

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
8 March 2012 (08.03.2012)

PCT

(10) International Publication Number
WO 2012/031072 A1

(51) International Patent Classification:

C07B 59/00 (2006.01) *C12P 17/18* (2006.01)
C07D 473/04 (2006.01)

(21) International Application Number:

PCT/US2011/050138

(22) International Filing Date:

1 September 2011 (01.09.2011)

(25) Filing Language:

English

(26) Publication Language:

English

(30) Priority Data:

61/379,182 1 September 2010 (01.09.2010) US

(71) Applicant (for all designated States except US): **CONCERT PHARMACEUTICALS, INC.** [US/US]; 99 Hayden Avenue, Lexington, MA 02421 (US).

(72) Inventors; and

(75) Inventors/Applicants (for US only): **KANAMARLAPUDI, Ramanaiiah, C.** [US/US]; 10 Langon Hollow Road, Bridgewater, NJ 08807 (US). **WEISSMAN, Steven, A.** [US/US]; 281 Forest Dr. South, Short Hills, NJ 07078 (US). **EISENREICH, Emerich** [US/US]; 2123 Bonnie Brae Avenue, Claremont, CA 91711 (US). **LIU, Xuejun** [CN/US]; 208 E. Newman Avenue, Arcadia, CA 91006 (US).

(74) Agents: **DAVIS, Steven G.** et al.; McCarter & English, LLP, 265 Franklin Street, Boston, MA 02110 (US).

(81) Designated States (unless otherwise indicated, for every kind of national protection available): AE, AG, AL, AM,

AO, AT, AU, AZ, BA, BB, BG, BH, BR, BW, BY, BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DK, DM, DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KN, KP, KR, KZ, LA, LC, LK, LR, LS, LT, LU, LY, MA, MD, ME, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PE, PG, PH, PL, PT, QA, RO, RS, RU, RW, SC, SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW.

(84) Designated States (unless otherwise indicated, for every kind of regional protection available): ARIPO (BW, GH, GM, KE, LR, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European (AL, AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU, LV, MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK, SM, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG).

Declarations under Rule 4.17:

- as to applicant's entitlement to apply for and be granted a patent (Rule 4.17(ii))
- as to the applicant's entitlement to claim the priority of the earlier application (Rule 4.17(iii))

Published:

- with international search report (Art. 21(3))

(54) Title: PROCESS FOR PREPARING AN ENANTIOMERICALLY ENRICHED, DEUTERATED SECONDARY ALCOHOL FROM A CORRESPONDING KETONE WITHOUT REDUCING DEUTERIUM INCORPORATION

(57) Abstract: The present invention provides a convenient and efficient process for the preparation of enantiomerically enriched, deuterated secondary alcohols without reducing deuterium incorporation.



WO 2012/031072 A1

***PROCESS FOR PREPARING AN ENANTIOMERICALLY ENRICHED,
DEUTERATED SECONDARY ALCOHOL FROM A CORRESPONDING KETONE
WITHOUT REDUCING DEUTERIUM INCORPORATION***

Related Application

This application is claims the benefit of U.S. Provisional Patent Application No. 61/379,182, filed September 1, 2010, the entire contents of which are hereby incorporated by reference.

Background of the Invention

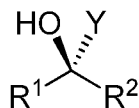
[1] The (*R*)M-1 metabolite of pentoxifylline is known as lisofylline and is known to have similar properties to pentoxifylline.

[2] Deuterated (*R*) M-1 metabolites of pentoxifylline and related compounds have been reported as having therapeutic utility in WO2009/108383. There is a need for commercially feasible methods for producing such deuterated (*R*)-M-1 metabolites, as well as other deuterated (*R*)- alcohols.

Summary of the Invention

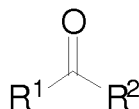
[3] Applicants have solved this problem by employing certain commercially available ketoreductases and carbonyl reductases to produce deuterated (*R*)-alcohols from the corresponding prochiral deuterated ketone in a highly stereoselective manner without loss of deuterium incorporation.

[4] The present invention provides a process for the preparation of a compound of Formula I:



(I)

comprising reacting a compound of formula II:



(II)

with a hydride source or a deuteride source in the presence of a ketoreductase or carbonyl reductase to form a compound of formula I with an enantiomeric excess of at least 80%, wherein:

Y is H when a compound of Formula II is reacted with a hydride source; or

Y is D when a compound of Formula II is reacted with a deuteride source;

R¹ is -CH₃ or -CD₃;

R² is a C₂-C₁₀ alkylene-X wherein X is H, D, or R³ and the C₂-C₁₀ alkylene portion of R² is optionally substituted with a group independently selected from the group consisting of (i) one or more deuterium, and (ii) one R³; and

R³ is (i) C₆-C₁₀ aryl, 5-10-membered heteroaryl, C₃-C₈ cycloalkyl, or saturated heterocyclyl, wherein R³ is optionally substituted with one or more substituent independently selected from deuterium, C₁-C₂ alkyl optionally substituted with deuterium, and -OH; or (ii) a tautomer thereof;

wherein at least one of R¹ and the C₂-C₁₀ alkylene portion of R² is substituted with deuterium; and

wherein the amount of deuterium incorporation at each deuterium in R¹ and the C₂-C₁₀ alkylene portion R² in the compound of formula I is substantially equal to the amount of deuterium incorporation at corresponding deuterium atoms in R¹ and R² in the compound of formula II.

[5] The process of this invention is particularly useful to reduce deuterated forms of pentoxifylline to their corresponding deuterated alcohols.

Detailed Description of the Invention

DEFINITIONS:

[6] “The term “alkyl” refers to a monovalent, saturated hydrocarbon group having the indicated number or range of carbon atoms. For example, C₂-C₁₀ alkyl is an alkyl having from 2 to 10 carbon atoms. An alkyl may be linear or branched. Examples of alkyl groups include methyl; ethyl; propyl, including *n*-propyl and isopropyl; butyl, including *n*-butyl, isobutyl, *sec*-butyl, and *t*-butyl; pentyl, including, for example, *n*-pentyl, isopentyl, and neopentyl; and hexyl, including, for example, *n*-hexyl, 2-methylpentyl and heptyl.

[7] The term “cycloalkyl” refers to a monovalent monocyclic or bicyclic saturated

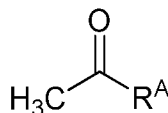
group containing only carbon ring atoms. The term “C₃-C₈ cycloalkyl” refers to a monocyclic saturated group containing between 3 and 7 carbon ring atoms. Examples of cycloalkyl include cyclopropyl, cyclobutyl, cyclopentyl, and cyclohexyl, cycloheptyl, *cis*- and *trans*-decalinyl, and norbornyl.

[8] The term “aryl” refers to an aromatic carbocycle. The term “C₆-C₁₀ aryl” refers to a monocyclic or bicyclic, aromatic carbocycle containing between 6 and 10 ring carbon atoms. Examples of aryl are phenyl and naphthyl.

[9] The term “saturated heterocyclyl” refers to a monovalent monocyclic or bicyclic saturated group containing between 3 and 8 ring atoms, wherein one or more ring atoms is a heteroatom independently selected from N, O, and S. Examples of saturated heterocycles include azepanyl, azetidiny, aziridiny, imidazolidiny, morpholinyl, oxazolidiny, piperaziny, piperidiny, pyrazolidiny, pyrrolidiny, tetrahydrofuranyl, and thiomorpholinyl.

[10] The term “heteroaryl” refers to a monovalent monocyclic or bicyclic aromatic group, wherein one or more ring atoms is a heteroatom independently selected from N, O, and S. A 5-10 membered heteroaryl is a monocyclic or bicyclic heteroaryl that contains between 5 and 10 ring atoms. Examples of heteroaryl groups include furanyl, thiazolyl, isothiazolyl, isoxazolyl, oxazolyl, pyrimidinyl, pyrazolyl, pyridazinyl, pyridinyl, pyrrolyl, thiadiazolyl, thiophenyl, triazinyl, triazolyl, quinolinyl, quinazolinyl, indolyl, isoindolyl, 3,7-dihydro-1H-purine-2,6-dion-yl; xanthinyl, hypoxanthinyl, theobrominyl, uric acid, isoguaninyl, thymine, and uracilyl.

[11] The term “ketoreductase or carbonyl reductase” refers to an enzyme belonging to Enzyme Classification Class 1.1.1.184, which, in the presence of which a hydride source, is capable of converting a methyl ketone into a secondary alcohol. The term



“methyl ketone” refers to a ketone of the formula: $\text{H}_3\text{C}-\text{C}(=\text{O})-\text{R}^{\text{A}}$, wherein R^A is C_nH_{2n+1} and n is an integer between 2 and 10.

[12] The term “substituted” refers to the replacement of one or more hydrogen atoms with the indicated substituent. For avoidance of doubt, substitutions may occur on the terminus of a moiety. For example, the terminal -CH₃ group on R² may be substituted with an R³. “Substituted with deuterium” refers to the replacement of one or more hydrogen atoms with a corresponding number of deuterium atoms.

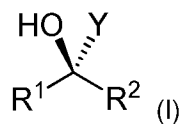
[13] When a position is designated specifically as “D” or deuterium, the position is understood to have deuterium at an abundance that is at least 1000 times greater than the natural abundance of deuterium, which is 0.015% (i.e., at least 15% incorporation of deuterium). In certain embodiments, when a position is designated as “D” or deuterium that position has at least 50.1% incorporation of deuterium, at least 75% incorporation of deuterium; at least 80% incorporation of deuterium, at least 85% incorporation of deuterium; at least 90% incorporation of deuterium; at least 95% incorporation of deuterium; at least 98% incorporation of deuterium; at least 99% incorporation of deuterium; or at least 99.5% incorporation of deuterium.

[14] When a position is designated specifically as “H” or hydrogen, the position is understood to have hydrogen at its natural isotopic abundance.

