscopy. Crystals were very temperature sensitive, they dissolve at higher temperature.

Box code: MCS 22AT Start date (d,m,y): 17.8.2001 Sample: GTC hSA: labeled 7F-5AC Drop: 8 µl sample + 2 µl reagent Temperatures: + 25 °C or + 7 °C Initial protein concentration: 11.7 mg/ml Final protein concentration: 58 mg/ml Buffer: 0.05 M K-Na-phosphate pH 7.4		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents	1d +25°C	4d + 25 °C	30d, +7°C	d, °C
A1	17% PEG 3350	N	N	N	
A2	18% PEG 3350	N	N	N	
A3	19% PEG 3350	N	N	N	
A4	22% PEG 3350	N	N	A	
A5	25% PEG 3350	N	N	N	
A6	30% PEG 3350	LL	LL	A,G	
B1	17% PEG 3350 0.4% caprylic acid	N	N	A	
B2	18% PEG 3350 0.4% caprylic acid	N	N	A	
B3	19% PEG 3350 0.4% caprylic acid	N	N	A	
B4	22% PEG 3350 0.4% caprylic acid	N	N	N	
B5	25% PEG 3350 0.4% caprylic acid	N	N	A,L	
B6	30% PEG 3350 0.4% caprylic acid	LL	LL	A,L	
C1	1.5 M (NH ₄) ₂ SO ₄	N	N	N	
C2	1.65M (NH ₄) ₂ SO ₄	N	N	N	
C3	1.8 M (NH ₄) ₂ SO ₄	N	N	N	
C4	2.1 M (NH ₄) ₂ SO ₄	N	N	A	
C5	2.4 M (NH ₄) ₂ SO ₄	A	N	A,G	
C6	2.7 M (NH ₄) ₂ SO ₄	GG	C,G	A,G	
D1	1.5 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D2	1.65M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D3	1.8 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D4	2.1 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	A	
D5	2.4 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	LL,GG	A	
D6	2.7 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	L,G	LL,GG	A	

For table 13 MCS 22 AT, Sample: GTC hSA: labeled 7F-5AC

- 5 PEG 3350 or (NH₄)₂SO₄ buffered with 0.05 M K-Na-phosphate pH 7.4 effect of caprylic acid additive.

Results: Unstable crystals were produced in only 2.7 M (NH₄)₂SO₄ without caprylic acid.

Table 14.

Start date (d,m,y): 17.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: Sigma A-9511					
Drop: 2 µl sample + 2 µl reagent					
Temperatures: + 25 °C or + 7 °C					
Initial protein concentration: 55 mg/ml Final protein concentration: 110 mg/ml Buffer: 0.05 M K-Na-phosphate pH 7.4					
well	Reagents	1 d +25°C	4d +25 °C	30d, +7 °C	d, °C
A1	17% PEG 3350	N	N	A,G	
A2	18% PEG 3350	N	N	N	
A3	19% PEG 3350	N	X	X	
A4	22% PEG 3350	N	X	X	
A5	25% PEG 3350	N	X	X	
A6	30% PEG 3350	GG	AA	X	
B1	17% PEG 3350 0.4% caprylic acid	N	N	A,G	
B2	18% PEG 3350 0.4% caprylic acid	N	N	A,G	
B3	19% PEG 3350 0.4% caprylic acid	N	N	A,G	
B4	22% PEG 3350 0.4% caprylic acid	N	N	N	
B5	25% PEG 3350 0.4% caprylic acid	N	N	N	
B6	30% PEG 3350 0.4% caprylic acid	A	A	N	
C1	1.5 M (NH ₄) ₂ SO ₄	N	N	N	
C2	1.65M (NH ₄) ₂ SO ₄	N	N	N	
C3	1.8 M (NH ₄) ₂ SO ₄	N	N	N	
C4	2.1 M (NH ₄) ₂ SO ₄	A	N	A	
C5	2.4 M (NH ₄) ₂ SO ₄	GG	GG	AA	
C6	2.7 M (NH ₄) ₂ SO ₄	GG	GG	AA	
D1	1.5 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D2	1.65M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D3	1.8 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	N	N	N	
D4	2.1 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	A,G	A,G	A,G	
D5	2.4 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	A,G	GG	AA	
D6	2.7 M (NH ₄) ₂ SO ₄ 0.4% caprylic acid	GG	GG	AA	

MCS 22 AT, Sample: Sigma hSA, A-9511

PEG 3350 or (NH₄)₂SO₄ buffered with 0.05 M K-Na-phosphate pH 7.4

effect of caprylic acid additive. Similar screen to the table 3.

- 5 **Results:** No crystals produced. Only precipitates at the higher reagent concentrations.

Table 15.

Start date (d,m,y): 10.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: GTC hSA: labeled 7F-5AC					
Drop: 5 µl sample + 1 µl reagent					
Temperatures + 7 °C					
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffers: 0.1 M Na-K-phosphates pH 5.0 – 7.0					
well	Reagents	number of days (d), temperature (°C)			
		3d, +7°C	8d, +7°C	10d, +7°C	40d, +7°C
A1	1.0 M (NH ₄) ₂ SO ₄ pH 5.0	N	A	A,G	A,G
A2	1.0 M (NH ₄) ₂ SO ₄ pH 5.6	N	N	N	N
A3	1.0M (NH ₄) ₂ SO ₄ pH 5.9	N	N	N	N
A4	1.0 M (NH ₄) ₂ SO ₄ pH 6.2	N	N	N	N
A5	1.0 M (NH ₄) ₂ SO ₄ pH 6.6	N	N	N	N
A6	1.0 M (NH ₄) ₂ SO ₄ pH 7.0	N	N	N	N
B1	1.5 M (NH ₄) ₂ SO ₄ pH 5.0	N	AA,GG	G	A,G
B2	1.5M (NH ₄) ₂ SO ₄ pH 5.6	N	N	A	A
B3	1.5 M (NH ₄) ₂ SO ₄ pH 5.9	N	N	A	A
B4	1.5 M (NH ₄) ₂ SO ₄ pH 6.2	N	N	A	A
B5	1.5 M (NH ₄) ₂ SO ₄ pH 6.6	N	N	A	A
B6	1.5 M (NH ₄) ₂ SO ₄ pH 7.0	N	N	A	A
C1	2.0 M (NH ₄) ₂ SO ₄ pH 5.0	AA	AA	GG	A,G
C2	2.0 M (NH ₄) ₂ SO ₄ pH 5.6	N	AA,G	GG	A
C3	2.0 M (NH₄)₂SO₄ pH 5.9	N	AA, C	GG	A
C4	2.0 M (NH₄)₂SO₄ pH 6.2	AA, C	AA	GG,C	A
C5	2.0 M (NH ₄) ₂ SO ₄ pH 6.6	A	A	CC	A
C6	2.0 M (NH ₄) ₂ SO ₄ pH 7.0	A	A	CC	A
D1	3.0 M (NH ₄) ₂ SO ₄ pH 5.0	AA,L	AA,GG	GG	A,G
D2	3.0 M (NH ₄) ₂ SO ₄ pH 5.6	AA,L	AA,GG	GG	A
D3	3.0 M (NH ₄) ₂ SO ₄ pH 5.9	AA,L	AA,GG	GG	A,G
D4	3.0 M (NH ₄) ₂ SO ₄ pH 6.2	A	AA,GG	GG	A
D5	3.0 M (NH ₄) ₂ SO ₄ pH 6.6	A	AA,GG	GG	A,G
D6	3.0 M (NH ₄) ₂ SO ₄ pH 7.0	AA,L	AA,GG	GG	A,G

MCS16 Sample: GTC hSA: labeled 7F-5AC

Ammonium sulfate buffered with phosphates

4 rows: A 1,0 M, B 1,5 M, C 2,0 M, D 3,0 M

5 6 columns: 0,1 M phosphates pH 5.0 pH 5.6 pH 5.9 pH 6.2 pH 6.6 pH 7.0

Results: Amorphous precipitates above 2M. Some unstable poor quality crystals which disappeared in 40d storage.

Table 16.

Note: Crystals were not stable.

Start date (d,m,y): 10.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: GTC hSA: labeled 7F-5AC					
Drop: 5 µl sample + 1 µl reagent					
Temperatures +7 °C					
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffers: 0.1 M Na-K-phosphates pH 5.0 – 7.0					
well	Reagents	number of days (d), temperature (°C)			
		3d, +7°C	6d, +7°C	10d, +7°C	40d, +7°C
A1	1.0 M sodium sulfate pH 5.0	N	N	N	N
A2	1.0 M sodium sulfate pH 5.6	N	N	N	N
A3	1.0 M sodium sulfate pH 5.9	N	N	N	N
A4	1.0 M sodium sulfate pH 6.2	N	N	N	N
A5	1.0 M sodium sulfate pH 6.6	N	N	N	N
A6	1.0 M sodium sulfate pH 7.0	N	N	N	N
B1	1.5 M sodium sulfate pH 5.0	N	N	AA	A
B2	1.5 M sodium sulfate pH 5.6	N	N	AA	A
B3	1.5 M sodium sulfate pH 5.9	N	N	AA	A
B4	1.5 M sodium sulfate pH 6.2	N	N	AA	A
B5	1.5 M sodium sulfate pH 6.6	N	N	AA	A
B6	1.5 M sodium sulfate pH 7.0	N	N	AA	A
C1	1.75 M sodium sulfate pH 5.0	N	G,C	AA	A
C2	1.75 M sodium sulfate pH 5.6	N	A,G	AA	A
C3	1.75 M sodium sulfate pH 5.9	N	A	AA	A
C4	1.75 M sodium sulfate pH 6.2	N	N	AA	A
C5	1.75 M sodium sulfate pH 6.6	N	N	AA	A
C6	1.75 M sodium sulfate pH 7.0	N	N	AA	A
D1	2.0 M sodium sulfate pH 5.0	AA,L	GG,C	LL,GG	A
D2	2.0 M sodium sulfate pH 5.6	AA,L	GG	LL,GG	A
D3	2.0 M sodium sulfate pH 5.9	AA,L	GG,C	A,GG	A
D4	2.0 M sodium sulfate pH 6.2	AA,L L	GG,L,C	L,GG	G,A
D5	2.0 M sodium sulfate pH 6.6	AA,L L	G,L,C	L,GG	G,A
D6	2.0 M sodium sulfate pH 7.0	A,LL	GG	AA	G,A

MCS17, Sample: GTC hSA: labeled 7F-5AC

Sodium sulfate buffered with phosphates5 4 rows: A 1,0 M, B 1,5 M, C 1.75 M, D 2.0 M Na₂SO₄

6 columns: 0,1 M phosphates pH 5.0 pH 5.6 pH 5.9 pH 6.2 pH 6.6 pH 7.0

Results: Unstable crystals in 1.75 M and 2.0 M Na₂SO₄Precipitation, amorphous and gel in 1.5 –2.0 M Na₂SO₄

Table 17.

Note: Crystals were not stable when moved to room temperature for microscopy.

Start date (d,m,y): 28.8.2001		Microscopy observations			
Sample: GTC hSA: labeled 7F-5AC		C = crystals			
Drop: 5 µl sample + 2 µl reagent		A = amorphous precipitate			
Temperatures +7 °C		L = liquid phase separation, spherical droplets			
Initial protein concentration: 10.3 mg/ml		G = gel, glassy solid irregular particles			
Final protein concentration: 36 mg/ml		N = no phase separations, clear solution			
Buffers: 0.1 M Na-K-phosphates pH 6.6 – 7.8		X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents: 0.36% decanol in all samples	number of days (d), temperature (°C)			
		12d, +7°C	22d, +7°C	28d, +7°C	
A1	1.6 M Na-K-phosphate pH 6.6	L	N	N	
A2	1.6 M Na-K-phosphate pH 7.0	L	N	N	
A3	1.6 M Na-K-phosphate pH 7.2	L	N	N	
A4	1.6 M Na-K-phosphate pH 7.4	L	N	N	
A5	1.6 M Na-K-phosphate pH 7.6	L	N	N	
A6	1.6 M Na-K-phosphate pH 7.8	G	N	N	
B1	1.8 M Na-K-phosphate pH 6.6	L	N	N	
B2	1.8 M Na-K-phosphate pH 7.0	L	N	N	
B3	1.8 M Na-K-phosphate pH 7.2	N	N	N	
B4	1.8 M Na-K-phosphate pH 7.4	N	N	N	
B5	1.8 M Na-K-phosphate pH 7.6	N	N	N	
B6	1.8 M Na-K-phosphate pH 7.8	L,G	N	N	
C1	2.0 M Na-K-phosphate pH 6.6	L	N	N	
C2	2.0 M Na-K-phosphate pH 7.0	L	N	N	
C3	2.0 M Na-K-phosphate pH 7.2	L	N	N	
C4	2.0 M Na-K-phosphate pH 7.4	L	N	N	
C5	2.0 M Na-K-phosphate pH 7.6	L	N	N	
C6	2.0 M Na-K-phosphate pH 7.8	L,G	N	N	
D1	2.2 M Na-K-phosphate pH 6.6	L	N	L	
D2	2.2 M Na-K-phosphate pH 7.0	CC	N	L	
D3	2.2 M Na-K-phosphate pH 7.2	CC	N	L	
D4	2.2 M Na-K-phosphate pH 7.4	CC	N	L	
D5	2.2 M Na-K-phosphate pH 7.6	CC	N	CC,L	
D6	2.2 M Na-K-phosphate pH 7.8	CC	N	CC,L	

MCSA30, Sample: GTC hSA: labeled 7F-5AC

1.6 – 2.2 M K-Na-phosphates pH 6.6 – 7.8, 0.36 % decanol in all drops

- 5 **Results:** Good quality crystals in 2.2 M phosphates pH 7.0 – 7.8. The crystals were very temperature sensitive, they dissolved after microscopy at room temperature and crystallized again in refrigerator.

