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EP-A1- 0 459 399
WO-A1-2006/005793
US-A- 5 494 651
US-A- 5 690 729
US-A1- 2004 225 050
US-A1- 2010 024 686
US-B1- 6 310 129
US-B2- 7 883 681

DESCRIPTION

FIELD OF THE INVENTION

[0001] The present invention relates to a method for preparing calcium carbonate coated calcium hydroxide particles using calcium hydroxide and carbon dioxide as starting materials. More specifically, the invention relates to the use of dry ice as the source of carbon dioxide in the method for preparing calcium carbonate coated calcium hydroxide particles. The application further relates to an apparatus for carrying out the method.

BACKGROUND OF THE INVENTION

[0002] In the production of acetylene gas, one of the waste by-products is "carbide lime". Canadian Patent Nos. 2,213,086 and 2,296,609, and U.S. Pat. No. 6,310,129 ("the '129 patent") each describe a method for converting raw "carbide lime" waste material into a composition usable as a filler in thermoplastic resin materials. All three patents contain essentially the same disclosure, and the '129 patent will typically be referred to hereinafter, and is representative of all three. As described in the '129 patent, the method comprises screening the raw carbide lime for size reduction, drying the screened carbide lime to obtain a low moisture content and a calcium carbonate content below 25 percent, fine grinding the dried material, and classifying the fine ground particles to separate a fraction of the particulates having a desired particle size, and corresponding lower specific gravity. As described in the '129 patent, this method results in a processed carbide lime composition which comprises 70 to 85 percent by weight calcium hydroxide and 5 to 25 percent by weight calcium carbonate, wherein the calcium carbonate is in the form of surface carbonation on the calcium hydroxide. Similarly, US 6,310,129 teaches a process for the manufacture of carbide lime in a form suitable for use as a filler in thermoplastic materials. In EP 0 459 399 A1 water is added to a methanol suspension of lime (unslaked and/or slaked). Carbon dioxide gas is let through the mixture for a carbonation reaction to produce vaterite calcium carbonate.

[0003] Since the advent of the processed carbide lime filler composition described in the '129 patent, certain benefits and drawbacks of the processed carbide lime composition have been discovered. One very significant beneficial quality discovered is that when the processed carbide lime composition is used as a filler and mixed with a resin to produce resin molded products, the composition imparts sterilizing properties to the molded product. It is known that calcium hydroxide, a main constituent of the carbide lime filler composition, has antibacterial, anti-viral, and anti-fungal properties which can last up to a hundred years. Resin molded products made using the processed carbide lime filler compositions apparently benefit from the calcium hydroxide content and are essentially sterilized. This characteristic makes resin molded products made with the processed carbide lime compositions especially useful in applications where sterilization is important.

[0004] Another benefit imparted to polyvinyl chloride (PVC) resin molded products made with the processed carbide lime filler composition is the ability of calcium hydroxide to neutralize toxic gases from PVC combustion. Calcium hydroxide reacts favourably with toxic chloride gas produced by PVC combustion, resulting in two harmless substances, i.e., water and salt. A complementary quality is that the carbide lime filler composition is also flame retardant due to its high melting point, and exhibits a "hard char" effect after burning. Consequently, coating for electrical wiring, for example, which is made from a resin containing the processed carbide lime filler composition, will not simply decompose when subjected to fire. Instead, the coating will form a hard coating on the wire, thus potentially preventing further hazard.

[0005] As explained in the ' 129 patent, commercial "synthetic" calcium hydroxide has been used, or the use thereof has been investigated, as fillers in resin molding systems. Some limitations and shortcomings of the use of calcium hydroxide as a filler are also described in that patent. The use of calcium carbonate as a filler material in resin molding systems is also known. There are numerous processes known for producing calcium carbonate, as described in, for example, WO 2006/005793 A1 and U.S. Pat. Nos. 6,458,335 and 6,475,459 ("the '459 patent"). The '459 patent, for example, describes a process for producing precipitated calcium carbonate, and explains that the use of precipitated calcium carbonate is growing in various industries, such as paper, plastic, and pharmaceutical industries. The process for preparing calcium carbonate particles described in the '459 patent comprises reacting a starting material containing calcium oxide with carbonate ions in the presence of water to produce calcium carbonate, and recovering the calcium carbonate, characterized in that the formation is carried out directly from calcium oxide to calcium carbonate without intermediate stages. Additionally, the process is carried out under intensive agitation such that the calcium carbonate becomes detached from the surface of the calcium hydroxide. Other methods known in the art for the manufacture of particles of calcium carbonate are described in numerous patent applications listed in the '459 patent.

[0006] Calcium carbonate does not exhibit, and does not impart, the aforementioned anti-microbial or flame retardant properties to resin molded products. Unmodified calcium hydroxide without the calcium carbonate surface coating has not been found to be as useful as the coated calcium hydroxide for application as a filler for resin molded products. This is apparently due to the surface carbonation providing a protective coating on the calcium hydroxide particles which permits the particles to be incorporated into the resin matrix in a manner in which unmodified calcium hydroxide cannot.

