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NOTICE OF ENTITLEMENT

We W. L. GORE & ASSOCIATES (UK) LTD

of 1 Bell Park, London WC2A 2JP, England

being the Applicant and Nominated Person, in respect of Application No. 34584/93, state the following:

Andrew Miller Allan and Akis Katsakoglou are the actual inventors of the invention the subject of the Application.

The inventors made the invention for and on behalf of the applicant and nominated person in the course of their duties as employees of the applicant.

W. L. Gore & Associates (UK) Ltd is the applicant of the application listed in the declaration under Article 8 of the PCT.

Convention priority is claimed from the following basic application referred to in the declaration under Article 8 of the PCT:

Basic Applicant	Application Number	Application Date	Country	Country Code
W L Gore & Associates	9202360	4 February 1992	Great Britain	GB

The basic application referred to in the declaration under Article 8 of the PCT was the first application made in a Convention country in respect of the invention the subject of the Application.

DATED this 27th day of March 1995

W. L. GORE & ASSOCIATES (UK) LTD
By their Patent Attorney

GRIFFITH HACK & CO

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(54) Title
FILTER

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(71) Applicant(s)
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(56) Prior Art Documents
AU 47893/93 B01D
AU 72547/87 B01D
EP 443728

(57) Claim

1. A gas permeable and liquid impermeable filter which comprises a mixture of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble hydrogen sulphide adsorbent;

the particles being fused together such as to form a gas permeable liquid impermeable network of interconnected particles.

12. An ostomy bag which comprises a filter according to any preceding claim.

13. A colostomy and ileostomy bag which comprises a filter according to any preceding claim.

.../2

14. A process for the production of a gas permeable and liquid-impermeable hydrogen sulphide filter material which comprises:

(A) forming a mixture in liquid suspension of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble hydrogen sulphide adsorbent;

(B) applying the liquid suspension to a substrate and allowing to dry; and

(C) baking so as to fuse the particles together such as to form a gas permeable liquid-impermeable network of interconnected articles.

OPI DATE 01/09/93 APPLN. ID 34584/93
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(81) Designated States: AU, CA, JP, US, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).

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(54) Title: FILTER

(57) Abstract

An ostomy filter for colostomy and ileostomy bags is gas-permeable to allow venting, and liquid-impermeable to prevent leakage. It includes a hydrogen sulphide adsorbent to remove smells. The filter comprises 9 to 50 % by weight of particles of unsintered granular polytetrafluoroethylene (PTFE), 30 to 82 % by weight of particles of comminuted sintered expanded porous PTFE, and 9 to 30 % by weight of particulate water-insoluble H_2S adsorbent. The particles are fused together by baking at elevated temperature to form a gas-permeable liquid-impermeable network. The comminuted sintered expanded porous PTFE is preferably formed by comminuting uniaxially expanded PTFE fibre.

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FILTER

Field of the Invention

The present invention relates to a filter which allows gas to be vented from colostomy and ileostomy bags, whilst at the same time filtering out any unpleasant smell, particularly hydrogen sulphide.

Background

After undergoing a colostomy or ileostomy operation, the patient is fitted with a disposable bag which receives the waste contents of the intestine. The bag is disposable and is emptied or replaced at regular intervals. To avoid the bag becoming over inflated by virtue of gas generated by the fermenting food matter, it is desirable to provide a vent. However, the vent requires to be filtered in order to prevent embarrassing smells being released.

It is currently conventional practise in colostomy bags to provide an activated charcoal filter in the form of a disc as the vent. For example the disc may have a diameter of 23.5 mm and be formed of activated carbon contained within a foamed polyurethane material, having polypropylene net facings on either or both sides to improve its strength and other mechanical properties. However, this conventional filter material has the significant disadvantage of being liquid-permeable, so

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that if the patient sits or lies down there is a significant danger of leakage of liquid through the filter onto the patient's skin or his clothing. This is particularly the case with ileostomy bags, where the bag is connected into the early part of the intestine where the food matter is largely undigested and still fermenting, and has a high liquid content. In fact conventional ileostomy bags are not provided with vents, and the filters used for colostomy bags would be quickly saturated with liquid if used for ileostomy.

