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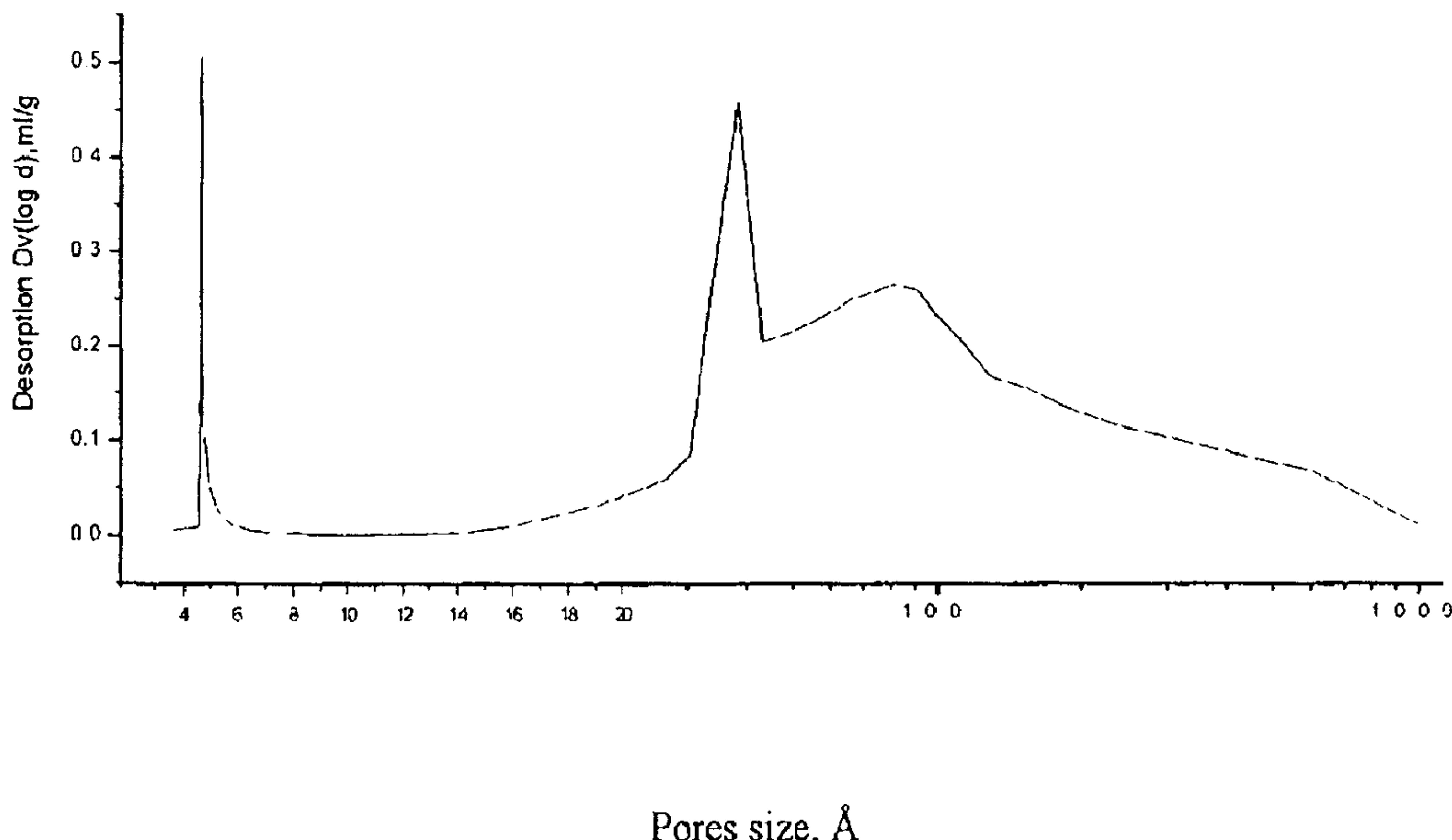
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Pores size, Å

(57) **Abrégé/Abstract:**

A catalyst for catalytically cracking hydrocarbon oils contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70% of the <2 nm pores, 5-70% of the 2-4 nm pores, 0-10% of the 4-6 nm pores,

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(57) **Abrégé(suite)/Abstract(continued):**

20-80% of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm. The catalyst of this invention has a large BET pore volume, a high capacity for cracking heavy oils, and a high capacity for resisting coking.

Abstract

A catalyst for catalytically cracking hydrocarbon oils contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70% of the <2 nm pores, 5-70% of the 2-4 nm pores, 0-10% of the 4-6 nm pores, 20-80% of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm. The catalyst of this invention has a large BET pore volume, a high capacity for cracking heavy oils, and a high capacity for resisting coking.

A catalytic cracking catalyst and the preparation and use thereof

Technical field

This invention relates to a catalyst for catalytically cracking hydrocarbon oils and its preparation method, especially to a catalytic cracking catalyst for producing light olefins and its preparation method.