[0007] U.S. Pat. No. 7,883,681 ("the '681 patent") discloses the use of calcium carbonate coated calcium hydroxide particles as a filler material in polyvinylchloride (PVC) resin molded products. These particles were found to combine the advantage of the calcium carbonate of being readily incorporated in PVC resin while retaining the advantageous properties of calcium hydroxide including the antimicrobial and flame retardant properties. In particular the '681 patent discloses a method of making calcium carbonate coated calcium hydroxide particles comprising 70-80% by weight of calcium hydroxide and about 5-25% by weight of calcium

carbonate in the form of a coating on the surface of the calcium hydroxide particles.

[0008] The '681 patent teaches a method of making the carbonate coated calcium hydroxide particles comprising suspending the calcium hydroxide particles in the air; carbonating said suspended particles by exposure to carbon dioxide; and carrying out the carbonation reaction for a predetermined period of time to create a surface carbonation on the calcium hydroxide in the proportions described above. The '681 patent describes using a gas, such as air, containing carbon dioxide as the carbon dioxide source, and further describes blowing the gas into a vessel containing the suspended calcium hydroxide particles, to create the surface carbonation on the suspended particles. This is an impinging process. Accordingly, the amount of carbon dioxide is controlled by the length of time of exposure to the gas containing carbon dioxide. In a particular embodiment, the '681 patent teaches the use of the exhaust gas of calcining ovens which contains carbon dioxide as a by product of the processes used to obtain the calcium oxide particles that are then hydrated to produce the calcium hydroxide particles.

[0009] One issue associated with the method of the '681 patent is that there is limited control over the amount of carbon dioxide exposure of the calcium hydroxide particles. As a result it may be difficult to control in an accurate manner, the amount of surface carbonation of the calcium hydroxide particles this may result in poor reproducibility and inconsistent product particles.

[0010] A further issue associated with the method described in the '681 patent is that suspending the calcium hydroxide particles in air requires a high velocity and turbulent conditions in the system. In such a system the calcium hydroxide particles will collide with one another resulting in particles of uneven shape and size. Furthermore, the flow of the carbon dioxide across the suspended particles may results in an uneven coating of calcium carbonate on the surface giving a "comet-like" shape to the coated particles having a rounded side at one face and a tail at the opposite face. Furthermore, the reaction described in the '681 patent occurs in turbulent air streams at high pressure, with carbon dioxide gas impingement causing particle size reduction due to attrition milling. In this method the aspect ratio of the particles is reduced and shear of individual particles may uncover more calcium hydroxide surface which may be detrimental to incorporation into resins.

[0011] Furthermore, the use of the by-product gas of the calcining process as described in the '681 patent may be difficult to control, as the exact amount of carbon dioxide in the by-product gas is not known. Furthermore, this method ties the processes together such that they must be done in tandem and in close proximity which may be limiting depending on the source of materials.

SUMMARY OF THE INVENTION

[0012] In one aspect of the present invention there is provided a method of preparing calcium carbonate (CaCO_3) coated calcium hydroxide ($\text{Ca}(\text{OH})_2$) particles comprising: introducing

calcium hydroxide particles into a reaction vessel; reacting the calcium hydroxide particles with carbon dioxide in the form of dry ice by introducing the dry ice into the reaction vessel and allowing the carbon dioxide to co-mingle with the calcium hydroxide particles and react to form a calcium carbonate coating on the calcium hydroxide particle; wherein the proportion of the calcium hydroxide particles to dry ice is controlled based on measurement of a specific gravity of the reaction product to provide calcium carbonate coated calcium hydroxide particles comprising 70-95% w/w calcium hydroxide and 5-30% w/w calcium carbonate surface coating.

[0013] In an embodiment of the invention the co-mingling of the calcium hydroxide particles with the carbon dioxide is by gravity settling of the particles.

[0014] In an embodiment of the invention the calcium hydroxide particles are about 44 micron. In a further embodiment the calcium hydroxide particles are in the form of a powder. In another embodiment of the invention the calcium hydroxide particles have a size distribution consisting of 95% population of 44 micron particles.

[0015] In a further embodiment the proportion of the dry ice to calcium hydroxide is 31.8 kg (70 lb) of dry ice per 907.2 kg (ton) of calcium hydroxide for a calcium carbonate surface coating of 20 % w/w.

[0016] In a further aspect of the invention there is a provided an apparatus for preparing calcium carbonate coated calcium hydroxide particles comprising:

a reactor;

an inlet for calcium hydroxide particles;

an inlet for dry ice;

a density meter for determining the specific gravity of the reaction product, wherein the specific gravity of the reaction product provides an indication of the percentage of surface carbonation formed by the reaction of the dry ice and calcium hydroxide; and whereby the amount of dry ice introduced into the system can be increased or decreased to provide a product having a selected specific gravity and percentage of surface carbonation.

BRIEF DESCRIPTION OF THE DRAWINGS

[0017] The features of the invention will become more apparent in the following detailed description in which reference is made to the appended drawings wherein:

Figure 1 is a depiction of a reactor system for the reaction of $\text{Ca}(\text{OH})_2$ and dry ice (CO_2) to provide calcium carbonate coated calcium hydroxide particles.