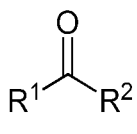
The amount of deuterium incorporation at a deuterium atom in a compound of Formula I is said to be “substantially equal” to the amount of deuterium incorporation at the corresponding deuterium atom in a compound of Formula II if the difference in the amount of deuterium incorporation between them is no more than about 5 %, as an example no more than about 3 %; no more than about 2 %; no more than about 1 %; or no more than about 0.5 %.

KETONES USEFUL AS COMPOUNDS OF FORMULA II

[15] It will be understood that each of R^1 and R^2 in a compound of Formula I,



, is structurally identical to the corresponding R^1 and R^2 in a compound



of Formula II, (II). Notwithstanding this, according to the present invention, the amount of deuterium incorporation at any deuterium present in R^1 and R^2 of a compound of Formula I is substantially equal to the amount of deuterium incorporation at the corresponding deuterium atoms in a compound of Formula II.

[16] In one embodiment, R^2 is substituted with one or two R^3 .

[17] In one embodiment, at least one of R^1 and R^2 comprises a deuterium bound to the carbon atom adjacent the carbonyl carbon.

[18] In one embodiment, each of R^1 and R^2 is substituted with one or more deuterium. In one aspect of this embodiment at least one of R^1 and R^2 comprises a deuterium bound to the carbon atom adjacent the carbonyl carbon.

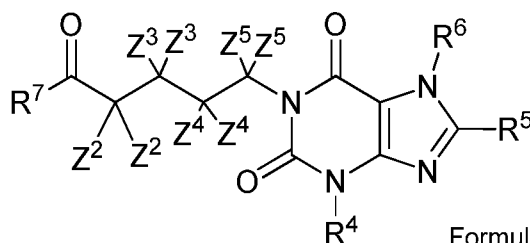
[19] In one embodiment, R^1 is CH_3 .

[20] In another embodiment, R^1 is CD_3 .

[21] In one embodiment, R^2 is C_2 - C_6 alkyl optionally substituted with one or more deuterium and optionally substituted with one or two R^3 . In one aspect of this embodiment, R^2 is $-CH_2$ -(C_1 - C_5 alkyl optionally substituted with one or more deuterium and optionally substituted with one R^3). In another aspect of this embodiment, R^2 is $-CH_2$ -(C_1 - C_5 alkyl optionally substituted with one or more deuterium and optionally substituted with one R^3).

[22] In one embodiment, R^3 is (i) 5-10-membered heteroaryl optionally substituted with one or more substituents independently selected from deuterium, C_1 - C_2 alkyl optionally substituted with deuterium, and $-OH$; or (ii) a tautomer thereof.

[23] In one embodiment, a compound of Formula II has structural Formula II-A:



Formula II-A, or a salt thereof, wherein:

each of R^4 , R^6 and R^7 is independently selected from $-CH_3$ and $-CD_3$;

R^5 is hydrogen or deuterium or a combination thereof;

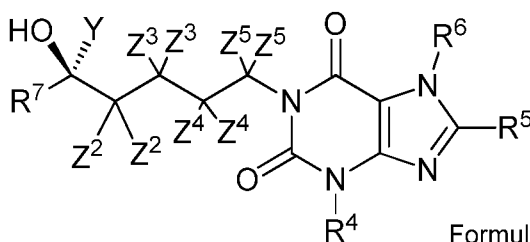
each Z^2 is the same and is hydrogen or deuterium;

each Z^3 is the same and is hydrogen or deuterium;

each Z^4 is the same and is hydrogen or deuterium;

each Z^5 is the same and is hydrogen or deuterium; and

either R^7 is $-CD_3$ or at least one of Z^2 , Z^3 , Z^4 and Z^5 is deuterium. In such an embodiment, the corresponding compound of Formula I has structural Formula I-A:



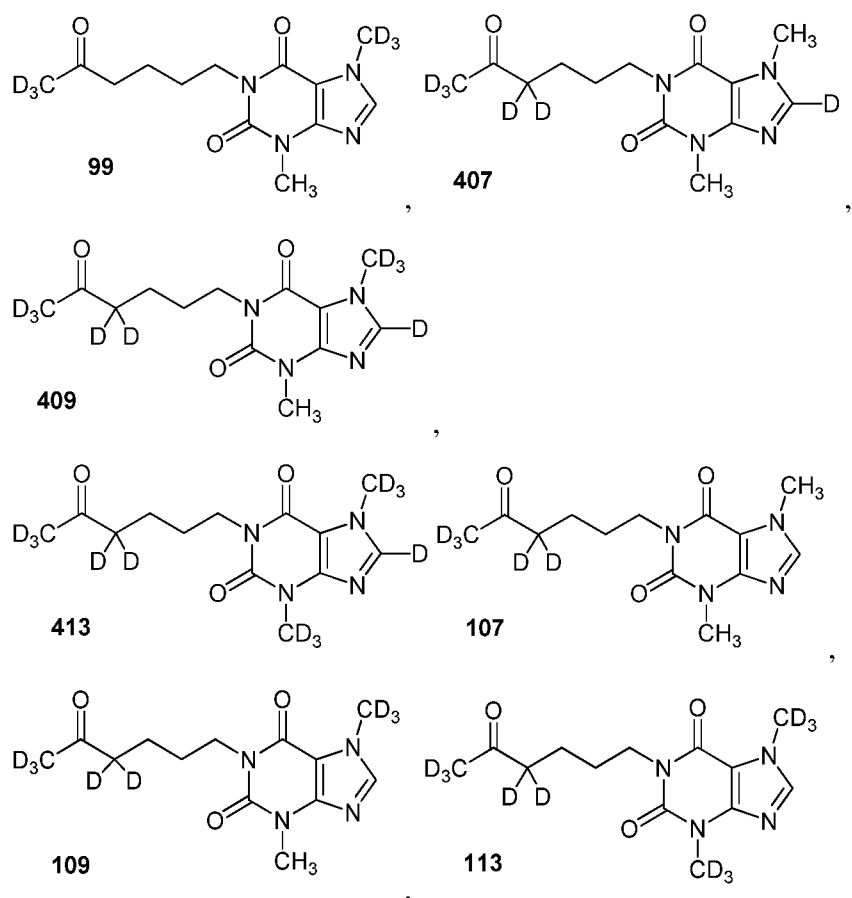
Formula I-A, wherein R^4 , R^5 , R^6 , R^7 , Z^2 , Z^3 , Z^4 and

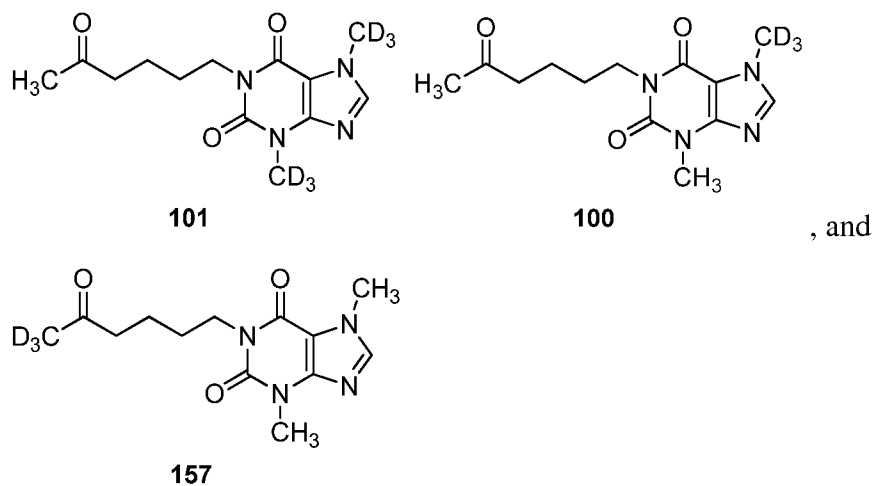
Z^5 are as defined for Formula II-A; and Y is as defined for Formula I.

[24] In one embodiment of Formula I-A and II-A, each R^7 is $-CD_3$.

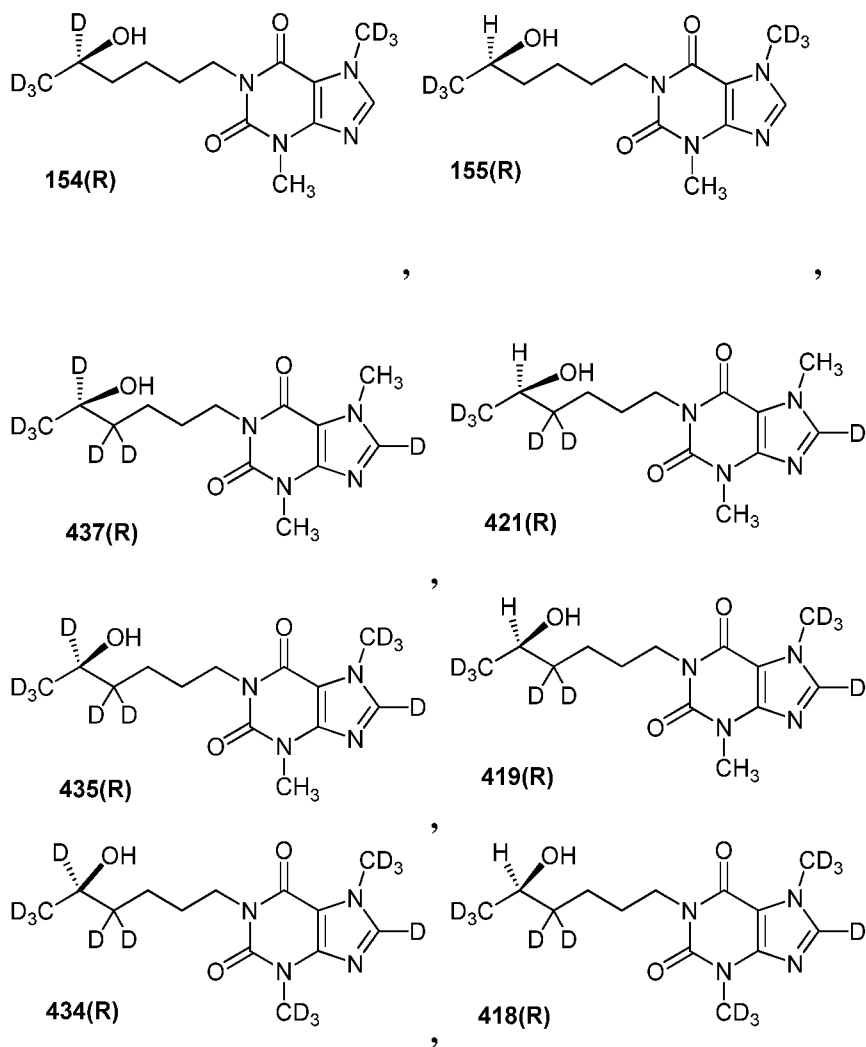
[25] In one embodiment of Formula I-A and II-A, each Z^2 is deuterium.