Table 18.

Notes: Reverse temperature effect; amorphous precipitate increases at higher temperature under microscopy. Crystals were not stable, they dissolved at higher temperature under microscopy.

temperature under microscopy.					
Start date (d,m,y): 10.8.2001		Microscopy observations			
Sample: GTC hSA: labeled 7F-5AC		C = crystals			
Drop: 5 µl sample + 1 µl reagent		A = amorphous precipitate			
temperatures + 7 °C		L = liquid phase separation, spherical droplets			
Initial protein concentration: 12.2 mg/ml		G = gel, glassy solid irregular particles			
Final protein concentration: 73 mg/ml		N = no phase separations, clear solution			
Buffers: Na-K-phosphates pH 4.3 – 6.2 pH		X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents	number of days (d), temperature (°C)			
		3d, +7°C	8d, +7°C	10d,+7°C	40d, +7°C
A1	1.2 M Na-K-phosphate pH 4.3	N	N	N	G,A
A2	1.2 M Na-K-phosphate pH 5.0	N	N	N	N
A3	1.2 M Na-K-phosphate pH 5.3	N	N	N	N
A4	1.2 M Na-K-phosphate pH 5.6	N	N	N	N
A5	1.2 M Na-K-phosphate pH 5.9	N	N	N	N
A6	1.2 M Na-K-phosphate pH 6.2	N	N	N	N
B1	1.6 M Na-K-phosphate pH 4.3	N	A	A	G,A
B2	1.6 M Na-K-phosphate pH 5.0	N	N	A	G,A
B3	1.6 M Na-K-phosphate pH 5.3	N	N	A	A
B4	1.6 M Na-K-phosphate pH 5.6	N	N	N	N
B5	1.6 M Na-K-phosphate pH 5.9	N	N	N	A
B6	1.6 M Na-K-phosphate pH 6.2	N	N	N	A
C1	1.8 M Na-K-phosphate pH 4.3	N	AA,GG	A	A,G
C2	1.8 M Na-K-phosphate pH 5.0	N	AA	A	A,G
C3	1.8 M Na-K-phosphate pH 5.3	N	N	A	A
C4	1.8 M Na-K-phosphate pH 5.6	N	N	A	A
C5	1.8 M Na-K-phosphate pH 5.9	N	N	A	A
C6	1.8 M Na-K-phosphate pH 6.2	N	N	A	A
D1	2.2 M Na-K-phosphate pH 4.3	AA	AA,GG	GG	A,G
D2	2.2 M Na-K-phosphate pH 5.0	N	AA	AA	A,G
D3	2.2 M Na-K-phosphate pH 5.3	N	GG,C	G	A,G
D4	2.2 M Na-K-phosphate pH 5.6	N	N	A	A
D5	2.2 M Na-K-phosphate pH 5.9	N	N	A	A
D6	2.2 M Na-K-phosphate pH 6.2	N	N	A,G	A,G

5

10

Table 19.

Note: reverse temperature effect; amorphous precipitates increase at higher temperature under microscopy. Crystals were not stable, they dissolved at higher temperature under microscopy.

microscopy.

Start date (d,m,y): 10.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: GTC hSA: labeled 7F-5AC					
Drop: 5 µl sample + 1 µl reagent					
Temperatures + 7 °C					
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffers: Na-K-phosphates pH 6.6 – 8.2					
well	Reagents	number of days (d), temperature (°C)			
		3d, +7°C	8d, +7°C	10d, +7°C	40d, +7°C
A1	1.2 M Na-K-phosphate pH 6.6	N	N	N	N
A2	1.2 M Na-K-phosphate pH 7.0	N	N	N	N
A3	1.2 M Na-K-phosphate pH 7.4	N	N	N	N
A4	1.2 M Na-K-phosphate pH 7.7	N	N	N	N
A5	1.2 M Na-K-phosphate pH 8.2	N	N	N	N
A6					
B1	1.6 M Na-K-phosphate pH 6.6	N	N	A	A
B2	1.6 M Na-K-phosphate pH 7.0	N	N	A	A
B3	1.6 M Na-K-phosphate pH 7.4	A	AA,GG	A	A
B4	1.6 M Na-K-phosphate pH 7.7	N	N	N	N
B5	1.6 M Na-K-phosphate pH 8.2	N	N	N	N
B6					
C1	1.8 M Na-K-phosphate pH 6.6	N	N	A	A
C2	1.8 M Na-K-phosphate pH 7.0	N	N	A	A
C3	1.8 M Na-K-phosphate pH 7.4	AA	AA,GG	CC,GG	AA
C4	1.8 M Na-K-phosphate pH 7.7	N	AA	GG	A
C5	1.8 M Na-K-phosphate pH 8.2	N	AA	GG	A
C6					
D1	2.2 M Na-K-phosphate pH 6.6	A	CC,A	GG	G,A
D2	2.2 M Na-K-phosphate pH 7.0	A	CC,G	GG	G,A
D3	2.2 M Na-K-phosphate pH 7.4	AA,L	GG,LL	GG	G,A
D4	2.2 M Na-K-phosphate pH 7.7	AA	AA	GG	AA
D5	2.2 M Na-K-phosphate pH 8.2	AA	AA	GG	AA
D6					

5 **Tables 18 and 19**

MCS 15 /1 and MCS 15 /2, Sample: GTC hSA: labeled 7F-5AC

Phosphates without any other additives

pH 4,3 – 8,2 Na-K-PO₄ concentration 1,2 M – 2,2 M

4 rows: A 1,2M, B 1,6 M, C 1,8 M, D 2,2 M

10 11 columns: pH 4.3(NaH₂PO₄) containing: pH 5.0 pH 5.3 pH 5.6 pH 5.9 pH 6.2 pH 6.6 pH 7.0 pH 7.4 pH 7.7 pH 8.2.

Results: Sharp optimum for precipitate at pH 7.4. Unstable crystals above pH 6.6 and at pH 5.3. Much potential for further study.

Table 20.

Table 20.

Start date (d,m,y): 14.8.2001		Microscopy observations			
Sample: GTC hSA: labeled 7F-5AC		C = crystals			
Drop: 5 µl sample + 1 µl reagent		A = amorphous precipitate			
Temperatures + 25 °C or 7°C		L = liquid phase separation, spherical droplets			
Initial protein concentration: 12.2 mg/ml		G = gel, glassy solid irregular particles			
Final protein concentration: 73 mg/ml		N = no phase separations, clear solution			
Buffers: 0.03 M Na-HEPES pH 7.5 - 7.8		X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents	number of days (d), temperature (°C)			
		6d, +25°C	30d, +7°C		
A1	25% 2-propanol, 20 mM MgCl ₂	N	N		
A2	30% 2-propanol, 20 mM MgCl ₂	G	G,A		
A3	35% 2-propanol, 20 mM MgCl ₂	G	L,A		
A4	1.5% benzyl alcohol, 20 mM MgCl ₂	N	A		
A5	1.5% benzyl alcohol, 50 mM MgCl ₂	N	N		
A6	1.5% benzyl alcohol, 100 mM MgCl ₂	N	N		
B1	25% 2-propanol, 100 mM MgCl ₂	N	N		
B2	30% 2-propanol, 100 mM MgCl ₂	G	G,A		
B3	35% 2-propanol, 100 mM MgCl ₂	L	L,A		
B4	1.5% benzyl alcohol, 200 mM MgCl ₂	N	N		
B5	1.5% benzyl alcohol, 300 mM MgCl ₂	N	N		
B6	1.5% benzyl alcohol, 400 mM MgCl ₂	N	N		
C1	25% 2-propanol, 200 mM MgCl ₂	N	N		
C2	30% 2-propanol, 200 mM MgCl ₂	G	G,A		
C3	35% 2-propanol, 200 mM MgCl ₂	G	G,A		
C4	1.25% benzyl alcohol, 20 mM MgCl ₂	N	N		
C5	1.25% benzyl alcohol, 100 mM MgCl ₂	N	N		
C6	1.25% benzyl alcohol, 300 mM MgCl ₂	N	N		
D1	25% 2-propanol, 300 mM MgCl ₂	N	N		
D2	30% 2-propanol, 300 mM MgCl ₂	N	N		
D3	35% 2-propanol, 300 mM MgCl ₂	N	N		
D4	1.0% benzyl alcohol, 20 mM MgCl ₂	N	N		
D5	1.0% benzyl alcohol, 100 mM MgCl ₂	N	N		
D6	1.0% benzyl alcohol, 300 mM MgCl ₂	N	N		

MCS21, Sample: GTC hSA: labeled 7F-5AC

Reagent combinations with magnesium chloride and containing 2-propanol or benzyl alcohol

- 5 **Results:** Only precipitates with 2-propanol containing samples. No effects with benzyl alcohol.

Table 21.

Start date (d,m,y): 10.8.2001			Microscopy observations			
Sample: GTC hSA: labeled 7F-5AC			C = crystals			
Drop: 5 µl sample + 1 µl reagent			A = amorphous precipitate			
temperatures + 7 °C			L = liquid phase separation, spherical droplets			
Initial protein concentration: 12.2 mg/ml			G = gel, glassy solid irregular particles			
Final protein concentration: 73 mg/ml			N = no phase separations, clear solution			
Buffers: 0.1 M Na-K-phosphates pH 5.0 – 7.0			X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents		number of days (d), temperature (°C)			
			3d, +7°C	4d, +7°C	10d, +7°C	40d, +7°C
A1	1.5 M NaCl	pH 5.0	N	N	N	N
A2	1.5 M NaCl	pH 5.6	N	N	N	N
A3	1.5 M NaCl	pH 5.9	N	N	N	N
A4	1.5 M NaCl	pH 6.2	N	N	N	N
A5	1.5 M NaCl	pH 6.6	N	N	N	N
A6	1.5 M NaCl	pH 7.0	N	N	N	N
B1	2.0 M NaCl	pH 5.0	N	N	N	N
B2	2.0 M NaCl	pH 5.6	N	N	N	N
B3	2.0 M NaCl	pH 5.9	N	N	N	N
B4	2.0 M NaCl	pH 6.2	N	N	N	N
B5	2.0 M NaCl	pH 6.6	N	N	N	N
B6	2.0 M NaCl	pH 7.0	N	N	N	N
C1	3.0 M NaCl	pH 5.0	N	N	N	N
C2	3.0 M NaCl	pH 5.6	N	N	N	N
C3	3.0 M NaCl	pH 5.9	N	N	N	N
C4	3.0 M NaCl	pH 6.2	N	N	N	N
C5	3.0 M NaCl	pH 6.6	N	N	N	N
C6	3.0 M NaCl	pH 7.0	N	N	N	N
D1	4.0 M NaCl	pH 5.0	N	N	N	N
D2	4.0 M NaCl	pH 5.6	N	N	N	N
D3	4.0 M NaCl	pH 5.9	N	N	N	N
D4	4.0 M NaCl	pH 6.2	N	N	N	N
D5	4.0 M NaCl	pH 6.6	N	N	N	N
D6	4.0 M NaCl	pH 7.0	N	N	N	N

Sample: GTC hSA: labeled 7F-5AC

Sodium chloride buffered with phosphates

4 rows: A 1,5 M, B 2.0 M, C 3.0 M, D 4,0 M

5 6 columns: 0,1 M phosphates pH 5.0 pH 5.6 pH 5.9 pH 6.2 pH 6.6 pH 7.0

Results: No precipitates or phase separations

Table 22.

Table 22:

Start date (d,m,y): 10.8.2001			Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: GTC hSA: labeled 7F-5AC						
Drop: 5 µl sample + 1 µl reagent						
Temperature: + 7 °C						
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffers: 0.1 M Na-K-phosphates pH 5.0 – 7.0						
well	Reagents		number of days (d), temperature (°C)			
			3d, +7°C	4d, +7°C	10d, +7°C	40d, +7°C
A1	1.5 M KCl	pH 5.0	N	N	N	N
A2	1.5 M KCl	pH 5.6	N	N	N	N
A3	1.5 M KCl	pH 5.9	N	N	N	N
A4	1.5 M KCl	pH 6.2	N	N	N	N
A5	1.5 M KCl	pH 6.6	N	N	N	N
A6	1.5 M KCl	pH 7.0	N	N	N	N
B1	2.0 M KCl	pH 5.0	N	N	N	N
B2	2.0 M KCl	pH 5.6	N	N	N	N
B3	2.0 M KCl	pH 5.9	N	N	N	N
B4	2.0 M KCl	pH 6.2	N	N	N	N
B5	2.0 M KCl	pH 6.6	N	N	N	N
B6	2.0 M KCl	pH 7.0	N	N	N	N
C1	3.0 M KCl	pH 5.0	N	N	N	N
C2	3.0 M KCl	pH 5.6	N	N	N	N
C3	3.0 M KCl	pH 5.9	N	N	N	N
C4	3.0 M KCl	pH 6.2	N	N	N	N
C5	3.0 M KCl	pH 6.6	N	N	N	N
C6	3.0 M KCl	pH 7.0	N	N	N	N
D1	3.9 M KCl	pH 5.0	N	N	N	N
D2	3.9 M KCl	pH 5.6	N	N	N	N
D3	3.9 M KCl	pH 5.9	N	N	N	N
D4	3.9 M KCl	pH 6.2	N	N	N	G,A
D5	3.9 M KCl	pH 6.6	N	N	N	G,A
D6	3.9 M KCl	pH 7.0	N	N	N	N

Sample: GTC hSA: labeled 7F-5AC**Potassium chloride buffered with phosphates**

4 rows: A 1,5 M, B 2.0 M, C 3.0 M, D 4,0 M

5 6 columns: 0,1 M phosphates pH 5.0 pH 5.6 pH 5.9 pH 6.2 pH 6.6 pH 7.0

Results: Mostly no precipitates or phase separations. Gel precipitates after 40d in 3.9 M KCl pH 6.2-6.6.

Table 23.