Figure 2a is a graph indicating the mean particle size of the Ca(OH)_2 particles

Figure 2b is a graph indicating the percentage of conversion by volume of the Ca(OH)_2 to CaCO_3 relative to the mass of the calcium hydroxide particles.

Figure 3a is a graph indicating the percentage of conversion by volume of the Ca(OH)_2 to CaCO_3 relative to time.

Figure 3b is a graph indicating the conversion of Ca(OH)_2 to CaCO_3 relative to particle size.

DETAILED DESCRIPTION OF THE INVENTION

[0018] Embodiments of the invention will now be described with reference to the figures.

[0019] As used herein the term "dry ice" refers to carbon dioxide (CO_2) in the solid from which sublimates to produce carbon dioxide gas at room temperature.

[0020] The terms "calcium hydroxide" and " Ca(OH)_2 " are used interchangeably herein. Similarly, the terms "calcium carbonate" and " CaCO_3 " are used interchangeably herein.

[0021] The terms "surface coating" and "coating" as used herein refer to a layer of one material substantially covering the surface of a particle of another material.

[0022] In an embodiment of the invention calcium hydroxide particles are combined with dry ice (CO_2) to provide calcium carbonate (CaCO_3) coated calcium hydroxide (Ca(OH)_2) particles. The dry ice is added in a measured ratio to calcium hydroxide in order to provide a final particle comprising 70-95% w/w calcium hydroxide (core) and 5-30% w/w calcium carbonate surface coating on the core. In a further embodiment the particle comprises 70-85% w/w calcium hydroxide. In a further aspect of the invention the calcium carbonate coating is 15-30% w/w. In still a further embodiment the calcium carbonate coating is 20% w/w.

[0023] In an embodiment of the invention the particle size of the calcium hydroxide particles is approximately 44 micron. In a further embodiment the particles size is less than 100 microns, in a further embodiment the particle size is less than 75 microns. In a further embodiment the mean particle size is 44 microns and the size distribution of the particles consists of 95% population of 44 micron particle as per the industry standard. In another embodiment the particle size may be expressed as a mesh size. In a particular embodiment the particle size is minus 25 micron (600 mesh) in a further embodiment the particle size is minus 45 micron (325 mesh).

[0024] It has been found that to obtain a surface coating of 20% by weight of calcium

carbonate on Ca(OH)_2 particles of 44 microns, 31.8 kg (70 lbs) of dry ice per 907.2 kg (ton) of Ca(OH)_2 is required.

[0025] In a particular embodiment the particle size of the calcium hydroxide particles is 44 micron. In an embodiment of the invention 28137 cm^3 (1 cubic foot (cu ft)) of Ca(OH)_2 in the form of 44 micron dry powder was found to have a weight of 18.1 kg (40 pounds (lbs)). 0.45 kg (one pound) of dry ice is equal to 0.25 m^3 (8.75 Cu Ft) of CO_2 gas at 101 kPa (1 atmosphere) and 21 °C (70 °F). Accordingly, for 20% surface conversion of Ca(OH)_2 to CaCO_3 , 31.8 kg (70 lb) of dry ice per 907.2 kg (ton) of Ca(OH)_2 is required.

[0026] The ratio of calcium hydroxide to carbon dioxide can be varied to provide particles having a different percentage of carbonation. The ratio of the components is based on particle size and weight per dry standard cubic foot compacted per ASTM standards for bulk density of powdered materials. Sublimed carbon dioxide gas produces the carbonate coating on the calcium hydroxide particle surfaces.

[0027] In a further aspect of the invention the calcium hydroxide particles and dry ice particles may be added simultaneously to a reaction vessel and allowed to mix by gravity settling. No further agitation of the calcium hydroxide particles is required, although some agitation or mixing of the reagents is permitted. The dry ice sublimates at room temperature to envelope the calcium hydroxide particles this provides an even coating of calcium carbonate on the calcium hydroxide particles. The minimal agitation of the calcium hydroxide allows for retention of the shape and size of particle as initially added to the reaction. Minimizing the agitation of the starting material also reduces the potential for changes in morphology and impact damage to surface carbonation and early release or exposure of the core calcium hydroxide material.

[0028] In a particular embodiment the calcium hydroxide starting material will contain particles having a narrow size distribution and having a spherical shape. Accordingly, the product calcium carbonate coated calcium hydroxide particles produced by this method will also have a spherical shape and narrow size distribution. It has been found that small particles of dry ice are most effective in providing an even layer of carbonation. In a particular embodiment the dry ice is in the form of small flakes or particles. For example, the dry ice particles will have a size of about 0.425 mm.

[0029] Furthermore, it has been found that the use of dry ice as the source of carbon dioxide combined with the calcium hydroxide in an acquiescent and non-turbulent manner provides a more consistent thickness of calcium carbonate coating around the circumference of the particle minimizing the "comet like" affect that results from blowing carbon dioxide gas over the particles. Furthermore, the minimal agitation required for the mixing of the reagents in this reaction provides a more consistent thickness of coating from one particle to the next. It has also been found that the use of dry ice as the source of carbon dioxide provides a smoother and more consistent product particle shape. This is believed to be due to the fact that the reaction rate can be more readily controlled and the vigorous agitation causing collisions of the

particle is avoided.