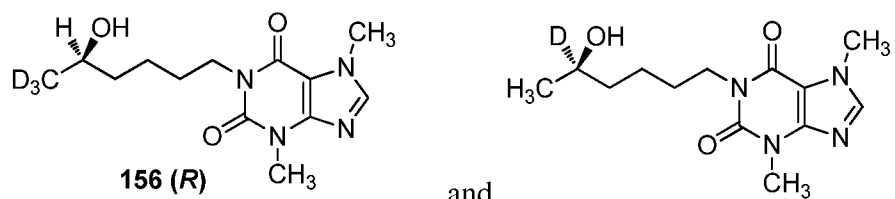
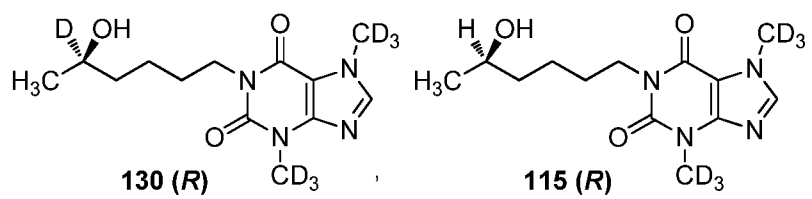
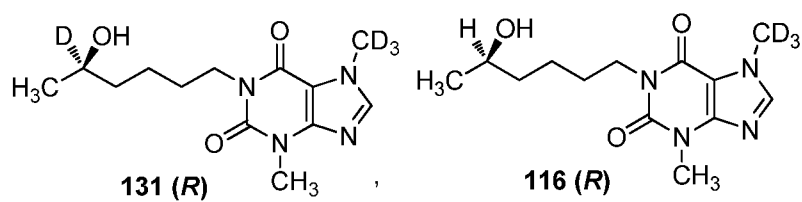
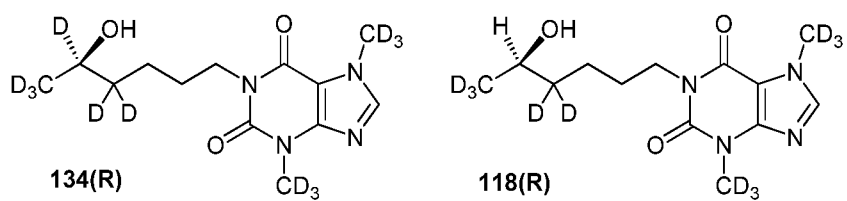
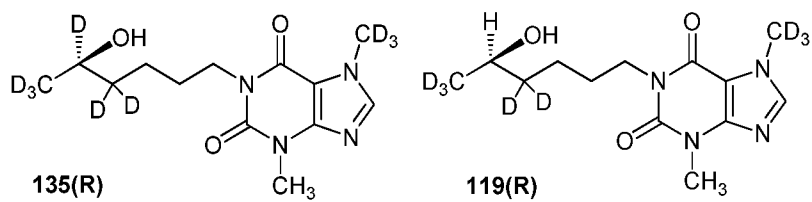
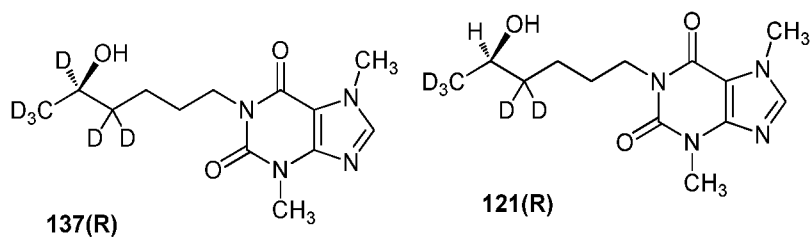
- [26] In another embodiment of Formula I-A and II-A, each Z^2 is hydrogen.
- [27] In one embodiment of Formula I-A and II-A, each R^5 is deuterium.
- [28] In one embodiment of Formula I-A and II-A, each R^5 is hydrogen.
- [29] In one embodiment of Formula I-A and II-A, each Z^3 , Z^4 and Z^5 is hydrogen. In one aspect of this embodiment each R^6 is $-\text{CH}_3$ and each R^7 is $-\text{CD}_3$. In a more specific aspect, each R^4 is $-\text{CH}_3$, each R^6 is $-\text{CH}_3$; and each R^7 is $-\text{CD}_3$. In another aspect of this embodiment each R^6 is $-\text{CD}_3$ and each R^7 is $-\text{CD}_3$.
- [30] In one embodiment of Formula I-A and II-A, each Z^3 , Z^4 and Z^5 is deuterium.
- [31] In one embodiment of Formula I-A and II-A, each R^6 and each R^4 is $-\text{CD}_3$.
- [32] In one embodiment of Formula II-A, the compound is selected from any one of:





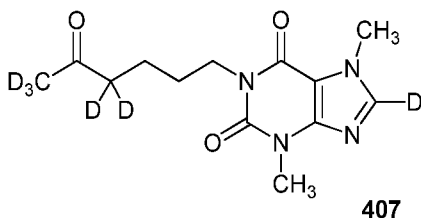
[33] In one embodiment of Formula I-A, the compound is selected from the following:



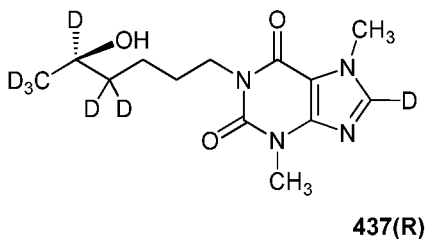


, and

[34] In one specific aspect, the compound of Formula II-A is

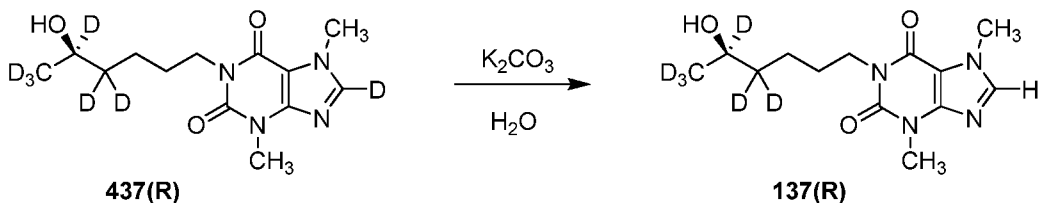


(Compound 407) and the compound of Formula I-A is



(Compound 437(R)).

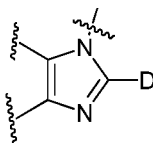
[35] In one embodiment, Compound 437 (R) is further converted to Compound 137(R) by treatment with K_2CO_3 and water. Thus, maintenance of the deuteration at that position during the enzymatic conversion to Compound 437(R) is unimportant:



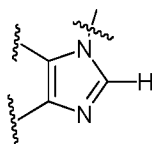
In one embodiment, compound 137(R) is substantially free of 437(R).

“Substantially free” means that the amount of 437(R) is equal to or less than 5%, more preferably equal to or less than 1%, or more preferably equal to or less than 0.1%, of the amount of 137(R).

In one embodiment, any compound of formula I-A having a group



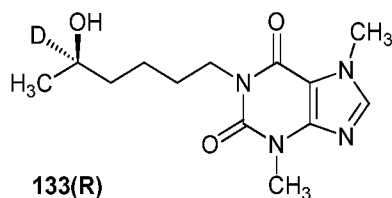
may be further converted to a compound having the same structure except for having a group



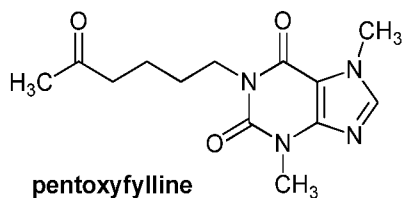
by treating with a suitable base and a proton source, such as water.

[36] Applicants have discovered that the use of a ketoreductase or carbonyl reductase to reduce a deuterium-containing ketone compound of Formula II, in particular a compound of Formula II-A, allows for both high enantiomeric enrichment and substantially no loss of deuterium incorporation. In particular, the amount of deuterium incorporation at each deuterium in R^1 and R^2 in the compound of formula I is substantially equal to the amount of deuterium incorporation at corresponding deuterium atoms in R^1 and R^2 in the compound of formula II. This is particularly surprising in that it was unexpected that one could provide buffer conditions that (1) allowed the ketoreductase or carbonyl reductase to efficiently reduce the ketone without also allowing the enzyme to catalyze deuterium-to-hydrogen exchange on the existing deuterium atoms; (2) would not result in an acidic pH which would be expected to cause deuterium-to-hydrogen exchange on the existing deuterium atoms; and (3) would not require for activity sufficiently basic or acidic conditions that would also be expected to cause deuterium-to-hydrogen exchange.

[37] In a related embodiment the invention provides a method of making Compound 133(R)



comprising the step of reacting pentoxifylline:



with a deuteride source in the presence of a ketoreductase or carbonyl reductase and an appropriate catalytic co-factor at a pH between 6.5 and 7.3 to form a compound of formula I with an enantiomeric excess of at least 90% and deuterium incorporation of at the hydroxy carbon of Compound 133(*R*) of least 90%.