Background arts

The catalysts for preparing light olefins by catalytic cracking or pyrolysis with petroleum hydrocarbons as feed stocks comprise three types: the first type is supported metal catalysts with oxides as substrates such as the catalysts disclosed in US3,541,179, US3,647,682, DD225,135, and SU1214726, which use SiO_2 , Al_2O_3 or other oxides as substrates to support metal elements of Groups IIB, VB, VIIIB, and VIIIB. This kind of catalysts are merely suitable for the preparation of light olefins by the catalytic cracking of light feed stocks (boiling range $<220^\circ\text{C}$). The second type is composite oxide catalysts such as the catalysts disclosed in US3,725,495 and US3,839,485, which use ZrO_2 and/or HfO_2 as main components and contain active alumina, at least one component selected from Cr_2O_3 , MnO , and Fe_2O_3 , and at least one component selected from oxides of alkali metals or alkali earth metals, and the catalyst disclosed by DD152,356, which uses amorphous $\text{SiO}_2 \cdot \text{Al}_2\text{O}_3$ as the catalyst for cracking hydrocarbon oils to prepare light olefins. The third type of catalysts is the zeolites containing catalysts, especially MFI-structured zeolite (five-member ring high silica zeolite) containing ones. This type of catalysts can be used alone or as catalytic cracking additive.

JP60-222428 discloses a process for preparing $\text{C}_2^\sim\text{-C}_4^\sim$ by catalytically cracking $\text{C}_5\text{-C}_{25}$ paraffins at $600\text{-}750^\circ\text{C}$ using a catalyst containing ZSM-5 zeolite and Al_2O_3 .

CN1205306C discloses a catalyst for preparing light olefins by cracking petroleum hydrocarbons, which catalyst contains 0-70 wt.% of clay, 5-99 wt.% of inorganic oxides and 1-50 wt.% of zeolites based on the weight of the catalyst, wherein said zeolite is 25-100 wt.% of MFI-structured zeolite and 0-75 wt.% of Y-zeolite, characterized in that said MFI-structured zeolite contains phosphor and a transition metal M

and has an anhydrous chemical formula of $(0\text{-}0.3)\text{Na}_2\text{O}\cdot(0.3\text{-}5)\text{Al}_2\text{O}_3\cdot(1\text{-}10)\text{P}_2\text{O}_5\cdot(0.7\text{-}15)\text{M}_x\text{O}_y\cdot(0\text{-}10)\text{RE}_2\text{O}_3\cdot(70\text{-}98)\text{SiO}_2$ based on the mass of the oxide, wherein M is one or two metals selected from Fe, Co, Ni, Cu, Zn, Mo, and Mn..

CN1069016A discloses a process for preparing ethylene by cracking heavy petroleum hydrocarbons at 650-900°C using a catalyst containing 30-90 wt.% of SiO_2 , 20-70 wt.% of Al_2O_3 , 0.5-30 % by weight of oxides of alkali metals or alkali earth metals, and 1-30 wt.% of faujasite.

CN1093101A discloses a cracking catalyst for producing light olefins, which catalyst consists of 0-70% of clay, 5-99% inorganic oxides, and 1-50% zeolites (based on the weight of the catalyst), wherein the zeolite is a mixture of 0-25 wt.% of REY or high silica Y-zeolite and 75-100 wt.% of five-member ring high silica zeolite containing phosphor and rare earths.

CN1048428C discloses a catalyst for converting petroleum hydrocarbons to light olefins, which catalyst consists of 0-70 wt.% of clay, 5-90 wt.% of inorganic oxides and 10-35 wt.% of zeolites, wherein the zeolite consists of 20-75 wt.% of five-member ring high silica zeolite containing phosphor and rare earths, 20-75 wt.% of high silica Y-zeolite, and 1-25 wt.% of Y-zeolite containing rare earths.

CN1222558A discloses a catalyst for preparing light olefins by catalytic pyrolysis, which catalyst has the following composition (based on the weight of the catalyst): 10-70 wt.% of clay, 5-85 wt.% of inorganic oxides and 1-50 wt.% of zeolites, wherein the zeolite is 0-25 wt.% of Y-zeolite and 75-100 wt.% of five-member ring high silica zeolite containing phosphor and aluminum or magnesium or calcium, and said high silica zeolite is ZSM-5, ZSM-8 or ZSM-11 type zeolite containing 2-8% phosphor and 0.3-3% aluminum or magnesium or calcium (in terms of oxide) with a silica/alumina ratio of 15-60.

CN1069682C discloses a pillared interlayered clay catalyst for preparing ethylene, propylene, and butene by the catalytic pyrolysis of heavy oils, which catalyst consists of 30-75 wt.% of aluminum cross-linked pillared interlayered clay, 10-40 wt.% of inorganic oxide binders containing aluminum or silicon or zirconium, 0-30 wt.% of high silica zeolite with the five-member ring structure, 0-10 wt.% of a

modifying component selected from magnesium, aluminum, phosphor, tin, polyethylene glycol or their mixture, and 0-50 wt.% of clay of the kaolin family.

CN1660967A discloses a catalyst for increasing the yield of ethylene and propylene by catalytic pyrolysis, which catalyst contains 7-70 wt.% of clay, 3-70 wt.% of mesopore silica-alumina materials, 5-80 wt.% of inorganic oxides, and 5-60 wt.% of MFI-structured zeolite

CN1354224A discloses a catalytic cracking catalyst for producing gasoline rich in isomeric alkanes, propylene, and isobutane, which catalyst consists of 0-70 wt.% of clay, 5-90 wt.% of inorganic oxides, and 1-50 wt.% of zeolites based on the weight of the catalyst, wherein said zeolite is a mixture of (1) 20-75% high silica Y-zeolite having a silica/alumina ratio of 5-15 and containing 8-20 wt.% of rare earths in terms of RE_2O_3 and (2) 20-75% high silica Y-zeolite having a silica/alumina ratio of 16-50 and containing 2-7 wt.% of rare earths in terms of RE_2O_3 and (3) 1-50% β -zeolite or mordenite or ZRP-zeolite based on the zeolite weight. By using this catalyst, the content of isomeric alkanes in gasoline can be increased together with the production of propylene and isobutane being increased.