[0030] In a further aspect of the invention the reaction of calcium hydroxide may be carried out as a batch reaction or as a continuous flow reaction.

[0031] In a further aspect of the invention there is provided an apparatus for carrying out the method described above. In an embodiment of the invention the calcium hydroxide particles are combined with dry ice in a reaction vessel such as a silo reactor having an inlet for dry ice (CO_2) and an inlet for $\text{Ca}(\text{OH})_2$. The inlet used for the dry ice may be the same or different than the inlet used for $\text{Ca}(\text{OH})_2$. In an embodiment of the invention the $\text{Ca}(\text{OH})_2$ and dry ice will be added to the reaction vessel at the same time either through the same or different inlets and will be allowed to mix via down draft gravity settling. In a further embodiment the inlets may be inlet manifolds. The silo reactor may be further provided with an outlet for removal of the reaction product, the calcium carbonate coated calcium hydroxide particles.

[0032] Figure 1 depicts a particular embodiment of the apparatus. Figure 1 shows a bulk transport delivery (1) for delivering calcium hydroxide particles. A storage silo (2) for storing calcium hydroxide particles and a means for transferring the calcium hydroxide from the transport delivery vehicle to the storage silo, for example, by pneumatic unloading. There is further provided a means for transferring the calcium hydroxide from the storage silo (2) to a reaction silo (3), for example, by aero mechanical conveyor. The reaction silo (3) also has an inlet for carbon dioxide (17), an inlet for calcium hydroxide (18) and an outlet (19) for removing the reaction product. There is further provided a means for transporting the product to the delivery product silo (5). The reaction silo (3) may further have one or more level indicators (10). The reaction silo (3) may also have air filters and/or temperature indicators (12). The reaction silo (3) may further have vibration bin dischargers (13). The discharged reaction product can be moved to delivery product silo (5) which may also have air filters and/or temperature indicators (12).

[0033] Figure 1 also shows a carbon dioxide tank (4) containing liquid carbon dioxide for dry ice plant. The dry ice plant comprises carbon dioxide liquid stored at high pressure and means for converting the liquid carbon dioxide to dry ice, for example, by flow of the liquid carbon dioxide through an injector or sparger mechanism into the reaction silo (3) at reduced pressure.

[0034] The delivery product silo (5) of figure 1 further has one or more density gauges (9) and a temperature gauge (11). The delivery product silo (5) may also have vibration bin dischargers (13). As shown in figure 1 the delivery product silo may have a two way valved product spool bypass, for directing the product to either a bulk transport vehicle (7) or a product bagging line (6). Figure 1 also shows flow control valves (15) for controlling the flow of the calcium hydroxide and carbon dioxide into the reaction silo (3).

[0035] Figure 1 further shows the process controls (8) for controlling the flow valves and monitoring the gauges and indicators. The process controls may be manual or may be

automated.

[0036] In a further aspect the apparatus may comprise a density meter that is used to determine the specific gravity of the particles in the reaction mixture. In a particular embodiment the commercially available Thermo Scientific nuclear density meter is used. It would be understood by a person of skill in the art that other density meters could be used.

[0037] The specific gravity of the starting material calcium hydroxide can be measured and the difference between the specific gravity of the starting material and the product can be determined or estimated. Based on the specific gravity of the particles in the reaction mixture the progress or degree of completion of the reaction can be monitored. The reaction conditions may be adjusted for example by adding more dry ice in order to achieve the desired degree of reaction.

[0038] Adjustment of the reaction conditions may be controlled and optimized manually by an operator observing the density measurements and adjusting the process reaction parameters or may be controlled and optimized by a computer that has been programmed to adjust various reaction parameters on the basis of the density measurements. In a further aspect of the invention the computer is a programmable logic controller.

[0039] It will be further understood that various other meters may be added to the reaction vessel to measure reaction conditions such as moisture or humidity levels, temperature, pressure and the like. These measurements may be used to adjust the reaction conditions such as time, temperature, and/or the proportion of reagents. These processes variables may be monitored and adjusted to achieve consistent quality control of the final product carbonate coated calcium hydroxide particles.

[0040] An embodiment of the invention will now be described by way of a specific example.

[0041] Example 1: Reaction of Calcium Hydroxide with Dry Ice in a Hobart™ Mixer.

[0042] Calcium hydroxide particles of 75 microns or minus 200 mesh were added to a Hobart™ flour mixer with dry ice that was previously crushed to reduce the size of the particles. The dry ice particles having a size range of approximately minus 1680 microns (12 mesh) to plus 1000 microns (18 mesh) size. The calcium hydroxide and carbon dioxide were allowed to react to produce a carbonate coating on the calcium hydroxide particles.