[38] Any ketoreductase or carbonyl reductase that produces a 90% or greater enantiomeric excess of the (*R*)-OH stereoisomer of Formula II may be utilized in the method of this invention. Commercially available kits containing different ketoreductases or carbonyl reductases are available from multiple vendors. A determination of whether or not a particular ketoreductase or carbonyl reductase produces a 90% or greater enantiomeric excess of the (*R*)-OH stereoisomer of Formula II may be achieved by standard techniques well-known in the art. For example, a compound of Formula II may be incubated with the ketoreductase or carbonyl reductase to be screened in the presence of a hydride or deuteride source.

[39] In one embodiment, the ketoreductase is a naturally occurring ketoreductase selected from the group consisting of *Candida magnoliae* ketoreductase, *Candida parapsilosis* ketoreductase, and *Sporobolomyces salmicolor* ketoreductase.

[40] In one embodiment, the ketoreductase or carbonyl reductase is selected from any one or ALMAC Carbonyl Reductases CRED A161, CRED A291, CRED A311, or CRED A601 (each commercially available from ALMAC Group Ltd, Craigavon, England), any one of CODEXIS Ketoreductases KRED-NADP-118, or KRED-NAD 1110 (each commercially available from Codexis Inc., Redwood City, CA), or SYNCORE Ketoreductases ES-KRED-120, ES-KRED-126, or ES-KRED-131 (each commercially available from Syncore Labs, Shanghai, China). In one aspect of this embodiment, the enzyme is selected from CRED A291, CRED A311, or CRED A601. In a more specific aspect, the enzyme is CRED A311.

[41] In one embodiment, the amount of enzyme used in the reaction ranges from 0.05 wt% to 10 wt% as a percentage of the weight of the substrate, such as 0.5 wt% to 5 wt%. In one embodiment, the amount of enzyme is between 1.0 wt% and 2.0 wt%. In a more specific aspect, the amount of enzyme is about 1.0 wt%.

[42] In one embodiment, the compound of formula I is formed with an enantiomeric excess of at least 90%. In one aspect of this embodiment, the enantiomeric excess is at least 94%. In a more particular aspect of this embodiment, the enantiomeric excess is at

least 96%. In a more particular aspect of this embodiment, the enantiomeric excess is at least 98%.

[43] The process of this invention requires the presence of a hydride source or a deuteride source. The term “hydride source” refers to a compound or mixture that is capable of providing a hydride anion or a synthetic equivalent of a hydride anion. Similarly, the term “deuteride source” refers to a compound or mixture that is capable of providing a deuteride anion or a synthetic equivalent of a deuteride anion. A hydride or deuteride source comprises a co-factor, which may be in catalytic or stoichiometric amounts. When the co-factor is in a catalytic amount, the hydride or deuteride source comprises a co-factor regeneration system.

[44] A co-factor used with the ketone reductase or carbonyl reductase in the process of this invention is selected from NAD, NADP, NADH, NADPH, NAD²H and NADP²H. The choice of co-factor may be based upon (a) the presence or absence of a co-factor regeneration system; (b) the requirement for a hydride versus a deuteride source; and (c) compatibility with the specific ketone reductase or carbonyl reductase employed. In embodiments where the hydride or deuteride source does not comprise a co-factor regeneration system, the co-factor is in a stoichiometric amount and is a reduced co-factor which is therefore selected from NADH and NADPH for a hydride source, or NAD²H and NADP²H for a deuteride source. It is well known in the art - or information is available from the commercial supplier of the specific ketone reductase or carbonyl reductase - whether NADH or NADPH is the appropriate co-factor for a given ketone reductase or carbonyl reductase. In this embodiment, the reduced co-factor is present in stoichiometric amounts as compared to the compound of Formula II.

[45] In another embodiment, the hydride or deuteride source additionally comprises a co-factor regeneration system. The high cost of co-factors, in particular the deuterated co-factors, makes their use on a stoichiometric basis impractical. A low-cost co-factor regeneration system continually produces and regenerates the reduced form of the co-factor, requiring the co-factor to be present in only catalytic amounts. Moreover, the use of a co-factor regeneration system eliminates the need to use a reduced co-factor or a deuterated co-factor. The co-factor regeneration system produces the required reduced or reduced and deuterated co-factor *in situ*. Accordingly, any cofactor or combinations of cofactors compatible with the chosen ketone reductase or carbonyl reductase can be employed with a co-factor regeneration system. In this embodiment, therefore, NAD is

interchangeable with NADH and NAD²H; and NADP is interchangeable with NADPH and NADP²H. Similarly, the designations “-NAD” and “-NADH”, and “-NADP” and “-NADPH”, respectively, are used interchangeably herein in conjunction with enzymes that use, respectively, NADH and NADPH as co-factors.

[46] When used in conjunction with a co-factor regeneration system the amount of co-factor can range from 0.1 wt% to 5 wt%. In one aspect of this embodiment, the amount of co-factor is between 1 wt% and 3 wt%. In an alternate aspect of this embodiment, the amount of cofactor is between 0.1 wt% and 1.1 wt%.

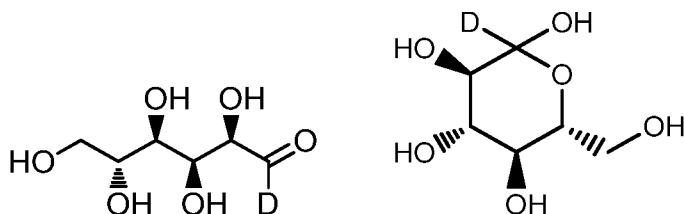
[47] A typical co-factor regeneration system consists of a dehydrogenase and a substrate for that dehydrogenase. Without being bound by theory or mechanism, Applicants believe that upon catalysis by the dehydrogenase, its substrate provides a hydride or deuteride anion to regenerate (reduce) the cofactor. The newly reduced cofactor can then subsequently donate a hydride or deuteride atom to the compound of Formula II to provide a compound of Formula I. In certain embodiments, the substrate for the dehydrogenase may be generated *in situ* from the corresponding ketone and a reducing agent. A second co-factor regeneration system takes advantage of the fact that certain ketoreductases and carbonyl reductases both possess alcohol dehydrogenase activity. In this system an alcohol dehydrogenase substrate is used and upon catalysis donates the hydride or deuteride ion to the co-factor.

[48] Examples of hydride cofactor regeneration systems include, but are not limited to, reducing sugars and their corresponding hydrogenase, e.g., glucose and glucose dehydrogenase (“GDH”), glucose-6-phosphate and glucose-6-phosphate dehydrogenase, etc.; formate and formate dehydrogenase; a secondary (e.g., isopropanol) alcohol and a secondary alcohol dehydrogenase; phosphite and phosphite dehydrogenase; molecular hydrogen and hydrogenase; and ethanol, aldehyde dehydrogenase and an alcohol dehydrogenase.

[49] Examples of deuteride co-factor regeneration systems include, but are not limited to, deuterated reducing sugars and their corresponding dehydrogenase, e.g., deuterated glucose and GDH, deuterated glucose-6-phosphate and glucose-6-phosphate dehydrogenase, etc.; deuterated formate and formate dehydrogenase; a secondary deuterated (e.g., deuterated isopropanol) alcohol alone or together with a secondary alcohol dehydrogenase; deuterated phosphite and phosphite dehydrogenase; molecular

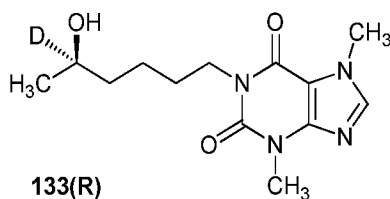
deuterium and hydrogenase; and deuterated ethanol and aldehyde dehydrogenase optionally together with an alcohol dehydrogenase.

[50] In one embodiment of the process, the deuteride co-factor regeneration system comprises a substrate having a $-C(D)OH$ functional group and its associated dehydrogenase. In a related embodiment, the substrate having a $-C(D)OH$ functional group is generated *in situ*. In this related embodiment, the deuteride co-factor regeneration system comprises (a) a compound having a $C=O$ functional group; (b) a metal deuteride or a mixed metal deuteride, such as a borodeuteride or aluminum deuteride of a metal such as sodium or lithium, capable of reducing the $C=O$ functional group to a $-C(D)OH$ functional group; and (c) a dehydrogenase that acts upon the $-C(D)OH$ functional group. As an example, the substrate having a $-C(D)OH$ functional group is a C_1 - C_6 alcohol such as $CH_3C(D)(OH)CH_3$. As another example, the substrate having a $-C(D)OH$ functional group is carbohydrate of the formula $C_6H_{11}DO_6$, such as deuterated glucose (shown below in its open chain and pyranose forms):



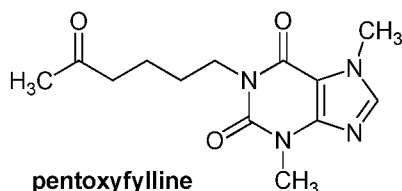
[51] As yet another example the deuterated glucose is generated *in situ* from D-glucono- δ -lactone and $NaBD_4$. This embodiment is advantageous in that an otherwise expensive deuterated glucose substrate is generated *in situ* from relatively inexpensive D-glucono- δ -lactone and $NaBD_4$.

[52] Moreover, the inventors have discovered that the use of deuterated glucose (or D-glucono- δ -lactone and $NaBD_4$) as part of the deuteride source consistently produced high deuterium incorporation (>90%) at the Y position of a compound of Formula I and in particular a compound of Formula I-A. The use of deuterated glucose in the deuteride



source in the production of

from pentoxifylline:



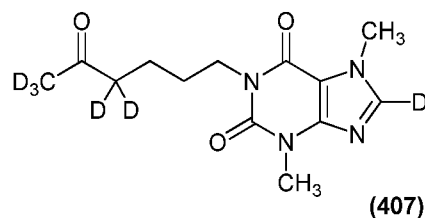
in accordance with this invention will also result in a surprisingly high deuterium incorporation at the indicated position of Compound 133(R).