CN1566267A discloses a catalytic pyrolysis process for preparing ethylene and propylene, which comprises introducing a preheated petroleum hydrocarbon feed stock into a lift pipe reactor, contacting the feed with a hot catalyst containing a five-member ring high silica zeolite, conducting reaction under catalytic pyrolysis conditions, separating the reaction products and spent catalyst. The reaction products are conveyed to the subsequent separation system for product separation, and the spent catalyst is returned to the reactor after being stripped and regenerated for recycle, wherein said five-member ring high silica zeolite contains phosphor and transition metals.

CN1043520A discloses a cracking catalyst, the substrate of which is 0-70 wt.% of clay and 5-99 wt.% of inorganic oxides, and the active component is a mixture of 1-50 wt.% of ZSM-5 and Y-type molecular sieve. In the active component, ZSM-5 accounts for 75-100% by weight and Y-type molecular sieve accounts for 0-25%.

CN1508223A discloses a hydrogenation catalyst wherein the substrate contains alumina, active component comprises molybdenum and/or W and Ni, the pore of a size of 2-6nm accounts for 70-90% of the total pore volume.

The content of macropores in the prior art catalysts is low, so these catalysts show an insufficient capacity for cracking heavy oils when used in catalytically cracking heavy oils and provide low yields when used for preparing light olefins and propylene by catalytic cracking.

Content of the invention

One of the technical problems to be solved by the present invention is to provide a catalyst for catalytically cracking hydrocarbon oils; the second technical problem to be solved is to provide a process for preparing the above catalyst; and the third problem to be solved is to provide a method for applying the catalyst in catalytic cracking, which method can increase the yield of light olefins.

This invention provides a catalyst for catalytically cracking hydrocarbon oils, which catalyst contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70% of the <2 nm pores, 5-70% of the 2-4 nm pores, 0-10% of the 4-6 nm pores, 20-80% of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm.

In a particular embodiment there is provided a catalyst for catalytically cracking hydrocarbon oils, which catalyst contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70% of the <2 nm pores, 5-70% of the 2-4 nm pores, 0-10% of the 4-6 nm pores, 20-80% of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm, the pore volume of the catalyst is measured according to RIPP151-90, said catalyst contains 60-95 wt.% of a substrate, 5-40 wt.% of a molecular sieve, and said molecular sieve contains 25-100 wt.% of MFI-structured zeolite, 0-75 wt.% of Y-zeolite, and 0-20 wt.% of β -zeolite, and said alumina is derived from alumina and/or its precursors, said precursor of alumina is

pseudo-boehmite or its mixture with one or more of alumina sol or phospho-alumina sol.

This invention provides a process for preparing a catalytic cracking catalyst, which process comprises the steps of mixing a substrate comprising alumina and/or its precursors with a molecular sieve, slurring and spray-drying the mixture, characterized in that a pore-extender is introduced in the mixing step and said pore-extender is one or more selected from boric acid and salts of alkali metals. The weight ratio of the pore-extender to the substrate is 0.1:100-15:100 based on the weight of the substrate.

This invention provides a catalytic cracking process, which comprises a step of contacting a hydrocarbon oil with a catalyst, characterized in that said catalyst comprises the catalyst according to the present invention.

Because a pore-extender is introduced in the preparation of the catalyst of this invention, the pore volume of macropores increases and thus raises the capacity of the catalyst for cracking heavy oils, coke-tolerance and coke-resistance of the substrate, the utilization rate of the active components, and the retention ratio of the crystallinity of the molecular sieve after deactivation. When metal halides are introduced during preparation, the abrasion resistance of the catalyst can be raised. The catalytic cracking process provided by this invention has a high capacity for cracking heavy oils and when the prepared catalyst contains MFI-structured molecular sieve, the yield of propylene in catalytic cracking is high. For example, the catalyst prepared by this invention contains 20 wt.% of a molecular sieve and 80% by weigh of substrate, wherein the molecular sieve contains 10 wt.% of REHY-zeolite and 90 wt.% of ZRP-zeolite. The substrate contains 26 wt.% of pseudo-boehmite and alumina sol, 69 wt.% of kaolin, 5% of the weight of TiO_2 . Potassium sulfate is used as a pore-extender in the preparation, and its amount is 7.4% of the weight of the substrate. The pore volume of the catalyst measured by BET method is 0.256 ml/g, and the abrasion index is 2% by weight, while the pore volume of the catalyst prepared according to a prior process for preparing the DCC catalyst containing the same amount of molecular sieve is 0.185 ml/g and the abrasion index is 2% by weight. When using 30 m.% of residual oil + 70 m.% of VGO as a feed stock and conducting the catalytic cracking reaction under the conditions of a temperature of 680°C, a catalyst/oil weight ratio of 10, a water/oil mass ratio of 0.8:1, and a weight hourly space velocity of 10 h^{-1} , the catalyst of this invention presents a propylene yield of 21.88% by weight, a coke yield of 1.09% by weight, and a heavy oil yield of 1.05% by weight, while the catalyst prepared by a prior art process presents a propylene yield of 19.26% by weight, a coke yield of 1.28% by weight, and a heavy oil yield of 1.55% by weight.