Table 23.

Start date (d,m,y): 15.8.2001				Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.	
Sample: GTC hSA: labeled 7F-5AC					
Drop: 5 µl sample + 1 µl reagent					
temperatures +25 °C or +4 °C					
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffers: 0.035M TrisHCl pH 8.0 or 8.4					
well	Reagents			date or number of days (temperature)	
				5d, +25 °C	30d, +4 °C
A1	10% PEG 6000	50mM NH ₄ -acetate	pH 8.0	N	N
A2	10% PEG 6000	100mM NH ₄ -acetate	pH 8.0	N	N
A3	10% PEG 6000	300mM NH ₄ -acetate	pH 8.0	N	N
A4	10% PEG 6000	50mM NH ₄ -acetate	pH 8.4	A,G	N
A5	10% PEG 6000	100mM NH ₄ -acetate	pH 8.4	A,G	A
A6	10% PEG 6000	300mM NH ₄ -acetate	pH 8.4	N	N
B1	15% PEG 6000	50mM NH ₄ -acetate	pH 8.0	N	N
B2	15% PEG 6000	100mM NH ₄ -acetate	pH 8.0	A	N
B3	15% PEG 6000	300mM NH ₄ -acetate	pH 8.0	LL	L,A
B4	15% PEG 6000	50mM NH ₄ -acetate	pH 8.4	A,G	N
B5	15% PEG 6000	100mM NH ₄ -acetate	pH 8.4	A,G	A
B6	15% PEG 6000	300mM NH ₄ -acetate	pH 8.4	N	N
C1	20% PEG 6000	50mM NH ₄ -acetate	pH 8.0	A,L	X
C2	20% PEG 6000	100mM NH ₄ -acetate	pH 8.0	N	A
C3	20% PEG 6000	300mM NH ₄ -acetate	pH 8.0	L	L,A
C4	20% PEG 6000	50mM NH ₄ -acetate	pH 8.4	L	A,G
C5	20% PEG 6000	100mM NH ₄ -acetate	pH 8.4	G	A,G
C6	20% PEG 6000	300mM NH ₄ -acetate	pH 8.4	L	L
D1	25% PEG 6000	50mM NH ₄ -acetate	pH 8.0	LL	L,G
D2	25% PEG 6000	100mM NH ₄ -acetate	pH 8.0	LL	L,G
D3	25% PEG 6000	300mM NH ₄ -acetate	pH 8.0	LL	L,G
D4	25% PEG 6000	50mM NH ₄ -acetate	pH 8.4	LL	A,G
D5	25% PEG 6000	100mM NH ₄ -acetate	pH 8.4	LL	L,G,A
D6	25% PEG 6000	300mM NH ₄ -acetate	pH 8.4	L	L,G

Sample: GTC hSA: labeled 7F-5AC

10 – 25% PEG 6000, 0.05-0.3 M ammonium acetate, 0.035 M Tris-HCl pH 8.0-8.4,

Results: No crystals. Various precipitates in most of the samples.

Table 24.

Table 24.

Start date (d,m,y): 14.8.2001		Microscopy observations C = crystals A = amorphous precipitate L = liquid phase separation, spherical droplets G = gel, glassy solid irregular particles N = no phase separations, clear solution X = experiment failed, discontinued, dried, microbial contamination etc.			
Sample: GTC hSA: labeled 7F-5AC					
Drop: 5 µl sample + 1 µl reagent					
temperatures: + 25 °C or + 4 °C					
Initial protein concentration: 12.2 mg/ml Final protein concentration: 73 mg/ml Buffer: 0.1M phosphate pH 7.4					
well	Reagents	4d, +25°C	10d, +4°C	30d, +4°C	d, °C
A1	10% PEG 400	N	N	A	
A2	10% PEG 600	N	N	N	
A3	10% PEG 1000	N	N	N	
A4	10% PEG 4000	N	N	N	
A5	10% PEG 6000	N	N	A	
A6	10% PEG 20,000	N	N	N	
B1	20% PEG 400	G	A	A	
B2	20% PEG 600	N	N	N	
B3	20% PEG 1000	N	N	N	
B4	20% PEG 4000	N	N	N	
B5	20% PEG 6000	N	N	N	
B6	20% PEG 20 000	N	N	A	
C1	30% PEG 400	N	A	N	
C2	30% PEG 600	N	N	L	
C3	30% PEG 1000	N	A	N	
C4	30% PEG 4000	A,G,L	N	N	
C5	30% PEG 6000	N	N	N	
C6	30% PEG 20 000	N	N	A	
D1	40% PEG 400	N	N	N	
D2	40% PEG 600	L	L	L	
D3	40% PEG 1000	N	N	N	
D4	40% PEG 4000	N	N	N	
D5	40% PEG 6000	L	N	N	
D6	40% PEG 20 000	LL	A,G	A,G	

Sample: GTC hSA: labeled 7F-5AC

PEG of various molecular weights 400 – 20 000, phosphate buffer pH 7.4 in the sample.

- 5 **Results:** No crystals and mostly no precipitates, amorphous forms at the highest concentration of PEG 6000.

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Table 25.

Start date (d,m,y): 15.8.2001				Microscopy observations			
Sample: GTC hSA: labeled 7F-5AC				C = crystals			
Drop: 5 µl sample + 1 µl reagent				A = amorphous precipitate			
Temperatures +25 °C or +4 °C				L = liquid phase separation, spherical droplets			
Initial protein concentration: 12.2 mg/ml				G = gel, glassy solid irregular particles			
Final protein concentration: 73 mg/ml				N = no phase separations, clear solution			
Buffers: 0.1 M K-Na-phosphates pH 4.8 – 8.2				X = experiment failed, discontinued, dried, microbial contamination etc.			
well	Reagents			5d, +25°C	30d, +4°C	d, °C	d, °C
A1	25% PEG 6000	10% 2-propanol	pH4.8	LL	L,G,A		
A2	25% PEG 6000	10% 2-propanol	pH5.3	LL	L,G,A		
A3	25% PEG 6000	10% 2-propanol	pH6.2	LL	L,G,A		
A4	25% PEG 6000	10% 2-propanol	pH7.0	LL	L,G,A		
A5	25% PEG 6000	10% 2-propanol	pH7.4	LL	L,G,A		
A6	25% PEG 6000	10% 2-propanol	pH8.2	L	L,A		
B1	25% PEG 6000	15% 2-propanol	pH4.8	LL	L,G,A		
B2	25% PEG 6000	15% 2-propanol	pH5.3	LL	L,G,A		
B3	25% PEG 6000	15% 2-propanol	pH6.2	LL	L,G,A		
B4	25% PEG 6000	10% 2-propanol	pH7.0	LL	L,G,A		
B5	25% PEG 6000	15% 2-propanol	pH7.4	L	L,G,A		
B6	25% PEG 6000	15% 2-propanol	pH8.2	L	L,G,A		
C1	25% PEG 6000	20% 2-propanol	pH4.8	LL	L,G,A		
C2	25% PEG 6000	20% 2-propanol	pH5.3	LL	L,G,A		
C3	25% PEG 6000	20% 2-propanol	pH6.2	LL	L,G,A		
C4	25% PEG 6000	20% 2-propanol	pH7.0	LL	L,A		
C5	25% PEG 6000	20% 2-propanol	pH7.4	LL	L,A		
C6	25% PEG 6000	20% 2-propanol	pH8.2	L	L,A		
D1	25% PEG 6000	30% 2-propanol	pH4.8	L,G	X		
D2	25% PEG 6000	30% 2-propanol	pH5.3	L	L,G		
D3	25% PEG 6000	30% 2-propanol	pH6.2	LG	L,G,A		
D4	25% PEG 6000	30% 2-propanol	pH7.0	L	L,A		
D5	25% PEG 6000	30% 2-propanol	pH7.4	LG	A,G		
D6	25% PEG 6000	30% 2-propanol	pH8.2	LG	X		

Sample: GTC hSA: labeled 7F-5AC

25 % PEG 6000 and 10-30% 2-propanol buffered with 0.1 M K-Na-phosphates pH 4.8 – 8.2

- 5 row A: 25% PEG 6000 and 10% 2-propanol with buffers pH 4.8, 5.3, 6.2, 7.0, 7.4 and 8.2
- row B: 25% PEG 6000 and 15% 2-propanol with buffers pH 4.8, 5.3, 6.2, 7.0, 7.4 and 8.2
- 10 row C: 25% PEG 6000 and 20% 2-propanol with buffers pH 4.8, 5.3, 6.2, 7.0, 7.4 and 8.2
- row D: 25% PEG 6000 and 30% 2-propanol with buffers pH 4.8, 5.3, 6.2, 7.0, 7.4 and 8.2

Results: Strong liquid phase separation in all samples, gel phase in 30% 2-propanol.

Recombinant Production

[0090] A growing number of recombinant proteins are being developed for therapeutic and diagnostic applications. However, many of these proteins may be difficult or expensive to produce in a functional form and/or in the required quantities using conventional methods. Conventional methods involve inserting the gene responsible for the production of a particular protein into host cells such as bacteria, yeast, or mammalian cells, e.g., COS or CHO cells, and then growing the cells in culture media. The cultured cells then synthesize the desired protein. Traditional bacteria or yeast systems may be unable to produce many complex proteins in a functional form. While mammalian cells can reproduce complex proteins, they are generally difficult and expensive to grow, and often produce only mg/L quantities of protein. In addition, non-secreted proteins are relatively difficult to purify from procaryotic or mammalian cells as they are not secreted into the culture medium.

[0091] In general, the transgenic technology features, a method of making and secreting a protein which is not normally secreted (a non-secreted protein). The method includes expressing the protein from a nucleic acid construct which includes:

- (a) a promoter, e.g., a mammary epithelial specific promoter, e.g., a milk protein promoter;
 - (b) a signal sequence which can direct the secretion of a protein, e.g. a signal sequence from a milk specific protein;
 - (c) optionally, a sequence which encodes a sufficient portion of the amino terminal coding region of a secreted protein, e.g., a protein secreted into milk, to allow secretion, e.g., in the milk of a transgenic mammal, of the non-secreted protein; and
 - (d) a sequence which encodes a non-secreted protein,
- wherein elements (a), (b), optionally (c), and (d) are preferably operatively linked in the order recited.

[0092] In preferred embodiments: elements a, b, c (if present), and d are from the same gene; the elements a, b, c (if present), and d are from two or more genes.

[0093] In preferred embodiments the secretion is into the milk of a transgenic mammal.

[0094] In preferred embodiments: the signal sequence is the β -casein signal sequence; the promoter is the β -casein promoter sequence.

[0095] In preferred embodiments the non-secreted protein-coding sequence: is of human origin; codes for a truncated, nuclear, or a cytoplasmic polypeptide; codes for
5 human serum albumin or other desired protein of interest.

[0096] The practice of the present invention will employ, unless otherwise indicated, conventional techniques of cell biology, cell culture, molecular biology, transgenic biology, microbiology, recombinant DNA, and immunology, which are within the skill of the art. Such techniques are described in the literature. See, for
10 example, *Molecular Cloning A Laboratory Manual*, 2nd Ed., ed. by Sambrook, Fritsch and Maniatis (Cold Spring Harbor Laboratory Press: 1989); *DNA Cloning*, Volumes I and II (D. N. Glover ed., 1985); *Oligonucleotide Synthesis* (M. J. Gait ed., 1984); Mullis et al. U.S. Patent No: 4,683,195; *Nucleic Acid Hybridization* (B. D. Hames & S. J. Higgins eds. 1984); *Transcription And Translation* (B. D. Hames & S. J. Higgins
15 eds. 1984); *Culture Of Animal Cells* (R. I. Freshney, Alan R. Liss, Inc., 1987); *Immobilized Cells And Enzymes* (IRL Press, 1986); B. Perbal, *A Practical Guide To Molecular Cloning* (1984); the treatise, *Methods In Enzymology* (Academic Press, Inc., N.Y.); *Gene Transfer Vectors For Mammalian Cells* (J. H. Miller and M. P. Calos eds., 1987, Cold Spring Harbor Laboratory); *Methods In Enzymology*, Vols. 154 and 155
20 (Wu et al. eds.), *Immunochemical Methods In Cell And Molecular Biology* (Mayer and Walker, eds., Academic Press, London, 1987); *Handbook Of Experimental Immunology*, Volumes I-IV (D. M. Weir and C. C. Blackwell, eds., 1986); *Manipulating the Mouse Embryo*, (Cold Spring Harbor Laboratory Press, Cold Spring Harbor, N.Y., 1986).

25

Milk Specific Promoters

[0097] The transcriptional promoters useful in practicing the present invention are those promoters that are preferentially activated in mammary epithelial cells, including promoters that control the genes encoding milk proteins such as caseins, beta
30 lactoglobulin (Clark et al., (1989) *Bio/Technology* 7: 487-492), whey acid protein (Gorton et al. (1987) *Bio/Technology* 5: 1183-1187), and lactalbumin (Soulier et al., (1992) *FEBS Letts.* 297: 13). Casein promoters may be derived from the alpha, beta, gamma or kappa casein genes of any mammalian species; a preferred promoter is

derived from the goat beta casein gene (DiTullio, (1992) *Bio/Technology* 10:74-77). The milk-specific protein promoter or the promoters that are specifically activated in mammary tissue may be derived from either cDNA or genomic sequences. Preferably, they are genomic in origin.