[53] When a combination of (a) GDH, glucose and a co-factor; (b)(i) GDH, deuterated glucose and a cofactor; or (b)(ii) GDH, D-glucono- δ -lactone, a metal deuteride or a mixed metal deuteride, and a cofactor is used as (a) the hydride source or (b) the deuteride source, respectively, the amount of GDH in the reaction can range from 0.01 wt% to 5 wt%. The term “wt%” means the amount of substance that is the recited percent of the amount of substrate present on a wt/wt basis. In one embodiment, the amount of GDH is between 0.05 wt% and 0.15 wt%. In an alternate embodiment, the amount of GDH is between 0.1 wt% and 0.2 wt%.

[54] An appropriate pH to perform the method according to the present invention means buffer conditions that maintain the pH at between 6.0 and 7.5 throughout the reaction. In one embodiment, the pH of the reaction was maintained at between 6.5 and 7.3. In another embodiment, the pH of the reaction was maintained between 6.0 and 7.0. Typically dropwise addition of KOH is used to maintain the desired pH because the enzymatic reaction generates acid. In one aspect, the pH of the reaction is maintained between 6.90 and 7.05. If the pH of the reaction is allowed to drop below the desired range, the enzyme will typically become irreversibly inactivated and the compound of Formulae I and II subject to acid-catalyzed deuterium-to-hydrogen exchanged.

[55] In one embodiment of the process of the invention, the process is performed at a temperature of about 20° C to 37° C. In one aspect of this embodiment, the temperature is about 29° C to 32° C.

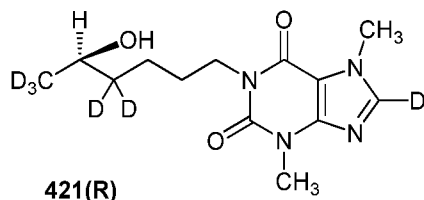
[56] In one embodiment of the process of the invention, the process is performed over a time period of about 12 hours to about 24 hours. In one embodiment, the time period is about 24 hours to about 40 hours. In one embodiment, the time period is about 40 hours to about 72 hours. In one embodiment, the time period is a time period sufficient for less than about 5% of the initial amount of compound of formula (II) to be present.

Example 1. Preparation of Compound 407.

[57] In a 50-L Jacket Glass Reactor, pentoxifylline (900 g) was reacted with deuterium oxide (99% of "D", 2.7 L) in the presence of potassium carbonate (0.25 equiv) in toluene (18 L) at 85-87°C (refluxing) over four hours. The reaction mixture was cooled to 55°C and the agitation was stopped to allow the layers to separate. The reaction mixture was held overnight at 55°C. ¹H NMR analysis of an IPC sample of the organic layer showed the deuterium incorporation was 94.4% "D" at the methyl position. The bottom aqueous layer was collected. Following the same exchange conditions, a second exchange was conducted with a solution of potassium carbonate (0.25 equiv) in deuterium oxide (99% of "D", 2.7 L). After separation, a third exchange was conducted with a solution of potassium carbonate (0.25 equiv) in deuterium oxide (99.8% of "D", 2.7 L). ¹H NMR analysis of an IPC sample of the organic layer showed the deuterium incorporation was 99.6% "D" at the methyl position after three exchanges. The organic layer was concentrated to ca. 5.5 L (6 vol) at 60°C (Batch temperature) and cooled slowly. The solids were formed at 36°C and n-heptane (1.8 L) was added to form a thin slurry. The slurry was stirred at 25°C over the weekend and filtered to provide white solids (825 g, wet). The solids were dried in vacuum oven (28.5 inch Hg) at 45-48°C over night to afford Compound 407 (778.5 g, 84.6% yield). ¹H NMR analysis of Compound 407 showed that the deuterium incorporation was 99.7% "D" at the methyl position. An HPLC purity check by area showed that the purity was 99.96%.

Example 2. Screening of Carbonyl Reductases and Ketoreductases.*ALMAC Carbonyl Reductases*

[58] The ability of the 40 individual carbonyl reductases in the ALMAC Carbonyl Reductase (CRED) Screening Kit to convert Compound 407 to Compound 421(*R*)



was tested as follows:

[59] Into a vial was added 1 mL of a 15 mg/mL solution of the CRED to be tested in 0.1M K₂HPO₄, pH 7.0. To that vial was added 100 µL of a 300 mg/mL solution of glucose; 100 µL of a 10 mg/mL solution of the appropriate co-factor NAD or NADP (as indicated in the table below) in 0.1M K₂HPO₄, pH 7.0; 100 µL of a 20 mg/mL solution of glucose dehydrogenase in 0.1M K₂HPO₄, pH 7.0; and approximately 20 mg of Compound 407 in 50-150 µL of DMSO or MTBE. The sample was shaken or stirred overnight at 30°C. The sample was then extracted with METE or EtOAc and analyzed by TLC and certain select samples by chiral GC/HPLC to determine conversion to Compound 421(*R*) and enantiomeric enrichment. The results are set forth in Table 1.

[60] Table 1. Screening of ALMAC Carbonyl Reductases

Enzyme	Cofactor	Estimated Conversion By TLC	Conversion By HPLC	S/R Ratio of Alcohol
A101	NADP	10%	N/A	N/A
A201	NADP	0%	N/A	N/A
A301	NADP	5%	N/A	N/A
A401	NADP	10%	N/A	N/A
A501	NADP	0%	N/A	N/A
A601	NADP	100%	99.90%	0.2/99.8
A701	NADP	0%	N/A	N/A
A801	NADP	20%	8.20%	92.4/7.6
A901	NADP	50%	32.10%	96.5/3.5
A121	NADP	10%	N/A	N/A
A131	NAD	100%	99.70%	99.7/0.3
A141	NADP	5%	N/A	N/A
A151	NAD	35%	20.10%	35.0/65.0
A161	NAD	100%	99.90%	2.6/97.4
A171	NAD	0%	N/A	N/A
A181	NADP	10%	N/A	N/A
A191	NAD	0%	N/A	N/A
A211	NADP	0%	N/A	N/A

Enzyme	Cofactor	Estimated Conversion By TLC	Conversion By HPLC	S/R Ratio of Alcohol
A221	NAD	0%	N/A	N/A
A231	NADP	5%	N/A	N/A
A241	NADP	0%	N/A	N/A
A251	NAD	100%	99.90%	99.9/0.1
A261	NADP	0%	N/A	N/A
A271	NADP	45%	36.50%	99.4/0.6
A281	NADP	40%	36.70%	73.2/26.8
A291	NADP	90%	97.20%	0.1/99.9
A311	NADP	100%	99.80%	0.1/99.9
A321	NADP	0%	N/A	N/A
A331	NADP	5%	N/A	N/A
A341	NADP	10%	N/A	N/A
A351	NADP	0%	N/A	N/A
A361	NADP	0%	N/A	N/A
A371	NADP	50%	51.60%	73.0/27.0
A381	NADP	0%	N/A	N/A
A391	NADP	0%	N/A	N/A
N501	NADP	0%	N/A	N/A
N701	NADP	0%	N/A	N/A
N121	NADP	0%	N/A	N/A
N131	NADP	5%	N/A	N/A
N151	NADP	10%	N/A	N/A

[61] The results of this experiment demonstrated that ALMAC Carbonyl Reductase CRED A291, CRED A311, CRED A161, or CRED A601 were useful in the process of this invention.

Codexis Ketoreductases.

[62] The CODEXIS Ketoreductase (KRED) Enzyme Screening Kit contained 34 enzymes that used either NADP (Kit KRED-22000) or NAD (Kit KRED-12000) as a co-factor. The screening Kit KRED-22000 contained 22 KRED-NADP enzymes and their screening test results were carried out according to manufacturer's directions using approximately 5 mg of KRED-NADP enzyme and 71 mg of Compound 407 and the appropriate CODEXIS buffer system (KRED-NADPH Recycle Mix A or KRED-NADH Recycle Mix A) for each reaction. Reactions were tested by TLC (data not shown) and selected reactions were tested by chiral HPLC after 40 hours. These results are set forth in Tables 2 and 3. Results indicated by a dash ("–") indicate an insufficient amount of

Compound 421(*R*) or its stereoisomer were produced by TLC to warrant detection by HPLC.

[63] Table 2. Screening of Codexis Ketoreductases in Kit KRED-22000.

KRED-NADP Enzyme	Conversion By HPLC	S/R Ratio of Alcohol
KRED-101	26.30%	29.8/70.2
KRED-102	-	-
KRED-103	-	-
KRED-107	-	-
KRED-112	23.80%	27.2/72.8
KRED-113	-	-
KRED-118	52.80%	7.8/92.2
KRED-119	99.70%	91.6/8.4
KRED-121	-	-
KRED-128	41.80%	72.0/28.0
KRED-129	-	-
KRED-130	99.50%	78.7/21.3
KRED-131	-	-
KRED-137	25.60%	96.4/3.6
KRED-140	-	-
KRED-142	-	-
KRED-147	-	-
KRED-148	76.70%	99.5/0.5
KRED-149	-	-
KRED-164	-	-
KRED-169	65.10%	98.9/1.1
KRED-174	73.90%	99.2/0.8

[64] Table 3. Screening of Codexis Ketoreductases in Kit KRED-12000.

KRED- NADH Enzyme	Conversion By HPLC	S/R Ratio of Alcohol
101	100%	100/0
102	100%	100/0
107	-	-
108	-	-
109	-	-
110	100%	1.5/98.5
112	99.90%	99.8/0.2
113	-	-
119	-	-

121	-	-
124	-	-
126	100%	>99.9/0.1

[65] The above results indicated that CODEXIS Ketoreductases KRED-118 and KRED-NADH 110 were useful in the process of this invention.