Brief description of the drawings

Fig. 1 illustrate the pore distribution of the catalyst of Example 1.

Specific mode for carrying out the invention

The singular forms “a”, “an”, and “the” include plural referents

unless the context clearly dictates otherwise.

The catalyst for catalytically cracking hydrocarbon oils according to the present invention contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70%, preferably 5-60%, of the <2 nm pores, 5-70%, preferably 10-60%, more preferably 15-50%, of the 2-4 nm pores, 0-10% of the 4-6 nm pores, 20-80%, preferably 25-70%, more preferably 30-60%, of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm.

The catalyst according to the present invention has a ratio of the volume of 6-20 nm pores to that of 2-4 nm pores being 0.5-4.

The volume of the 6-10 nm pores in the catalyst according to the present invention accounts for 10-50%, preferably 15-40%.

The catalyst according to the present invention preferably contains 60-95 wt.% of a substrate, 5-40 wt.% of a molecular sieve, and said molecular sieve contains 25-100 wt.% of MFI-structured zeolite, 0-75 wt.% of Y-zeolite, and 0-20 wt.% of β -zeolite. The content of alumina in the substrate coming from alumina and/or its precursors is 5-100% by weight, and the content of other substrate components does not exceed 95% by weight. The pore volume of said catalyst measured by the BET method is 0.19-0.4 ml/g.

In the catalyst according to the present invention, said substrate contains one or more types of alumina derived from alumina or its precursors, and the content of alumina is preferably 5-80% by weight. The alumina and its precursor are preferably one or more of alumina sol, phospho-alumina sol, various aluminum-containing salts (such as various aluminates, and sulfate, nitrate, and halides of aluminum), γ -alumina, η -alumina, θ -alumina, and χ -alumina, hydrated alumina with the structure of pseudo-boehmite, hydrated alumina with the structure of diasporite, hydrated alumina with the structure of gibbsite, and hydrated alumina with the structure of bayerite. More preferably, said alumina and its precursor are pseudo-boehmite or mixtures of pseudo-boehmite with one or more of alumina and other precursors of alumina.

The catalyst according to the present invention may also contain one or more of clay and oxides of Groups IIIA and IVA non-aluminum elements. Said oxides of non-aluminum elements are derived from one or

more of the oxides of said non-aluminum elements or their precursors. For example, silica and its precursors may be one or more selected from silica sol, water glass, silicates, silica-alumina sol, silica-alumina gel, and various organo-silicon compounds, preferably water glass and/or silica sol. The content of clay and said non-aluminum oxides does not exceed 95% by weight based on the weight of the substrate, and the content of clay preferably does not exceed 60% by weight. It is preferable that the weight ratio of the non-aluminum oxide to the alumina substrate in the substrate is 1: (0.3-1) calculated in oxide.

In the catalyst according to the present invention, said zeolite is one or more of MFI-structured zeolite, Y-zeolite, and β -zeolite. Said Y-zeolite is preferably one or more of Y-zeolite containing phosphor and/or rare earths, ultrastable Y-zeolite, ultrastable Y-zeolite containing phosphor and/or rare earths, HY-zeolite, and HY-zeolite containing phosphor and/or rare earths. More preferably, said zeolite is one or more of ultrastable Y-zeolite, REY, or REHY. Said MFI-structured zeolite is one or more selected from ZSM-5 zeolite, ZRP-zeolite, and their modifications such as the modified MFI-structured zeolite containing phosphor and transition metals disclosed in CN 1465527A, i.e., ZSM-5 zeolite modified with phosphor and one metal selected from Fe, Co, and Ni, having an anhydrous chemical formula of $(0.0-0.3)Na_2O \cdot (0.5-5)Al_2O_3 \cdot (1.3-10)P_2O_5 \cdot (0.7-15)M_xO_y \cdot (70-97)SiO_2$ calculated in the mass of the oxide, where x denotes the atom number of M; y denotes the atom number of O; and M is one of Fe, Co, and Ni.

In the catalyst according to the present invention, said substrate preferably also contains metal components coming from halides of Groups IIA, IB, IIB, and IVB metals, and the content of said metal component does not exceed 15% by weight based on the weight of the substrate, preferably being 0.1-12% by weight, and more preferably, being 0.1-6% by weight. Said metal component is more preferably one or more of Groups IVB and IIA metals, and most preferably, it is Ti and/or Mg. If the substrate contains said metal components, the abrasion resistance of the catalyst is raised.

The pore volume of the catalyst provided by the present invention measured by the nitrogen adsorption volumetric method is 0.19-0.4 ml/g,

preferably 0.196-0.26 ml/g. For the nitrogen adsorption volumetric method, please refer to analytical method RIPP151-90 in "Yang Cuiding et al, Analytic Methods in Petroleum Chemical Industry" (RIPP Experimental Methods), Science press, 1990.

Figure 1 illustrate the pore distribution of the catalyst of Example 1, which is measured by the nitrogen adsorption volumetric method. As can be seen from the figure, there is a distinct adsorption peak at 6-20nm, showing that said catalyst comprises pores of 6-20nm.

In the catalyst preparation process according to the present invention, the weight ratio of said pore-extender to the substrate is preferably 0.1:100-10:100. Said salt of alkali metals is preferably one or more of soluble salts of alkali metals K, Na, or Li such as borates, phosphates, sulfates, nitrates, carbonates, or hydrochloride.