5 [0098] DNA sequence information is available for all of the mammary gland specific genes listed above, in at least one, and often several organisms. See, e.g., Richards et al., *J. Biol. Chem.* 256, 526-532 (1981) (α -lactalbumin rat); Campbell et al., *Nucleic Acids Res.* 12, 8685-8697 (1984) (rat WAP); Jones et al., *J. Biol. Chem.* 260, 7042-7050 (1985) (rat β -casein); Yu-Lee & Rosen, *J. Biol. Chem.* 258, 10794-10804
 10 (1983) (rat γ -casein); Hall, *Biochem. J.* 242, 735-742 (1987) (α -lactalbumin human); Stewart, *Nucleic Acids Res.* 12, 389 (1984) (bovine α s1 and κ casein cDNAs); Gorodetsky et al., *Gene* 66, 87-96 (1988) (bovine β casein); Alexander et al., *Eur. J. Biochem.* 178, 395-401 (1988) (bovine κ casein); Brignon et al., *FEBS Lett.* 188, 48-55 (1977) (bovine α S2 casein); Jamieson et al., *Gene* 61, 85-90 (1987), Ivanov et al., *Biol.*
 15 *Chem.* Hoppe-Seyler 369, 425-429 (1988), Alexander et al., *Nucleic Acids Res.* 17, 6739 (1989) (bovine β lactoglobulin); Vilotte et al., *Biochimie* 69, 609-620 (1987) (bovine α -lactalbumin). The structure and function of the various milk protein genes are reviewed by Mercier & Vilotte, *J. Dairy Sci.* 76, 3079-3098 (1993) (incorporated by reference in its entirety for all purposes). To the extent that additional sequence data
 20 might be required, sequences flanking the regions already obtained could be readily cloned using the existing sequences as probes. Mammary-gland specific regulatory sequences from different organisms are likewise obtained by screening libraries from such organisms using known cognate nucleotide sequences, or antibodies to cognate proteins as probes.

25

Signal Sequences

[0099] Among the signal sequences that are useful in accordance with this invention are milk-specific signal sequences or other signal sequences which result in the secretion of eukaryotic or prokaryotic proteins. Preferably, the signal sequence is
 30 selected from milk-specific signal sequences, i.e., it is from a gene which encodes a product secreted into milk. Most preferably, the milk-specific signal sequence is related to the milk-specific promoter used in the expression system of this invention. The size of the signal sequence is not critical for this invention. All that is required is

that the sequence be of a sufficient size to effect secretion of the desired recombinant protein, e.g., in the mammary tissue. For example, signal sequences from genes coding for caseins, e.g., alpha, beta, gamma or kappa caseins, beta lactoglobulin, whey acid protein, and lactalbumin are useful in the present invention. The preferred signal
5 sequence is the goat β -casein signal sequence.

[00100] Signal sequences from other secreted proteins, e.g., proteins secreted by liver cells, kidney cell, or pancreatic cells can also be used.

Transgenic Mammals

10 [00101] The DNA constructs of the protein of interest, in this case human serum albumin, are introduced into the germ line of a mammal. For example, one or several copies of the construct may be incorporated into the genome of a mammalian embryo by standard transgenic techniques.

[00102] Any non-human mammal can be usefully employed in this invention.
15 Mammals are defined herein as all animals, excluding humans, that have mammary glands and produce milk. Preferably, mammals that produce large volumes of milk and have long lactating periods are preferred. Preferred mammals are cows, sheep, goats, mice, oxen, camels and pigs. Of course, each of these mammals may not be as effective as the others with respect to any given expression sequence of this invention.
20 For example, a particular milk-specific promoter or signal sequence may be more effective in one mammal than in others. However, one of skill in the art may easily make such choices by following the teachings of this invention.

[00103] Although the foregoing invention has been described in some detail by way of illustration and example for purposes of understanding, it will be apparent to
25 those skilled in the art that certain changes and modifications may be practiced. Therefore, the description and examples should not be construed as limiting the scope of the invention, which is delineated by the appended claims.

[00104] It should also be noted that while albumin is crystallized with various compounds, ethanol and mineral salts including phosphates industrial methods for
30 crystallization with phosphates are not found in the literature. Through the preferred embodiments of the current invention it has now been found that human albumin can be crystallized advantageously with phosphate salts by utilizing in full extent the invented

key process parameters and/or conditions of the current invention. The invented parameters and some variations thereof are listed and described above.

- [00105] Accordingly, it is to be understood that the embodiments of the invention herein providing for crystallized and purified human albumin are merely
- 5 illustrative of the application of the principles of the invention. It will be evident from the foregoing description that changes in the form, methods of use, and applications of the elements of the disclosed may be resorted to without departing from the spirit of the invention, or the scope of the appended claims.

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CLAIMS**What is claimed is:**

1. A crystalline human albumin product comprising at least a portion of the material resulting from a process of:
 - a) concentrating an albumin containing fluid until said fluid has at least 15 grams of albumin per liter of solution;
 - b) adding a first phosphate mixture to said albumin containing fluid until the concentration of said phosphate mixture is in the range of 2.4 – 2.6 molar;
 - 10 c) providing a first filtering of said albumin containing solution so as to form a resultant crystallizing batch solution to remove impurities;
 - d) cooling the resultant filtrate of said crystallizing batch solution to a temperature of at most 15 °C;
 - e) allowing the human albumin in said crystallizing batch solution to crystallize;
 - 15 f) adding more of said first phosphate mixture to said crystallizing batch solution sufficient to achieve a concentration of at most 3.0 molar;
 - g) making a first separation of albumin crystals from any remaining fluid;
 - h) suspending the albumin crystals from said first separation of albumin crystals in a second phosphate mixture wherein said second phosphate mixture has a concentration of 2.7 – 3.0 M;
 - 20 i) heating the crystal suspension from said first separation of albumin crystals up to temperature in the range of 40 – 50 °C in order to dissolve the crystals,
 - j) providing a second filtering to the dissolved crystal suspension from said first separation of albumin crystals;
 - 25 k) cooling the resultant dissolved crystal suspension from said first separation of albumin crystals to a temperature of at most 15 °C; and
 - l) allowing albumin crystals to form from the resultant cooled crystal suspension;
- 30 wherein the application of these specific steps allows the purification and crystallization of human albumin from a given human albumin containing feedstream.

2. The process of claim 1 wherein said first phosphate mixture is comprised of a sodium phosphate salt.
3. The process of claim 1 wherein said first phosphate mixture is a potassium phosphate salt.
- 5 4. The process of claim 1 wherein said first phosphate mixture is comprised of both a sodium and a potassium salt.
5. The process of claim 1 wherein said albumin containing fluid has a concentration of albumin in one liter of solution in a range of 15 – 50 grams.
6. The process of claim 1 wherein the temperature of said first phosphate mixture
10 at the time of addition is in the range of 20 – 30 °C.
7. The process of claim 1 wherein said first phosphate mixture at the time of addition has a pH in the range of pH 6.0 – 6.7.
8. The process of claim 1 wherein said filtrate collected after filtering said crystallizing batch is cooled to a temperature of at most 10 °C.
- 15 9. The process of claim 1 wherein said crystallizing batch solution is allowed to crystallize for at most 12 hours.
10. The process of claim 1 wherein said crystallizing batch solution is allowed to crystallize for at most 24 hours.
11. The process of claim 1 wherein said crystallizing batch solution is allowed to
20 crystallize for at least 24 hours
12. The process of claim 1 wherein said first separation of albumin crystals is accomplished by filtration.
13. The process of claim 1 wherein said first separation of albumin crystals is accomplished by centrifugation.
- 25 14. The process of claim 1 wherein said first separation of albumin crystals is accomplished by gravity.
15. The process of claim 1 wherein said first separation of albumin crystals is accomplished by drying.
17. The process of claim 1 wherein said second phosphate mixture is comprised of
30 a sodium phosphate salt.
18. The process of claim 1 wherein said second phosphate mixture is a potassium phosphate salt.
19. The process of claim 1 wherein said second phosphate mixture is comprised of both a sodium and a potassium salt.

20. The process of claim 1 wherein said dissolved crystal suspension from said first separation of albumin crystals is cooled to a temperature of at most 10 °C.
21. The process of claim 20 wherein the albumin crystals precipitating out of the dissolved crystal suspension are dissolved back into solution again and re-crystallized at least once.
22. The process of claim 1 wherein said albumin containing fluid is previously clarified to remove impurities not in solution.
23. The process of claim 1 wherein said feedstream is milk or other bodily fluid from a transgenic mammal.
24. The process of claim 23 wherein milk from a transgenic mammal is clarified to remove impurities and some milk proteins.
25. The process of claim 23 wherein the level of purity in a given feedstream is at least 10%, that is, wherein human albumin constitutes at least 10% of the total protein of a given solution.
26. The process according to claim 1, wherein the pH of said resultant crystallizing batch solution is 5.6 - 7.8.
27. The process according to claim 1, wherein the pH of said resultant crystallizing batch solution is 6.0 – 6.5.
28. The process according to claim 1, wherein the pH of said resultant crystallizing batch solution is 7.0 – 7.8.
29. The process according to claim 1, wherein said the concentration of said first phosphate mixture has a concentration in the range of 2.2 – 3.0 M.
30. The process of claim 1 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 400 grams per liter of solution.
31. The process of claim 1 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 300 grams per liter of solution.
32. The process of claim 1 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 100 grams per liter of solution.
33. The process of claim 1 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 40 grams per liter of solution.
34. The process of claim 1 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 10 grams per liter of solution.
35. The process of claim 1 wherein said crystalline human albumin product is utilized as an excipient in pharmaceutical preparations.

36. The process of claim 1 wherein said crystalline human albumin product is utilized as an therapeutic agent in a pharmaceutical composition.
37. The process of claim 1 wherein said feedstream is a culture supernatant or bodily fluid derived from a host which expresses recombinant human albumin.
- 5 38. The process of claim 37 wherein said host is a mammalian cell culture.
39. The process of claim 37 wherein said host is a yeast cell culture.
40. The process of claim 37 wherein said host is an insect cell culture.
41. The process of claim 37 wherein said host is a prokaryotic cell culture.
42. The process of claim 1 wherein said crystalline human albumin product is
10 utilized to treat a medical condition.
43. The process of claim 42 wherein said medical condition is selected from the group consisting of:
- a) Edema;
 - b) Hypovolemia;
 - 15 c) Hypoalbuminemia;
 - d) Adult Respiratory Distress Syndrome (ARDS);
 - e) Nephrosis;
 - f) Hemolytic Disease of the Newborn (HDN);
 - g) Severe burn;
 - 20 h) Hypoproteinemia; and,
 - i) Acute pancreatitis,
44. The process of claim 1 wherein said crystalline human albumin product is utilized during cardiopulmonary bypass surgery.
45. A method of producing crystalline human albumin comprising:
- 25 a) concentrating an albumin containing fluid until said fluid has at least 15 grams of albumin per liter of solution;
- b) adding a first phosphate mixture to said albumin containing fluid until the concentration of said phosphate mixture is in the range of 2.4 – 2.6 molar;
- c) providing a first filtering of said albumin containing solution so as to form a
30 resultant crystallizing batch solution to remove impurities;
- d) cooling the resultant filtrate of said crystallizing batch solution to a temperature of at most 15 °C;
- e) allowing the human albumin in said crystallizing batch solution to crystallize;

- 5 f) adding more of said first phosphate mixture to said crystallizing batch solution sufficient to achieve a concentration of at most 3.0 molar;
- g) making a first separation of albumin crystals from any remaining fluid;
- h) suspending the albumin crystals from said first separation of albumin crystals in a second phosphate mixture wherein said second phosphate mixture has a concentration of 2.7 – 3.0 M;
- 10 i) heating the crystal suspension from said first separation of albumin crystals up to temperature in the range of 40 – 50 °C in order to dissolve the crystals,
- j) providing a second filtering to the dissolved crystal suspension from said first separation of albumin crystals;
- 10 k) cooling the resultant dissolved crystal suspension from said first separation of albumin crystals to a temperature of at most 15 °C; and
- l) allowing albumin crystals to form from the resultant cooled crystal suspension;

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wherein the application of these specific steps allows the purification and crystallization of human albumin from a given human albumin containing feedstream.

46. The method of claim 45 wherein said first phosphate mixture is comprised of a sodium phosphate salt.
- 20 47. The method of claim 45 wherein said first phosphate mixture is a potassium phosphate salt.
48. The method of claim 45 wherein said first phosphate mixture is comprised of both a sodium and a potassium salt.
- 25 49. The method of claim 45 wherein said albumin containing fluid has a concentration of albumin in one liter of solution in a range of 15 – 50 grams.
50. The method of claim 45 wherein the temperature of said first phosphate mixture at the time of addition is in the range of 20 – 30 °C.
51. The method of claim 45 wherein said first phosphate mixture at the time of addition has a pH in the range of pH 6.0 – 6.7.
- 30 52. The method of claim 45 wherein said filtrate collected after filtering said crystallizing batch is cooled to a temperature of at most 10 °C.
53. The method of claim 45 wherein said crystallizing batch solution is allowed to crystallize for at most 12 hours.

54. The method of claim 45 wherein said crystallizing batch solution is allowed to crystallize for at most 24 hours.
55. The method of claim 45 wherein said crystallizing batch solution is allowed to crystallize for at least 24 hours
- 5 56. The method of claim 45 wherein said first separation of albumin crystals is accomplished by filtration.
57. The method of claim 45 wherein said first separation of albumin crystals is accomplished by centrifugation.
58. The method of claim 45 wherein said first separation of albumin crystals is accomplished by gravity.
- 10 59. The method of claim 45 wherein said first separation of albumin crystals is accomplished by drying.
60. The method of claim 45 wherein said second phosphate mixture is comprised of a sodium phosphate salt.
- 15 61. The method of claim 45 wherein said second phosphate mixture is a potassium phosphate salt.
62. The method of claim 45 wherein said second phosphate mixture is comprised of both a sodium and a potassium salt.
63. The method of claim 45 wherein said dissolved crystal suspension from said first separation of albumin crystals is cooled to a temperature of at most 10 °C.
- 20 64. The method of claim 63 wherein the albumin crystals precipitating out of the dissolved crystal suspension are dissolved back into solution again and re-crystallized at least once.
65. The method of claim 45 wherein said albumin containing fluid is previously clarified to remove impurities not in solution.
- 25 66. The method of claim 45 wherein said feedstream is milk or other bodily fluid from a transgenic mammal.
67. The method of claim 66 wherein milk from a transgenic mammal is clarified to remove impurities and some milk proteins.
- 30 68. The method of claim 66 wherein the level of purity in a given feedstream is at least 10%, that is, wherein human albumin constitutes at least 10% of the total protein of a given solution.
69. The method according to claim 45, wherein the pH of said resultant crystallizing batch solution is 5.6 - 7.8.