[0043] Table 1 indicates the weight of calcium hydroxide starting material as "weight in" and the weight of the product as "weight out" for a series of reactions 1-8. The change in weight from starting material to product is indicated as well as the percentage difference. The average weight difference from starting material calcium hydroxide to product across all the reactions was 2.08%. The calcium hydroxide starting material was supplied by Sylvette in Putnam (Cameuse) having a moisture content less than 2.5 %. The reactions were split into multiple

batches due to the size of the reactions vessel. The batches are indicated in Table 2 below, for example reaction 2 was carried out in two batches 2a and 2b.

Table 1:

Reaction Number	Weight in (kg)	Weight out (kg)	Weight Difference (kg)	Gain or Loss in percent (%)	Weight Cross check
1	9.517	9.83	0.313	+2.28	9.83
2	9.682	9.9	0.218	+2.252	9.9
3	9.448	9.56	0.112	+1.12	9.56
4	8.935	9.12	0.185	+2.0	9.14
5	8.924	9.21	0.286	+3.0	9.14
6	10.036	10.24	0.204	+2.0	10.24
7	8.92	9.12	0.20	+2.0	9.12
8	8.91	9.12	0.20	+2	9.12

[0044] Table 2 indicates the weight of Ca(OH)_2 and the weight of dry ice used in each batch of each reaction.

Table 2:

Reaction number	Ca(OH)_2 weight (kg)	Dry Ice weight in (kg)
2a	4.5	.92
2b	3.8	.76
3a	4.5	0.92
3b	3.6	0.7
4a	4.5	0.92
4b	3.3	0.66
5a	4.8	0.96
5b	3.0	0.90
6a	4.5	0.92
6b	5.36	1.107
7a	4.5	0.9
7b	3.3	0.66
8a	4.5	0.90
8b	3.3	0.66

[0045] It has been found that the 44 micron calcium hydroxide is approximately 18.1 kg (40 lbs) per 28317 cm^3 (cu ft). Based on the average weight increase of 2.08% measured for the reactions listed above, the average weight per 28317 cm^3 (cu ft) of the product would be

18.521 kg (40.832 lbs) per 28317 cm³ (cu ft).

$(2.08/100) \times 18,1 = 0.377$ kg of gain per 28317 cm³. $[(2.08/100) \times 40 = 0.832$ lbs of gain per cu ft.]

[0046] If the bulk density of CaCO₃ is 19.96 kg (44 lbs) per 28317 cm³ (cu ft.) at specific gravity of 2.7 then surface treated Ca(OH)₂ at a bulk density of 18.521 kg (40.832 lbs) per 28317 cm³ (cu ft) is 2.505 specific gravity.

$(2.7/19.96) \times 18,521 = 2.505$ $[(2.7/44) \times 40.832 = 2.505]$ specific gravity.

[0047] This calculation confirms that the calcium carbonate coating has been converted in approximately the desired proportion to the calcium hydroxide.

[0048] In an embodiment of the invention the thermoplastic or thermoset material is one or more of a thermoplastic or thermoset polymer, a thermoplastic or thermoset elastomer and a thermoplastic or thermoset rubber.

[0049] In a further embodiment of the invention the composition comprising calcium carbonate coated calcium hydroxide particles prepared by the method described above as a filler with a thermoplastic or thermoset material can further comprise one or more of lubricants, stabilizers, antioxidants, plasticizers, pigments, dyes, anti-blocking agents, antistatic agents, flame retardants, impact modifiers, coupling agents, wetting agents, processing aids or fibrous reinforcing agents.

REFERENCES CITED IN THE DESCRIPTION

Cited references

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Patent documents cited in the description

- CA2213086 [0002]

- CA2296609 [0002]
- US6310129B [0002] [0002]
- EP0459399A1 [0002]
- WO2006005793A1 [0005]
- US6458335B [0005]
- US6475459B [0005]
- US7883681B [0007]

Patentkrav

1. Fremgangsmåde til fremstilling af calciumcarbonat (CaCO_3)-belagte calciumhydroxid ($\text{Ca}(\text{OH})_2$)-partikler som et
5 reaktionsprodukt, der omfatter:
indførelse af calciumhydroxid-partikler i en reaktionsbeholder;
reaktion af calciumhydroxid-partiklerne med carbondioxid i form af tør is ved indførelse af tørisen i reaktionsbeholderen og
muliggørelse for carbondioxiden at sammenblende med
10 calciumhydroxid-partiklerne og reagere til frembringelse af en calciumcarbonat-belægning på calciumhydroxid-partiklerne;
hvor forholdet mellem calciumhydroxid-partiklerne og tør is kontrolleres baseret på måling af massefylden af reaktionsproduktet til tilvejebringelse af calciumcarbonat-
15 belagte calciumhydroxid-partikler, der omfatter 70-95 vægt-% calciumhydroxid og 5-30 vægt-% calciumcarbonat-overfladebelægning.
2. Fremgangsmåde ifølge krav 1, hvor sammenblandingen af
20 calciumhydroxid-partiklerne med carbondioxiden sker ved hjælp af tyngdekraftbundfældning af partiklerne.
3. Fremgangsmåde ifølge krav 1 eller 2, hvor calciumhydroxid-partiklerne er mindre end 75 μm , især 44 μm , og er i form af et
25 pulver.
4. Fremgangsmåde ifølge et hvilket som helst af kravene 1-3, hvor forholdet mellem tør is og calciumhydroxid er 31,8 kg (70 lb) tør is pr. 907,2 kg (ton) calciumhydroxid til en
30 calciumcarbonat-overfladebelægning på 20 vægt-%.
5. Fremgangsmåde ifølge et hvilket som helst af kravene 1-4, hvor calciumcarbonaten danner en jævn belægning på overfladen af calciumhydroxiden.
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6. Fremgangsmåde ifølge et hvilket som helst af kravene 1-5, hvor calciumcarbonat-belagte calciumhydroxid-partikler omfatter