In the catalyst preparation process according to the present invention, said technique for mixing and slurring the substrate and molecular sieve is well known to the skilled in the art. It is possible to slurry the substrate and molecular sieve separately, and then mix the two slurries, or mix and slurry a part of the substrate in the preparation of the substrate, and then introduce the molecular sieve and the remaining substrate and slurry, or introduce the substrate into the molecular sieve slurry and then slurry. Said pore-extender is introduced into the slurry before spray drying. It is preferable that the pore-extender is introduced into the substrate-containing slurry. After introducing the pore-extender, slurring is performed to dispense the pore-extender into the slurry. The slurring step is conducted for at least 5 min, preferably 10-90 min. The slurry containing pore-extender is aged in static state under the temperature of 50-80°C for a time of 0.5-3 hr after the pore-extender is incorporated thereinto.

Phosphoric acid can be introduced in the step of mixing in the catalyst preparation process according to the present invention.

In the catalyst preparation process according to the present invention, one or more of halides of Groups IIA, IB, IIB, and IVB metals can be introduced into the slurring step. Said metal halide is preferably introduced after introducing the pore-extender and before spray drying. The amount of the introduced metal halide does not exceed 15% by

weight, preferably 0.1-12% by weight, and more preferably 0.1-6% by weight based on the weight of the substrate. Said metal halide is preferably one or more of the halides of Groups IVB and IIA metals, more preferably one or more of the halides of Ti and/or Mg such as TiCl_4 , MgF_2 , and MgCl_2 . The introduction of the metal halide can improve the abrasion resistance of the prepared catalyst.

In the catalyst preparation process according to the present invention, the amount of the substrate and molecular sieve is preferably such that the finally obtained catalyst contains 60-95 wt.% of the substrate and 5-40 wt.% of the molecular sieve.

In the catalyst preparation process according to the present invention, said alumina is preferably one or more of γ -alumina, η -alumina, θ -alumina, and χ -alumina. Said precursor of alumina is preferably alumina sol, phospho-alumina sol, various aluminum-containing salts (such as various aluminates, and sulfate, nitrate, and halide of aluminum), hydrated alumina with the structure of pseudo-boehmite, hydrated alumina with the structure of diaspore, hydrated alumina with the structure of gibbsite, and hydrated alumina with the structure of bayerite. More preferably, said precursor of alumina is pseudo-boehmite or its mixtures with one or more selected from alumina sol, phospho-alumina sol, hydrated alumina with the structure of diaspore, hydrated alumina with the structure of gibbsite, and hydrated alumina with the structure of bayerite. It is preferable that said alumina and/or its precursor are pseudo-boehmite or mixtures of pseudo-boehmite with one or more of alumina or other alumina precursors. More preferably, said substrate contains pseudo-boehmite and alumina sol. The content of pseudo-boehmite in the substrate is preferably 5-95% by weight calculated in oxide, based on the weight of the substrate.

In the catalyst preparation process according to the present invention, said substrate may also contain the substrates commonly used in other catalytic cracking catalysts such as one or more of non-aluminum inorganic oxide substrates and clay. Said non-aluminum inorganic oxide substrate is preferably one or more of the oxides of Groups IIIA and IVA elements and their precursors and more preferably, it is one or more of oxides of silicon, boron, tin, lead, gallium, and indium and their oxide

precursors. Preferably, the amounts of various components are such that, the content of alumina and/or its precursor is 5-100% by weight calculated in alumina; the content of the non-aluminum inorganic oxide does not exceed 95% by weight calculated in oxide; and the content of clay does not exceed 95% by weight, based on the weight of the substrate. More preferably, the content of alumina and/or its precursors is 5-80% by weight and the content of clay does not exceed 60% by weight.

In the catalyst preparation process according to the present invention, said oxide of silicon and their precursors are one or more of silica gel, silica sol, silica hydrosol, water glass, silicates, organo-silicon compounds, silica-alumina sol, and silica-alumina gel.

In the catalyst preparation process according to the present invention, said clay is one or more of clay customarily used for cracking catalysts such as one or more of kaolin, halloysite, montmorillonite, kieselguhr, endellite, soapstone, rectorite, sepiolite, attapulgite, hydrotalcite, and bentonite.

In the catalyst preparation process according to the present invention, said molecular sieve is one or more selected from the molecular sieve commonly used for catalytic cracking, preferably an MFI-structured zeolite or mixtures of the MFI-structured zeolite with one or more selected from Y-type molecular sieve, and β -zeolite.

In the catalyst preparation process according to the present invention, said spray drying is known in the art and there is no special requirement for it. For example, the temperature of the tail gas in spray drying is 100-300°C.

The catalyst preparation process according to the present invention may also comprise the steps of calcining, washing, and drying. Said methods of calcining, washing, and drying are known in the art and there is no special requirement for them. For example, the calcination temperature is 300-700°C; the drying temperature is 100-300°C; and the catalyst is washed with deionized water until the content of sodium oxide in the catalyst does not exceed 0.5% by weight.

In the catalytic cracking process according to the present invention, said conditions for contacting the catalyst with hydrocarbon oils are known in the art. For example, the contacting temperature is 400-750°C.

According to the catalytic cracking process according to the present invention, when the catalyst used contains MFI-structured zeolite, the reaction temperature is preferably 480°C-560°C, and steam is introduced during the reaction with the ratio of steam to the raw oil being 0.7-14:1.