70. The method according to claim 45, wherein the pH of said resultant crystallizing batch solution is 6.0 – 6.5.
71. The method according to claim 45, wherein the pH of said resultant crystallizing batch solution is 7.0 – 7.8.
- 5 72. The method according to claim 45, wherein said the concentration of said first phosphate mixture has a concentration in the range of 2.2 – 3.0 M.
73. The method of claim 45 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 400 grams per liter of solution.
74. The method of claim 45 wherein said albumin containing fluid has an albumin
10 concentration in a range of 3 – 300 grams per liter of solution.
75. The method of claim 45 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 100 grams per liter of solution.
76. The method of claim 45 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 40 grams per liter of solution.
- 15 77. The method of claim 45 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 10 grams per liter of solution.
78. The method of claim 45 wherein said crystalline human albumin product is utilized as an excipient in pharmaceutical preparations.
79. The method of claim 45 wherein said crystalline human albumin product is
20 utilized as an therapeutic agent in a pharmaceutical composition.
80. The method of claim 45 wherein said feedstream is a culture supernatant or bodily fluid from a host which expresses recombinant human albumin.
81. The method of claim 80 wherein said host is a mammalian cell.
82. The method of claim 80 wherein said host is a yeast cell.
- 25 83. The method of claim 80 wherein said host is an insect cell.
84. The method of claim 80 wherein said host is a prokaryotic cell.
85. The method of claim 45 wherein said crystalline human albumin product is utilized to treat a medical condition.
86. The method of claim 85 wherein said medical condition is selected from the
30 group consisting of:
- a) Edema;
 - b) Hypovolemia;
 - c) Hypoalbuminemia;
 - d) Adult Respiratory Distress Syndrome (ARDS);

- e) Nephrosis;
 - f) Hemolytic Disease of the Newborn (HDN);
 - g) Severe burn;
 - h) Hypoproteinemia; and,
 - 5 i) Acute pancreatitis.
87. The method of claim 85 wherein said crystalline human albumin product is utilized during cardiopulmonary bypass surgery.
88. A human albumin product comprising at least a portion of the material resulting from a process of:
- 10 a) concentrating an albumin containing fluid until said fluid has at least 15 grams of albumin per liter of solution;
 - b) adding a first phosphate mixture to said albumin containing fluid until the concentration of said phosphate mixture is in the range of 2.6 – 3.0 molar and the pH is in the range of 6.1 – 6.3;
 - 15 c) cooling the resultant filtrate of said crystallizing batch solution to a temperature of at most 15 °C;
 - d) allowing the human albumin in said crystallizing batch solution to crystallize; and
 - e) separating the albumin crystals from any remaining fluid;
 - 20 wherein the application of these specific steps allows the purification and crystallization of human albumin from a given human albumin containing feedstream.
89. The process of claim 88 wherein said first phosphate mixture is comprised of a sodium phosphate salt.
- 25 90. The process of claim 88 wherein said first phosphate mixture is a potassium phosphate salt.
91. The process of claim 88 wherein said first phosphate mixture is comprised of both a sodium and a potassium salt.
92. The process of claim 88 wherein said albumin containing fluid has a
- 30 concentration of albumin in one liter of solution in a range of 15 – 50 grams.
93. The process of claim 88 wherein the temperature of said first phosphate mixture at the time of addition is in the range of 20 – 30 °C.
94. The process of claim 88 wherein said crystallizing batch solution is allowed to crystallize for at most 12 hours.

95. The process of claim 88 wherein said crystallizing batch solution is allowed to crystallize for at most 24 hours.
96. The process of claim 88 wherein said crystallizing batch solution is allowed to crystallize for at least 24 hours
- 5 97. The process of claim 88 wherein said first separation of albumin crystals is accomplished by filtration.
98. The process of claim 88 wherein said first separation of albumin crystals is accomplished by centrifugation.
99. The process of claim 88 wherein said first separation of albumin crystals is accomplished by gravity.
- 10 100. The process of claim 88 wherein said first separation of albumin crystals is accomplished by drying.
101. The process of claim 88 wherein the albumin crystals precipitating out of the dissolved crystal suspension are dissolved back into solution again and re-
- 15 crystallized at least once.
102. The process of claim 88 wherein said human albumin containing fluid from said feedstream is previously clarified to remove impurities not in solution.
103. The process of claim 88 wherein said feedstream is milk or other bodily fluid from a transgenic mammal.
- 20 104. The process of claim 103 wherein milk from a transgenic mammal is clarified to remove impurities and some milk proteins.
105. The process of claim 103 wherein the level of purity in a given feedstream is at least 10%, that is, wherein human albumin constitutes at least 10% of the total protein of a given solution.
- 25 106. The process of claim 88 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 400 grams per liter of solution.
107. The process of claim 88 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 300 grams per liter of solution.
108. The process of claim 88 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 100 grams per liter of solution.
- 30 109. The process of claim 88 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 40 grams per liter of solution.
110. The process of claim 88 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 10 grams per liter of solution.

111. The process of claim 88 wherein said crystalline human albumin product is utilized as an excipient in pharmaceutical preparations.
112. The process of claim 88 wherein said crystalline human albumin product is utilized as an therapeutic agent in a pharmaceutical composition.
- 5 113. The process of claim 88 wherein said feedstream is or is derived from a culture supernatant or bodily fluid from a host which expresses recombinant human albumin.
114. The process of claim 113 wherein said host is a mammalian cell culture.
115. The process of claim 113 wherein said host is a transgenic mammal.
- 10 116. The process of claim 113 wherein said host is a transgenic avian.
117. The process of claim 113 wherein said host is a transgenic plant.
118. The process of claim 113 wherein said host is a yeast cell culture.
119. The process of claim 113 wherein said host is an insect cell culture.
120. The process of claim 113 wherein said host is a prokaryotic cell culture.
- 15 121. The process of claim 88 wherein said crystalline human albumin product is utilized to treat a medical condition.
122. The process of claim 121 wherein said medical condition is selected from the group consisting of:
- a) Edema;
 - 20 b) Hypovolemia;
 - c) Hypoalbuminemia;
 - d) Adult Respiratory Distress Syndrome (ARDS);
 - e) Nephrosis;
 - f) Hemolytic Disease of the Newborn (HDN);
 - 25 g) Severe burn;
 - h) Hypoproteinemia; and,
 - i) Acute pancreatitis,
123. The process of claim 88 wherein said crystalline human albumin product is utilized during cardiopulmonary bypass surgery.
- 30 124. The process of claim 88, in which the albumin crystals are further purified by one or more recrystallization steps comprising:
- a) suspending the albumin crystals from said first separation of albumin crystals in a second phosphate mixture wherein said second phosphate

mixture has a concentration of 2.7 – 3.0 M and a pH in the range of 6.1 – 6.3;

- b) heating the crystal suspension from said first separation of albumin crystals up to temperature in the range of 40 – 50 °C in order to dissolve the crystals,
 - 5 c) providing a second filtering to the dissolved crystal suspension from said first separation of albumin crystals;
 - d) cooling the resultant dissolved crystal suspension from said first separation of albumin crystals to a temperature of at most 15 °C;
 - e) allowing albumin crystals to form from the resultant cooled crystal
 - 10 suspension; and
 - f) separating the albumin crystals from any remaining fluid;
- wherein the application of these specific steps allows the purification and crystallization of human albumin from a given feedstream.
125. The process of claim 124 wherein said second phosphate mixture is comprised
- 15 of a sodium phosphate salt.
126. The process of claim 124 wherein said second phosphate mixture is a potassium phosphate salt.
127. The process of claim 124 wherein said second phosphate mixture is comprised of both a sodium and a potassium salt.
- 20 128. A human albumin product comprising at least a portion of the material resulting from a process of:
- a) concentrating an albumin containing fluid until said fluid has at least 15 grams of albumin per liter of solution;
- b) adding a first phosphate mixture to said albumin containing fluid until the
- 25 concentration of said phosphate mixture is at most 2.6 molar and the pH is in the range of 6.1 – 6.3;
- c) providing a first filtering of said albumin containing solution so as to form a resultant crystallizing batch solution to remove impurities;
- d) cooling the resultant filtrate of said crystallizing batch solution to a
- 30 temperature of at most 15 °C;
- e) adding more of said first phosphate mixture to said crystallizing batch solution sufficient to achieve a concentration of at most 3.0 molar;
- f) allowing the human albumin in said crystallizing batch solution to crystallize; and

- g) separating the albumin crystals from any remaining fluid;
wherein the application of these specific steps allows the purification and
crystallization of human albumin from a given feedstream.
129. The process of claim 128 wherein said first phosphate mixture is comprised of a
5 sodium phosphate salt.
130. The process of claim 128 wherein said first phosphate mixture is a potassium
phosphate salt.
131. The process of claim 128 wherein said first phosphate mixture is comprised of
both a sodium and a potassium salt.
- 10 132. The process of claim 128 wherein said albumin containing fluid has a
concentration of albumin in one liter of solution in a range of 15 – 50 grams.
133. The process of claim 128 wherein the temperature of said first phosphate
mixture at the time of addition is in the range of 20 – 30 °C.
134. The process of claim 128 wherein said crystallizing batch solution is allowed to
15 crystallize for at most 12 hours.
135. The process of claim 128 wherein said crystallizing batch solution is allowed to
crystallize for at most 24 hours.
136. The process of claim 128 wherein said crystallizing batch solution is allowed to
crystallize for at least 24 hours.
- 20 137. The process of claim 128 wherein said first separation of albumin crystals is
accomplished by filtration.
138. The process of claim 128 wherein said first separation of albumin crystals is
accomplished by centrifugation.
139. The process of claim 128 wherein said first separation of albumin crystals is
25 accomplished by gravity.
140. The process of claim 128 wherein said first separation of albumin crystals is
accomplished by drying.
141. The process of claim 128 wherein the albumin crystals precipitating out of the
dissolved crystal suspension are dissolved back into solution again and re-
30 crystallized at least once.
142. The process of claim 128 wherein said human albumin containing fluid from
said feedstream is previously clarified to remove impurities not in solution.
143. The process of claim 128 wherein said feedstream is milk or other bodily fluid
from a transgenic mammal.

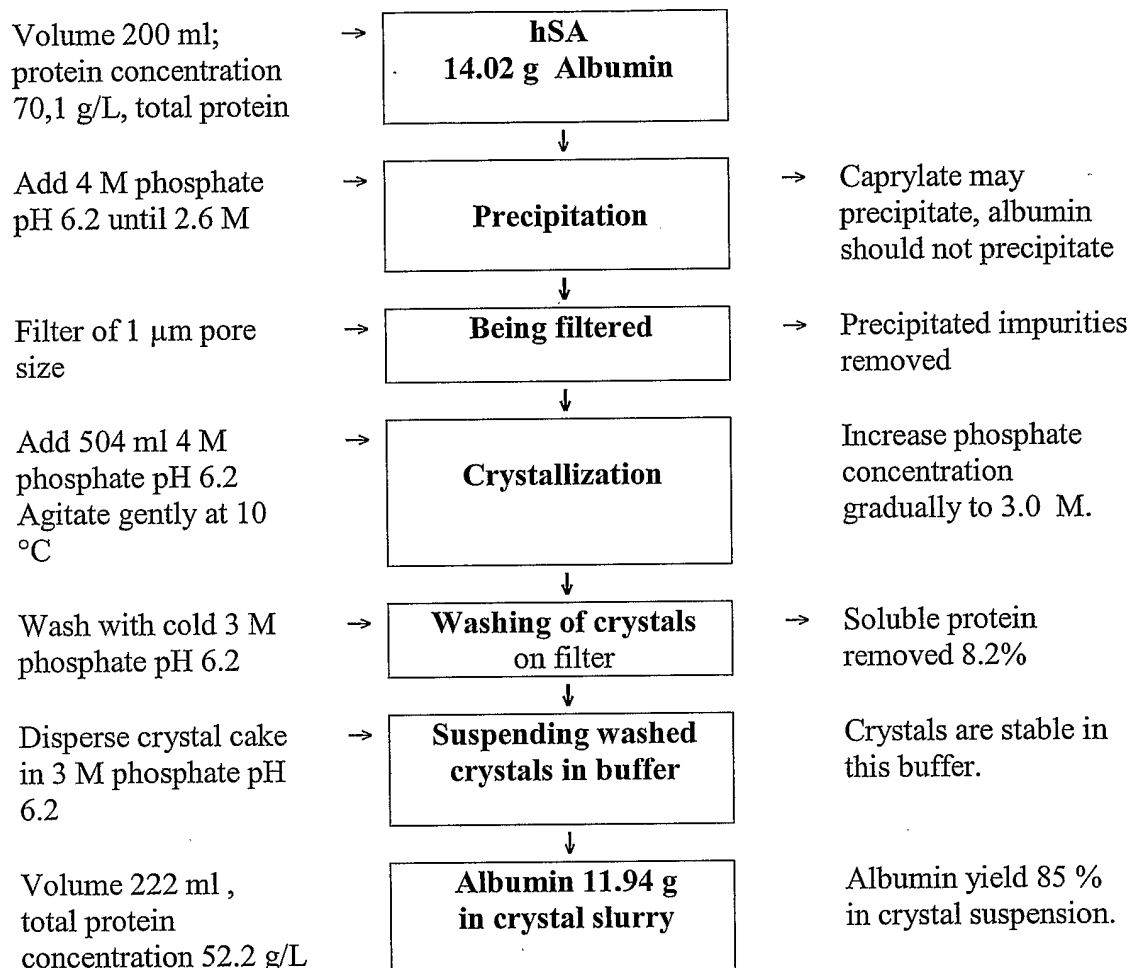
144. The process of claim 103 wherein milk from a transgenic mammal is clarified to remove impurities and some milk proteins.
145. The process of claim 103 wherein the level of purity in a given feedstream is at least 10%, that is, wherein human albumin constitutes at least 10% of the total protein of a given solution.
146. The process of claim 128 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 400 grams per liter of solution.
147. The process of claim 128 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 300 grams per liter of solution.
148. The process of claim 128 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 100 grams per liter of solution.
149. The process of claim 128 wherein said albumin containing fluid has an albumin concentration in a range of 3 – 40 grams per liter of solution.
150. The process of claim 128 wherein said albumin containing fluid has an albumin concentration in a range of 2 – 10 grams per liter of solution.
151. The process of claim 128 wherein said crystalline human albumin product is utilized as an excipient in pharmaceutical preparations.
152. The process of claim 128 wherein said crystalline human albumin product is utilized as an therapeutic agent in a pharmaceutical composition.
153. The process of claim 128 wherein said feedstream is a culture supernatant or bodily fluid from a host which expresses recombinant human albumin.
154. The process of claim 153 wherein said host is a mammalian cell culture.
155. The process of claim 153 wherein said host is a transgenic mammal.
156. The process of claim 153 wherein said host is a transgenic avian.
157. The process of claim 153 wherein said host is a transgenic plant.
158. The process of claim 153 wherein said host is a yeast cell culture.
159. The process of claim 153 wherein said host is an insect cell culture.
160. The process of claim 153 wherein said host is a prokaryotic cell culture.
161. The process of claim 128 wherein said crystalline human albumin product is utilized to treat a medical condition.
162. The process of claim 161 wherein said medical condition is selected from the group consisting of:
- a) Edema;
 - b) Hypovolemia;