15-30 vægt-% calciumcarbonat-belægning, fortrinsvis 20 vægt-% calciumcarbonat-belægning.

7. Fremgangsmåde ifølge et hvilket som helst af kravene 1-6,
5 hvor tørisen er i form af flager med en omtrentlig partikelstørrelse i intervallet fra ca. minus 1680 μm (12 mesh) til plus 1000 μm (18 mesh).

8. Fremgangsmåde ifølge et hvilket som helst af kravene 1-7,
10 hvor reaktionen udføres i batcher.

9. Fremgangsmåde ifølge et hvilket som helst af kravene 1-7, hvor reaktionen udføres i en kontinuerlig strøm.

15 10. Fremgangsmåde ifølge et hvilket som helst af kravene 1-9, hvor calciumhydroxid-partiklerne har en gennemsnitlig partikelstørrelse på 44 μm og har en størrelsesfordeling, der består af 95 % af en population af 44 μm -partikler.

20 11. Apparat til fremstilling af calciumcarbonat-belagte calciumhydroxid-partikler, som omfatter:

en reaktor;

et indløb til calciumhydroxid-partikler;

et indløb til tøris;

25 en densitetsmåler til bestemmelse af massefylden af et reaktionsprodukt,

hvor massefylden af reaktionsproduktet tilvejebringer en indikation af procenten af overfladecarbonering, der er dannet ved reaktionen af tørisen og calciumhydroxid; og

30 hvor mængden af tøris, der indføres i systemet, kan øges eller reduceres til tilvejebringelse af et produkt med en valgt massefylde og procent af overfladecarbonering.

12. Apparat ifølge krav 11, hvor densitetsmåleren er forbundet
35 med en computer, der styrer indløbet til $\text{Ca}(\text{OH})_2$ og indløbet til tøris til tilvejebringelse af et forhold mellem calciumhydroxid og tøris i reaktionsbeholderen til opnåelse af et produkt med en bestemt massefylde.

13. Apparat ifølge krav 11 eller 12, som yderligere omfatter et udløb til fjernelse af det carbonat-belagte calciumhydroxid-partikelprodukt.

5

14. Apparat ifølge et hvilket som helst af kravene 11-13, hvor $\text{Ca}(\text{OH})_2$ og tøris kan tilsættes til reaktionsbeholderen samtidigt til muliggørelse af tyngdekraftblanding af reaktionsbestanddelene.