According to the instant catalytic cracking process, besides the catalyst provided by the present invention, said catalyst may also contain other cracking catalysts. For example, when the catalyst according to the present invention contains MFI-structured zeolite, the catalyst according to the present invention may be used solely, or as an additive for producing light olefins after mixing with other cracking catalysts. When used as an additive, the content of the catalyst according to the present invention is 1-30% by weight, preferably 5-30% by weight based on the total weight of the catalyst.

Cracking catalysts with macropore substrates can be prepared by the catalyst preparation process of this invention. The catalyst according to the present invention can be used as an additive or catalyst in the catalytic cracking of hydrocarbon oils, and it is especially suitable for the catalytic cracking of heavy oils. Said hydrocarbon oils include, for example, atmospheric gas oil, vacuum gas oil, atmospheric residual oil, and vacuum residual oil. The process according to the present invention can be used for producing light olefins, especially propylene.

The present invention is further illustrated with the following examples, but is not intended to be limited thereby

In the examples and comparative examples, ZRP-zeolite, REHY-zeolite, and β -zeolite are all the products of Catalyst Plant, Qilu Petrochemicals Co., wherein ZRP-zeolite has a $\text{SiO}_2/\text{Al}_2\text{O}_3$ mole ratio of 30 and contains 2.0 wt.% of RE_2O_3 and 4.0 wt.% of P_2O_5 . For the determination of abrasion index and pore volume, reference is made to RIPP29-90 and RIPP151-90 in "Yang Cuiding et al, Analytic Methods in Petroleum Chemical Industry" (RIPP Experimental Method), Science press, 1990".

Example 1

20 kg deionized water was mixed with 11.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight). The mixture was slurried and adjusted to a pH value of 3

with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and slurried for 5 min, and then added with 1.75 kg potassium borate (analytically pure), the mixture being slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixed slurry was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4 (adjusted with hydrochloric acid). Then the temperature was decreased to 55°C and added with 13.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight). The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 2.0 kg REHY-zeolite and 9.0 kg ZRP-zeolite) was added. 2 kg TiCl₄ was added and the mixture was stirred uniformly. The resultant slurry was spray dried and washed to remove free Na ions, yielding catalyst A after being dried. The pore distribution is shown in Table 1.

Example 2

20 kg deionized water was mixed with 11.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight). The mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and slurried for 5 min, and then added with 3 kg potassium sulfate (industrially pure, 98wt%), the mixture being slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixed slurry was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4 (adjusted with hydrochloric acid). Then the temperature was decreased to 55°C and added with 13.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight). The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 1.0 kg REHY-zeolite, 8.5 kg by weight of ZRP-zeolite, and 0.5 kg β -zeolite) was added. 5 kg TiCl₄ was added and the mixture was stirred uniformly. The resultant slurry was spray dried and washed to remove free Na ions, yielding catalyst B after being dried. The pore

distribution is shown in Table 1.

Example 3

20 kg deionized water was mixed with 11.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight). The mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and slurried for 5 min, and then added with 15.0 kg water glass (product of Catalyst Plant, Qilu Petrochemicals Co. with an SiO_2 content of 19.9% by weight). The mixture was slurried for 15 min and adjusted to a pH value of 3 with hydrochloric acid, added with 3kg potassium sulfate, and slurried for 15min. The above two slurries were mixed and stirred uniformly, and then the mixture was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4. Then the temperature was decreased to 55°C and 13.5 kg alumina sol was added (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al_2O_3 content of 21.7% by weight). The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 1.0 kg REHY-zeolite, 8.5 kg by weight of ZRP-zeolite, and 0.5 kg β -zeolite) was added. 5kg TiCl_4 was added and the mixture was stirred uniformly. The slurry was spray dried and molded, and washed to remove free Na ions, yielding catalyst C after being dried. The pore distribution is shown in Table 1.

Example 4

20 kg deionized water was mixed with 11.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight). The mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and slurried for 5 min, and then added with 1.75 kg boric acid (analytically pure), the mixture being slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixed slurry was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4 (adjusted with hydrochloric acid). Then

the temperature was decreased to 60°C and added with 13.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight). The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 2.0 kg REHY-zeolite and 9.0 kg ZRP-zeolite) was added. The resultant slurry was spray dried and washed to remove free Na ions, yielding catalyst D after being dried. The pore distribution is shown in Table 1.

Example 5

20 kg deionized water was mixed with 9.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight). The mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and slurried for 5 min, and then added with 4.01 kg potassium borate (analytically pure). The mixture was slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixture was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4. Then the temperature was decreased to 55°C and 13.5 kg alumina sol was added (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight). The mixture was stirred for 40 min and 18.7 kg molecular sieve slurry (containing 1.0 kg REHY-zeolite, 5.2 kg by weight of ZRP-zeolite) was added. 4kg TiCl₄ was added and the mixture was stirred uniformly. The slurry was spray dried and molded, and washed to remove free Na ions, yielding catalyst E after being dried. The pore distribution is shown in Table 1.

Example 6

20 kg deionized water was mixed with 14.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight) and the mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and the mixture was slurried for 5

min. Then 1.6 kg potassium sulfate (industrially pure, 98%) was added, and the mixture was slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixture was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4. Then the temperature was decreased to 55°C and 13.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight) was added. The mixture was stirred for 40 min and 45.1 kg molecular sieve slurry (containing 1.5 kg REHY-zeolite, 11.3 kg of ZRP-zeolite, and 1 kg β-zeolite) was added. 3 kg TiCl₄ was added and the mixture was stirred uniformly. The slurry was spray dried and molded and washed to remove free Na ions, yielding catalyst F after being dried. The pore distribution is shown in Table 1.