- c) Hypoalbuminemia;
 - d) Adult Respiratory Distress Syndrome (ARDS);
 - e) Nephrosis;
 - f) Hemolytic Disease of the Newborn (HDN);
 - 5 g) Severe burn;
 - h) Hypoproteinemia; and,
 - i) Acute pancreatitis,
163. The process of claim 128 wherein said crystalline human albumin product is utilized during cardiopulmonary bypass surgery.
- 10 164. The process of claim 128, in which the albumin crystals are further purified by one or more recrystallization steps comprising:
- g) suspending the albumin crystals from said first separation of albumin crystals in a second phosphate mixture wherein said second phosphate mixture has a concentration of 2.7 – 3.0 M and a pH in the range of 6.1 –
 - 15 6.3;
 - h) heating the crystal suspension from said first separation of albumin crystals up to temperature in the range of 40 – 50 °C in order to dissolve the crystals,
 - i) providing a second filtering to the dissolved crystal suspension from said first separation of albumin crystals;
 - 20 j) cooling the resultant dissolved crystal suspension from said first separation of albumin crystals to a temperature of at most 15 °C;
 - k) allowing albumin crystals to form from the resultant cooled crystal suspension; and
 - l) separating the albumin crystals from any remaining fluid;
 - 25 wherein the application of these specific steps allows the purification and crystallization of human albumin from a given feedstream.
165. The process of claim 164 wherein said second phosphate mixture is comprised of a sodium phosphate salt.
166. The process of claim 164 wherein said second phosphate mixture is a potassium
- 30 phosphate salt.
167. The process of claim 164 wherein said second phosphate mixture is comprised of both a sodium and a potassium salt.

168. The process of claim 1 wherein said human albumin containing feedstream contains a compound bound to a dissolved human serum albumin product, said compound being selected from the group including:
- a) Caprylate;
 - 5 b) A fatty acid; and
 - c) A long chain alcohol.
169. The process of claim 1 wherein said human albumin product is purified to a concentrate said concentrate being in one of a variety of phases said condition being selected from the group consisting of:
- 10 a) Crystalline;
 - b) gel;
 - c) precipitant; and
 - d) droplet
170. The process of claim 88 wherein said human albumin containing feedstream contains a compound bound to a dissolved human serum albumin product, said compound being selected from the group including:
- 15 a) Caprylate;
 - b) A fatty acid; and
 - c) A long chain alcohol.
- 20 171. The process of claim 88 wherein said human albumin product is purified to a concentrate said concentrate being in one of a variety of phases said condition being selected from the group consisting of:
- a) Crystalline;
 - b) gel;
 - 25 c) precipitant; and
 - d) droplet
172. The process of claim 128 wherein said human albumin containing feedstream contains a compound bound to a dissolved human serum albumin product, said compound being selected from the group including:
- 30 a) Caprylate;
 - b) A fatty acid; and
 - c) A long chain alcohol.

173. The process of claim 128 wherein said human albumin product is purified to a concentrate said concentrate being in one of a variety of phases said condition being selected from the group consisting of:
- a) Crystalline;
 - 5 b) gel;
 - c) precipitant; and
 - d) droplet
174. A method of producing crystalline human albumin comprising:
- a) concentrating an albumin containing fluid until said fluid has at least 15
10 grams of albumin per liter of solution;
 - b) adding a sufficient amount of a first chemical modifying agent to said albumin containing fluid;
 - c) providing a first filtering of said albumin containing solution so as to form a resultant crystallizing batch solution to remove impurities;
 - 15 d) cooling the resultant filtrate of said crystallizing batch solution to a temperature of at most 20 °C;
 - e) allowing the human albumin in said crystallizing batch solution to crystallize;
 - f) adding more of said first chemical modifying agent to said crystallizing
20 batch solution sufficient to achieve a concentration of at most 3.0 molar;
 - g) making a first separation of albumin crystals from any remaining fluid;
 - h) suspending the albumin crystals from said first separation of albumin crystals in a second chemical modifying agent;
 - i) heating the crystal suspension from said first separation of albumin crystals
25 up to temperature in the range of 40 – 50 °C in order to dissolve the crystals,
 - j) providing a second filtering to the dissolved crystal suspension from said first separation of albumin crystals;
 - k) cooling the resultant dissolved crystal suspension from said first separation of albumin crystals to a temperature of at most 15 °C; and
 - 30 l) allowing albumin crystals to form from the resultant cooled crystal suspension;
- wherein the application of these specific steps allows the purification and crystallization of human albumin from a given human albumin containing feedstream.

175. The method of claim 174 wherein said first chemical modifying agent is Polyethylene Glycol and said second chemical modifying agent is decanol.
176. The method of claim 174 wherein said first chemical modifying agent is $(\text{NH}_4)_2\text{SO}_4$ and said second chemical modifying agent is decanol.
- 5 177. The method of claim 174 wherein said first chemical modifying agent is Polyethylene Glycol and said second chemical modifying agent is caprylic acid.
178. The method of claim 174 wherein said first chemical modifying agent is $(\text{NH}_4)_2\text{SO}_4$ and said second chemical modifying agent is caprylic acid.
179. The method of claim 174 wherein said first chemical modifying agent is 2-
10 Propanol and said second chemical modifying agent is MgCl_2 .
180. The method of claim 174 wherein said first chemical modifying agent is Benzyl Alcohol and said second chemical modifying agent is MgCl_2 .
181. The method of claim 174 wherein said first chemical modifying agent is
15 Potassium Chloride and said second chemical modifying agent is Potassium Chloride
182. The method of claim 174 wherein said first chemical modifying agent is Polyethylene Glycol and said second chemical modifying agent is Ammonium Acetate.
- 20 183. The method of claim 174 wherein said first chemical modifying agent is Polyethylene Glycol and said second chemical modifying agent is Polyethylene Glycol.
184. The method of claim 174 wherein said first chemical modifying agent is Polyethylene Glycol and said second chemical modifying agent is 2-Propanol.

PROCESS FLOW DIAGRAM FOR CRYSTALLIZATION OF RECOMBINANT HUMAN SERUM ALBUMIN**FIG. 1/14**

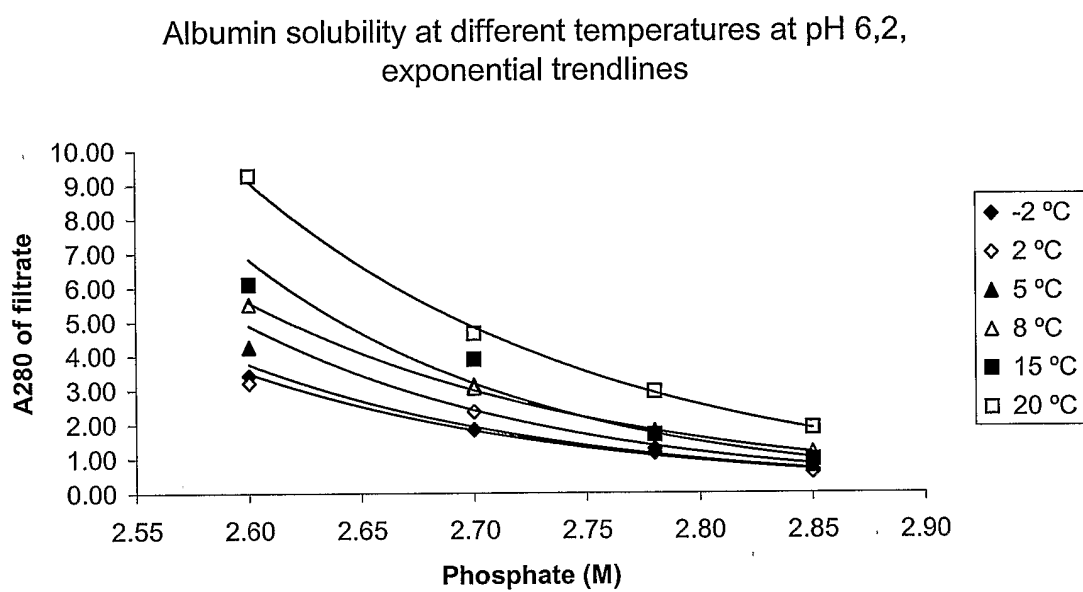


FIG. 2/14

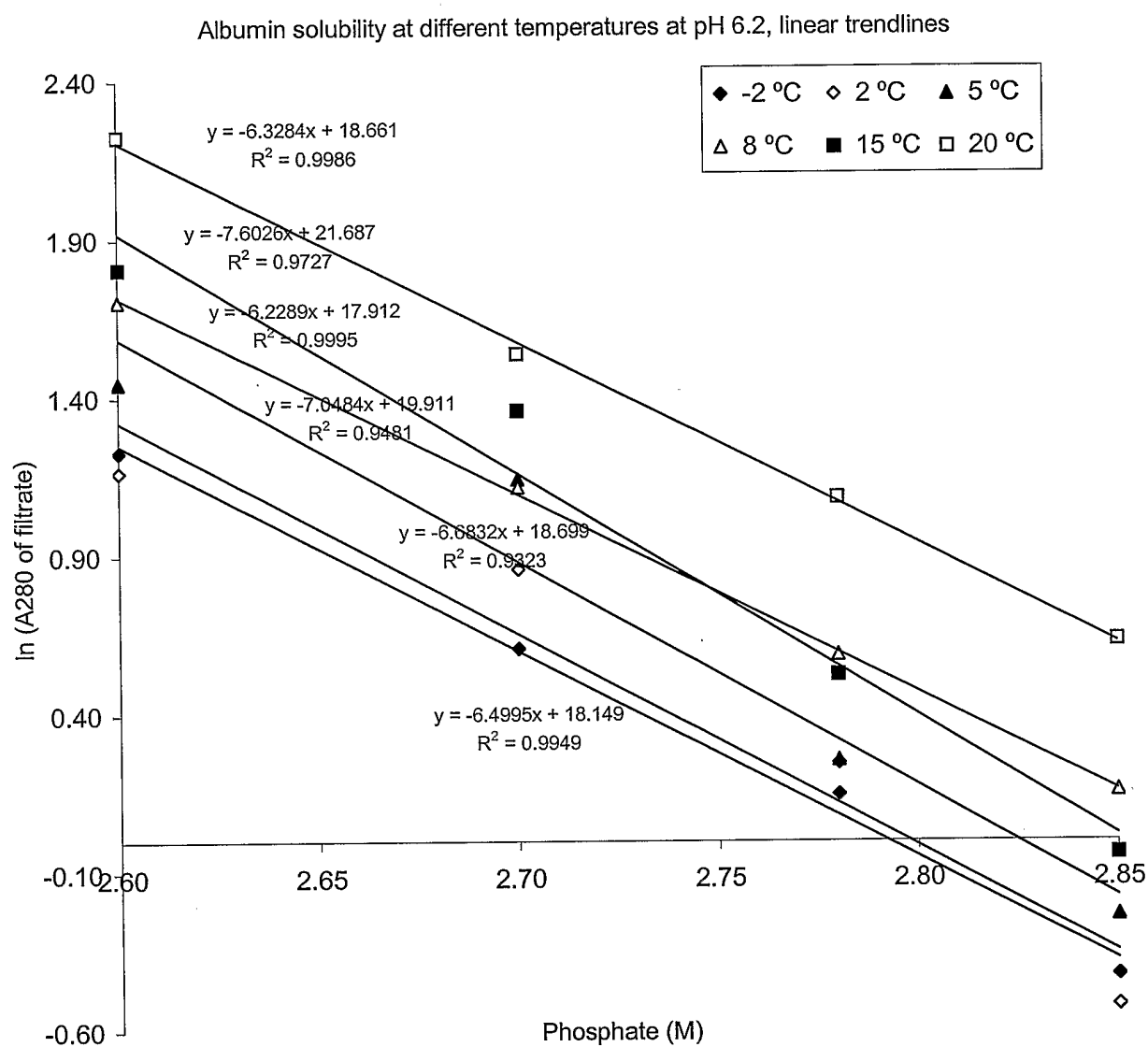
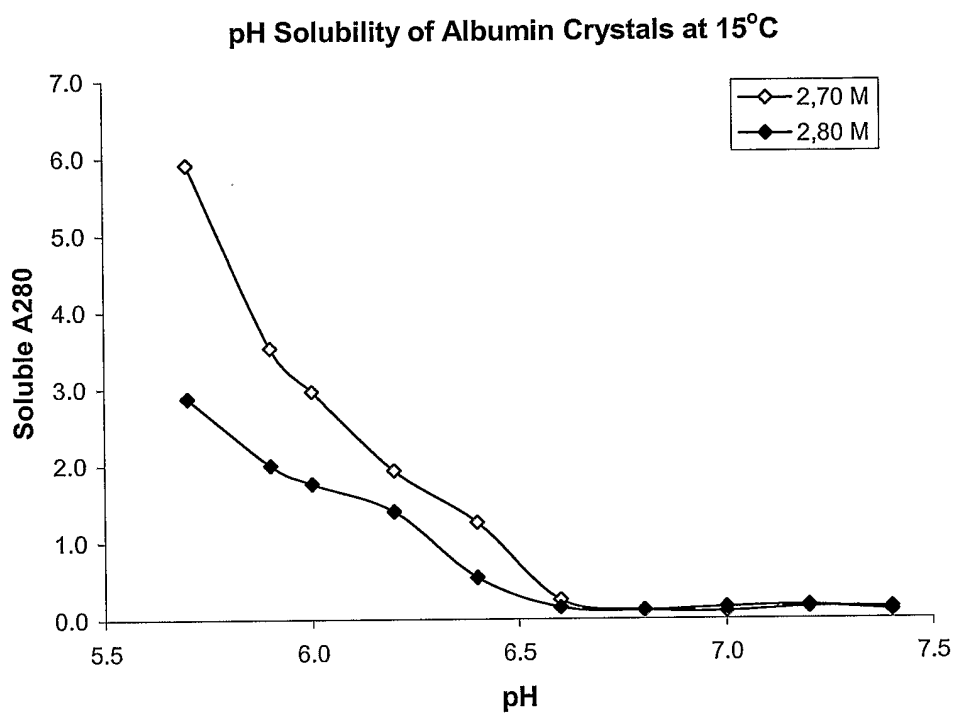