A porous polytetrafluoroethylene structure containing active carbon is disclosed in our British patent application GB2242431. However, the material disclosed is insufficiently gas permeable.

Patent specification GB 1399213 discloses a gas-permeable liquid impermeable membrane which includes finely divided high surface area carbon for the production of hydrogen sulphide.

It is an object of the present invention to provide a filter which mitigates these problems.

Summary of the Invention

The invention provides a gas permeable and liquid impermeable filter which comprises a mixture of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

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(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble hydrogen sulphide adsorbent;

the particles being fused together such as to form a gas permeable liquid impermeable network of interconnected particles.

The invention also provides a gas perr eable and liquid-impermeable filter which comprises a mixture of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble adsorbent comprising activated carbon impregnated with copper oxide;

the particles being fused together such as to form a gas permeable liquid impermeable network of interconnected particles.

The invention further provides a process for the production of a gas permeable and liquid-impermeable hydrogen sulphide filter material which comprises:

(A) forming a mixture in liquid suspension of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble hydrogen sulphide adsorbent;

(B) applying the liquid suspension to a substrate and allowing to dry; and

(C) baking so as to fuse the particles together such as to form a gas permeable liquid-impermeable network of interconnected particles.

Preferred Embodiments

The permeable nature of the polytetrafluoroethylene (PTFE) structure results from the particulate nature of

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the PTFE used to form it. The baking conditions are chosen such that the PTFE particles become partially fused or sintered into an integral permeable network during baking.

A feature of the present invention is that granular type PTFE is employed as a component. As is well known, PTFE can exist in two quite different forms viz; the granular form produced by precipitation polymerisation techniques, and the powdered form produced by dispersion polymerisation processes (i.e. fine-powder PTFE). These two types of PTFE have quite different properties and have to be considered separately.

Unsintered granular PTFE generally has a crystallinity in excess of 95% as determined by differential scanning calorimetry or by infra-red techniques. The degree of crystallinity is reduced by

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sintering (i.e. baking), and the finished structure of the present invention will typically have a crystallinity of less than 95%, often less than 80%. An unsintered granular PTFE is available from DuPont as Grade 7A.

The average particle size of the granular-type PTFE is usually in the range 1-500, particularly 1-200, especially 1-100 microns. Depending on the desired porosity of the structure, the particles may have substantially the same particle size, or a range of varying particle sizes may be included which pack to influence the porosity of the structure. The granular PTFE may be milled or unmilled.

The comminuted porous expanded polytetrafluoroethylene (PTFE) material comprises irregularly shaped particles of porous expanded PTFE. The starting material from which the comminuted expanded PTFE particles are produced may be any form of sintered porous expanded PTFE, such as film, sheet, rod, fibre or tube. Preferably the comminuted PTFE particles are derived from expanded porous PTFE which has been uniaxially expanded to form fibre or biaxially expanded to form sheet prior to comminution. It is preferably produced by comminuting (e.g. by chopping or grinding) expanded porous PTFE material (produced as described in US patent 3 953 566) to a particle size of 5 to 200 microns, particularly 40-100 microns. Generally speaking, the lower limit of particle size is 5 microns, preferably 20 microns and more preferably 40 microns; whilst the upper limit is 500 microns, preferably 200 microns and more preferably 100 microns. The structure of porous expanded PTFE is well known, being characterized by

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nodes interconnected by fibrils as described in US Patent 3,953,566 to form a waterproof, but water vapor-permeable porous material. The expanded PTFE is sintered to give dimensional stability, and to mitigate shrinkage during baking of the mixture to form the filter material. The particles of sintered porous PTFE may be produced by shredding or chopping sintered porous expanded PTFE to reduce it to small pieces, and then grinding these porous expanded PTFE pieces in water between closely spaced grinding surfaces to obtain sheared and ground particles of porous expanded PTFE, separating the sheared and ground particles from the water and drying the separated particles. Any suitable apparatus for grinding or comminuting tough polymeric or elastomeric materials may be used for producing the porous expanded PTFE particles, such as the apparatus disclosed in US-A-4614310 and US-A-4841623.