Example 7

20 kg deionized water was mixed with 14.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight) and the mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg deionized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and the mixture was slurried for 5 min. Then 2.6 kg potassium sulfate (industrially pure, 98%) was added, and the mixture was slurried for 15 min. The above two slurries were mixed and stirred uniformly, and then the mixture was standing at 65°C for 1.5 h for aging, with the pH value being maintained at 2-4. Then the temperature was decreased to 55°C and 15.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with an Al₂O₃ content of 21.7% by weight) was added. The mixture was stirred for 40 min and 22.1 kg molecular sieve slurry (containing 0.5 kg REHY-zeolite, 6.3 kg of ZRP-zeolite, and 1.5 kg β-zeolite) was added. 3 kg TiCl₄ was added and the mixture was stirred uniformly. The slurry was spray dried and molded and washed to remove free Na ions, yielding catalyst G after being dried. The pore distribution is shown in Table 1.

Comparative Example 1

A catalyst was prepared according to the process for preparing the

DCC industrial catalyst (the process in CN1048428C).

92.6 kg decationized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and the mixture was slurried. Then 15.9 kg pseudo-boehmite was added and the pH value of the mixture was adjusted to 3 with hydrochloric acid, the mixture being stirred uniformly. Then the mixture was standing at 65 °C for aging for 1 h, and its pH value was maintained at 2-4. The temperature was decreased to 55 °C and 13.5 kg alumina sol was added. The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 1.0 kg by weight of REHY-zeolite and 9.0 kg by weight of ZRP-zeolite) was added. The mixture was slurried, spray dried, and molded, and washed to remove free Na ions, yielding comparative catalyst DB-1 after being dried. The pore distribution is shown in Table 1.

Comparative Example 2

20 kg decationized water was mixed with 11.9 kg pseudo-boehmite (industrial product of Shandong Aluminum Plant with a solid content of 63% by weight) and the mixture was slurried and adjusted to a pH value of 3 with hydrochloric acid. 72.6 kg decationized water was mixed with 38.7 kg halloysite (industrial product of Suzhou Porcelain Clay Co. with a solid content of 72.3% by weight) and the mixture was slurried for 5 min. The above two slurries were mixed and stirred uniformly, and standing at 65 °C for 1.5 h for aging, with the pH value being maintained at 2-4. The temperature was then decreased to 55 °C and 13.5 kg alumina sol (product of Catalyst Plant, Qilu Petrochemicals Co. with a Al_2O_3 content of 21.7% by weight) was added. The mixture was stirred for 40 min and 32.1 kg molecular sieve slurry (containing 1.0 kg by weight of REHY-zeolite, 8.5 kg by weight of ZRP-zeolite, and 0.5 kg β -zeolite) was added. 5 kg TiCl_4 was added, and the mixture was slurried uniformly. The resultant slurry was spray dried and molded, and washed to remove free Na ions, yielding catalyst sample DB-2 after being dried.

The abrasion indices, pore volumes and crystallinity of Catalysts A-G and DB-1, DB-2 are shown in Table 2.

Examples 8-9

Catalyst samples A-B were evaluated on a small fixed fluidized bed apparatus with 30 m.% of residual oil + 70 m.% of wax oil (its properties are shown in Table 3) as a feed stock under a reaction temperature of 680°C, a catalyst/oil weight ratio of 10, a water/oil mass ratio of 0.8:1, and a weight hourly space velocity of 10 h⁻¹. The catalyst was pre-treated with 100% steam at 800°C for 17 h and the load of the catalyst was 180 g. The evaluation results are shown in Table 4.

Comparative Example 3

Catalyst DB-1 was evaluated according to the method in Example 8. The evaluation results are shown in Table 4.

Table 1

Example No.	1	2	3	4	5	6	7	Comparative Example 1	Comparative Example 2
Catalyst No.	A	B	C	D	E	F	G	DB-1	DB-2
<2nm	21	20	23	21	13	35	15	22	18
2-4nm	17	20	16	25	10	35	37	70	74
4-6nm	5	3	3	2	1	7	1	3	2
6-20nm	47	42	52	45	75	20	20	4.5	5
6-10nm	25	22	27	20	15	15	16	3	3
20-100nm	10	15	6	7	1	3	27	0.5	1
6-20nm/2-4nm	2.76	2.10	3.25	1.80	7.50	0.57	0.54	0.064	0.068

Table 2

Example No.	Comparative Example 1	Comparative Example 2	1	2	3	4	5	6	7
Catalyst No.	DB-1	DB-2	A	B	C	D	E	F	G

AI, %	2.0	1.0	1.5	2.0	1.9	2.9	1.0	1.9	2.7
V _{BET} , ml/g	0.185	0.190	0.238	0.256	0.247	0.240	0.236	0.241	0.257
ACR, % (Crystal structure of fresh catalyst)	15.6	15.4	16.6	16.3	16.4	16.1	16.6	16.2	15.3
ACR, % (800°C/17h deactivated)	11.4	11.2	13.8	13.3	13.5	13.4	13.2	13.5	11.9