FIG. 3/14

**FIG. 4/14**

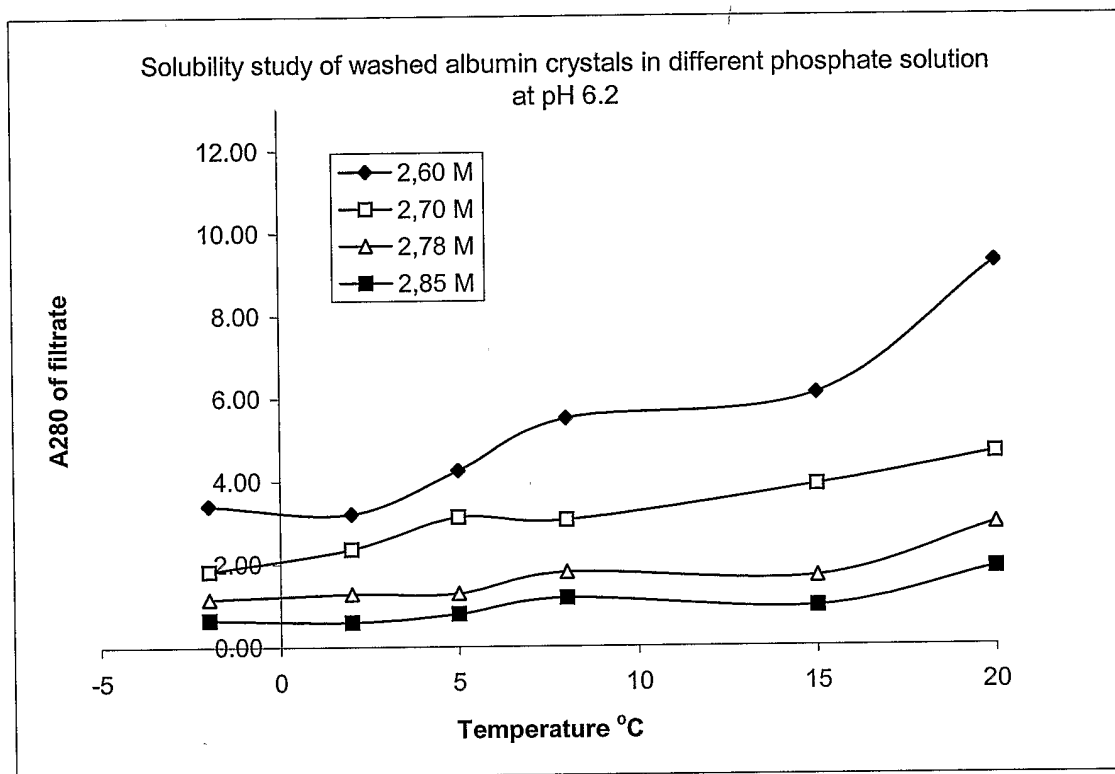


FIG. 5/14

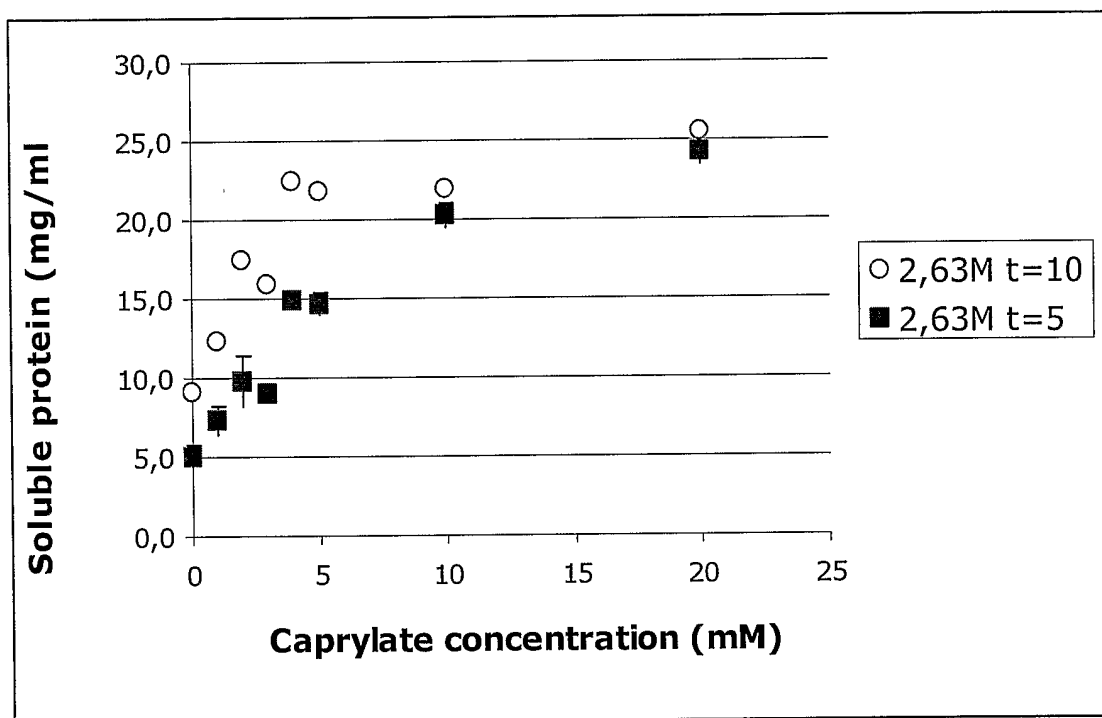


FIG. 6/14

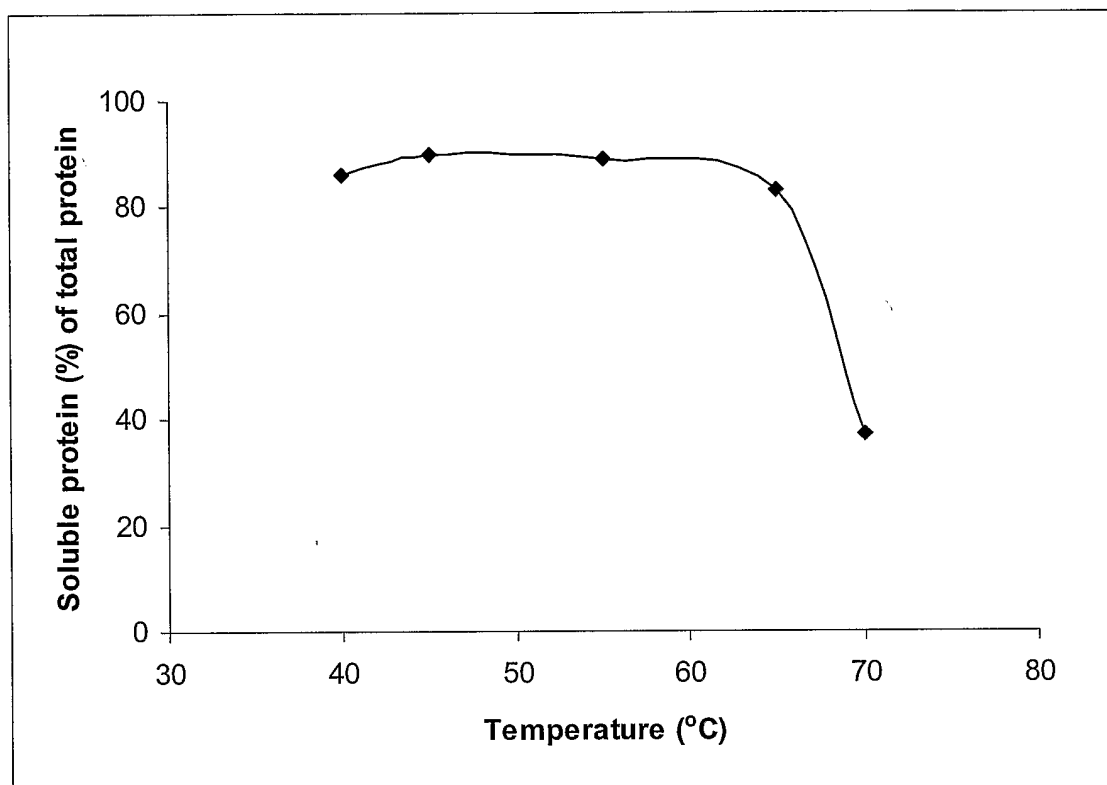


FIG. 7/14

**PROCESS FLOW DIAGRAM FOR PREPARATIVE CRYSTALLIZATION
OF ALBUMIN**

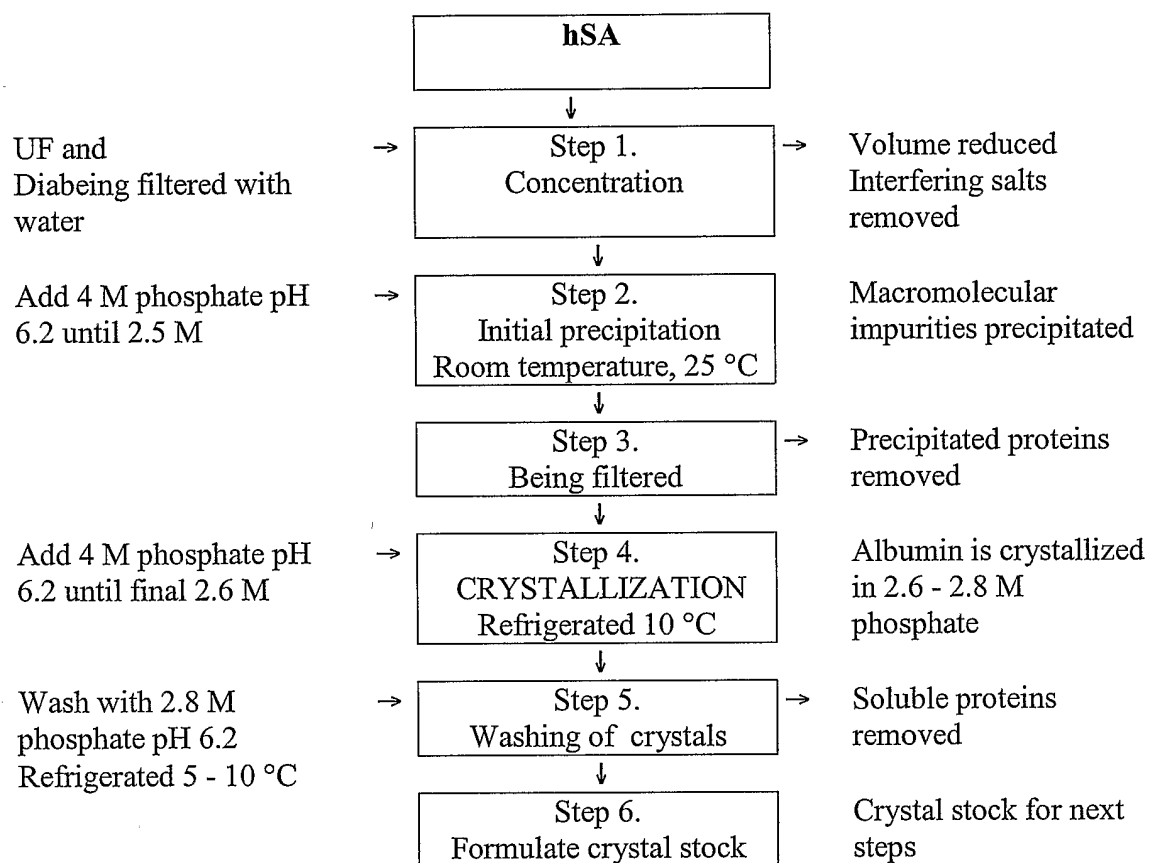


FIG. 8/14