In order to deodorise the gas vented from the ostomy bag, hydrogen sulphide is filtered out by adsorption. The hydrogen sulphide adsorbent preferably includes a high surface area support material impregnated with a water-insoluble H_2S-adsorbent substance. The support material may be any suitable material known in the art, such as activated carbon, diatomaceous earth etc. Activated carbon is commercially available and is formed, for example, by heating carbon with steam to 800-900°C. In order to avoid removal or deactivation by water, the

H_2S-adsorbent is water-insoluble, and typically comprises a water-insoluble copper oxide.

A preferred material is activated carbon impregnated with copper oxide. This may be produced by soaking the activated carbon in cupric nitrate solution to produce cupric nitrate, and then drying and igniting to generate black copper oxide attached to the activated carbon. The copper oxide is insoluble in water or ethanol. Hydrogen sulphide is adsorbed by reaction to produce copper sulphide.

In order to provide good H_2S adsorption, the filter preferably comprises 10 to 30% by weight of impregnated high surface area adsorptive material. Typically, the H_2S-adsorbent constitutes 2 to 10% of the weight of the support material.

Particularly preferred embodiments of the invention comprise the components (i) - (iii) as defined above in the following weight percentages;

(i) 9-50%, preferably 10-40% (or 30-50%);

(ii) 30-82%, preferably 40-80% (or 30-50%); and

(iii) 9-30%, preferably 10-20% (or 10-30%).

The filter material is generally formed by applying to a substrate a suspension comprising the mixture of PTFE particles and impregnated support material, allowing to dry and baking at a temperature usually in the range 335 to 350°C for 0.5 to 3 hours. However, the conditions may be varied when the process is conducted as a continuous

operation, when reduced heating times of 1 to 30 mins may be used. The thickness may be created in a single step or may be built up by applying a number of layers and allowing each to dry between applications, prior to baking the layered composite. Generally, the process is conducted at substantially atmospheric pressure. Spraying ensures that no air pockets are left between the substrate and the coating. However, other known application techniques, such as a doctor blade can be used. The suspension is usually an aqueous suspension comprising appropriate surfactants, thickening agents and/or suspending agents. The temperature may be progressively raised over a few hours e.g. 1 to 10 hours in order to remove such additives, prior to baking.

The structure of the present invention generally has a specific gravity of 0.5 to 1.0, usually 0.6 to 0.9. The specific gravity tends to go down as the proportion of comminuted PTFE increases. In comparison, solid PTFE typically has a specific gravity of 2.16. It is important to get good gas permeability commensurate with acceptable physical strength.

The gas permeable PTFE filter is generally hydrophobic in nature and typically has a water entry pressure (measured as described in GB 2242431) in excess of 1.5, preferably 2.0 lbs per square inch. It is therefore liquid impermeable under normal conditions of usage.

The thickness of the filter will vary depending on the desired gas permeability and degree of adsorption, but is usually in the region 0.8 to 6mm, preferably 1 to 5 mm, and especially 1.5 to 2.5mm.

Preferably the filter has a gas permeability of at least 500 cc/min/cm^2.

The filter preferably allows a gas flow rate in excess of 1 litre per hour, preferably at least 5 litres, more preferably at least 10 litres per hour. Typical gas flow rates from a patient are approximately 2.5 litres per day, though peak flow rates during a day may exceed this. The filter is preferably capable of maintaining a level of H_2S in the filtered gas below one part per million for at least 20, preferably 40 minutes. In normal use on a patient this means that the filter would require changing every day or two. Principal gas flows occur after each meal as the food is digested. The filter is usually in the shape of a disc and may be arranged for flow of gas in a direction perpendicular to the plane of the disc. Alternatively for a longer flow path, it may be arranged to flow radially from a central entry point to the periphery of the disc (or vice versa). This may be achieved by skinning the surface of the filter disc during production and providing a central pinhole entry, or by masking the corresponding areas.