Table 3

Density (20°C), g/cm ³		0.9006
Kinematic viscosity (100°C), mm ² /s		11.0
Conradson Carbon residue, wt%		3.14
Element composition, wt%	C	85.7
	H	12.8
	N	0.38
	S	0.77
Family composition (hydrocarbon species), wt%	Saturated HCs	57.5
	Aromatics	24.5
	Gum	16.9
	Asphaltene	1.1
Metal content, ppm	Ni	5.0
	V	0.8
Boiling range, °C	IBP	-
	5%	217
	40%	396
	70%	456
Characterization factor		12.0

Table 4

Example No.	Comparative Example 3	8	9
Catalyst No.	DB-1	A	B
Dry gas, wt %	3.86	4.41	4.07
Hydrogen, wt %	0.06	0.08	0.05
Methane, wt %	0.42	0.46	0.40
Ethane, wt %	0.31	0.33	0.28
Ethylene, wt %	3.06	3.54	3.59
LPG, wt %	43.67	45.24	48.34
Propane, wt %	2.04	2.22	2.10
Propylene, wt %	19.26	21.08	21.88
n-Butane, wt %	1.19	1.15	1.23
Iso-butane, wt %	5.55	5.34	5.45
Butene-1, wt %	2.74	2.76	3.07
Iso-butene, wt %	6.45	6.5	7.40
cis-butene-2, wt %	2.71	2.57	3.06
trans-butene-2, wt %	3.74	3.62	4.15
Gasoline, wt %	43.34	40.55	40.36
Diesel oil, wt %	6.29	7.1	5.21
Heavy oil, wt %	1.55	1.41	1.05
Coke, wt %	1.28	1.27	1.09
Conversion wt %	92.14	91.47	93.74

Claims

1. A catalyst for catalytically cracking hydrocarbon oils, which catalyst contains a substrate comprising alumina and a molecular sieve, characterized in that the pore distribution of said catalyst is 5-70% of the <2 nm pores, 5-70% of the 2-4 nm pores, 0-10% of the 4-6 nm pores, 20-80% of the 6-20 nm pores, and 0-40% of the 20-100 nm pores, based on the pore volume of pores having a size of no more than 100 nm, the pore volume of the catalyst is measured according to RIPP151-90, said catalyst contains 60-95 wt.% of a substrate, 5-40 wt.% of a molecular sieve, and said molecular sieve contains 25-100 wt.% of MFI-structured zeolite, 0-75 wt.% of Y-zeolite, and 0-20 wt.% of β -zeolite, and

 said alumina is derived from alumina and/or its precursors,

 said precursor of alumina is pseudo-boehmite or its mixture with one or more of alumina sol or phospho-alumina sol.

2. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that the ratio of the volume of 6-20 nm pores to that of 2-4 nm pores is 0.5-4.

3. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that the volume of the 6-10 nm pores accounts for 10-50%.

4. The catalyst for catalytically cracking hydrocarbon oils according to claim 3, characterized in that the volume of the 6-10 nm pores accounts for 15-40%.

5. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that the volume of the <2 nm pores in said catalyst accounts for 5-60%.

6. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that the volume of the 2-4 nm pores in said catalyst accounts for 10-60%.

7. The catalyst for catalytically cracking hydrocarbon oils according to claim 6, characterized in that the volume of the 2-4 nm pores in said catalyst accounts for 15-50%.

8. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that the volume of the 6-20 nm pores in said catalyst accounts for 25-70%.

9. The catalyst for catalytically cracking hydrocarbon oils according to claim 8, characterized in that the volume of the 6-20 nm pores in said catalyst accounts for 30-60%.

10. The catalyst for catalytically cracking hydrocarbon oils according to claim 1, characterized in that said substrate further contains one or more of oxides of non-aluminum elements of Groups IIIA and IVA and their precursors, and clay.

11. The catalyst for catalytically cracking hydrocarbon oils according to claim 10, characterized in that said substrate contains one or more of clay, silica sol, water glass, or silica-alumina gel.

12. The catalyst according to claim 1, characterized in that the pore volume of said catalyst measured by the BET method is 0.19-0.4 ml/g.

13. The catalyst according to claim 12, characterized in that the pore volume of said catalyst measured by the BET method is 0.19-0.26 ml/g.

14. A process for preparing catalytic cracking catalysts according to claim 1, which process comprises the steps of mixing a substrate comprising alumina and/or its precursors with a molecular sieve, slurring and spray-drying the mixture, characterized in that a pore-extender is introduced in the mixing step and said pore-extender is one or more of boric acid, a borate, a phosphate, a sulfate, a nitrate, a carbonate, or a chloride of K, Na, or lithium, the weight ratio of the pore-extender to the substrate being 0.1:100-15:100 based on the weight of the substrate, wherein said precursor of alumina is pseudo-boehmite or its mixture with one or more of alumina sol or phospho-alumina sol.

15. The process according to claim 14, characterized in that one or more of halides of Groups IIA, IB, IIB, and IVB metals are introduced in said step of mixing the substrate and molecular sieve, and the amount of said introduced metal halide does not exceed 15% by weight based on the weight of substrate.

16. The process according to claim 15, characterized in that said metal halide is one or more of halides of Groups IVB and IIA metals.

17. The process according to claim 16, characterized in that said metal halide is a halide of Ti and/or Mg.
18. The process according to claim 14, characterized in that phosphoric acid is also introduced in the step of mixing.
19. A catalytic cracking process, which comprises a step of contacting a hydrocarbon oil with a catalyst, characterized in that said catalyst comprises a catalyst according to any one of claims 1-14.

Figure 1