DRAWINGS

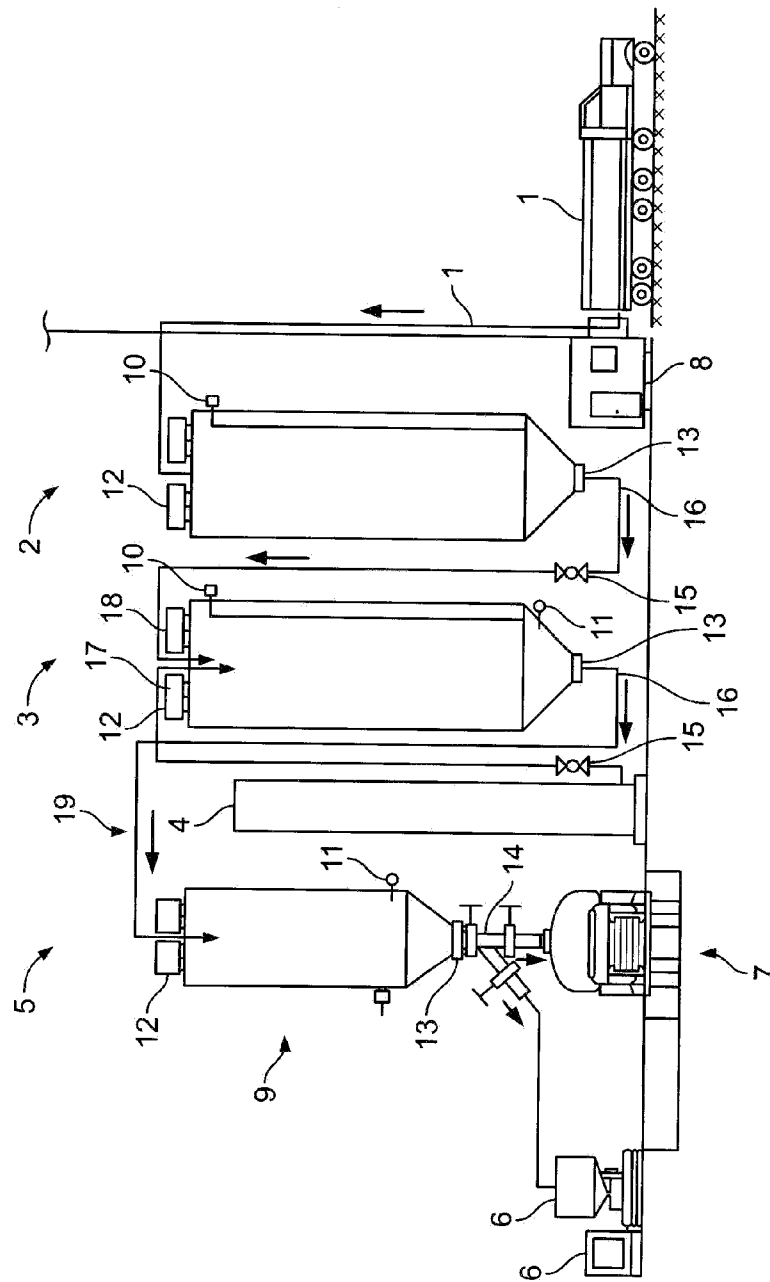


FIG. 1

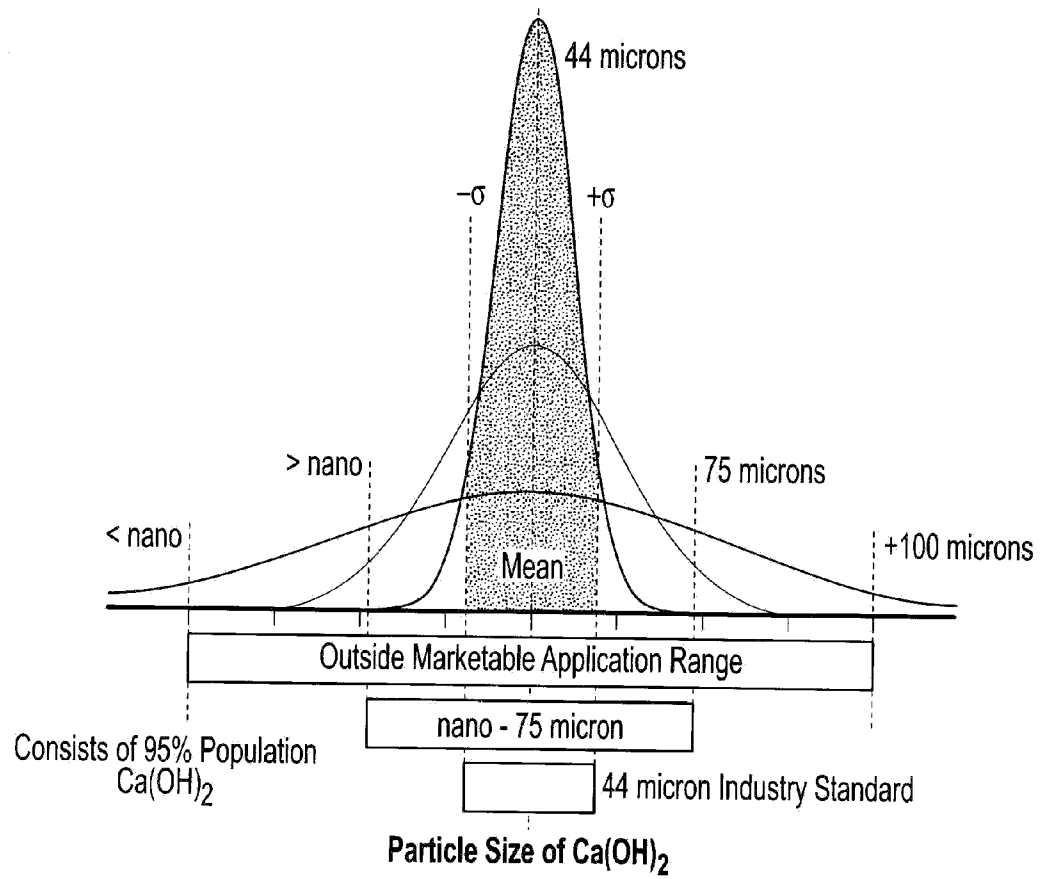


FIG. 2A

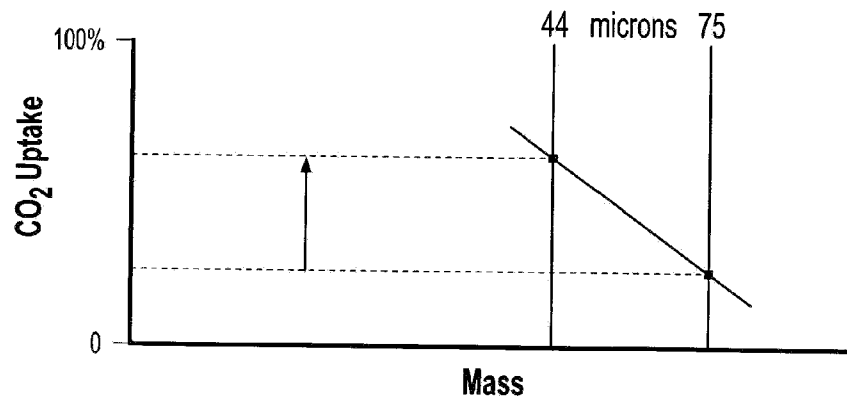