The ostomy filter of the present invention has a high water entry pressure which makes the filter impervious to liquid water under normal conditions of operation, whilst having good gas permeability and H_2S removal capacity. By

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including impregnants for different gases in the support material, the filter can be adapted to remove gases other than hydrogen sulphide.

The invention also relates to an ostomy bag including the filter, either as a removable replaceable filter element or integral with the bag (e.g. heat welded to the bag).

Detailed Description of Preferred Embodiments.

Embodiments of the invention will now be described by way of example only.

PREPARATION OF COMMINUTED EXPANDED POROUS POLYTETRAFLUOROETHYLENE PARTICLES.

Comminuted expanded porous PTFE was produced from sintered porous expanded PTFE material obtained from W.L. Gore & Associates, Inc. in sheet, rod, fibre or tube form. The porous expanded PTFE material was cut into pieces of about 6mm (quarter inch) largest dimension in a rotary cutting mill. The cut material was mixed with water to form a slurry, and the slurry fed between closely spaced grinding surfaces of a grinding mill, such as that disclosed in US-A-4841623, to crush and shear the pieces of porous expanded PTFE into particles. The ground slurry is then filtered or centrifuged to separate the porous expanded PTFE particles from the water, and the separated finely ground particles were oven dried at from 125°C - 150°C.

The product was a comminuted porous expanded PTFE material comprising finely ground particles of irregular shape.

The comminuted particles preferably will have a mean particle size between 20 and 500 microns, preferably between 40 and 200 microns. Particle size was determined as follows: using a magnetic stirrer and ultrasonic agitation, 2.5 grams of milled PTFE powder were dispersed in 60 ml isopropyl alcohol. (Ultrasonic Probe Model W-385, manufactured by Heat Systems-Ultrasonics, Inc.). Aliquots of 4-6 ml of the dispersed particles were added to approximately 250 ml of circulating isopropyl alcohol in a Leeds & Northup Microtrac FRA Particle Size Analyzer of analysis. Each analysis consisted of three 30-second runs at a sample circulation rate of 2 litres/minute during which light scattering by the dispersed particles is automatically measured and the particle size distribution automatically calculated from the measurements.

The particles will preferably have an average surface area of between 1 and 3 m^2/gm, as determined by specific surface area measured by a Leeds and Northrup surface area analyzer. The surface area analyzer uses the BET(1) method to calculate surface area. In this sample analysis, the desorption isotherm of a single point analysis was used to calculate the surface area.

EXAMPLE 1

The general procedure outlined in British Patent Publication GB 2242431A was followed. Teflon grade 7A resin (DuPont Speciality Polymers Division, Wilmington, U.S.A., average specific gravity 2.16 and particle size 35 microns) was mixed with the comminuted PTFE (particle size 50 to 100 microns), and activated carbon grade 209M (Sutcliffe Speakman) in the following percentages by weight:

Solids: 40% PTFE grade 7A
40% comminuted PTFE
20% activated carbon 209M

The solids were then blended in a Waring blender for 5 mins with liquid of the following composition by weight, in a ratio of 1 kg solids to 2 l of liquid, to produce a suspension.

Liquid: 43% water
43% carboxymethyl cellulose
6% Zonyl FSN100 surfactant
8% Pluronic L121 surfactant

Pluronics are a class of polyethylenepolypropylene glycol non-ionic surfactants.

The suspension was then sprayed as a coating onto a metal tray (as described in GB 2242431A) as a single layer. The thickness of the sprayed layer was about 20% greater than the desired thickness in the finished sample, to allow for shrinkage during baking. The coating was

then dried in an oven at 115°C for 30 mins. The temperature was raised to 280°C; then progressively to 333-348°C and baked at that temperature for 60 mins.

The specific gravity of the baked coating was 0.78. The water entry pressure was approximately 2 lbs per square inch.

EXAMPLE 2

Samples 1,2 and 3 as produced in Example 1 of varying thickness were cut into discs 23 mm in diameter (4.16 cm^2) and tested for gas deodorisation. The test gas comprised 80% nitrogen, 20% methane and 25ppm H_2S, and the flow rate was 0.5l/min. The test apparatus comprised a sample holder, a test gas inlet, an H_2S detector and read-out unit.