Syncore Ketoreductases

[66] SYNCORE Ketoreductase (ES-KRED) Enzyme Screening Kit contained 75 enzymes. Twenty-one ketoreductases (NADH dependent) were tested for the reduction of Compound 407 on 100 mg scale. The CODEXIS buffer system (KRED-NADH Recycle Mix A) was used for these screening tests. The reduction was conducted with 5 wt% of enzyme loading in 50 vol of buffer at 30°C. The reactions were checked by TLC (data not shown) and selected reaction mixtures were checked by chiral HPLC and worked up. Results indicated by a dash (“-”) indicate an insufficient amount of Compound 421(R) or its stereoisomer were produced by TLC to warrant detection by HPLC. The results are summarized in Table 4.

Table 4. Screening of Syncore NADH-dependent Ketoreductases.

Enzyme	Conversion By HPLC	S/R Ratio of Alcohol
ES-KRED-121	99.62%	100/0
ES-KRED-122	-	
ES-KRED-125	-	
ES-KRED-126	100.00%	0/100
ES-KRED-128	99.42%	99.83/0.17
ES-KRED-129	-	
ES-KRED-130	100.00%	100/0
ES-KRED-132	-	
ES-KRED-133	-	
ES-KRED-134	-	
ES-KRED-137	-	
ES-KRED-138	-	
ES-KRED-141	-	
ES-KRED-142	100.00%	100/0
ES-KRED-143	-	
ES-KRED-144	-	
ES-KRED-155	-	
ES-KRED-159	-	
ES-KRED-165	-	
ES-KRED-166	-	
ES-KRED-175	22.71%	100/0

[67] The remaining 54 NADPH dependent ketoreductases from Syncore were also tested for the reduction of Compound 407 (100 mg) using the CODEXIS buffer system (KRED-NADPH Recycle Mix A). The reduction was conducted with 5 wt% of enzyme loading in 50 vol of buffer at 30°C. The reactions were checked by TLC (data not shown) and selected reaction mixtures were checked by chiral HPLC and worked up. Results indicated by a dash (“-”) indicate an insufficient amount of Compound 421(*R*) or its stereoisomer were produced by TLC to warrant detection by HPLC. The results are summarized in Table 5.

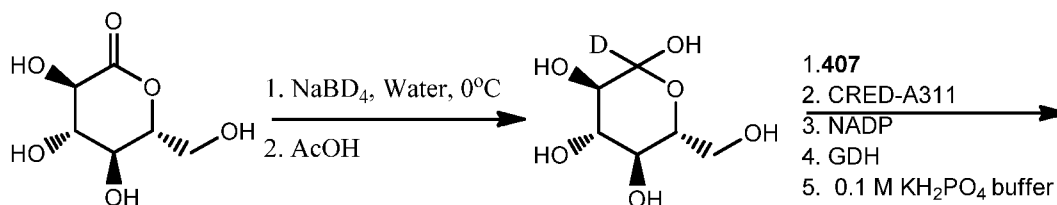
[68] Table 5. Screening of Syncore NADPH-dependent Ketoreductases.

Enzyme	Conversion By HPLC	S/R Ratio of Alcohol
ES-KRED-101	-	-
ES-KRED-102	-	-
ES-KRED-103	-	-
ES-KRED-104	-	-
ES-KRED-105	-	-
ES-KRED-106	-	-
ES-KRED-107	-	-
ES-KRED-108	-	-
ES-KRED-109	-	-
ES-KRED-110	-	-
ES-KRED-111	-	-
ES-KRED-112	-	-
ES-KRED-113	-	-
ES-KRED-114	-	-
ES-KRED-115	-	-
ES-KRED-116	-	-
ES-KRED-117	-	-
ES-KRED-118	-	-
ES-KRED-119	-	-
ES-KRED-120	99.30%	0.18/99.82
ES-KRED-123	-	-
ES-KRED-124	-	-
ES-KRED-127	-	-
ES-KRED-131	99.90%	0.06/99.94
ES-KRED-135	-	-
ES-KRED-136	-	-
ES-KRED-139	-	-
ES-KRED-140	-	-

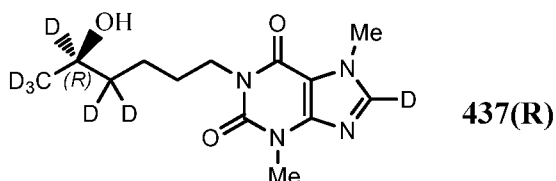
Enzyme	Conversion By HPLC	S/R Ratio of Alcohol
ES-KRED-145	-	-
ES-KRED-146	-	-
ES-KRED-147	-	-
ES-KRED-148	-	-
ES-KRED-149	-	-
ES-KRED-150	-	-
ES-KRED-151	-	-
ES-KRED-152	-	-
ES-KRED-153	-	-
ES-KRED-154	-	-
ES-KRED-156	-	-
ES-KRED-157	-	-
ES-KRED-158	-	-
ES-KRED-160	-	-
ES-KRED-161	-	-
ES-KRED-162	-	-
ES-KRED-163	-	-
ES-KRED-164	-	-
ES-KRED-167	-	-
ES-KRED-168	-	-
ES-KRED-169	99.96%	99.94/0.06
ES-KRED-170	-	-
ES-KRED-171	100%	98.70/1.30
ES-KRED-172	-	-
ES-KRED-173	-	-
ES-KRED-174	-	-

[69] From the above experiments, it was determined that SYNCORE Ketoreductases ES-KRED-120, ES-KRED-126, and ES-KRED-131 were suitable for use in the present invention.

[70] Example 3. Preparation of Compound 437(*R*) from Compound 407 Using CRED-A311 and Deuterated Glucose Generated In Situ.



D(+)-gluconic lactone



a) ***In situ* generation of deuterated Glucose:**

Deuterated glucose (D-[1-²H]₁ Glucose) was prepared according to the procedure described in *Liebigs Ann.Chem.*1992, 1201-1203. D-Glucono-δ-lactone (5 g, 28.09 mmol) was added in one portion to ice-cold water (35 mL, 0-3°C) and stirred for 10 min. A freshly prepared, ice-cold solution of NaBD₄ (0.294 g, 7.02 mmol, 99%D) in 10 mL of water was added slowly during 10 min. The reaction is slightly exothermic (2° to 10°C) and the pH of the reaction was 7.42. Stirring was continued for 30 min, keeping the temperature by cooling to 0-3°C. Acetic acid (0.32 mL, 5.61 mmol) was added and stirring was continued further 30 min.

b) **Preparation of compound 437(R) from compound 407:**

The reaction mixture obtained in step (a) was diluted with 18 mL of water and the solution was heated to 25-30°C. KH₂PO₄ (0.85 g) was added to the mixture and the pH was adjusted to 7 with 4M KOH solution. To this was added 2.5 g (8.8 mmol) of **407**. A solution of NADP (15 mg), GDH (2.5 mg), CRED A311 (25 mg) in 12.5 mL of 0.1 M KH₂PO₄ buffer was added. The resulting solution was stirred at 25-30°C. The pH of the reaction mixture was maintained between 6 and 7 by adding 4M KOH solution dropwise. The reaction was monitored by HPLC and was complete after 12 hours with 99.97% conversion by HPLC. Sodium chloride (12.5 g) was added and stirred for 30 min. The mixture was extracted with ethyl acetate (3 x 25 mL). The organic layer was separated, filtered through celite pad and concentrated to a small volume (~ 5 vol) and product solids were precipitated. Heptanes (20 mL) were added to the slurry (at 40-60°C) over 10 minutes. The slurry was stirred overnight at 20-25°C and filtered. The wet cake was dried at 50°C for 12 hours to afford **437(R)** as a white solid. (2.12 g, 85%

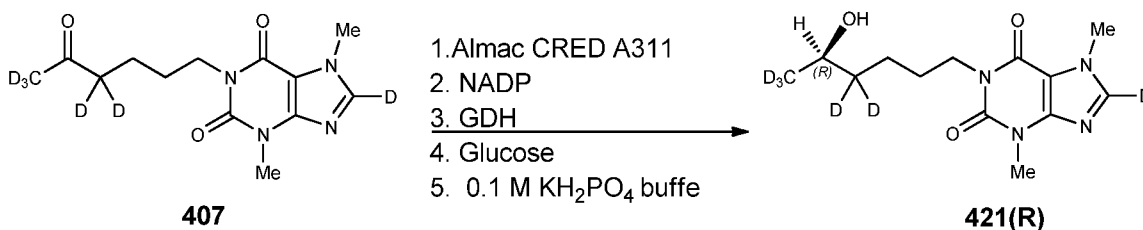
yield). The isolated product purity was >99.95% by HPLC and as a single enantiomer by chiral HPLC.

Compound 437 (*R*) may be further converted to Compound 137(*R*) by treatment with K_2CO_3 and water, as follows:

Preparation of Compound 137(*R*) from Compound 437(*R*).

In a 3-L 3-necked RB flask, Compound 437(*R*) (100 g) was charged followed by water (1.0 L) and K_2CO_3 (0.25 equiv). The reaction mixture was heated to $80 \pm 5^\circ C$ and monitored by 1H NMR. The reaction was complete after 24 hours and worked up after 65 hours. The resulting product was extracted with three times with EtOAc and the solid products from the three extractions combined and re-dissolved in 5 volumes of EtOAc at $60-65^\circ C$. n-heptane (5.5 vol.) was added at $60-65^\circ C$ over 15 minutes and cooled to $20^\circ C$ over night (16 hrs). The slurry was filtered and the wet cake was washed with n-heptane (2x1 vol. to afford product Compound 137(*R*) after drying at $40-50^\circ C$. A total of 92.4 g of Compound 137(*R*) was isolated. HPLC purity was 99.92% (AUC) and chiral selectivity was 100% to “S” enantiomer. The 1H NMR analysis showed 99.2% of “H” at the 8-position in the 3,4,5,7-tetrahydro-1H-purine-2,6-dione ring and 99.4% of “D” at the methyl position.