FIG. 2B

Commingled Flow Rate

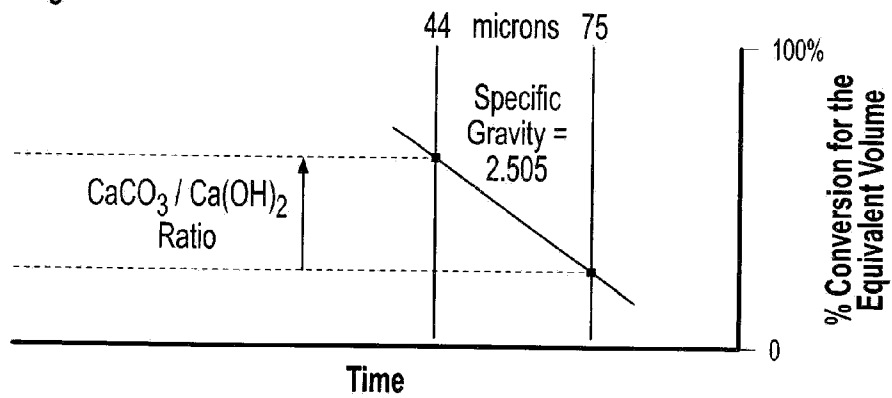


FIG. 3A

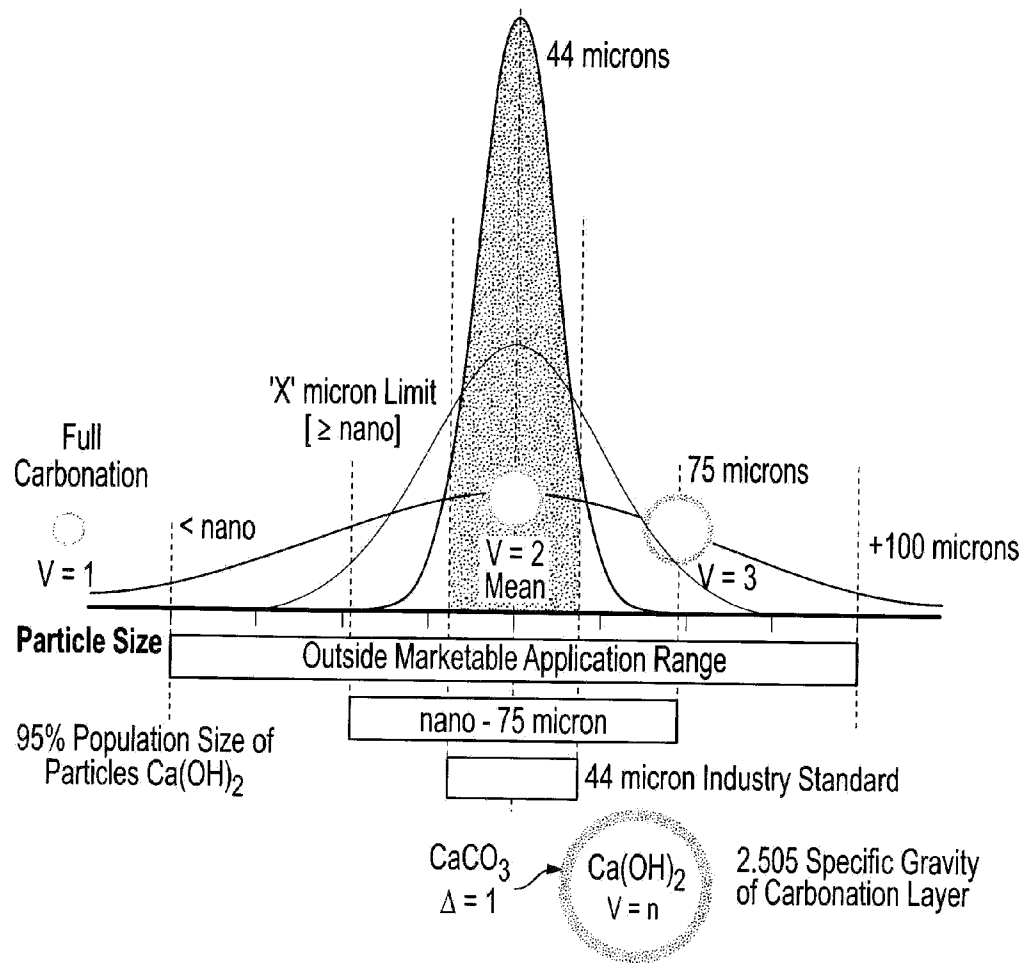


FIG. 3B