During the test the gas is allowed to flow to the centre of the filter sample, which is clamped in position in the holder. The gas flow through the sample may be axial or radial (for an increased path). The H_2S detector attached to the other side of the sample monitors the efficiency of the filter in removing the hydrogen sulphide. Once this efficiency begins to fall below 100% the detector reading is noted against time. The results are expressed as the time the electrochemical detector remains at zero (and moves to 0.1 ppm) as well as the time taken to reach 1.0 ppm.

The results are shown in Table 1.

TABLE 1				
Sample	Thickness mm	Gas* deodorisation litres	Time to detect [H_2S] 1.0 ppm (minutes)	Gas** permeability cc/min
1	2.7	9	18	1250
2	3.3	15	30	300
3	4.0	52.5	105	250

*target value = 9
** pressure of 4 cm waterhead

Example 3

The general procedure of Example 1 was repeated with two further compositions as follows:

TABLE 2		
Sample	4	5
PTFE grade 7A	10%	20%
Comminuted PTFE	80%	60%
Activated carbon 209M	10%	20%
Gas permeability cc/min/cm^2	4000	1000

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The comminuted PTFE was formed from Rastex (trademark) fibre expanded at 80:1 and of particle size 50 to 100 microns.

The drying regime employed was as follows. The wet sprayed coating was oven dried at 90°C overnight. The temperature was then raised to 115°C. Then the temperature was raised progressively from 115°C to 340°C over 7 hours. Finally, the coating was baked at 340°C for 30 mins.

The specific gravity was about 0.6 - 0.8 g/cc.

The coating was cut into discs about 23mm diameter and 2mm thick, and the gas permeability measured using a Gurley Densometer according to standard protocol. The Gurley number is defined as the time in seconds for 100cc of air to pass through one square inch of filter at 4.88 inches of water pressure differential. The Gurley number is then converted into a gas flow rate in cc/min/cm^2. The gas permeabilities are given in Table 2.

THE CLAIMS

1. A gas permeable and liquid impermeable filter which comprises a mixture of:

(i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);

(ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and

(iii) a particulate water-insoluble hydrogen sulphide adsorbent;

the particles being fused together such as to form a gas permeable liquid impermeable network of interconnected particles.

2. A filter according to claim 1 which comprises:

9 to 50% by weight of particles (i);

30 to 82% by weight of particles (ii); and

9 to 30% by weight of particles (iii);

particles (i), (ii) and (iii) being those respectively defined in claim 1.

3. A filter according to claim 1 which comprises:

10 to 40% by weight of particles (i);

40 to 80% by weight of particles (ii); and

10 to 20% by weight of particles (iii);

particles (i), (ii) and (iii) being those respectively defined in claim 1.

4. A filter according to claim 1 which comprises:

30 to 50% by weight of particles (i);

30 to 50% by weight of particles (ii); and

10 to 30% by weight of particles (iii);

particles (i), (ii) and (iii) being those respectively defined in claim 1.

5. A filter according to any preceding claim wherein the particles of comminuted porous PTFE have a particle size in the range 40 to 200 microns.

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6. A filter according to any preceding claim wherein the expanded porous PTFE, from which said comminuted PTFE particles are derived, is material which has been uniaxially expanded to form fibre prior to comminution.

7. A filter according to any of claims 1 to 5 wherein expanded porous PTFE, from which said comminuted PTFE particles are derived, has been biaxially expanded to form sheet prior to comminution.

8. A filter according to any preceding claim wherein the hydrogen sulphide adsorbent is activated carbon impregnated with copper oxide.