[71] Example 4.



Preparation of Compound 421(*R*) from Compound 407 Using CRED A131

[72] A 100mL 3-necked RB flask equipped with a heating mantle, a J-Kem thermocouple, magnetic stir bar, a reflux condenser, and a pH probe was charged with CTP-499-A (500 mg, 1.75 mmol), D(+) Glucose (750 mg, 1.5 wt) in 10 mL buffer (0.1M KH_2PO_4 , pH = 7.0) and heated to $25-30^\circ C$. A solution of NADP (15 mg, 3 wt%), GDH (3 mg, 0.6 wt%), ALMAC CRED A311 (30 mg, 6 wt%) in 0.1 M KH_2PO_4 buffer was added and maintained reaction temperature $25-30^\circ C$.

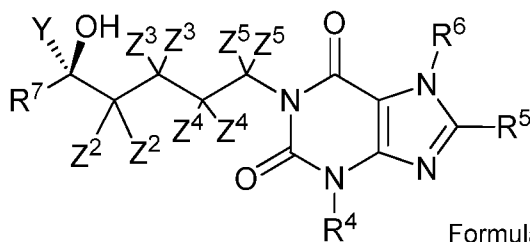
[73] To this added 1mL of methyl-*t*-butyl ether (MTBE). The pH of the reaction mixture was maintained between 6 and 7 adding 4M KOH solution drop-wise. The

reaction was monitored by HPLC and was complete after 29 hours with 99.87A% conversion by HPLC. Sodium chloride (2.5 g, 5 wt) was added and stirred for 20 min. The reaction mixture was extracted with ethyl acetate (3 x 15 mL). The organic layer was separated, filtered through celite pad and concentrated to a small volume (~ 5 vol) and product solids were precipitated. Heptanes (5 mL) was added to the slurry (at 40-60°C) over 5 minutes. The slurry was stirred at 20-25°C and filtered. The wet cake was dried at 50°C for 12 hours to afford CTP-499-G as a white solid. (0.422 g, 84% yield). The isolated product purity was >99.5% by HPLC and single enantiomer by chiral HPLC.

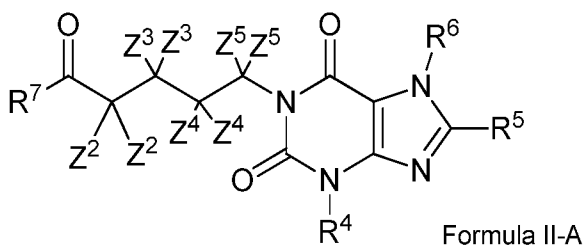
Claims

What is claimed is:

1. A process for the preparation of a compound of Formula I-



A
Formula I-A, comprising the step of reacting a compound of Formula II-A:



Formula II-A

, or a salt thereof, with a hydride source or a deuteride source in the presence of a ketoreductase or carbonyl reductase to form a compound of formula I with an enantiomeric excess of at least 80%, wherein:

each of R^4 , R^6 and R^7 is independently selected from $-CH_3$ and $-CD_3$;

each R^5 is hydrogen or deuterium or a combination thereof;

each Z^2 is the same and is hydrogen or deuterium;

each Z^3 is the same and is hydrogen or deuterium;

each Z^4 is the same and is hydrogen or deuterium;

each Z^5 is the same and is hydrogen or deuterium; and

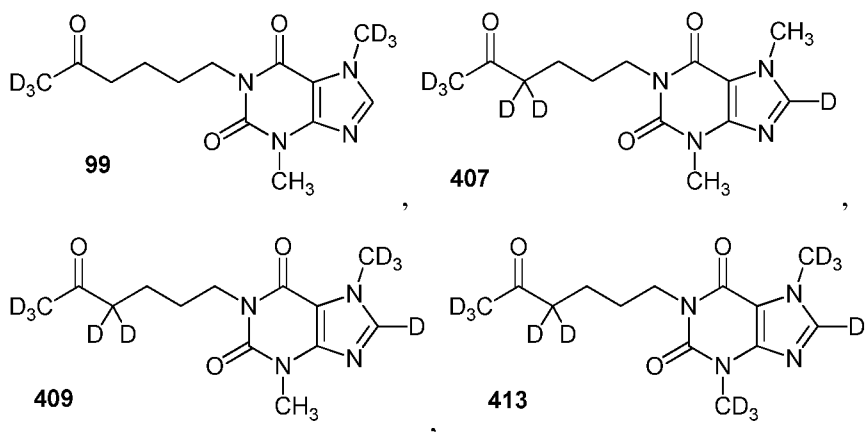
Y is H when a compound of Formula II-A is reacted with a hydride source; or

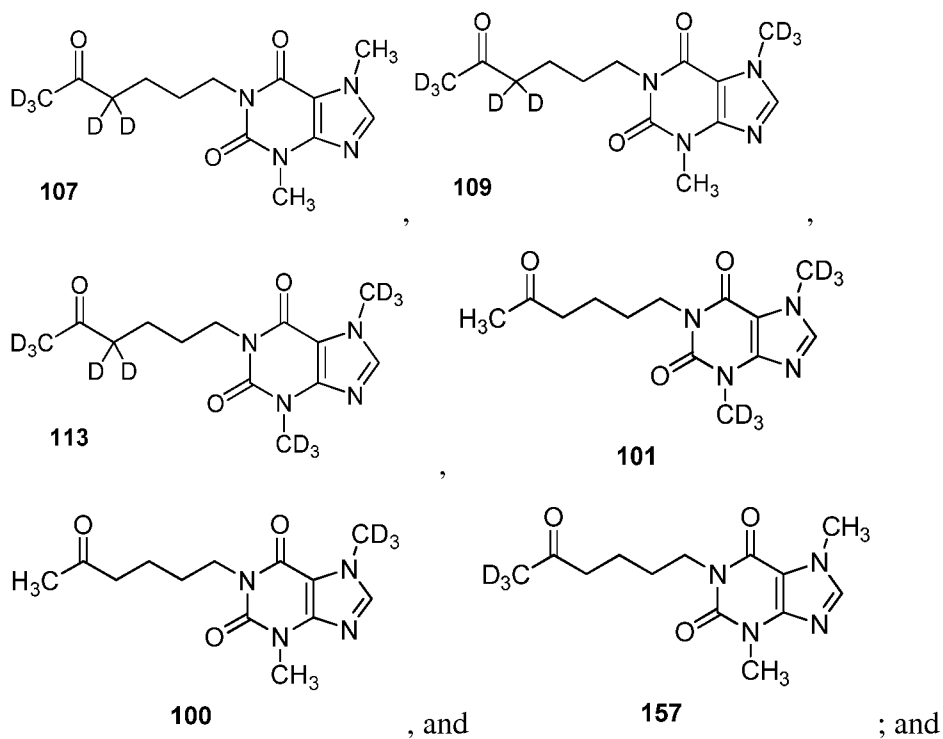
Y is D when a compound of Formula II-A is reacted with a deuteride source,

wherein either R^7 is $-CD_3$ or at least one of Z^2 , Z^3 , Z^4 and Z^5 is deuterium and wherein the amount of deuterium incorporation at each deuterium in R^7 , Z^2 , Z^3 , Z^4 and Z^5 in the compound of formula I is substantially equal to the amount of deuterium incorporation at corresponding deuterium atoms in R^7 , Z^2 , Z^3 , Z^4 and Z^5 in the compound of formula II.

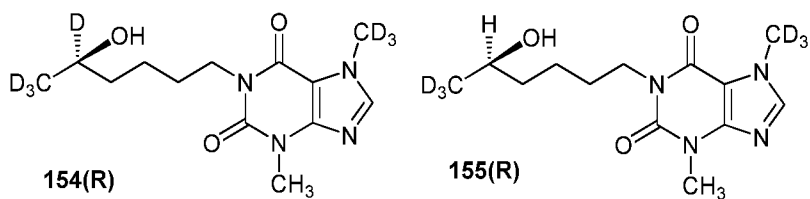
2. The process of claim 1, wherein each R^7 is $-CD_3$.

3. The process of claim 1 or 2, wherein each Z^2 is deuterium.
4. The process of claim 1 or 2, wherein each Z^2 is hydrogen.
5. The process of any one of claims 1-4, wherein each R^5 is deuterium.
6. The process of any one of claims 1-4, wherein each R^5 is hydrogen.
7. The process of any one of claims 1-6, wherein each Z^3 , Z^4 and Z^5 is hydrogen.
8. The process of claim 7, wherein R^6 is $-\text{CH}_3$ and R^7 is $-\text{CD}_3$.
9. The process of claim 8, wherein R^4 is $-\text{CH}_3$.
10. The process of claim 7, wherein R^6 is $-\text{CD}_3$ and R^7 is $-\text{CD}_3$.
11. The process of any one of claims 1-6, wherein each Z^3 , Z^4 and Z^5 is deuterium.
12. The process of claim 11, wherein each R^6 and each R^4 is $-\text{CD}_3$.
13. The process of claim 1, wherein:
 - a. the compound of Formula II-A is selected from any one of:

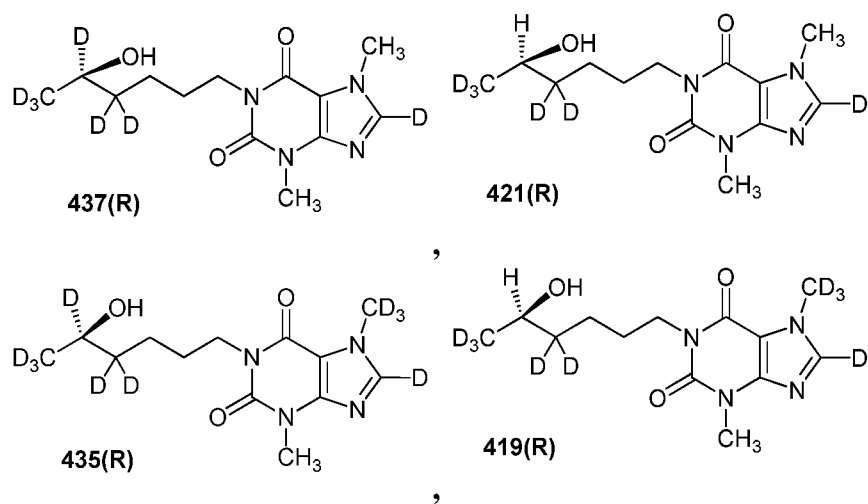


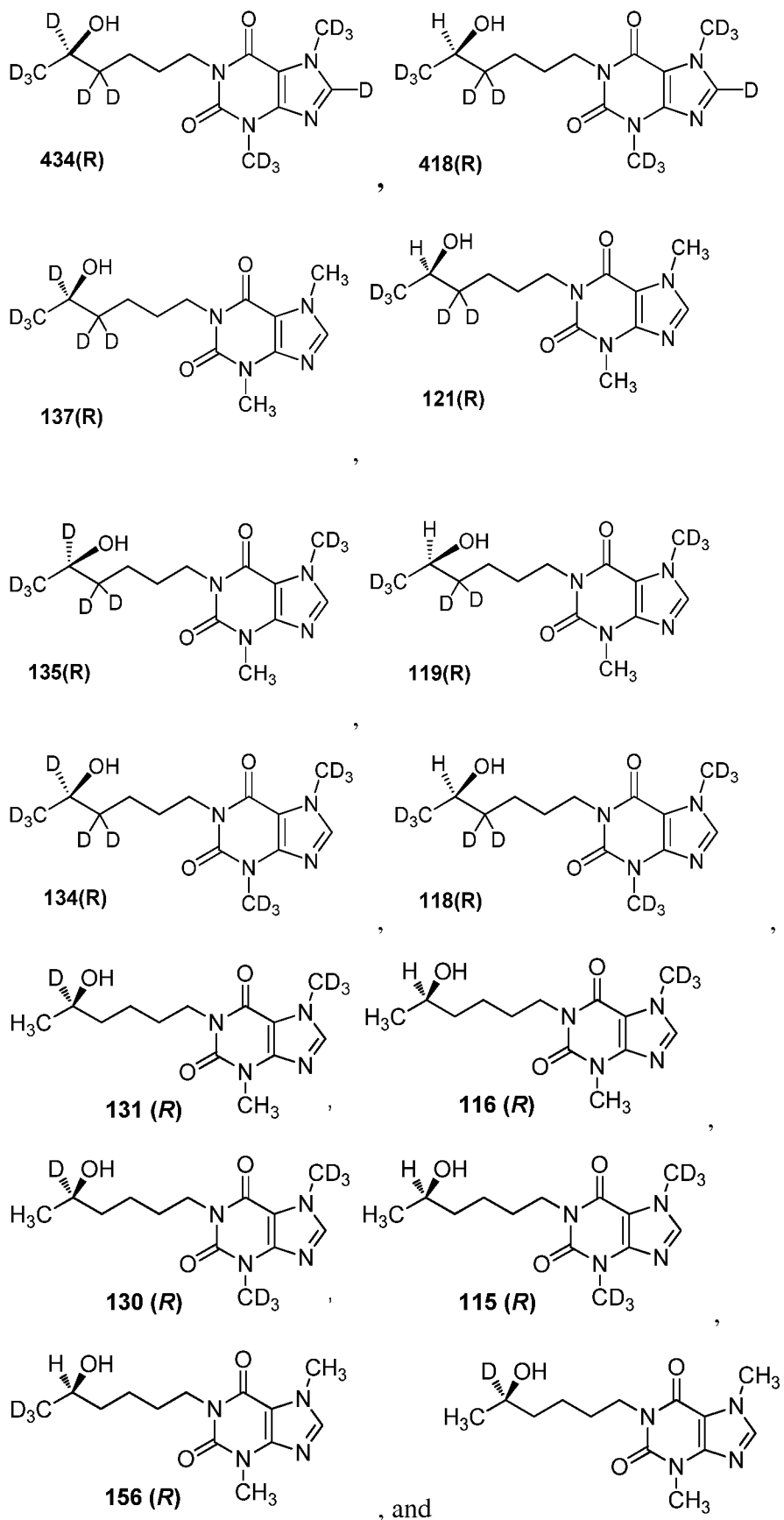


b. the compound of Formula I-A is selected from any one of the

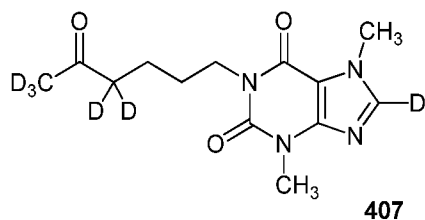


following



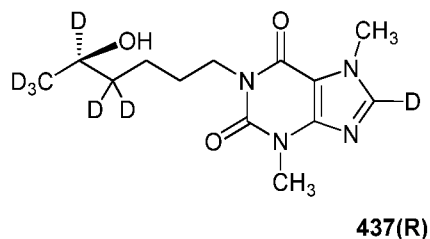


14. The process of claim 1, wherein:



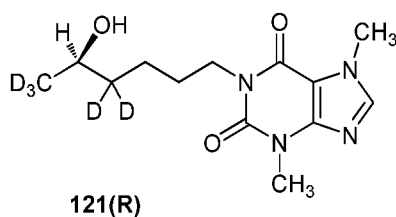
the compound of Formula II-A is

(Compound



407); and the compound of Formula I-A is
(Compound 437(R)).

15. The process of claim 14, further comprising the step of converting



Compound 421(R) to Compound 121(R):

16. The process of claim 1, wherein the hydride source or deuteride source is (i) a cofactor selected from NAD, NADH, NADP and NADPH, (ii) a reducing sugar and (iii) a dehydrogenase that dehydrogenates the reducing sugar.
17. The process of claim 16, wherein Y is H; and the hydride source is (i) a cofactor selected from NAD, NADH, NADP and NADPH, (ii) glucose and (iii) glucose hydrogenase.
18. The process of claim 16, wherein Y is D; and the deuteride source is (i) a cofactor selected from NAD and NADP, (ii) deuterated glucose, and (iii) glucose hydrogenase.

19. The process of claim 18, wherein the deuteride source is (i) a cofactor selected from NAD and NADP, (ii) D-glucono- δ -lactone, and (iii) a metal deuteride or a mixed metal deuteride.
20. The process of claim 19, wherein the metal deuteride or mixed metal deuteride is NaBD₄.
21. The process of any one of claims 1-20, wherein the step of reacting a compound of Formula II-A or a salt thereof with a hydride source or a deuteride source is performed at a pH between 6.0 and 7.5.
22. The process of claims 21, wherein the appropriate pH is between 6.90 and 7.05.
23. The process of any one of claims 1-22, wherein the ketoreductase or carbonyl reductase is CRED A311.

INTERNATIONAL SEARCH REPORT

International application No

PCT/US2011/050138

A. CLASSIFICATION OF SUBJECT MATTER
 INV. C07B59/00 C07D473/04 C12P17/18
 ADD.

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
 C07B C07D C12P

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, CHEM ABS Data, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	WO 2009/108383 A2 (CONCERT PHARMACEUTICALS INC [US]; TUNG ROGER D [US]; LIU JULIE F [US];) 3 September 2009 (2009-09-03) cited in the application the whole document	1-23
A	----- ELZBIETA PEKALA ET AL.: "Enantioselective biotransformation of pentoxifylline into lisofylline using wine yeast biocatalysis", ACTA POLONIAE PHARMACEUTICA, vol. 64, no. 2, 2007, pages 109-113, XP002660610, the whole document	1-23
A	----- EP 0 435 153 A2 (HOECHST AG [DE]) 3 July 1991 (1991-07-03) the whole document ----- -/-	1-23



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier document but published on or after the international filing date

"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"&" document member of the same patent family

Date of the actual completion of the international search

5 October 2011

Date of mailing of the international search report

11/11/2011

Name and mailing address of the ISA/

European Patent Office, P.B. 5818 Patentlaan 2
 NL - 2280 HV Rijswijk
 Tel. (+31-70) 340-2040,
 Fax: (+31-70) 340-3016

Authorized officer

Diederer, Jeroen

INTERNATIONAL SEARCH REPORT

International application No

PCT/US2011/050138

C(Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	EP 0 435 152 A2 (HOECHST AG [DE]) 3 July 1991 (1991-07-03) the whole document -----	1-23

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No

PCT/US2011/050138

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 2009108383	A2	03-09-2009	
		AU 2009217680 A1	03-09-2009
		CA 2716788 A1	03-09-2009
		CN 101998957 A	30-03-2011
		EA 201001391 A1	30-08-2011
		EP 2265334 A2	29-12-2010
		EP 2265612 A1	29-12-2010
		JP 2011513307 A	28-04-2011
		JP 2011513309 A	28-04-2011
		KR 20100121527 A	17-11-2010
		US 2009239886 A1	24-09-2009
		WO 2009108375 A1	03-09-2009

EP 0435153	A2	03-07-1991	
		AT 137237 T	15-05-1996
		DE 3942871 A1	27-06-1991
		DE 59010302 D1	30-05-1996
		DK 0435153 T3	05-08-1996
		ES 2086359 T3	01-07-1996
		GR 3019860 T3	31-08-1996
		JP 4210688 A	31-07-1992
		JP 7107063 B	15-11-1995
		US 5407815 A	18-04-1995

EP 0435152	A2	03-07-1991	
		AT 145247 T	15-11-1996
		DE 3942872 A1	27-06-1991
		DE 59010566 D1	19-12-1996
		DK 0435152 T3	21-04-1997
		ES 2096574 T3	16-03-1997
		GR 3021611 T3	28-02-1997
		JP 2726760 B2	11-03-1998
		JP 6009633 A	18-01-1994