PROCESS FLOW DIAGRAM FOR CRYSTALLIZATION OF RECOMBINANT HUMAN SERUM ALBUMIN

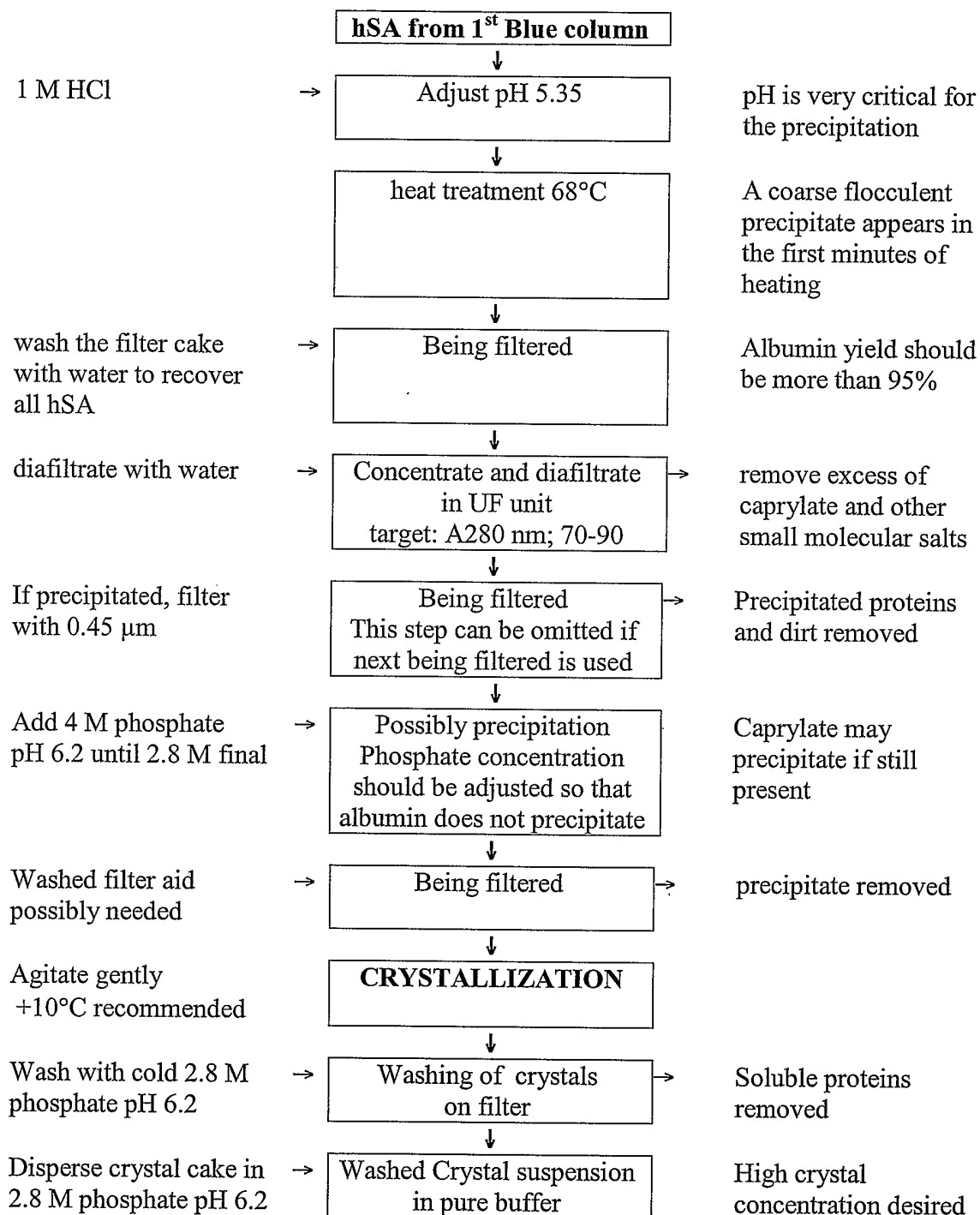
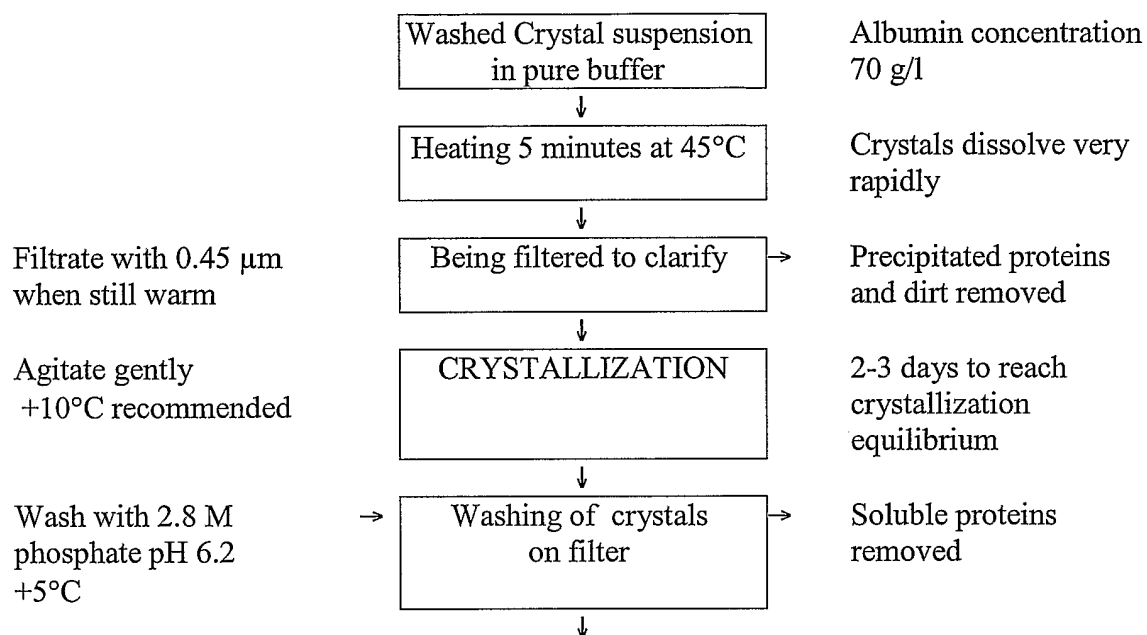


FIG. 9/14

RE-CRYSTALLIZATION OF RECOMBINANT HUMAN SERUM ALBUMIN**FIG. 10/14**

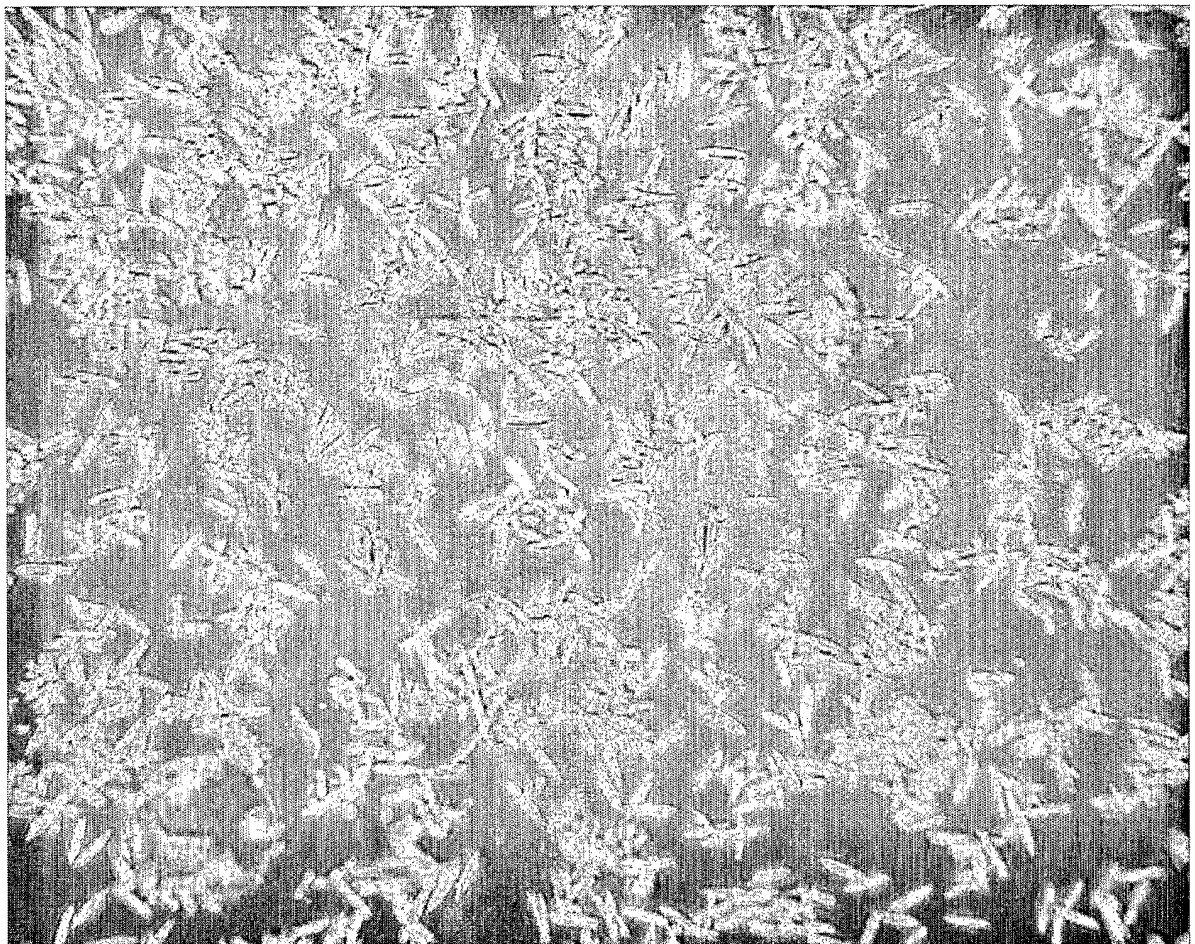


FIG. 11/14



FIG. 12/14



FIG. 13/14

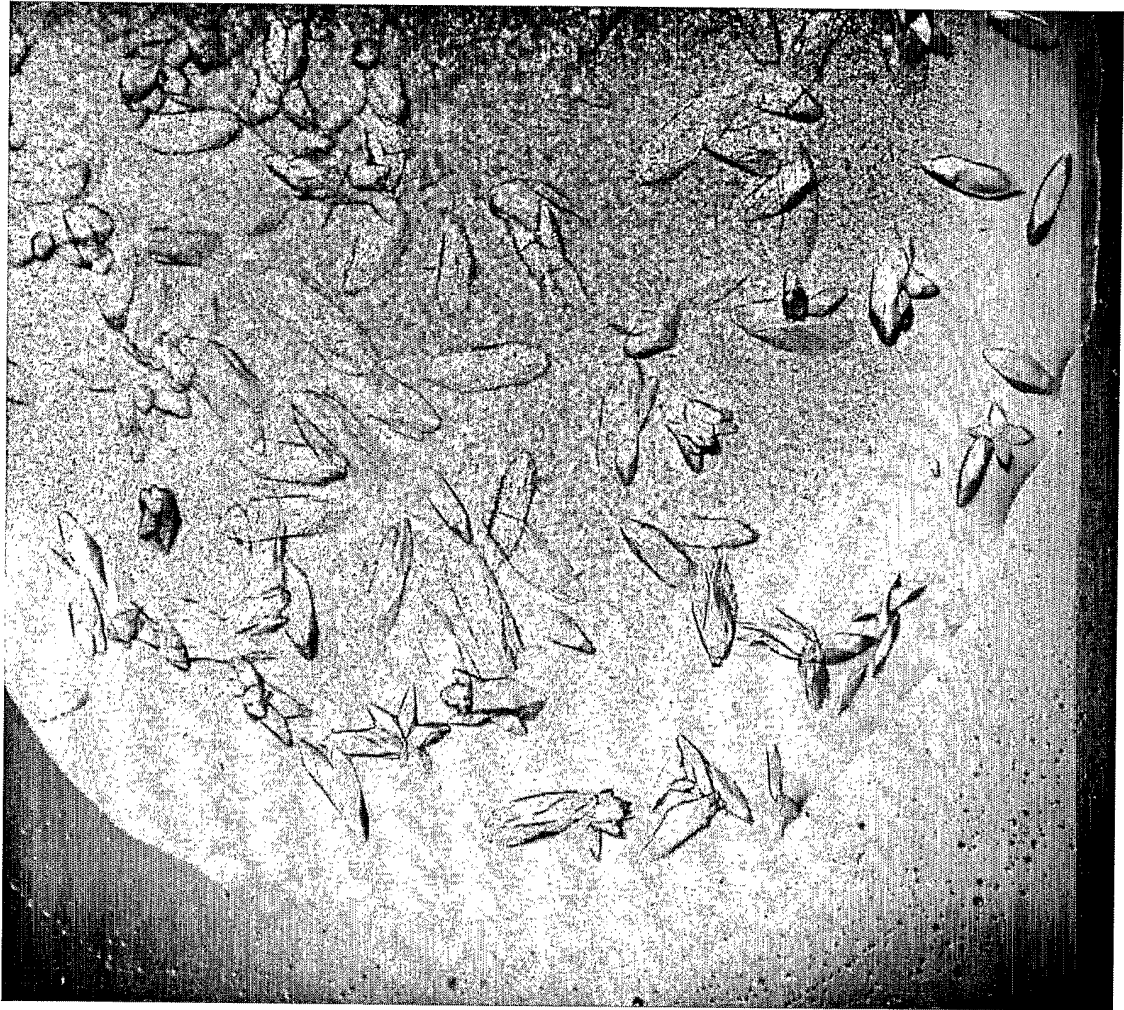


FIG. 14/14