9. A filter according to any preceding claim having a specific gravity of 0.5 to 1.0 g/cc.

10. A filter according to any preceding claim in the form of a disc of thickness 1.0 to 5.00mm.

11. A filter according to any preceding claim having a gas permeability of at least 500 cc/min/cm^2.

12. An ostomy bag which comprises a filter according to any preceding claim.

13. A colostomy and ileostomy bag which comprises a filter according to any preceding claim.

14. A process for the production of a gas permeable and liquid-impermeable hydrogen sulphide filter material which comprises:

(A) forming a mixture in liquid suspension of:
  (i) particles of unsintered granular-type polytetrafluoroethylene (PTFE);
  (ii) particles of comminuted sintered expanded porous polytetrafluoroethylene (PTFE); and
  (iii) a particulate water-insoluble hydrogen sulphide adsorbent;

(B) applying the liquid suspension to a substrate and allowing to dry; and

(C) baking so as to fuse the particles together such as to form a gas permeable liquid-impermeable network of interconnected particles.

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15. A process according to claim 14 wherein the temperature of the dried suspension is gradually raised to baking temperature over 1 to 10 hours.

16. A process according to claim 14 or 15 wherein baking occurs at 335° to 350°C for 0.5 to 3 hours.

17. A gas permeable and liquid impermeable filter substantially as herein described with reference to Example 1 or Example 2.

18. A process for the production of a gas permeable and liquid-impermeable hydrogen sulphide filter material substantially as herein described with reference to Example 1 or Example 2.

Dated this 22nd day of November 1995

W. L. GORE & ASSOCIATES (UK) LTD

By their Patent Attorneys

GRIFFITH HACK & CO

AUSTRALIA PATENT OFFICE

INTERNATIONAL SEARCH REPORT

International Application No PCT/GB 93/00232

I. CLASSIFICATION OF SUBJECT MATTER (if several classification symbols apply, indicate all)[6]

According to International Patent Classification (IPC) or to both National Classification and IPC

Int.Cl. 5 A61F5/441

II. FIELDS SEARCHED

Minimum Documentation Searched[7]

Classification System	Classification Symbols
Int.Cl. 5	A61F ; C08J ; B01D

Documentation Searched other than Minimum Documentation to the Extent that such Documents are included in the Fields Searched[8]

III. DOCUMENTS CONSIDERED TO BE RELEVANT[9]

Category °	Citation of Document,[11] with indication, where appropriate, of the relevant passages[12]	Relevant to Claim No.[13]
A	GB,A,2 059 797 (HOLLISTER) 29 April 1981 see page 2, line 98 - page 3, line 129	1,12
A	EP,A,0 443 728 (E.R. SQUIBB & SONS) 28 August 1991 see column 3, line 51 - column 4, line 25	1,12
A	EP,A,0 358 316 (E.R. SQUIBB & SONS) 14 March 1990 see claim 1	1,12
A	GB,A,2 139 501 (CRAIG MEDICAL) 14 November 1984	
A	PATENT ABSTRACTS OF JAPAN vol. 8, no. 255 (C-253)(1984) & JP,A,59 133 386 (ASAHI GLAS) see abstract	14

° Special categories of cited documents :[10]

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier document but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

IV. CERTIFICATION

Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report
16 APRIL 1993	23. 04. 93
International Searching Authority	**Signature of Authorized Officer**
EUROPEAN PATENT OFFICE	SANCHEZ Y SANCHEZ J.

ANNEX TO THE INTERNATIONAL SEARCH REPORT ON INTERNATIONAL PATENT APPLICATION NO.

GB 9300232
SA 69550

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on
The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information. 16/04/93

Patent document cited in search report	Publication date	Patent family member(s)		Publication date
GB-A-2059797	29-04-81	US-A-	4274848	23-06-81
		AU-B-	534649	09-02-84
		AU-A-	6248580	09-04-81
		CA-A-	1146874	24-05-83
		DE-A,C	3036009	09-04-81
		FR-A,B	2465510	27-03-81
		JP-A-	56054836	15-05-81
		SE-B-	443504	03-03-86
		SE-A-	8006502	25-03-81
EP-A-0443728	28-08-91	JP-A-	4218156	07-08-92
EP-A-0358316	14-03-90	GB-A-	2221854	21-02-90
		JP-A-	2082969	23-03-90
GB-A-2139501	14-11-84	None		

EPO FORM P0479

For more details about this annex : see Official Journal of the European Patent Office, No. 12/82